

2-Butanone, 3-methyl-

Other names:	2-Acetylpropane 2-Methylbutan-3-one 3-METHYL-2-BUTANONE 3-Methyl-2-butanoate 3-Methylbutan-2-one 3-methylbutanone Isopropyl methyl ketone Ketone, isopropyl methyl METHYLBUTANONE MIPK Methyl butanone-2 Methyl isopropyl ketone NSC 9379 UN 2397 iso-C3H7COCH3
Inchi:	InChI=1S/C5H10O/c1-4(2)5(3)6/h4H,1-3H3
InchiKey:	SYBYTAAJFKOIEJ-UHFFFAOYSA-N
Formula:	C5H10O
SMILES:	CC(=O)C(C)C
Mol. weight [g/mol]:	86.13
CAS:	563-80-4

Physical Properties

Property code	Value	Unit	Source
af	0.3310		KDB
affp	836.30	kJ/mol	NIST Webbook
basg	804.40	kJ/mol	NIST Webbook
chl	-3097.20 ± 0.80	kJ/mol	NIST Webbook
dm	2.80	debye	KDB
gf	-140.14	kJ/mol	Joback Method
hf	-262.57 ± 0.87	kJ/mol	NIST Webbook
hfl	-299.47 ± 0.86	kJ/mol	NIST Webbook
hfus	6.78	kJ/mol	Joback Method
hvap	36.90	kJ/mol	NIST Webbook
hvap	36.80	kJ/mol	NIST Webbook
hvap	36.87	kJ/mol	NIST Webbook
hvap	36.81	kJ/mol	NIST Webbook

ie	9.31 ± 0.02	eV	NIST Webbook
ie	9.30 ± 0.04	eV	NIST Webbook
ie	9.36	eV	NIST Webbook
ie	9.30 ± 0.01	eV	NIST Webbook
ie	9.30 ± 0.02	eV	NIST Webbook
ie	9.30 ± 0.01	eV	NIST Webbook
ie	9.30 ± 0.01	eV	NIST Webbook
ie	9.32 ± 0.02	eV	NIST Webbook
log10ws	-0.12		Aqueous Solubility Prediction Method
log10ws	-0.12		Estimated Solubility Method
logp	1.231		Crippen Method
mccvol	82.880	ml/mol	McGowan Method
pc	3850.00	kPa	KDB
pc	3800.00 ± 20.00	kPa	NIST Webbook
pc	3850.00 ± 48.30	kPa	NIST Webbook
rhoc	278.21 ± 24.98	kg/m3	NIST Webbook
rinpol	657.00		NIST Webbook
rinpol	646.00		NIST Webbook
rinpol	641.00		NIST Webbook
rinpol	640.90		NIST Webbook
rinpol	650.00		NIST Webbook
rinpol	651.00		NIST Webbook
rinpol	647.00		NIST Webbook
rinpol	650.00		NIST Webbook
rinpol	642.00		NIST Webbook
rinpol	636.00		NIST Webbook
rinpol	643.00		NIST Webbook
rinpol	635.00		NIST Webbook
rinpol	659.00		NIST Webbook
rinpol	640.00		NIST Webbook
rinpol	673.00		NIST Webbook
rinpol	658.00		NIST Webbook
rinpol	642.00		NIST Webbook
rinpol	640.90		NIST Webbook
rinpol	642.78		NIST Webbook
rinpol	639.36		NIST Webbook
rinpol	639.89		NIST Webbook
rinpol	640.49		NIST Webbook
rinpol	641.53		NIST Webbook
rinpol	650.00		NIST Webbook
rinpol	640.00		NIST Webbook
rinpol	640.00		NIST Webbook
rinpol	642.00		NIST Webbook

rinpol	646.00	NIST Webbook
rinpol	627.00	NIST Webbook
rinpol	650.00	NIST Webbook
rinpol	647.20	NIST Webbook
rinpol	636.00	NIST Webbook
rinpol	673.00	NIST Webbook
rinpol	640.00	NIST Webbook
rinpol	625.00	NIST Webbook
rinpol	641.00	NIST Webbook
rinpol	641.00	NIST Webbook
rinpol	666.10	NIST Webbook
rinpol	628.00	NIST Webbook
rinpol	638.00	NIST Webbook
rinpol	659.00	NIST Webbook
rinpol	654.00	NIST Webbook
rinpol	628.00	NIST Webbook
rinpol	639.00	NIST Webbook
rinpol	637.00	NIST Webbook
rinpol	658.00	NIST Webbook
rinpol	641.00	NIST Webbook
rinpol	653.00	NIST Webbook
rinpol	640.00	NIST Webbook
rinpol	640.00	NIST Webbook
rinpol	641.00	NIST Webbook
rinpol	642.00	NIST Webbook
rinpol	641.53	NIST Webbook
ripol	965.00	NIST Webbook
ripol	954.40	NIST Webbook
ripol	959.60	NIST Webbook
ripol	943.20	NIST Webbook
ripol	929.00	NIST Webbook
ripol	936.00	NIST Webbook
ripol	929.00	NIST Webbook
ripol	929.00	NIST Webbook
ripol	918.00	NIST Webbook
ripol	929.00	NIST Webbook
ripol	927.00	NIST Webbook
ripol	989.00	NIST Webbook
ripol	956.00	NIST Webbook
ripol	929.00	NIST Webbook
ripol	929.00	NIST Webbook
ripol	970.00	NIST Webbook
ripol	949.00	NIST Webbook
ripol	936.00	NIST Webbook

ripol	918.00		NIST Webbook
ripol	929.00		NIST Webbook
ripol	965.00		NIST Webbook
ripol	949.40		NIST Webbook
ripol	925.00		NIST Webbook
sl	268.50	J/mol×K	NIST Webbook
tb	367.65 ± 2.00	K	NIST Webbook
tb	366.65 ± 1.00	K	NIST Webbook
tb	366.65 ± 1.00	K	NIST Webbook
tb	366.65 ± 1.00	K	NIST Webbook
tb	367.65 ± 2.00	K	NIST Webbook
tb	365.55 ± 0.30	K	NIST Webbook
tb	366.65 ± 1.00	K	NIST Webbook
tb	366.15 ± 1.00	K	NIST Webbook
tb	367.65 ± 2.00	K	NIST Webbook
tb	367.15 ± 1.00	K	NIST Webbook
tb	368.30 ± 2.00	K	NIST Webbook
tb	367.48	K	KDB
tb	368.65 ± 1.00	K	NIST Webbook
tb	366.65 ± 1.00	K	NIST Webbook
tb	366.70 ± 0.50	K	NIST Webbook
tb	365.15 ± 2.00	K	NIST Webbook
tb	368.15 ± 2.00	K	NIST Webbook
tb	366.65 ± 1.00	K	NIST Webbook
tb	366.65 ± 1.00	K	NIST Webbook
tb	365.65 ± 5.00	K	NIST Webbook
tb	366.65 ± 2.00	K	NIST Webbook
tb	366.15 ± 1.00	K	NIST Webbook
tb	367.30 ± 1.00	K	NIST Webbook
tb	365.15 ± 5.00	K	NIST Webbook
tb	367.41 ± 0.50	K	NIST Webbook
tb	368.15 ± 2.00	K	NIST Webbook
tb	366.65 ± 1.00	K	NIST Webbook
tb	365.65 ± 2.00	K	NIST Webbook
tb	368.55 ± 2.00	K	NIST Webbook
tb	367.35 ± 0.50	K	NIST Webbook
tb	366.15 ± 2.00	K	NIST Webbook
tb	367.90 ± 0.50	K	NIST Webbook
tb	367.65 ± 1.00	K	NIST Webbook
tb	367.35 ± 0.50	K	NIST Webbook
tb	367.70	K	NIST Webbook
tb	367.40	K	NIST Webbook
tb	389.50 ± 0.30	K	NIST Webbook
tb	367.65 ± 1.00	K	NIST Webbook

tb	367.15 ± 1.00	K	NIST Webbook
tb	368.60 ± 0.50	K	NIST Webbook
tb	368.30 ± 0.60	K	NIST Webbook
tb	368.00 ± 0.40	K	NIST Webbook
tc	553.40 ± 0.83	K	NIST Webbook
tc	553.40	K	NIST Webbook
tc	553.10 ± 0.40	K	NIST Webbook
tc	553.40	K	KDB
tf	181.00	K	KDB
tf	178.75 ± 0.40	K	NIST Webbook
tf	181.15 ± 0.60	K	NIST Webbook
tf	180.78	K	Aqueous Solubility Prediction Method
tt	180.01 ± 0.06	K	NIST Webbook
vc	0.310	m ³ /kmol	KDB
zc	0.2593860		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	172.09	J/mol×K	473.15	NIST Webbook
cpg	166.77	J/mol×K	453.15	NIST Webbook
cpg	161.25	J/mol×K	433.15	NIST Webbook
cpg	154.26	J/mol×K	408.15	NIST Webbook
cpg	146.82	J/mol×K	383.15	NIST Webbook
cpg	139.58	J/mol×K	358.15	NIST Webbook
cpl	179.90	J/mol×K	298.15	NIST Webbook
cpl	180.00	J/mol×K	298.15	NIST Webbook
dvisc	0.0005129	Pa×s	305.17	Joback Method
dvisc	0.0012505	Pa×s	243.10	Joback Method
dvisc	0.0002843	Pa×s	367.23	Joback Method
dvisc	0.0023744	Pa×s	212.07	Joback Method
dvisc	0.0056166	Pa×s	181.04	Joback Method
dvisc	0.0003716	Pa×s	336.20	Joback Method
dvisc	0.0007615	Pa×s	274.13	Joback Method
hfust	9.34	kJ/mol	180.00	NIST Webbook
hfust	9.34	kJ/mol	180.00	NIST Webbook
hfust	9.34	kJ/mol	180.01	NIST Webbook
hvapt	35.50	kJ/mol	340.00	NIST Webbook
hvapt	32.30 ± 0.10	kJ/mol	367.00	NIST Webbook
hvapt	32.35	kJ/mol	367.40	NIST Webbook

hvapt	32.60	kJ/mol	452.50	NIST Webbook
hvapt	33.80	kJ/mol	389.00	NIST Webbook
hvapt	35.00 ± 0.10	kJ/mol	327.00	NIST Webbook
hvapt	35.00	kJ/mol	352.50	NIST Webbook
hvapt	33.80 ± 0.10	kJ/mol	346.00	NIST Webbook
rfi	1.38620		298.15	Vapor-Liquid Equilibria in the Binary and Ternary Systems Composed of 2-Methylpentane, 3-Methyl-2-butanone and 3-Methyl-2-butanol
rfi	1.38620		298.15	Isothermal vapour liquid equilibria in the binary and ternary systems composed of 2-propanol, 3-methyl-2-butanone and 2,2,4-trimethylpentane
rhoI	798.51	kg/m3	298.15	Thermal and Volumetric Properties of Some C5 and C6 Alkanones at Infinite Dilution in Water
rhoI	803.00	kg/m3	293.00	KDB
rhoI	808.30	kg/m3	288.15	Thermal and Volumetric Properties of Some C5 and C6 Alkanones at Infinite Dilution in Water
rhoI	800.63	kg/m3	298.15	Liquid-liquid equilibria for the pseudo-ternary system {aqueous sulfuric acid solution + methyl ethyl ketone or methyl isopropyl ketone + phosphonium-based ionic liquids} at 298.15 K and atmospheric pressure

rhoI	799.55	kg/m3	298.15	Vapour-liquid equilibria in binary and ternary systems composed of 2,3-dimethylbutane, diisopropyl ether, and 3-methyl-2-butanone at 313.15, 323.15 and 313.15 K
rhoI	788.60	kg/m3	308.15	Thermal and Volumetric Properties of Some C5 and C6 Alkanones at Infinite Dilution in Water
rhoI	778.62	kg/m3	318.15	Thermal and Volumetric Properties of Some C5 and C6 Alkanones at Infinite Dilution in Water
sfust	51.90	J/mol×K	180.01	NIST Webbook

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.42556e+01
Coeff. B	-2.91500e+03
Coeff. C	-6.45290e+01
Temperature range (K), min.	273.22
Temperature range (K), max.	390.44

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C \cdot \ln(T) + D \cdot T^2$
Coeff. A	2.01851e+02
Coeff. B	-1.16914e+04
Coeff. C	-2.86327e+01
Coeff. D	2.74487e-05
Temperature range (K), min.	181.15
Temperature range (K), max.	553.00

Sources

KDB:

<https://www.chemic.org/files/research/kdb/mol/mol1195.mol>

Vapor-Liquid Equilibria in the Binary and Ternary Systems Composed of 2-Methyl-2-butanol, 3-Methyl-2-butanone and 3-Methyl-2-butanol: McGowan Method:

<https://www.doi.org/10.1021/je050062a>

<http://pubs.acs.org/doi/abs/10.1021/ci990307l>

<http://link.springer.com/article/10.1007/BF02311772>

KDB Vapor Pressure Data:

<https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=1195>

Estimated Solubility Method:

http://pubs.acs.org/doi/suppl/10.1021/ci034243x/suppl_file/ci034243xsi20040112_053635.txt

Ternary liquid-liquid equilibria for methyl isopropyl ketone + (resorcinol or phenol) + water system have been determined from aqueous solutions by the COSMO-SAC model and experimental properties (enthalpy).

Isothermal vapour liquid equilibria in the binary and ternary systems composed of 2-propanol, 3-methyl-2-butanone and 5-(2,4-dimethylpentan-3-yl)-2-thiofuranol.

Experimental result and data correlation of liquid-liquid equilibrium between methyl isopropyl ketone and ternary mixtures composed of at 333.15 K and 0.1 MPa for 2-propanol and other, Aqueous methanol measurement critical point extrapolation isopropanol dilution for differential heats and ketones in binary liquid phase experimental data and correlation with figure Liquid Equilibria for methyl isopropyl ketone Properties of some organic solvents and infinite dilution water:

<https://www.doi.org/10.1016/j.fluid.2016.08.040>

<https://www.doi.org/10.1016/j.fluid.2017.08.007>

<https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=1195>

<https://www.doi.org/10.1016/j.fluid.2007.10.016>

https://en.wikipedia.org/wiki/Joback_method

<https://www.doi.org/10.1016/j.ijct.2018.08.041>

<https://www.doi.org/10.1016/j.fluid.2013.01.020>

<https://www.doi.org/10.1021/acs.jced.9b00726>

<https://www.doi.org/10.1016/j.fluid.2015.09.003>

<https://www.doi.org/10.1021/acs.jced.5b00895>

<https://www.doi.org/10.1021/acs.jced.7b00035>

<http://webbook.nist.gov/cgi/cbook.cgi?ID=C563804&Units=SI>

<https://www.doi.org/10.1016/j.fluid.2016.08.034>

<https://www.sciencedirect.com/book/9780128029992/the-vaws-handbook-of-vapor-pressure>

Determination and modeling of liquid-liquid equilibrium for ternary mixtures of methoxypropyl ketone, Pressureomers and water: Aqueous Solubility Prediction Method:

<http://onschallenge.wikispaces.com/file/view/AqueousDataset002.xlsx/351826032/AqueousDataset002.xlsx>

Extraction of o-, m- and p-cresol from aqueous solution with methyl isopropyl ketone, ethyl acetate, hexan-2-one, and the ternary azeotropic systems of (water–methyl isopropyl ketone–methyl isopropyl ketone) and (water–methyl isopropyl ketone–ethyl acetate) at 101.3 kPa and atmospheric pressure: 198–15 K.

<https://www.doi.org/10.1016/j.jct.2017.07.033>

<https://www.doi.org/10.1016/j.jct.2003.11.011>

<https://www.doi.org/10.1016/j.fluid.2013.07.054>

Legend

af: Acentric Factor

affp: Proton affinity

basq: Gas basicity

chl: Standard liquid enthalpy of combustion

cpg: Ideal gas heat capacity

cpl: Liquid phase heat capacity

dm: Dipole Moment

dvisc: Dynamic viscosity

gf:	Standard Gibbs free energy of formation
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhof:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sl:	Liquid phase molar entropy at standard conditions
tb:	Normal Boiling Point Temperature
tc:	Critical Temperature
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility

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<https://www.cheméo.com/cid/21-446-3/2-Butanone-3-methyl.pdf>

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