Benzene

Other names: 1,3,5-Cyclohexatriene

Benzeen
Benzen
Benzin
Benzine
Benzol
Benzole
Benzolene
Benzolo

Bicarburet of hydrogen

Carbon oil
Coal naphtha
Cyclohexatriene

Fenzen

Mineral naphtha Motor benzol NCI-C55276 NSC 67315 Phene

Phenyl hydride Pyrobenzol Pyrobenzole

Rcra waste number U019

UN 1114 [6]Annulene

Inchi: InChl=1S/C6H6/c1-2-4-6-5-3-1/h1-6H InchiKey: UHOVQNZJYSORNB-UHFFFAOYSA-N

Formula: C6H6

SMILES: c1ccccc1

Mol. weight [g/mol]: 78.11

CAS: 71-43-2

Physical Properties

Property code	Value	Unit	Source
af	0.2120		KDB
affp	750.40	kJ/mol	NIST Webbook

affp	746.40	kJ/mol	NIST Webbook
aigt	864.82	Komoi	KDB
basg	721.70	kJ/mol	NIST Webbook
basg	725.40	kJ/mol	NIST Webbook
dm	0.00	debye	KDB
dvisc	0.0006080	Paxs	Densities and Viscosities of Binary Liquid Mixtures of Trichloroethylene and Tetrachloroethylene with Some Polar and Nonpolar Solvents
dvisc	0.0006040	Paxs	Densities and Viscosities for the Ternary Systems of Methyl tert-Butyl Ether + Methanol + Benzene and Methyl tert-Butyl Ether + Methanol + Toluene and Their Sub-binary Systems at 298.15 K
fII	1.30	% in Air	KDB
flu	7.90	% in Air	KDB
fpo	262.04	K	KDB
gf	129.70	kJ/mol	KDB
gyrad	3.0040		KDB
hcg	3267.62	kJ/mol	KDB
hcn	3135.573	kJ/mol	KDB
hf	82.98	kJ/mol	KDB
hf	82.90 ± 0.90	kJ/mol	NIST Webbook
hf	82.80	kJ/mol	NIST Webbook
hf	82.93 ± 0.50	kJ/mol	NIST Webbook
hf	79.90	kJ/mol	NIST Webbook
hfl	46.00	kJ/mol	NIST Webbook
hfl	49.04 ± 0.50	kJ/mol	NIST Webbook
hfl	48.95 ± 0.54	kJ/mol	NIST Webbook
hfl	49.00 ± 0.90	kJ/mol	NIST Webbook
hfus	5.73	kJ/mol	Joback Method
hsub	44.40	kJ/mol	NIST Webbook
hvap	30.56	kJ/mol	Joback Method
ie	9.24	eV	NIST Webbook
ie	9.25	eV	NIST Webbook
ie	9.23	eV	NIST Webbook
ie	9.24 ± 0.01	eV	NIST Webbook
ie	9.80 ± 0.10	eV	NIST Webbook
ie	9.25 ± 0.01	eV	NIST Webbook
ie	9.25 ± 0.00	eV	NIST Webbook
ie	9.25	eV	NIST Webbook
ie	9.20	eV	NIST Webbook
ie	9.25	eV	NIST Webbook

ie	9.25	eV	NIST Webbook
ie	9.22	eV	NIST Webbook
ie	9.23	eV	NIST Webbook
ie	9.24	eV	NIST Webbook
ie	9.24	eV	NIST Webbook
ie	9.20	eV	NIST Webbook
ie	9.30	eV	NIST Webbook
ie	9.25 ± 0.03	eV	NIST Webbook
ie	9.24	eV	NIST Webbook
ie	9.24	eV	NIST Webbook
ie	9.23	eV	NIST Webbook
ie	9.24	eV	NIST Webbook
ie	9.24 ± 0.01	eV	NIST Webbook
ie	9.24 ± 0.02	eV	NIST Webbook
ie	9.25 ± 0.05	eV	NIST Webbook
ie	9.24 ± 0.00	eV	NIST Webbook
ie	9.24 ± 0.00	eV	NIST Webbook
ie	9.24 ± 0.00	eV	NIST Webbook
ie	9.20	eV	NIST Webbook
ie	9.23 ± 0.03	eV	NIST Webbook
ie	9.25	eV	NIST Webbook
ie	9.23	eV	NIST Webbook
ie	9.25	eV	NIST Webbook
ie	9.24 ± 0.00	eV	NIST Webbook
ie	9.44	eV	NIST Webbook
ie	9.25	eV	NIST Webbook
ie	9.22	eV	NIST Webbook
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ie	9.25 ± 0.02	eV	NIST Webbook
ie	9.24	eV	NIST Webbook
ie	9.24	eV	NIST Webbook
ie	9.70	eV	NIST Webbook
ie	9.25	eV	NIST Webbook
ie	9.20 ± 0.10	eV	NIST Webbook
ie	9.26 ± 0.06	eV	NIST Webbook
ie	9.27	eV	NIST Webbook
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ie	9.20 ± 0.04	eV	NIST Webbook

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ie	9.26 ± 0.02	eV	NIST Webbook
ie	9.25 ± 0.01	eV	NIST Webbook
ie	9.24 ± 0.01	eV	NIST Webbook
ie	9.25 ± 0.00	eV	NIST Webbook
log10ws	-1.64		Aqueous Solubility Prediction Method
log10ws	-1.64		Estimated Solubility Method
logp	1.687		Crippen Method
mcvol	71.640	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=2)		KDB
рс	4900.00 ± 10.13	kPa	NIST Webbook
рс	4897.00 ± 10.00	kPa	NIST Webbook
рс	4887.00 ± 3.00	kPa	NIST Webbook
рс	4889.00 ± 3.00	kPa	NIST Webbook
рс	4900.00 ± 50.66	kPa	NIST Webbook
рс	4885.89 ± 5.06	kPa	NIST Webbook
рс	4885.89 ± 4.05	kPa	NIST Webbook
рс	4898.00 ± 2.00	kPa	NIST Webbook
рс	4898.00 ± 5.00	kPa	NIST Webbook
рс	4896.00 ± 10.34	kPa	NIST Webbook
рс	4875.75 ± 30.00	kPa	NIST Webbook
рс	4892.00 ± 8.10	kPa	NIST Webbook
рс	4936.65 ± 55.15	kPa	NIST Webbook
рс	4853.47 ± 50.66	kPa	NIST Webbook
рс	4898.00 ± 10.13	kPa	NIST Webbook
рс	4875.00 ± 27.58	kPa	NIST Webbook
рс	4852.30 ± 53.33	kPa	NIST Webbook
pc	4894.00 ± 10.00	kPa	NIST Webbook
pc	4900.00 ± 10.00	kPa	NIST Webbook
рс	5020.00 ± 101.33	kPa	NIST Webbook
pc	4910.00 ± 4.90	kPa	NIST Webbook
pc	4852.27 ± 39.99	kPa	NIST Webbook
рс	6120.00 ± 709.28	kPa	NIST Webbook
рс	4884.00 ± 20.00	kPa	NIST Webbook
рс	4895.00 ± 6.00	kPa	NIST Webbook
pc	4930.90 ± 40.00	kPa	NIST Webbook
pc	4895.00	kPa	KDB
•		kg/m3	NIST Webbook
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rhoc	306.20 ± 2.34	kg/m3	NIST Webbook
rhoc	316.35 ± 4.69	kg/m3	NIST Webbook
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rhoc	300.73 ± 6.25	kg/m3	NIST Webbook
rhoc	304.40 ± 3.91	kg/m3	NIST Webbook
rhoc	303.78 ± 3.91	kg/m3	NIST Webbook
rhoc	304.64 ± 0.47	kg/m3	NIST Webbook
rhoc	296.98 ± 7.81	kg/m3	NIST Webbook
rhoc	304.48 ± 3.91	kg/m3	NIST Webbook
rhoc	302.29 ± 6.25	kg/m3	NIST Webbook
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rinpol	654.00	NIST Webbook
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rinpol	657.00	NIST Webbook
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rinpol	644.00	NIST Webbook
rinpol	650.40	NIST Webbook
rinpol	663.00	NIST Webbook
Пірог	000.00	THE TWO DOOR

ا م موند	024.00	NIST Webbook
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rinpol	644.00	NIST Webbook
rinpol	665.00	NIST Webbook
rinpol	666.00	NIST Webbook
rinpol	669.00	NIST Webbook
rinpol	653.00	NIST Webbook
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	tf	267.65 ± 1.50	K	NIST Webbook

tf	278.66	K	Aqueous Solubility Prediction Method
tf	278.45 ± 0.40	K	NIST Webbook
tf	277.00 ± 2.00	K	NIST Webbook
tf	278.58 ± 0.05	K	NIST Webbook
tf	278.55 ± 0.10	K	NIST Webbook
tf	278.63 ± 0.07	K	NIST Webbook
tf	278.63 ± 0.30	K	NIST Webbook
tf	278.63 ± 0.10	K	NIST Webbook
tf	278.25 ± 0.30	K	NIST Webbook
tf	278.60 ± 0.80	K	NIST Webbook
tf	278.58 ± 0.25	K	NIST Webbook
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tf	278.60 ± 0.25	K	NIST Webbook
tf	278.70 ± 0.40	K	NIST Webbook
tf	278.55 ± 0.20	K	NIST Webbook
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tf	278.70 ± 1.00	K	NIST Webbook
tf	278.70 ± 0.60	K	NIST Webbook
tf	278.66 ± 0.02	K	NIST Webbook
tf	279.10 ± 1.00	K	NIST Webbook
tf	278.60 ± 0.03	K	NIST Webbook
VC	0.256	m3/kmol	KDB
vols	0.00	m3/kg	PVT Relationships of Binary Mixtures of Indole with 2-Methylnaphthalene and Biphenyl at 333.15 K and Pressures up to 270 MPa
ZC	0.2681520		KDB
zra	0.27		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	139.47 ± 0.08	J/mol×K	500.15	NIST Webbook
cpg	123.39	J/mol×K	436.15	NIST Webbook
cpg	123.93 ± 0.07	J/mol×K	438.15	NIST Webbook

cpg	132.42	J/mol×K	471.10	NIST Webbook	
cpg	132.94 ± 0.08	J/mol×K	473.15	NIST Webbook	
cpg	131.40 ± 1.30	J/mol×K	481.00	NIST Webbook	
cpg	145.59 ± 0.09	J/mol×K	527.15	NIST Webbook	
cpg	115.48	J/mol×K	410.00	NIST Webbook	
cpg	114.29 ± 0.07	J/mol×K	403.15	NIST Webbook	
cpg	113.93	J/mol×K	402.30	NIST Webbook	
cpg	117.60 ± 1.30	J/mol×K	417.00	NIST Webbook	
cpg	110.50 ± 1.30	J/mol×K	393.00	NIST Webbook	
cpg	110.88	J/mol×K	390.00	NIST Webbook	
cpg	126.80 ± 1.30	J/mol×K	463.00	NIST Webbook	
cpg	108.80 ± 1.30	J/mol×K	388.00	NIST Webbook	
cpg	104.77	J/mol×K	371.20	NIST Webbook	
cpg	105.02	J/mol×K	370.00	NIST Webbook	
cpg	103.98 ± 0.06	J/mol×K	368.15	NIST Webbook	
cpg	97.99 ± 0.06	J/mol×K	348.15	NIST Webbook	
cpg	95.81	J/mol×K	341.60	NIST Webbook	
cpg	118.80 ± 1.30	J/mol×K	428.00	NIST Webbook	
cpg	93.32 ± 0.06	J/mol×K	333.15	NIST Webbook	
cpl	130.00	J/mol×K	298.00	NIST Webbook	
cpl	134.61	J/mol×K	293.15	NIST Webbook	
cpl	135.75	J/mol×K	298.15	NIST Webbook	
cpl	134.63	J/mol×K	298.15	NIST Webbook	
cpl	135.62	J/mol×K	298.15	NIST Webbook	
cpl	135.90	J/mol×K	298.50	NIST Webbook	
cpl	135.69	J/mol×K	298.15	NIST Webbook	
cpl	145.80	J/mol×K	335.15	Measurement of heat capacities of ionic liquids by differential scanning calorimetry	
cpl	144.15	J/mol×K	330.15	Measurement of heat capacities of ionic liquids by differential scanning calorimetry	
cpl	142.50	J/mol×K	325.15	Measurement of heat capacities of ionic liquids by differential scanning calorimetry	
cpl	140.85	J/mol×K	320.15	Measurement of heat capacities of ionic liquids by differential scanning calorimetry	

	cpl	139.20	J/mol×K	315.15	Measurement of heat capacities of ionic liquids by differential scanning calorimetry	
	cpl	137.90	J/mol×K	310.15	Measurement of heat capacities of ionic liquids by differential scanning calorimetry	
	cpl	136.50	J/mol×K	305.15	Measurement of heat capacities of ionic liquids by differential scanning calorimetry	
	cpl	135.40	J/mol×K	300.15	Measurement of heat capacities of ionic liquids by differential scanning calorimetry	
	cpl	134.80	J/mol×K	295.15	Measurement of heat capacities of ionic liquids by differential scanning calorimetry	
	cpl	135.71	J/mol×K	298.15	NIST Webbook	
	cpl	136.62	J/mol×K	303.15 1-E	Excess Heat Capacities of Binary and Ternary Mixtures Containing thyl-3-methylimidazolium Tetrafluoroborate and Anilines	
	cpl	135.32	J/mol×K	298.15 1-E	Excess Heat Capacities of Binary and Ternary Mixtures Containing thyl-3-methylimidazolium Tetrafluoroborate and Anilines	
	cpl	133.63	J/mol×K	293.15 1-E	Excess Heat Capacities of Binary and Ternary Mixtures Containing thyl-3-methylimidazolium Tetrafluoroborate and Anilines	
	cpl	139.90	J/mol×K	322.05	NIST Webbook	
	cpl	137.40	J/mol×K	303.15	NIST Webbook	
	cpl	134.60	J/mol×K	293.00	NIST Webbook	
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cpl	136.40	J/mol×K	303.00	NIST Webbook	
cpl	135.23	J/mol×K	298.00	NIST Webbook	
cpl	31.80	J/mol×K	293.00	NIST Webbook	_
cpl	136.06	J/mol×K	298.15	NIST Webbook	
cpl	119.00	J/mol×K	295.00	NIST Webbook	
cpl	133.50	J/mol×K	298.00	NIST Webbook	
cpl	136.00	J/mol×K	298.10	NIST Webbook	
cpl	135.44	J/mol×K	298.20	NIST Webbook	
cpl	131.40	J/mol×K	287.80	NIST Webbook	
cpl	131.40	J/mol×K	287.80	NIST Webbook	
cpl	131.40	J/mol×K	298.15	NIST Webbook	
cpl	135.10	J/mol×K	298.10	NIST Webbook	
cpl	143.57	J/mol×K	323.15	NIST Webbook	
cpl	135.10	J/mol×K	300.00	NIST Webbook	
cpl	149.30	J/mol×K	345.15	Measurement of heat capacities of ionic liquids by differential scanning calorimetry	
cpl	132.20	J/mol×K	298.00	NIST Webbook	
cpl	133.10	J/mol×K	293.20	NIST Webbook	
cpl	133.90	J/mol×K	303.00	NIST Webbook	
cpl	137.20	J/mol×K	298.00	NIST Webbook	
cpl	133.50	J/mol×K	298.00	NIST Webbook	
cpl	136.06	J/mol×K	298.15	NIST Webbook	
cpl	135.10	J/mol×K	316.00	NIST Webbook	
cpl	135.72	J/mol×K	298.15	NIST Webbook	
cpl	136.24	J/mol×K	298.15	NIST Webbook	
cpl	136.50	J/mol×K	300.00	NIST Webbook	
cpl	135.70	J/mol×K	298.15	NIST Webbook	
cpl	135.74	J/mol×K	298.15	NIST Webbook	
cpl	135.60	J/mol×K	298.15	NIST Webbook	
cpl	133.60	J/mol×K	293.15	NIST Webbook	
cpl	135.61	J/mol×K	298.15	NIST Webbook	
cpl	135.90	J/mol×K	298.15	NIST Webbook	
cpl	135.60	J/mol×K	298.15	NIST Webbook	
cpl	135.76	J/mol×K	298.15	NIST Webbook	
cpl	135.76	J/mol×K	298.15	NIST Webbook	
cpl	135.70	J/mol×K	298.15	NIST Webbook	
cpl	134.30	J/mol×K	298.00	NIST Webbook	
cpl	151.20	J/mol×K	350.15	Measurement of heat capacities of ionic liquids by differential scanning calorimetry	
cpl	135.90	J/mol×K	298.15	NIST Webbook	

cpl	135.90	J/mol×K	298.00	NIST Webbook	
cpl	135.90	J/mol×K	298.15	NIST Webbook	
cpl	147.55	J/mol×K	340.15	Measurement of heat capacities of ionic liquids by differential scanning calorimetry	
cpl	135.40	J/mol×K	298.00	NIST Webbook	
cps	47.86	J/mol×K	90.00	NIST Webbook	
cps	118.40	J/mol×K	273.00	NIST Webbook	
cps	97.90	J/mol×K	223.90	NIST Webbook	
dvisc	0.0003932	Paxs	333.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K	
dvisc	0.0005272	Pa×s	308.15	Viscometric and Volumetric Properties of 10 Regular Binary Systems at 308.15 K and 313.15 K	
dvisc	0.0004942	Pa×s	313.15	Viscometric and Volumetric Properties of 10 Regular Binary Systems at 308.15 K and 313.15 K	
dvisc	0.0006025	Pa×s	298.15	Ultrasonic and viscometric study of molecular interactions in binary mixtures of aniline with 1-propanol, 2-propanol, 2-methyl-1-propanol at different temperatures	

dvisc	0.0004670	Paxs	318.15	Ultrasonic and viscometric study of molecular interactions in binary mixtures of aniline with 1-propanol, 2-propanol, 2-methyl-1-propanol and 2-methyl-2-propanol at different temperatures
dvisc	0.0005610	Paxs	303.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure
dvisc	0.0004360	Paxs	323.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure
dvisc	0.0003880	Paxs	333.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure
dvisc	0.0003450	Paxs	343.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure

dvisc	0.0006010	Paxs	298.15	Densities, viscosities, and excess properties of (N-methylmorpholine + cyclohexane, + benzene, and + toluene) at T = (298.15, 303.15, 313.15, 323.15) K
dvisc	0.0005630	Paxs	303.15	Densities, viscosities, and excess properties of (N-methylmorpholine + cyclohexane, + benzene, and + toluene) at T = (298.15, 303.15, 313.15, 323.15) K
dvisc	0.0004940	Paxs	313.15	Densities, viscosities, and excess properties of (N-methylmorpholine + cyclohexane, + benzene, and + toluene) at T = (298.15, 303.15, 313.15, 323.15) K
dvisc	0.0004360	Paxs	323.15	Densities, viscosities, and excess properties of (N-methylmorpholine + cyclohexane, + benzene, and + toluene) at T = (298.15, 303.15, 313.15, 323.15) K
dvisc	0.0006030	Paxs	298.15	Densities, Viscosities, and Thermodynamic Properties of (N,N-Dimethylformamide + Benzene + Chlorobenzene) Ternary Mixtures at (298.15, 303.15, 308.15, and 313.15) K

dvisc	0.0005680	Paxs	303.15	Densities, Viscosities, and Thermodynamic Properties of (N,N-Dimethylformamide + Benzene + Chlorobenzene) Ternary Mixtures at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0004930	Paxs	313.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure
dvisc	0.0005310	Paxs	308.15	Densities, Viscosities, and Thermodynamic Properties of (N,N-Dimethylformamide + Benzene + Chlorobenzene) Ternary Mixtures at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0005000	Paxs	313.15	Densities, Viscosities, and Thermodynamic Properties of (N,N-Dimethylformamide + Benzene + Chlorobenzene) Ternary Mixtures at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0006020	Paxs	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for CmH2m+1(OCH2CH2)nOH (m) 1 or 2 or 4 andn) 1) + Benzene, + Toluene, + (o-, m-, and p-) Xylenes, + Ethylbenzene, and + Cyclohexane

dvisc	0.0005260	Paxs	308.15 Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for CmH2m+1(OCH2CH2)nOH (m) 1 or 2 or 4 andn) 1) + Benzene, + Toluene, + (o-, m-, and p-) Xylenes, + Ethylbenzene, and + Cyclohexane
dvisc	0.0006038	Paxs	298.15 Excess Molar Volumes and Viscosities of Binary Mixtures of Sulfolane with Benzene, Toluene, Ethylbenzene, p-Xylene, o-Xylene, and m-Xylene at 303.15 and 323.15 K and Atmospheric Pressure
dvisc	0.0004362	Paxs	323.15 Excess Molar Volumes and Viscosities of Binary Mixtures of Sulfolane with Benzene, Toluene, Ethylbenzene, p-Xylene, o-Xylene, and m-Xylene at 303.15 and 323.15 K and Atmospheric Pressure
dvisc	0.0007090	Pa×s	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene with Anisole at (288.15, 293.15, 298.15, and 303.15) K

dvisc	0.0006480	Paxs	293.15	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene with Anisole at (288.15, 293.15, 298.15, and 303.15) K	
dvisc	0.0006040	Paxs	298.15	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene with Anisole at (288.15, 293.15, 298.15, and 303.15) K	
dvisc	0.0005710	Paxs	303.15	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene with Anisole at (288.15, 293.15, 298.15, and 303.15) K	
dvisc	0.0006010	Paxs	298.15	Densities and Viscosities of N-Formylmorpholine + Benzene, + Toluene at Different Temperatures and Atmospheric Pressures	
dvisc	0.0005620	Paxs	303.15	Densities and Viscosities of N-Formylmorpholine + Benzene, + Toluene at Different Temperatures and Atmospheric Pressures	

dvisc	0.0004930	Paxs	313.15	Densities and Viscosities of N-Formylmorpholine + Benzene, + Toluene at Different Temperatures and Atmospheric Pressures
dvisc	0.0004360	Paxs	323.15	Densities and Viscosities of N-Formylmorpholine + Benzene, + Toluene at Different Temperatures and Atmospheric Pressures
dvisc	0.0003890	Pa×s	333.15	Densities and Viscosities of N-Formylmorpholine + Benzene, + Toluene at Different Temperatures and Atmospheric Pressures
dvisc	0.0003540	Paxs	343.15	Densities and Viscosities of N-Formylmorpholine + Benzene, + Toluene at Different Temperatures and Atmospheric Pressures
dvisc	0.0005640	Paxs	303.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0005232	Paxs	308.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K

dvisc	0.0005001	Paxs	313.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K	
dvisc	0.0004714	Paxs	318.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K	
dvisc	0.0004397	Paxs	323.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K	
dvisc	0.0004145	Paxs	328.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K	
dvisc	0.0005612	Paxs	303.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Sulfolane with Benzene, Toluene, Ethylbenzene, p-Xylene, o-Xylene, and m-Xylene at 303.15 and 323.15 K and Atmospheric Pressure	

dvisc	0.0006030	Paxs	298.15	Densities and Viscosities of Binary Mixtures of Methyl 4-Chlorobutyrate with Aromatic Hydrocarbons at T) (298.15 to 318.15) K	
dvisc	0.0005330	Paxs	308.15	Densities and Viscosities of Binary Mixtures of Methyl 4-Chlorobutyrate with Aromatic Hydrocarbons at T) (298.15 to 318.15) K	
dvisc	0.0004660	Paxs	318.15	Densities and Viscosities of Binary Mixtures of Methyl 4-Chlorobutyrate with Aromatic Hydrocarbons at T) (298.15 to 318.15) K	
dvisc	0.0005690	Paxs	303.15	Physical Properties of Binary Mixtures of Ethyl Formate with Benzene, Isopropyl Benzene, Isobutyl Benzene, and Butylbenzene at (303.15, 308.15, and 313.15) K	
dvisc	0.0005340	Paxs	308.15	Physical Properties of Binary Mixtures of Ethyl Formate with Benzene, Isopropyl Benzene, Isobutyl Benzene, and Butylbenzene at (303.15, 308.15, and 313.15) K	
dvisc	0.0004970	Pa×s	313.15	Physical Properties of Binary Mixtures of Ethyl Formate with Benzene, Isopropyl Benzene, Isobutyl Benzene, and Butylbenzene at (303.15, 308.15, and 313.15) K	

dvisc	0.0005690	Paxs	303.15	Density and Viscosity of Propyl Formate + Aromatic Hydrocarbons at T = (303.15, 308.15, and 313.15) K
dvisc	0.0005340	Paxs	308.15	Density and Viscosity of Propyl Formate + Aromatic Hydrocarbons at T = (303.15, 308.15, and 313.15) K
dvisc	0.0004970	Paxs	313.15	Density and Viscosity of Propyl Formate + Aromatic Hydrocarbons at T = (303.15, 308.15, and 313.15) K
dvisc	0.0005395	Paxs	308.15	Ultrasonic and viscometric study of molecular interactions in binary mixtures of aniline with 1-propanol, 2-propanol, 2-methyl-1-propanol, and 2-methyl-2-propanol at different
hfust	9 92	k.l/mol	278 65	temperatures
hfust	9.92 9.30	kJ/mol	278.65 279.10	temperatures NIST Webbook
hfust	9.30	kJ/mol	279.10	temperatures NIST Webbook NIST Webbook
hfust hfust	9.30 8.95	kJ/mol kJ/mol	279.10 278.80	temperatures NIST Webbook NIST Webbook NIST Webbook
hfust	9.30	kJ/mol	279.10 278.80 278.60	temperatures NIST Webbook NIST Webbook
hfust hfust hfust	9.30 8.95 9.94	kJ/mol kJ/mol kJ/mol	279.10 278.80	temperatures NIST Webbook NIST Webbook NIST Webbook NIST Webbook
hfust hfust hfust hfust	9.30 8.95 9.94 9.80	kJ/mol kJ/mol kJ/mol	279.10 278.80 278.60 278.60	temperatures NIST Webbook NIST Webbook NIST Webbook NIST Webbook NIST Webbook
hfust hfust hfust hfust hfust	9.30 8.95 9.94 9.80 9.87	kJ/mol kJ/mol kJ/mol kJ/mol	279.10 278.80 278.60 278.60 278.69	temperatures NIST Webbook
hfust hfust hfust hfust hfust hfust	9.30 8.95 9.94 9.80 9.87 9.88	kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol	279.10 278.80 278.60 278.60 278.69 278.55	temperatures NIST Webbook
hfust hfust hfust hfust hfust hfust hfust hfust	9.30 8.95 9.94 9.80 9.87 9.88 10.00	kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol	279.10 278.80 278.60 278.60 278.69 278.55 278.64	temperatures NIST Webbook
hfust	9.30 8.95 9.94 9.80 9.87 9.88 10.00 9.87	kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol	279.10 278.80 278.60 278.60 278.69 278.55 278.64 278.70	temperatures NIST Webbook
hfust hfust hfust hfust hfust hfust hfust hfust hfust hsubt	9.30 8.95 9.94 9.80 9.87 9.88 10.00 9.87 45.60	kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol	279.10 278.80 278.60 278.60 278.69 278.55 278.64 278.70 244.50	temperatures NIST Webbook
hfust hfust hfust hfust hfust hfust hfust hfust hfust hsubt hsubt	9.30 8.95 9.94 9.80 9.87 9.88 10.00 9.87 45.60 49.40 ± 0.40	kJ/mol	279.10 278.80 278.60 278.69 278.55 278.64 278.70 244.50 193.00	temperatures NIST Webbook
hfust hfust hfust hfust hfust hfust hfust hfust hsubt hsubt hsubt	9.30 8.95 9.94 9.80 9.87 9.88 10.00 9.87 45.60 49.40 ± 0.40 43.10	kJ/mol	279.10 278.80 278.60 278.60 278.69 278.55 278.64 278.70 244.50 193.00 229.00	temperatures NIST Webbook
hfust hfust hfust hfust hfust hfust hfust hfust hsubt hsubt hsubt hsubt	9.30 8.95 9.94 9.80 9.87 9.88 10.00 9.87 45.60 49.40 ± 0.40 43.10 45.20	kJ/mol	279.10 278.80 278.60 278.60 278.69 278.55 278.64 278.70 244.50 193.00 229.00 251.00	temperatures NIST Webbook
hfust hfust hfust hfust hfust hfust hfust hfust hfust hsubt hsubt hsubt hsubt hsubt hsubt	9.30 8.95 9.94 9.80 9.87 9.88 10.00 9.87 45.60 49.40 ± 0.40 43.10 45.20 41.70	kJ/mol	279.10 278.80 278.60 278.60 278.69 278.55 278.64 278.70 244.50 193.00 229.00 251.00 265.50	temperatures NIST Webbook
hfust hfust hfust hfust hfust hfust hfust hfust hsubt hsubt hsubt hsubt hsubt hsubt hsubt	9.30 8.95 9.94 9.80 9.87 9.88 10.00 9.87 45.60 49.40 ± 0.40 43.10 45.20 41.70 44.60	kJ/mol	279.10 278.80 278.60 278.60 278.69 278.55 278.64 278.70 244.50 193.00 229.00 251.00 265.50 279.00	temperatures NIST Webbook

hsubt	45.10	kJ/mol	278.00	NIST Webbook	
hsubt	44.60	kJ/mol	273.00	NIST Webbook	
hsubt	43.30	kJ/mol	226.00	NIST Webbook	
hsubt	53.90 ± 0.80	kJ/mol	193.00	NIST Webbook	
hvapt	30.60	kJ/mol	353.00	NIST Webbook	
hvapt	34.40	kJ/mol	328.00	NIST Webbook	
hvapt	31.50	kJ/mol	387.50	NIST Webbook	
hvapt	30.20	kJ/mol	461.00	NIST Webbook	
hvapt	30.30	kJ/mol	531.50	NIST Webbook	
hvapt	30.80	kJ/mol	352.00	NIST Webbook	
hvapt	30.50	kJ/mol	361.00	NIST Webbook	
hvapt	30.20	kJ/mol	366.00	NIST Webbook	
hvapt	35.30	kJ/mol	343.00	NIST Webbook	
hvapt	31.00	kJ/mol	350.00	NIST Webbook	
hvapt	33.00 ± 0.10	kJ/mol	313.00	NIST Webbook	
hvapt	31.40	kJ/mol	344.00	NIST Webbook	
hvapt	32.20 ± 0.10	kJ/mol	328.00	NIST Webbook	
hvapt	33.10	kJ/mol	314.00	NIST Webbook	
hvapt	31.80 ± 0.10	kJ/mol	333.00	NIST Webbook	
hvapt	33.25	kJ/mol	298.00	Enthalpies of Vaporization and Vapor Pressures of Some Deuterated Hydrocarbons. Liquid-Vapor Pressure Isotope Effects	
hvapt	31.60 ± 0.40	kJ/mol	345.00	NIST Webbook	
hvapt	31.40 ± 0.10	kJ/mol	343.00	NIST Webbook	
hvapt	34.50	kJ/mol	310.50	NIST Webbook	
hvapt	33.40	kJ/mol	335.50	NIST Webbook	
hvapt	34.10	kJ/mol	321.00	NIST Webbook	
hvapt	31.20	kJ/mol	294.00	NIST Webbook	
hvapt	34.10	kJ/mol	318.00	NIST Webbook	
hvapt	30.76	kJ/mol	353.30	KDB	
hvapt	34.10	kJ/mol	293.00	NIST Webbook	
hvapt	34.10	kJ/mol	319.00	NIST Webbook	
hvapt	30.90 ± 0.10	kJ/mol	353.00	NIST Webbook	
hvapt	32.50 ± 0.50	kJ/mol	328.00	NIST Webbook	
hvapt	30.72	kJ/mol	353.30	NIST Webbook	
hvapt	33.20	kJ/mol	325.00	NIST Webbook	
hvapt	35.60	kJ/mol	285.50	NIST Webbook	
-	33.50	kJ/mol	336.50	NIST Webbook	
-	31.90	kJ/mol	332.00	NIST Webbook	
hvapt	33.40	kJ/mol	307.00	NIST Webbook	
hvapt hvapt hvapt hvapt hvapt hvapt hvapt hvapt hvapt	32.50 ± 0.50 30.72 33.20 35.60 33.50 31.90 32.40	kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol kJ/mol	328.00 353.30 325.00 285.50 336.50 332.00 324.00	NIST Webbook	

hvapt	32.60 ± 0.40	kJ/mol	313.00	NIST Webbook	
psub	0.53	kPa	250.68	Recommended sublimation pressure and enthalpy of benzene	
psub	0.81	kPa	255.67	Recommended sublimation pressure and enthalpy of benzene	
psub	0.81	kPa	255.67	Recommended sublimation pressure and enthalpy of benzene	
psub	0.65	kPa	253.17	Recommended sublimation pressure and enthalpy of benzene	
psub	0.65	kPa	253.17	Recommended sublimation pressure and enthalpy of benzene	
psub	0.65	kPa	253.17	Recommended sublimation pressure and enthalpy of benzene	
psub	0.53	kPa	250.68	Recommended sublimation pressure and enthalpy of benzene	
psub	0.53	kPa	250.68	Recommended sublimation pressure and enthalpy of benzene	
psub	0.42	kPa	248.18	Recommended sublimation pressure and enthalpy of benzene	
psub	1.23	kPa	260.68	Recommended sublimation pressure and enthalpy of benzene	
psub	0.42	kPa	248.18	Recommended sublimation pressure and enthalpy of benzene	
psub	0.34	kPa	245.68	Recommended sublimation pressure and enthalpy of benzene	

psub	0.42	kPa	248.18	Recommended sublimation pressure and enthalpy of benzene	
psub	0.34	kPa	245.68	Recommended sublimation pressure and enthalpy of benzene	
psub	0.34	kPa	245.68	Recommended sublimation pressure and enthalpy of benzene	
psub	0.27	kPa	243.20	Recommended sublimation pressure and enthalpy of benzene	
psub	0.27	kPa	243.20	Recommended sublimation pressure and enthalpy of benzene	
psub	0.27	kPa	243.20	Recommended sublimation pressure and enthalpy of benzene	
psub	0.21	kPa	240.70	Recommended sublimation pressure and enthalpy of benzene	
psub	0.16	kPa	238.21	Recommended sublimation pressure and enthalpy of benzene	
psub	0.16	kPa	238.21	Recommended sublimation pressure and enthalpy of benzene	
psub	0.16	kPa	238.21	Recommended sublimation pressure and enthalpy of benzene	
psub	0.13	kPa	235.70	Recommended sublimation pressure and enthalpy of benzene	
psub	0.13	kPa	235.70	Recommended sublimation pressure and enthalpy of benzene	

psub 0.10 KPa 233.20 Recommended sublimination pressure and enthalpy of benzene
psub 0.10 kPa 233.20 Recommended sublimation pressure and enthalpy of benzene psub 0.21 kPa 240.70 Recommended sublimation pressure and enthalpy of benzene psub 0.81 kPa 255.67 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.23 kPa 260.68 Recommended sublimation pressure and enthalpy of benzene psub 1.23 kPa 260.68 Recommended sublimation pressure and enthalpy of benzene psub 0.21 kPa 240.70 Recommended sublimation pressure and enthalpy of benzene psub 0.21 kPa 240.70 Recommended sublimation pressure and enthalpy of benzene psub 0.13 kPa 235.70 Recommended sublimation pressure and enthalpy of benzene psub 0.13 kPa 235.70 Recommended sublimation pressure and enthalpy of benzene
psub 0.21 kPa 240.70 Recommended sublimation pressure and enthalpy of benzene psub 0.81 kPa 255.67 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.23 kPa 260.68 Recommended sublimation pressure and enthalpy of benzene psub 1.23 kPa 260.68 Recommended sublimation pressure and enthalpy of benzene psub 0.21 kPa 240.70 Recommended sublimation pressure and enthalpy of benzene psub 0.21 kPa 240.70 Recommended sublimation pressure and enthalpy of benzene psub 0.13 kPa 235.70 Recommended sublimation pressure and enthalpy of benzene psub 0.13 kPa 235.70 Recommended sublimation pressure and enthalpy of benzene
psub 0.81 kPa 255.67 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.00 kPa 258.16 Recommended sublimation pressure and enthalpy of benzene psub 1.23 kPa 260.68 Recommended sublimation pressure and enthalpy of benzene psub 1.23 kPa 260.68 Recommended sublimation pressure and enthalpy of benzene psub 1.23 kPa 260.68 Recommended sublimation pressure and enthalpy of benzene psub 0.21 kPa 240.70 Recommended sublimation pressure and enthalpy of benzene psub 0.21 kPa 240.70 Recommended sublimation pressure and enthalpy of benzene psub 0.13 kPa 235.70 Recommended sublimation pressure and enthalpy of benzene
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psub 0.13 kPa 235.70 Recommended sublimation pressure and enthalpy of benzene
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pvap	39.52	kPa	325.60	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts
pvap	6.08	kPa	283.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	7.85	kPa	288.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine
pvap	10.03	kPa	293.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	12.69	kPa	298.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	15.93	kPa	303.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures

pvap	19.81	kPa	308.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	24.40	kPa	313.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	29.85	kPa	318.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	36.24	kPa	323.15	Total vapour pressure and excess Gibbs energy for binary mixtures of 1,1,2,2-tetrachlorethane or tetrachloroethene with benzene at nine temperatures
pvap	49.45	kPa	331.70	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts
pvap	69.20	kPa	341.70	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts
pvap	101.60	kPa	353.60	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts

pvap	247.52	kPa	385.30	Extension of the	
				DSC method to measuring vapor pressures of narrow boiling range oil cuts	
pvap	499.10	kPa	415.80	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts	
pvap	750.14	kPa	435.40	Extension of the DSC method to measuring vapor pressures of narrow boiling range oil cuts	
pvap	101.33	kPa	353.25	Vapor Liquid Equilibrium Data for Binary Systems of N,N-Dimethylacetamide with Cyclohexene, Cyclohexane, and Benzene Separately at Atmospheric Pressure	
pvap	12.71	kPa	298.15	(Vapour + liquid) equilibria of (1-butanol + benzene, or toluene, or o-, or m-, or p-xylene) at T = 308.15 K	
pvap	15.63	kPa	303.15	Vapor Pressure Measurements for Binary Mixtures Containing Ionic Liquid and Predictions by the Conductor-like Screening Model for Real Solvents	
pvap	9.98	kPa	293.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression	

pvap	36.60	kPa	323.15	Vapor Pressure Measurements for Binary Mixtures Containing Ionic Liquid and Predictions by the Conductor-like Screening Model for Real Solvents
pvap	53.12	kPa	333.15	Vapor Pressure Measurements for Binary Mixtures Containing Ionic Liquid and Predictions by the Conductor-like Screening Model for Real Solvents
pvap	74.82	kPa	343.15	Vapor Pressure Measurements for Binary Mixtures Containing Ionic Liquid and Predictions by the Conductor-like Screening Model for Real Solvents
pvap	101.33	kPa	353.27	Isobaric Vapor Liquid Equilibrium for Binary and Ternary Systems of Isoamyl Alcohol + Isoamyl Acetate + Dimethyl Sulfoxide at 101.33 kPa
pvap	101.30	kPa	353.25	Vapor-Liquid Equilibrium for Binary Systems of Allyl Alcohol + Water and Allyl Alcohol + Benzene at 101.3 kPa
pvap	43.65	kPa	328.15	Vapor Liquid Equilibrium and Excess Enthalpy Data for Systems Containing N,N-Dimethylacetamide

pvap	137.28	kPa	363.15	Vapor-Liquid Equilibria for Four Binary Systems at 363.15 K: N-Methylformamide + Hexane, + Benzene, + Chlorobenzene, and + Acetonitrile
pvap	24.35	kPa	313.14	Vapor-Liquid Equilibrium for Benzene + 2-Methylpentane and Allyl Alcohol + 1-Propanol
pvap	36.15	kPa	323.14	Vapor-Liquid Equilibrium for Benzene + 2-Methylpentane and Allyl Alcohol + 1-Propanol
pvap	52.17	kPa	333.13	Vapor-Liquid Equilibrium for Benzene + 2-Methylpentane and Allyl Alcohol + 1-Propanol
pvap	379.30	kPa	403.15	Isothermal Vapor-Liquid Equilibrium for Methanol and 2,3-Dimethyl-1-butene at 343.06 K, 353.27 K, 363.19 K, and 372.90 K
pvap	35.47	kPa	323.15	Isothermal Phase Equilibria and Excess Molar Enthalpies for Binary Systems with Dimethyl Ether at 323.15 K
pvap	52.11	kPa	333.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	2877.00	kPa	520.05	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS

pvap	2183.00	kPa	500.15	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS	
pvap	1622.00	kPa	480.45	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS	
pvap	1173.00	kPa	460.35	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS	
pvap	778.00	kPa	437.45	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS	
pvap	572.00	kPa	421.85	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS	
pvap	366.00	kPa	401.25	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS	

pvap	205.00	kPa	378.35	Quantitative comparison between predicted and experimental binary n-alkane p benzene phase behaviors using cubic and PC-SAFT EOS
pvap	101.33	kPa	353.15	Phase equilibria of three binary systems containing 2,5-dimethylthiophene and 2-ethylthiophene in hydrocarbons
pvap	100.91	kPa	353.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	86.27	kPa	348.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	73.35	kPa	343.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	62.01	kPa	338.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression

pvap	43.51	kPa	328.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression	
pvap	36.09	kPa	323.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression	
pvap	29.73	kPa	318.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression	
pvap	24.30	kPa	313.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression	
pvap	19.71	kPa	308.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression	
pvap	24.45	kPa	313.15	Vapor Pressure Measurements for Binary Mixtures Containing Ionic Liquid and Predictions by the Conductor-like Screening Model for Real Solvents	

pvap	15.85	kPa	303.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression	
pvap	79.99	kPa	345.61	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components	
pvap	12.64	kPa	298.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression	
pvap	101.33	kPa	353.26	Isobaric vapor-liquid equilibrium for binary system of cinnamaldehyde + benzaldehyde at 10, 20 and 30 kPa	
pvap	86.40	kPa	348.15	Phase equilibria and excess molar enthalpies study of the binary systems (pyrrole + hydrocarbon, or an alcohol) and modeling	
pvap	62.10	kPa	338.15	Phase equilibria and excess molar enthalpies study of the binary systems (pyrrole + hydrocarbon, or an alcohol) and modeling	
pvap	101.30	kPa	353.30	Isobaric vapor-liquid equilibrium for the binary mixtures of nonane with cyclohexane, toluene, m-xylene, or p-xylene at 101.3 kPa	

pvap	100.00	kPa	353.15 Vapor liquid equilibria and density measurement for binary mixtures of toluene, benzene, o-xylene, m-xylene, sulfolane and nonane at 333.15K and 353.15K
pvap	52.45	kPa	333.15 Vapor liquid equilibria and density measurement for binary mixtures of toluene, benzene, o-xylene, m-xylene, sulfolane and nonane at 333.15K and 353.15K
pvap	12.70	kPa	298.15 Thermodynamic properties of mixtures containing ionic liquids Vapor pressures and activity coefficients of n-alcohols and benzene in binary mixtures with 1-methyl-3-butyl-imidazolium bis(trifluoromethyl-sulfonyl) imide
pvap	93.32	kPa	350.50 Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	66.66	kPa	340.06 Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components

pvap	53.33	kPa	333.56 Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	40.00	kPa	325.60 Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	24.33	kPa	313.15 Thermodynamic properties of mixtures containing ionic liquids Vapor pressures and activity coefficients of n-alcohols and benzene in binary mixtures with 1-methyl-3-butyl-imidazolium bis(trifluoromethyl-sulfonyl) imide
pvap	19.66	kPa	308.15 Thermodynamic properties of mixtures containing ionic liquids Vapor pressures and activity coefficients of n-alcohols and benzene in binary mixtures with 1-methyl-3-butyl-imidazolium bis(trifluoromethyl-sulfonyl) imide
pvap	15.92	kPa	303.15 Thermodynamic properties of mixtures containing ionic liquids Vapor pressures and activity coefficients of n-alcohols and benzene in binary mixtures with 1-methyl-3-butyl-imidazolium bis(trifluoromethyl-sulfonyl) imide

rfi	1.48490	303.15	Excess molar volumes and refractive indices of (methoxybenzene + benzene, or toluene, or o-xylene, or m-xylene, or p-xylene, or mesitylene) binary mixtures between T = (288.15 to 303.15) K	
rfi	1.38820	293.10	Liquid liquid equilibria of methylcyclohexane benzene N-formylmorpholine at several temperatures	
rfi	1.49290	313.15	Volumetric, Viscometric, Ultrasonic, and Refractive Index Properties of Liquid Mixtures of Benzene with Industrially Important Monomers at Different Temperatures	
rfi	1.49440	308.15	Volumetric, Viscometric, Viscometric, Ultrasonic, and Refractive Index Properties of Liquid Mixtures of Benzene with Industrially Important Monomers at Different Temperatures	
rfi	1.49620	303.15	Volumetric, Viscometric, Viscometric, Ultrasonic, and Refractive Index Properties of Liquid Mixtures of Benzene with Industrially Important Monomers at Different Temperatures	

rfi	1.49790	298.15	Volumetric, Viscometric, Viscometric, Ultrasonic, and Refractive Index Properties of Liquid Mixtures of Benzene with Industrially Important Monomers at Different Temperatures	
rfi	1.49110	318.15	Densities and Refractive Indices of Binary Mixtures of Benzene with Triethylamine and Tributylamine at Different Temperatures	
rfi	1.49290	313.15	Densities and Refractive Indices of Binary Mixtures of Benzene with Triethylamine and Tributylamine at Different Temperatures	
rfi	1.49440	308.15	Densities and Refractive Indices of Binary Mixtures of Benzene with Triethylamine and Tributylamine at Different Temperatures	
rfi	1.49620	303.15	Densities and Refractive Indices of Binary Mixtures of Benzene with Triethylamine and Tributylamine at Different Temperatures	
rfi	1.49790	298.15	Densities and Refractive Indices of Binary Mixtures of Benzene with Triethylamine and Tributylamine at Different Temperatures	
rfi				

rfi	1.49810	298.15	Separation of aromatic hydrocarbons from alkanes using ammonium ionic liquid C2NTf2 at T = 298.15K	
rfi	1.49785	298.15	Isothermal vapor liquid equilibrium at 323.15K and excess molar volumes and refractive indices at 298.15K for the ternary system propyl vinyl ether + 1-propanol + benzene and its binary sub-systems	
rfi	1.49764	298.15	Isothermal vapor-liquid equilibrium at T = 333.15 K and excess volumes and molar refractivity deviation at T = 298.15 K for the ternary mixtures {di-methyl carbonate (DMC) + ethanol + benzene} and {DMC+ ethanol + toluene}	
rfi	1.49774	298.15	Experimental data, correlation and prediction of the extraction of benzene from cyclic hydrocarbons using [Epy][ESO4] ionic liquid	
rfi	1.50090	293.15	Effect of temperature on the volumetric properties of (cyclohexanone + an aromatic hydrocarbon)	
rfi	1.50090	293.15	A study of densities and volumetric properties of binary mixtures containing nitrobenzene at T = (293.15 to 353.15) K	

rfi	1.49210	308.15	Topological and thermodynamic investigations of molecular interactions in binary mixtures: Molar excess volumes and molar excess enthalpies	
rfi	1.49790	298.15	Excess Molar Volumes of (propiophenone + benzene, or toluene, or ethylbenzene, or butylbenzene) at temperatures 298.15 K and 328.15 K	
rfi	1.49692	298.15	Azeotropic behaviour of (benzene + cyclohexane + chlorobenzene) ternary mixture using chlorobenzene as entrainer at 101.3 kPa	
rfi	1.49710	298.15	Excess and deviation properties for the binary mixtures of methylcyclohexane with benzene, toluene, p-xylene, mesitylene, and anisole at T = (298.15, 303.15, and 308.15) K	
rfi	1.49360	303.15	Excess and deviation properties for the binary mixtures of methylcyclohexane with benzene, toluene, p-xylene, mesitylene, and anisole at T = (298.15, 303.15, and 308.15) K	

rfi	1.49030	308.15	Excess and deviation properties for the binary mixtures of methylcyclohexane with benzene, toluene, p-xylene, mesitylene, and anisole at T = (298.15, 303.15, and 308.15) K	
rfi	1.50500	288.15	Excess molar volumes and refractive indices of (methoxybenzene + benzene, or toluene, or o-xylene, or m-xylene, or p-xylene, or mesitylene) binary mixtures between T = (288.15 to 303.15) K	
rfi	1.50110	293.15	Excess molar volumes and refractive indices of (methoxybenzene + benzene, or toluene, or o-xylene, or m-xylene, or p-xylene, or mesitylene) binary mixtures between T = (288.15 to 303.15) K	
rfi	1.49790	298.15	Excess molar volumes and refractive indices of (methoxybenzene + benzene, or toluene, or o-xylene, or m-xylene, or p-xylene, or mesitylene) binary mixtures between T = (288.15 to 303.15) K	

rfi	1.50090	293.10	Densities and volumetric properties of N-methyl-2-pyrrolidone with aromatic hydrocarbon at different temperature
rfi	1.49540	303.15	Study of activity coefficients for sodium iodide in (methanol + benzene) system by (vapour + liquid) equilibrium measurements
rfi	1.50090	298.15	Densities and excess volumes of binary mixtures of N,N-dimethylformamide with aromatic hydrocarbon at different temperature
rfi	1.50090	293.10	A study on densities and excess volumes in the (c-butyrolactone + aromatic hydrocarbon) system at various temperatures
rfi	1.50240	293.10	(Liquid + liquid) equilibria of three ternary systems: (heptane + benzene + N-formylmorpholine), (heptane + toluene + N-formylmorpholine), (heptane + xylene + N-formylmorpholine) from T = (298.15 to 353.15) K
rfi	1.50090	298.15	Effects of the presence of ethylacetate or benzene on the densities and volumetric properties of mixture (styrene + N,N-dimethylformamide)

rfi	1.49790	298.15	Excess molar volumes of (octane + benzene, or toluene, or 1,3-xylene, or 1,3,5-trimethylbenzen at temperatures between (298.15 and 328.15) K	e)
rfi	1.49790	298.15	p, Vm, T) measurements of (octane + benzene) at temperatures from (298.15 to 328.15) K and at pressures up to 40 MPa	
rfi	1.49774	298.15	Thermophysical properties of the binary mixtures of 2-methyl-tetrahydrofur with benzene and halobenzenes	an
rfi	1.49900	298.15	Liquid-liquid equilibria for mixtures of (Furfural + an Aromatic hydrocarbon + an alkane) at T=298.15 K	
rfi	1.50150	293.15	Infinite Dilution Activity Coefficients of Hydrocarbons in Triethylene Glycol and Tetraethylene Glycol	
rfi	1.50110	293.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of Anisole with Benzene, Methylbenzene, Ethylbenzene, Propylbenzene, and Butylbenzene at (293.15 and 303.15) K	

rfi	1.49470	303.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of Anisole with Benzene, Methylbenzene, Ethylbenzene, Propylbenzene, and Butylbenzene at (293.15 and 303.15) K
rfi	1.49720	298.20	Liquid-Liquid Equilibria for Ternary Mixtures (an Ionic Liquid + Benzene +Heptane or Hexadecane) at T) 298.2 K and Atmospheric Pressure
rfi	1.49774	298.15	Separation of Benzene from Linear Alkanes (C6-C9) Using 1-Ethyl-3-Methylimidazolium Ethylsulfate at T = 298.15 K
rfi	1.50110	293.15	Solubilities of Phosphorus-Containing Compounds in Selected Solvents
rfi	1.49774	298.15	Liquid Extraction of Benzene from Its Mixtures Using 1-Ethyl-3-methylimidazolium Ethylsulfate as a Solvent
rfi	1.49774	298.15	Liquid-Liquid Equilibria of the Ternary Systems of Alkane + Aromatic + 1-Ethylpyridinium Ethylsulfate Ionic Liquid at T = (283.15 and 298.15) K

rfi	1.49774	298.15 Extraction of Benzene from Aliphatic Compounds Using Commercial Ionic Liquids as Solvents: Study of the Liquid Liquid Equilibrium at T = 298.15 K
rfi	1.49774	298.15 Liquid Liquid Extraction of Aromatic Compounds from Cycloalkanes Using 1-Butyl-3-methylimidazolium Methylsulfate Ionic Liquid
rfi	1.49764	298.15 Isothermal Vapor-Liquid Equilibrium at 333.15 K, Density, and Refractive Index at 298.15 K for the Ternary Mixture of Dibutyl Ether + Ethanol + Benzene and Binary Subsystems
rfi	1.49740	298.15 Experimental Isobaric Vapor-Liquid Equilibria of Binary Mixtures of 2,2,2-Trifluoroethanol with Benzene or Toluene
rfi	1.50420	288.15 Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K
rfi	1.50110	293.15 Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K

rfi	1.49800	Indic M Tetra with Hyd Ten from	defractive ties of Binary ixtures of ahydrofuran the Aromatic rocarbon at mperatures to (288.15 to 18.15) K
rfi	1.49490	Indic M Tetra with Hyd Ten from	defractive les of Binary ixtures of ahydrofuran h Aromatic rocarbon at mperatures n (288.15 to 18.15) K
rfi	1.49180	Indic M Tetra with Hyd Ten from	defractive les of Binary lixtures of ahydrofuran h Aromatic rocarbon at mperatures n (288.15 to 18.15) K
rfi	1.48870	Indic M Tetra with Hyd Ten from	defractive less of Binary ixtures of ahydrofuran h Aromatic rocarbon at mperatures n (288.15 to 18.15) K
rfi	1.48560	Indic M Tetra with Hyd Ten from	defractive res of Binary ixtures of ahydrofuran h Aromatic rocarbon at mperatures of (288.15 to 18.15) K
rfi	1.50420	288.15 D R Inc Pro Bina of 1 with T o m p-X Me Ten from	Densities, defractive dices, and Excess Deperties of Ary Mixtures A-Dioxane Denzene, Coluene, D-Xylene, D-

rfi	1.50110	293.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K	
rfi	1.49800	298.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K	
rfi	1.49490	303.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K	
rfi	1.49180	308.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K	

rfi	1.48870	313.15 Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K
rfi	1.50110	293.15 Solubilities of Triphenylphosphine Oxide in Selected Solvents
rfi	1.49765	298.15 Isobaric Vapor-Liquid Equilibria for the Binary Systems Benzene + Methyl Ethanoate, Benzene + Butyl Ethanoate, and Benzene + Methyl Heptanoate at 101.31kPa
rfi	1.50110	293.15 Solubilities of Methyldiphenylphosphine Oxide in Selected Solvents
rfi	1.50110	293.15 Solubilities of 3,9-Dimethyl-3,9-dioxide-2,4,8,10-tetraoxa-3,9-diphosphaspiro[5.5]unded in Selected Solvents
rfi	1.50090	298.15 The volumetric properties of (1,2-propanediol carbonate + benzene, or toluene, or styrene) binary mixtures at temperatures from T = 293.15 K to T = 353.15 K

rfi	1.50765	Density, Speed of Sound, and Refractive Index of the Binary Systems Cyclohexane (1) or Methylcyclohexane (1) or Cyclo-octane (1) with Benzene (2), Toluene (2), and Ethylbenzene (2) at Two Temperatures
rfi	1.49774	298.15 Density, Speed of Sound, and Refractive Index of the Binary Systems Cyclohexane (1) or Methylcyclohexane (1) or Cyclo-octane (1) with Benzene (2), Toluene (2), and Ethylbenzene (2) at Two Temperatures
rfi	1.49774	298.15 Effect of the Chain Length on the Aromatic Ring in the Separation of Aromatic Compounds from Methylcyclohexane Using the Ionic Liquid 1-Ethyl-3-methylpyridinium Ethylsulfate
rfi	1.48560	318.15 Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K

rfi	1.50090		293.15	Experimental densities and excess volumes for binary mixtures of (dimethyl sulfoxide + an aromatic hydrocarbon) at temperatures from (293.15 to 353.15) K at atmospheric pressure	
rhol	885.00	kg/m3	289.00	KDB	
rhol	884.25	kg/m3	288.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)	
rhol	878.92	kg/m3	293.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)	
rhol	873.58	kg/m3	298.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)	

rhol	868.23	kg/m3	303.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)	
rhol	862.87	kg/m3	308.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)	
rhol	857.50	kg/m3	313.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)	
rhol	884.30	kg/m3	288.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K	

rhol	878.95	kg/m3	293.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K	
rhol	873.61	kg/m3	298.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K	
rhol	868.26	kg/m3	303.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K	
rhol	862.90	kg/m3	308.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K	

rhol	857.56	kg/m3	313.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K	
rhol	852.23	kg/m3	318.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K	
rhol	873.62	kg/m3	298.15	Topological Investigations of Excess Molar Volumes and Excess Isentropic Compressibilities of Ternary Mixtures Containing Pyrrolidin-2-one at 308.15 K	
rhol	873.66	kg/m3	298.15	Densities, Viscosities, Speeds of Sound, and Refractive Indices of Binary Mixtures of 2-Ethyl-1-hexanol with Benzene and Halobenzenes	
rhol	868.29	kg/m3	303.15	Densities, Viscosities, Speeds of Sound, and Refractive Indices of Binary Mixtures of 2-Ethyl-1-hexanol with Benzene and Halobenzenes	

rhol	862.92	kg/m3	308.15	Densities, Viscosities, Speeds of Sound, and Refractive Indices of Binary Mixtures of 2-Ethyl-1-hexanol with Benzene and Halobenzenes	
rhol	873.55	kg/m3	298.15	Experimental and predicted vapour liquid equilibrium of 1,4-dioxane with cycloalkanes and benzene	
rhol	884.25	kg/m3	288.15	Effect of temperature on the excess molar volumes of some alcohol + aromatic mixtures and modelling by cubic EOS mixing rules	
rhol	873.60	kg/m3	298.15	Fluid Phase Topology of Benzene + Cyclohexane + 1-Propanol at 101.3 kPa	
rhol	878.92	kg/m3	293.15	Effect of temperature on the excess molar volumes of some alcohol + aromatic mixtures and modelling by cubic EOS mixing rules	
rhol	873.58	kg/m3	298.15	Effect of temperature on the excess molar volumes of some alcohol + aromatic mixtures and modelling by cubic EOS mixing rules	
rhol	868.23	kg/m3	303.15	Effect of temperature on the excess molar volumes of some alcohol + aromatic mixtures and modelling by cubic EOS mixing rules	

rhol	862.87	kg/m3	308.15	Effect of temperature on the excess molar volumes of some alcohol + aromatic mixtures and modelling by cubic EOS mixing rules	
rhol	857.50	kg/m3	313.15	Effect of temperature on the excess molar volumes of some alcohol + aromatic mixtures and modelling by cubic EOS mixing rules	
rhol	873.67	kg/m3	298.10	Excess enthalpies of binary mixtures of 2-ethoxyethanol with four hydrocarbons at 298.15, 308.15, and 318.15K An experimental and theoretical study	
rhol	873.58	kg/m3	298.15	Thermodynamic study of 1,1,2,2-tetrachloroetha + hydrocarbon mixtures I. Excess and solvation enthalpies	ine
rhol	884.25	kg/m3	288.15	Volumetric properties of the ternary system ethanol + chloroform + benzene at temperature range (288.15 313.15) K: Experimental data, correlation and prediction by cubic EOS	

rhol	878.92	kg/m3	293.15	Volumetric properties of the ternary system ethanol + chloroform + benzene at temperature range (288.15 313.15) K: Experimental data, correlation and prediction by cubic EOS	
rhol	873.58	kg/m3	298.15	Volumetric properties of the ternary system ethanol + chloroform + benzene at temperature range (288.15 313.15) K: Experimental data, correlation and prediction by cubic EOS	
rhol	868.23	kg/m3	303.15	Volumetric properties of the ternary system ethanol + chloroform + benzene at temperature range (288.15 313.15) K: Experimental data, correlation and prediction by cubic EOS	
rhol	862.87	kg/m3	308.15	Volumetric properties of the ternary system ethanol + chloroform + benzene at temperature range (288.15 313.15) K: Experimental data, correlation and prediction by cubic EOS	
rhol	857.50	kg/m3	313.15	Volumetric properties of the ternary system ethanol + chloroform + benzene at temperature range (288.15 313.15) K: Experimental data, correlation and prediction by cubic EOS	

Page	behavior of the binary systems benzene + cyclohexane and benzene + 2.2.4-trimethyl-pentane at temperatures 293.15-323.15K rhol 868.30 kg/m3 303.00 Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2.2.4-trimethyl-pentane at temperatures 293.15-323.15K rhol 857.57 kg/m3 313.00 Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2.2.4-trimethyl-pentane at temperatures 293.15-323.15K rhol 846.76 kg/m3 323.00 Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2.2.4-trimethyl-pentane at temperatures 293.15-323.15K rhol 846.76 kg/m3 323.00 Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2.2.4-trimethyl-pentane at temperatures 293.15-323.15K rhol 873.53 kg/m3 298.15 Phase behaviour of ionic liquid 1-butyl-1-methyl-pyrolidinium tris(pentalfurorethyl)triflucrophosphate with alcohols, water and aromatic hydrocarbons rhol 873.79 kg/m3 298.15 Liquid-liquid equilibrium data for temary mixtures composed of n-hexane, benzene and acetonitrile at (298.15, 308.15, 308.15, and 318.15) K rhol 873.54 kg/m3 298.15 Heat capacities of binary and temary mixtures containing o-chlorotoluene,					
behavior of the binary systems benzene + cyclohexane and benzene + 2.2.4-trimethyl-pentane at temperatures 293.15-323.15K rhol 857.57 kg/m3 313.00 Volumetric behavior of the binary systems benzene + 2.2.4-trimethyl-pentane at temperatures 293.15-323.15K rhol 846.76 kg/m3 323.00 Volumetric behavior of the binary systems benzene + 2.2.4-trimethyl-pentane at temperatures 293.15-323.15K rhol 846.76 kg/m3 323.00 Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2.2.4-trimethyl-pentane at temperatures 293.15-323.15K rhol 873.53 kg/m3 298.15 Phase behaviour of ionic liquid 1-butyl-1-methylpyrolidinium tris(pentafluoroethyl)trifluorophosphate with alcohols, water and aromatic hydrocarbons water and aromatic for temary mixtures composed of n-hexane, benzene and acetonitrile at (298.15, 308.15, and 318.15) K rhol 873.54 kg/m3 298.15 Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and	behavior of the binary systems benzene + cyclohexane and benzene + 2.2,4-trimethyl-pentane at temperatures 293.15-323.15K rhol 857.57 kg/m3 313.00 Volumetric behavior of the binary systems benzene + cyclohexane and benzene + cyclohexane and benzene + 2.2,4-trimethyl-pentane at temperatures 293.15-323.15K rhol 846.76 kg/m3 323.00 Volumetric behavior of the binary systems benzene + cyclohexane and benzene + cyclohexane and benzene + 2.2,4-trimethyl-pentane at temperatures 293.15-323.15K rhol 873.53 kg/m3 298.15 Phase behavior of the binary systems benzene + 2.2,4-trimethyl-pentane at temperatures 293.15-323.15K rhol 873.53 kg/m3 298.15 Phase behavior of the binary systems benzene + 2.2,4-trimethyl-pentane at temperatures 293.15-323.15K rhol 873.54 kg/m3 298.15 Liquid-liquid equilibrium data for ternary mixtures composed of historic pental furore and accondition at a containing and ternary mixtures containing o-chlorotoluene, cyclic ether and aromatic	rhol	878.98	kg/m3		behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures
behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures 293.15-323.15K rhol 846.76 kg/m3 323.00 Volumetric behavior of the binary systems benzene + 2,2,4-trimethyl-pentane at temperatures 293.15-323.15K rhol 873.53 kg/m3 298.15 Phase behaviour of ionic liquid 1-butyl-1-methylpyrrolidinium tris(pentafluoroethyl)trifluorophosphate with alcohols, water and aromatic hydrocarbons rhol 873.79 kg/m3 298.15 Liquid-liquid equilibrium data for ternary mixtures composed of n-hexane, benzene and acetonitrile at (298.15, 308.15, and 318.15) K rhol 873.54 kg/m3 298.15 Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and	behavior of the binary systems benzene + cyclohexane and benzene + 2.2.4-trimethyl-pentane at temperatures 293.15-323.15K Thol 846.76 kg/m3 323.00 Volumetric behavior of the binary systems benzene + cyclohexane and benzene + cyclohexane and benzene + 2.2.4-trimethyl-pentane at temperatures 293.15-323.15K Thol 873.53 kg/m3 298.15 Phase behaviour of ionic liquid 1-butyl-1-methyl-pyrrolidinium tris(pentaffuoroethyl)trifluorophosphate with alcohols, water and aromatic hydrocarbons Thol 873.79 kg/m3 298.15 Liquid-liquid equilibrium data for ternary mixtures composed of n-hexane, benzene and acetonitrile at (298.15, 308.15, 308.15, and 318.15) K Thol 873.54 kg/m3 298.15 Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and aromatic	rhol	868.30	kg/m3		behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures
behavior of the binary systems benzene + cyclohexane and benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures 293.15-323.15K Thol 873.53 kg/m3 298.15 Phase behaviour of ionic liquid 1-butyl-1-methylpyrrolidinium tris(pentafluoroethyl)trifluorophosphate with alcohols, water and aromatic hydrocarbons Thol 873.79 kg/m3 298.15 Liquid-liquid equilibrium data for ternary mixtures composed of n-hexane, benzene and acetonitrile at (298.15, 308.15, and 318.15) K Thol 873.54 kg/m3 298.15 Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and	behavior of the binary systems benzene + cyclohexane and benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures 293.15-323.15K rhol 873.53 kg/m3 298.15 Phase behaviour of ionic liquid 1-butyl-1-methylpyrrolidinium tris(pentafluoroethyl)trifluorophosphate with alcohols, water and aromatic hydrocarbons rhol 873.79 kg/m3 298.15 Liquid-liquid equilibrium data for ternary mixtures composed of n-hexane, benzene and accetonitrile at (298.15, 308.15, and 318.15) K rhol 873.54 kg/m3 298.15 Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and aromatic	rhol	857.57	kg/m3		behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures
of ionic liquid 1-butyl-1-methylpyrrolidinium tris(pentafluoroethyl)trifluorophosphate with alcohols, water and aromatic hydrocarbons rhol 873.79 kg/m3 298.15 Liquid-liquid equilibrium data for ternary mixtures composed of n-hexane, benzene and acetonitrile at (298.15, 308.15, and 318.15) K rhol 873.54 kg/m3 298.15 Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and	of ionic liquid 1-butyl-1-methylpyrrolidinium tris(pentafluoroethyl)trifluorophosphate with alcohols, water and aromatic hydrocarbons rhol 873.79 kg/m3 298.15 Liquid-liquid equilibrium data for ternary mixtures composed of n-hexane, benzene and acetonitrile at (298.15, 308.15, and 318.15) K rhol 873.54 kg/m3 298.15 Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and aromatic	rhol	846.76	kg/m3		behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures
equilibrium data for ternary mixtures composed of n-hexane, benzene and acetonitrile at (298.15, 308.15, and 318.15) K rhol 873.54 kg/m3 298.15 Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and	equilibrium data for ternary mixtures composed of n-hexane, benzene and acetonitrile at (298.15, 308.15, and 318.15) K rhol 873.54 kg/m3 298.15 Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and aromatic	rhol	873.53	kg/m3	1-b	of ionic liquid outyl-1-methylpyrrolidinium tafluoroethyl)trifluorophosphate with alcohols, water and aromatic
of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and	of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and aromatic	rhol	873.79	kg/m3	298.15	equilibrium data for ternary mixtures composed of n-hexane, benzene and acetonitrile at (298.15, 308.15,
		rhol	873.54	kg/m3	298.15	of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and aromatic

rhol	868.20	kg/m3	303.15	Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and aromatic hydrocarbons
rhol	862.84	kg/m3	308.15	Heat capacities of binary and ternary mixtures containing o-chlorotoluene, cyclic ether and aromatic hydrocarbons
rhol	868.20	kg/m3	303.15	Thermodynamic Properties of Ternary Liquid Mixtures Containing o-Chlorotoluene: Excess Molar Volumes and Excess Isentropic Compressibilities
rhol	873.53	kg/m3	298.15	Phase behaviour of
				tricyanomethanide-based ionic liquids with alcohols and hydrocarbons
rhol	873.73	kg/m3	298.15	Liquid liquid equilibria in the ternary systems {hexadecane + BTX aromatics + 2-methoxyethanol or acetonitrile} at 298.15 K
rhol	873.71	kg/m3	298.15	Study of the suitability of two ammonium-based ionic liquids for the extraction of benzene from its mixtures with aliphatic hydrocarbons.
rhol	873.71	kg/m3	298.15 bis	Application of the ionic liquid tributylmethylammonium (trifluoromethylsulfonyl)imide as solvent for the extraction of benzene from octane and decane at T = 298.15 K and atmospheric pressure

rhol	873.20	kg/m3	298.15 Ternary (liquid + liquid) equilibria for mixtures of 1-hexyl-3-methylimidazolium (tetrafluoroborate or hexafluorophosphate) + benzene + an alkane at T = 298.2 K and p = 0.1 MPa
rhol	878.90	kg/m3	293.15 Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhol	868.20	kg/m3	303.15 Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhol	857.40	kg/m3	313.15 Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhol	873.95	kg/m3	298.15 Liquid liquid equilibrium of ternary systems 1-butyl-3-methylimidazolium hexafluorophosphate + aromatic + aliphatic
rhol	846.50	kg/m3	323.15 Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhol	835.70	kg/m3	333.15 Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K

	rhol	824.70	kg/m3	343.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K	
	rhol	874.16	kg/m3	298.15	Experimental and theoretical study of surface tension of binary mixtures of (n-alkyl acetates + heptane, benzene, and toluene)	
_	rhol	883.90	kg/m3	288.15	Volumetric properties of binary liquid mixtures: Application of the Prigogine Flory Patterson theory to excess molar volumes of dichloromethane with benzene or toluene	
	rhol	876.85	kg/m3	293.15	Volumetric properties of binary liquid mixtures: Application of the Prigogine Flory Patterson theory to excess molar volumes of dichloromethane with benzene or toluene	
_	rhol	873.36	kg/m3	298.15	Volumetric properties of binary liquid mixtures: Application of the Prigogine Flory Patterson theory to excess molar volumes of dichloromethane with benzene or toluene	

rhol	868.71	kg/m3	303.15	Volumetric properties of binary liquid mixtures: Application of the Prigogine Flory Patterson theory to excess molar volumes of dichloromethane with benzene or toluene
rhol	873.57	kg/m3	298.15	Evaluation of ionic liquids as solvent for aromatic extraction: Experimental, correlation and COSMO-RS predictions
rhol	873.45	kg/m3	298.15	Experimental and predicted data of excess molar enthalpies and excess molar volumes for the ternary system (1,3-dichlorobenzene + benzene + 1-chlorohexane) at T = 298.15 K
rhol	873.57	kg/m3	298.15	(Liquid + liquid) equilibrium at T = 298.15 K for ternary mixtures of alkane + aromatic compounds + imidazolium-based ionic liquids
rhol	878.89	kg/m3	293.15	Excess heat capacities of mixtures containing 1-methylpyrrolidin-2-one, chlorotoluenes and benzene
rhol	873.54	kg/m3	298.15	Excess heat capacities of mixtures containing 1-methylpyrrolidin-2-one, chlorotoluenes and benzene
rhol	868.20	kg/m3	303.15	Excess heat capacities of mixtures containing 1-methylpyrrolidin-2-one, chlorotoluenes and benzene

rhol	873.57	kg/m3	298.15 1-b	Measurements and equation-of-state modelling of thermodynamic properties of binary mixtures of utyl-1-methylpyrrolidinium
				tetracyanoborate ionic liquid with molecular compounds
rhol	873.71	kg/m3	298.15	Determination and correlation of (liquid + liquid) equilibria of ternary and quaternary systems with octane, decane, benzene and [BMpyr][DCA] at T = 298.15 K and atmospheric pressure
rhol	878.87	kg/m3	293.15	Theoretical and experimental study on volumetric and electromagnetic properties of binary systems consisting of 1,2-dichloroethane with benzene and its derivatives at T = (293.15 to 333.15) K
rhol	857.44	kg/m3	313.15	Theoretical and experimental study on volumetric and electromagnetic properties of binary systems consisting of 1,2-dichloroethane with benzene and its derivatives at T = (293.15 to 333.15) K
rhol	846.62	kg/m3	323.15	Theoretical and experimental study on volumetric and electromagnetic properties of binary systems consisting of 1,2-dichloroethane with benzene and its derivatives at T = (293.15 to 333.15) K

rhol	835.71	kg/m3	333.15	Theoretical and experimental study on volumetric and electromagnetic properties of binary systems consisting of 1,2-dichloroethane with benzene and its derivatives at T = (293.15 to 333.15) K	
rhol	868.30	kg/m3	303.15	Studies of partial molar volumes of alkylamine in non-electrolyte solvents I. Alkylamines in hydrocarbons at 303.15 and 313.15K	
rhol	857.59	kg/m3	313.15	Studies of partial molar volumes of alkylamine in non-electrolyte solvents I. Alkylamines in hydrocarbons at 303.15 and 313.15K	
rhol	868.42	kg/m3	303.15	Volumetric and transport properties of ternary mixtures containing 1-propanol + ethyl ethanoate + cyclohexane or benzene at 303.15 K: Experimental data, correlation and prediction by ERAS model	
rhol	873.64	kg/m3	298.15	Excess molar volumes and isentropic compressibilities changes of mixing of tetrahydropyran + benzene + cyclo or n-alkanes ternary mixtures at 308.15 K	

rhol	878.93	kg/m3	293.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	873.62	kg/m3	298.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	868.29	kg/m3	303.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	862.94	kg/m3	308.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K

rhol	857.58	kg/m3	313.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	852.19	kg/m3	318.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	873.40	kg/m3	298.15	Mutual Solubility of Pyridinium-Based Tetrafluoroborates and Toluene
rhol	873.64	kg/m3	298.15	Molar Excess Volumes and Excess Isentropic Compressibilities of {2-Methylaniline (i) + Benzene (j) + Methylbenzene}, {2-Methylaniline (i) + Benzene (j) + 1,2-Dimethylbenzene (k)}, and {2-Methylaniline (i) + Benzene (j) + 1,4-Dimethylbenzene (k)} at T = 308.15 K
rhol	873.50	kg/m3	298.15	Density, Speed of Sound, and Refractive Index for Binary Mixtures Containing Cycloalkanes and Aromatic Compounds at T = 313.15 K

rhol	846.60	kg/m3	323.15	Volumetric Behavior of the Binary Mixtures of Methyl Ethyl Ketone with n-Hexane, Cyclohexane, and Benzene at T) (303.15, 313.15, and 323.15) K	
rhol	857.40	kg/m3	313.15	Volumetric Behavior of the Binary Mixtures of Methyl Ethyl Ketone with n-Hexane, Cyclohexane, and Benzene at T) (303.15, 313.15, and 323.15) K	
rhol	868.10	kg/m3	303.15	Volumetric Behavior of the Binary Mixtures of Methyl Ethyl Ketone with n-Hexane, Cyclohexane, and Benzene at T) (303.15, 313.15, and 323.15) K	
rhol	857.50	kg/m3	313.15	Densities and Excess Molar Volumes of the Ternary Mixture 2-Butanol + Chloroform + Benzene and Binary Mixtures 2-Butanol + Chloroform, or + Benzene over the Temperature Range (288.15 to 313.15) K	
rhol	862.87	kg/m3	308.15	Densities and Excess Molar Volumes of the Ternary Mixture 2-Butanol + Chloroform + Benzene and Binary Mixtures 2-Butanol + Chloroform, or + Benzene over the Temperature Range (288.15 to 313.15) K	

rhol	868.23	kg/m3	303.15	Densities and Excess Molar Volumes of the Ternary Mixture 2-Butanol + Chloroform + Benzene and Binary Mixtures 2-Butanol + Chloroform, or + Benzene over the Temperature Range (288.15 to 313.15) K	
rhol	873.58	kg/m3	298.15	Densities and Excess Molar Volumes of the Ternary Mixture 2-Butanol + Chloroform + Benzene and Binary Mixtures 2-Butanol + Chloroform, or + Benzene over the Temperature Range (288.15 to 313.15) K	
rhol	878.92	kg/m3	293.15	Densities and Excess Molar Volumes of the Ternary Mixture 2-Butanol + Chloroform + Benzene and Binary Mixtures 2-Butanol + Chloroform, or + Benzene over the Temperature Range (288.15 to 313.15) K	
rhol	884.25	kg/m3	288.15	Densities and Excess Molar Volumes of the Ternary Mixture 2-Butanol + Chloroform + Benzene and Binary Mixtures 2-Butanol + Chloroform, or + Benzene over the Temperature Range (288.15 to 313.15) K	

rhol	824.89	kg/m3	343.15 Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhol	835.76	kg/m3	333.15 Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhol	846.05	kg/m3	323.15 Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhol	856.82	kg/m3	313.15 Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhol	862.21	kg/m3	308.15 Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K

rhol	867.59	kg/m3	303.15 Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhol	873.11	kg/m3	298.15 Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhol	878.23	kg/m3	293.15 Densities of Ionic Liquids, 1-Butyl-3-methylimidazolium Hexafluorophosphate and 1-Butyl-3-methylimidazolium Tetrafluoroborate, with Benzene, Acetonitrile, and 1-Propanol at T = (293.15 to 343.15) K
rhol	873.58	kg/m3	298.15 Excess Enthalpies of Chloroalkylbenzene + Alkylbenzene Mixtures
rhol	862.84	kg/m3	308.15 Thermodynamic Properties of Ternary Liquid Mixtures Containing o-Chlorotoluene: Excess Molar Volumes and Excess Isentropic Compressibilities

rhol	846.77	kg/m3	323.15 Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	873.54	kg/m3	298.15 Thermodynamic Properties of Ternary Liquid Mixtures Containing o-Chlorotoluene: Excess Molar Volumes and Excess Isentropic Compressibilities
rhol	873.57	kg/m3	298.15 Excess Molar Volumes of 2,4,6,8-Tetramethylcyclotetrasiloxane with Benzene, Toluene, and Xylene at T = (288.15, 298.15, and 308.15) K
rhol	846.60	kg/m3	323.15 Viscometric Behavior of Binary Mixtures of Butan-2-one with Benzene at T = (303.15, 313.15, and 323.15) K
rhol	857.40	kg/m3	313.15 Viscometric Behavior of Binary Mixtures of Butan-2-one with Benzene at T = (303.15, 313.15, and 323.15) K
rhol	868.10	kg/m3	303.15 Viscometric Behavior of Binary Mixtures of Butan-2-one with Benzene at T = (303.15, 313.15, and 323.15) K

rhol	875.47	kg/m3	298.15	Calorimetric Study of Nitrile Group-Solvent Interactions and Comparison with Dispersive Quasi-Chemical (DISQUAC) Predictions	
rhol	873.58	kg/m3	298.15	Volumetric Properties of the Binary Methanol + Chloroform and Ternary Methanol + Chloroform + Benzene Mixtures at (288.15, 293.15, 298.15, 303.15, 308.15, and 313.15) K	
rhol	876.53	kg/m3	293.20	Isobaric Vapor-Liquid Equilibria for Binary Mixtures of 1,2-Dibromoethane with Benzene, Toluene, Fluorobenzene, and Bromobenzene at Atmospheric Pressure	
rhol	873.64	kg/m3	298.15	Vapor-Liquid Equilibria and Excess Enthalpies for Binary Systems of Dimethoxymethane with Hydrocarbons	
rhol	873.45	kg/m3	298.10	Excess Molar Enthalpies of Propyl Propanoate + 1-Hexanol + Benzene at the Temperatures of 25 :C and 35 :C	
rhol	874.00	kg/m3	298.15	Liquid Liquid Equilibrium data for the ternary systems of Water, Isopropyl alcohol, and selected entrainers	

rhol	868.20	kg/m3	303.15	Theoretical and experimental study on volumetric and electromagnetic properties of binary systems consisting of 1,2-dichloroethane with benzene and its derivatives at T = (293.15 to 333.15) K	
sfust	35.40	J/mol×K	278.69	NIST Webbook	
sfust	35.59	J/mol×K	278.65	NIST Webbook	
sfust	33.30	J/mol×K	279.10	NIST Webbook	
sfust	32.10	J/mol×K	278.80	NIST Webbook	
sfust	35.19	J/mol×K	278.60	NIST Webbook	
sfust	35.50	J/mol×K	278.55	NIST Webbook	
sfust	35.90	J/mol×K	278.64	NIST Webbook	
speedsl	1298.27	m/s	298.15	Temperature influence on mixing properties of {ethyl tert-butyl ether (ETBE) + gasoline additives}	
speedsl	1298.30	m/s	298.15	Speeds of Sound and Isentropic Compressibilities for Binary Mixtures of a Cyclic Diether with a Cyclic Compound at Three Temperatures	
speedsl	1229.50	m/s	313.15	Speeds of Sound and Isentropic Compressibilities for Binary Mixtures of a Cyclic Diether with a Cyclic Compound at Three Temperatures	
speedsl	1345.47	m/s	288.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	

speedsl	1368.70	m/s	283.15	Speeds of Sound and Isentropic Compressibilities for Binary Mixtures of a Cyclic Diether with a Cyclic Compound at Three Temperatures	
speedsl	1321.59	m/s	293.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1309.88	m/s	295.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1298.27	m/s	298.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1286.68	m/s	300.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1275.13	m/s	303.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1263.59	m/s	305.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	

speedsl	1252.08	m/s	308.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1240.69	m/s	310.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1229.29	m/s	313.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1217.94	m/s	315.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1206.70	m/s	318.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1195.55	m/s	320.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
speedsl	1184.63	m/s	323.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	

speedsl	1298.00	m/s	298.15	Isentropic Compressibilities Changes of Mixing of Tetrahydropyran and Aromatic Hydrocarbons Ternary Mixtures at 308.15 K
speedsl	1316.50	m/s	293.00	Ultrasonic velocity, viscosity and excess properties of binary mixture of tetrahydrofuran with 1-propanol and 2-propanol
speedsl	1294.00	m/s	298.00	Ultrasonic velocity, viscosity and excess properties of binary mixture of tetrahydrofuran with 1-propanol and 2-propanol
speedsl	1272.80	m/s	303.00	Ultrasonic velocity, viscosity and excess properties of binary mixture of tetrahydrofuran with 1-propanol and 2-propanol
speedsl	1226.50	m/s	313.00	Ultrasonic velocity, viscosity and excess properties of binary mixture of tetrahydrofuran with 1-propanol and 2-propanol
speedsl	1298.20	m/s	298.15	Sound speed and density measurements for tetra-n-butylammonium bromide in benzene and carbon tetrachloride solutions at T = 298.15 K
speedsl	1345.47	m/s	288.15	Temperature influence on mixing properties of {ethyl tert-butyl ether (ETBE) + gasoline additives}

speedsl	1260.00	m/s	308.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene	
speedsl	1300.00	m/s	298.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene	
speedsl	1260.00	m/s	308.15	Densities, Excess Molar Volumes at T = (298.15 to 313.15) K, Speeds of Sound, Excess Isentropic Compressibilities, Relative Permittivities and Deviations in Molar Polarizations at T = (298.15 and 308.15) K for Methyl Methacrylate + 2-Butoxyethanol or + Dibutyl Ether + Benzene, + Toluene and + p-Xylene	

speedsl	1299.00	m/s	298.15	Densities, Excess Molar Volumes at T = (298.15 to 313.15) K, Speeds of Sound, Excess Isentropic Compressibilities, Relative Permittivities and Deviations in Molar Polarizations at T = (298.15 and 308.15) K for Methyl Methacrylate + 2-Butoxyethanol or + Dibutyl Ether + Benzene, + Toluene and + p-Xylene	
speedsl	1184.50	m/s	323.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K	
speedsl	1207.00	m/s	318.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K	
speedsl	1229.80	m/s	313.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K	

speedsl	1252.80	m/s	308.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K	
speedsl	1276.00	m/s	303.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K	
speedsl	1299.30	m/s	298.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K	
speedsl	1322.70	m/s	293.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K	
speedsl	1184.47	m/s	323.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K	
speedsl	1207.04	m/s	318.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K	

speedsl	1229.76	m/s	313.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K	
speedsl	1252.76	m/s	308.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K	
speedsl	1275.96	m/s	303.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K	
speedsl	1299.33	m/s	298.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K	
speedsl	1322.72	m/s	293.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K	
speedsl	1207.80	m/s	318.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods	

speedsl	1229.30	m/s	313.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods	
speedsl	1252.40	m/s	308.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods	
speedsl	1275.70	m/s	303.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods	
speedsl	1299.50	m/s	298.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods	
speedsl	1324.40	m/s	293.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods	

speedsl	1259.00	m/s	308.15	Thermodynamic and topological investigations of molecular interactions in binary and ternary mixtures containing 1-methyl pyrrolidin-2-one at T = 308.15 K	
speedsl	1298.00	m/s	298.15	Thermodynamic and topological investigations of molecular interactions in binary and ternary mixtures containing 1-methyl pyrrolidin-2-one at T = 308.15 K	
speedsl	1184.63	m/s	323.15	Temperature influence on mixing properties of {ethyl tert-butyl ether (ETBE) + gasoline additives}	
speedsl	1333.44	m/s	290.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives	
srf	0.03	N/m	293.20	KDB	
srf	0.03	N/m	280.25	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	
srf	0.03	N/m	283.13	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	
srf	0.03	N/m	285.64	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	
srf	0.03	N/m	288.11	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	

srf	0.03	N/m	290.58	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	
srf	0.03	N/m	293.08	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	
srf	0.03	N/m	295.46	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	
srf	0.03	N/m	298.09	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	
srf	0.03	N/m	300.41	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	
srf	0.03	N/m	303.24	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	
srf	0.03	N/m	306.00	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	
srf	0.03	N/m	308.05	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	
srf	0.03	N/m	310.32	Standard reference data for the air-liquid and vapor-liquid surface tension of benzene	
srf	0.03	N/m	313.44	Standard reference data for the air-liquid and vapor-liquid surface tension	

srf	0.03	N/m	293.15 1-Vir	Investigation of Surface Properties and Solubility of nyl-3-alkyl/Esterimidazolium Halide Ionic Liquids by Density Functional Methods
tcondl	0.15	W/m×K	281.18	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.15	W/m×K	281.49	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.15	W/m×K	281.76	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.14	W/m×K	295.92	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

tcondl	0.14	W/m×K	301.87	Thermal
		· · · · · · · · · · · · · · · · · · ·	001101	Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.14	W/m×K	296.53	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.14	W/m×K	301.25	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.14	W/m×K	301.59	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.13	W/m×K	319.14	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

tcondl	0.13	W/m×K	319.49	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.13	W/m×K	319.79	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.14	W/m×K	302.75	Thermal Conductivity Measurement of Polyglycol Alkyl Ethers at Temperatures from (303.15 to 393.15) K	
tcondl	0.13	W/m×K	332.54	Thermal Conductivity Measurement of Polyglycol Alkyl Ethers at Temperatures from (303.15 to 393.15) K	
tcondl	0.12	W/m×K	362.39	Thermal Conductivity Measurement of Polyglycol Alkyl Ethers at Temperatures from (303.15 to 393.15) K	
tcondl	0.11	W/m×K	392.16	Thermal Conductivity Measurement of Polyglycol Alkyl Ethers at Temperatures from (303.15 to 393.15) K	

tcondl	0.14	W/m×K	296.25	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated	
				Hydrocarbons	

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbp	353.35	K	96.60	Low cost apparatus for rapid boiling point determination of small air sensitive samples under inert atmosphere
tfp	370.85	K	400000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa
tfp	303.15	K	92220.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction
tfp	313.15	K	133290.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction

tfp	323.15	K	176820.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction	
tfp	333.15	К	222810.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction	
tfp	343.15	К	271270.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction	
tfp	353.15	К	322200.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction	
tfp	306.44	K	100000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	
tfp	329.93	К	200000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	

tfp	351.25	K	300000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	
tfp	293.15	K	53620.00	Influence of size and shape effects on the high-pressure solubility of n-alkanes: Experimental data, correlation and prediction	
tfp	389.07	K	500000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	
tfp	406.15	K	600000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	
tfp	422.25	K	700000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	
tfp	437.52	К	800000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	

tfp	452.06	K	900000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	
tfp	465.96	К	100000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	
tfp	538.73	К	1500000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	
tfp	584.85	К	2000000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	
tfp	625.73	K	2500000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	

tfp	663.67	К	300000.00	Fusion Curves and Enthalpy and Internal Energy Changes of Benzene, Nitrobenzene, Bromobenzene, and Chlorobenzene at Pressures up to 3500 MPa	
tfp	278.94	К	100.00	Activity coefficient at infinite dilution, azeotropic data, excess enthalpies and solid liquid-equilibria for binary systems of alkanes and aromatics with esters	

Correlations

Information Value

Property code	pvap
Equation	In(Pvp) = A + B/(T + C)
Coeff. A	1.36756e+01
Coeff. B	-2.51081e+03
Coeff. C	-7.60040e+01
Temperature range (K), min.	263.55
Temperature range (K), max.	376.19

Information Value

Property code	pvap	
Equation	$ln(Pvp) = A + B/T + C*ln(T) + D*T^2$	
Coeff. A	7.11072e+01	
Coeff. B	-6.28104e+03	
Coeff. C	-8.43361e+00	
Coeff. D	6.19841e-06	
Temperature range (K), min.	278.68	
Temperature range (K), max.	562.16	

Datasets

Mass density, kg/m3

Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
2100.00	877.4
3100.00	878.1
4100.00	878.8
5000.00	879.6
10100.00	883.4
20000.00	890.4
30000.00	896.9
40000.00	902.9
50000.00	908.6
60000.00	914.0
70000.00	919.6
2100.00	857.0
3100.00	857.8
4100.00	858.7
5000.00	859.6
10100.00	863.9
20000.00	871.5
30000.00	878.7
40000.00	885.2
50000.00	891.6
60000.00	897.5
70000.00	902.9
2100.00	835.1
3100.00	836.0
4100.00	837.0
5000.00	838.0
10100.00	842.7
20000.00	851.8
30000.00	859.4
40000.00	867.0
50000.00	874.2
60000.00	880.8
70000.00	886.7
2100.00	813.1
3100.00	814.2
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353.00	4100.00	815.4
353.00	5000.00	816.5
353.00	10100.00	822.3
353.00	20000.00	832.3
353.00	30000.00	841.2
353.00	40000.00	849.5
353.00	50000.00	857.0
353.00	60000.00	864.3
353.00	70000.00	871.2
373.00	2100.00	790.7
373.00	3100.00	792.1
373.00	4100.00	793.4
373.00	5000.00	794.7
373.00	10100.00	801.4
373.00	20000.00	812.9
373.00	30000.00	823.1
373.00	40000.00	832.3
373.00	50000.00	840.7
373.00	60000.00	848.2
373.00	70000.00	855.7
393.00	2100.00	767.6
393.00	3100.00	769.4
393.00	4100.00	770.9
393.00	5000.00	772.5
393.00	10100.00	780.0
393.00	20000.00	793.0
393.00	30000.00	804.5
393.00	40000.00	814.6
393.00	50000.00	824.0
393.00	60000.00	832.6
393.00	70000.00	841.0
413.00	2100.00	743.0
413.00	3100.00	745.1
413.00	4100.00	747.0
413.00	5000.00	748.8
413.00	10100.00	758.0
413.00	20000.00	773.2
413.00	30000.00	786.2
413.00	40000.00	797.5
413.00	50000.00	807.8
413.00	60000.00	817.2
413.00	70000.00	825.8
433.00	2100.00	716.7
433.00	3100.00	719.4

433.00	4100.00	721.8
433.00	5000.00	724.0
433.00	10100.00	735.4
433.00	20000.00	753.0
433.00	30000.00	767.8
433.00	40000.00	780.3
433.00	50000.00	791.6
433.00	60000.00	801.7
433.00	70000.00	811.0
448.00	2100.00	696.0
448.00	3100.00	699.2
448.00	4100.00	702.1
448.00	5000.00	704.8
448.00	10100.00	717.8
448.00	20000.00	738.0
448.00	30000.00	754.2
448.00	40000.00	767.8
448.00	50000.00	779.8
448.00	60000.00	790.6
448.00	70000.00	800.3
468.00	2100.00	666.9
468.00	3100.00	670.7
468.00	4100.00	674.3
468.00	5000.00	677.8
468.00	10100.00	693.2
468.00	20000.00	717.0
468.00	30000.00	735.1
468.00	40000.00	750.3
468.00	50000.00	763.6
468.00	60000.00	775.5
468.00	70000.00	786.1

Reference

https://www.doi.org/10.1016/j.fluid.2016.09.021

Speed of sound, m/s

Temperature, K - Liquid	Pressure, kPa - Liquid	Speed of sound, m/s - Liquid
283.15	101.00	1371.6
283.15	1112.00	1376.8
283.15	2281.00	1382.4
283.15	4616.00	1393.2

283.15	6766.00	1403.3
283.15	9100.00	1413.6
283.15	11628.00	1424.5
283.15	14278.00	1436.0
283.15	15957.00	1443.4
283.15	18556.00	1454.0
283.15	20823.00	1463.0
283.15	23405.00	1473.4
298.15	101.00	1299.9
298.15	888.00	1305.0
298.15	1246.00	1305.8
298.15	2254.00	1311.8
298.15	2506.00	1312.2
298.15	4580.00	1322.5
298.15	4719.00	1323.9
298.15	6991.00	1334.4
298.15	7131.00	1335.5
298.15	9327.00	1346.2
298.15	9335.00	1346.2
298.15	9408.00	1346.0
298.15	11563.00	1355.8
298.15	11640.00	1357.0
298.15	14137.00	1368.5
298.15	14317.00	1368.6
298.15	15927.00	1375.9
298.15	16524.00	1379.1
298.15	18655.00	1388.6
298.15	18844.00	1389.0
298.15	20826.00	1398.1
298.15	21001.00	1398.6
298.15	23151.00	1407.9
298.15	23834.00	1410.7
298.15	25699.00	1418.5
298.15	26172.00	1420.5
298.15	28369.00	1428.5
298.15	101.00	1300.2
313.15	101.00	1230.8
313.15	2047.00	1241.3
313.15	3268.00	1247.8
313.15	5111.00	1257.8
313.15	7199.00	1268.7
313.15	9383.00	1280.0
313.15	11613.00	1291.3
313.15	14139.00	1303.7

313.15	16386.00	1314.6
313.15	18686.00	1325.5
313.15	21242.00	1337.2
313.15	23254.00	1346.4
313.15	24384.00	1351.3
313.15	25607.00	1357.2
313.15	25608.00	1357.3
313.15	28210.00	1368.6
333.15	101.00	1142.4
333.15	1260.00	1148.0
333.15	2426.00	1155.0
333.15	5026.00	1170.5
333.15	7135.00	1182.9
333.15	9195.00	1194.5
333.15	11729.00	1208.4
333.15	14011.00	1220.6
333.15	16310.00	1232.7
333.15	18687.00	1244.8
333.15	20059.00	1251.8
333.15	21112.00	1257.2
333.15	23196.00	1267.4
333.15	25517.00	1278.7
333.15	28165.00	1287.7

Reference

https://www.doi.org/10.1016/j.jct.2004.04.013

Temperature, K	Pressure, kPa	Frequency, MHz	Speed of sound, m/s
303.15	101.33	2.0	1257.0
Reference		https://www.c	doi.org/10.1016/j.jct.2004.12.001

Pressure, kPa	Temperature, K	Speed of sound, m/s
29815.10	283.21	1498.11
24857.00	283.20	1479.03
20203.80	283.20	1460.21
15331.80	283.20	1439.87
10233.80	283.20	1418.25
5280.10	283.20	1395.99
102.10	283.20	1372.03
30106.10	298.20	1436.88
25017.80	298.20	1415.76
20104.10	298.20	1394.27

14866.50	298.20	1371.03
10068.60	298.20	1349.48
5421.70	298.20	1326.99
84.20	298.20	1299.74
29980.00	313.20	1375.67
25204.40	313.20	1354.82
20194.50	313.20	1332.15
15331.60	313.20	1309.02
10140.00	313.20	1283.5
5536.50	313.20	1259.76
61.20	313.20	1230.41
30145.60	333.21	1299.17
24756.40	333.21	1273.95
19600.70	333.21	1248.51
15038.40	333.21	1225.05
10149.20	333.21	1198.3
5378.80	333.21	1171.44
153.70	333.21	1139.68
30063.00	353.21	1225.96
24679.70	353.21	1198.74
19917.50	353.20	1173.19
15092.20	353.20	1146.64
10006.90	353.21	1116.2
5094.90	353.21	1084.94
172.30	353.21	1052.25

Reference https://www.doi.org/10.1021/je501065g

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
313.20	690.00	0.0004790
313.20	5000.00	0.0005000
313.20	10000.00	0.0005240
313.20	20000.00	0.0005740
313.20	30000.00	0.0006250
313.20	40000.00	0.0006750
313.20	50000.00	0.0007250
313.20	60000.00	0.0007740
333.20	690.00	0.0003870
333.20	5000.00	0.0004040

333.20	10000.00	0.0004240
333.20	20000.00	0.0004660
333.20	30000.00	0.0005090
333.20	40000.00	0.0005530
333.20	50000.00	0.0005970
333.20	60000.00	0.0006410
353.20	690.00	0.0003170
353.20	5000.00	0.0003310
353.20	10000.00	0.0003470
353.20	20000.00	0.0003800
353.20	30000.00	0.0004150
353.20	40000.00	0.0004510
353.20	50000.00	0.0004890
353.20	60000.00	0.0005260
373.20	690.00	0.0002690
373.20	5000.00	0.0002790
373.20	10000.00	0.0002910
373.20	20000.00	0.0003160
373.20	30000.00	0.0003440
373.20	40000.00	0.0003720
373.20	50000.00	0.0004020
373.20	60000.00	0.0004340
393.20	690.00	0.0002390
393.20	5000.00	0.0002460
393.20	10000.00	0.0002550
393.20	20000.00	0.0002730
393.20	30000.00	0.0002940
393.20	40000.00	0.0003150
393.20	50000.00	0.0003390
393.20	60000.00	0.0003640

Reference

https://www.doi.org/10.1016/j.fluid.2007.08.010

Temperature, K	Pressure, kPa	Viscosity, Pa*s
303.15	101.30	0.0005390
Reference		https://www.doi.org/10.1021/je034204h

Sources

Infinite dilution activity coefficients of https://www.doi.org/10.1016/j.jct.2013.05.035 volatile organic compounds in two Effection peraps seen the volumetric https://www.doi.org/10.1016/j.jct.2004.07.010 Effection (new perstars conditions of the persistent of conditions of the persistent https://www.doi.org/10.1016/j.jct.2014.04.024 https://www.doi.org/10.1016/j.fluid.2006.01.014 https://www.doi.org/10.1016/j.jct.2008.12.005 https://www.doi.org/10.1016/j.fluid.2010.09.021 https://www.doi.org/10.1016/j.jct.2014.05.020 https://www.doi.org/10.1016/j.jct.2009.06.011 https://www.doi.org/10.1016/j.jct.2016.09.021 date of Anythms consisting of the LLE https://www.doi.org/10.1010/j.jct.2016.0 date of Anythms of the LLE https://www.doi.org/10.1021/je501111d https://www.doi.org/10.1021/je501111d https://www.doi.org/10.1021/je100341q braphyrics/waisected Solvents:

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Extractive Distillation:

Densities and Volumetric Properties of https://www.doi.org/10.1007/s10765-010-0768-y Binary Mixtures of Butyl Acrylate with Belizante, frontlembinical multiplembine and arrowalism and with Belight Michigan and are and with Belight Michigan and are and https://www.doi.org/10.1016/j.jct.2009.11.001 http://pubs.acs.org/doi/abs/10.1021/ci990307l diphatic hydrocarbons: Measurement of activity coefficients at https://www.doi.org/10.1016/j.jct.2013.10.017 infinite dilution of organic solutes in the infinite dilution Activity crefficients at infinite dilution and physical corporations for properties for properties for properties for the control of the cont https://www.doi.org/10.1016/j.jct.2013.05.008 https://www.doi.org/10.1016/j.tca.2015.04.011 https://www.doi.org/10.1016/j.fluid.2014.07.034 https://www.doi.org/10.1016/j.fluid.2018.09.024 https://www.doi.org/10.1016/j.fluid.2016.02.028 https://www.doi.org/10.1016/j.fluid.2014.03.003 https://www.doi.org/10.1016/j.jct.2012.03.015 Model for Predicting the Solubility of Liquid-Diguid Estatiling A-PerBeerstore https://www.doi.org/10.1021/je900324s ACING PARTICIPANTS OF THE COLUMN https://www.doi.org/10.1016/j.jct.2013.10.038 https://www.doi.org/10.1016/j.jct.2007.11.009 THE TRANSPORT OF THE PROPERTY https://www.doi.org/10.1016/j.fluid.2013.10.033 https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=651 https://www.doi.org/10.1021/je9008443 of Organic Solutes in Interpretation of Organic Solutes in Interpretation of Interpr https://www.doi.org/10.1021/je500050p https://www.doi.org/10.1021/je010317u http://webbook.nist.gov/cgi/cbook.cgi?ID=C71432&Units=SI

Legend

af: Acentric Factor affp: Proton affinity

aigt: Autoignition Temperature

basg: Gas basicity

cpg: Ideal gas heat capacitycpl: Liquid phase heat capacitycps: Solid phase heat capacity

dm: Dipole Momentdvisc: Dynamic viscosity

fli: Lower Flammability Limit flu: Upper Flammability Limit

fpo: Flash Point (Open Cup Method)

gf: Standard Gibbs free energy of formation

gyrad: Radius of Gyration

hcg: Heat of Combustion, Gross form hcn: Heat of Combustion, Net Form

hf: Enthalpy of formation at standard conditions

hfl: Liquid phase enthalpy of formation at standard conditions

hfus: Enthalpy of fusion at standard conditions hfust: Enthalpy of fusion at a given temperature

hsub: Enthalpy of sublimation at standard conditions hsubt: Enthalpy of sublimation at a given temperature hvap: Enthalpy of vaporization at standard conditions hvapt: Enthalpy of vaporization at a given temperature

ie: Ionization energy

log10ws: Log10 of Water solubility in mol/l logp: Octanol/Water partition coefficient McGowan's characteristic volume mcvol:

NFPA Fire Rating nfpaf: NFPA Health Rating nfpah: Critical Pressure pc: psub: Sublimation pressure

pvap: Vapor pressure rfi: Refractive Index rhoc: Critical density rhol: Liquid Density

rinpol: Non-polar retention indices ripol: Polar retention indices

sfust:

Entropy of fusion at a given temperature

sl: Liquid phase molar entropy at standard conditions

speedsl: Speed of sound in fluid

Surface Tension srf:

ss: Solid phase molar entropy at standard conditions

tb: Normal Boiling Point Temperature tbp: Boiling point at given pressure

tc: Critical Temperature

tcondl: Liquid thermal conductivity Normal melting (fusion) point tf:

Melting point tfp: vc: Critical Volume Specific Volume vols:

ZC: Critical Compressibility Rackett Parameter zra:

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