

2-Propanol, 2-methyl-

Other names:	1,1-Dimethylethanol
	2-METHYL-2-PROPANOL
	2-Methyl n-propan-2-ol
	2-Methylpropan-2-ol
	2-Methylpropanol-2
	Alcool butylique tertiaire
	Butanol tertiaire
	Ethanol, 1,1-Dimethyl-
	Methanol, trimethyl-
	Methyl-2 propanol-2
	NCI-C55367
	TERT-BUTANOL
	TERT-BUTYL ALCOHOL
	TRIMETHYLMETHANOL
	Tert.-butyl alcohol
	Trimethylcarbinol
	t-Butanol
	t-Butyl hydroxide
	tert-Butyl hydroxide
	tert-C4H9OH
Inchi:	InChI=1S/C4H10O/c1-4(2,3)5/h5H,1-3H3
InchiKey:	DKGAVHZHDRPRBM-UHFFFAOYSA-N
Formula:	C4H10O
SMILES:	CC(C)(C)O
Mol. weight [g/mol]:	74.12
CAS:	75-65-0

Physical Properties

Property code	Value	Unit	Source
af	0.6120		KDB
affp	802.60	kJ/mol	NIST Webbook
aigt	753.15	K	KDB
basg	772.20	kJ/mol	NIST Webbook
chl	-2644.00 ± 0.79	kJ/mol	NIST Webbook
chs	-2633.00	kJ/mol	NIST Webbook
dm	1.70	debye	KDB
fil	2.35	% in Air	KDB

flu	8.00	% in Air	KDB
fpc	289.26	K	KDB
fpo	284.26	K	KDB
gf	-178.80	kJ/mol	KDB
gyrad	3.0190		KDB
hf	-309.70	kJ/mol	NIST Webbook
hf	-312.60 ± 0.88	kJ/mol	NIST Webbook
hf	-313.00 ± 1.50	kJ/mol	NIST Webbook
hf	-312.80	kJ/mol	KDB
hfl	-359.20 ± 0.84	kJ/mol	NIST Webbook
hfl	-356.00	kJ/mol	NIST Webbook
hfl	-359.30 ± 0.79	kJ/mol	NIST Webbook
hfus	2.79	kJ/mol	Joback Method
hsub	41.00	kJ/mol	NIST Webbook
hvap	39.88	kJ/mol	Joback Method
ie	10.23	eV	NIST Webbook
ie	10.23	eV	NIST Webbook
ie	10.25 ± 0.03	eV	NIST Webbook
ie	9.97 ± 0.02	eV	NIST Webbook
ie	10.25	eV	NIST Webbook
ie	9.90 ± 0.03	eV	NIST Webbook
ie	9.90 ± 0.03	eV	NIST Webbook
ie	10.26	eV	NIST Webbook
log10ws	-0.87		Crippen Method
logp	0.777		Crippen Method
mcvol	73.090	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=1)		KDB
pc	3972.00	kPa	KDB
pc	3970.00 ± 20.00	kPa	NIST Webbook
pc	3972.00	kPa	NIST Webbook
pc	4232.00	kPa	NIST Webbook
rhoc	257.94	kg/m3	NIST Webbook
rhoc	270.02	kg/m3	NIST Webbook
rhoc	269.80 ± 1.48	kg/m3	NIST Webbook
rinpol	472.00		NIST Webbook
rinpol	512.00		NIST Webbook
rinpol	509.00		NIST Webbook
rinpol	519.00		NIST Webbook
rinpol	512.00		NIST Webbook
rinpol	500.00		NIST Webbook
rinpol	530.00		NIST Webbook
rinpol	500.00		NIST Webbook
rinpol	507.30		NIST Webbook

rinpol	519.00	NIST Webbook
rinpol	534.00	NIST Webbook
rinpol	531.00	NIST Webbook
rinpol	518.00	NIST Webbook
rinpol	526.30	NIST Webbook
rinpol	523.50	NIST Webbook
rinpol	488.00	NIST Webbook
rinpol	472.00	NIST Webbook
rinpol	493.00	NIST Webbook
rinpol	514.00	NIST Webbook
rinpol	527.00	NIST Webbook
rinpol	524.00	NIST Webbook
rinpol	493.00	NIST Webbook
rinpol	478.10	NIST Webbook
rinpol	488.00	NIST Webbook
rinpol	472.00	NIST Webbook
rinpol	488.00	NIST Webbook
rinpol	487.00	NIST Webbook
rinpol	491.00	NIST Webbook
rinpol	521.00	NIST Webbook
rinpol	493.00	NIST Webbook
rinpol	515.00	NIST Webbook
rinpol	500.00	NIST Webbook
rinpol	500.00	NIST Webbook
rinpol	500.00	NIST Webbook
rinpol	471.00	NIST Webbook
rinpol	472.10	NIST Webbook
rinpol	512.00	NIST Webbook
rinpol	509.00	NIST Webbook
rinpol	512.00	NIST Webbook
rinpol	518.00	NIST Webbook
rinpol	543.00	NIST Webbook
rinpol	512.00	NIST Webbook
rinpol	530.00	NIST Webbook
rinpol	512.00	NIST Webbook
rinpol	543.00	NIST Webbook
rinpol	471.00	NIST Webbook
rinpol	472.10	NIST Webbook
rinpol	488.00	NIST Webbook
rinpol	524.00	NIST Webbook
rinpol	514.00	NIST Webbook
rinpol	515.00	NIST Webbook
ripol	900.00	NIST Webbook
ripol	875.00	NIST Webbook

ripol	914.00		NIST Webbook
ripol	879.00		NIST Webbook
ripol	891.00		NIST Webbook
ripol	902.00		NIST Webbook
ripol	875.00		NIST Webbook
ripol	897.00		NIST Webbook
ripol	875.00		NIST Webbook
ripol	882.00		NIST Webbook
ripol	934.00		NIST Webbook
ripol	863.00		NIST Webbook
ripol	871.00		NIST Webbook
ripol	880.00		NIST Webbook
ripol	906.00		NIST Webbook
ripol	867.00		NIST Webbook
ripol	934.00		NIST Webbook
ripol	942.00		NIST Webbook
ripol	930.00		NIST Webbook
ripol	942.00		NIST Webbook
ripol	930.00		NIST Webbook
ripol	897.00		NIST Webbook
ripol	920.00		NIST Webbook
ripol	871.00		NIST Webbook
ripol	916.00		NIST Webbook
ripol	881.00		NIST Webbook
ripol	897.00		NIST Webbook
sl	189.50	J/mol×K	NIST Webbook
sl	197.50	J/mol×K	NIST Webbook
ss	170.87	J/mol×K	NIST Webbook
tb	355.47 ± 0.10	K	NIST Webbook
tb	355.60 ± 0.10	K	NIST Webbook
tb	355.56 ± 0.10	K	NIST Webbook
tb	355.75 ± 0.50	K	NIST Webbook
tb	355.15 ± 1.00	K	NIST Webbook
tb	355.25 ± 1.00	K	NIST Webbook
tb	355.15 ± 1.00	K	NIST Webbook
tb	354.65 ± 1.00	K	NIST Webbook
tb	355.75 ± 0.30	K	NIST Webbook
tb	355.95 ± 0.30	K	NIST Webbook
tb	355.15 ± 1.00	K	NIST Webbook
tb	355.95 ± 0.50	K	NIST Webbook
tb	356.15 ± 1.00	K	NIST Webbook
tb	354.65 ± 2.00	K	NIST Webbook
tb	355.65 ± 2.00	K	NIST Webbook
tb	355.65 ± 1.00	K	NIST Webbook

tb	353.65 ± 2.00	K	NIST Webbook
tb	355.40 ± 0.25	K	NIST Webbook
tb	355.50 ± 0.50	K	NIST Webbook
tb	355.55 ± 0.50	K	NIST Webbook
tb	355.70 ± 1.00	K	NIST Webbook
tb	355.95 ± 0.50	K	NIST Webbook
tb	354.61 ± 0.10	K	NIST Webbook
tb	355.60 ± 0.40	K	NIST Webbook
tb	355.47 ± 0.12	K	NIST Webbook
tb	355.65 ± 0.20	K	NIST Webbook
tb	355.60 ± 0.50	K	NIST Webbook
tb	355.70 ± 0.30	K	NIST Webbook
tb	355.70 ± 0.30	K	NIST Webbook
tb	355.40 ± 0.50	K	NIST Webbook
tb	355.45 ± 0.40	K	NIST Webbook
tb	355.70 ± 0.40	K	NIST Webbook
tb	375.50 ± 0.30	K	NIST Webbook
tb	355.50	K	NIST Webbook
tb	355.55 ± 0.30	K	NIST Webbook
tb	355.65 ± 0.25	K	NIST Webbook
tb	355.55 ± 0.25	K	NIST Webbook
tb	355.00	K	NIST Webbook
tb	355.50	K	NIST Webbook
tb	355.55 ± 0.30	K	NIST Webbook
tb	355.60 ± 0.10	K	NIST Webbook
tb	355.60 ± 0.30	K	NIST Webbook
tb	355.30 ± 0.40	K	NIST Webbook
tb	355.60 ± 0.30	K	NIST Webbook
tb	355.60 ± 0.30	K	NIST Webbook
tb	355.85 ± 0.50	K	NIST Webbook
tb	355.56	K	Isobaric Vapor Liquid Equilibrium of tert-Butyl Alcohol + Water + Triethanolamine-Based Ionic Liquid Ternary Systems at 101.3 kPa
tb	355.58	K	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
tb	355.51	K	Isobaric Vapor Liquid Equilibrium for the Binary Systems of sec-Butyl Acetate + n-Butyl Alcohol, Isobutyl Alcohol, or tert-Butyl Alcohol at 101.3 kPa
tb	355.65 ± 1.00	K	NIST Webbook

tb	357.65 ± 2.00	K	NIST Webbook
tb	355.80	K	Isobaric vapour-liquid equilibrium of (tert-butanol + water) system with biological buffer TRIS at 101.3 kPa
tb	356.00 ± 1.00	K	NIST Webbook
tb	355.55	K	Measurement and correlation of binary vapor liquid equilibria of isomeric butanols with 1,4-dioxane
tb	355.33	K	Isobaric vapor liquid equilibrium for ternary mixtures of ethanol and methylcyclohexane with 3-methylpentane and tert-butyl alcohol at 101.3 kPa
tb	355.50	K	KDB
tb	354.15 ± 3.00	K	NIST Webbook
tb	354.65 ± 1.00	K	NIST Webbook
tb	355.65 ± 2.00	K	NIST Webbook
tb	355.65 ± 0.10	K	NIST Webbook
tb	355.75 ± 0.50	K	NIST Webbook
tb	355.85 ± 0.50	K	NIST Webbook
tb	355.37 ± 0.20	K	NIST Webbook
tb	355.75 ± 0.30	K	NIST Webbook
tb	355.59	K	Isobaric Vapor-Liquid Equilibrium for Binary and Ternary Systems of tert-Butanol + tert-Butyl Acetate + Chlorobenzene at 101.33 kPa
tb	325.70 ± 0.25	K	NIST Webbook
tb	355.70 ± 0.20	K	NIST Webbook
tb	356.01 ± 0.20	K	NIST Webbook
tb	355.15 ± 0.50	K	NIST Webbook
tb	355.40 ± 0.30	K	NIST Webbook
tb	355.55 ± 0.50	K	NIST Webbook
tb	354.90 ± 1.00	K	NIST Webbook
tb	356.09 ± 0.50	K	NIST Webbook
tb	356.20 ± 1.00	K	NIST Webbook
tb	355.72 ± 0.30	K	NIST Webbook
tb	355.75 ± 0.50	K	NIST Webbook
tb	355.35 ± 0.30	K	NIST Webbook
tb	355.10 ± 0.50	K	NIST Webbook
tc	506.20	K	KDB
tc	506.35	K	Experimental study of the isochoric heat capacity of tert-butanol in the critical and supercritical regions

tc	508.10	K	NIST Webbook
tc	508.90	K	NIST Webbook
tc	506.20	K	NIST Webbook
tc	506.20	K	NIST Webbook
tc	506.20 ± 0.30	K	NIST Webbook
tf	298.50	K	KDB
tf	297.99	K	Solubility of Benzimidazoles in Alcohols
tf	298.70	K	Solid liquid equilibria of mixtures containing tert-butanol, m-chlorophenol, and p-chlorophenol and development of adductive crystallization processes
tt	298.96 ± 0.06	K	NIST Webbook
tt	298.50 ± 0.20	K	NIST Webbook
tt	298.97 ± 0.06	K	NIST Webbook
vc	0.275	m ³ /kmol	NIST Webbook
vc	0.275	m ³ /kmol	KDB
zc	0.2595270		KDB
zra	0.26		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	137.95	J/mol×K	383.15	NIST Webbook
cpg	145.10 ± 1.10	J/mol×K	410.85	NIST Webbook
cpg	136.20 ± 1.10	J/mol×K	372.85	NIST Webbook
cpg	139.20 ± 1.10	J/mol×K	385.65	NIST Webbook
cpg	148.07	J/mol×K	419.15	NIST Webbook
cpg	151.90 ± 1.10	J/mol×K	439.85	NIST Webbook
cpg	153.55	J/mol×K	437.15	NIST Webbook
cpg	133.40 ± 1.10	J/mol×K	360.55	NIST Webbook
cpg	132.63	J/mol×K	365.15	NIST Webbook
cpg	187.30 ± 1.10	J/mol×K	591.55	NIST Webbook
cpg	183.40 ± 1.10	J/mol×K	575.05	NIST Webbook
cpg	172.60 ± 1.10	J/mol×K	528.75	NIST Webbook
cpg	165.70 ± 1.10	J/mol×K	499.25	NIST Webbook
cpg	159.10 ± 1.10	J/mol×K	470.75	NIST Webbook
cpg	152.20 ± 1.10	J/mol×K	441.45	NIST Webbook
cpg	142.88	J/mol×K	401.15	NIST Webbook
cpl	224.70	J/mol×K	300.00	NIST Webbook

cpl	224.90	J/mol×K	298.15	NIST Webbook
cpl	210.00	J/mol×K	298.15	NIST Webbook
cpl	210.00	J/mol×K	298.00	NIST Webbook
cpl	221.88	J/mol×K	299.15	NIST Webbook
cpl	215.37	J/mol×K	298.15	NIST Webbook
cpl	218.60	J/mol×K	298.15	NIST Webbook
cps	146.11	J/mol×K	298.15	NIST Webbook
dvisc	0.0044360	Pa×s	298.15	Densities, Viscosities, and Excess Molar Enthalpies of 2-Pyrrolidone + Butanol Isomers at T) (293.15, 298.15, and 303.15) K
dvisc	0.0026110	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of 1-Bromobutane with Butanol Isomers at Several Temperatures
dvisc	0.0016850	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of 1-Chlorobutane with Butanol Isomers at Several Temperatures
dvisc	0.0020740	Pa×s	313.15	Densities and Viscosities of Binary Mixtures of 1-Chlorobutane with Butanol Isomers at Several Temperatures
dvisc	0.0026110	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of 1-Chlorobutane with Butanol Isomers at Several Temperatures
dvisc	0.0033550	Pa×s	303.15	Densities and Viscosities of Binary Mixtures of 1-Chlorobutane with Butanol Isomers at Several Temperatures

dvisc	0.0044330	Pa×s	298.15	Densities and Viscosities of Binary Mixtures of 1-Chlorobutane with Butanol Isomers at Several Temperatures
dvisc	0.0044330	Pa×s	298.15	Densities and Viscosities of Binary Mixtures of 1-Bromobutane with Butanol Isomers at Several Temperatures
dvisc	0.0020740	Pa×s	313.15	Densities and Viscosities of Binary Mixtures of 1-Bromobutane with Butanol Isomers at Several Temperatures
dvisc	0.0016850	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of 1-Bromobutane with Butanol Isomers at Several Temperatures
dvisc	0.0033780	Pa×s	303.15	Densities, Viscosities, and Excess Molar Enthalpies of 2-Pyrrolidone + Butanol Isomers at T) (293.15, 298.15, and 303.15) K
dvisc	0.0054860	Pa×s	293.15	Densities, Viscosities, and Excess Molar Enthalpies of 2-Pyrrolidone + Butanol Isomers at T) (293.15, 298.15, and 303.15) K
dvisc	0.0007603	Pa×s	343.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K

dvisc	0.0017369	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0008734	Pa×s	338.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0010160	Pa×s	333.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0011964	Pa×s	328.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0026905	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0021423	Pa×s	313.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0033550	Pa×s	303.15	Densities and Viscosities of Binary Mixtures of 1-Bromobutane with Butanol Isomers at Several Temperatures

dvisc	0.0014284	Paxs	323.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
hfust	6.70	kJ/mol	299.00	NIST Webbook
hfust	6.70	kJ/mol	299.00	NIST Webbook
hfust	6.78	kJ/mol	298.50	NIST Webbook
hfust	0.49	kJ/mol	294.50	NIST Webbook
hfust	0.83	kJ/mol	286.10	NIST Webbook
hsubt	51.30	kJ/mol	275.50	NIST Webbook
hvapt	41.00 ± 0.10	kJ/mol	343.00	NIST Webbook
hvapt	39.04	kJ/mol	355.90	KDB
hvapt	42.50 ± 0.10	kJ/mol	330.00	NIST Webbook
hvapt	39.00 ± 0.10	kJ/mol	356.00	NIST Webbook
hvapt	40.40 ± 0.10	kJ/mol	346.00	NIST Webbook
hvapt	39.07	kJ/mol	355.50	NIST Webbook
hvapt	42.70	kJ/mol	345.50	NIST Webbook
hvapt	43.40	kJ/mol	340.00	NIST Webbook
hvapt	46.20	kJ/mol	337.00	NIST Webbook
hvapt	41.40	kJ/mol	355.00	NIST Webbook
hvapt	43.20	kJ/mol	418.00	NIST Webbook
hvapt	39.80	kJ/mol	409.00	NIST Webbook
hvapt	33.60	kJ/mol	479.50	NIST Webbook
hvapt	42.60	kJ/mol	346.00	NIST Webbook
hvapt	46.12 ± 0.05	kJ/mol	303.20	NIST Webbook
hvapt	46.20 ± 0.10	kJ/mol	303.00	NIST Webbook
hvapt	44.90 ± 0.10	kJ/mol	313.00	NIST Webbook
hvapt	43.00 ± 0.10	kJ/mol	328.00	NIST Webbook
hvapt	37.20 ± 0.10	kJ/mol	368.00	NIST Webbook
hvapt	44.70	kJ/mol	331.50	NIST Webbook
hvapt	46.50	kJ/mol	334.50	NIST Webbook
hvapt	44.20	kJ/mol	334.00	NIST Webbook
hvapt	38.70	kJ/mol	439.50	NIST Webbook
hvapt	42.10	kJ/mol	348.00	NIST Webbook
hvapt	41.40	kJ/mol	355.00	NIST Webbook
hvapt	41.30 ± 0.10	kJ/mol	340.00	NIST Webbook
hvapt	40.00 ± 0.10	kJ/mol	349.00	NIST Webbook
hvapt	44.70	kJ/mol	328.00	NIST Webbook

kvisc	0.0000056	m2/s	298.15	Viscosities of Binary Mixtures of Isomeric Butanols or Isomeric Chlorobutanes with 2-Methyltetrahydrofuran
kvisc	0.0000027	m2/s	313.15	Viscosities of Binary Mixtures of Isomeric Butanols or Isomeric Chlorobutanes with 2-Methyltetrahydrofuran
pvap	79.99	kPa	349.23	Isobaric Phase Equilibrium of tert-Butyl Alcohol + Glycerol at Local and Subatmospheric Pressures, Volumetric Properties, and Molar Refractivity from 303.15 to 333.15 K of tert-Butyl Alcohol + Glycerol, tert-Butyl Alcohol + Water, and Water + Glycerol Binary Systems
pvap	142.60	kPa	364.50	Vapour liquid equilibrium for the systems butane + methanol, +2-propanol, +1-butanol, +2-butanol, +2-methyl-2-propanol at 364.5K
pvap	13.77	kPa	313.08	Vapour liquid equilibrium for the 2-methylpropane + methanol, +ethanol, +2-propanol, +2-butanol and +2-methyl-2-propanol systems at 313.15K
pvap	23.80	kPa	323.20	Vapor Liquid Equilibrium for Butane + Methanol, + Ethanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-Propanol (TBA) at 323 K

pvap	143.30	kPa	364.52	Vapor Liquid Equilibrium for the Systems trans-2-Butene + Methanol, + 1-Propanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-propanol at 364.5 K
pvap	142.60	kPa	364.50	Vapor Liquid Equilibrium for the Systems 2-Methylpropane + Methanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-propanol at 364.5 K
pvap	101.30	kPa	355.80	Isobaric vapour-liquid equilibrium of (tert-butanol + water) system with biological buffer TRIS at 101.3 kPa
pvap	40.00	kPa	333.90	Isobaric Vapor-Liquid Equilibria for Tetrahydropyran and Alcohol Systems
pvap	53.33	kPa	340.13	Isobaric Vapor-Liquid Equilibria for Tetrahydropyran and Alcohol Systems
pvap	66.66	kPa	345.21	Isobaric Vapor-Liquid Equilibria for Tetrahydropyran and Alcohol Systems
pvap	79.99	kPa	349.53	Isobaric Vapor-Liquid Equilibria for Tetrahydropyran and Alcohol Systems
pvap	98.66	kPa	354.61	Isobaric Vapor-Liquid Equilibria for Tetrahydropyran and Alcohol Systems

pvap	100.00	kPa	355.20	Isobaric vapor-liquid equilibria for the extractive distillation of tert-butyl alcohol + water mixtures using 1-ethyl-3-methylimidazolium dicyanamide ionic liquid
pvap	66.66	kPa	344.84	Isobaric Phase Equilibrium of tert-Butyl Alcohol + Glycerol at Local and Subatmospheric Pressures, Volumetric Properties, and Molar Refractivity from 303.15 to 333.15 K of tert-Butyl Alcohol + Glycerol, tert-Butyl Alcohol + Water, and Water + Glycerol Binary Systems
pvap	95.99	kPa	353.80	Isobaric Phase Equilibrium of tert-Butyl Alcohol + Glycerol at Local and Subatmospheric Pressures, Volumetric Properties, and Molar Refractivity from 303.15 to 333.15 K of tert-Butyl Alcohol + Glycerol, tert-Butyl Alcohol + Water, and Water + Glycerol Binary Systems
pvap	143.00	kPa	364.52	Vapor-Liquid Equilibrium for the cis-2-Butene + Methanol, + 2-Propanol, + 2-Butanol, + 2-Methyl-2-propanol Systems at 364.5 K
pvap	101.33	kPa	355.59	Isobaric Vapor-Liquid Equilibrium for Binary and Ternary Systems of tert-Butanol + tert-Butyl Acetate + Chlorobenzene at 101.33 kPa

pvap	38.60	kPa	333.15	Isothermal Vapor-Liquid Equilibria for Binary Mixtures Composed of the Closely Boiling Compounds 1,2-Dimethoxybenzene and 2-Methoxyphenol with an Adducted Agent: tert-Butanol or Morpholine
pvap	60.80	kPa	343.15	Isothermal Vapor-Liquid Equilibria for Binary Mixtures Composed of the Closely Boiling Compounds 1,2-Dimethoxybenzene and 2-Methoxyphenol with an Adducted Agent: tert-Butanol or Morpholine
pvap	92.40	kPa	353.15	Isothermal Vapor-Liquid Equilibria for Binary Mixtures Composed of the Closely Boiling Compounds 1,2-Dimethoxybenzene and 2-Methoxyphenol with an Adducted Agent: tert-Butanol or Morpholine
pvap	36.97	kPa	332.06	Vapor Liquid Equilibrium for the Trans-2-Butene + Methanol, + Ethanol, + 2-Propanol, + 2-Butanol and + 2-Methyl-2-Propanol Systems at 332 K
pvap	23.07	kPa	322.78	Isothermal Vapor Liquid Equilibrium for Binary 2-Methylpropene - C1-C4 Alcohol-Systems

pvap	8.96	kPa	305.87	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	11.51	kPa	310.08	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	38.57	kPa	333.15	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	13.72	kPa	313.14	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	16.11	kPa	316.04	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	19.43	kPa	319.50	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	23.28	kPa	322.94	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene

pvap	27.62	kPa	326.30	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	32.74	kPa	329.74	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	101.00	kPa	355.56	Isobaric Vapor Liquid Equilibrium of tert-Butyl Alcohol + Water + Triethanolamine-Based Ionic Liquid Ternary Systems at 101.3 kPa
pvap	44.94	kPa	336.41	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	52.29	kPa	339.74	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	61.09	kPa	343.25	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	70.27	kPa	346.50	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene

pvap	80.85	kPa	349.84	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	92.53	kPa	353.15	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	100.91	kPa	355.31	Vapor-Liquid Equilibrium for Benzaldehyde with 1-Methylethylbenzene and for 2-Methyl-propan-2-ol with 2,4,4-Trimethyl-1-pentene
pvap	192.46	kPa	373.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	818.16	kPa	423.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	191.18	kPa	373.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	816.37	kPa	423.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation

pvap	142.70	kPa	364.52	Isothermal Vapor Liquid Equilibrium for 2-Methylpropene + Methanol, + 1-Propanol, + 2-Propanol, + 2-Butanol, and + 2-Methyl-2-propanol Binary Systems at 364.5 K
pvap	93.32	kPa	353.32	Isobaric Vapor-Liquid Equilibria for Tetrahydropyran and Alcohol Systems
rfi	1.37667		313.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.38510		298.15	Isobaric (vapour + liquid) equilibrium for N-methyl-2-pyrrolidone with branched alcohols
rfi	1.38520		298.15	Excess Gibbs free energies of the binary mixtures of acetonitrile with butanols at 94.83 kPa
rfi	1.38520		298.15	(Vapor + liquid) equilibria of the binary mixtures of m-cresol with C1 C4 aliphatic alcohols at 95.5 kPa
rfi	1.38520		298.15	(Vapor + liquid) equilibria of binary mixtures formed by iso-octane with a variety of compounds at 95.8 kPa

rfi	1.38810	293.15	Liquid-liquid equilibrium for the ternary system water + 2-methyl-1-propanol + butyl acetate and water + 2-methyl-2-propanol + butyl acetate at (298.15 and 323.15) K
rfi	1.38510	298.15	Volumetric behavior of carbon dioxide + 2-methyl-1-propanol and carbondioxide + 2-methyl-2-propanol mixtures at 313.15 K
rfi	1.38510	298.15	Excess volumes and excess enthalpies of N-methyl-2-pyrrolidone with branched alcohols
rfi	1.38520	298.15	Excess Gibbs energies of selected binary mixtures formed by N,N-dimethyl formamide at 95.5 kPa
rfi	1.38520	298.15	Activity coefficients of the binary mixtures of a-cresol or p-cresol with C 1-C4 aliphatic alcohols near ambient pressure
rfi	1.37384	318.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.38510	298.15	Isobaric vapor-liquid equilibria for the binary systems isobutyl alcohol + isobutyl acetate and tert-butyl alcohol + tert-butyl acetate at 20 and 101.3 kPa

rfi	1.37097	323.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.38200	303.15	Isobaric Vapor-Liquid Equilibria and Excess Quantities for Binary Mixtures of an Ethyl Ester + tert-Butanol and a New Approach to VLE Data Processing
rfi	1.38870	298.15	Bubble Temperatures of the Binary Mixtures of Dimethylcarbonate with Some Alcohols at 95.8 kPa
rfi	1.38500	298.15	Bubble-Temperature Measurements on Some Binary Mixtures Formed by Tetrahydrofuran or Amyl Alcohol with Hydrocarbons, Chlorohydrocarbons, or Butanols at (94.6 or 95.8) kPa
rfi	1.37410	318.15	Excess Properties and Isobaric Vapor-Liquid Equilibria for Binary Mixtures of Methyl Esters + tert-Butanol
rfi	1.38481	298.15	Densities, Viscosities, and Refractive Indices for Binary and Ternary Mixtures of Ethanol, 2-Methylpropan-2-ol, and 2,2,4-Trimethylpentane

rfi	1.37960	308.15	Densities, Viscosities, and Refractive Indices for Binary and Ternary Mixtures of Ethanol, 2-Methylpropan-2-ol, and 2,2,4-Trimethylpentane
rfi	1.37416	318.15	Densities, Viscosities, and Refractive Indices for Binary and Ternary Mixtures of Ethanol, 2-Methylpropan-2-ol, and 2,2,4-Trimethylpentane
rfi	1.38220	303.15	Correlation and Prediction of Excess Quantities and Vapor-Liquid Equilibria of Alkyl Esters + tert-Butyl Alcohol: Experimental Data for Propyl Esters + tert-Butyl Alcohol
rfi	1.38222	303.15	Experimental Determination of Densities and Refractive Indices of the Ternary Mixture 2-Methyl-2-propanol + Cyclohexylamine + n-Heptane at T = (303.15 to 323.15) K
rfi	1.37947	308.15	Experimental Determination of Densities and Refractive Indices of the Ternary Mixture 2-Methyl-2-propanol + Cyclohexylamine + n-Heptane at T = (303.15 to 323.15) K

rfi	1.37667	313.15	Experimental Determination of Densities and Refractive Indices of the Ternary Mixture 2-Methyl-2-propanol + Cyclohexylamine + n-Heptane at T = (303.15 to 323.15) K
rfi	1.37947	308.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.37097	323.15	Experimental Determination of Densities and Refractive Indices of the Ternary Mixture 2-Methyl-2-propanol + Cyclohexylamine + n-Heptane at T = (303.15 to 323.15) K
rfi	1.38770	293.15	Isobaric Vapor Liquid Equilibrium Data for the Binary Mixtures 2-Methyl Propan-2-ol with Tetraethoxysilane and 1-Phenyl Ethanone at 95.5 kPa
rfi	1.38780	293.15	Isobaric Vapor Liquid Equilibrium Data of 2-Methyl-propan-2-ol (1) + Heptan-1-ol (2), Methanol (1) + Heptan-1-ol (2), Ethanol (1) + Heptan-1-ol (2), and Propan-1-ol (1) + Heptan-1-ol (2) at 96.5 kPa

rfi	1.38520		298.15	Vapor-Liquid Equilibrium and Excess Gibbs Energies of Hexane + N,N-Dimethyl Formamide, 2-Methylpropan-2-ol + 2-Aminophenol, N,N-Dimethyl Formamide, and 2-Propanol + Diisopropyl Amine at 94.4 kPa
rfi	1.37384		318.15	Experimental Determination of Densities and Refractive Indices of the Ternary Mixture 2-Methyl-2-propanol + Cyclohexylamine + n-Heptane at T = (303.15 to 323.15) K
rfi	1.38222		303.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rhoI	764.95	kg/m3	313.15	Measurement and modeling of volumetric properties and speeds of sound of several mixtures of alcohol liquids containing 1-propanol and 2-propanol at T= (298.15 - 323.15) K and ambient pressure
rhoI	779.48	kg/m3	299.15	Densities and volume properties of (water + tert-butanol) over the temperature range of (274.15 to 348.15) K at pressure of 0.1 MPa

rhoI	781.20	kg/m3	298.15	Bubble point temperatures of the binary mixtures of nitrobenzene with C1 C4 aliphatic alcohols at 94.95 kPa
rhoI	781.00	kg/m3	298.15	(Vapour + liquid) equilibrium of binary mixtures (1,3-dioxolane or 1,4-dioxane + 2-methyl-1-propanol or 2-methyl-2-propanol) at isobaric conditions
rhoI	754.01	kg/m3	323.15	Excess specific volume of water + tert-butyl alcohol solvent mixtures: Experimental data, modeling and derived excess partial specific thermodynamic quantities.
rhoI	759.47	kg/m3	318.15	Excess specific volume of water + tert-butyl alcohol solvent mixtures: Experimental data, modeling and derived excess partial specific thermodynamic quantities.
rhoI	764.86	kg/m3	313.15	Excess specific volume of water + tert-butyl alcohol solvent mixtures: Experimental data, modeling and derived excess partial specific thermodynamic quantities.

rho1	770.17	kg/m3	308.15	Excess specific volume of water + tert-butyl alcohol solvent mixtures: Experimental data, modeling and derived excess partial specific thermodynamic quantities.
rho1	775.38	kg/m3	303.15	Excess specific volume of water + tert-butyl alcohol solvent mixtures: Experimental data, modeling and derived excess partial specific thermodynamic quantities.
rho1	779.48	kg/m3	299.15	Excess specific volume of water + tert-butyl alcohol solvent mixtures: Experimental data, modeling and derived excess partial specific thermodynamic quantities.
rho1	754.10	kg/m3	323.15	Measurement and modeling of volumetric properties and speeds of sound of several mixtures of alcohol liquids containing 1-propanol and 2-propanol at T= (298.15 - 323.15) K and ambient pressure
rho1	759.56	kg/m3	318.15	Measurement and modeling of volumetric properties and speeds of sound of several mixtures of alcohol liquids containing 1-propanol and 2-propanol at T= (298.15 - 323.15) K and ambient pressure

rhoI	775.39	kg/m3	303.15	Densities and volume properties of (water + tert-butanol) over the temperature range of (274.15 to 348.15) K at pressure of 0.1 MPa
rhoI	770.25	kg/m3	308.15	Measurement and modeling of volumetric properties and speeds of sound of several mixtures of alcohol liquids containing 1-propanol and 2-propanol at T=(298.15 - 323.15) K and ambient pressure
rhoI	775.46	kg/m3	303.15	Measurement and modeling of volumetric properties and speeds of sound of several mixtures of alcohol liquids containing 1-propanol and 2-propanol at T=(298.15 - 323.15) K and ambient pressure
rhoI	780.57	kg/m3	298.15	Measurement and modeling of volumetric properties and speeds of sound of several mixtures of alcohol liquids containing 1-propanol and 2-propanol at T=(298.15 - 323.15) K and ambient pressure
rhoI	781.04	kg/m3	298.15	Vapor-liquid equilibria of binary systems composed of polyoxyethylene 4-octylphenyl ether and alcohols: Experimental measurements and correlation

rhoI	754.01	kg/m3	323.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules
rhoI	759.49	kg/m3	318.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules
rhoI	764.88	kg/m3	313.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules
rhoI	770.19	kg/m3	308.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules
rhoI	775.41	kg/m3	303.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules

rhoI	775.10	kg/m3	303.15	Viscous synergy and antagonism and isentropic compressibility of ternary mixtures containing 1,3-dioxolane, water and monoalkanols at 303.15K
rhoI	760.13	kg/m3	318.15	Densities and Volumetric Properties of Binary Mixtures of Aniline with 1-Propanol, 2-Propanol, 2-Methyl-1-Propanol, and 2-Methyl-2-Propanol at Temperatures from 293.15 to 318.15 K
rhoI	770.15	kg/m3	308.15	Densities and volume properties of (water + tert-butanol) over the temperature range of (274.15 to 348.15) K at pressure of 0.1 MPa
rhoI	765.26	kg/m3	313.15	Densities and Volumetric Properties of Binary Mixtures of Aniline with 1-Propanol, 2-Propanol, 2-Methyl-1-Propanol, and 2-Methyl-2-Propanol at Temperatures from 293.15 to 318.15 K
rhoI	764.84	kg/m3	313.15	Densities and volume properties of (water + tert-butanol) over the temperature range of (274.15 to 348.15) K at pressure of 0.1 MPa

rhoI	759.46	kg/m3	318.15	Densities and volume properties of (water + tert-butanol) over the temperature range of (274.15 to 348.15) K at pressure of 0.1 MPa
rhoI	775.51	kg/m3	303.15	Densities and Volumetric Properties of Binary Mixtures of Aniline with 1-Propanol, 2-Propanol, 2-Methyl-1-Propanol, and 2-Methyl-2-Propanol at Temperatures from 293.15 to 318.15 K
rhoI	742.70	kg/m3	333.15	Densities and volume properties of (water + tert-butanol) over the temperature range of (274.15 to 348.15) K at pressure of 0.1 MPa
rhoI	731.31	kg/m3	343.15	Densities and Viscosities of Binary Mixtures of 2-Butanol + Isobutanol, 2-Butanol + tert-Butanol, and Isobutanol + tert-Butanol from (308.15 to 343.15) K
rhoI	725.06	kg/m3	348.15	Densities and volume properties of (water + tert-butanol) over the temperature range of (274.15 to 348.15) K at pressure of 0.1 MPa
rhoI	780.61	kg/m3	298.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa

rhoI	775.42	kg/m3	303.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa
rhoI	770.21	kg/m3	308.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa
rhoI	764.92	kg/m3	313.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa
rhoI	759.42	kg/m3	318.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa
rhoI	753.95	kg/m3	323.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa
rhoI	780.72	kg/m3	298.15	Experimental and theoretical excess molar properties of imidazolium based ionic liquids with isomers of butanol
rhoI	770.21	kg/m3	308.15	Experimental and theoretical excess molar properties of imidazolium based ionic liquids with isomers of butanol

rhoI	759.50	kg/m3	318.15	Experimental and theoretical excess molar properties of imidazolium based ionic liquids with isomers of butanol
rhoI	780.86	kg/m3	298.15	Liquid Liquid Equilibria, Equilibrium Phase Densities, and Refractive Indices for the Quaternary Mixtures Containing 2-Propanol or 2-Methyl-2-Propanol of Fuel Oxygenate at T = 298.15 and 318.15 K
rhoI	780.85	kg/m3	298.15	Excess Molar Volumes and Surface Tensions of 1,2,4-Trimethylbenzene and 1,3,5-Trimethylbenzene with 1-Butanol, 2-Methyl-1-propanol, 2-Butanol, and 2-Methyl-2-propanol at 298.15 K
rhoI	780.78	kg/m3	298.15	Surface Tensions of the Ternary Mixtures Containing an Isomeric Butanol + n-Hexane + 1-Chlorobutane at 298.15 K
rhoI	770.36	kg/m3	308.15	Densities and Viscosities of Binary Mixtures of 2-Butanol + Isobutanol, 2-Butanol + tert-Butanol, and Isobutanol + tert-Butanol from (308.15 to 343.15) K

rhoI	759.67	kg/m3	318.15	Densities and Viscosities of Binary Mixtures of 2-Butanol + Isobutanol, 2-Butanol + tert-Butanol, and Isobutanol + tert-Butanol from (308.15 to 343.15) K
rhoI	754.19	kg/m3	323.15	Densities and Viscosities of Binary Mixtures of 2-Butanol + Isobutanol, 2-Butanol + tert-Butanol, and Isobutanol + tert-Butanol from (308.15 to 343.15) K
rhoI	748.62	kg/m3	328.15	Densities and Viscosities of Binary Mixtures of 2-Butanol + Isobutanol, 2-Butanol + tert-Butanol, and Isobutanol + tert-Butanol from (308.15 to 343.15) K
rhoI	742.95	kg/m3	333.15	Densities and Viscosities of Binary Mixtures of 2-Butanol + Isobutanol, 2-Butanol + tert-Butanol, and Isobutanol + tert-Butanol from (308.15 to 343.15) K
rhoI	737.19	kg/m3	338.15	Densities and Viscosities of Binary Mixtures of 2-Butanol + Isobutanol, 2-Butanol + tert-Butanol, and Isobutanol + tert-Butanol from (308.15 to 343.15) K
rhoI	780.78	kg/m3	298.15	Densities and Viscosities of the Ternary Mixtures 2-Methyl-1-propanol (or 2-Methyl-2-propanol) + N-Hexane + 1-Chlorobutane at 298.15 K

rhoI	780.44	kg/m3	298.15	Isothermal Vapor-Liquid Equilibria in the Two Binary and the Ternary Systems Composed of tert-Amyl Methyl Ether, tert-Butanol, and Isooctane	
rhoI	780.63	kg/m3	298.15	Densities and Volumetric Properties of Binary Mixtures of Aniline with 1-Propanol, 2-Propanol, 2-Methyl-1-Propanol, and 2-Methyl-2-Propanol at Temperatures from 293.15 to 318.15 K	
rhoI	785.75	kg/m3	293.15	Densities and Volumetric Properties of Binary Mixtures of Aniline with 1-Propanol, 2-Propanol, 2-Methyl-1-Propanol, and 2-Methyl-2-Propanol at Temperatures from 293.15 to 318.15 K	
rhoI	770.39	kg/m3	308.15	Densities and Volumetric Properties of Binary Mixtures of Aniline with 1-Propanol, 2-Propanol, 2-Methyl-1-Propanol, and 2-Methyl-2-Propanol at Temperatures from 293.15 to 318.15 K	
rhoI	787.00	kg/m3	293.00	KDB	
rhoI	765.07	kg/m3	313.15	Densities and Viscosities of Binary Mixtures of 2-Butanol + Isobutanol, 2-Butanol + tert-Butanol, and Isobutanol + tert-Butanol from (308.15 to 343.15) K	

rhoI	753.94	kg/m3	323.15	Densities and volume properties of (water + tert-butanol) over the temperature range of (274.15 to 348.15) K at pressure of 0.1 MPa
sfust	22.42	J/mol×K	299.00	NIST Webbook
sfust	2.90	J/mol×K	286.10	NIST Webbook
sfust	1.66	J/mol×K	294.50	NIST Webbook
sfust	22.72	J/mol×K	298.50	NIST Webbook
speedsl	1055.36	m/s	313.15	Temperature influence on mixing properties of {ethyl tert-butyl ether (ETBE) + gasoline additives}
speedsl	1098.21	m/s	303.15	Temperature influence on mixing properties of {ethyl tert-butyl ether (ETBE) + gasoline additives}
speedsl	1057.40	m/s	313.15	Densities and speeds of sound for binary mixtures of (1,3-dioxolane or 1,4-dioxane) with (2-methyl-1-propanol or 2-methyl-2-propanol) at the temperatures 298.15 K and 313.15 K
speedsl	1122.80	m/s	298.15	Densities and speeds of sound for binary mixtures of (1,3-dioxolane or 1,4-dioxane) with (2-methyl-1-propanol or 2-methyl-2-propanol) at the temperatures 298.15 K and 313.15 K
speedsl	1014.76	m/s	323.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives

speedsl	1025.17	m/s	320.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1013.01	m/s	323.15	Temperature influence on mixing properties of {ethyl tert-butyl ether (ETBE) + gasoline additives}	
speedsl	1046.12	m/s	315.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1056.73	m/s	313.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1067.22	m/s	310.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1077.71	m/s	308.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1088.33	m/s	305.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1099.02	m/s	303.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	

speedsl	1101.90	m/s	303.15	Excess Enthalpy, Density, and Speed of Sound for the Mixtures α -Pinene + 2-Methyl-1-propanol or 2-Methyl-2-propanol at Several Temperatures	
speedsl	1056.40	m/s	313.15	Excess Enthalpy, Density, and Speed of Sound for the Mixtures α -Pinene + 2-Methyl-1-propanol or 2-Methyl-2-propanol at Several Temperatures	
speedsl	1035.66	m/s	318.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1015.90	m/s	323.15	Excess Enthalpy, Density, and Speed of Sound for the Mixtures α -Pinene + 2-Methyl-1-propanol or 2-Methyl-2-propanol at Several Temperatures	
speedsl	1108.98	m/s	301.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
srf	0.02	N/m	328.15	Equilibrium surface tension and the interaction energy of DMSO with tert-butyl alcohol or iso-amyl alcohol at various temperatures	

srf	0.02	N/m	318.15	Equilibrium surface tension and the interaction energy of DMSO with tert-butyl alcohol or iso-amyl alcohol at various temperatures
srf	0.02	N/m	308.15	Equilibrium surface tension and the interaction energy of DMSO with tert-butyl alcohol or iso-amyl alcohol at various temperatures
srf	0.02	N/m	298.15	Equilibrium surface tension and the interaction energy of DMSO with tert-butyl alcohol or iso-amyl alcohol at various temperatures
srf	0.02	N/m	318.20	KDB

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.44210e+01
Coeff. B	-2.46322e+03
Coeff. C	-1.04219e+02
Temperature range (K), min.	278.50
Temperature range (K), max.	374.62

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C \cdot \ln(T) + D \cdot T^2$
Coeff. A	9.13446e+01
Coeff. B	-8.70216e+03
Coeff. C	-1.06233e+01

Coeff. D	1.15210e-06
Temperature range (K), min.	293.00
Temperature range (K), max.	506.20

Datasets

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
303.15	101.33	0.0033870
Reference		https://www.doi.org/10.1016/j.fluid.2010.10.009

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
308.15	101.30	770.14
323.15	101.30	753.94
323.15	10000.00	764.58
323.15	25000.00	778.73
323.15	50000.00	798.2
323.15	75000.00	813.79
323.15	100000.00	827.34
Reference		https://www.doi.org/10.1016/j.jct.2012.09.026

Temperature, K	Pressure, kPa	Mass density, kg/m3
308.15	97.00	770.2
348.15	98.00	725.1
303.15	99.00	775.3
313.15	99.00	764.8
323.15	99.00	753.9
343.15	99.00	731.0
353.15	99.00	719.0
318.15	100.00	759.4

338.15	100.00	737.1
328.15	101.00	748.4
333.15	103.00	742.8
358.15	103.00	712.8
358.15	293.00	713.1
348.15	295.00	725.3
313.15	298.00	765.0
318.15	298.00	759.6
323.15	298.00	754.1
328.15	298.00	748.7
303.15	298.00	775.5
308.15	298.00	770.4
363.15	299.00	706.4
353.15	300.00	719.3
343.15	305.00	731.3
333.15	307.00	743.1
338.15	309.00	737.3
318.15	498.00	759.8
348.15	498.00	725.7
358.15	498.00	713.4
328.15	499.00	748.9
303.15	499.00	775.7
308.15	500.00	770.6
353.15	501.00	719.6
313.15	502.00	765.2
323.15	502.00	754.4
333.15	502.00	743.3
363.15	502.00	706.8
343.15	503.00	731.6
338.15	505.00	737.6
308.15	897.00	771.0
353.15	897.00	720.2
328.15	898.00	749.4
338.15	898.00	738.1
348.15	898.00	726.2
303.15	898.00	776.1
358.15	899.00	714.0
318.15	901.00	760.3
323.15	901.00	754.9
343.15	901.00	732.1
363.15	901.00	707.4
313.15	904.00	765.7
333.15	915.00	743.8
353.15	1000.00	720.3

303.15	1002.00	776.2
308.15	1002.00	771.1
343.15	1002.00	732.2
363.15	1002.00	707.6
338.15	1003.00	738.2
358.15	1003.00	714.2
323.15	1004.00	755.0
348.15	1004.00	726.4
328.15	1005.00	749.5
318.15	1006.00	760.4
333.15	1007.00	744.0
313.15	1009.00	765.8
343.15	2000.00	733.6
353.15	2000.00	721.8
328.15	2001.00	750.7
338.15	2001.00	739.5
318.15	2001.00	761.5
363.15	2001.00	709.2
323.15	2003.00	756.1
348.15	2006.00	727.8
303.15	2007.00	777.1
358.15	2008.00	715.7
308.15	2009.00	772.1
333.15	2013.00	745.2
313.15	2016.00	766.8
353.15	2999.00	723.2
308.15	3000.00	773.1
328.15	3001.00	751.9
343.15	3001.00	734.9
348.15	3001.00	729.2
323.15	3002.00	757.2
318.15	3003.00	762.6
358.15	3003.00	717.3
338.15	3005.00	740.8
363.15	3005.00	710.8
333.15	3006.00	746.4
313.15	3006.00	767.8
303.15	3007.00	778.1
303.15	4999.00	780.0
353.15	4999.00	726.1
328.15	5001.00	754.1
318.15	5002.00	764.7
333.15	5002.00	748.8
363.15	5002.00	713.9

338.15	5003.00	743.2
358.15	5003.00	720.2
323.15	5004.00	759.4
343.15	5005.00	737.5
348.15	5005.00	731.9
308.15	5006.00	775.1
313.15	5010.00	769.9
348.15	6999.00	734.5
353.15	6999.00	728.8
328.15	7001.00	756.3
323.15	7002.00	761.5
303.15	7003.00	781.9
358.15	7003.00	723.0
343.15	7004.00	740.0
333.15	7005.00	751.1
318.15	7005.00	766.7
308.16	7005.00	777.0
313.15	7006.00	771.8
338.15	7014.00	745.6
363.15	7023.00	716.9
303.15	8992.00	783.7
353.15	8998.00	731.4
318.15	8999.00	768.7
333.15	9001.00	753.3
358.15	9001.00	725.8
363.15	9001.00	719.7
323.15	9002.00	763.5
328.15	9004.00	758.5
338.15	9004.00	747.9
313.15	9005.00	773.7
308.15	9006.00	778.8
348.15	9012.00	737.0
343.15	9033.00	742.4
358.15	9998.00	727.1
328.15	9999.00	759.5
333.15	9999.00	754.3
338.15	10002.00	749.0
323.15	10002.00	764.5
318.15	10002.00	769.7
353.15	10003.00	732.6
303.15	10005.00	784.6
313.15	10007.00	774.7
308.15	10007.00	779.7
363.15	10009.00	721.1

348.15	10014.00	738.2
343.15	10020.00	743.6
353.15	11997.00	735.1
338.15	11998.00	751.2
328.15	11999.00	761.6
318.15	11999.00	771.6
303.15	11999.00	786.3
323.15	12000.00	766.5
343.15	12001.00	745.8
333.15	12003.00	756.5
348.15	12003.00	740.6
308.15	12005.00	781.5
313.15	12005.00	776.5
358.15	12010.00	729.7
363.15	12038.00	723.8
363.15	14998.00	727.6
338.15	14999.00	754.4
348.15	14999.00	744.0
323.15	14999.00	769.3
358.15	14999.00	733.3
333.15	15000.00	759.6
353.15	15001.00	738.7
343.15	15002.00	749.1
328.15	15004.00	764.5
313.15	15005.00	779.2
318.15	15010.00	774.4
308.15	15021.00	784.1
333.15	17995.00	762.5
338.15	17997.00	757.5
318.15	17998.00	777.0
323.15	17998.00	772.1
348.15	17999.00	747.3
353.15	17999.00	742.1
363.15	18000.00	731.3
343.15	18001.00	752.3
313.15	18003.00	781.8
328.15	18006.00	767.4
308.16	18006.00	786.6
358.15	18040.00	736.9
328.15	19995.00	769.2
333.15	19997.00	764.4
358.15	19997.00	739.1
308.15	19998.00	788.2
323.15	20000.00	773.9

348.15	20000.00	749.4
353.15	20000.00	744.2
318.15	20006.00	778.8
338.15	20007.00	759.4
313.15	20015.00	783.5
343.15	20018.00	754.4
363.15	20033.00	733.7
343.15	21994.00	756.4
358.15	21995.00	741.3
333.15	21996.00	766.2
348.15	21998.00	751.5
338.15	21999.00	761.4
318.15	21999.00	780.5
353.15	21999.00	746.4
328.15	22000.00	771.0
323.15	22000.00	775.7
313.15	22002.00	785.1
308.15	22003.00	789.8
363.15	22005.00	735.9
308.15	24990.00	792.2
318.15	24994.00	782.9
333.15	24994.00	768.9
328.15	24996.00	773.6
348.15	24996.00	754.4
353.15	24997.00	749.4
338.15	25000.00	764.2
323.15	25000.00	778.2
363.15	25000.00	739.2
313.15	25007.00	787.5
358.15	25017.00	744.5
343.15	25026.00	759.3
343.15	27993.00	762.1
333.15	27993.00	771.6
338.15	27994.00	766.9
358.15	27994.00	747.6
323.15	27995.00	780.7
348.15	27995.00	757.3
328.15	27998.00	776.2
353.15	27999.00	752.5
313.15	28002.00	789.9
318.15	28005.00	785.4
308.15	28006.00	794.5
363.15	28009.00	742.4
358.15	29991.00	749.6

313.15	30000.00	791.4
318.15	30001.00	787.0
323.15	30002.00	782.4
333.15	30003.00	773.3
343.15	30004.00	763.9
353.15	30004.00	754.4
328.15	30005.00	777.9
308.15	30005.00	796.0
338.15	30011.00	768.6
363.15	30011.00	744.4
348.15	30045.00	759.3
343.15	32000.00	765.7
348.15	32000.00	761.0
323.15	32000.00	784.0
318.15	32001.00	788.5
313.16	32001.00	792.9
358.15	32001.00	751.5
353.15	32003.00	756.3
333.15	32004.00	775.0
328.15	32005.00	779.5
338.15	32005.00	770.4
363.15	32033.00	746.5
333.15	32850.00	775.7
333.15	32871.00	775.7
348.15	32878.00	761.8
343.15	32963.00	766.6
363.15	32982.00	747.4
353.15	32985.00	757.1
318.15	32993.00	789.3
358.15	32997.00	752.5
338.15	32998.00	771.2
323.15	33000.00	784.7
343.15	33001.00	766.6
313.15	33001.00	793.7
323.15	33001.00	784.7
353.15	33002.00	757.2
318.15	33002.00	789.3
348.15	33012.00	761.9
313.15	33012.00	793.6
363.15	33012.00	747.4
358.15	33015.00	752.5
328.15	33023.00	780.3
338.15	33033.00	771.2
328.15	33038.00	780.4

333.15	34000.00	776.6
348.15	34000.00	762.8
353.15	34000.00	758.1
323.15	34000.00	785.5
343.15	34002.00	767.5
313.15	34006.00	794.4
338.15	34007.00	772.0
318.15	34010.00	790.0
328.15	34013.00	781.1
363.15	34035.00	748.4
358.15	34056.00	753.5
333.15	34990.00	777.4
363.15	34999.00	749.3
338.15	35000.00	772.9
348.15	35001.00	763.7
318.15	35001.00	790.8
343.15	35003.00	768.3
353.15	35004.00	759.0
328.15	35004.00	781.9
323.15	35004.00	786.2
313.15	35008.00	795.1
358.15	35075.00	754.4
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363.15	37998.00	752.1
318.15	38000.00	793.0
323.15	38000.00	788.5
348.15	38001.00	766.3
328.15	38002.00	784.3
333.15	38004.00	779.8
313.15	38012.00	797.2
343.15	38027.00	770.8
338.15	38031.00	775.3
363.16	38458.00	752.5
353.15	38477.00	762.2
363.15	39147.00	753.2
333.15	39997.00	781.4
343.15	39998.00	772.5
323.15	39998.00	790.0
348.15	39999.00	768.0
358.15	40001.00	758.8
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353.15	40002.00	763.4
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318.15	40010.00	794.4

338.15	40024.00	776.9
328.15	40024.00	785.8
348.15	41997.00	769.6
323.15	41998.00	791.5
338.15	41998.00	778.5
333.15	41998.00	782.9
363.15	41998.00	755.7
328.15	41999.00	787.2
343.15	42000.00	774.1
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313.15	42007.00	800.0
318.15	42021.00	795.9
353.15	42035.00	765.1
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338.15	44574.00	780.4
333.15	44909.00	785.1
313.15	44997.00	802.0
348.15	44999.00	772.0
363.15	44999.00	758.4
323.15	45000.00	793.6
358.15	45002.00	763.1
328.15	45002.00	789.4
318.15	45005.00	797.9
353.15	45022.00	767.6
338.15	46152.00	781.6
358.15	47995.00	765.5
323.15	47996.00	795.7
363.15	47996.00	760.9
328.15	47997.00	791.6
318.15	47997.00	799.9
353.15	48092.00	770.1
333.15	48119.00	787.4
338.15	48333.00	783.3
353.15	49989.00	771.5
328.15	49992.00	793.0
318.15	49998.00	801.3
363.15	49998.00	762.5
333.15	50000.00	788.7
323.15	50000.00	797.1
358.15	50001.00	767.0
338.15	50050.00	784.5
328.16	51996.00	794.3
323.15	51998.00	798.4
363.15	52002.00	764.2

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Viscosity of the binary systems
2-methyl-2-propanol with n-alkanes at T
Excess Gibbs free energy, G^E , and
binary mixtures of acetone with ethyl
methyl ketone, 2-butanone, 2-pentanone,
2-methylpropane + methanol, + ethanol,
2-propanol, + 2-methyl-2-propanol
isopentane-2-methyl-2-propanol, + 2-methyl-
2-propanol, containing 2-butoxolane,
+ 2-methyl-2-propanol at 303.15K:
2-methyl-2-propanol + 2-methyl-2-propanol
Alcohols in the presence of disodium
factors of disodium sulphate at $T =$
tert-butyl alcohol solvent mixtures:
Experimental data, modeling and
thermodynamic partial properties
thermodynamic data of water: Ternary
Systems: Measurement and Modeling:

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The Yaws Handbook of Vapor

Pressure:

Solubilities of cinnamic acid esters in binary mixtures of ionic liquids and organic solvents.

Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Diethyl Ether.

Effect of Temperature on Investigation of Ternary Activity Coefficient Liquid Equilibria for Dimethyl Carbonate + 2-Methyl-1-Propanol.

Activity Coefficients of Binary Mixtures based on Limiting Activity Coefficients, Data Using Spanning Organic and Inorganic Liquid Excess and Azeotropic Mixtures.

Properties of Ester-Quaternary Ammonium Salt Systems at Infinite Dilution and the Mutual Diffusion Coefficients of the Binary Systems of Ethyl Acetate + Propyl Acetate and Ethyl Acetate + Methyl Acetate.

Activity Coefficients of Binary Mixtures of Organic Solvents with 1-Butanol: Solubility and Density Data.

Activity Coefficients of Binary Mixtures of Organic Solvents with 1-Butanol: Solubility and Density Data.

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Activity Coefficients of Binary Mixtures of Organic Solvents with 1-Butanol: Solubility and Density Data.

Activity Coefficients of Binary Mixtures of Organic Solvents with 1-Butanol: Solubility and Density Data.

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af:	Acentric Factor
affp:	Proton affinity
aigt:	Autoignition Temperature
basg:	Gas basicity
chl:	Standard liquid enthalpy of combustion
chs:	Standard solid enthalpy of combustion
cpg:	Ideal gas heat capacity

cpl:	Liquid phase heat capacity
cps:	Solid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
fill:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpc:	Flash Point (Closed Cup Method)
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hsub:	Enthalpy of sublimation at standard conditions
hsubt:	Enthalpy of sublimation at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
kvisc:	Kinematic viscosity
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhof:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
ss:	Solid phase molar entropy at standard conditions
tb:	Normal Boiling Point Temperature
tc:	Critical Temperature
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility

zra:

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