

Propane

Other names:	A-108
	C3H8
	Dimethylmethane
	Freon 290
	HC 290
	Hydrocarbon propellant A-108
	LPG
	Liquefied petroleum gas
	Propyl hydride
	R 290
	UN 1978
	n-Propane
Inchi:	InChI=1S/C3H8/c1-3-2/h3H2,1-2H3
InchiKey:	ATUOYWHBWRKTHZ-UHFFFAOYSA-N
Formula:	C3H8
SMILES:	CCC
Mol. weight [g/mol]:	44.10
CAS:	74-98-6

Physical Properties

Property code	Value	Unit	Source
af	0.1530		KDB
affp	625.70	kJ/mol	NIST Webbook
aigt	723.15	K	KDB
basg	607.80	kJ/mol	NIST Webbook
chg	-2204.00 ± 0.54	kJ/mol	NIST Webbook
chg	-2207.00	kJ/mol	NIST Webbook
chg	-2219.20 ± 0.46	kJ/mol	NIST Webbook
chg	-2219.90 ± 0.50	kJ/mol	NIST Webbook
dm	0.00	debye	KDB
fil	2.10	% in Air	KDB
flu	9.50	% in Air	KDB
fpo	168.71	K	KDB
gf	-23.49	kJ/mol	KDB
gyrad	2.4260		KDB
hcg	2203.42	kJ/mol	KDB
hcn	2027.399	kJ/mol	KDB

hf	-103.80 ± 0.59	kJ/mol	NIST Webbook
hf	-103.90	kJ/mol	KDB
hf	-104.70 ± 0.50	kJ/mol	NIST Webbook
hfl	-119.80 ± 0.59	kJ/mol	NIST Webbook
hfus	3.53	kJ/mol	Joback Method
hvap	16.25	kJ/mol	NIST Webbook
ie	10.97	eV	NIST Webbook
ie	10.95 ± 0.05	eV	NIST Webbook
ie	11.22	eV	NIST Webbook
ie	11.12	eV	NIST Webbook
ie	11.07	eV	NIST Webbook
ie	11.51	eV	NIST Webbook
ie	11.09 ± 0.05	eV	NIST Webbook
ie	11.06	eV	NIST Webbook
ie	10.94 ± 0.05	eV	NIST Webbook
ie	11.01 ± 0.07	eV	NIST Webbook
ie	11.27 ± 0.05	eV	NIST Webbook
ie	10.90 ± 0.10	eV	NIST Webbook
ie	10.96	eV	NIST Webbook
ie	11.00 ± 1.00	eV	NIST Webbook
ie	10.94 ± 0.05	eV	NIST Webbook
ie	11.50 ± 0.10	eV	NIST Webbook
ie	11.50	eV	NIST Webbook
ie	11.50	eV	NIST Webbook
ie	11.07	eV	NIST Webbook
log10ws	-2.19		Aqueous Solubility Prediction Method
log10ws	-1.94		Estimated Solubility Method
logp	1.416		Crippen Method
mcvol	53.130	ml/mol	McGowan Method
nfpaf	%!d(float64=4)		KDB
nfpah	%!d(float64=1)		KDB
pc	4248.00	kPa	KDB
pc	4260.00	kPa	Critical parameters for propane determined by the image analysis
pc	4247.00	kPa	Critical Properties of Three Dimethyl Ether Binary Systems: Dimethyl Ether (RE-170) + Propane (HC-290), Butane (HC-600), and 2-Methyl Propane (HC-600A)
pt	1.69e-07	kPa	NIST Webbook
pt	1.69e-07 ± 1.00e-10	kPa	NIST Webbook
rhoc	224.01 ± 1.50	kg/m3	NIST Webbook
rhoc	232.30 ± 3.97	kg/m3	NIST Webbook

rhoc	245.17 ± 3.09	kg/m3	NIST Webbook
rhoc	220.30 ± 3.97	kg/m3	NIST Webbook
rhoc	220.04 ± 0.44	kg/m3	NIST Webbook
rhoc	230.18 ± 19.84	kg/m3	NIST Webbook
rhoc	220.48	kg/m3	NIST Webbook
rhoc	218.49 ± 2.20	kg/m3	NIST Webbook
rhoc	2.20e-04	kg/m3	NIST Webbook
rhoc	212.98 ± 0.21	kg/m3	NIST Webbook
rhoc	213.86 ± 2.13	kg/m3	NIST Webbook
rhoc	226.21 ± 2.20	kg/m3	NIST Webbook
rhoc	216.95 ± 3.09	kg/m3	NIST Webbook
rhoc	216.95	kg/m3	NIST Webbook
rhoc	220.49 ± 3.09	kg/m3	NIST Webbook
sl	171.00	J/mol×K	NIST Webbook
tb	231.00	K	KDB
tc	369.76 ± 0.10	K	NIST Webbook
tc	369.96 ± 0.05	K	NIST Webbook
tc	373.30 ± 0.55	K	NIST Webbook
tc	367.80 ± 0.60	K	NIST Webbook
tc	370.70 ± 1.00	K	NIST Webbook
tc	370.15 ± 1.00	K	NIST Webbook
tc	370.00 ± 3.00	K	NIST Webbook
tc	375.00 ± 5.00	K	NIST Webbook
tc	369.81 ± 0.22	K	NIST Webbook
tc	369.90 ± 0.40	K	NIST Webbook
tc	370.00 ± 0.40	K	NIST Webbook
tc	370.02 ± 0.20	K	NIST Webbook
tc	369.81 ± 0.06	K	NIST Webbook
tc	369.74 ± 0.20	K	NIST Webbook
tc	369.75 ± 0.15	K	NIST Webbook
tc	369.75 ± 0.15	K	NIST Webbook
tc	369.75 ± 0.15	K	NIST Webbook
tc	369.80 ± 0.15	K	NIST Webbook
tc	372.00 ± 2.22	K	NIST Webbook
tc	369.76 ± 0.10	K	NIST Webbook
tc	369.74 ± 0.20	K	NIST Webbook
tc	369.80	K	NIST Webbook
tc	369.80 ± 0.00	K	NIST Webbook
tc	369.85 ± 0.10	K	NIST Webbook
tc	369.85	K	NIST Webbook
tc	369.80	K	NIST Webbook
tc	369.98 ± 0.05	K	NIST Webbook
tc	369.85 ± 0.07	K	NIST Webbook
tc	369.91 ± 0.10	K	NIST Webbook

tc	369.82	K	NIST Webbook
tc	369.83 ± 0.10	K	NIST Webbook
tc	364.59 ± 0.15	K	NIST Webbook
tc	369.77 ± 0.20	K	NIST Webbook
tc	369.80 ± 0.10	K	NIST Webbook
tc	369.84	K	Validation of a New Apparatus Using the Dynamic Method for Determining the Critical Properties of Binary Gas/Gas Mixtures
tc	369.83	K	KDB
tc	370.20 ± 1.00	K	NIST Webbook
tc	370.00 ± 0.20	K	NIST Webbook
tc	370.45 ± 1.00	K	NIST Webbook
tf	83.25 ± 0.50	K	NIST Webbook
tf	85.50 ± 0.20	K	NIST Webbook
tf	85.46	K	KDB
tf	85.35	K	Aqueous Solubility Prediction Method
tf	85.35 ± 0.50	K	NIST Webbook
tf	85.46 ± 0.20	K	NIST Webbook
tf	86.05 ± 0.15	K	NIST Webbook
tt	85.53	K	Thermodynamic Properties of Propane. II. Molar Heat Capacity at Constant Volume from (85 to 345) K with Pressures to 35 MPa
tt	81.22 ± 0.00	K	NIST Webbook
tt	85.52 ± 0.01	K	NIST Webbook
tt	85.47 ± 0.05	K	NIST Webbook
tt	83.25 ± 0.30	K	NIST Webbook
tt	85.52	K	KDB
tt	85.47 ± 0.05	K	NIST Webbook
tt	85.47	K	NIST Webbook
tt	85.45 ± 0.07	K	NIST Webbook
vc	0.198 ± 0.004	m3/kmol	NIST Webbook
vc	0.200	m3/kmol	NIST Webbook
vc	0.200	m3/kmol	KDB
vc	0.200 ± 0.001	m3/kmol	NIST Webbook
vc	0.202 ± 0.003	m3/kmol	NIST Webbook
zc	0.2762970		KDB
zra	0.28		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	140.62	J/mol×K	693.15	NIST Webbook
cpg	128.66	J/mol×K	603.25	NIST Webbook
cpg	121.75	J/mol×K	561.95	NIST Webbook
cpg	116.69	J/mol×K	521.15	NIST Webbook
cpg	104.89	J/mol×K	452.55	NIST Webbook
cpg	90.46	J/mol×K	387.75	NIST Webbook
cpg	87.45	J/mol×K	368.55	NIST Webbook
cpg	85.19	J/mol×K	360.05	NIST Webbook
cpg	84.40 ± 0.08	J/mol×K	353.15	NIST Webbook
cpg	82.26	J/mol×K	343.65	NIST Webbook
cpg	80.54	J/mol×K	334.05	NIST Webbook
cpg	80.30 ± 0.08	J/mol×K	333.15	NIST Webbook
cpg	76.11 ± 0.08	J/mol×K	313.15	NIST Webbook
cpg	73.55	J/mol×K	300.37	NIST Webbook
cpg	72.67 ± 0.07	J/mol×K	293.15	NIST Webbook
cpg	67.74	J/mol×K	272.38	NIST Webbook
cpg	65.90	J/mol×K	258.00	NIST Webbook
cpg	59.29	J/mol×K	219.20	NIST Webbook
cpg	58.58	J/mol×K	213.10	NIST Webbook
cpg	50.38	J/mol×K	157.80	NIST Webbook
cpg	48.91	J/mol×K	148.20	NIST Webbook
cpl	98.28	J/mol×K	230.00	NIST Webbook
cpl	119.60	J/mol×K	300.00	NIST Webbook
cpl	98.36	J/mol×K	230.00	NIST Webbook
dvisc	0.0001447	Pa×s	268.04	Joback Method
dvisc	0.0001801	Pa×s	243.96	Joback Method
dvisc	0.0002350	Pa×s	219.88	Joback Method
dvisc	0.0003273	Pa×s	195.80	Joback Method
dvisc	0.0005005	Pa×s	171.73	Joback Method
dvisc	0.0008789	Pa×s	147.65	Joback Method
dvisc	0.0019221	Pa×s	123.57	Joback Method
hfust	3.52	kJ/mol	85.50	NIST Webbook
hfust	3.52	kJ/mol	85.50	NIST Webbook
hfust	3.51	kJ/mol	85.50	NIST Webbook
hsubt	28.50	kJ/mol	86.00	NIST Webbook
hvapt	19.20	kJ/mol	349.00	NIST Webbook
hvapt	19.00	kJ/mol	256.00	NIST Webbook
hvapt	22.10	kJ/mol	134.50	NIST Webbook
hvapt	19.50	kJ/mol	206.50	NIST Webbook

hvapt	18.80	kJ/mol	305.00	NIST Webbook
hvapt	18.90	kJ/mol	339.50	NIST Webbook
hvapt	18.77	kJ/mol	231.04	NIST Webbook
hvapt	18.77	kJ/mol	231.10	KDB
hvapt	18.77	kJ/mol	256.00	NIST Webbook
hvapt	20.00	kJ/mol	198.50	NIST Webbook
hvapt	19.04	kJ/mol	231.10	NIST Webbook
pvap	3822.46	kPa	364.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	574.00	kPa	279.47	Isothermal Vapor-Liquid Equilibria for 1,1-Difluoroethane (R152a) + Propane (R290) at Temperatures between (254.31 and 287.94) K
pvap	422.00	kPa	269.26	Isothermal Vapor-Liquid Equilibria for 1,1-Difluoroethane (R152a) + Propane (R290) at Temperatures between (254.31 and 287.94) K
pvap	303.00	kPa	259.27	Isothermal Vapor-Liquid Equilibria for 1,1-Difluoroethane (R152a) + Propane (R290) at Temperatures between (254.31 and 287.94) K
pvap	257.00	kPa	254.31	Isothermal Vapor-Liquid Equilibria for 1,1-Difluoroethane (R152a) + Propane (R290) at Temperatures between (254.31 and 287.94) K
pvap	4183.04	kPa	369.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	4182.95	kPa	369.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	4182.88	kPa	369.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	4182.82	kPa	369.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	4108.59	kPa	368.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	4108.52	kPa	368.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	4108.41	kPa	368.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	4108.37	kPa	368.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3963.03	kPa	366.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3962.97	kPa	366.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	3962.97	kPa	366.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3962.93	kPa	366.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3892.08	kPa	365.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3892.07	kPa	365.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3892.02	kPa	365.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3891.97	kPa	365.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3892.00	kPa	365.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3822.47	kPa	364.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	727.00	kPa	287.94	Isothermal Vapor-Liquid Equilibria for 1,1-Difluoroethane (R152a) + Propane (R290) at Temperatures between (254.31 and 287.94) K	
pvap	1906.00	kPa	327.97	Phase equilibrium data for mixtures involving 1,1,2,3,3,3-hexafluoro-1-propene with either propane or n-butane between 312 and 343 K	
pvap	3822.43	kPa	364.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa	
pvap	3822.44	kPa	364.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa	
pvap	3686.50	kPa	362.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa	
pvap	3686.37	kPa	362.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa	
pvap	3686.37	kPa	362.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa	
pvap	3686.35	kPa	362.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa	

pvap	3554.51	kPa	360.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3554.45	kPa	360.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3554.50	kPa	360.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3555.07	kPa	360.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3554.44	kPa	360.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3554.39	kPa	360.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3555.10	kPa	360.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3555.09	kPa	360.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	583.10	kPa	280.00	Measurements of Vapor Pressures from 280 to 369 K and (p, rho, T) Properties from 340 to 400 K at Pressures to 200 MPa for Propane
pvap	999.00	kPa	300.00	Measurements of Vapor Pressures from 280 to 369 K and (p, rho, T) Properties from 340 to 400 K at Pressures to 200 MPa for Propane
pvap	1599.80	kPa	320.00	Measurements of Vapor Pressures from 280 to 369 K and (p, rho, T) Properties from 340 to 400 K at Pressures to 200 MPa for Propane
pvap	2432.20	kPa	340.00	Measurements of Vapor Pressures from 280 to 369 K and (p, rho, T) Properties from 340 to 400 K at Pressures to 200 MPa for Propane
pvap	3556.30	kPa	360.00	Measurements of Vapor Pressures from 280 to 369 K and (p, rho, T) Properties from 340 to 400 K at Pressures to 200 MPa for Propane
pvap	3894.10	kPa	365.00	Measurements of Vapor Pressures from 280 to 369 K and (p, rho, T) Properties from 340 to 400 K at Pressures to 200 MPa for Propane
pvap	4036.80	kPa	367.00	Measurements of Vapor Pressures from 280 to 369 K and (p, rho, T) Properties from 340 to 400 K at Pressures to 200 MPa for Propane

pvap	4184.40	kPa	369.00	Measurements of Vapor Pressures from 280 to 369 K and (p, rho, T) Properties from 340 to 400 K at Pressures to 200 MPa for Propane
pvap	244.20	kPa	253.15	Vapor liquid equilibria for the carbon dioxide + propane system over a temperature range from 253.15 to 323.15K
pvap	344.70	kPa	263.15	Vapor liquid equilibria for the carbon dioxide + propane system over a temperature range from 253.15 to 323.15K
pvap	473.90	kPa	273.15	Vapor liquid equilibria for the carbon dioxide + propane system over a temperature range from 253.15 to 323.15K
pvap	636.30	kPa	283.15	Vapor liquid equilibria for the carbon dioxide + propane system over a temperature range from 253.15 to 323.15K
pvap	836.30	kPa	293.15	Vapor liquid equilibria for the carbon dioxide + propane system over a temperature range from 253.15 to 323.15K
pvap	1079.60	kPa	303.15	Vapor liquid equilibria for the carbon dioxide + propane system over a temperature range from 253.15 to 323.15K

pvap	1369.80	kPa	313.15	Vapor liquid equilibria for the carbon dioxide + propane system over a temperature range from 253.15 to 323.15K
pvap	1714.50	kPa	323.15	Vapor liquid equilibria for the carbon dioxide + propane system over a temperature range from 253.15 to 323.15K
pvap	407.90	kPa	268.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures
pvap	474.60	kPa	273.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures
pvap	549.40	kPa	278.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures
pvap	636.60	kPa	283.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures

pvap	735.00	kPa	288.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures
pvap	836.20	kPa	293.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures
pvap	954.80	kPa	298.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures
pvap	1078.40	kPa	303.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures
pvap	1213.00	kPa	308.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures

pvap	1363.80	kPa	313.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures
pvap	1369.00	kPa	313.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures
pvap	1530.80	kPa	318.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures
pvap	1709.20	kPa	323.15	Measurement of vapor liquid equilibria for the binary systems of propane + 1,1,1,2-tetrafluoroethane and 1,1,1-trifluoroethane + propane at various temperatures
pvap	474.00	kPa	273.15	Measurement of vapor liquid equilibria for the binary mixture of propylene (R-1270) + propane (R-290)
pvap	550.80	kPa	278.15	Measurement of vapor liquid equilibria for the binary mixture of propylene (R-1270) + propane (R-290)

pvap	636.00	kPa	283.15	Measurement of vapor liquid equilibria for the binary mixture of propylene (R-1270) + propane (R-290)
pvap	836.20	kPa	293.15	Measurement of vapor liquid equilibria for the binary mixture of propylene (R-1270) + propane (R-290)
pvap	1077.60	kPa	303.15	Measurement of vapor liquid equilibria for the binary mixture of propylene (R-1270) + propane (R-290)
pvap	1368.00	kPa	313.15	Measurement of vapor liquid equilibria for the binary mixture of propylene (R-1270) + propane (R-290)
pvap	1374.00	kPa	313.15	Vapor liquid equilibria of the 1,1,1-trifluoroethane (HFC-143a) + propane (HC-290) system
pvap	1712.00	kPa	323.15	Vapor liquid equilibria of the 1,1,1-trifluoroethane (HFC-143a) + propane (HC-290) system
pvap	2115.00	kPa	333.15	Vapor liquid equilibria of the 1,1,1-trifluoroethane (HFC-143a) + propane (HC-290) system
pvap	2586.00	kPa	343.15	Vapor liquid equilibria of the 1,1,1-trifluoroethane (HFC-143a) + propane (HC-290) system
pvap	3151.00	kPa	353.15	Vapor liquid equilibria of the 1,1,1-trifluoroethane (HFC-143a) + propane (HC-290) system

pvap	3767.00	kPa	363.15	Vapor liquid equilibria of the 1,1,1-trifluoroethane (HFC-143a) + propane (HC-290) system
pvap	345.90	kPa	263.15	Isothermal vapor liquid equilibria for the pentafluoroethane + propane and pentafluoroethane + 1,1,1,2,3,3,3-heptafluoropropane systems
pvap	552.70	kPa	278.15	Isothermal vapor liquid equilibria for the pentafluoroethane + propane and pentafluoroethane + 1,1,1,2,3,3,3-heptafluoropropane systems
pvap	839.70	kPa	293.15	Isothermal vapor liquid equilibria for the pentafluoroethane + propane and pentafluoroethane + 1,1,1,2,3,3,3-heptafluoropropane systems
pvap	1217.20	kPa	308.15	Isothermal vapor liquid equilibria for the pentafluoroethane + propane and pentafluoroethane + 1,1,1,2,3,3,3-heptafluoropropane systems
pvap	1714.50	kPa	323.15	Isothermal vapor liquid equilibria for the pentafluoroethane + propane and pentafluoroethane + 1,1,1,2,3,3,3-heptafluoropropane systems
pvap	852.60	kPa	293.94	Infinite dilution activity coefficient and vapour liquid equilibrium measurements for dimethylsulphide and tetrahydrothiophene with hydrocarbons

pvap	853.10	kPa	293.97	Infinite dilution activity coefficient and vapour liquid equilibrium measurements for dimethylsulphide and tetrahydrothiophene with hydrocarbons
pvap	1358.50	kPa	312.85	Infinite dilution activity coefficient and vapour liquid equilibrium measurements for dimethylsulphide and tetrahydrothiophene with hydrocarbons
pvap	1361.30	kPa	312.87	Infinite dilution activity coefficient and vapour liquid equilibrium measurements for dimethylsulphide and tetrahydrothiophene with hydrocarbons
pvap	1072.00	kPa	302.97	Phase equilibrium data for mixtures involving 1,1,2,3,3,3-hexafluoro-1-propene with either propane or n-butane between 312 and 343 K
pvap	1214.00	kPa	307.96	Phase equilibrium data for mixtures involving 1,1,2,3,3,3-hexafluoro-1-propene with either propane or n-butane between 312 and 343 K
pvap	1361.00	kPa	312.99	Phase equilibrium data for mixtures involving 1,1,2,3,3,3-hexafluoro-1-propene with either propane or n-butane between 312 and 343 K

pvap	1522.00	kPa	317.89	Phase equilibrium data for mixtures involving 1,1,2,3,3,3-hexafluoro-1-propene with either propane or n-butane between 312 and 343 K
pvap	1712.00	kPa	322.99	Phase equilibrium data for mixtures involving 1,1,2,3,3,3-hexafluoro-1-propene with either propane or n-butane between 312 and 343 K
pvap	3554.47	kPa	360.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2103.00	kPa	332.93	Phase equilibrium data for mixtures involving 1,1,2,3,3,3-hexafluoro-1-propene with either propane or n-butane between 312 and 343 K
pvap	2336.00	kPa	337.91	Phase equilibrium data for mixtures involving 1,1,2,3,3,3-hexafluoro-1-propene with either propane or n-butane between 312 and 343 K
pvap	2582.00	kPa	342.91	Phase equilibrium data for mixtures involving 1,1,2,3,3,3-hexafluoro-1-propene with either propane or n-butane between 312 and 343 K

pvap	6.00e-04	kPa	110.00	Measurement of the (p,.rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	3.20e-03	kPa	120.00	Measurement of the (p,.rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	0.02	kPa	130.00	Measurement of the (p,.rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	0.08	kPa	140.00	Measurement of the (p,.rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter

pvap	0.28	kPa	150.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	0.85	kPa	160.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	2.21	kPa	170.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	5.07	kPa	180.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter

pvap	10.55	kPa	190.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	20.19	kPa	200.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	36.03	kPa	210.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	60.57	kPa	220.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter

pvap	96.78	kPa	230.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	148.00	kPa	240.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	217.96	kPa	250.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	310.69	kPa	260.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter

pvap	430.43	kPa	270.00	Measurement of the (p,ρ,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	581.68	kPa	280.00	Measurement of the (p,ρ,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	769.14	kPa	290.00	Measurement of the (p,ρ,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	997.68	kPa	300.00	Measurement of the (p,ρ,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter

pvap	1272.43	kPa	310.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	1598.87	kPa	320.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	1983.00	kPa	330.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter
pvap	2431.45	kPa	340.00	Measurement of the (p,,rho.,T) relation of propane, propylene, n-butane, and isobutane in the temperature range from (95 to 340) K at pressures up to 12 MPa using an accurate two-sinker densimeter

pvap	6.02	kPa	182.33	Vapour pressure and excess Gibbs free energy of binary mixtures of hydrogen sulphide with ethane, propane, and n-butane at temperature of 182.33 K
pvap	638.00	kPa	283.15	(Vapour + liquid) equilibria of the {trifluoromethane (HFC-23) + propane} and {trifluoromethane (HFC-23) + n-butane} systems
pvap	840.00	kPa	293.15	(Vapour + liquid) equilibria of the {trifluoromethane (HFC-23) + propane} and {trifluoromethane (HFC-23) + n-butane} systems
pvap	1083.00	kPa	303.15	(Vapour + liquid) equilibria of the {trifluoromethane (HFC-23) + propane} and {trifluoromethane (HFC-23) + n-butane} systems
pvap	1375.00	kPa	313.15	(Vapour + liquid) equilibria of the {trifluoromethane (HFC-23) + propane} and {trifluoromethane (HFC-23) + n-butane} systems
pvap	111.30	kPa	233.22	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows

pvap	121.30	kPa	235.21	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	131.70	kPa	237.18	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	143.20	kPa	239.20	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	155.40	kPa	241.22	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	168.20	kPa	243.21	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows

pvap	182.10	kPa	245.26	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	195.60	kPa	247.13	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	211.10	kPa	249.14	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	227.40	kPa	251.14	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	244.50	kPa	253.14	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows

pvap	262.50	kPa	255.14	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	281.50	kPa	257.13	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	301.80	kPa	259.15	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	322.70	kPa	261.12	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	345.30	kPa	263.15	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows

pvap	368.60	kPa	265.14	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	393.20	kPa	267.14	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	419.00	kPa	269.14	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	446.10	kPa	271.14	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	474.30	kPa	273.14	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows

pvap	503.90	kPa	275.14	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	535.00	kPa	277.14	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	567.40	kPa	279.15	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	601.40	kPa	281.15	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	636.70	kPa	283.15	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows

pvap	673.50	kPa	285.15	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	711.80	kPa	287.14	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	752.00	kPa	289.15	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	793.70	kPa	291.16	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows
pvap	836.80	kPa	293.15	Experimental measurement of vapor pressures and (vapor + liquid) equilibrium for {1,1,1,2-tetrafluoroethane (R134a) + propane (R290)} by a recirculation apparatus with view windows

pvap	1072.00	kPa	302.97	Experimental (vapour + liquid) equilibrium data and modelling for binary mixtures of decafluorobutane with propane and 1-butene
pvap	1214.00	kPa	307.96	Experimental (vapour + liquid) equilibrium data and modelling for binary mixtures of decafluorobutane with propane and 1-butene
pvap	1361.00	kPa	312.99	Experimental (vapour + liquid) equilibrium data and modelling for binary mixtures of decafluorobutane with propane and 1-butene
pvap	1522.00	kPa	317.89	Experimental (vapour + liquid) equilibrium data and modelling for binary mixtures of decafluorobutane with propane and 1-butene
pvap	1712.00	kPa	322.99	Experimental (vapour + liquid) equilibrium data and modelling for binary mixtures of decafluorobutane with propane and 1-butene
pvap	1906.00	kPa	327.97	Experimental (vapour + liquid) equilibrium data and modelling for binary mixtures of decafluorobutane with propane and 1-butene
pvap	2103.00	kPa	332.93	Experimental (vapour + liquid) equilibrium data and modelling for binary mixtures of decafluorobutane with propane and 1-butene

pvap	2336.00	kPa	337.91	Experimental (vapour + liquid) equilibrium data and modelling for binary mixtures of decafluorobutane with propane and 1-butene
pvap	2582.00	kPa	342.91	Experimental (vapour + liquid) equilibrium data and modelling for binary mixtures of decafluorobutane with propane and 1-butene
pvap	236.00	kPa	252.10	PVTx properties in the gas phase for binary R290/R134a system
pvap	273.30	kPa	256.21	PVTx properties in the gas phase for binary R290/R134a system
pvap	311.10	kPa	260.10	PVTx properties in the gas phase for binary R290/R134a system
pvap	358.70	kPa	264.21	PVTx properties in the gas phase for binary R290/R134a system
pvap	406.00	kPa	268.09	PVTx properties in the gas phase for binary R290/R134a system
pvap	460.20	kPa	272.13	PVTx properties in the gas phase for binary R290/R134a system
pvap	519.70	kPa	276.14	PVTx properties in the gas phase for binary R290/R134a system
pvap	585.80	kPa	280.21	PVTx properties in the gas phase for binary R290/R134a system

pvap	653.20	kPa	284.09	PVTx properties in the gas phase for binary R290/R134a system
pvap	731.40	kPa	288.10	PVTx properties in the gas phase for binary R290/R134a system
pvap	814.20	kPa	292.10	PVTx properties in the gas phase for binary R290/R134a system
pvap	906.20	kPa	296.21	PVTx properties in the gas phase for binary R290/R134a system
pvap	1001.80	kPa	300.18	PVTx properties in the gas phase for binary R290/R134a system
pvap	1107.50	kPa	304.19	PVTx properties in the gas phase for binary R290/R134a system
pvap	1219.80	kPa	308.18	PVTx properties in the gas phase for binary R290/R134a system
pvap	1339.60	kPa	312.17	PVTx properties in the gas phase for binary R290/R134a system
pvap	1468.90	kPa	316.20	PVTx properties in the gas phase for binary R290/R134a system
pvap	1606.70	kPa	320.19	PVTx properties in the gas phase for binary R290/R134a system
pvap	291.60	kPa	258.15	(Vapor + liquid) phase equilibrium measurements for {trifluoroiodomethane (R13I1) + propane (R290)} from T = (258.150 to 283.150) K

pvap	345.30	kPa	263.15	(Vapor + liquid) phase equilibrium measurements for {trifluoroiodomethane (R13I1) + propane (R290)} from T = (258.150 to 283.150) K
pvap	474.50	kPa	273.15	(Vapor + liquid) phase equilibrium measurements for {trifluoroiodomethane (R13I1) + propane (R290)} from T = (258.150 to 283.150) K
pvap	636.80	kPa	283.15	(Vapor + liquid) phase equilibrium measurements for {trifluoroiodomethane (R13I1) + propane (R290)} from T = (258.150 to 283.150) K
pvap	836.30	kPa	293.15	Measurements of isothermal (vapor + liquid) equilibrium for the (propane + cis-1,3,3,3-tetrafluoropropene) system at temperatures from (253.150 to 293.150) K
pvap	636.40	kPa	283.15	Measurements of isothermal (vapor + liquid) equilibrium for the (propane + cis-1,3,3,3-tetrafluoropropene) system at temperatures from (253.150 to 293.150) K
pvap	474.40	kPa	273.15	Measurements of isothermal (vapor + liquid) equilibrium for the (propane + cis-1,3,3,3-tetrafluoropropene) system at temperatures from (253.150 to 293.150) K

pvap	345.10	kPa	263.15	Measurements of isothermal (vapor + liquid) equilibrium for the (propane + cis-1,3,3,3-tetrafluoropropene) system at temperatures from (253.150 to 293.150) K	
pvap	244.10	kPa	253.15	Measurements of isothermal (vapor + liquid) equilibrium for the (propane + cis-1,3,3,3-tetrafluoropropene) system at temperatures from (253.150 to 293.150) K	
pvap	836.80	kPa	293.18	Experimental determination of the critical loci for R-23 + (npropane or n-hexane) and R-116 + n-propane binary mixtures	
pvap	950.80	kPa	298.15	Experimental determination of the critical loci for R-23 + (npropane or n-hexane) and R-116 + n-propane binary mixtures	
pvap	1380.10	kPa	313.15	Experimental determination of the critical loci for R-23 + (npropane or n-hexane) and R-116 + n-propane binary mixtures	
pvap	1713.00	kPa	323.15	Experimental determination of the critical loci for R-23 + (npropane or n-hexane) and R-116 + n-propane binary mixtures	
pvap	3135.40	kPa	353.15	Experimental determination of the critical loci for R-23 + (npropane or n-hexane) and R-116 + n-propane binary mixtures	

pvap	437.50	kPa	270.51	Surface tension and critical point measurements of methane + propane mixtures
pvap	583.70	kPa	280.13	Surface tension and critical point measurements of methane + propane mixtures
pvap	715.40	kPa	287.35	Surface tension and critical point measurements of methane + propane mixtures
pvap	762.10	kPa	289.65	Surface tension and critical point measurements of methane + propane mixtures
pvap	806.20	kPa	291.75	Surface tension and critical point measurements of methane + propane mixtures
pvap	948.20	kPa	297.98	Surface tension and critical point measurements of methane + propane mixtures
pvap	1021.20	kPa	300.92	Surface tension and critical point measurements of methane + propane mixtures
pvap	1398.00	kPa	314.06	Surface tension and critical point measurements of methane + propane mixtures
pvap	456.00	kPa	271.77	Surface tension and critical point measurements of methane + propane mixtures
pvap	680.60	kPa	285.35	Surface tension and critical point measurements of methane + propane mixtures
pvap	1083.10	kPa	303.37	Surface tension and critical point measurements of methane + propane mixtures

pvap	1030.00	kPa	305.90	Experimental High-Pressure Isochoric/Isoplethic Equilibrium for the Systems Propane + n-Pentane and Propane + Diethyl Ether
pvap	1270.00	kPa	319.20	Experimental High-Pressure Isochoric/Isoplethic Equilibrium for the Systems Propane + n-Pentane and Propane + Diethyl Ether
pvap	2260.00	kPa	326.80	Experimental High-Pressure Isochoric/Isoplethic Equilibrium for the Systems Propane + n-Pentane and Propane + Diethyl Ether
pvap	2350.00	kPa	334.30	Experimental High-Pressure Isochoric/Isoplethic Equilibrium for the Systems Propane + n-Pentane and Propane + Diethyl Ether
pvap	3040.00	kPa	349.30	Experimental High-Pressure Isochoric/Isoplethic Equilibrium for the Systems Propane + n-Pentane and Propane + Diethyl Ether
pvap	3920.00	kPa	362.10	Experimental High-Pressure Isochoric/Isoplethic Equilibrium for the Systems Propane + n-Pentane and Propane + Diethyl Ether
pvap	4440.00	kPa	367.90	Experimental High-Pressure Isochoric/Isoplethic Equilibrium for the Systems Propane + n-Pentane and Propane + Diethyl Ether

pvap	536.00	kPa	277.17	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	638.00	kPa	283.22	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	734.00	kPa	288.26	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	838.00	kPa	293.27	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	955.00	kPa	298.30	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa

pvap	1055.00	kPa	302.27	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	1236.00	kPa	308.80	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	1326.00	kPa	311.80	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	1370.00	kPa	313.24	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	1537.00	kPa	318.22	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa

pvap	1716.00	kPa	323.22	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	1911.00	kPa	328.26	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	2120.00	kPa	333.29	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	2346.00	kPa	338.31	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	2591.00	kPa	343.26	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa

pvap	2852.00	kPa	348.31	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	3134.00	kPa	353.41	Vapor-Liquid Equilibrium Data for the Azeotropic Difluoromethane + Propane System at Temperatures from 294.83 to 343.26 K and Pressures up to 5.4 MPa
pvap	3554.41	kPa	360.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	549.40	kPa	278.15	Vapor-Liquid Equilibria for the Binary System Difluoromethane (HFC-32) + Propane (HC-290) at Seven Temperatures [(268.15, 278.15, 283.15, 288.15, 298.15, 308.15, and 318.15) K]
pvap	636.40	kPa	283.15	Vapor-Liquid Equilibria for the Binary System Difluoromethane (HFC-32) + Propane (HC-290) at Seven Temperatures [(268.15, 278.15, 283.15, 288.15, 298.15, 308.15, and 318.15) K]

pvap	735.00	kPa	288.15	Vapor-Liquid Equilibria for the Binary System Difluoromethane (HFC-32) + Propane (HC-290) at Seven Temperatures [(268.15, 278.15, 283.15, 288.15, 298.15, 308.15, and 318.15) K]
pvap	954.80	kPa	298.15	Vapor-Liquid Equilibria for the Binary System Difluoromethane (HFC-32) + Propane (HC-290) at Seven Temperatures [(268.15, 278.15, 283.15, 288.15, 298.15, 308.15, and 318.15) K]
pvap	1213.00	kPa	308.15	Vapor-Liquid Equilibria for the Binary System Difluoromethane (HFC-32) + Propane (HC-290) at Seven Temperatures [(268.15, 278.15, 283.15, 288.15, 298.15, 308.15, and 318.15) K]
pvap	1530.80	kPa	318.15	Vapor-Liquid Equilibria for the Binary System Difluoromethane (HFC-32) + Propane (HC-290) at Seven Temperatures [(268.15, 278.15, 283.15, 288.15, 298.15, 308.15, and 318.15) K]
pvap	475.00	kPa	273.15	Measurement of Vapor-Liquid Equilibria for the Binary Mixture of Propane (R-290) + Isobutane (R-600a)

pvap	637.80	kPa	283.15	Measurement of Vapor-Liquid Equilibria for the Binary Mixture of Propane (R-290) + Isobutane (R-600a)
pvap	836.00	kPa	293.15	Measurement of Vapor-Liquid Equilibria for the Binary Mixture of Propane (R-290) + Isobutane (R-600a)
pvap	1078.40	kPa	303.15	Measurement of Vapor-Liquid Equilibria for the Binary Mixture of Propane (R-290) + Isobutane (R-600a)
pvap	407.90	kPa	268.15	Measurement of Vapor-Liquid Equilibria for the Binary Mixture of Pentafluoroethane (HFC-125) + Propane (R-290)
pvap	476.90	kPa	273.15	Measurement of Vapor-Liquid Equilibria for the Binary Mixture of Pentafluoroethane (HFC-125) + Propane (R-290)
pvap	637.20	kPa	283.15	Measurement of Vapor-Liquid Equilibria for the Binary Mixture of Pentafluoroethane (HFC-125) + Propane (R-290)
pvap	839.20	kPa	293.15	Measurement of Vapor-Liquid Equilibria for the Binary Mixture of Pentafluoroethane (HFC-125) + Propane (R-290)
pvap	1074.60	kPa	303.15	Measurement of Vapor-Liquid Equilibria for the Binary Mixture of Pentafluoroethane (HFC-125) + Propane (R-290)
pvap	1364.30	kPa	313.15	Measurement of Vapor-Liquid Equilibria for the Binary Mixture of Pentafluoroethane (HFC-125) + Propane (R-290)

pvap	147.90	kPa	240.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)
pvap	147.90	kPa	240.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)
pvap	217.70	kPa	250.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)
pvap	310.30	kPa	260.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)
pvap	429.60	kPa	270.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)
pvap	768.60	kPa	290.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)
pvap	997.60	kPa	300.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)
pvap	1272.10	kPa	310.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)
pvap	1600.70	kPa	320.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)
pvap	1988.80	kPa	330.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)

pvap	2429.70	kPa	340.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)
pvap	2948.00	kPa	350.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)
pvap	3552.20	kPa	360.00	Liquid-Phase Thermodynamic Properties for Propane (1), n-Butane (2), and Isobutane (3)
pvap	472.50	kPa	273.15	Vapor-Liquid Equilibria for the 1,1-Difluoroethane (HFC-152a) + Propane (R-290) System
pvap	633.90	kPa	283.15	Vapor-Liquid Equilibria for the 1,1-Difluoroethane (HFC-152a) + Propane (R-290) System
pvap	832.94	kPa	293.15	Vapor-Liquid Equilibria for the 1,1-Difluoroethane (HFC-152a) + Propane (R-290) System
pvap	1077.00	kPa	303.15	Vapor-Liquid Equilibria for the 1,1-Difluoroethane (HFC-152a) + Propane (R-290) System
pvap	1370.00	kPa	313.15	Vapor-Liquid Equilibria for the 1,1-Difluoroethane (HFC-152a) + Propane (R-290) System
pvap	168.00	kPa	243.23	Phase Equilibria of H2S-Hydrocarbons (Propane, n-Butane, and n-Pentane) Binary Systems at Low Temperatures

pvap	168.20	kPa	243.23	Phase Equilibria of H2S-Hydrocarbons (Propane, n-Butane, and n-Pentane) Binary Systems at Low Temperatures
pvap	473.50	kPa	273.12	Phase Equilibria of H2S-Hydrocarbons (Propane, n-Butane, and n-Pentane) Binary Systems at Low Temperatures
pvap	476.00	kPa	273.15	Vapor-Liquid Equilibria for Propane (R-290) + 1,1,1,2,3,3,3-Heptafluoropropane (HFC-227ea) at Various Temperatures
pvap	632.00	kPa	283.15	Vapor-Liquid Equilibria for Propane (R-290) + 1,1,1,2,3,3,3-Heptafluoropropane (HFC-227ea) at Various Temperatures
pvap	833.00	kPa	293.15	Vapor-Liquid Equilibria for Propane (R-290) + 1,1,1,2,3,3,3-Heptafluoropropane (HFC-227ea) at Various Temperatures
pvap	1079.00	kPa	303.15	Vapor-Liquid Equilibria for Propane (R-290) + 1,1,1,2,3,3,3-Heptafluoropropane (HFC-227ea) at Various Temperatures
pvap	1366.00	kPa	313.15	Vapor-Liquid Equilibria for Propane (R-290) + 1,1,1,2,3,3,3-Heptafluoropropane (HFC-227ea) at Various Temperatures

pvap	1709.00	kPa	323.15	Vapor-Liquid Equilibria for Propane (R-290) + 1,1,1,2,3,3,3-Heptafluoropropane (HFC-227ea) at Various Temperatures
pvap	476.00	kPa	273.15	Vapor-Liquid Equilibria for Propane (R290) + n-Butane (R600) at Various Temperatures
pvap	633.00	kPa	283.15	Vapor-Liquid Equilibria for Propane (R290) + n-Butane (R600) at Various Temperatures
pvap	833.00	kPa	293.15	Vapor-Liquid Equilibria for Propane (R290) + n-Butane (R600) at Various Temperatures
pvap	1079.00	kPa	303.15	Vapor-Liquid Equilibria for Propane (R290) + n-Butane (R600) at Various Temperatures
pvap	1366.00	kPa	313.15	Vapor-Liquid Equilibria for Propane (R290) + n-Butane (R600) at Various Temperatures
pvap	1709.00	kPa	323.15	Vapor-Liquid Equilibria for Propane (R290) + n-Butane (R600) at Various Temperatures
pvap	344.00	kPa	263.30	Isothermal Vapor-Liquid Equilibrium Data for the Hexafluoroethane (R116) + Propane System at Temperatures from (263 to 323) K

pvap	639.00	kPa	283.25	Isothermal Vapor-Liquid Equilibrium Data for the Hexafluoroethane (R116) + Propane System at Temperatures from (263 to 323) K
pvap	795.00	kPa	291.22	Isothermal Vapor-Liquid Equilibrium Data for the Hexafluoroethane (R116) + Propane System at Temperatures from (263 to 323) K
pvap	906.00	kPa	296.23	Isothermal Vapor-Liquid Equilibrium Data for the Hexafluoroethane (R116) + Propane System at Temperatures from (263 to 323) K
pvap	1221.00	kPa	308.21	Isothermal Vapor-Liquid Equilibrium Data for the Hexafluoroethane (R116) + Propane System at Temperatures from (263 to 323) K
pvap	1715.00	kPa	323.19	Isothermal Vapor-Liquid Equilibrium Data for the Hexafluoroethane (R116) + Propane System at Temperatures from (263 to 323) K
pvap	430.71	kPa	270.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	430.73	kPa	270.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	430.74	kPa	270.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	430.74	kPa	270.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	430.74	kPa	270.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	430.73	kPa	270.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	430.75	kPa	270.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	581.90	kPa	280.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	581.90	kPa	280.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	581.91	kPa	280.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	581.91	kPa	280.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	581.94	kPa	280.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	581.94	kPa	280.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	769.26	kPa	290.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	769.26	kPa	290.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	769.28	kPa	290.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	769.30	kPa	290.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	769.32	kPa	290.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	997.42	kPa	300.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	997.43	kPa	300.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	997.45	kPa	300.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	997.45	kPa	300.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	997.48	kPa	300.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1271.79	kPa	310.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1272.28	kPa	310.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1272.27	kPa	310.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1271.80	kPa	310.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	1271.96	kPa	310.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1271.99	kPa	310.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1272.32	kPa	310.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1271.82	kPa	310.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1271.97	kPa	310.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1271.99	kPa	310.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1272.35	kPa	310.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1271.87	kPa	310.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1271.86	kPa	310.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	1333.33	kPa	312.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1333.31	kPa	312.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1333.37	kPa	312.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1333.40	kPa	312.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1396.09	kPa	314.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1396.13	kPa	314.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1396.12	kPa	314.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1396.17	kPa	314.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	1428.23	kPa	315.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1428.25	kPa	315.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1428.28	kPa	315.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1428.32	kPa	315.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1428.29	kPa	315.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1461.86	kPa	316.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1461.72	kPa	316.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1461.60	kPa	316.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1461.47	kPa	316.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	1598.85	kPa	320.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1598.43	kPa	320.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1598.74	kPa	320.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1598.70	kPa	320.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1598.30	kPa	320.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1598.70	kPa	320.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1598.76	kPa	320.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1598.43	kPa	320.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	1598.77	kPa	320.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1598.76	kPa	320.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1598.31	kPa	320.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1598.45	kPa	320.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1598.46	kPa	320.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1782.57	kPa	325.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1782.71	kPa	325.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1782.59	kPa	325.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1782.74	kPa	325.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	1782.65	kPa	325.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1782.79	kPa	325.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1782.69	kPa	325.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1782.82	kPa	325.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1982.09	kPa	330.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1982.26	kPa	330.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1982.12	kPa	330.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1982.16	kPa	330.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	1982.33	kPa	330.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1982.31	kPa	330.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1982.19	kPa	330.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1982.37	kPa	330.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	1982.35	kPa	330.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2197.66	kPa	335.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2197.75	kPa	335.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2197.75	kPa	335.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2197.90	kPa	335.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	2197.99	kPa	335.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2197.83	kPa	335.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2198.02	kPa	335.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2198.07	kPa	335.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2198.06	kPa	335.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2430.87	kPa	340.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2430.87	kPa	340.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2430.38	kPa	340.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	2430.37	kPa	340.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2430.39	kPa	340.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2430.40	kPa	340.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2430.43	kPa	340.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2430.65	kPa	340.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2430.70	kPa	340.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2431.05	kPa	340.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2430.74	kPa	340.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2430.71	kPa	340.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	2431.05	kPa	340.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2430.74	kPa	340.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2681.46	kPa	345.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2681.50	kPa	345.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2681.50	kPa	345.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2681.74	kPa	345.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2681.72	kPa	345.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2681.73	kPa	345.00	Thermodynamic Properties of Propane. I. p-?-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	2681.56	kPa	345.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2681.78	kPa	345.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2951.27	kPa	350.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2951.31	kPa	350.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2951.32	kPa	350.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2951.53	kPa	350.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2951.38	kPa	350.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2951.39	kPa	350.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2951.57	kPa	350.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	2951.57	kPa	350.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	2951.64	kPa	350.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3241.62	kPa	355.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3241.63	kPa	355.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3241.61	kPa	355.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3241.66	kPa	355.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3241.77	kPa	355.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3241.78	kPa	355.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa

pvap	3241.72	kPa	355.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3241.82	kPa	355.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3241.89	kPa	355.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3241.89	kPa	355.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3554.97	kPa	360.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3554.97	kPa	360.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	3554.44	kPa	360.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
pvap	407.90	kPa	268.15	Vapor-Liquid Equilibria for the Binary System Difluoromethane (HFC-32) + Propane (HC-290) at Seven Temperatures [(268.15, 278.15, 283.15, 288.15, 298.15, 308.15, and 318.15) K]

pvap	3554.45	kPa	360.00	Thermodynamic Properties of Propane. I. p-T Behavior from (265 to 500) K with Pressures to 36 MPa
rhoI	582.00	kg/m3	231.00	KDB
srf	0.01	N/m	223.20	KDB
srf	0.01	N/m	303.12	Surface Tension of Propane (R-290) + 1,1-Difluoroethane (R-152a) from (248 to 328) K
srf	0.01	N/m	298.10	Surface Tension of Propane (R-290) + 1,1-Difluoroethane (R-152a) from (248 to 328) K
srf	0.01	N/m	293.13	Surface Tension of Propane (R-290) + 1,1-Difluoroethane (R-152a) from (248 to 328) K
srf	0.01	N/m	288.17	Surface Tension of Propane (R-290) + 1,1-Difluoroethane (R-152a) from (248 to 328) K
srf	0.01	N/m	283.16	Surface Tension of Propane (R-290) + 1,1-Difluoroethane (R-152a) from (248 to 328) K
srf	0.00	N/m	333.30	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	333.30	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	331.79	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K

srf	0.00	N/m	331.79	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	329.79	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	329.79	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	327.40	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	327.40	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	325.32	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	323.34	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	323.34	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	321.41	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	321.41	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K

srf	0.00	N/m	319.43	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	319.43	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	317.64	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	317.64	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	315.71	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.00	N/m	315.71	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	314.39	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	314.39	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	310.73	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	310.73	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K

srf	0.01	N/m	308.01	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	308.01	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	305.17	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	305.17	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	303.54	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	303.54	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	301.45	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	301.45	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	299.41	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	299.41	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K

srf	0.01	N/m	297.40	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	297.40	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	295.73	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	295.73	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	293.85	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	293.85	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	289.27	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	289.27	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	281.48	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	281.48	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K

srf	0.01	N/m	279.39	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	279.39	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	277.43	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	277.43	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	278.18	Surface tension of dimethyl ether + propane from 243 to 333 K
srf	0.01	N/m	275.38	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	275.38	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	273.20	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	273.20	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	270.72	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K

srf	0.01	N/m	270.72	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	268.88	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	268.88	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	267.09	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	267.09	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	265.09	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	265.09	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	262.70	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	262.70	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	260.71	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K

srf	0.01	N/m	260.71	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	258.68	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	258.68	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	256.89	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	256.89	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	254.80	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	254.80	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	253.08	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	253.08	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
srf	0.01	N/m	303.18	Surface tension of dimethyl ether + propane from 243 to 333 K
srf	0.01	N/m	298.10	Surface tension of dimethyl ether + propane from 243 to 333 K

srf	0.01	N/m	293.18	Surface tension of dimethyl ether + propane from 243 to 333 K
srf	0.01	N/m	288.19	Surface tension of dimethyl ether + propane from 243 to 333 K
srf	0.01	N/m	283.18	Surface tension of dimethyl ether + propane from 243 to 333 K
srf	0.00	N/m	325.32	Surface Tension Measurements of Propane (R-290) and Isobutane (R-600a) from (253 to 333) K
svapt	81.26	J/mol×K	231.04	NIST Webbook

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.41497e+01
Coeff. B	-2.04899e+03
Coeff. C	-1.60660e+01
Temperature range (K), min.	163.88
Temperature range (K), max.	369.89

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C \cdot \ln(T) + D \cdot T^2$
Coeff. A	4.81426e+01
Coeff. B	-3.38399e+03
Coeff. C	-5.39553e+00
Coeff. D	9.13211e-06
Temperature range (K), min.	85.46
Temperature range (K), max.	369.82

Datasets

Speed of sound, m/s

Temperature, K - Fluid (supercritical or subcritical phases)	Pressure, kPa - Fluid (supercritical or subcritical phases)	Speed of sound, m/s - Fluid (supercritical or subcritical phases)
239.99	90166.80	1640.817
239.99	100174.00	1680.922
239.99	80159.80	1598.498
239.99	70152.60	1553.684
239.99	60145.60	1505.9
239.99	45135.30	1427.438
239.99	50138.70	1454.624
239.99	30125.00	1338.192
239.99	40131.90	1399.073
239.99	35128.50	1369.388
239.99	25121.40	1305.293
239.99	4106.02	1140.489
239.99	20117.90	1270.399
240.00	17616.20	1252.102
240.00	15114.40	1233.171
240.00	12612.80	1213.533
240.00	8109.64	1176.198
240.00	9110.30	1184.734
240.00	10111.00	1193.131
240.00	7108.53	1167.505
240.00	3105.35	1131.113
240.00	2104.77	1121.558
240.00	4106.04	1140.474
240.00	5106.62	1149.654
240.00	6107.73	1158.658
240.00	1304.27	1113.771
260.00	1302.58	983.5408
260.00	3103.75	1004.491
260.00	2102.21	992.9799
260.00	5105.07	1026.613
260.00	4104.35	1015.694
260.00	7106.63	1047.67
260.00	6105.93	1037.263

260.00	9107.76	1067.784
260.00	100173.00	1607.488
260.00	15112.00	1123.433
260.00	8107.02	1057.835
260.00	12610.20	1101.017
260.00	10108.50	1077.521
260.00	17614.10	1144.892
260.00	25119.30	1204.425
260.00	20115.80	1165.483
260.00	70151.40	1473.216
260.00	50136.80	1367.385
260.00	60144.40	1422.346
260.00	80158.40	1520.707
260.00	35126.20	1275.003
260.00	90165.50	1565.332
260.00	40129.70	1307.344
260.00	45133.20	1338.078
260.00	30123.50	1240.759
260.00	20116.70	1165.453
260.00	40130.50	1307.318
260.00	10109.80	1077.491
260.00	4105.33	1015.671
260.00	1303.62	983.5115
280.00	80159.00	1447.866
280.00	1303.58	851.1862
280.00	50138.10	1285.387
280.00	70152.10	1397.839
280.00	90166.00	1494.682
280.00	45134.50	1253.96
280.00	60145.10	1343.97
280.00	7105.57	929.3663
280.00	1301.77	851.1421
280.00	4103.27	890.9079
280.00	5104.02	904.1486
280.00	6104.83	916.9569
280.00	35127.40	1185.77
280.00	100173.00	1538.771
280.00	3102.56	877.1981
280.00	17614.80	1041.793
280.00	30123.50	1148.404
280.00	30123.90	1148.414
280.00	40131.00	1220.836
280.00	2101.78	862.9532
280.00	20117.00	1064.973

280.00	8107.69	941.4215
280.00	12611.10	991.7594
280.00	15112.90	1017.445
280.00	17614.80	1041.793
280.00	9108.52	953.1252
280.00	10109.20	964.5195
280.00	4105.52	890.9461
280.00	20116.50	1064.973
280.00	25120.50	1108.345
280.00	10109.70	964.529
280.00	1303.37	851.1624
280.00	2102.52	862.9646
280.00	1302.00	851.1568
280.00	5104.27	904.1507
280.00	3103.04	877.1961
280.00	6105.02	916.9548
280.00	4103.71	890.9119
300.00	4105.71	764.6092
300.00	5106.43	781.1521
300.00	4105.12	764.5885
300.00	5105.62	781.1336
300.00	3104.51	747.1675
300.00	1303.44	713.1682
300.00	2104.01	728.7458
300.00	7106.68	812.03
300.00	8107.32	826.541
300.00	9107.93	840.5098
300.00	6106.13	796.919
300.00	100172.00	1474.781
300.00	10108.80	853.9894
300.00	35126.50	1101.932
300.00	70150.90	1327.616
300.00	90164.90	1428.907
300.00	60144.00	1270.887
300.00	40130.10	1139.761
300.00	80157.80	1380.039
300.00	20115.90	969.1239
300.00	25119.40	1017.346
300.00	30123.00	1061.33
300.00	45133.50	1175.263
300.00	50137.00	1208.787
300.00	12610.70	885.8175
300.00	15112.40	915.3736
300.00	17614.20	943.0459

300.00	20116.80	969.1168
300.00	10109.80	853.9783
300.00	1303.69	713.1424
300.00	4105.65	764.5708
320.00	2103.55	583.7172
320.00	6106.06	675.4465
320.00	7106.72	694.4484
320.00	3104.22	609.7601
320.00	4104.78	633.4124
320.00	5105.45	655.1847
320.00	8107.88	712.38
320.00	9108.59	729.3853
320.00	10109.30	745.5906
320.00	12611.10	783.169
320.00	15112.90	817.3588
320.00	60143.20	1203.103
320.00	80157.20	1317.197
320.00	70150.20	1262.54
320.00	90164.20	1367.953
320.00	5105.03	655.1587
320.00	100171.00	1415.461
320.00	2102.94	583.6663
320.00	4104.90	633.377
320.00	6105.69	675.4154
320.00	15112.40	817.3419
320.00	3103.70	609.7187
320.00	7106.34	694.4143
320.00	8107.00	712.3441
320.00	17614.30	848.8529
320.00	35126.70	1023.657
320.00	40130.20	1064.246
320.00	50137.40	1137.653
320.00	9107.75	729.3543
320.00	12610.20	783.1411
320.00	25119.60	931.6534
320.00	30123.20	979.7363
320.01	10108.40	745.5583
320.01	20116.20	878.1866
320.01	45133.80	1102.098
320.05	2103.95	583.3338
340.00	5106.10	521.8842
340.00	3604.91	472.3201
340.00	6106.82	549.7914
340.00	4105.32	490.155

340.00	8109.21	597.9286
340.00	9109.81	619.2078
340.00	7108.49	574.9388
340.00	10110.50	639.0854
340.00	17614.80	759.6101
340.00	12611.60	683.9784
340.00	15113.20	723.7083
340.00	20116.50	792.5299
340.00	30123.50	903.8544
340.00	35126.80	951.0835
340.00	25119.90	851.5837
340.00	40129.90	994.3745
340.00	45133.20	1034.493
340.00	70150.60	1202.518
340.00	50136.70	1071.972
340.00	60143.70	1140.589
340.00	80157.50	1259.232
340.00	90164.40	1311.718
340.00	100171.00	1360.704
340.00	3103.03	452.6192
340.00	3603.40	472.2484
340.00	2602.67	430.6004
340.00	4103.70	490.0808
360.00	6104.88	414.5491
360.00	12610.50	588.7956
360.00	15112.30	635.0499
360.00	20115.80	712.6116
360.00	17614.10	675.8427
360.00	4103.37	307.5344
360.00	5103.90	369.8779
360.00	3602.91	257.6812
360.00	3954.62	295.0016
360.00	4603.61	342.1055
360.00	30123.50	833.8591
360.00	50137.10	1011.687
360.00	35127.00	884.2953
360.00	25120.00	777.4163
360.00	40130.40	930.1585
360.00	60144.10	1083.208
360.00	45133.80	972.4
360.00	7105.23	450.8164
360.00	7105.18	450.8112
360.00	100172.00	1310.302
360.00	3604.27	257.8326

360.00	8105.96	481.9514
360.00	70151.30	1147.408
360.00	3854.08	285.6235
360.00	9106.67	509.5406
360.00	10107.30	534.4944
360.00	90165.40	1259.986
360.00	80158.40	1205.952
360.00	3954.13	294.9448
360.00	3854.64	285.6711
360.00	3604.40	257.7434
380.00	14112.00	532.306
380.00	15112.70	552.6036
380.00	13111.20	510.6122
380.00	12110.40	487.2269
380.00	10108.90	433.6062
380.00	8106.95	365.1279
380.00	7606.54	344.0347
380.00	11109.70	461.751
380.00	7106.10	320.3863
380.00	9108.12	401.9067
380.00	17614.90	598.5104
380.00	20116.60	639.153
380.00	6605.68	293.1749
380.00	22618.30	675.8875
380.00	30123.40	769.9397
380.00	40130.20	871.5647
380.00	35126.80	823.3524
380.00	25120.00	709.5618
380.00	6105.31	260.5574
380.00	45133.70	915.7351
380.00	50137.10	956.634
380.00	60144.10	1030.755
380.00	7105.92	320.3959
380.00	70151.00	1096.962
380.00	6605.55	293.1752
380.00	7606.31	344.0509
380.00	80157.90	1157.136
380.00	100172.00	1263.993
380.00	90164.90	1212.527
380.00	6105.22	260.5618
400.00	13111.10	431.5813
400.00	17113.90	519.5737
400.00	14111.80	455.9735
400.00	19115.30	556.1864

400.00	16113.20	499.7133
400.00	18114.60	538.3533
400.00	20116.00	573.1901
400.00	15112.50	478.5871
400.00	12109.90	404.9956
400.00	25119.70	648.5369
400.00	22617.90	612.6439
400.00	10608.50	359.7235
400.00	10108.10	342.7723
400.00	11109.00	375.6713
400.00	27621.50	681.6052
400.00	30123.20	712.3563
400.00	9607.68	324.6564
400.00	40130.20	818.5907
400.00	45133.70	864.4181
400.00	35126.70	768.3421
400.00	9107.26	305.1695
400.00	80158.50	1112.567
400.00	50137.30	906.7114
400.00	60144.20	983.0545
400.00	70151.10	1050.995
400.00	80157.90	1112.57
420.00	13110.70	366.9736
420.00	12610.40	353.4876
420.00	11108.70	309.8133
420.00	12110.10	339.4714
420.00	11609.00	324.8867
420.00	14110.80	392.4725
420.00	15111.50	416.2585
420.00	16112.20	438.5192
420.00	17113.00	459.4635
420.00	18113.70	479.2532
420.00	50136.70	861.6993
420.00	60143.80	939.8528
420.00	70150.80	1009.204
420.00	19114.30	498.0285
420.00	20115.00	515.91
420.00	25118.30	594.8312
420.00	27619.90	629.2942
420.01	21115.70	532.993
420.01	22616.70	557.3021
420.01	40129.50	771.1221
420.01	45133.10	818.2814
420.01	35126.00	719.2618

Thermal conductivity, W/m/K

Temperature, K - Gas	Pressure, kPa - Gas	Thermal conductivity, W/m/K - Gas
369.12	3948.00	0.0413
369.12	3960.00	0.0417
369.12	4020.00	0.0434
369.12	4040.00	0.0442
369.12	4115.00	0.0486
369.12	4120.00	0.0491
369.12	4125.00	0.0496
369.12	4130.00	0.0501
369.12	4135.00	0.0507
369.12	4140.00	0.0513
369.12	4145.00	0.0521
369.12	4150.00	0.0529
369.12	4154.00	0.0537
369.12	4156.00	0.0540
369.12	4158.00	0.0544
369.12	4160.00	0.0549
369.12	4162.00	0.0554
369.12	4164.00	0.0574
369.12	4166.00	0.0603
369.12	4168.00	0.0639
369.12	4170.00	0.0686
369.12	4172.00	0.0743
369.12	4180.00	0.1130
369.12	4182.00	0.1270
369.12	4184.00	0.1426
369.12	4186.00	0.1588
369.12	4188.00	0.1790
369.12	4190.00	0.1956
369.12	4192.00	0.2155
368.46	2968.00	0.0321
368.46	2972.00	0.0321
368.46	2978.00	0.0321
368.46	3000.00	0.0322
368.46	3030.00	0.0324

368.46	3100.00	0.0328
368.46	3150.00	0.0330
368.46	3200.00	0.0333
368.46	3250.00	0.0336
368.46	3300.00	0.0340
368.46	3350.00	0.0343
368.46	3400.00	0.0347
368.46	3500.00	0.0355
368.46	3575.00	0.0363
368.46	3650.00	0.0370
368.46	3700.00	0.0376
368.46	3720.00	0.0379
368.46	3730.00	0.0380
368.46	3740.00	0.0381
368.46	3750.00	0.0382
368.46	3755.00	0.0383
368.46	3765.00	0.0384
368.46	3775.00	0.0386
368.46	3785.00	0.0387
368.46	3790.00	0.0388
368.46	3800.00	0.0389
368.46	3850.00	0.0397
368.46	3900.00	0.0407
368.46	3950.00	0.0419
368.46	4000.00	0.0435
368.46	4038.00	0.0452
368.46	4060.00	0.0465
368.46	4080.00	0.0481
368.46	4096.00	0.0497
368.46	4099.00	0.0501
368.46	4102.00	0.0505
368.46	4104.00	0.0508
368.46	4106.00	0.0510
368.46	4112.00	0.0520
368.46	4114.00	0.0524
368.46	4115.00	0.0525
368.46	4116.00	0.0527
368.46	4117.00	0.0529
368.46	4118.00	0.0531
368.46	4119.00	0.0534
368.46	4120.00	0.0535
368.46	4121.00	0.0538
368.46	4122.00	0.0539
368.46	4123.00	0.0542

368.46	4124.00	0.0565
368.46	4125.00	0.0589
368.46	4126.00	0.0618
368.46	4127.00	0.0649
368.46	4128.00	0.0686
368.46	4129.00	0.0728
368.46	4130.00	0.0775
368.46	4131.00	0.0828
368.46	4132.00	0.0888
368.46	4133.00	0.0957
368.46	4134.00	0.1033
368.46	4135.00	0.1122
368.46	4136.00	0.1221
368.46	4137.00	0.1337
368.46	4138.00	0.1478
368.46	4139.00	0.1619
368.46	4140.00	0.1793
368.46	4141.00	0.2022
368.46	4142.00	0.2140
368.46	4143.00	0.2272
368.46	4144.00	0.2410
367.32	4010.00	0.0465
367.32	4012.00	0.0466
367.32	4014.00	0.0469
367.32	4025.00	0.0479
367.32	4026.00	0.0508
367.32	4027.00	0.0539
367.32	4028.00	0.0564
367.32	4029.00	0.0596
367.32	4030.00	0.0629
367.32	4031.00	0.0665
367.32	4032.00	0.0700
367.32	4033.00	0.0741
367.32	4034.00	0.0782
367.32	4035.00	0.0823
367.32	4036.00	0.0872
367.32	4037.00	0.0917
367.32	4038.00	0.0966
367.32	4039.00	0.1018
367.32	4040.00	0.1068
367.32	4041.00	0.1118
367.32	4042.00	0.1171
367.32	4043.00	0.1226
367.32	4044.00	0.1282

367.32	4045.00	0.1340
367.32	4046.00	0.1397
367.32	4047.00	0.1450
367.32	4048.00	0.1514
367.32	4050.00	0.1645
367.32	4051.00	0.1714
367.32	4052.00	0.1781
367.32	4053.00	0.1856
367.32	4054.00	0.1925
367.32	4055.00	0.1998
367.32	4056.00	0.2078
367.32	4057.00	0.2153
367.32	4058.00	0.2233
367.32	4059.00	0.2315
366.45	3595.00	0.0369
366.45	3610.00	0.0371
366.45	3880.00	0.0419
366.45	3882.00	0.0420
366.45	3908.00	0.0428
366.45	3915.00	0.0432
366.45	3920.00	0.0434
366.45	3925.00	0.0436
366.45	3930.00	0.0438
366.45	3935.00	0.0441
366.45	3937.00	0.0442
366.45	3949.00	0.0449
366.45	3950.00	0.0449
366.45	3951.00	0.0450
366.45	3952.00	0.0450
366.45	3953.00	0.0451
366.45	3954.00	0.0451
366.45	3955.00	0.0485
366.45	3956.00	0.0498
366.45	3957.00	0.0512
366.45	3958.00	0.0529
366.45	3959.00	0.0545
366.45	3960.00	0.0565
366.45	3961.00	0.0585
366.45	3962.00	0.0606
366.45	3963.00	0.0631
366.45	3964.00	0.0657
366.45	3965.00	0.0682
366.45	3966.00	0.0711
366.45	3967.00	0.0741

366.45	3968.00	0.0775
366.45	3969.00	0.0819
366.45	3970.00	0.0871
366.45	3971.00	0.0934
366.45	3972.00	0.0978
366.45	3973.00	0.1017
366.45	3974.00	0.1080
366.45	3975.00	0.1140
366.45	3976.00	0.1185
366.45	3977.00	0.1239
366.45	3978.00	0.1288
366.45	3979.00	0.1341
366.45	3980.00	0.1393
366.45	3981.00	0.1449
366.45	3982.00	0.1502
366.45	3983.00	0.1559
366.45	3984.00	0.1614
366.45	3985.00	0.1661
366.45	3986.00	0.1732
366.45	3987.00	0.1794
366.45	3988.00	0.1853
366.45	3989.00	0.1916
366.45	3990.00	0.1977
366.45	3991.00	0.2045
366.45	3992.00	0.2108
366.45	3993.00	0.2174
366.45	3994.00	0.2240
366.45	3995.00	0.2309
366.45	3996.00	0.2389
365.72	3306.00	0.0340
365.72	3882.00	0.0428
365.72	3883.00	0.0429
365.72	3884.00	0.0457
365.72	3885.00	0.0461
365.72	3890.00	0.0516
365.72	3891.00	0.0531
365.72	3892.00	0.0553
365.72	3893.00	0.0573
365.72	3894.00	0.0593
365.72	3895.00	0.0613
365.72	3896.00	0.0634
365.72	3897.00	0.0657
365.72	3898.00	0.0681
365.72	3899.00	0.0705

365.72	3900.00	0.0728
365.72	3901.00	0.0750
365.72	3902.00	0.0780
365.72	3903.00	0.0811
365.72	3904.00	0.0842
365.72	3905.00	0.0873
365.72	3906.00	0.0904
365.72	3907.00	0.0936
365.72	3908.00	0.0970
365.72	3909.00	0.1001
365.72	3910.00	0.1033
365.72	3911.00	0.1068
365.72	3912.00	0.1099
365.72	3913.00	0.1132
365.72	3914.00	0.1164
365.72	3915.00	0.1201
365.72	3916.00	0.1234
365.72	3917.00	0.1273
365.72	3918.00	0.1307
365.72	3919.00	0.1341
365.72	3920.00	0.1379
365.72	3921.00	0.1413
365.72	3922.00	0.1454
365.72	3923.00	0.1490
365.72	3924.00	0.1527
365.72	3925.00	0.1565
365.72	3926.00	0.1605
365.72	3927.00	0.1644
365.72	3928.00	0.1684
365.72	3929.00	0.1724
365.72	3930.00	0.1763
365.72	3931.00	0.1804
365.72	3932.00	0.1846
365.72	3933.00	0.1886
365.72	3934.00	0.1932
365.72	3935.00	0.1972
365.72	3936.00	0.2015
365.72	3937.00	0.2059
365.72	3938.00	0.2104
365.72	3939.00	0.2148
365.72	3940.00	0.2193
365.72	3941.00	0.2241
365.72	3942.00	0.2290
365.72	3943.00	0.2336

365.72	3944.00	0.2401
364.65	3818.00	0.0419
364.65	3819.00	0.0419
364.65	3820.00	0.0419
364.65	3826.00	0.0480
364.65	3827.00	0.0504
364.65	3828.00	0.0537
364.65	3829.00	0.0568
364.65	3830.00	0.0599
364.65	3831.00	0.0635
364.65	3832.00	0.0673
364.65	3833.00	0.0716
364.65	3834.00	0.0754
364.65	3835.00	0.0797
364.65	3836.00	0.0840
364.65	3837.00	0.0879
364.65	3838.00	0.0920
364.65	3839.00	0.0960
364.65	3840.00	0.1002
364.65	3841.00	0.1044
364.65	3842.00	0.1088
364.65	3843.00	0.1131
364.65	3844.00	0.1173
364.65	3845.00	0.1218
364.65	3846.00	0.1263
364.65	3847.00	0.1307
364.65	3848.00	0.1350
364.65	3849.00	0.1400
364.65	3850.00	0.1445
364.65	3851.00	0.1491
364.65	3852.00	0.1538
364.65	3853.00	0.1584
364.65	3854.00	0.1635
364.65	3855.00	0.1693
364.65	3856.00	0.1732
364.65	3857.00	0.1782
364.65	3858.00	0.1831
364.65	3859.00	0.1881
364.65	3860.00	0.1933
364.65	3861.00	0.1983
364.65	3862.00	0.2036
364.65	3863.00	0.2089
364.65	3864.00	0.2141
364.65	3865.00	0.2194

364.65	3866.00	0.2249
364.65	3867.00	0.2303
364.65	3868.00	0.2361
364.65	3869.00	0.2404

Reference

<https://www.doi.org/10.1016/j.fluid.2017.06.019>

Thermal conductivity, W/m/K

Temperature, K - Fluid (supercritical or subcritical phases)	Pressure, kPa - Fluid (supercritical or subcritical phases)	Thermal conductivity, W/m/K - Fluid (supercritical or subcritical phases)
370.45	15100.00	0.0809
370.45	11300.00	0.0765
370.45	11200.00	0.0774
370.45	11000.00	0.0768
370.45	10500.00	0.0762
370.45	10000.00	0.0757
370.45	9500.00	0.0755
370.45	9000.00	0.0742
370.45	8500.00	0.0738
370.45	8000.00	0.0728
370.45	7500.00	0.0718
370.45	7000.00	0.0709
370.45	6500.00	0.0700
370.45	6000.00	0.0687
370.45	5760.00	0.0681
370.45	5550.00	0.0679
370.45	5500.00	0.0678
370.45	5000.00	0.0672
370.45	4800.00	0.0665
370.45	4580.00	0.0677
370.45	4560.00	0.0681
370.45	4420.00	0.0701
370.45	4400.00	0.0710
370.45	4377.00	0.0722
370.45	4360.00	0.0739
370.45	4355.00	0.0753
370.45	4350.00	0.0767
370.45	4345.00	0.0781
370.45	4340.00	0.0812
370.45	4335.00	0.0881

370.45	4330.00	0.0920
370.45	4325.00	0.0963
370.45	4320.00	0.1010
370.45	4315.00	0.1061
370.45	4310.00	0.1181
370.45	4305.00	0.1291
370.45	4300.00	0.1452
370.45	4295.00	0.1560
370.45	4290.00	0.1423
370.45	4285.00	0.1252
370.45	4280.00	0.1118
370.45	4275.00	0.0962
370.45	4270.00	0.0880
370.45	4265.00	0.0811
370.45	4260.00	0.0774
370.45	4255.00	0.0743
370.45	4250.00	0.0712
370.45	4245.00	0.0688
370.45	4244.00	0.0686
370.45	4241.00	0.0672
370.45	4232.00	0.0638
370.45	4227.00	0.0625
370.45	4224.00	0.0613
370.45	4217.00	0.0590
370.45	4205.00	0.0558
370.45	4200.00	0.0550
370.45	4190.00	0.0533
370.45	4170.00	0.0510
370.45	4105.00	0.0462
370.45	4042.00	0.0439
370.45	3986.00	0.0420
370.45	3856.00	0.0394
370.45	3770.00	0.0381
370.45	3487.00	0.0359
370.45	3452.00	0.0356
371.05	11600.00	0.0776
371.05	9500.00	0.0750
371.05	8900.00	0.0742
371.05	8500.00	0.0734
371.05	7500.00	0.0715
371.05	6800.00	0.0700
371.05	6200.00	0.0693
371.05	6100.00	0.0692
371.05	5672.00	0.0683

371.05	5350.00	0.0677
371.05	5200.00	0.0675
371.05	5000.00	0.0671
371.05	4840.00	0.0667
371.05	4720.00	0.0670
371.05	4715.00	0.0672
371.05	4590.00	0.0678
371.05	4560.00	0.0682
371.05	4555.00	0.0685
371.05	4485.00	0.0692
371.05	4440.00	0.0711
371.05	4420.00	0.0723
371.05	4414.00	0.0736
371.05	4408.00	0.0749
371.05	4402.00	0.0763
371.05	4396.00	0.0778
371.05	4392.00	0.0786
371.05	4387.00	0.0801
371.05	4383.00	0.0814
371.05	4375.00	0.0841
371.05	4370.00	0.0862
371.05	4367.00	0.0884
371.05	4365.00	0.0899
371.05	4361.00	0.0931
371.05	4360.00	0.0940
371.05	4358.00	0.0966
371.05	4356.00	0.0993
371.05	4354.00	0.1028
371.05	4351.00	0.1081
371.05	4349.00	0.1121
371.05	4347.00	0.1159
371.05	4346.00	0.1178
371.05	4345.00	0.1185
371.05	4344.00	0.1192
371.05	4343.00	0.1192
371.05	4342.00	0.1192
371.05	4340.00	0.1185
371.05	4339.00	0.1178
371.05	4338.00	0.1172
371.05	4337.00	0.1159
371.05	4336.00	0.1140
371.05	4334.00	0.1104
371.05	4332.00	0.1075
371.05	4331.00	0.1054

371.05	4329.00	0.1013
371.05	4328.00	0.0993
371.05	4326.00	0.0957
371.05	4325.00	0.0940
371.05	4324.00	0.0911
371.05	4322.00	0.0884
371.05	4319.00	0.0841
371.05	4318.00	0.0814
371.05	4313.00	0.0766
371.05	4308.00	0.0733
371.05	4301.00	0.0687
371.05	4295.00	0.0660
371.05	4289.00	0.0636
371.05	4284.00	0.0612
371.05	4276.00	0.0585
371.05	4265.00	0.0567
371.05	4252.00	0.0539
371.05	4235.00	0.0519
371.05	4215.00	0.0491
371.05	4155.00	0.0463
371.05	4095.00	0.0442
371.05	3900.00	0.0406
371.05	3655.00	0.0374
371.05	3375.00	0.0346
371.05	3100.00	0.0334
371.05	2710.00	0.0321
371.97	15100.00	0.0807
371.97	8810.00	0.0727
371.97	7600.00	0.0715
371.97	6800.00	0.0700
371.97	6400.00	0.0692
371.97	5900.00	0.0680
371.97	5200.00	0.0664
371.97	4850.00	0.0660
371.97	4740.00	0.0662
371.97	4650.00	0.0664
371.97	4570.00	0.0667
371.97	4550.00	0.0676
371.97	4530.00	0.0688
371.97	4505.00	0.0700
371.97	4500.00	0.0702
371.97	4490.00	0.0723
371.97	4475.00	0.0732
371.97	4465.00	0.0751

371.97	4460.00	0.0764
371.97	4455.00	0.0779
371.97	4450.00	0.0809
371.97	4445.00	0.0842
371.97	4440.00	0.0878
371.97	4435.00	0.0916
371.97	4430.00	0.0937
371.97	4425.00	0.0968
371.97	4420.00	0.0997
371.97	4418.00	0.1001
371.97	4416.00	0.1001
371.97	4414.00	0.1000
371.97	4412.00	0.0996
371.97	4410.00	0.0992
371.97	4408.00	0.0985
371.97	4406.00	0.0981
371.97	4404.00	0.0974
371.97	4402.00	0.0960
371.97	4400.00	0.0943
371.97	4398.00	0.0931
371.97	4396.00	0.0918
371.97	4394.00	0.0897
371.97	4392.00	0.0877
371.97	4390.00	0.0866
371.97	4388.00	0.0848
371.97	4386.00	0.0831
371.97	4384.00	0.0817
371.97	4382.00	0.0799
371.97	4380.00	0.0792
371.97	4378.00	0.0775
371.97	4374.00	0.0749
371.97	4370.00	0.0727
371.97	4368.00	0.0715
371.97	4366.00	0.0703
371.97	4362.00	0.0676
371.97	4354.00	0.0636
371.97	4348.00	0.0612
371.97	4342.00	0.0592
371.97	4336.00	0.0572
371.97	4324.00	0.0546
371.97	4312.00	0.0527
371.97	4294.00	0.0505
371.97	4286.00	0.0498
371.97	3803.00	0.0378

371.97	3701.00	0.0365
371.97	3070.00	0.0331
371.97	3025.00	0.0330
373.20	11900.00	0.0782
373.20	10500.00	0.0764
373.20	8900.00	0.0735
373.20	7780.00	0.0715
373.20	7400.00	0.0709
373.20	6700.00	0.0693
373.20	6300.00	0.0688
373.20	5540.00	0.0670
373.20	5100.00	0.0662
373.20	4900.00	0.0661
373.20	4740.00	0.0671
373.20	4680.00	0.0680
373.20	4660.00	0.0689
373.20	4640.00	0.0698
373.20	4610.00	0.0712
373.20	4605.00	0.0717
373.20	4590.00	0.0724
373.20	4574.00	0.0745
373.20	4568.00	0.0753
373.20	4564.00	0.0764
373.20	4556.00	0.0781
373.20	4550.00	0.0799
373.20	4544.00	0.0819
373.20	4536.00	0.0842
373.20	4530.00	0.0855
373.20	4524.00	0.0866
373.20	4518.00	0.0877
373.20	4510.00	0.0873
373.20	4508.00	0.0869
373.20	4506.00	0.0868
373.20	4504.00	0.0866
373.20	4502.00	0.0864
373.20	4500.00	0.0862
373.20	4498.00	0.0858
373.20	4496.00	0.0855
373.20	4494.00	0.0851
373.20	4486.00	0.0831
373.20	4484.00	0.0824
373.20	4482.00	0.0818
373.20	4476.00	0.0796
373.20	4470.00	0.0772

373.20	4466.00	0.0755
373.20	4462.00	0.0739
373.20	4452.00	0.0704
373.20	4450.00	0.0696
373.20	4444.00	0.0675
373.20	4436.00	0.0650
373.20	4428.00	0.0626
373.20	4416.00	0.0600
373.20	4404.00	0.0579
373.20	4384.00	0.0550
373.20	4346.00	0.0516
373.20	4270.00	0.0476
373.20	4230.00	0.0461
373.20	4150.00	0.0436
373.20	4060.00	0.0415
373.20	4030.00	0.0408
373.20	3820.00	0.0379
373.20	3780.00	0.0375
373.20	3450.00	0.0349
373.20	3103.00	0.0332
374.28	6760.00	0.0687
374.28	6323.00	0.0683
374.28	5798.00	0.0671
374.28	5500.00	0.0664
374.28	5200.00	0.0658
374.28	5000.00	0.0660
374.28	4900.00	0.0669
374.28	4820.00	0.0678
374.28	4780.00	0.0687
374.28	4760.00	0.0691
374.28	4740.00	0.0698
374.28	4720.00	0.0703
374.28	4710.00	0.0710
374.28	4685.00	0.0724
374.28	4670.00	0.0733
374.28	4650.00	0.0748
374.28	4640.00	0.0760
374.28	4630.00	0.0775
374.28	4625.00	0.0785
374.28	4620.00	0.0796
374.28	4615.00	0.0804
374.28	4610.00	0.0812
374.28	4605.00	0.0816
374.28	4600.00	0.0815

374.28	4595.00	0.0811
374.28	4590.00	0.0808
374.28	4585.00	0.0802
374.28	4580.00	0.0795
374.28	4575.00	0.0788
374.28	4570.00	0.0779
374.28	4565.00	0.0766
374.28	4560.00	0.0752
374.28	4550.00	0.0727
374.28	4545.00	0.0712
374.28	4535.00	0.0687
374.28	4520.00	0.0655
374.28	4518.00	0.0650
374.28	4515.00	0.0642
374.28	4510.00	0.0632
374.28	4485.00	0.0596
374.28	4475.00	0.0582
374.28	4460.00	0.0563
374.28	4450.00	0.0548
374.28	4440.00	0.0538
374.28	4425.00	0.0524
374.28	4380.00	0.0496
374.28	4320.00	0.0472
374.28	4280.00	0.0456
374.28	4200.00	0.0438
374.28	4080.00	0.0412
374.28	3975.00	0.0392
374.28	3945.00	0.0389
374.28	3424.00	0.0345
374.28	3087.00	0.0327
374.28	2900.00	0.0316
375.10	10360.00	0.0750
375.10	9700.00	0.0739
375.10	9500.00	0.0736
375.10	8950.00	0.0727
375.10	8020.00	0.0711
375.10	7140.00	0.0696
375.10	6540.00	0.0685
375.10	6480.00	0.0684
375.10	5830.00	0.0669
375.10	5580.00	0.0664
375.10	5322.00	0.0658
375.10	5226.00	0.0653
375.10	5160.00	0.0653

375.10	5140.00	0.0653
375.10	5040.00	0.0653
375.10	4950.00	0.0653
375.10	4920.00	0.0655
375.10	4890.00	0.0660
375.10	4850.00	0.0668
375.10	4800.00	0.0681
375.10	4790.00	0.0685
375.10	4770.00	0.0697
375.10	4750.00	0.0706
375.10	4740.00	0.0711
375.10	4720.00	0.0726
375.10	4710.00	0.0735
375.10	4700.00	0.0741
375.10	4695.00	0.0747
375.10	4685.00	0.0754
375.10	4680.00	0.0757
375.10	4675.00	0.0760
375.10	4670.00	0.0762
375.10	4665.00	0.0765
375.10	4660.00	0.0764
375.10	4655.00	0.0761
375.10	4650.00	0.0758
375.10	4645.00	0.0754
375.10	4640.00	0.0751
375.10	4635.00	0.0745
375.10	4630.00	0.0737
375.10	4625.00	0.0729
375.10	4620.00	0.0722
375.10	4610.00	0.0705
375.10	4605.00	0.0697
375.10	4600.00	0.0688
375.10	4595.00	0.0679
375.10	4590.00	0.0671
375.10	4585.00	0.0661
375.10	4580.00	0.0651
375.10	4575.00	0.0642
375.10	4570.00	0.0633
375.10	4565.00	0.0626
375.10	4560.00	0.0619
375.10	4555.00	0.0612
375.10	4550.00	0.0605
375.10	4545.00	0.0597
375.10	4535.00	0.0585

375.10	4525.00	0.0572
375.10	4520.00	0.0565
375.10	4510.00	0.0555
375.10	4450.00	0.0515
375.10	4400.00	0.0491
375.10	4350.00	0.0474
375.10	4315.00	0.0459
375.10	4300.00	0.0453
375.10	4210.00	0.0428
375.10	3794.00	0.0376
375.10	3790.00	0.0373
375.10	3780.00	0.0369
375.90	13000.00	0.0785
375.90	12000.00	0.0772
375.90	11500.00	0.0765
375.90	11028.00	0.0760
375.90	11000.00	0.0759
375.90	10000.00	0.0744
375.90	9806.00	0.0741
375.90	9190.00	0.0731
375.90	9000.00	0.0729
375.90	8500.00	0.0720
375.90	7800.00	0.0706
375.90	7200.00	0.0696
375.90	6800.00	0.0688
375.90	6200.00	0.0675
375.90	6000.00	0.0671
375.90	5900.00	0.0670
375.90	5820.00	0.0668
375.90	5700.00	0.0667
375.90	5550.00	0.0663
375.90	5500.00	0.0663
375.90	5250.00	0.0659
375.90	5200.00	0.0660
375.90	5100.00	0.0662
375.90	5050.00	0.0662
375.90	4950.00	0.0671
375.90	4880.00	0.0683
375.90	4840.00	0.0694
375.90	4820.00	0.0699
375.90	4800.00	0.0705
375.90	4780.00	0.0711
375.90	4760.00	0.0721
375.90	4740.00	0.0726

375.90	4720.00	0.0728
375.90	4700.00	0.0716
375.90	4690.00	0.0706
375.90	4680.00	0.0697
375.90	4670.00	0.0683
375.90	4660.00	0.0670
375.90	4650.00	0.0657
375.90	4640.00	0.0645
375.90	4630.00	0.0628
375.90	4620.00	0.0613
375.90	4600.00	0.0595
375.90	4590.00	0.0583
375.90	4580.00	0.0571
375.90	4570.00	0.0561
375.90	4560.00	0.0550
375.90	4540.00	0.0535
375.90	4510.00	0.0517
375.90	4450.00	0.0488
375.90	4400.00	0.0473
375.90	4350.00	0.0459
375.90	4250.00	0.0435
375.90	4125.00	0.0409
375.90	4050.00	0.0399
375.90	4000.00	0.0393
375.90	3800.00	0.0375
375.90	3600.00	0.0360
375.90	3550.00	0.0356
375.90	3300.00	0.0343
375.90	3250.00	0.0341
375.90	3134.00	0.0338
375.90	3110.00	0.0337
381.00	14750.00	0.0785
381.00	12000.00	0.0753
381.00	11000.00	0.0737
381.00	10110.00	0.0723
381.00	9036.00	0.0703
381.00	7583.00	0.0677
381.00	7300.00	0.0671
381.00	7162.00	0.0670
381.00	6900.00	0.0664
381.00	6500.00	0.0655
381.00	6200.00	0.0650
381.00	5900.00	0.0642
381.00	5700.00	0.0644

381.00	5550.00	0.0644
381.00	5450.00	0.0644
381.00	5390.00	0.0643
381.00	5350.00	0.0644
381.00	5300.00	0.0644
381.00	5250.00	0.0648
381.00	5200.00	0.0645
381.00	5150.00	0.0645
381.00	5100.00	0.0637
381.00	5060.00	0.0627
381.00	5040.00	0.0620
381.00	5020.00	0.0612
381.00	5000.00	0.0605
381.00	4960.00	0.0587
381.00	4920.00	0.0568
381.00	4900.00	0.0559
381.00	4880.00	0.0551
381.00	4860.00	0.0542
381.00	4800.00	0.0519
381.00	4780.00	0.0513
381.00	4740.00	0.0499
381.00	4660.00	0.0476
381.00	4600.00	0.0462
381.00	4560.00	0.0454
381.00	4520.00	0.0446
381.00	4220.00	0.0403
381.00	4100.00	0.0389
381.00	4040.00	0.0382
381.00	3880.00	0.0370
381.00	3820.00	0.0367
381.00	3580.00	0.0356
381.00	3428.00	0.0350
381.00	3320.00	0.0345
381.00	3260.00	0.0343
381.00	3253.00	0.0343

Reference

<https://www.doi.org/10.1021/je500395f>

Molar heat capacity at constant volume, J/K/mol

Temperature, K - Fluid (supercritical or subcritical phases)	Pressure, kPa - Fluid (supercritical or subcritical phases)	Molar heat capacity at constant volume, J/K/mol - Fluid (supercritical or subcritical phases)
270.15	4427.00	71.7436
275.15	7953.00	71.2585
280.15	11458.00	71.3026
285.15	14939.00	72.6255
290.15	18398.00	73.4633
295.15	21836.00	74.5657
300.15	25251.00	74.6098
305.15	28640.00	74.3452
310.15	6561.00	74.5657
315.15	9049.00	75.2271
320.15	11532.00	76.1531
325.15	3660.00	77.9611
325.15	14008.00	76.3736
330.15	5594.00	78.7548
330.15	16475.00	76.6382
335.15	7530.00	78.3138
335.15	18934.00	76.9028
340.15	9468.00	77.6965
340.15	21386.00	77.2114
345.15	11404.00	77.2555
345.15	23827.00	76.3295
350.15	13339.00	79.4603
350.15	26253.00	77.5201
355.15	15273.00	77.3878
355.15	28668.00	77.4319
360.15	17203.00	77.7406
365.15	19126.00	78.6225
370.15	21044.00	79.1516
375.15	5095.00	98.5978
380.15	5744.00	93.0418
385.15	6404.00	89.6023
390.15	7072.00	86.0747
395.15	7746.00	84.84
400.15	8425.00	80.4304
405.15	9109.00	78.843
410.15	9795.00	79.9895
420.15	11176.00	79.8131
425.15	11869.00	81.7533

Reference

<https://www.doi.org/10.1007/s10765-005-8592-5>

Molar heat capacity at constant volume, J/K/mol

Temperature, K - Liquid	Pressure, kPa - Liquid	Molar heat capacity at constant volume, J/K/mol - Liquid
236.31	2219.00	65.7907
238.69	4211.00	66.2316
241.04	6180.00	66.6726
243.36	8127.00	66.5844
245.69	10074.00	66.9372
250.09	2085.00	67.5986
252.35	3780.00	68.1277
254.59	5476.00	68.1277
256.82	7162.00	67.9073
259.03	8839.00	68.4805
261.25	10512.00	68.6128
264.41	2430.00	69.0978
266.66	3950.00	69.186
268.92	5488.00	70.2443
271.21	7042.00	70.3325
273.50	8593.00	70.2002
275.81	10155.00	70.553
283.73	2629.00	71.6113
287.25	4679.00	71.92
289.61	6040.00	71.9641
291.99	7411.00	72.3609
294.35	8774.00	72.846
296.69	10124.00	72.9342
299.00	11450.00	73.2428
301.28	12754.00	73.2428
306.13	1912.00	74.698
308.58	3022.00	75.5799
311.04	4140.00	75.624
313.50	5260.00	76.4177
315.96	6379.00	76.55
318.43	7498.00	76.5941
320.89	8615.00	77.5201
323.37	9735.00	77.7406
325.84	10852.00	78.1815
328.28	11956.00	78.8871
330.71	13052.00	79.328

332.33	10672.00	78.8871
334.81	11722.00	79.8131
337.26	12761.00	80.4745
339.76	13813.00	80.6509
284.60	1745.00	71.3026
286.92	3057.00	71.8759
289.25	4373.00	72.2286
291.57	5681.00	72.3168
293.90	6981.00	72.9783
296.28	8309.00	73.1546
298.66	9622.00	73.1987
300.98	10901.00	74.3452
303.33	12177.00	74.6539
305.66	13418.00	75.0948

Reference

<https://www.doi.org/10.1016/j.jct.2018.05.022>

Temperature, K	Pressure, kPa	Molar heat capacity at constant pressure, J/K/mol
108.15	1160.00	84.97
108.15	3680.00	86.69
108.15	5160.00	86.65
108.15	5330.00	84.80
118.15	1170.00	84.75
118.15	3650.00	87.09
118.15	5180.00	87.04
118.15	5430.00	85.46
128.15	1180.00	85.28
128.15	3640.00	86.65
128.15	3670.00	86.30
128.15	5190.00	86.56
128.15	5430.00	85.55
143.15	1130.00	86.43
143.15	3690.00	86.69
143.15	5180.00	86.56
153.15	1190.00	87.62
153.15	5200.00	88.68
163.15	1170.00	87.97
163.15	5210.00	89.34
188.15	1190.00	91.15
188.15	5220.00	91.10
228.15	1150.00	98.73
228.15	3670.00	98.42
228.15	5220.00	98.11

238.15	1110.00	101.24
238.15	3680.00	100.71
238.15	5220.00	100.63
248.15	1160.00	103.58
248.15	3670.00	102.17
248.15	5190.00	101.46
258.15	1160.00	105.65
258.15	3680.00	104.11
258.15	5220.00	103.76

Reference

<https://www.doi.org/10.1021/je300762m>

Viscosity, Pa*s

Temperature, K - Fluid (supercritical or subcritical phases)	Pressure, kPa - Fluid (supercritical or subcritical phases)	Viscosity, Pa*s - Fluid (supercritical or subcritical phases)
273.15	40.93	0.0000074
273.15	51.05	0.0000074
273.15	100.76	0.0000074
273.15	149.62	0.0000074
273.15	196.97	0.0000074
273.15	243.87	0.0000074
273.15	289.30	0.0000074
273.15	333.56	0.0000074
273.15	376.67	0.0000074
273.15	420.03	0.0000074
273.15	459.55	0.0000074
273.15	459.58	0.0000074
273.15	420.03	0.0000074
298.15	44.70	0.0000081
298.15	55.55	0.0000081
298.15	110.39	0.0000081
298.15	164.09	0.0000081
298.15	164.66	0.0000081
298.15	217.05	0.0000081
298.15	217.09	0.0000081
298.15	268.78	0.0000081
298.15	318.03	0.0000081
298.15	369.40	0.0000081
298.15	418.44	0.0000081
298.15	464.73	0.0000081

298.15	498.81	0.0000081
298.15	513.59	0.0000081
298.15	559.93	0.0000081
298.15	600.75	0.0000081
298.15	604.00	0.0000081
298.15	646.36	0.0000081
298.15	691.04	0.0000081
298.15	692.19	0.0000081
298.15	783.49	0.0000081
298.15	849.03	0.0000081
298.15	875.16	0.0000082
298.15	878.68	0.0000082
298.15	646.36	0.0000081
366.15	68.97	0.0000099
366.15	136.86	0.0000099
366.15	270.35	0.0000099
366.15	400.53	0.0000100
366.15	527.04	0.0000100
366.15	649.96	0.0000100
366.15	772.49	0.0000100
366.15	897.82	0.0000100
366.15	1004.80	0.0000101
366.15	1119.80	0.0000101
366.15	1222.30	0.0000101
366.15	1738.70	0.0000103
366.15	2181.80	0.0000106
366.15	2559.10	0.0000108
366.15	2883.00	0.0000111
366.15	3154.40	0.0000115
366.15	3381.10	0.0000119
366.15	3559.50	0.0000123
366.15	3704.10	0.0000128
366.15	3704.90	0.0000128
373.15	70.00	0.0000101
373.15	139.24	0.0000101
373.15	275.58	0.0000101
373.15	408.76	0.0000101
373.15	538.60	0.0000102
373.15	666.93	0.0000102
373.15	733.66	0.0000102
373.15	917.57	0.0000103
373.15	1023.30	0.0000103
373.15	1147.80	0.0000103
373.15	1248.00	0.0000104

373.15	1781.80	0.0000106
373.15	1781.90	0.0000106
373.15	2244.20	0.0000108
373.15	2244.50	0.0000108
373.15	2640.80	0.0000111
373.15	2640.90	0.0000111
373.15	2984.30	0.0000115
373.15	2984.40	0.0000115
373.15	3288.70	0.0000119
373.15	3289.00	0.0000119
373.15	3531.30	0.0000123
373.15	3531.60	0.0000123
373.15	3739.80	0.0000127
373.15	3740.20	0.0000127
373.15	3909.10	0.0000132
373.15	3909.30	0.0000132
373.15	4152.50	0.0000143
373.15	4152.60	0.0000143
373.15	4314.60	0.0000156
373.15	4400.60	0.0000169
373.15	4400.70	0.0000169
373.15	4432.90	0.0000177
373.15	4458.20	0.0000188
373.15	4477.30	0.0000200
373.15	4477.40	0.0000200
373.15	4491.90	0.0000213
373.15	4492.00	0.0000214
373.15	4502.70	0.0000225
373.15	4512.20	0.0000235
373.15	4515.00	0.0000238
373.15	4515.10	0.0000238
373.15	4530.10	0.0000252
373.15	4530.20	0.0000252
373.15	4556.00	0.0000270
373.15	4556.10	0.0000270
373.15	4576.20	0.0000280
373.15	4576.30	0.0000281
373.15	4606.10	0.0000293
373.15	4657.20	0.0000308
373.15	4657.50	0.0000308
373.15	4809.30	0.0000337
373.15	4809.50	0.0000337
373.15	5105.60	0.0000371
373.15	5105.80	0.0000371

373.15	5614.70	0.0000408
373.15	5616.40	0.0000408
373.15	5652.10	0.0000410
373.15	5664.60	0.0000410
373.15	5665.90	0.0000411
373.15	6602.80	0.0000455
373.15	6603.50	0.0000455
373.15	8140.10	0.0000508
373.15	8140.40	0.0000508
373.15	10482.00	0.0000567
373.15	10483.00	0.0000567
373.15	13841.00	0.0000635
373.15	18565.00	0.0000713
373.15	18567.00	0.0000713
373.15	25008.00	0.0000801
373.15	25010.00	0.0000802
373.15	28973.00	0.0000853
373.15	28975.00	0.0000853
373.15	29829.00	0.0000863
373.15	29830.00	0.0000863
373.15	4314.60	0.0000156
373.15	4432.90	0.0000177
373.15	4458.20	0.0000188
373.15	4502.70	0.0000225
373.15	4512.20	0.0000235
373.15	4606.10	0.0000293
373.15	13841.00	0.0000634
373.15	25008.00	0.0000802
373.15	25010.00	0.0000801
373.15	28975.00	0.0000854
373.15	4432.90	0.0000177
373.15	28975.00	0.0000853
423.15	79.37	0.0000114
423.15	158.25	0.0000114
423.15	313.56	0.0000114
423.15	466.92	0.0000114
423.15	467.03	0.0000114
423.15	611.20	0.0000115
423.15	611.47	0.0000115
423.15	763.44	0.0000115
423.15	763.61	0.0000115
423.15	920.80	0.0000115
423.15	1060.20	0.0000116
423.15	1061.30	0.0000116

423.15	1192.70	0.0000116
423.15	1193.50	0.0000116
423.15	1334.70	0.0000116
423.15	1335.70	0.0000116
423.15	1454.80	0.0000117
423.15	2110.00	0.0000119
423.15	2110.70	0.0000119
423.15	2704.30	0.0000122
423.15	2704.80	0.0000122
423.15	3242.60	0.0000125
423.15	3243.30	0.0000125
423.15	3747.90	0.0000128
423.15	3749.20	0.0000128
423.15	4207.40	0.0000132
423.15	4207.90	0.0000132
423.15	4616.70	0.0000136
423.15	4617.30	0.0000137
423.15	5007.50	0.0000141
423.15	5008.60	0.0000141
423.15	5358.60	0.0000146
423.15	5360.20	0.0000146
423.15	5989.50	0.0000157
423.15	5989.80	0.0000157
423.15	6545.10	0.0000170
423.15	6545.30	0.0000170
423.15	7033.00	0.0000184
423.15	7033.70	0.0000184
423.15	7520.10	0.0000200
423.15	7520.80	0.0000200
423.15	7992.20	0.0000218
423.15	7992.60	0.0000218
423.15	8516.00	0.0000240
423.15	8516.40	0.0000239
423.15	9079.60	0.0000262
423.15	9079.90	0.0000262
423.15	9738.40	0.0000288
423.15	9738.50	0.0000288
423.15	10543.00	0.0000316
423.15	10544.00	0.0000316
423.15	11566.00	0.0000348
423.15	12882.00	0.0000383
423.15	12884.00	0.0000383
423.15	14693.00	0.0000424
423.15	17064.00	0.0000469

423.15	17065.00	0.0000469
423.15	20192.00	0.0000521
423.15	20193.00	0.0000521
423.15	24333.00	0.0000580
423.15	24334.00	0.0000580
423.15	29700.00	0.0000646
423.15	29703.00	0.0000647
423.15	920.80	0.0000115
423.15	1454.80	0.0000117
423.15	11566.00	0.0000348
423.15	14693.00	0.0000423

Reference

<https://www.doi.org/10.1021/je101178u>

Mass density, kg/m3

Temperature, K - Gas	Pressure, kPa - Gas	Mass density, kg/m3 - Gas
293.10	803.62	17.2181
293.12	340.88	6.5552
293.12	106.57	1.9628
288.22	653.34	13.8134
288.21	538.60	11.0628
288.21	421.87	8.433
288.22	322.62	6.3129
288.22	217.75	4.1713
288.22	101.88	1.9105
283.13	615.83	13.2515
283.13	452.56	9.3303
283.13	284.93	5.6533
283.13	101.63	1.942
278.14	542.76	11.76
278.14	283.52	5.7427
278.15	105.47	2.0544
273.15	462.55	10.0438
273.14	250.22	5.1361
273.15	101.65	2.0177
273.15	101.64	2.0179
268.16	386.83	8.4369
268.16	297.13	6.3169
268.14	251.50	5.2792
268.15	101.59	2.0567

263.17	314.80	6.8907
263.16	209.67	4.4546
263.17	101.09	2.0885
258.15	276.61	6.1388
258.15	201.63	4.3743
258.14	101.23	2.1368

Reference

<https://www.doi.org/10.1016/j.fluid.2015.09.010>

Temperature, K	Pressure, kPa	Mass density, kg/m3
283.37	449.40	9.302
288.36	459.30	9.3
293.35	468.80	9.298
298.35	478.60	9.295
303.33	488.40	9.293
308.32	497.90	9.291
313.33	507.70	9.289
318.31	517.00	9.286
323.31	527.00	9.284
328.30	536.30	9.282
333.28	545.90	9.28
338.28	555.00	9.278
343.27	564.20	9.275
348.28	573.50	9.273
353.29	583.50	9.271
283.37	541.40	11.462
288.36	554.00	11.459
293.35	566.10	11.456
298.35	578.60	11.454
303.33	590.90	11.451
308.32	602.90	11.448
313.33	614.90	11.445
318.31	626.70	11.443
323.31	638.80	11.44
328.30	650.60	11.437
333.28	662.40	11.435
338.28	674.20	11.432
343.27	685.90	11.429
348.28	697.60	11.426
353.29	709.30	11.424
298.35	870.60	18.472
303.33	891.20	18.467
308.33	912.30	18.463

313.33	933.20	18.458
318.31	953.20	18.454
323.31	973.80	18.449
328.30	993.70	18.445
333.28	1013.90	18.441
338.28	1033.10	18.436
343.27	1052.80	18.432
348.28	1072.60	18.427
353.29	1092.10	18.423

Reference

<https://www.doi.org/10.1016/j.fluid.2019.04.033>

Mass density, kg/m3

Temperature, K - Fluid (supercritical or subcritical phases)	Pressure, kPa - Fluid (supercritical or subcritical phases)	Mass density, kg/m3 - Fluid (supercritical or subcritical phases)
360.00	200000.00	624.04
360.00	180000.00	614.83
360.00	160000.00	605.2
360.00	140000.00	594.1
360.00	120000.00	582.46
360.00	100000.00	568.67
360.00	90000.00	560.92
360.00	80000.00	552.56
360.00	70000.00	543.15
360.00	60000.00	532.63
360.00	50000.00	520.66
400.00	200000.00	605.48
400.00	180000.00	595.54
400.00	160000.00	584.9
400.00	140000.00	573.12
400.00	120000.00	559.78
400.00	100000.00	544.28
400.00	90000.00	535.66
400.00	80000.00	525.98
400.00	70000.00	515.19
400.00	60000.00	503.01
400.00	50000.00	488.73
440.00	200000.00	587.69
440.00	180000.00	577.17
440.00	160000.00	565.72

440.00	140000.00	552.91
440.00	120000.00	538.35
440.00	100000.00	521.48
440.00	90000.00	511.84
440.00	80000.00	500.95
440.00	70000.00	488.72
440.00	60000.00	474.47
440.00	50000.00	457.63
500.00	200000.00	563.13
500.00	180000.00	551.84
500.00	160000.00	539.2
500.00	140000.00	524.91
500.00	120000.00	508.54
500.00	100000.00	489.12
500.00	90000.00	477.92
500.00	80000.00	465.53
500.00	70000.00	450.94
500.00	60000.00	434.04
500.00	50000.00	413.41
550.00	200000.00	544.69
550.00	180000.00	532.53
550.00	160000.00	518.92
550.00	140000.00	503.64
550.00	120000.00	485.88
550.00	100000.00	464.72
550.00	90000.00	452.84
550.00	80000.00	438.76
550.00	70000.00	422.59
550.00	60000.00	403.51
550.00	50000.00	380.04
600.00	200000.00	527.68
600.00	180000.00	514.78
600.00	160000.00	500.33
600.00	140000.00	484.26
600.00	120000.00	465.07
600.00	100000.00	442.26
600.00	90000.00	428.88
600.00	80000.00	413.71
600.00	70000.00	396.1
600.00	60000.00	375.39
600.00	50000.00	349.68

Reference

<https://www.doi.org/10.1007/s10765-012-1383-x>

Temperature, K	Pressure, kPa	Mass density, kg/m3
280.00	581.40	519.39
280.00	604.80	519.45
280.00	628.10	519.49
280.00	651.40	519.57
280.00	674.70	519.62
280.00	698.00	519.69
280.00	721.40	519.75
300.00	1006.00	489.83
300.00	1029.40	489.89
300.00	1052.60	489.98
300.00	1075.90	490.05
300.00	1099.30	490.1
300.00	1122.60	490.2
300.00	1145.90	490.3
320.00	1611.10	455.49
320.00	1634.40	455.61
320.00	1657.60	455.75
320.00	1680.90	455.88
320.00	1704.20	455.99
320.00	1727.50	456.09
320.00	1750.70	456.24
340.00	2447.10	412.74
340.00	2470.30	412.98
340.00	2493.40	413.23
340.00	2516.60	413.48
340.00	2539.80	413.66
340.00	2563.00	413.88
340.00	2586.20	414.08
360.00	3558.00	346.61
360.00	3558.80	346.43
360.00	3566.80	346.83
360.00	3569.10	347.17
360.00	3569.90	346.97
360.00	3580.30	347.61
360.00	3591.60	348.04
360.00	3592.20	347.94
360.00	3602.80	348.46
360.00	3614.00	348.96
360.00	3614.50	348.91
360.00	3622.60	349.31
360.00	3625.20	349.4
360.00	3636.50	349.82
360.00	3636.90	349.82

360.00	3647.80	350.25
360.00	3659.00	350.7
360.00	3659.40	350.7
360.00	3670.30	351.13
360.00	3678.70	351.52
360.00	3681.80	351.59
360.00	3704.30	352.44
360.00	3726.80	353.19
365.00	3897.80	317.84
365.00	3903.00	318.4
365.00	3923.70	320.49
365.00	3944.70	322.39
365.00	3965.90	324.14
365.00	3987.20	325.86
365.00	4008.70	327.39
365.00	4030.40	328.84

Reference

<https://www.doi.org/10.1016/j.jct.2006.07.012>

Temperature, K	Pressure, kPa	Mass density, kg/m3
280.00	1000.00	520.5
280.00	2000.00	522.64
280.00	3000.00	524.74
280.00	5000.00	528.56
280.00	10000.00	537.44
280.00	20000.00	551.94
280.00	30000.00	563.74
280.00	40000.00	573.78
280.00	50000.00	582.55
280.00	60000.00	590.49
280.00	70000.00	597.67
280.00	80000.00	604.54
280.00	90000.00	610.6
280.00	100000.00	616.37
280.00	120000.00	627.11
280.00	140000.00	636.51
280.00	160000.00	645.22
280.00	180000.00	653.38
280.00	200000.00	660.82
300.00	1000.00	489.81
300.00	2000.00	492.87
300.00	3000.00	495.95
300.00	5000.00	501.37

300.00	10000.00	512.99
300.00	20000.00	530.94
300.00	30000.00	544.91
300.00	40000.00	556.1
300.00	50000.00	566.32
300.00	60000.00	575.16
300.00	70000.00	583.22
300.00	80000.00	590.34
300.00	90000.00	597.08
300.00	100000.00	603.47
300.00	120000.00	614.69
300.00	140000.00	624.98
300.00	160000.00	634.04
300.00	180000.00	642.55
300.00	200000.00	650.24
320.00	2000.00	457.48
320.00	3000.00	462.23
320.00	5000.00	470.53
320.00	10000.00	486.59
320.00	20000.00	509.27
320.00	30000.00	525.89
320.00	40000.00	539.36
320.00	50000.00	550.64
320.00	60000.00	560.7
320.00	70000.00	569.45
320.00	80000.00	577.41
320.00	90000.00	584.63
320.00	100000.00	591.38
320.00	120000.00	603.54
320.00	140000.00	614.39
320.00	160000.00	624.07
320.00	180000.00	632.92
320.00	200000.00	641.18
340.00	3000.00	418.14
340.00	5000.00	433.26
340.00	10000.00	457.48
340.00	20000.00	486.91
340.00	30000.00	506.87
340.00	40000.00	522.28
340.00	50000.00	534.97
340.00	60000.00	545.94
340.00	70000.00	555.7
340.00	80000.00	564.27
340.00	90000.00	572.21

340.00	100000.00	579.45
340.00	120000.00	592.54
340.00	140000.00	603.89
340.00	160000.00	614.28
340.00	180000.00	623.6
340.00	200000.00	632.17
360.00	5000.00	380.9
360.00	10000.00	424.08
360.00	20000.00	463.3
360.00	30000.00	487.16
360.00	40000.00	505.03
360.00	50000.00	519.45
360.00	60000.00	531.56
360.00	70000.00	542.12
360.00	80000.00	551.67
360.00	90000.00	560.11
360.00	100000.00	568.02
360.00	120000.00	581.93
360.00	140000.00	593.99
360.00	160000.00	604.85
360.00	180000.00	614.61
360.00	200000.00	623.73
380.00	10000.00	384.1
380.00	20000.00	438.22
380.00	30000.00	466.67
380.00	40000.00	487.15
380.00	50000.00	503.08
380.00	60000.00	516.47
380.00	70000.00	527.94
380.00	80000.00	538.06
380.00	90000.00	547.06
380.00	100000.00	555.29
380.00	120000.00	570.05
380.00	140000.00	582.94
380.00	160000.00	594.15
380.00	180000.00	604.41
380.00	200000.00	613.68
400.00	10000.00	334.74
400.00	20000.00	411.69
400.00	30000.00	445.87
400.00	40000.00	469.1
400.00	50000.00	486.87
400.00	60000.00	501.44
400.00	70000.00	513.89

400.00	80000.00	524.67
400.00	90000.00	534.43
400.00	100000.00	543.41
400.00	120000.00	558.91
400.00	140000.00	572.19
400.00	160000.00	583.93
400.00	180000.00	594.64
400.00	200000.00	604.15
420.00	20000.00	384.77
420.00	30000.00	425.47
420.00	40000.00	451.66
420.00	50000.00	471.39
420.00	60000.00	487.29
420.00	70000.00	500.74
420.00	80000.00	512.43
420.00	90000.00	522.77
420.00	100000.00	532.04
420.00	120000.00	548.04
420.00	140000.00	562.28
420.00	160000.00	574.66
420.00	180000.00	585.51
420.00	200000.00	595.61
440.00	20000.00	357.43
440.00	30000.00	405.22
440.00	40000.00	434.68
440.00	50000.00	456.37
440.00	60000.00	473.51
440.00	70000.00	488.02
440.00	80000.00	500.46
440.00	90000.00	511.55
440.00	100000.00	521.4
440.00	120000.00	538.39
440.00	140000.00	553.07
440.00	160000.00	565.84
440.00	180000.00	577.32
440.00	200000.00	587.63

Reference

<https://www.doi.org/10.1016/j.jct.2007.03.012>

Temperature, K	Pressure, kPa	Mass density, kg/m3
207.35	1466.90	609.37
208.31	2745.80	609.32
209.06	3635.60	609.28

209.75	4364.70	609.25
215.17	10724.00	608.98
222.43	1045.60	592.03
222.75	19646.00	608.63
223.37	2016.70	591.98
224.52	3087.10	591.93
225.47	4153.80	591.89
226.91	5632.50	591.82
231.06	30008.00	608.23
231.07	10051.00	591.62
239.51	39217.00	607.87
240.49	1194.00	571.45
240.67	19671.00	591.21
240.92	1528.80	571.44
242.87	3265.50	571.39
244.55	4758.90	571.35
245.44	5554.00	571.33
250.10	9711.40	571.2
250.12	29984.00	590.79
251.11	51133.00	607.38
259.96	1060.80	547.54
261.06	19770.00	571.13
261.18	40016.00	590.35
261.19	1975.00	547.51
262.52	3059.70	547.47
262.52	2951.90	547.48
263.78	4004.00	547.44
265.28	5120.20	547.4
266.44	5840.10	547.37
267.87	6954.70	547.34
270.11	49092.00	589.98
270.22	1044.70	533.77
271.68	2041.50	533.71
272.12	30057.00	570.94
272.12	10829.00	547.66
272.13	10235.00	547.22
273.11	3025.30	533.66
274.51	3979.10	533.61
276.20	5186.10	533.54
283.08	995.20	515.52
283.43	38987.00	570.26
283.64	10260.00	533.26
284.77	2002.10	515.46
284.98	19876.00	546.88

286.56	3090.50	515.39
288.23	4086.10	515.33
289.90	5086.20	515.27
295.92	49573.00	569.78
297.68	1075.00	493.21
298.14	10031.00	514.99
298.15	10038.00	514.99
298.15	19981.00	532.71
298.15	30100.00	546.7
298.15	30027.00	546.51
298.18	19921.00	532.75
298.19	20084.00	532.74
299.62	2037.90	493.14
301.57	3036.90	493.08
303.56	4053.80	493.01
305.53	5060.20	492.95
311.44	39238.00	545.97
313.68	30193.00	532.17
315.23	2005.20	466.11
315.23	19842.00	514.41
315.23	9905.50	492.64
315.23	10017.00	492.63
317.42	2930.20	466.04
319.89	3981.70	465.97
322.25	4976.50	465.9
332.01	29682.00	513.86
333.97	19538.00	492.04
334.14	9861.60	465.55
344.57	49972.00	531.11
353.14	42004.00	513.17
353.14	29253.00	491.45
353.15	17921.00	464.99

Reference

<https://www.doi.org/10.1021/je300148f>

Sources

The (p,q,T,x) properties of (x1 propane + x2 n-butane) with x1 = (0.0000, 0.2729, 0.5000, 0.7000) and excess Gibbs free energy of binary mixtures of hydrogen systems n-butane-propane and n-butane + decalindene at temperatures 600, 623, 646, 673, 700, 723, 750, 773, 800, 823, 850, 873, 900, 923, 950, 973, 1000 K: single source general diagrams of Propane + Decalindene and Propane + Naphthalene Mixtures:

<https://www.doi.org/10.1016/j.jct.2007.06.014>

<https://www.doi.org/10.1016/j.jct.2006.03.013>

<https://www.doi.org/10.1016/j.jct.2014.10.001>

<https://www.doi.org/10.1021/je0341458>

Saturated liquid densities of propane at
T = (280 to 365) K:
Fluid Phase Equilibria of Binary
n-Alkane + Squalene Systems:
Critical parameters for propane
determined by the image analysis:
Bubble Point Measurements of
n-Butane + n-Octane and n-Butane +
Nonadecane Mixtures:
Measurements of the Surface
Tension of the R290 + R32 Mixture:
(p, rho, T, x) Properties of CO 2
/Propane Binary Mixtures at 280 K to
Maximum Pressure and the Thermal
conductivity of propane at the
approach of the critical point for mixtures
involving
Measures of the Thermodynamic
Consistency of Propane in the
Gas-liquid Region (P, rho, T)
Properties for Pure Hydrocarbons at
Temperatures Above Critical and Sub-
and Supercritical Propane MPa:
Surface tension and critical point
measurements of methane + propane
Henry's law constants and infinite
dilution activity coefficients of propane,
NIST Webbook
Propane, butane, isobutane, 1-butene,
isobutene, trans-2-butene, and
thermodynamic properties of (R1234yf
+ R290), Isochoric P, rho, Tx and
gas-fugacity coefficient for the carbon
flexible elements and system uovers of
equilibrium of hydrogen and water
near Propane and Carbon Dioxide
Thermodynamic modeling of liquid
phase equilibrium conditions for
the binary {1,1,2,2-tetrafluoroethane
Experimental Study of the T
Relation of Propane compressed liquid
Phase equilibria of hydrocarbon and
Two mass fractions to tetranitrodipic
solubility of Tetranitrodimerglycoluril
(TNDGU) in Different Solvents at
Temperatures Between 273K and Sub-
and Supercritical Propane:
Phase equilibrium data and
thermodynamic modelling of the
System Behavior of Binary and Ternary
Systems involving Carbon Dioxide,
Propane, and Glycidyl propyl ether at
high pressure: Method for Determining
the Critical Parameters of Binary and
ternary mixtures of
Density of 1,9-dimethylcyclohexane with
tri-n-octamethane (HFC-227 + propane)
Anhydrous methanol over 260 °C propane.
h-Butane Behavior from (265 to 500) K
with pressures to 36 MPa
Mixtures of HFC-125 + Propane from 298.15 to
423.15 K compositions and infinite dilution
activity coefficients of propane,
butane, butane, isobutane, 1-butene,
isobutene, trans-2-butene, and
hydrocarbon mixtures Data for the
Equilibrium between liquid and vapor
systems at temperatures from 194.83 to
Dilution Activity Coefficients of 4 MPa:
Propane, n-pentane, Ethane Sulfide +
2-methylpropane (25 to 365) K,
2-methylpropane, trans-2-Butene,
cis-2-Butene, 1,3-Butadiene, Dimethyl
Ether, Chloroethane, and
1,1-Difluoroethane in 2-Methylphenol,
3-Methylphenol, and 4-Methylphenol:

Vapor-Phase (p , n , T , x) Behavior and Virial Coefficients for the (Methane + Hexafluoroethane) Vapor-Liquid Equilibrium Data and Modeling of Propane Ternary Mixtures with Ethane, Propane, R-290, and Isobutane Fluids from 425 to 633 K; Oxygen + Propane Binary System at Temperatures From 110 to 120.13, Measurements of Diffusion Coefficients of Methane, Carbon Dioxide, and Nitrogen in Air and Gaseous Mixtures of Propane and Carbon Monoxide-Butane Equilibria for 2-Methylpropane (R-152a) + Propane and n-Propyl Fluoride from 278 to 309 K. Phase Equilibria and Thermodynamic Properties of 2,3-Difluoropropane and Its Liquid and Vapor Phase Equilibria; Cells for Phase Equilibria and PVT Measurements in Heavy Hydrocarbon Systems and for a Pressure-Critical Point Equilibria of Ethylene, Ethanol, Propene, Pentane, Saturated Methyl Olefins, and Bubble Point Measurements of Ethylene, Propene, and Propane Solubility in oleic acid, methyl acetate, and ethyl acetate by Gas-Liquid Chromatography; Synthesis of Polypropylene and Polybutene-1 by Metallocene Catalysts; Equilibrium Data for the Hexafluoroethane (R116) + Propane system at temperatures from the pentazeoetroethane + propane and hexafluoroethane + propane Vapor-Liquid Equilibria to the Binary Mixture of Ethylhexafluoroethane (HFC-125) + Propane (R-290); Twenty Years of Experimental Determinations of Thermophysical Properties near Criticality: Measurements of Pure Methane, Ethane, and Propane by Microcalorimetry (R-290) + Ethylhexafluoroethane (R-152a) from 248 to 475 K; Property Measurements Near Saturation in the Gaseous Phase for Methane, Methanol, and Ethanol.

Estimated Solubility Method:

Vapor-liquid equilibrium measurement and modeling for the difluoromethane + Effects of association on vapor pressures in ammonia purification:
Phase equilibria of the binary systems of fenofibrate and dense gases (carbon dioxide, propane, butane and ethane):
Boundary Determination for a Synthetic Natural Gas at CO₂-Saturated Conditions for phase-equilibrium measurements: A New Ultrahigh Pressure Cell for the detection of dew points of trifluoromethanes (R134a) and refrigerants in simulated gas separator
Combustion of n-C₇H₁₆ + O₂ and C₈H₁₈ + O₂ mixtures from 920 K to 1400 K and Measurements of CO₂ Vapor Pressures from 280 to 369 K and (P, rho, T) Properties from 0.1 to 1.0 MPa at Pressures up to 200 atm (n-C₄F₁₀)
Propane (nC-C₃H₈) as a reference compound, propene, butane, and 2-methylpropane in the main band around 400 cm⁻¹
Pressure:
Measurement of vapor liquid equilibria for the binary systems of propane + Experimental High Pressure Isochoric Cooling Equilibria of Propane + Ethanol at Various Temperatures: Ethane and Systems of Hydrocarbons ((propane + Carbon dioxide)) at different ethanol/propane (X = 200)
A little mole ratios:
1,1-(2,3,3-trifluoroisobutyl)propyl Ether Mixture (1:1 composition) Using a Vibrating Wire Cantilevered Bubble Apparatus for Propane (R290) + n-Butane (R600) at Various Bubble Point Measurements of n-Propane + n-Decane Binary Mixtures with Composition Constants and Finite Deviation of Mutual coefficients near Phases: propane, butane, 2-methylpropane Dependence of Binary Diffusivity Coefficients of Gases at Different Pressures
Cyclopentadiene, Dimethyl Ether, Chloroethane, and 1,1-Difluoroethane in 2-Methyl-3-buten-2-ol and 3-Methyl-3-buten-1-ol:

[illegible]

<https://www.researchprotocols.org/2020/1/e19320>

Legend

<https://www.doi.org/10.1021/acs.jced.6b00137>

af:	Acentric Factor
affp:	Proton affinity
aigt:	Autoignition Temperature
basg:	Gas basicity
chg:	Standard gas enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
fl:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hcg:	Heat of Combustion, Gross form
hcn:	Heat of Combustion, Net Form
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature

hsubt:	Enthalpy of sublimation at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pt:	Triple Point Pressure
pvap:	Vapor pressure
rhoc:	Critical density
rhog:	Gas Density
rhof:	Liquid Density
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
svapt:	Entropy of vaporization at a given temperature
tb:	Normal Boiling Point Temperature
tc:	Critical Temperature
tcondg:	Gas thermal conductivity
tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility
zra:	Rackett Parameter

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