

1,3-Propanediol

Other names:	1,3-Dihydroxypropane 1,3-Propylene glycol 1,3-Propylenediol 2-(Hydroxymethyl)ethanol 2-DEOXYGLYCEROL BETA-PROPYLENE GLYCOL NSC 65426 PG Polypropylene glycol 425 Propane-1,3-diol Propanediol-(1,3) Trimethylene glycol propan-1,3-diol «beta»-Propylene glycol «omega»-Propanediol Â«betaÂ»-Propylene glycol Â«omegaÂ»-Propanediol
Inchi:	InChI=1S/C3H8O2/c4-2-1-3-5/h4-5H,1-3H2
InchiKey:	YPFDHNVEDLHUCE-UHFFFAOYSA-N
Formula:	C3H8O2
SMILES:	OCCCO
Mol. weight [g/mol]:	76.09
CAS:	504-63-2

Physical Properties

Property code	Value	Unit	Source
affp	876.20	kJ/mol	NIST Webbook
affp	857.60 ± 0.50	kJ/mol	NIST Webbook
affp	850.40	kJ/mol	NIST Webbook
affp	837.90	kJ/mol	NIST Webbook
basg	820.00	kJ/mol	NIST Webbook
basg	827.30 ± 0.20	kJ/mol	NIST Webbook
basg	808.00	kJ/mol	NIST Webbook
basg	825.90	kJ/mol	NIST Webbook
chl	-1843.00 ± 5.10	kJ/mol	NIST Webbook
chl	-1859.00 ± 2.30	kJ/mol	NIST Webbook
dm	3.70	debye	KDB

gf	-299.26	kJ/mol	Joback Method
hf	-392.00 ± 3.00	kJ/mol	NIST Webbook
hf	-409.10	kJ/mol	KDB
hf	-408.40 ± 5.10	kJ/mol	NIST Webbook
hfl	-480.80 ± 5.10	kJ/mol	NIST Webbook
hfl	-465.00 ± 3.00	kJ/mol	NIST Webbook
hfus	11.70	kJ/mol	Joback Method
hvap	55.63	kJ/mol	Joback Method
log10ws	0.39		Crippen Method
logp	-0.639		Crippen Method
mcvol	64.870	ml/mol	McGowan Method
pc	8950.00	kPa	KDB
rinpol	820.00		NIST Webbook
rinpol	793.00		NIST Webbook
rinpol	793.00		NIST Webbook
rinpol	820.00		NIST Webbook
rinpol	814.00		NIST Webbook
rinpol	812.00		NIST Webbook
rinpol	781.00		NIST Webbook
ripol	1820.00		NIST Webbook
ripol	1820.00		NIST Webbook
ripol	1790.00		NIST Webbook
ripol	1789.00		NIST Webbook
ripol	1770.00		NIST Webbook
ripol	1747.00		NIST Webbook
ripol	1747.00		NIST Webbook
ripol	1789.00		NIST Webbook
ripol	1799.00		NIST Webbook
tb	487.60	K	KDB
tb	487.43	K	Vapor-liquid equilibrium data of binary mixtures of 1-hexanol, 1-heptanol, 1-nonanol and 1,3-propanediol at P = 101.3 kPa using differential scanning calorimetry (DSC)
tc	721.00	K	Critical temperatures and pressures of straight-chain alkanediols (C3 to C12)
tc	721.00	K	Vapor-liquid critical point measurements of fifteen compounds by the pulse-heating method
tc	724.00	K	KDB
tf	246.50 ± 0.60	K	NIST Webbook
tf	241.15 ± 0.70	K	NIST Webbook
tf	246.40	K	KDB

tf	332.00 ± 2.00	K	NIST Webbook
tt	245.50 ± 0.10	K	NIST Webbook
vc	0.241	m3/kmol	Joback Method

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	164.16	J/mol×K	611.56	Joback Method
cpg	150.54	J/mol×K	531.98	Joback Method
cpg	145.64	J/mol×K	505.45	Joback Method
cpg	140.55	J/mol×K	478.93	Joback Method
cpg	135.27	J/mol×K	452.40	Joback Method
cpg	159.79	J/mol×K	585.04	Joback Method
cpg	155.25	J/mol×K	558.51	Joback Method
cpl	176.26	J/mol×K	299.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	178.42	J/mol×K	303.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	179.15	J/mol×K	305.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	179.87	J/mol×K	306.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	180.59	J/mol×K	308.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	181.32	J/mol×K	309.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	182.05	J/mol×K	311.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	194.59	J/mol×K	336.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	183.51	J/mol×K	314.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	184.24	J/mol×K	315.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	184.97	J/mol×K	317.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	185.70	J/mol×K	318.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	186.44	J/mol×K	320.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	187.17	J/mol×K	321.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	187.91	J/mol×K	323.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	188.65	J/mol×K	324.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	189.38	J/mol×K	326.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	190.12	J/mol×K	327.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	190.87	J/mol×K	329.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	191.61	J/mol×K	330.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	192.35	J/mol×K	332.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	193.10	J/mol×K	333.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	193.84	J/mol×K	335.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	173.40	J/mol×K	293.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	177.70	J/mol×K	302.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	196.09	J/mol×K	339.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	196.84	J/mol×K	341.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	197.59	J/mol×K	342.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	198.34	J/mol×K	344.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	199.10	J/mol×K	345.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	199.85	J/mol×K	347.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	200.61	J/mol×K	348.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	201.37	J/mol×K	350.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	202.13	J/mol×K	351.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	176.98	J/mol×K	300.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	175.78	J/mol×K	298.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	175.54	J/mol×K	297.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	174.83	J/mol×K	296.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	174.11	J/mol×K	294.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	202.89	J/mol×K	353.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	182.78	J/mol×K	312.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	195.34	J/mol×K	338.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
dvisc	0.0421146	Pa×s	279.74	Joback Method
dvisc	0.0086422	Pa×s	314.27	Joback Method
dvisc	0.0024266	Pa×s	348.80	Joback Method
dvisc	0.0008566	Pa×s	383.34	Joback Method
dvisc	0.0003591	Pa×s	417.87	Joback Method
dvisc	0.0001719	Pa×s	452.40	Joback Method
dvisc	0.3206001	Pa×s	245.21	Joback Method
hfust	11.40	kJ/mol	249.00	NIST Webbook
hvapt	57.86	kJ/mol	273.00	NIST Webbook
hvapt	73.00 ± 2.00	kJ/mol	383.00	NIST Webbook
hvapt	57.20	kJ/mol	390.00	NIST Webbook
hvapt	69.80	kJ/mol	298.15	Vaporization Enthalpies of the r,o-Alkanediols by Correlation Gas Chromatography
hvapt	63.30	kJ/mol	408.00	NIST Webbook
hvapt	60.40	kJ/mol	460.50	NIST Webbook
pvap	23.46	kPa	441.95	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling

pvap	33.22	kPa	451.65	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	36.69	kPa	454.65	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	40.04	kPa	457.49	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	43.37	kPa	459.85	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling

pvap	46.67	kPa	461.95	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	49.97	kPa	463.95	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	53.24	kPa	465.45	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	6.67	kPa	414.20	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling

pvap	13.33	kPa	427.55	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	33.33	kPa	453.15	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	39.99	kPa	457.45	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	46.66	kPa	461.95	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling

pvap	101.30	kPa	487.43	Vapor-liquid equilibrium data of binary mixtures of 1-hexanol, 1-heptanol, 1-nonanol and 1,3-propanediol at P = 101.3 kPa using differential scanning calorimetry (DSC)
pvap	1.86e-03	kPa	293.50	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols
pvap	4.47e-03	kPa	303.20	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols
pvap	7.88e-03	kPa	309.30	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols
pvap	9.97e-03	kPa	312.20	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols
pvap	0.01	kPa	315.30	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols
pvap	0.02	kPa	318.40	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols
pvap	0.02	kPa	321.30	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols
pvap	0.03	kPa	324.30	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols

pvap	30.22	kPa	448.65	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	0.04	kPa	330.30	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols
pvap	0.06	kPa	333.50	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols
pvap	0.07	kPa	336.40	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols
pvap	0.08	kPa	339.40	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols
pvap	0.11	kPa	342.30	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols
pvap	0.01	kPa	313.20	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	0.03	kPa	323.26	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	0.06	kPa	333.23	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol

pvap	0.12	kPa	343.16	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	0.22	kPa	351.33	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	0.43	kPa	361.61	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	0.46	kPa	362.97	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	0.79	kPa	371.65	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	1.40	kPa	381.70	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	2.38	kPa	391.70	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	2.37	kPa	391.73	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	3.88	kPa	401.64	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol

pvap	6.21	kPa	411.71	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	9.63	kPa	421.69	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	14.62	kPa	431.74	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	26.66	kPa	445.30	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	31.44	kPa	451.78	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	44.81	kPa	461.85	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol
pvap	19.99	kPa	438.05	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling

pvap	16.75	kPa	433.90	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	13.47	kPa	427.60	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	9.93	kPa	420.80	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	6.65	kPa	414.20	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	0.14	kPa	346.40	Benchmark thermodynamic properties of 1,3-propanediol: Comprehensive experimental and theoretical study

pvap	0.12	kPa	344.30	Benchmark thermodynamic properties of 1,3-propanediol: Comprehensive experimental and theoretical study	
pvap	0.08	kPa	338.70	Benchmark thermodynamic properties of 1,3-propanediol: Comprehensive experimental and theoretical study	
pvap	5.84e-03	kPa	306.30	Benchmark thermodynamic properties of 1,3-propanediol: Comprehensive experimental and theoretical study	
pvap	3.46e-03	kPa	300.40	Benchmark thermodynamic properties of 1,3-propanediol: Comprehensive experimental and theoretical study	
pvap	2.39e-03	kPa	296.40	Benchmark thermodynamic properties of 1,3-propanediol: Comprehensive experimental and theoretical study	
pvap	1.67e-03	kPa	292.50	Benchmark thermodynamic properties of 1,3-propanediol: Comprehensive experimental and theoretical study	
pvap	21.63	kPa	441.73	Vapor-Liquid Equilibria of Glycerol, 1,3-Propanediol, Glycerol + Water, and Glycerol + 1,3-Propanediol	
pvap	0.04	kPa	327.30	Vapor Pressures and Enthalpies of Vaporization of a Series of the 1,3-Alkanediols	

rfi	1.44089	288.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
rfi	1.43800	298.15	Study of the Acoustic and Thermodynamic Properties of 1,2- and 1,3-Propanediol by Means of High-Pressure Speed of Sound Measurements at Temperatures from (293 to 318) K and Pressures up to 101 MPa
rfi	1.43860	298.15	Densities, Dynamic Viscosities, Speeds of Sound, and Relative Permittivities for Water + Alkanediols (Propane-1,2- and -1,3-diol and Butane-1,2-, -1,3-, -1,4-, and -2,3-Diol) at Different Temperatures
rfi	1.43930	293.15	Vapor-liquid equilibria, density and sound velocity measurements of (water or methanol or ethanol + 1,3-propanediol) binary systems at different temperatures

rfi	1.43099	323.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
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rfi	1.43244	318.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
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rfi	1.43387	313.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
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rfi	1.43526	308.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
rfi	1.43665	303.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
rfi	1.43805	298.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination

rfi	1.43947		293.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
rhoI	1052.80	kg/m3	293.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination
rhoI	1033.84	kg/m3	323.15	Measurement and modeling of volumetric properties and speeds of sound of several mixtures of alcohol liquids containing 1-propanol and 2-propanol at T= (298.15 - 323.15) K and ambient pressure
rhoI	1042.70	kg/m3	308.15	Structural and interactional studies of homologous series of a,x-alkanediols in N,N-dimethylformamide
rhoI	1042.70	kg/m3	308.15	Molecular interactions of a,x-alkanediols in pyrrolidin-2-one: Thermophysical and spectroscopic measurements

rhoI	1055.96	kg/m3	288.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhoI	1052.87	kg/m3	293.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhoI	1049.76	kg/m3	298.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling

rhoI	1046.64	kg/m3	303.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhoI	1043.50	kg/m3	308.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhoI	1040.35	kg/m3	313.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling

rhoI	1037.18	kg/m3	318.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhoI	1033.98	kg/m3	323.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhoI	1030.77	kg/m3	328.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling

rhoI	1027.53	kg/m3	333.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhoI	1049.60	kg/m3	298.15	Investigation on some thermophysical properties of poly(ethylene glycol) binary mixtures at different temperatures
rhoI	1046.20	kg/m3	303.15	Investigation on some thermophysical properties of poly(ethylene glycol) binary mixtures at different temperatures
rhoI	1043.10	kg/m3	308.15	Investigation on some thermophysical properties of poly(ethylene glycol) binary mixtures at different temperatures
rhoI	1049.68	kg/m3	298.15	Isobaric (vapor + liquid) equilibria for the ternary system of (ethanol + water + 1,3-propanediol) and three constituent binary systems at P = 101.3 kPa
rhoI	1053.03	kg/m3	293.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures

rhoI	1049.90	kg/m3	298.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhoI	1046.77	kg/m3	303.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhoI	1043.63	kg/m3	308.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhoI	1040.49	kg/m3	313.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhoI	1037.33	kg/m3	318.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhoI	1034.16	kg/m3	323.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhoI	1046.56	kg/m3	303.15	Densities, ultrasonic speeds, excess and partial molar properties of binary mixtures of 2-pyrrolidone with isomeric propanediols at temperatures from 303.15 K to 323.15 K

rhoI	1043.43	kg/m3	308.15	Densities, ultrasonic speeds, excess and partial molar properties of binary mixtures of 2-pyrrolidone with isomeric propanediols at temperatures from 303.15 K to 323.15 K
rhoI	1040.28	kg/m3	313.15	Densities, ultrasonic speeds, excess and partial molar properties of binary mixtures of 2-pyrrolidone with isomeric propanediols at temperatures from 303.15 K to 323.15 K
rhoI	1037.11	kg/m3	318.15	Densities, ultrasonic speeds, excess and partial molar properties of binary mixtures of 2-pyrrolidone with isomeric propanediols at temperatures from 303.15 K to 323.15 K
rhoI	1033.92	kg/m3	323.15	Densities, ultrasonic speeds, excess and partial molar properties of binary mixtures of 2-pyrrolidone with isomeric propanediols at temperatures from 303.15 K to 323.15 K
rhoI	1053.00	kg/m3	293.15	Thermodynamic and transport properties of acetonitrile + alkanediols liquid mixtures at different temperatures, experimental measurements and modeling

rhoI	1049.00	kg/m3	298.15	Thermodynamic and transport properties of acetonitrile + alkanediols liquid mixtures at different temperatures, experimental measurements and modeling	
rhoI	1046.00	kg/m3	303.15	Thermodynamic and transport properties of acetonitrile + alkanediols liquid mixtures at different temperatures, experimental measurements and modeling	
rhoI	1049.90	kg/m3	298.15	Excess enthalpies of binary mixtures of some propylamines + some propanols at 298.15K	
rhoI	1046.20	kg/m3	303.15	Thermodynamic study on some alkanediol solutions: measurement and molecular modeling	
rhoI	1043.10	kg/m3	308.15	Thermodynamic study on some alkanediol solutions: measurement and molecular modeling	
rhoI	1049.60	kg/m3	298.15	Thermodynamic study on some alkanediol solutions: measurement and molecular modeling	

rhoI	1055.96	kg/m3	288.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.
rhoI	1052.86	kg/m3	293.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.
rhoI	1049.75	kg/m3	298.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.

rhoI	1046.63	kg/m3	303.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.
rhoI	1043.50	kg/m3	308.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.
rhoI	1040.35	kg/m3	313.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.

rhoI	1037.17	kg/m3	318.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.
rhoI	1033.98	kg/m3	323.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.
rhoI	1065.90	kg/m3	273.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhoI	1059.80	kg/m3	283.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhoI	1053.60	kg/m3	293.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhoI	1047.40	kg/m3	303.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhoI	1041.10	kg/m3	313.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol

rhoI	1034.80	kg/m3	323.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhoI	1028.40	kg/m3	333.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhoI	1021.90	kg/m3	343.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhoI	1015.30	kg/m3	353.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhoI	1078.20	kg/m3	253.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhoI	1075.40	kg/m3	258.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhoI	1072.30	kg/m3	263.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhoI	1069.00	kg/m3	268.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhoI	1049.90	kg/m3	298.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures

rhoI	1047.00	kg/m3	303.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures
rhoI	1044.10	kg/m3	308.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures
rhoI	1040.80	kg/m3	313.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures
rhoI	1037.80	kg/m3	318.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures
rhoI	1034.80	kg/m3	323.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures

rhoI	1055.89	kg/m3	288.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination
rhoI	1028.20	kg/m3	333.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures
rhoI	1053.66	kg/m3	293.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhoI	1050.29	kg/m3	298.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K

rhoI	1047.09	kg/m3	303.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhoI	1043.92	kg/m3	308.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhoI	1040.61	kg/m3	313.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhoI	1037.60	kg/m3	318.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhoI	1034.51	kg/m3	323.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K

rhoI	1031.00	kg/m3	328.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhoI	1037.02	kg/m3	318.15	Measurement and modeling of volumetric properties and speeds of sound of several mixtures of alcohol liquids containing 1-propanol and 2-propanol at T= (298.15 - 323.15) K and ambient pressure
rhoI	1040.19	kg/m3	313.15	Measurement and modeling of volumetric properties and speeds of sound of several mixtures of alcohol liquids containing 1-propanol and 2-propanol at T= (298.15 - 323.15) K and ambient pressure
rhoI	1043.34	kg/m3	308.15	Measurement and modeling of volumetric properties and speeds of sound of several mixtures of alcohol liquids containing 1-propanol and 2-propanol at T= (298.15 - 323.15) K and ambient pressure

rhoI	1046.48	kg/m3	303.15	Measurement and modeling of volumetric properties and speeds of sound of several mixtures of alcohol liquids containing 1-propanol and 2-propanol at T=(298.15 - 323.15) K and ambient pressure
rhoI	1049.61	kg/m3	298.15	Measurement and modeling of volumetric properties and speeds of sound of several mixtures of alcohol liquids containing 1-propanol and 2-propanol at T=(298.15 - 323.15) K and ambient pressure
rhoI	1033.91	kg/m3	323.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination
rhoI	1037.11	kg/m3	318.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination

rhoI	1040.28	kg/m3	313.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination
rhoI	1043.43	kg/m3	308.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination
rhoI	1046.57	kg/m3	303.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination

rhoI	1049.69	kg/m3	298.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination
rhoI	1049.68	kg/m3	298.15	Isobaric vapor-liquid equilibria for the binary and ternary mixtures of 2-propanol, water, and 1,3-propanediol at p = 101.3 kPa: Effect of the 1,3-propanediol addition
rhoI	1040.12	kg/m3	313.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K
rhoI	1046.51	kg/m3	303.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K
rhoI	1049.68	kg/m3	298.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K

rhoI	1052.85	kg/m3	293.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K
rhoI	1059.14	kg/m3	283.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K
rhoI	1053.00	kg/m3	293.00	KDB
rhoI	1031.40	kg/m3	328.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbrp	383.20	K	1.60	NIST Webbook

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.64154e+01
Coeff. B	-4.84399e+03
Coeff. C	-7.66890e+01
Temperature range (K), min.	377.04
Temperature range (K), max.	684.00

Datasets

Speed of sound, m/s

Temperature, K - Liquid	Pressure, kPa - Liquid	Speed of sound, m/s - Liquid
293.15	100.00	1635.213
293.15	5030.00	1649.982
293.15	10062.00	1664.642
293.15	15066.00	1678.921
293.15	20096.00	1692.938
293.15	24997.00	1706.35
293.15	30029.00	1719.901
313.15	99.00	1589.462
313.15	5048.00	1605.093
313.15	10031.00	1620.261
313.15	15138.00	1635.434
313.15	20064.00	1649.763
313.15	25191.00	1664.415
313.15	30167.00	1678.273
333.15	100.00	1544.067
333.15	5058.00	1560.325
333.15	10054.00	1576.249
333.15	15024.00	1591.679
333.15	20153.00	1607.231
333.15	25135.00	1622.05
333.15	30136.00	1636.643
353.15	101.00	1497.623
353.15	5038.00	1514.638
353.15	10023.00	1531.32
353.15	15089.00	1547.839
353.15	20158.00	1563.937
353.15	25109.00	1579.311
353.15	30076.00	1594.386

Reference

<https://www.doi.org/10.1016/j.jct.2016.06.001>

Sources

Liquid-Liquid Equilibria in Binary Mixtures of Dihydroxy Alcohols and Monomeric Esters of Lipids: r,o-Alkanediols by Correlation Gas Capacities, viscosities and refractive indices of binary mixtures containing Heat Capacities of Solution theory.

alpha-methyl-omega-hydroxy alcohols + CO

Jalilak Method: Difference between (293.15 and 353.15) K:

Excess volumes and excess heat capacities for alkanediol + water systems at different temperatures intervals bridges in van der Waals XIV. Polyhydric alcohols + diesters and esters (r vapor + liquid) equilibria at T = 298 K to T = 373 K and at pressures up to 0.1 MPa: (1,2-propanediol + 1,3-propanediol), Densities and Excess Molar Properties for Binary Glycerol + 1-Propanol, + 2-propanol, + 1,2-butanediol, + 1,3-butanediol, and + meso-isomers of mixtures compounds by bubble-point-coating method:

Investigation on some thermophysical properties of poly(ethylene glycol) binary systems and activity coefficients at infinite dilution for glycolic solutes, water and diols in the thermodynamic Properties of 1,2- and 1,3-propanediol binary systems of: Measurement and correlation for vapor pressures and equilibrium for mixtures of 1,2-propanediol and 1,3-propanediol with ethanediol in a homologous series of α,ω -alkanediols in N₂ and in binary mixtures, Speeds of Sound, and Relative Permittivities Measurement and others in propane, 1,2-propanediol, tetraerythritol, liquid 2-liquid equilibrium, equilibrium data, binary mixtures of 1,2-hexanediol with different alcohols, 1,2-propanediol at P = 101.32 kPa, 1,3-hexanediol with 1,2-hexanediol, 1,3-hexanediol with 1,4-hexanediol, 1,3-hexanediol with 1,5-hexanediol, 1,3-hexanediol with 1,6-hexanediol, 1,3-hexanediol with 1,7-heptanediol, 1,3-hexanediol with 1,8-octanediol, 1,3-hexanediol with 1,9-nonanediol, 1,3-hexanediol with 1,10-decanediol, 1,3-hexanediol with 1,11-undecanediol, 1,3-hexanediol with 1,12-dodecanediol, 1,3-hexanediol with 1,13-tridecanediol, 1,3-hexanediol with 1,14-tetradecanediol, 1,3-hexanediol with 1,15-pentadecanediol, 1,3-hexanediol with 1,16-hexadecanediol, 1,3-hexanediol with 1,17-heptadecanediol, 1,3-hexanediol with 1,18-octadecanediol, 1,3-hexanediol with 1,19-nonadecanediol, 1,3-hexanediol with 1,20-eicosanediol, 1,3-hexanediol with 1,21-heneicosanediol, 1,3-hexanediol with 1,22-docosanediol, 1,3-hexanediol with 1,23-tricosanediol, 1,3-hexanediol with 1,24-tetracosanediol, 1,3-hexanediol with 1,25-pentacosanediol, 1,3-hexanediol with 1,26-hexacosanediol, 1,3-hexanediol with 1,27-heptacosanediol, 1,3-hexanediol with 1,28-octacosanediol, 1,3-hexanediol with 1,29-nonacosanediol, 1,3-hexanediol with 1,30-triacontanediol, 1,3-hexanediol with 1,31-dotriacontanediol, 1,3-hexanediol with 1,32-tetratriacontanediol, 1,3-hexanediol with 1,33-pentatriacontanediol, 1,3-hexanediol with 1,34-hexatriacontanediol, 1,3-hexanediol with 1,35-heptatriacontanediol, 1,3-hexanediol with 1,36-octatriacontanediol, 1,3-hexanediol with 1,37-nonatriacontanediol, 1,3-hexanediol with 1,38-decatriacontanediol, 1,3-hexanediol with 1,39-undecatriacontanediol, 1,3-hexanediol with 1,40-dodecatriacontanediol, 1,3-hexanediol with 1,41-tridecatriacontanediol, 1,3-hexanediol with 1,42-tetradecatriacontanediol, 1,3-hexanediol with 1,43-pentadecatriacontanediol, 1,3-hexanediol with 1,44-hexadecatriacontanediol, 1,3-hexanediol with 1,45-heptadecatriacontanediol, 1,3-hexanediol with 1,46-octadecatriacontanediol, 1,3-hexanediol with 1,47-nonadecatriacontanediol, 1,3-hexanediol with 1,48-eicosacontanediol, 1,3-hexanediol with 1,49-heneicosacontanediol, 1,3-hexanediol with 1,50-dotriacontanediol, 1,3-hexanediol with 1,51-tritriacontanediol, 1,3-hexanediol with 1,52-tetracontanediol, 1,3-hexanediol with 1,53-pentacosacontanediol, 1,3-hexanediol with 1,54-hexacosacontanediol, 1,3-hexanediol with 1,55-heptacosacontanediol, 1,3-hexanediol with 1,56-octacosacontanediol, 1,3-hexanediol with 1,57-nonacosacontanediol, 1,3-hexanediol with 1,58-decacosanediol, 1,3-hexanediol with 1,59-undecacosanediol, 1,3-hexanediol with 1,60-dodecacosanediol, 1,3-hexanediol with 1,61-tridecacosanediol, 1,3-hexanediol with 1,62-tetradecacosanediol, 1,3-hexanediol with 1,63-pentadecacosanediol, 1,3-hexanediol with 1,64-hexadecacosanediol, 1,3-hexanediol with 1,65-heptadecacosanediol, 1,3-hexanediol with 1,66-octadecacosanediol, 1,3-hexanediol with 1,67-nonadecacosanediol, 1,3-hexanediol with 1,68-eicosacontanediol, 1,3-hexanediol with 1,69-heneicosacontanediol, 1,3-hexanediol with 1,70-dotriacontanediol, 1,3-hexanediol with 1,71-tritriacontanediol, 1,3-hexanediol with 1,72-tetracontanediol, 1,3-hexanediol with 1,73-pentacosacontanediol, 1,3-hexanediol with 1,74-hexacosacontanediol, 1,3-hexanediol with 1,75-heptacosacontanediol, 1,3-hexanediol with 1,76-octacosacontanediol, 1,3-hexanediol with 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<https://www.doi.org/10.1021/acs.jced.9b00283>

<https://www.doi.org/10.1021/je060333x>

<https://www.doi.org/10.1016/j.fluid.2016.02.031>

<https://www.doi.org/10.1021/je800356x>

https://en.wikipedia.org/wiki/Joback_method

<https://www.doi.org/10.1016/j.fluid.2013.06.041>

<https://www.doi.org/10.1016/j.jct.2005.08.015>

<https://www.doi.org/10.1016/j.ijct.2016.01.019>

<https://www.chemic.org/files/research/kdb/mol/mol911.mol>

<https://www.doi.org/10.1021/je060496l>

<https://www.doi.org/10.1016/j.fluid.2014.07.038>

<https://www.chemeo.com/doc/models/crippen> log10ws

<https://www.doi.org/10.1016/j.jct.2012.11.016>

<https://www.doi.org/10.1016/j.ijct.2014.04.024>

<https://www.doi.org/10.1021/je7004374>

<https://www.doi.org/10.1021/acs.jced.8b01219>

<https://www.doi.org/10.1021/acs.jced.8b00403>

<https://www.doi.org/10.1016/j.jct.2006.10.004>

<https://www.doi.org/10.1021/je0340755>

<https://www.doi.org/10.1016/j.jct.2017.03.014>

<https://www.doi.org/10.1016/j.jct.2018.12.030>

<https://www.doi.org/10.1016/j.jct.2012.06.031>

<https://www.doi.org/10.1016/j.fluid.2014.02.006>

<https://www.doi.org/10.1016/j.fluid.2013.06.048>

<https://www.doi.org/10.1016/j.fluid.2011.11.004>

<https://www.doi.org/10.1016/j.fluid.2014.04.002>

<https://www.doi.org/10.1021/je200766t>

<https://www.doi.org/10.1016/j.jct.2013.08.020>

<https://www.doi.org/10.1016/j.jct.2016.07.014>

<https://www.doi.org/10.1016/j.jct.2015.04.033>

<https://www.doi.org/10.1016/j.jct.2016.07.005>

<https://www.sciencedirect.com/book/9780128029992/the-yaws-handbook-of-vapor-pressure>

<https://www.doi.org/10.1021/je700037z>

<https://www.doi.org/10.1016/j.jct.2005.06.018>

<http://link.springer.com/article/10.1007/BF02311772>

<https://www.doi.org/10.1016/j.jct.2015.01.014>

<https://www.doi.org/10.1016/j.jct.2017.03.022>

<https://www.doi.org/10.1016/j.fluid.2013.02.008>

<https://www.doi.org/10.1016/j.jct.2007.08.005>

1,3-Propanediol and some of its mixtures at different temperatures (298, 303, 308, 313, 318, 323, 328, 333, 338, 343, 348, 353, 358, 363, 368, 373, 378, 383, 388, 393, 398, 403, 408, 413, 418, 423, 428, 433, 438, 443, 448, 453, 458, 463, 468, 473, 478, 483, 488, 493, 498, 503, 508, 513, 518, 523, 528, 533, 538, 543, 548, 553, 558, 563, 568, 573, 578, 583, 588, 593, 598, 603, 608, 613, 618, 623, 628, 633, 638, 643, 648, 653, 658, 663, 668, 673, 678, 683, 688, 693, 698, 703, 708, 713, 718, 723, 728, 733, 738, 743, 748, 753, 758, 763, 768, 773, 778, 783, 788, 793, 798, 803, 808, 813, 818, 823, 828, 833, 838, 843, 848, 853, 858, 863, 868, 873, 878, 883, 888, 893, 898, 903, 908, 913, 918, 923, 928, 933, 938, 943, 948, 953, 958, 963, 968, 973, 978, 983, 988, 993, 998, 1003, 1008, 1013, 1018, 1023, 1028, 1033, 1038, 1043, 1048, 1053, 1058, 1063, 1068, 1073, 1078, 1083, 1088, 1093, 1098, 1103, 1108, 1113, 1118, 1123, 1128, 1133, 1138, 1143, 1148, 1153, 1158, 1163, 1168, 1173, 1178, 1183, 1188, 1193, 1198, 1203, 1208, 1213, 1218, 1223, 1228, 1233, 1238, 1243, 1248, 1253, 1258, 1263, 1268, 1273, 1278, 1283, 1288, 1293, 1298, 1303, 1308, 1313, 1318, 1323, 1328, 1333, 1338, 1343, 1348, 1353, 1358, 1363, 1368, 1373, 1378, 1383, 1388, 1393, 1398, 1403, 1408, 1413, 1418, 1423, 1428, 1433, 1438, 1443, 1448, 1453, 1458, 1463, 1468, 1473, 1478, 1483, 1488, 1493, 1498, 1503, 1508, 1513, 1518, 1523, 1528, 1533, 1538, 1543, 1548, 1553, 1558, 1563, 1568, 1573, 1578, 1583, 1588, 1593, 1598, 1603, 1608, 1613, 1618, 1623, 1628, 1633, 1638, 1643, 1648, 1653, 1658, 1663, 1668, 1673, 1678, 1683, 1688, 1693, 1698, 1703, 1708, 1713, 1718, 1723, 1728, 1733, 1738, 1743, 1748, 1753, 1758, 1763, 1768, 1773, 1778, 1783, 1788, 1793, 1798, 1803, 1808, 1813, 1818, 1823, 1828, 1833, 1838, 1843, 1848, 1853, 1858, 1863, 1868, 1873, 1878, 1883, 1888, 1893, 1898, 1903, 1908, 1913, 1918, 1923, 1928, 1933, 1938, 1943, 1948, 1953, 1958, 1963, 1968, 1973, 1978, 1983, 1988, 1993, 1998, 2003, 2008, 2013, 2018, 2023, 2028, 2033, 2038, 2043, 2048, 2053, 2058, 2063, 2068, 2073, 2078, 2083, 2088, 2093, 2098, 2103, 2108, 2113, 2118, 2123, 2128, 2133, 2138, 2143, 2148, 2153, 2158, 2163, 2168, 2173, 2178, 2183, 2188, 2193, 2198, 2203, 2208, 2213, 2218, 2223, 2228, 2233, 2238, 2243, 2248, 2253, 2258, 2263, 2268, 2273, 2278, 2283, 2288, 2293, 2298, 2303, 2308, 2313, 2318, 2323, 2328, 2333, 2338, 2343, 2348, 2353, 2358, 2363, 2368, 2373, 2378, 2383, 2388, 2393, 2398, 2403, 2408, 2413, 2418, 2423, 2428, 2433, 2438, 2443, 2448, 2453, 2458, 2463, 2468, 2473, 2478, 2483, 2488, 2493, 2498, 2503, 2508, 2513, 2518, 2523, 2528, 2533, 2538, 2543, 2548, 2553, 2558, 2563, 2568, 2573, 2578, 2583, 2588, 2593, 2598, 2603, 2608, 2613, 2618, 2623, 2628, 2633, 2638, 2643, 2648, 2653, 2658, 2663, 2668, 2673, 2678, 2683, 2688, 2693, 2698, 2703, 2708, 2713, 2718, 2723, 2728, 2733, 2738, 2743, 2748, 2753, 2758, 2763, 2768, 2773, 2778, 2783, 2788, 2793, 2798, 2803, 2808, 2813, 2818, 2823, 2828, 2833, 2838, 2843, 2848, 2853, 2858, 2863, 2868, 2873, 2878, 2883, 2888, 2893, 2898, 2903, 2908, 2913, 2918, 2923, 2928, 2933, 2938, 2943, 2948, 2953, 2958, 2963, 2968, 2973, 2978, 2983, 2988, 2993, 2998, 3003, 3008, 3013, 3018, 3023, 3028, 3033, 3038, 3043, 3048, 3053, 3058, 3063, 3068, 3073, 3078, 3083, 3088, 3093, 3098, 3103, 3108, 3113, 3118, 3123, 3128, 3133, 3138, 3143, 3148, 3153, 3158, 3163, 3168, 3173, 3178, 3183, 3188, 3193, 3198, 3203, 3208, 3213, 3218, 3223, 3228, 3233, 3238, 3243, 3248, 3253, 3258, 3263, 3268, 3273, 3278, 3283, 3288, 3293, 3298, 3303, 3308, 3313, 3318, 3323, 3328, 3333, 3338, 3343, 3348, 3353, 3358, 3363, 3368, 3373, 3378, 3383, 3388, 3393, 3398, 3403, 3408, 3413, 3418, 3423, 3428, 3433, 3438, 3443, 3448, 3453, 3458, 3463, 3468, 3473, 3478, 3483, 3488, 3493, 3498, 3503, 3508, 3513, 3518, 3523, 3528, 3533, 3538, 3543, 3548, 3553, 3558, 3563, 3568, 3573, 3578, 3583, 3588, 3593, 3598, 3603, 3608, 3613, 3618, 3623, 3628, 3633, 3638, 3643, 3648, 3653, 3658, 3663, 3668, 3673, 3678, 3683, 3688, 3693, 3698, 3703, 3708, 3713, 3718, 3723, 3728, 3733, 3738, 3743, 3748, 3753, 3758, 3763, 3768, 3773, 3778, 3783, 3788, 3793, 3798, 3803, 3808,

<https://www.doi.org/10.1016/j.tca.2013.03.010>
<https://www.doi.org/10.1016/j.tca.2016.09.005>
<https://www.doi.org/10.1021/je101353r>
<https://www.doi.org/10.1016/j.fluid.2014.06.005>
<https://www.doi.org/10.1016/j.jct.2016.06.001>
<https://www.doi.org/10.1021/je700499d>
<http://webbook.nist.gov/cgi/cbook.cgi?ID=C504632&Units=SI>
<https://www.doi.org/10.1016/j.tca.2006.08.006>
<https://www.doi.org/10.1016/j.jct.2009.11.018>
<http://pubs.acs.org/doi/abs/10.1021/ci990307l>
<https://www.doi.org/10.1016/j.jct.2017.06.004>
<https://www.doi.org/10.1007/s10765-014-1740-z>
<https://www.doi.org/10.1021/je060419q>
<https://www.doi.org/10.1016/j.jct.2012.07.024>
<https://www.doi.org/10.1016/j.tca.2013.03.025>

affp:	Proton affinity
basg:	Gas basicity
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
gf:	Standard Gibbs free energy of formation
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices

speedsl:	Speed of sound in fluid
tb:	Normal Boiling Point Temperature
tbrp:	Boiling point at reduced pressure
tc:	Critical Temperature
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume

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