1-Hexene

Other names:	1-C6H12
	1-N-HEXENE
	BUTYLETHYLENE
	Dialene 6
	HEXENE
	Hex-1-ene
	Hexene-1
	Hexylene
	NSC 74121
	Neodene 6 XHP
	UN 2370
Inchi:	InChI=1S/C6H12/c1-3-5-6-4-2/h3H,1,4-6H2,2H3
InchiKey:	LIKMAJRDDDTEIG-UHFFFAOYSA-N
Formula:	C6H12
SMILES:	C=CCCCC
Mol. weight [g/mol]:	84.16
CAS:	592-41-6

Physical Properties

Property code	Value	Unit	Source
af	0.2850		KDB
affp	805.20	kJ/mol	NIST Webbook
aigt	544.82	K	KDB
ap	295.950	K	KDB
basg	776.30	kJ/mol	NIST Webbook
dm	0.40	debye	KDB
fll	1.20	% in Air	KDB
fpc	255.37	K	KDB
fpo	247.04	K	KDB
gf	87.50	kJ/mol	KDB
gyrad	3.6470		KDB
hcg	4003.75	kJ/mol	KDB
hcn	3739.659	kJ/mol	KDB
hf	-41.70	kJ/mol	KDB
hf	-42.10 ± 1.20	kJ/mol	NIST Webbook
hf	-44.80 ± 1.40	kJ/mol	NIST Webbook
hf	-41.70	kJ/mol	NIST Webbook

hf	-41.40 ± 0.90	kJ/mol	NIST Webbook
hf	-42.10 ± 2.10	kJ/mol	NIST Webbook
hf	-43.00 ± 1.50	kJ/mol	NIST Webbook
hf	-41.50 ± 1.00	kJ/mol	NIST Webbook
hf	-41.50 ± 1.20	kJ/mol	NIST Webbook
hf	-42.09	kJ/mol	NIST Webbook
hf	-44.80 ± 1.00	kJ/mol	NIST Webbook
hfl	-75.40 ± 1.40	kJ/mol	NIST Webbook
hfl	-72.00 ± 0.80	kJ/mol	NIST Webbook
hfl	-72.10 ± 1.20	kJ/mol	NIST Webbook
hfl	-72.30 ± 1.20	kJ/mol	NIST Webbook
hfl	-73.60 ± 1.50	kJ/mol	NIST Webbook
hfl	-72.10 ± 1.00	kJ/mol	NIST Webbook
hfl	-72.70 ± 1.20	kJ/mol	NIST Webbook
hfl	-72.70 ± 2.10	kJ/mol	NIST Webbook
hfl	-75.40 ± 1.00	kJ/mol	NIST Webbook
hfus	10.02	kJ/mol	Joback Method
hvap	30.60	kJ/mol	NIST Webbook
hvap	30.60	kJ/mol	NIST Webbook
hvap	30.60	kJ/mol	NIST Webbook
ie	9.46 ± 0.05	eV	NIST Webbook
ie	9.31	eV	NIST Webbook
ie	9.33	eV	NIST Webbook
ie	9.45 ± 0.02	eV	NIST Webbook
ie	9.65 ± 0.01	eV	NIST Webbook
ie	9.44	eV	NIST Webbook
ie	9.44	eV	NIST Webbook
ie	9.48 ± 0.00	eV	NIST Webbook
ie	9.37 ± 0.02	eV	NIST Webbook
ie	9.46 ± 0.02	eV	NIST Webbook
ie	9.44 ± 0.04	eV	NIST Webbook
log10ws	-3.23		Estimated Solubility Method
log10ws	-3.23		Aqueous Solubility Prediction Method
logp	2.363		Crippen Method
mcvol	91.100	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=1)		KDB
pc	3210.00 ± 30.00	kPa	NIST Webbook
pc	3210.00	kPa	KDB
rhoc	237.33 ± 2.52	kg/m3	NIST Webbook
rinpol	598.00		NIST Webbook
rinpol	594.00		NIST Webbook
rinpol	594.10		NIST Webbook

rinpol	594.30	NIST Webbook
rinpol	594.40	NIST Webbook
rinpol	594.60	NIST Webbook
rinpol	594.80	NIST Webbook
rinpol	593.00	NIST Webbook
rinpol	589.00	NIST Webbook
rinpol	587.00	NIST Webbook
rinpol	589.10	NIST Webbook
rinpol	589.40	NIST Webbook
rinpol	589.70	NIST Webbook
rinpol	590.00	NIST Webbook
rinpol	590.40	NIST Webbook
rinpol	590.00	NIST Webbook
rinpol	583.50	NIST Webbook
rinpol	584.50	NIST Webbook
rinpol	585.20	NIST Webbook
rinpol	586.20	NIST Webbook
rinpol	587.10	NIST Webbook
rinpol	588.20	NIST Webbook
rinpol	582.00	NIST Webbook
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rinpol	596.00	NIST Webbook
rinpol	582.10	NIST Webbook
rinpol	582.50	NIST Webbook
rinpol	582.36	NIST Webbook
rinpol	583.00	NIST Webbook
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rinpol	584.00	NIST Webbook
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rinpol	583.00	NIST Webbook
rinpol	589.00	NIST Webbook
rinpol	589.00	NIST Webbook
rinpol	581.38	NIST Webbook
rinpol	586.90	NIST Webbook
rinpol	584.00	NIST Webbook
rinpol	584.00	NIST Webbook
rinpol	583.00	NIST Webbook
rinpol	589.60	NIST Webbook
rinpol	582.30	NIST Webbook

rinpol	582.00	NIST Webbook
rinpol	589.00	NIST Webbook
rinpol	580.00	NIST Webbook
rinpol	596.00	NIST Webbook
rinpol	584.00	NIST Webbook
rinpol	583.10	NIST Webbook
rinpol	588.90	NIST Webbook
rinpol	588.00	NIST Webbook
rinpol	596.00	NIST Webbook
rinpol	582.00	NIST Webbook
rinpol	583.00	NIST Webbook
rinpol	584.00	NIST Webbook
rinpol	584.00	NIST Webbook
rinpol	593.00	NIST Webbook
rinpol	583.00	NIST Webbook
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rinpol	588.20	NIST Webbook
rinpol	587.90	NIST Webbook
rinpol	587.90	NIST Webbook
rinpol	584.20	NIST Webbook
rinpol	588.40	NIST Webbook
rinpol	588.20	NIST Webbook
rinpol	587.90	NIST Webbook
rinpol	587.90	NIST Webbook
rinpol	584.67	NIST Webbook
rinpol	584.79	NIST Webbook
rinpol	585.00	NIST Webbook
rinpol	585.00	NIST Webbook
rinpol	596.00	NIST Webbook
rinpol	590.00	NIST Webbook
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rinpol	581.50	NIST Webbook
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rinpol	584.70	NIST Webbook
rinpol	585.32	NIST Webbook
rinpol	589.00	NIST Webbook
rinpol	587.00	NIST Webbook
rinpol	584.00	NIST Webbook
rinpol	590.00	NIST Webbook
rinpol	591.00	NIST Webbook
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rinpol	584.00	NIST Webbook
rinpol	589.00	NIST Webbook
rinpol	584.00	NIST Webbook
rinpol	591.00	NIST Webbook
rinpol	583.00	NIST Webbook
rinpol	601.00	NIST Webbook
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rinpol	587.00	NIST Webbook
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rinpol	588.00		NIST Webbook
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rinpol	587.00		NIST Webbook
rinpol	588.96		NIST Webbook
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rinpol	590.00		NIST Webbook
rinpol	589.00		NIST Webbook
rinpol	589.00		NIST Webbook
rinpol	583.00		NIST Webbook
rinpol	592.00		NIST Webbook
ripol	648.00		NIST Webbook
ripol	649.00		NIST Webbook
ripol	648.50		NIST Webbook
ripol	648.70		NIST Webbook
ripol	648.70		NIST Webbook
ripol	648.50		NIST Webbook
ripol	632.00		NIST Webbook
ripol	622.00		NIST Webbook
ripol	674.00		NIST Webbook
ripol	610.00		NIST Webbook
ripol	674.00		NIST Webbook
sl	295.18	J/mol×K	NIST Webbook
tb	336.70 ± 0.50	K	NIST Webbook
tb	338.40 ± 1.50	K	NIST Webbook

tb	336.65 ± 0.50	K	NIST Webbook
tb	337.15 ± 3.00	K	NIST Webbook
tb	336.64 ± 0.50	K	NIST Webbook
tb	336.40 ± 0.70	K	NIST Webbook
tb	336.60 ± 0.30	K	NIST Webbook
tb	336.70 ± 0.60	K	NIST Webbook
tb	336.65 ± 0.30	K	NIST Webbook
tb	336.60 ± 0.30	K	NIST Webbook
tb	336.60 ± 0.30	K	NIST Webbook
tb	336.67 ± 0.20	K	NIST Webbook
tb	336.65 ± 0.50	K	NIST Webbook
tb	336.70 ± 0.60	K	NIST Webbook
tb	337.10 ± 1.50	K	NIST Webbook
tb	336.75 ± 0.50	K	NIST Webbook
tb	336.65 ± 1.00	K	NIST Webbook
tb	336.60 ± 0.40	K	NIST Webbook
tb	339.90 ± 1.20	K	NIST Webbook
tb	337.00 ± 0.60	K	NIST Webbook
tb	336.65 ± 0.30	K	NIST Webbook
tb	341.45 ± 0.50	K	NIST Webbook
tb	336.70 ± 0.60	K	NIST Webbook
tb	335.65 ± 3.00	K	NIST Webbook
tb	337.90 ± 1.50	K	NIST Webbook
tb	335.15 ± 0.50	K	NIST Webbook
tb	336.50 ± 0.30	K	NIST Webbook
tb	335.15 ± 1.50	K	NIST Webbook
tb	336.50 ± 0.30	K	NIST Webbook
tb	336.70 ± 2.00	K	NIST Webbook
tb	340.15 ± 2.00	K	NIST Webbook
tb	340.00 ± 2.00	K	NIST Webbook
tb	336.48	K	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
tb	335.23 ± 0.60	K	NIST Webbook
tb	336.63	K	KDB
tb	338.65 ± 2.00	K	NIST Webbook
tb	336.95 ± 1.00	K	NIST Webbook
tb	280.00 ± 3.00	K	NIST Webbook
tb	337.30 ± 0.20	K	NIST Webbook
tb	337.30 ± 0.40	K	NIST Webbook
tb	336.80 ± 1.00	K	NIST Webbook
tb	336.70 ± 0.20	K	NIST Webbook
tb	336.66 ± 0.30	K	NIST Webbook

tb	336.64 ± 0.50	K	NIST Webbook
tb	336.50	K	NIST Webbook
tb	339.00 ± 3.00	K	NIST Webbook
tc	503.98 ± 0.30	K	NIST Webbook
tc	504.00	K	KDB
tc	504.00 ± 0.30	K	NIST Webbook
tf	133.70 ± 2.00	K	NIST Webbook
tf	133.18	K	Aqueous Solubility Prediction Method
tf	133.39	K	KDB
tf	133.15 ± 1.00	K	NIST Webbook
tf	133.25 ± 0.30	K	NIST Webbook
tf	133.28 ± 0.30	K	NIST Webbook
tf	128.15 ± 1.50	K	NIST Webbook
tf	133.11 ± 0.30	K	NIST Webbook
tf	135.15 ± 2.00	K	NIST Webbook
tf	134.00 ± 6.00	K	NIST Webbook
tf	132.15 ± 1.50	K	NIST Webbook
tt	133.39 ± 0.01	K	NIST Webbook
tt	133.39 ± 0.02	K	NIST Webbook
tt	133.38 ± 0.05	K	NIST Webbook
vc	0.355	m3/kmol	KDB
vc	0.355	m3/kmol	NIST Webbook
zc	0.2720120		KDB
zra	0.27		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	199.69	J/mol×K	500.05	Joback Method
cpg	155.65	J/mol×K	361.14	Joback Method
cpg	165.17	J/mol×K	388.92	Joback Method
cpg	174.32	J/mol×K	416.71	Joback Method
cpg	183.12	J/mol×K	444.49	Joback Method
cpg	191.57	J/mol×K	472.27	Joback Method
cpg	145.77	J/mol×K	333.36	Joback Method
cpl	182.77	J/mol×K	298.56	NIST Webbook
cpl	183.30	J/mol×K	298.15	NIST Webbook

dvisc	0.0002360	Pa×s	313.15	Density, Viscosity, and Isobaric Heat Capacity of the Mixture (1-Butanol + 1-Hexene)
dvisc	0.0002570	Pa×s	303.15	Density, Viscosity, and Isobaric Heat Capacity of the Mixture (1-Butanol + 1-Hexene)
dvisc	0.0002800	Pa×s	293.15	Density, Viscosity, and Isobaric Heat Capacity of the Mixture (1-Butanol + 1-Hexene)
hfust	9.35	kJ/mol	133.39	NIST Webbook
hfust	9.35	kJ/mol	133.40	NIST Webbook
hfust	9.35	kJ/mol	133.40	NIST Webbook
hvapt	30.60	kJ/mol	318.50	NIST Webbook
hvapt	30.40	kJ/mol	317.00	NIST Webbook
hvapt	31.00	kJ/mol	313.00	NIST Webbook
hvapt	31.60	kJ/mol	308.00	NIST Webbook
hvapt	28.28	kJ/mol	337.90	KDB
pvap	218.50	kPa	363.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	84.93	kPa	331.01	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa

pvap	24.77	kPa	298.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	30.46	kPa	303.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	19.98	kPa	293.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	12.64	kPa	283.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	7.69	kPa	273.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)

pvap	44.98	kPa	313.15	Vapour-liquid equilibria of binary and ternary mixtures containing 1-butanol, 2,2,4-trimethylpentane and 1-hexene at T = 313.15 K
pvap	89.70	kPa	333.23	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures
pvap	89.55	kPa	333.15	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures
pvap	64.40	kPa	323.19	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures
pvap	64.28	kPa	323.15	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures

pvap	45.00	kPa	313.20	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures
pvap	44.98	kPa	313.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	64.60	kPa	323.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	44.96	kPa	313.15	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures
pvap	30.60	kPa	303.22	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures

pvap	30.54	kPa	303.15	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures	
pvap	20.10	kPa	293.22	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures	
pvap	20.08	kPa	293.15	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures	
pvap	12.80	kPa	283.24	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures	

pvap	12.71	kPa	283.15	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures	
pvap	7.70	kPa	273.32	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures	
pvap	7.72	kPa	273.15	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures	
pvap	4.46	kPa	263.15	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures	
pvap	34.84	kPa	306.31	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	

pvap	45.00	kPa	313.15	Isothermal vapor liquid equilibrium and molar excess Gibbs energies of two ternary systems containing either 1-butanol or 2-butanol + 1-hexene + methylbenzene at 313.15 K	
pvap	44.98	kPa	313.15	Phase equilibrium properties of binary and ternary mixtures containing 2-butanol, 2,2,4-trimethylpentane and 1-hexene at 313.15 K	
pvap	101.30	kPa	336.48	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	97.45	kPa	335.24	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	94.82	kPa	334.38	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	92.54	kPa	333.62	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	

pvap	89.92	kPa	332.74	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	90.44	kPa	333.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	123.79	kPa	343.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	165.99	kPa	353.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	24.93	kPa	298.07	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa

pvap	27.41	kPa	300.32	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	30.08	kPa	302.55	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	32.46	kPa	304.54	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	72.44	kPa	326.29	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	37.48	kPa	308.20	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	39.96	kPa	309.84	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	

pvap	42.53	kPa	311.51	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	44.96	kPa	312.98	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	47.42	kPa	314.38	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	49.92	kPa	315.79	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	52.53	kPa	317.17	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	54.98	kPa	318.43	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	

pvap	57.39	kPa	319.62	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	59.94	kPa	320.84	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	62.51	kPa	322.02	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	64.97	kPa	323.16	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	67.45	kPa	324.21	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	69.88	kPa	325.25	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	

pvap	87.33	kPa	331.86	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	75.04	kPa	327.32	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	77.45	kPa	328.25	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	79.98	kPa	329.21	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	82.42	kPa	330.11	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa	
pvap	4.50	kPa	263.45	Isothermal (vapor + liquid) equilibria and excess enthalpy data of {1-hexene + methyl butyl ether (MBE)} and {1-hexene + methyl tert-butyl ether (MTBE)} binary systems at several temperatures	

rfi	1.38380	293.15	Vapor Liquid Equilibrium Data for 1-Methyl-2-Pyrrolidone + (1-Butanol or 1-Hexene or Water) Binary Mixtures
rfi	1.38502	298.15	KDB
rfi	1.38490	298.15	Phase equilibria on four binary systems containing 3-methylthiophene
rfi	1.38510	298.15	Vapor-Liquid Equilibrium for Binary System of Thiophene + n-Hexane at (338.15 and 323.15) K and Thiophene + 1-Hexene at (333.15 and 323.15) K
rfi	1.38530	298.15	Solubility of a-Carotene in Binary Solvents Formed by Some Hydrocarbons with 2,5,8-Trioxanonane, 2-Propanone, and Cyclohexanone
rfi	1.38520	298.15	Vapor-Liquid Equilibrium for Binary System of Diethyl Sulfide + n-Hexane at (338.15 and 323.15) K and Diethyl Sulfide + 1-Hexene at (333.15 and 323.15) K
rfi	1.38790	293.15	Excess Volume of the 1-Propanol + 1-Alkene Systems in Terms of an Equation of State with Association
rfi	1.38510	298.15	Vapor Liquid Equilibrium for Methoxymethane + Thiophene, + Diethylsulfide, + 2-Methyl-2-propanethiol and 1-Hexene, + 1-Propanethiol

rhol	668.76	kg/m3	298.15	Excess Molar Enthalpies of Dipropyl Ether + Dibutyl Ether + (1-Hexene or Tetrahydrofuran) at 298.15 K
rhol	668.73	kg/m3	298.15	Excess Enthalpies of Binary Mixtures of 1-Hexene with Some n-Alkanes at 298.15 K
rhol	673.00	kg/m3	293.00	KDB
rhol	668.73	kg/m3	298.15	Excess enthalpies of binary mixtures of 1-hexene with some branched alkanes at the temperature 298.15 K
rhol	668.73	kg/m3	298.15	Excess molar enthalpies of the ternary mixtures (1-hexene + tetrahydrofuran or 2-methyltetrahydrofuran + methyl tert-butyl ether) at the temperature 298.15K.
rhol	673.23	kg/m3	293.15	Isothermal vapour-liquid equilibrium data for binary systems of (CHF3 or C2F6) with (1-hexene or 3-methylpentane)
rhol	670.87	kg/m3	295.15	Isothermal vapour-liquid equilibrium data for binary systems of (CHF3 or C2F6) with (1-hexene or 3-methylpentane)
rhol	668.99	kg/m3	297.15	Isothermal vapour-liquid equilibrium data for binary systems of (CHF3 or C2F6) with (1-hexene or 3-methylpentane)

rhol	668.03	kg/m3	298.15	Isothermal vapour-liquid equilibrium data for binary systems of (CHF3 or C2F6) with (1-hexene or 3-methylpentane)	
rhol	665.00	kg/m3	301.35	Isothermal vapour-liquid equilibrium data for binary systems of (CHF3 or C2F6) with (1-hexene or 3-methylpentane)	
rhol	655.00	kg/m3	313.15	Total Pressure Phase Equilibrium Measurements for the Binary Systems of n-Pentane + Cyclohexane and 1-Hexene + 2-Propanol	
rhol	669.34	kg/m3	298.15	Evaluation of Diethyl Carbonate and Methyl Isobutyl Ketone as Entrainers for the Separation of 1-Hexene and n-Hexane	
sfust	70.07	J/mol×K	133.39	NIST Webbook	
srf	0.02	N/m	298.20	KDB	
tcondl	0.12	W/m×K	301.27	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.11	W/m×K	315.04	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	

tcondl	0.11	W/m×K	315.38	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.11	W/m×K	329.14	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.11	W/m×K	329.53	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.11	W/m×K	329.89	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.11	W/m×K	314.67	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	

tcondl	0.12	W/m×K	301.96	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.13	W/m×K	259.93	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.13	W/m×K	260.19	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.13	W/m×K	260.47	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.12	W/m×K	275.98	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	

tcondl	0.12	W/m×K	276.28	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.12	W/m×K	276.60	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.12	W/m×K	295.84	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.12	W/m×K	296.26	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.12	W/m×K	296.53	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	

tcondl	0.12	W/m×K	301.73	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

Correlations

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)
Coeff. A	1.42313e+01
Coeff. B	-2.91733e+03
Coeff. C	-3.35220e+01
Temperature range (K), min.	242.74
Temperature range (K), max.	360.58

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/T + C*ln(T) + D*T^2
Coeff. A	7.43339e+01
Coeff. B	-6.02031e+03
Coeff. C	-9.06686e+00
Coeff. D	8.22835e-06
Temperature range (K), min.	133.39
Temperature range (K), max.	504.03

Datasets

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid

273.15	100.00	691.9
273.15	1000.00	692.7
273.15	2000.00	693.6
273.15	5000.00	696.4
273.15	10000.00	700.6
273.15	15000.00	704.6
273.15	20000.00	708.5
273.15	30000.00	715.6
273.15	40000.00	722.2
273.15	50000.00	728.2
273.15	60000.00	733.9
273.15	70000.00	739.4
293.15	100.00	673.3
293.15	1000.00	674.3
293.15	2000.00	675.4
293.15	5000.00	678.6
293.15	10000.00	683.5
293.15	15000.00	688.1
293.15	20000.00	692.4
293.15	30000.00	700.4
293.15	40000.00	707.6
293.15	50000.00	714.3
293.15	60000.00	720.5
293.15	70000.00	726.4
313.15	100.00	654.2
313.15	1000.00	655.3
313.15	2000.00	656.6
313.15	5000.00	660.3
313.15	10000.00	666.0
313.15	15000.00	671.2
313.15	20000.00	676.1
313.15	30000.00	685.1
313.15	40000.00	693.1
313.15	50000.00	700.4
313.15	60000.00	707.4
313.15	70000.00	713.5
333.15	100.00	634.7
333.15	1000.00	636.0
333.15	2000.00	637.5
333.15	5000.00	641.9
333.15	10000.00	648.5
333.15	15000.00	654.5
333.15	20000.00	660.1
333.15	30000.00	670.1

333.15	40000.00	679.0
333.15	50000.00	687.0
333.15	60000.00	694.4
333.15	70000.00	701.2

Reference *https://www.doi.org/10.1016/j.jct.2012.07.018*

Temperature, K	Pressure, kPa	Mass density, kg/m3
283.59	100.00	682.2
283.58	500.00	682.3
283.57	1000.00	683.2
283.57	3000.00	685.2
283.57	5000.00	687.2
283.57	10000.00	691.9
283.57	15000.00	696.4
283.57	20000.00	700.6
283.57	25000.00	704.7
283.57	30000.00	708.5
283.57	35000.00	712.4
283.58	40000.00	714.7
283.57	45000.00	719.4
283.58	50000.00	722.4
283.58	55000.00	725.5
283.58	60000.00	728.6
283.58	70000.00	734.4
283.58	80000.00	739.9
283.59	90000.00	745.2
283.59	100000.00	750.1
293.51	100.00	673.1
293.51	500.00	673.5
293.50	1000.00	674.1
293.51	3000.00	676.3
293.51	5000.00	678.4
293.51	10000.00	683.5
293.52	15000.00	688.3
293.51	20000.00	692.8
293.51	25000.00	697.0
293.51	30000.00	701.1
293.51	35000.00	704.9
293.52	40000.00	708.6
293.52	45000.00	712.5
293.52	50000.00	715.6
293.51	55000.00	718.9

293.51	60000.00	722.1
293.51	70000.00	728.2
293.51	80000.00	733.8
293.51	90000.00	739.3
293.51	100000.00	744.4
303.41	100.00	663.5
303.40	500.00	664.1
303.40	1000.00	664.6
303.41	3000.00	667.0
303.41	5000.00	669.3
303.41	10000.00	674.8
303.41	15000.00	679.9
303.41	20000.00	684.7
303.41	25000.00	689.2
303.42	30000.00	693.5
303.42	35000.00	698.2
303.42	40000.00	701.5
303.42	45000.00	705.8
303.42	50000.00	708.8
303.42	55000.00	712.8
303.42	60000.00	715.5
303.42	70000.00	721.8
303.42	80000.00	727.7
303.42	90000.00	733.2
303.42	100000.00	738.5
313.34	100.00	654.1
313.35	500.00	654.2
313.35	1000.00	655.3
313.35	3000.00	657.9
313.35	5000.00	660.3
313.35	10000.00	666.1
313.35	15000.00	671.6
313.34	20000.00	676.6
313.35	25000.00	681.4
313.35	30000.00	685.9
313.35	35000.00	690.2
313.35	40000.00	694.3
313.35	45000.00	698.3
313.35	50000.00	701.9
313.35	55000.00	705.7
313.35	60000.00	709.0
313.36	70000.00	715.9
313.35	80000.00	721.9
313.35	90000.00	727.6

313.35	100000.00	733.2
323.18	100.00	644.5
323.19	500.00	644.9
323.19	1000.00	645.8
323.19	3000.00	648.6
323.19	5000.00	651.3
323.19	10000.00	657.6
323.20	15000.00	663.4
323.20	20000.00	668.8
323.21	25000.00	673.8
323.20	30000.00	678.6
323.20	35000.00	683.4
323.20	40000.00	687.3
323.21	45000.00	691.8
323.19	50000.00	695.2
323.19	55000.00	699.3
323.18	60000.00	702.5
323.20	70000.00	709.4
323.20	80000.00	715.7
323.20	90000.00	721.6
323.20	100000.00	727.2
333.08	500.00	635.3
333.08	1000.00	636.0
333.08	3000.00	639.1
333.08	5000.00	642.0
333.08	10000.00	648.8
333.09	15000.00	655.0
333.09	20000.00	660.8
333.09	25000.00	666.1
333.09	30000.00	671.1
333.09	35000.00	676.4
333.09	40000.00	680.2
333.09	45000.00	685.1
333.09	50000.00	688.5
333.09	55000.00	693.0
333.09	60000.00	696.1
333.09	70000.00	703.3
333.09	80000.00	709.8
333.09	90000.00	715.9
333.09	100000.00	721.7
342.96	500.00	625.6
342.96	1000.00	626.4
342.97	3000.00	629.8
342.97	5000.00	633.0

342.97	10000.00	640.3
342.97	15000.00	647.0
342.97	20000.00	653.2
342.97	25000.00	658.8
342.97	30000.00	664.1
342.97	35000.00	669.6
342.97	40000.00	673.8
342.97	45000.00	678.8
342.97	50000.00	682.3
342.97	55000.00	687.0
342.97	60000.00	690.4
342.97	70000.00	697.6
342.97	80000.00	704.3
342.97	90000.00	710.7
342.97	100000.00	716.6
352.85	500.00	615.7
352.85	1000.00	617.0
352.85	3000.00	620.7
352.85	5000.00	624.2
352.86	10000.00	632.2
352.85	15000.00	639.4
352.86	20000.00	645.7
352.86	25000.00	651.7
352.86	30000.00	657.4
352.86	35000.00	662.8
352.86	40000.00	667.4
352.86	45000.00	672.4
352.86	50000.00	676.6
352.86	55000.00	680.9
352.86	60000.00	684.8
352.86	70000.00	692.4
352.86	80000.00	699.4
352.86	90000.00	705.9
352.86	100000.00	712.0
362.70	500.00	604.1
362.70	1000.00	605.5
362.71	3000.00	609.5
362.71	5000.00	613.3
362.71	10000.00	622.0
362.71	15000.00	629.7
362.71	20000.00	636.7
362.71	25000.00	643.0
362.71	30000.00	648.9
362.71	35000.00	654.7

362.71	40000.00	659.6
362.71	45000.00	664.8
362.71	50000.00	669.0
362.71	55000.00	673.7
362.71	60000.00	677.6
362.71	70000.00	685.4
362.71	80000.00	692.6
362.71	90000.00	699.3
362.70	100000.00	705.7

Reference *https://www.doi.org/10.1021/acs.jced.8b00229*

Pressure, kPa	Temperature, K	Mass density, kg/m3
98.00	298.15	669.71
98.00	303.15	664.87
98.00	312.92	655.77
98.00	325.17	644.12
24510.00	298.15	696.93
24510.00	303.15	690.93
24510.00	326.00	675.1
24510.00	364.73	645.55
24510.00	398.43	618.11
24510.00	423.18	598.39
24510.00	452.77	575.45
24510.00	471.92	560.56
49030.00	298.15	714.95
49030.00	303.15	711.55
49030.00	326.02	694.93
49030.00	364.69	670.17
49030.00	398.87	645.8
49030.00	423.10	630.04
49030.00	453.14	608.12
49030.00	471.73	598.79
98060.00	298.15	744.22
98060.00	303.15	741.4
98060.00	325.99	729.28
98060.00	364.75	706.69
98060.00	398.78	687.13
98060.00	422.90	672.81
98060.00	453.19	656.91
98060.00	471.78	646.27
147100.00	298.15	763.36
147100.00	303.15	761.37

147100.00	326.05	750.05
147100.00	364.83	731.74
147100.00	398.25	715.97
147100.00	422.74	703.54
147100.00	453.28	687.84
147100.00	472.02	680.82
196130.00	298.15	778.91
196130.00	303.15	776.19
196130.00	326.12	767.98
196130.00	364.63	751.74
196130.00	398.37	736.05
196130.00	422.71	726.21
196130.00	453.14	712.63
196130.00	471.55	704.21
245160.00	298.15	793.17
245160.00	303.15	791.19
245160.00	326.15	783.2
245160.00	364.25	767.68
245160.00	398.35	753.74
245160.00	422.37	743.17
245160.00	453.52	732.58
245160.00	471.64	725.42

Reference *https://www.doi.org/10.1021/je401015e*

Sources

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Measurements of activity coefficients at infinite dilution for organic solutes and water in the ionic liquid [illegible]	https://www.doi.org/10.1016/j.jct.2013.07.004
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Thermodynamics and activity coefficients at infinite dilution [illegible]	https://www.doi.org/10.1016/j.jct.2011.06.007
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Legend

af:	Acentric Factor
affp:	Proton affinity
aigt:	Autoignition Temperature
ap:	Aniline Point
basg:	Gas basicity
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
fll:	Lower Flammability Limit
fpc:	Flash Point (Closed Cup Method)
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hcg:	Heat of Combustion, Gross form
hcn:	Heat of Combustion, Net Form
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sl:	Liquid phase molar entropy at standard conditions
srf:	Surface Tension
tb:	Normal Boiling Point Temperature

tc:	Critical Temperature
tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility
zra:	Rackett Parameter