Propylene Glycol

Other names:	(.+-.)-1,2-propanediol
	(.+/-.)-1,2-Propanediol
	(R,S)-1,2-propanediol
	(RS)-1,2-Propanediol
	1,2-Dihydroxypropane
	1,2-PROPANEDIOL
	1,2-PROPYLENE GLYCOL
	1,2-Propandiol
	1,2-Propylenglykol
	1,2-propanediol (propylene glycol)
	2,3-Propanediol
	2-Hydroxypropanol
	DL-1,2-Propanediol
	DL-Propylene glycol
	Dowfrost
	Ilexan P
	Isopropylene glycol
	METHYLETHYLENE GLYCOL
	Methylethyl glycol
	Monopropylene glycol
	NSC 69860
	PG 12
	Prolugen
	Propane-1,2-diol
	Propylene glycol USP
	Propylenglycol
	SIRLENE
	Sentry Propylene Glycol
	Solar winter ban
	Solargard P
	Trimethyl glycol
	Ucar 35
	propanediol
	propylene glycol (1,2-propanediol)
	«alpha»-Propylene glycol
	Â«alphaÂ»-Propylene glycol
Inchi:	InChI=1S/C3H8O2/c1-3(5)2-4/h3-5H,2H2,1H3
InchiKey:	DNIAPMSPPWPWGF-UHFFFAOYSA-N
Formula:	C3H8O2
SMILES:	CC(O)CO

Mol. weight [g/mol]: 76.09
CAS: 57-55-6

Physical Properties

Property code	Value	Unit	Source
chl	-1823.50 ± 1.80	kJ/mol	NIST Webbook
chl	-1822.90 ± 4.10	kJ/mol	NIST Webbook
chl	-1838.10 ± 2.30	kJ/mol	NIST Webbook
dm	3.60	debye	KDB
gf	-301.70	kJ/mol	Joback Method
hf	-421.00 ± 3.00	kJ/mol	NIST Webbook
hf	-435.30	kJ/mol	NIST Webbook
hf	-424.20	kJ/mol	KDB
hf	-429.80 ± 4.10	kJ/mol	NIST Webbook
hfl	-500.30 ± 1.80	kJ/mol	NIST Webbook
hfl	-501.00 ± 4.10	kJ/mol	NIST Webbook
hfl	-486.00 ± 3.00	kJ/mol	NIST Webbook
hfus	8.18	kJ/mol	Joback Method
hvap	55.24	kJ/mol	Joback Method
log10ws	0.28		Crippen Method
logp	-0.640		Crippen Method
mcvol	64.870	ml/mol	McGowan Method
nfpaf	%!d(float64=1)		KDB
nfpah	%!d(float64=1)		KDB
pc	6070.00	kPa	KDB
rinpol	719.00		NIST Webbook
rinpol	753.00		NIST Webbook
rinpol	758.00		NIST Webbook
rinpol	764.00		NIST Webbook
rinpol	710.00		NIST Webbook
rinpol	745.00		NIST Webbook
rinpol	722.00		NIST Webbook
rinpol	745.00		NIST Webbook
rinpol	710.00		NIST Webbook
rinpol	710.00		NIST Webbook
rinpol	722.00		NIST Webbook
rinpol	745.00		NIST Webbook
rinpol	705.00		NIST Webbook
rinpol	740.00		NIST Webbook
rinpol	732.00		NIST Webbook

rinpol	716.00		NIST Webbook
rinpol	758.00		NIST Webbook
ripol	1583.00		NIST Webbook
ripol	1594.00		NIST Webbook
ripol	1599.00		NIST Webbook
ripol	1603.00		NIST Webbook
ripol	1611.00		NIST Webbook
ripol	1589.00		NIST Webbook
ripol	1585.00		NIST Webbook
ripol	1612.00		NIST Webbook
ripol	1611.00		NIST Webbook
ripol	1599.00		NIST Webbook
ripol	1603.00		NIST Webbook
ripol	1597.00		NIST Webbook
ripol	1599.00		NIST Webbook
ripol	1612.00		NIST Webbook
ripol	1600.00		NIST Webbook
ripol	1591.00		NIST Webbook
ripol	1605.00		NIST Webbook
ripol	1603.00		NIST Webbook
ripol	1603.00		NIST Webbook
ripol	1612.00		NIST Webbook
ripol	1602.00		NIST Webbook
ripol	1599.00		NIST Webbook
ripol	1600.00		NIST Webbook
tb	460.15 ± 2.00	K	NIST Webbook
tb	460.20	K	NIST Webbook
tb	460.45	K	NIST Webbook
tb	461.65 ± 3.00	K	NIST Webbook
tb	458.45 ± 3.00	K	NIST Webbook
tb	460.15 ± 2.00	K	NIST Webbook
tb	462.00 ± 2.00	K	NIST Webbook
tb	460.55 ± 0.50	K	NIST Webbook
tb	459.15 ± 1.00	K	NIST Webbook
tb	460.50	K	KDB
tb	461.00 ± 0.20	K	NIST Webbook
tb	460.60 ± 0.50	K	NIST Webbook
tb	461.15 ± 3.00	K	NIST Webbook
tb	459.15 ± 1.00	K	NIST Webbook
tb	459.80 ± 0.50	K	NIST Webbook
tb	459.15 ± 2.00	K	NIST Webbook
tc	625.00	K	KDB
tf	213.00	K	KDB
vc	0.237	m3/kmol	KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	165.24	J/mol×K	614.38	Joback Method
cpg	160.76	J/mol×K	587.31	Joback Method
cpg	156.10	J/mol×K	560.24	Joback Method
cpg	151.24	J/mol×K	533.17	Joback Method
cpg	146.19	J/mol×K	506.10	Joback Method
cpg	140.93	J/mol×K	479.03	Joback Method
cpg	135.47	J/mol×K	451.96	Joback Method
cpl	197.00	J/mol×K	313.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	180.30	J/mol×K	276.70	NIST Webbook
cpl	177.00	J/mol×K	303.00	NIST Webbook
cpl	189.90	J/mol×K	298.00	NIST Webbook
cpl	215.30	J/mol×K	353.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	210.60	J/mol×K	343.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	206.00	J/mol×K	333.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	201.30	J/mol×K	323.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	192.80	J/mol×K	303.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)

dvisc	0.0195800	Pa×s	313.15	Excess molar volume and viscosity deviation for binary mixtures of polyethylene glycol dimethyl ether 250 with 1,2-alkanediols (C3 C6) at T = (293.15 to 323.15) K	
dvisc	0.0127900	Pa×s	323.15	Excess molar volume and viscosity deviation for binary mixtures of polyethylene glycol dimethyl ether 250 with 1,2-alkanediols (C3 C6) at T = (293.15 to 323.15) K	
dvisc	0.0324000	Pa×s	303.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)	
dvisc	0.0326300	Pa×s	303.15	Excess molar volume and viscosity deviation for binary mixtures of polyethylene glycol dimethyl ether 250 with 1,2-alkanediols (C3 C6) at T = (293.15 to 323.15) K	
dvisc	0.0121000	Pa×s	323.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)	

dvisc	0.0081900	Pa×s	333.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)	
dvisc	0.0057040	Pa×s	343.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)	
dvisc	0.0434340	Pa×s	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures	
dvisc	0.0242440	Pa×s	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures	

dvisc	0.0454403	Pa×s	298.15	Densities, Viscosities, and Volumetric Properties of Binary Mixtures of 1,2-Propanediol + 1-Heptanol or 1-Hexanol and 1,2-Ethanediol + 2-Butanol or 2-Propanol at T = (298.15, 303.15, and 308.15) K	
dvisc	0.0263377	Pa×s	308.15	Densities, Viscosities, and Volumetric Properties of Binary Mixtures of 1,2-Propanediol + 1-Heptanol or 1-Hexanol and 1,2-Ethanediol + 2-Butanol or 2-Propanol at T = (298.15, 303.15, and 308.15) K	
dvisc	0.0562100	Pa×s	293.15	Excess molar volume and viscosity deviation for binary mixtures of polyethylene glycol dimethyl ether 250 with 1,2-alkanediols (C3 C6) at T = (293.15 to 323.15) K	
dvisc	0.0191200	Pa×s	313.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)	
dvisc	0.0339949	Pa×s	303.15	Densities, Viscosities, and Volumetric Properties of Binary Mixtures of 1,2-Propanediol + 1-Heptanol or 1-Hexanol and 1,2-Ethanediol + 2-Butanol or 2-Propanol at T = (298.15, 303.15, and 308.15) K	

hvapt	56.20 ± 0.20	kJ/mol	430.50	NIST Webbook
hvapt	52.00 ± 0.30	kJ/mol	430.50	NIST Webbook
hvapt	58.60	kJ/mol	389.50	NIST Webbook
hvapt	64.00 ± 2.00	kJ/mol	353.00	NIST Webbook
hvapt	58.20	kJ/mol	378.00	NIST Webbook
hvapt	56.00	kJ/mol	431.50	NIST Webbook
hvapt	66.50	kJ/mol	390.50	NIST Webbook
hvapt	47.50 ± 0.60	kJ/mol	430.50	NIST Webbook
hvapt	60.00 ± 0.30	kJ/mol	430.50	NIST Webbook
pvap	36.61	kPa	429.55	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	40.01	kPa	432.05	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	43.33	kPa	433.70	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling

pvap	46.66	kPa	436.07	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	50.00	kPa	437.77	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	53.25	kPa	439.74	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	56.74	kPa	441.27	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling

pvap	59.99	kPa	443.15	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	19.99	kPa	413.23	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	26.66	kPa	421.21	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	33.33	kPa	427.16	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling

pvap	39.99	kPa	432.05	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	8.20	kPa	393.22	Vapor-Liquid Equilibrium for Propylene Glycol + 2-(2-Hexyloxyethoxy)ethanol and 1-Methyl-2-pyrrolidone + 1-Methoxypropan-2-ol
pvap	8.21	kPa	393.25	Vapor-Liquid Equilibrium for Propylene Glycol + 2-(2-Hexyloxyethoxy)ethanol and 1-Methyl-2-pyrrolidone + 1-Methoxypropan-2-ol
pvap	10.23	kPa	398.09	Vapor-Liquid Equilibrium for Propylene Glycol + 2-(2-Hexyloxyethoxy)ethanol and 1-Methyl-2-pyrrolidone + 1-Methoxypropan-2-ol
pvap	12.77	kPa	403.14	Vapor-Liquid Equilibrium for Propylene Glycol + 2-(2-Hexyloxyethoxy)ethanol and 1-Methyl-2-pyrrolidone + 1-Methoxypropan-2-ol
pvap	12.77	kPa	403.15	Vapor-Liquid Equilibrium for Propylene Glycol + 2-(2-Hexyloxyethoxy)ethanol and 1-Methyl-2-pyrrolidone + 1-Methoxypropan-2-ol

pvap	33.57	kPa	427.23	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	19.36	kPa	413.10	Vapor-Liquid Equilibrium for Propylene Glycol + 2-(2-Hexyloxyethoxy)ethanol and 1-Methyl-2-pyrrolidone + 1-Methoxypropan-2-ol
pvap	19.39	kPa	413.15	Vapor-Liquid Equilibrium for Propylene Glycol + 2-(2-Hexyloxyethoxy)ethanol and 1-Methyl-2-pyrrolidone + 1-Methoxypropan-2-ol
pvap	23.68	kPa	418.16	Vapor-Liquid Equilibrium for Propylene Glycol + 2-(2-Hexyloxyethoxy)ethanol and 1-Methyl-2-pyrrolidone + 1-Methoxypropan-2-ol
pvap	28.69	kPa	423.15	Vapor-Liquid Equilibrium for Propylene Glycol + 2-(2-Hexyloxyethoxy)ethanol and 1-Methyl-2-pyrrolidone + 1-Methoxypropan-2-ol
pvap	28.81	kPa	423.26	Vapor-Liquid Equilibrium for Propylene Glycol + 2-(2-Hexyloxyethoxy)ethanol and 1-Methyl-2-pyrrolidone + 1-Methoxypropan-2-ol

pvap	4.00	kPa	378.00	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and y-Butyrolactone (GBL)
pvap	10.00	kPa	398.24	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and y-Butyrolactone (GBL)
pvap	12.00	kPa	402.54	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and y-Butyrolactone (GBL)
pvap	20.00	kPa	415.13	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and y-Butyrolactone (GBL)
pvap	30.00	kPa	425.72	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and y-Butyrolactone (GBL)
pvap	40.00	kPa	433.59	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and y-Butyrolactone (GBL)

pvap	50.00	kPa	439.90	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and y-Butyrolactone (GBL)
pvap	60.00	kPa	445.20	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and y-Butyrolactone (GBL)
pvap	70.00	kPa	449.79	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and y-Butyrolactone (GBL)
pvap	80.00	kPa	453.84	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and y-Butyrolactone (GBL)
pvap	90.00	kPa	457.48	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and y-Butyrolactone (GBL)
pvap	100.00	kPa	460.79	Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and y-Butyrolactone (GBL)

pvap	10.00	kPa	398.23	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa
pvap	0.62	kPa	345.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression
pvap	0.70	kPa	347.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression
pvap	0.84	kPa	350.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression
pvap	1.00	kPa	353.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression
pvap	1.13	kPa	355.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression

pvap	1.27	kPa	357.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression
pvap	1.51	kPa	360.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression
pvap	1.78	kPa	363.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression
pvap	1.99	kPa	365.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression
pvap	30.00	kPa	424.50	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	2.60	kPa	370.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression

pvap	3.03	kPa	373.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression
pvap	3.36	kPa	375.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression
pvap	3.72	kPa	377.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression
pvap	26.62	kPa	421.20	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling
pvap	23.34	kPa	417.15	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling

pvap	19.96	kPa	412.95	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling	
pvap	16.61	kPa	408.60	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling	
pvap	13.33	kPa	402.95	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling	
pvap	10.00	kPa	396.95	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling	

pvap	6.67	kPa	389.39	Excess properties and isobaric (vapor + liquid) equilibrium at sub-atmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modelling	
pvap	24.59	kPa	420.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	20.22	kPa	415.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	16.53	kPa	410.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	13.44	kPa	405.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	10.86	kPa	400.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	8.71	kPa	395.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	6.95	kPa	390.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	

pvap	5.50	kPa	385.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	4.32	kPa	380.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	3.36	kPa	375.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	2.60	kPa	370.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	1.99	kPa	365.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	1.51	kPa	360.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	1.13	kPa	355.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	
pvap	0.84	kPa	350.15	Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression	

pvap	15.89	kPa	408.30	Vapor-Liquid Equilibrium for Propylene Glycol + 2-(2-Hexyloxyethoxy)ethanol and 1-Methyl-2-pyrrolidone + 1-Methoxypropan-2-ol
pvap	2.21	kPa	367.15	Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression
rfi	1.43247		293.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
rfi	1.43230		298.15	Densities, Excess Molar Volumes, Viscosity, and Refractive Indices of Binary and Ternary Liquid Mixtures of Methanol (1) + Ethanol (2) + 1,2-Propanediol (3) at P = 81.5 kPa
rfi	1.43143		293.15	Liquid-Liquid Equilibria of (Limonene + Linalool + Ethylene Glycol or Diethylene Glycol or Triethylene Glycol or 1,2-Propylene Glycol) Ternary Systems

rfi	1.43100	298.15	Study of the Acoustic and Thermodynamic Properties of 1,2- and 1,3-Propanediol by Means of High-Pressure Speed of Sound Measurements at Temperatures from (293 to 318) K and Pressures up to 101 MPa
rfi	1.43230	298.15	Excess Molar Enthalpies of 1,2-Propanediol + Alkan-1-ols (C1-C6) and Their Correlations at 298.15 K and Ambient Pressure (81.5 kPa)
rfi	1.43140	298.15	Densities, Dynamic Viscosities, Speeds of Sound, and Relative Permittivities for Water + Alkanediols (Propane-1,2- and -1,3-diol and Butane-1,2-, -1,3-, -1,4-, and -2,3-Diol) at Different Temperatures
rfi	1.43262	298.15	Phase Equilibrium Involving Xylose, Water, and Ethylene Glycol or 1,2-Propylene Glycol at Different Temperatures

rfi	1.42230	323.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
rfi	1.43350	298.15	Vapor Liquid Equilibrium for Ternary and Binary Mixtures of Tetrahydrofuran, Cyclohexane, and 1,2-Propanediol at 101.3 kPa
rfi	1.42407	318.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
rfi	1.42581	313.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination

rfi	1.42751	308.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
rfi	1.42915	303.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
rfi	1.43081	298.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination

rfi	1.43411		288.15	Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination
rhol	1036.00	kg/m3	293.00	KDB
rhol	1005.79	kg/m3	333.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhol	1036.17	kg/m3	293.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K
rhol	1032.52	kg/m3	298.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K

rhol	1028.83	kg/m3	303.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K
rhol	1025.09	kg/m3	308.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K
rhol	1021.31	kg/m3	313.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K
rhol	1017.49	kg/m3	318.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K
rhol	1036.13	kg/m3	293.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K

rhol	1032.48	kg/m3	298.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	
rhol	1028.78	kg/m3	303.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	
rhol	1025.05	kg/m3	308.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	
rhol	1021.28	kg/m3	313.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	
rhol	1017.47	kg/m3	318.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	

rhol	1036.21	kg/m3	293.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K
rhol	1032.55	kg/m3	298.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K
rhol	1028.84	kg/m3	303.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K
rhol	1025.09	kg/m3	308.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K
rhol	1021.31	kg/m3	313.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K

rhol	1036.22	kg/m3	293.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	
rhol	1032.56	kg/m3	298.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	
rhol	1028.85	kg/m3	303.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	
rhol	1025.10	kg/m3	308.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	
rhol	1021.31	kg/m3	313.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	

rhol	1017.49	kg/m3	318.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K
rhol	1036.30	kg/m3	293.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhol	1032.62	kg/m3	298.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhol	1028.91	kg/m3	303.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhol	1025.16	kg/m3	308.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhol	1021.39	kg/m3	313.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhol	1017.57	kg/m3	318.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures

rhol	1013.72	kg/m3	323.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhol	1036.00	kg/m3	293.15	Thermodynamic and transport properties of acetonitrile + alkanediols liquid mixtures at different temperatures, experimental measurements and modeling
rhol	1033.00	kg/m3	298.15	Thermodynamic and transport properties of acetonitrile + alkanediols liquid mixtures at different temperatures, experimental measurements and modeling
rhol	1029.00	kg/m3	303.15	Thermodynamic and transport properties of acetonitrile + alkanediols liquid mixtures at different temperatures, experimental measurements and modeling
rhol	1033.60	kg/m3	298.15	Excess enthalpies of binary mixtures of some propylamines + some propanols at 298.15K
rhol	1028.80	kg/m3	303.15	Thermodynamic study on some alkanediol solutions: measurement and molecular modeling
rhol	1025.20	kg/m3	308.15	Thermodynamic study on some alkanediol solutions: measurement and molecular modeling

rhol	1032.70	kg/m3	298.15	Thermodynamic study on some alkanediol solutions: measurement and molecular modeling	
rhol	1039.87	kg/m3	288.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.	
rhol	1020.75	kg/m3	313.15	Volumetric, ultrasonic and spectroscopic (FT-IR) studies for the binary mixtures of imidazolium based ILs with 1,2-propanediol	
rhol	1032.56	kg/m3	298.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.	

rhol	1028.88	kg/m3	303.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.
rhol	1025.14	kg/m3	308.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.
rhol	1021.35	kg/m3	313.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.

rhol	1017.52	kg/m3	318.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.	
rhol	1013.66	kg/m3	323.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.	
rhol	1032.30	kg/m3	298.15	Isobaric Vapor Liquid Equilibria for Binary Systems of Diethyl Carbonate + Propylene Carbonate, Diethyl Carbonate + Propylene Glycol, and Ethanol + Propylene Carbonate at 101.3 kPa	
rhol	1039.77	kg/m3	288.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids	

rhol	1036.15	kg/m3	293.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids
rhol	1032.49	kg/m3	298.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids
rhol	1028.78	kg/m3	303.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids
rhol	1025.03	kg/m3	308.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids
rhol	1021.25	kg/m3	313.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids

rhol	1017.43	kg/m3	318.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids
rhol	1039.78	kg/m3	288.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids
rhol	1036.16	kg/m3	293.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids
rhol	1021.24	kg/m3	313.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids
rhol	1017.42	kg/m3	318.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids

rhol	1032.48	kg/m3	298.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids
rhol	1028.77	kg/m3	303.15	Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol. An Attempt to Design Hydraulic Liquids
rhol	1032.58	kg/m3	298.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa
rhol	1028.88	kg/m3	303.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa

rhol	1025.13	kg/m3	308.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa
rhol	1021.35	kg/m3	313.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa
rhol	1017.52	kg/m3	318.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa
rhol	1013.66	kg/m3	323.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa

rhol	1009.75	kg/m3	328.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa
rhol	1005.80	kg/m3	333.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa
rhol	1052.17	kg/m3	273.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1044.74	kg/m3	283.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1037.22	kg/m3	293.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1029.64	kg/m3	303.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1021.98	kg/m3	313.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1014.25	kg/m3	323.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1006.45	kg/m3	333.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	998.57	kg/m3	343.15	Density of Working Liquids for Diffusion Vacuum Pumps

rhol	990.62	kg/m3	353.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	982.60	kg/m3	363.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1051.30	kg/m3	273.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhol	1042.90	kg/m3	283.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhol	1035.50	kg/m3	293.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhol	1028.10	kg/m3	303.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhol	1020.60	kg/m3	313.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhol	1013.00	kg/m3	323.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhol	1005.30	kg/m3	333.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhol	997.70	kg/m3	343.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol
rhol	989.50	kg/m3	353.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol

rhol	1065.80	kg/m3	253.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol	
rhol	1062.20	kg/m3	258.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol	
rhol	1058.60	kg/m3	263.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol	
rhol	1054.90	kg/m3	268.15	Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol	
rhol	1026.15	kg/m3	308.15	Excess Molar Enthalpies of Binary Mixtures Containing Glycols or Polyglycols + Dimethyl Sulfoxide at 308.15 K	
rhol	1026.15	kg/m3	308.15	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Glycols or Poly(Ethylene Glycols) and 2-Phenylethyl Alcohol at 308.15 K and Atmospheric Pressure	
rhol	1032.50	kg/m3	298.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures	

rhol	1029.20	kg/m3	303.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures	
rhol	1025.30	kg/m3	308.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures	
rhol	1021.50	kg/m3	313.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures	
rhol	1018.00	kg/m3	318.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures	
rhol	1014.00	kg/m3	323.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures	

rhol	1010.20	kg/m3	328.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures
rhol	1006.20	kg/m3	333.15	Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures
rhol	1031.90	kg/m3	298.15	Isobaric Vapor Liquid Equilibrium for Two Binary Systems{Propane-1,2-diol + Ethane-1,2-diol and Propane-1,2-diol + Butane-1,2-diol} at p = (10.0, 20.0, and 40.0) kPa
rhol	1036.57	kg/m3	293.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhol	1032.86	kg/m3	298.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K

rhol	1029.15	kg/m3	303.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhol	1025.57	kg/m3	308.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhol	1021.44	kg/m3	313.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhol	1017.59	kg/m3	318.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhol	1013.74	kg/m3	323.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K

rhol	1009.71	kg/m3	328.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K	
rhol	1024.55	kg/m3	308.15	Volumetric, ultrasonic and spectroscopic (FT-IR) studies for the binary mixtures of imidazolium based ILs with 1,2-propanediol	
rhol	1028.31	kg/m3	303.15	Volumetric, ultrasonic and spectroscopic (FT-IR) studies for the binary mixtures of imidazolium based ILs with 1,2-propanediol	
rhol	1032.03	kg/m3	298.15	Volumetric, ultrasonic and spectroscopic (FT-IR) studies for the binary mixtures of imidazolium based ILs with 1,2-propanediol	
rhol	1035.73	kg/m3	293.15	Volumetric, ultrasonic and spectroscopic (FT-IR) studies for the binary mixtures of imidazolium based ILs with 1,2-propanediol	
rhol	1032.55	kg/m3	298.15	Excess volumes and excess heat capacities of {1,2- alkanediol + methanol} mixtures and ionic volumes in these systems	

rhol	1009.78	kg/m3	328.15	Densities, surface tensions, and isobaric vapor-liquid equilibria for the mixtures of 2-propanol, water, and 1,2-propanediol	
rhol	1017.51	kg/m3	318.15	Densities, surface tensions, and isobaric vapor-liquid equilibria for the mixtures of 2-propanol, water, and 1,2-propanediol	
rhol	1025.21	kg/m3	308.15	Densities, surface tensions, and isobaric vapor-liquid equilibria for the mixtures of 2-propanol, water, and 1,2-propanediol	
rhol	1032.69	kg/m3	298.15	Densities, surface tensions, and isobaric vapor-liquid equilibria for the mixtures of 2-propanol, water, and 1,2-propanediol	
rhol	1013.66	kg/m3	323.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination	

rhol	1017.52	kg/m3	318.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination	
rhol	1021.35	kg/m3	313.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination	
rhol	1009.75	kg/m3	328.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling	

rhol	1025.14	kg/m3	308.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination
rhol	1028.88	kg/m3	303.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination
rhol	1032.59	kg/m3	298.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination

rhol	1013.66	kg/m3	323.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling	
rhol	1039.87	kg/m3	288.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination	
rhol	1021.48	kg/m3	313.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	
rhol	1029.10	kg/m3	303.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	
rhol	1032.86	kg/m3	298.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	

rhol	1036.58	kg/m3	293.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K
rhol	1043.89	kg/m3	283.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K
rhol	1017.52	kg/m3	318.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhol	1021.35	kg/m3	313.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling

rhol	1025.14	kg/m3	308.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhol	1028.88	kg/m3	303.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhol	1032.59	kg/m3	298.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling

rhol	1036.25	kg/m3	293.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhol	1039.87	kg/m3	288.15	Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure: Measurements and modeling
rhol	997.86	kg/m3	343.15	Densities and derived thermodynamic properties of (2-methoxyethanol + 1-propanol, or 2-propanol, or 1,2-propandiol) at temperatures from T = (293.15 to 343.15) K
rhol	1005.86	kg/m3	333.15	Densities and derived thermodynamic properties of (2-methoxyethanol + 1-propanol, or 2-propanol, or 1,2-propandiol) at temperatures from T = (293.15 to 343.15) K

rhol	1013.68	kg/m3	323.15	Densities and derived thermodynamic properties of (2-methoxyethanol + 1-propanol, or 2-propanol, or 1,2-propandiol) at temperatures from T = (293.15 to 343.15) K
rhol	1021.35	kg/m3	313.15	Densities and derived thermodynamic properties of (2-methoxyethanol + 1-propanol, or 2-propanol, or 1,2-propandiol) at temperatures from T = (293.15 to 343.15) K
rhol	1028.89	kg/m3	303.15	Densities and derived thermodynamic properties of (2-methoxyethanol + 1-propanol, or 2-propanol, or 1,2-propandiol) at temperatures from T = (293.15 to 343.15) K
rhol	1036.30	kg/m3	293.15	Densities and derived thermodynamic properties of (2-methoxyethanol + 1-propanol, or 2-propanol, or 1,2-propandiol) at temperatures from T = (293.15 to 343.15) K
rhol	1036.25	kg/m3	293.15	Volumetric and viscometric behavior of the binary systems ethyl lactate + 1,2- propanediol, + 1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination

rhol	1016.92	kg/m3	318.15	Volumetric, ultrasonic and spectroscopic (FT-IR) studies for the binary mixtures of imidazolium based ILs with 1,2-propanediol	
rhol	1036.25	kg/m3	293.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.	
speedsl	1510.60	m/s	298.15	Volumetric and compressibility properties of liquid water as a solute in glycolic, propylene carbonate, and tetramethylurea solutions at T = 298.15 K	
tcondl	0.20	W/m×K	332.90	Density, Viscosity and Thermal Conductivity of Aqueous Solutions of Propylene Glycol, Dipropylene Glycol, and Tripropylene Glycol between 290 K and 460 K	
tcondl	0.19	W/m×K	411.40	Density, Viscosity and Thermal Conductivity of Aqueous Solutions of Propylene Glycol, Dipropylene Glycol, and Tripropylene Glycol between 290 K and 460 K	

tcondl	0.21	W/m×K	283.15	Thermal conductivity of dry anatase and rutile nano-powders and ethylene and propylene glycol-based TiO2 nanofluids	
tcondl	0.19	W/m×K	391.10	Density, Viscosity and Thermal Conductivity of Aqueous Solutions of Propylene Glycol, Dipropylene Glycol, and Tripropylene Glycol between 290 K and 460 K	
tcondl	0.19	W/m×K	371.60	Density, Viscosity and Thermal Conductivity of Aqueous Solutions of Propylene Glycol, Dipropylene Glycol, and Tripropylene Glycol between 290 K and 460 K	
tcondl	0.19	W/m×K	430.40	Density, Viscosity and Thermal Conductivity of Aqueous Solutions of Propylene Glycol, Dipropylene Glycol, and Tripropylene Glycol between 290 K and 460 K	
tcondl	0.21	W/m×K	303.15	Thermal conductivity of dry anatase and rutile nano-powders and ethylene and propylene glycol-based TiO2 nanofluids	
tcondl	0.21	W/m×K	323.15	Thermal conductivity of dry anatase and rutile nano-powders and ethylene and propylene glycol-based TiO2 nanofluids	

tcondl	0.21	W/m×K	343.15	Thermal conductivity of dry anatase and rutile nano-powders and ethylene and propylene glycol-based TiO2 nanofluids	
tcondl	0.20	W/m×K	299.10	Density, Viscosity and Thermal Conductivity of Aqueous Solutions of Propylene Glycol, Dipropylene Glycol, and Tripropylene Glycol between 290 K and 460 K	
tcondl	0.18	W/m×K	450.80	Density, Viscosity and Thermal Conductivity of Aqueous Solutions of Propylene Glycol, Dipropylene Glycol, and Tripropylene Glycol between 290 K and 460 K	
tcondl	0.20	W/m×K	313.60	Density, Viscosity and Thermal Conductivity of Aqueous Solutions of Propylene Glycol, Dipropylene Glycol, and Tripropylene Glycol between 290 K and 460 K	
tcondl	0.19	W/m×K	352.30	Density, Viscosity and Thermal Conductivity of Aqueous Solutions of Propylene Glycol, Dipropylene Glycol, and Tripropylene Glycol between 290 K and 460 K	

vols	9.65e-04	m3/kg	293.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.56e-04	m3/kg	279.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.57e-04	m3/kg	281.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.58e-04	m3/kg	282.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.58e-04	m3/kg	283.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	9.59e-04	m3/kg	284.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.60e-04	m3/kg	285.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.60e-04	m3/kg	286.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.61e-04	m3/kg	287.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.62e-04	m3/kg	288.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	9.62e-04	m3/kg	289.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.63e-04	m3/kg	290.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.64e-04	m3/kg	291.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.64e-04	m3/kg	292.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.55e-04	m3/kg	278.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	9.66e-04	m3/kg	294.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.54e-04	m3/kg	277.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.67e-04	m3/kg	296.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.68e-04	m3/kg	297.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.68e-04	m3/kg	298.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	9.69e-04	m3/kg	299.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.70e-04	m3/kg	300.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.70e-04	m3/kg	301.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.71e-04	m3/kg	302.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.72e-04	m3/kg	303.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	9.73e-04	m3/kg	304.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.73e-04	m3/kg	305.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.74e-04	m3/kg	306.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.75e-04	m3/kg	307.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.75e-04	m3/kg	308.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	9.76e-04	m3/kg	309.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.77e-04	m3/kg	310.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.78e-04	m3/kg	311.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.78e-04	m3/kg	312.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.79e-04	m3/kg	313.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	9.62e-04	m3/kg	288.34	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.54e-04	m3/kg	276.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.53e-04	m3/kg	275.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.53e-04	m3/kg	274.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.52e-04	m3/kg	273.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	9.62e-04	m3/kg	288.31	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.66e-04	m3/kg	295.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.56e-04	m3/kg	280.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.62e-04	m3/kg	288.05	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

Correlations

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)
Coeff. A	1.64972e+01
Coeff. B	-4.64181e+03

Coeff. C	-6.92380e+01
Temperature range (K), min.	335.73
Temperature range (K), max.	485.20

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/T + C*ln(T) + D*T^2
Coeff. A	2.23565e+02
Coeff. B	-1.60975e+04
Coeff. C	-3.08431e+01
Coeff. D	2.42067e-05
Temperature range (K), min.	213.15
Temperature range (K), max.	626.00

Datasets

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
298.15	98.00	1032.56
303.15	98.00	1028.87
312.98	98.00	1022.16
335.78	98.00	1005.31
364.39	98.00	981.63
394.95	98.00	953.22
423.51	98.00	926.76
452.17	98.00	900.36
298.15	49030.00	1055.29
303.15	49030.00	1052.03
313.00	49030.00	1046.22
335.80	49030.00	1029.3
364.66	49030.00	1007.36
395.11	49030.00	982.98
423.62	49030.00	959.18
452.10	49030.00	934.51
298.15	98060.00	1072.94
303.15	98060.00	1070.79
313.05	98060.00	1065.24

335.76	98060.00	1050.34
364.83	98060.00	1031.15
395.17	98060.00	1010.62
423.90	98060.00	989.94
452.14	98060.00	965.53
298.15	147100.00	1088.48
303.15	147100.00	1086.25
313.03	147100.00	1081.67
335.78	147100.00	1068.19
364.87	147100.00	1051.61
395.38	147100.00	1033.92
423.97	147100.00	1016.34
452.19	147100.00	996.01
298.15	196130.00	1104.32
303.15	196130.00	1101.4
313.04	196130.00	1095.69
335.80	196130.00	1082.92
365.00	196130.00	1067.32
395.57	196130.00	1051.9
424.05	196130.00	1038.38
452.18	196130.00	1022.83
298.15	245160.00	1115.28
303.15	245160.00	1112.65
313.03	245160.00	1107.51
336.01	245160.00	1095.8
364.99	245160.00	1081.56
395.68	245160.00	1067.12
424.30	245160.00	1054.25
452.07	245160.00	1042.31

Reference *https://www.doi.org/10.1016/j.fluid.2017.07.006*

Temperature, K	Pressure, kPa	Mass density, kg/m3
278.15	100.00	1047.1
278.15	1000.00	1047.3
278.15	5000.00	1049.2
278.15	10000.00	1051.2
278.15	15000.00	1053.4
278.15	20000.00	1055.5
278.15	25000.00	1057.6
278.15	30000.00	1059.6
278.15	35000.00	1061.6
278.15	40000.00	1063.6

278.15	45000.00	1065.6
278.15	50000.00	1067.5
278.15	55000.00	1069.3
278.15	60000.00	1071.4
288.15	100.00	1039.9
288.15	1000.00	1040.2
288.15	5000.00	1042.1
288.15	10000.00	1044.4
288.15	15000.00	1046.7
288.15	20000.00	1048.9
288.15	25000.00	1051.1
288.15	30000.00	1053.2
288.15	35000.00	1055.4
288.15	40000.00	1057.4
288.15	45000.00	1059.4
288.15	50000.00	1061.4
288.15	55000.00	1063.4
288.15	60000.00	1065.3
298.15	100.00	1032.5
298.15	1000.00	1032.9
298.15	5000.00	1034.8
298.15	10000.00	1037.2
298.15	15000.00	1039.6
298.15	20000.00	1041.9
298.15	25000.00	1044.1
298.15	30000.00	1046.3
298.15	35000.00	1048.4
298.15	40000.00	1050.6
298.15	45000.00	1052.5
298.15	50000.00	1054.6
298.15	55000.00	1056.6
298.15	60000.00	1058.5
308.15	100.00	1025.3
308.15	1000.00	1025.5
308.15	5000.00	1027.5
308.15	10000.00	1030.1
308.15	15000.00	1032.5
308.15	20000.00	1034.9
308.15	25000.00	1037.2
308.15	30000.00	1039.5
308.15	35000.00	1041.6
308.15	40000.00	1043.8
308.15	45000.00	1046.0
308.15	50000.00	1048.1

308.15	55000.00	1050.1
308.15	60000.00	1052.2
318.15	100.00	1017.7
318.15	1000.00	1018.0
318.15	5000.00	1020.2
318.15	10000.00	1022.8
318.15	15000.00	1025.4
318.15	20000.00	1027.9
318.15	25000.00	1030.3
318.15	30000.00	1032.7
318.15	35000.00	1035.0
318.15	40000.00	1037.2
318.15	45000.00	1039.4
318.15	50000.00	1041.5
318.15	55000.00	1043.6
318.15	60000.00	1045.7
328.15	100.00	1010.0
328.15	1000.00	1010.3
328.15	5000.00	1012.7
328.15	10000.00	1015.4
328.15	15000.00	1018.0
328.15	20000.00	1020.6
328.15	25000.00	1023.1
328.15	30000.00	1025.6
328.15	35000.00	1027.9
328.15	40000.00	1030.3
328.15	45000.00	1032.5
328.15	50000.00	1034.7
328.15	55000.00	1036.9
328.15	60000.00	1039.0
338.15	100.00	1002.2
338.15	1000.00	1002.4
338.15	5000.00	1004.8
338.15	10000.00	1007.6
338.15	15000.00	1010.4
338.15	20000.00	1013.0
338.15	25000.00	1015.6
338.15	30000.00	1018.2
338.15	35000.00	1020.7
338.15	40000.00	1023.2
338.15	45000.00	1025.5
338.15	50000.00	1027.9
338.15	55000.00	1030.2
338.15	60000.00	1032.4

348.15	100.00	994.1
348.15	1000.00	994.5
348.15	5000.00	996.9
348.15	10000.00	999.9
348.15	15000.00	1002.8
348.15	20000.00	1005.5
348.15	25000.00	1008.2
348.15	30000.00	1010.9
348.15	35000.00	1013.4
348.15	40000.00	1016.0
348.15	45000.00	1018.4
348.15	50000.00	1020.9
348.15	55000.00	1023.2
348.15	60000.00	1025.6
358.15	100.00	985.8
358.15	1000.00	986.2
358.15	5000.00	988.8
358.15	10000.00	991.9
358.15	15000.00	995.0
358.15	20000.00	997.8
358.15	25000.00	1000.6
358.15	30000.00	1003.4
358.15	35000.00	1006.0
358.15	40000.00	1008.5
358.15	45000.00	1011.2
358.15	50000.00	1013.6
358.15	55000.00	1016.1
358.15	60000.00	1018.5

Reference *https://www.doi.org/10.1016/j.jct.2012.08.014*

Temperature, K	Pressure, kPa	Mass density, kg/m3
272.69	5240.00	1054.19
272.68	10290.00	1056.38
272.68	15270.00	1058.53
272.72	20360.00	1060.64
272.73	30580.00	1064.73
272.73	50680.00	1072.45
272.77	71000.00	1079.68
272.74	91400.00	1086.61
272.76	50810.00	1072.51
272.78	15370.00	1058.52
293.18	5180.00	1039.1

293.18	10100.00	1041.39
293.18	15210.00	1043.73
293.18	20190.00	1045.96
293.18	30240.00	1050.35
293.18	50550.00	1058.66
293.18	70760.00	1066.35
293.18	90990.00	1073.55
293.18	50680.00	1058.72
293.18	15310.00	1043.77
313.12	5120.00	1024.21
313.13	10070.00	1026.73
313.13	15110.00	1029.21
313.12	20290.00	1031.71
313.13	30290.00	1036.38
313.12	50710.00	1045.31
313.12	71030.00	1053.5
313.12	91240.00	1061.08
313.12	50990.00	1045.42
313.12	15580.00	1029.43
352.99	5010.00	993.23
353.00	10100.00	996.26
353.00	15280.00	999.29
352.99	20210.00	1002.06
352.99	30360.00	1007.57
353.00	50610.00	1017.74
352.99	70750.00	1027.01
352.99	91060.00	1035.61
352.99	50620.00	1017.76
352.99	15390.00	999.36
392.94	5080.00	959.54
392.94	10090.00	963.15
392.95	15190.00	966.67
392.96	20230.00	970.02
392.97	30430.00	976.54
392.95	50730.00	988.44
392.94	70890.00	999.07
392.94	90950.00	1008.71
392.95	50820.00	988.49
392.96	15180.00	966.75
283.21	5190.00	1046.44
283.19	10060.00	1048.67
283.17	15100.00	1050.92
283.17	20200.00	1053.13
283.17	30530.00	1057.48

283.18	50550.00	1065.43
283.19	70990.00	1072.96
283.18	91270.00	1079.99
283.18	50490.00	1065.4
283.17	15140.00	1050.94
298.12	5090.00	1035.37
298.12	10070.00	1037.74
298.12	15240.00	1040.15
298.12	20170.00	1042.4
298.12	30300.00	1046.89
298.12	50590.00	1055.32
298.11	70930.00	1063.17
298.12	91050.00	1070.41
298.12	50650.00	1055.35
298.12	15160.00	1040.11
333.05	5260.00	1009.12
333.05	10050.00	1011.76
333.05	15120.00	1014.46
333.05	20250.00	1017.1
333.05	30400.00	1022.19
333.05	50610.00	1031.67
333.06	70910.00	1040.39
333.06	91130.00	1048.43
333.06	51080.00	1031.87
333.06	15210.00	1014.48
373.34	10320.00	980.11
373.34	15330.00	983.26
373.34	20360.00	986.4
373.34	30530.00	992.32
373.34	50610.00	1003.25
373.34	70990.00	1013.23
373.35	91190.00	1022.41
373.35	50860.00	1003.34
373.35	15540.00	983.34
373.35	5160.00	976.65
313.03	5190.00	1024.2
313.03	10100.00	1026.69
313.03	15280.00	1029.25
313.03	20240.00	1031.64
313.03	30440.00	1036.4
313.03	50660.00	1045.24
313.03	70960.00	1053.42
313.03	91090.00	1061.0
313.03	50710.00	1045.28

313.03	15210.00	1029.23

Reference *https://www.doi.org/10.1016/j.jct.2018.10.016*

Speed of sound, m/s

Temperature, K - Liquid	Pressure, kPa - Liquid	Speed of sound, m/s - Liquid
303.15	99.00	1494.429
303.15	5091.00	1513.504
303.15	10060.00	1532.024
303.15	15098.00	1550.199
303.15	20084.00	1567.713
303.15	25068.00	1584.711
303.15	30167.00	1601.587
313.15	99.00	1465.858
313.15	5014.00	1485.499
313.15	10053.00	1504.824
313.15	15011.00	1523.212
313.15	20095.00	1541.536
313.15	25202.00	1559.357
313.15	30222.00	1576.498
333.15	100.00	1408.863
333.15	5039.00	1429.721
333.15	10054.00	1450.066
333.15	15107.00	1469.848
333.15	20131.00	1488.963
333.15	25131.00	1507.384
333.15	30024.00	1524.874
353.15	99.00	1350.887
353.15	5042.00	1373.03
353.15	10055.00	1394.56
353.15	15135.00	1415.607
353.15	20093.00	1435.461
353.15	25086.00	1454.828
353.15	30207.00	1474.064

Reference *https://www.doi.org/10.1016/j.jct.2016.06.001*

Sources

Isobaric specific heat capacity of typical lithium chloride liquid desiccants using scanning calorimetry:	https://www.doi.org/10.1016/j.jct.2013.10.028
Thermodynamics and activity coefficients at infinite dilution for organic solutes, water and diols in the ionic liquid choline bis(trifluoromethylsulfonyl)imide:	https://www.doi.org/10.1016/j.jct.2014.04.024
Solubility of Dimethyl Fumarate in Methanol, Ethanol, 1-Propanol, 2-Propanol, 1,2-Propanediol, and Water from (289.95 to 347.15) K:	https://www.doi.org/10.1021/je100964a
Equilibrium solubility, dissolution thermodynamics and preferential solvation of adenosine in aqueous solutions of N,N-dimethylformamide, 1-methyl-2-pyrrolidone, dimethylsulfoxide and propylene glycol:	https://www.doi.org/10.1016/j.jct.2017.07.023
Densities and derived thermodynamic properties of (2-methoxyethanol + 1-propanol, or 2-propanol, or 1,2-propanediol) at temperatures from T = (288.15 to 343.15) K:	https://www.doi.org/10.1016/j.jct.2006.06.001
Measurement, Correlation, and Thermodynamics of Solubility of Isatin in Nine Different Green Solvents at (298.15 to 338.15) K:	https://www.doi.org/10.1021/je501036r
Densities, Excess Molar Volumes, Viscosity, and Refractive Indices of Binary and Ternary Liquid Mixtures of Methanol (1) + Ethanol (2) + 1,2-Propanediol (3) at P = 81.5 kPa:	https://www.doi.org/10.1021/je800633a
Densities and Excess Molar Volumes for Binary Glycerol + 1-Propanol, + 2-Propanol, + 1,2-Propanediol, and + 1,3-Propanediol Mixtures at Different Temperatures:	https://www.doi.org/10.1021/je060496l
Liquid−Liquid Equilibria of (Limonene + Linalool + Ethylene Glycol or Diethylene Glycol or Triethylene Glycol or 1,2-Propylene Glycol) Ternary Systems:	https://www.doi.org/10.1021/je700577t
Vapor-liquid equilibrium in systems (water + organic solvent + salt) at low salt concentrations but high ratios of salt to water: experimental results and modelling:	https://www.doi.org/10.1016/j.fluid.2004.07.017
Solution thermodynamics of indomethacin in propylene glycol + water mixtures:	https://www.doi.org/10.1016/j.fluid.2011.11.001
Solubility modelling and preferential solvation of adenine in solvent mixtures of (N,N-dimethylformamide, N-methyl-pyrrolidone, propylene glycol and dimethyl sulfoxide) plus water:	https://www.doi.org/10.1016/j.jct.2018.05.030
Experimental measurements and modelling of volumetric properties, refractive index and viscosity of selected binary systems with butyl lactate at 288.15 to 323.15 K and atmospheric pressure. New UNIFAC-VISCO interaction parameters.:	https://www.doi.org/10.1016/j.tca.2013.03.025
KDB:	https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=910
Potential heat transfer enhancement of functionalized graphene nanoplatelet dispersions in a propylene glycol-water mixture. Thermophysical profile:	https://www.doi.org/10.1016/j.jct.2018.04.007
Thermodynamic study of the solubility of ibuprofen and naproxen in some ethanol + propylene glycol mixtures:	https://www.doi.org/10.1016/j.fluid.2007.07.076
Thermodynamic study on some alkanediol solutions: measurement and molecular modeling:	https://www.doi.org/10.1016/j.tca.2013.03.010
Thermophysical characterization of aqueous ternary system containing N-tris [hydroxymethyl]methyl-3-amino propanesulfonic acid and glycol (PG or DPG or TPG):	https://www.doi.org/10.1016/j.jct.2012.12.005
Measurement and Correlation of the Solubility of Palmatine Chloride in Four Different Binary Solvent Systems at (283.15–328.15) K:	https://www.doi.org/10.1021/acs.jced.8b01055
Volumetric, ultrasonic and spectroscopic (FT-IR) studies for the binary mixtures of imidazolium based IL with 1,2-propanediol:	https://www.doi.org/10.1016/j.fluid.2015.12.007
Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 293.15 to 333.15 K at 0.1 MPa:	https://www.doi.org/10.1021/acs.jced.7b00621
Volumetric and viscosimetric behavior of the binary systems ethyl lactate+1,2-propanediol, +1,3-propanediol, + tetrahydrofuran and + tetraethylene glycol dimethyl ether. New UNIFAC-VISCO and ASOG-VISCO parameters determination:	https://www.doi.org/10.1016/j.fluid.2014.04.002
Solubility of Clonazepam and Diazepam in Polyethylene Glycol 200, Propylene Glycol, N-Methyl Pyrrolidone, Ethanol, and Water at (298.2 to 318.2) K and in Binary and Ternary Mixtures of Polyethylene Glycol 200, Propylene Glycol, and Water at 298.2 K:	https://www.doi.org/10.1021/je3009842
[illegible]	http://pubs.acs.org/doi/abs/10.1021/ci990307l
DSC determination of partial ternary phase diagrams of methanol/sodium chloride/water and propylene glycol/sodium chloride/water and their applications for synthesized diagrams:	https://www.doi.org/10.1016/j.tca.2010.10.012
Solubility Determination and Modeling for Artesunate in Binary Solvent Mixtures of Methanol, Ethanol, Isopropanol, and Propylene Glycol + Water:	https://www.doi.org/10.1021/acs.jced.8b00988
Solubility of sulfamethizole in some propylene glycol + water mixtures at several temperatures:	https://www.doi.org/10.1016/j.fluid.2012.03.014
Solubility of Etoricoxib in Aqueous Solutions of Glycerin, Methanol, Polyethylene Glycols 200, 400, 600, and Propylene Glycol at 298.2 K:	https://www.doi.org/10.1021/acs.jced.7b00709
Apparent Molar Volumes and Isentropic Compressibilities of Tetraalkylammonium Bromides in Aqueous Propane-1,2-diol: An Attempt to Design Hydraulic Liquids:	https://www.doi.org/10.1021/acs.jced.5b00964
Heat Capacities of Four Promising Alternatives to Lithium Bromide Aqueous Solution in Absorption Refrigerators:	https://www.doi.org/10.1021/je400605x
Solubility of Phenothiazine in Water, Ethanol, and Propylene Glycol at (298.2 to 338.2) K and Their Binary and Ternary Mixtures at 298.2 K:	https://www.doi.org/10.1021/je2001649
Excess Molar Enthalpies of Binary Mixtures Containing Glycols or Polyglycols + Dimethyl Sulfoxide at 308.15 K:	https://www.doi.org/10.1021/je034007i
Solubility and Saturation Apparent Volume of Propranolol Hydrochloride in Some Binary Aqueous Cosolvent Mixtures at 298.15 K:	https://www.doi.org/10.1021/acs.jced.5b00167
Liquid extraction of polyhydric alcohols from water using [A336][SCN] as a solvent:	https://www.doi.org/10.1016/j.jct.2015.04.033
Solubility of Hydrogen Sulfide in Ethanediol, 1,2-Propanediol, 1-Propanol, and 2-Propanol: Experimental Measurement and Modeling:	https://www.doi.org/10.1021/acs.jced.5b00680
Solubility, Density, Refractive Index, and Viscosity for the Polyhydric Alcohol + CsBr + H2O Ternary Systems at Different Temperatures:	https://www.doi.org/10.1021/je301222e
Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixtures:	https://www.doi.org/10.1021/je9010568
Experimental Solubility and Density Functional Theory Studies of Deferasirox in Binary Solvent Mixtures: Performance of Polarizable Continuum Model and Jouyban-Acree Model:	https://www.doi.org/10.1021/acs.jced.8b01001
Isobaric Vapor-Liquid Equilibrium for Two Binary Systems {Propane-1,2-diol + Ethane-1,2-diol and Propane-1,2-diol + Butane-1,2-diol} at p = (10.0, 20.0, and 40.0) kPa:	https://www.doi.org/10.1021/je5010824

Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa:	https://www.doi.org/10.1021/je400082c
Vapor Liquid Equilibrium for Ternary and Binary Mixtures of Tetrahydrofuran, Cyclohexane, and 1,2-Propanediol at 101.3 kPa:	https://www.doi.org/10.1021/je4004993
Density, Viscosity, and Thermal Conductivity of Aqueous Solutions of Propylene Glycol, Dipropylene Glycol, and Tripropylene Glycol between 290 K and 460 K:	https://www.doi.org/10.1021/je049960h
Excess enthalpies of binary mixtures of some propylamines + some propanols at 298.15 K:	https://www.doi.org/10.1016/j.tca.2006.08.006
Density of Working Liquids for Diffusion Vacuum Pumps:	https://www.doi.org/10.1021/acs.jced.8b00028
Densities, ultrasonic speeds, excess and partial molar properties of binary mixtures of 2-pyrrolidone with isomeric propanediols at temperatures from 303.15 K to 323.15 K:	https://www.doi.org/10.1016/j.jct.2017.03.022
Thermodynamics of solvation in propylene glycol and methyl cellosolve:	https://www.doi.org/10.1016/j.jct.2014.06.006
Solubility of Bifonazole in Four Binary Solvent Mixtures: Experimental Measurement and Thermodynamic Modeling:	https://www.doi.org/10.1021/acs.jced.9b00097
Phase behavior of imidazolium and phosphonium tetrafluoroborates with dihydroxy alcohols:	https://www.doi.org/10.1016/j.fluid.2014.08.028
Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures:	https://www.doi.org/10.1021/je0340248
Molar heat capacities of some aqueous 2-amino-2-hydroxymethyl-1,3-propanediol + glycol systems:	https://www.doi.org/10.1016/j.jct.2012.02.022
Thermodynamic studies of fluphenazine decanoate solubility in propylene glycol + water mixtures and correlation with the Jouyban-Acree model:	https://www.doi.org/10.1016/j.fluid.2011.06.008
Density and viscosity of propylene glycol at high temperatures and high pressures:	https://www.doi.org/10.1016/j.fluid.2017.07.006
Thermodynamic solubility modeling, solvent effect and preferential solvation of curcumin in aqueous co-solvent mixtures of ethanol, n-propanol, isopropanol and propylene glycol:	https://www.doi.org/10.1016/j.jct.2018.11.022
Thermodynamic analysis of the solubility of ketoprofen in some propylene glycol + water cosolvent mixtures:	https://www.doi.org/10.1016/j.fluid.2010.03.031
Liquid phase behavior of hexafluorophosphate ionic liquids with polyhydric alcohols:	https://www.doi.org/10.1016/j.fluid.2011.11.004
Isobaric Vapor Liquid Equilibria for Binary Systems of Diethyl Carbonate + Propylene Carbonate, Diethyl Carbonate + Propylene Glycol, and Ethanol + Propylene Carbonate at 101.3 kPa:	https://www.doi.org/10.1021/acs.jced.5b00064
Solubility of 7-Chloro-2-methylamino-5-phenyl-3H-1,4-benzodiazepine-4-oxide, 7-Chloro-1,3-dihydro-5-phenyl-2H-1,4-benzodiazepin-2-one, and 7-Chloro-5-(2-chlorophenyl)-3-hydroxy-1,3-dihydro-1,4-benzodiazepin-2-one in (Propane-1,2-diol + Water) at a Temperature of 303.2 K:	https://www.doi.org/10.1021/je900451d
Solubility of CO2 in Alcohols, Glycols, Ethers, and Ketones at High Pressures from (288.15 to 318.15) K:	https://www.doi.org/10.1021/je101344v
Excess Molar Enthalpies of 1,2-Propanediol + Alkan-1-ols (C1-C6) and Their Correlation at 298.15 K and Ambient Pressure (81.5 kPa):	https://www.doi.org/10.1021/je060086x
Phase diagrams for (water + 1,2-propanediol + 2-ethyl-1-hexanol) systems: Experimental data and UNIQUAC:	https://www.doi.org/10.1016/j.jct.2012.06.001
Densities, Viscosities, and Volumetric Properties of Binary Mixtures of 1,2-Propanediol + 1-Heptanol or 1-Hexanol and 1,2-Ethanediol + 2-Butanol or 2-Propanol at T = (298.15, 303.15, and 308.15) K:	https://www.doi.org/10.1021/je900954y
Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Glycols or Poly(Ethylene Glycols) and 2-Phenylethyl Alcohol at 308.15 K and Atmospheric Pressure:	https://www.doi.org/10.1021/je049943s
Solubility of Rofecoxib in the Presence of Aqueous Solutions of Glycerol, Propylene Glycol, Ethanol, Span 20, Tween 80, and Sodium Lauryl Sulfate at (298.15, 303.15, and 308.15) K:	https://www.doi.org/10.1021/je050276s
Methane and carbon dioxide solubility in 1,2-propylene glycol at temperatures ranging from 303 to 423 K and pressures up to 12 MPa:	https://www.doi.org/10.1016/j.fluid.2009.12.006
Experimental study of the excess molar volume of ternary mixtures containing {water + (1,2-propanediol, or 1,3-propanediol, or 1,2-butanediol, or 1,3-butanediol, or 1,4-butanediol, or 2,3-butanediol) + electrolytes} at a temperature of 298.15 K and atmospheric pressure:	https://www.doi.org/10.1016/j.jct.2009.11.018
PρT measurements and derived properties of liquid 1,2-alkanediols:	https://www.doi.org/10.1016/j.jct.2012.08.014
(Liquid + liquid) equilibrium data for the system (propylene glycol + water + tetrabutylammonium 2-naphthalenesulfonate):	https://www.doi.org/10.1016/j.jct.2012.04.002
Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr):	https://www.doi.org/10.1016/j.jct.2008.12.022
Speed of sound in saturated aliphatic alcohols (propan-2-ol, butan-2-ol and 2-methylpropan-1-ol) and alkanediols (ethane-1,2-diol, propane-1,2- and -1,3-diol) at temperature between 293.15 K and 353.15 K and pressures up to 30 MPa:	https://www.doi.org/10.1016/j.jct.2016.06.001
Solubility evaluation and thermodynamic modeling of β-lapachone in water and ten organic solvents at different temperatures:	https://www.doi.org/10.1016/j.fluid.2018.05.005
Solubility of Metoclopramide Hydrochloride in Six Green Solvents at (293.15 to 313.15) K:	https://www.doi.org/10.1021/je500154k
Densities and volumetric properties of (formamide + ethanol, or 1-propanol, or 1,2-ethanediol, or 1,2-propanediol) mixtures at temperatures between 293.15 K and 318.15 K:	https://www.doi.org/10.1016/j.jct.2006.07.021
Determination and correlation of solubility and thermodynamics of mixing of 4-aminobutyric acid in mono-solvents and binary solvent mixtures:	https://www.doi.org/10.1016/j.jct.2016.07.014
Crippen Method:	https://www.chemeo.com/doc/models/crippen_log10ws
Excess molar volume and viscosity deviation for binary mixtures of polyethylene glycol dimethyl ether 250 with 1,2-alkanediols (C3 C6) at T = (293.15 to 328.15) K:	https://www.doi.org/10.1016/j.jct.2008.01.022
Excess properties and isobaric (vapor + liquid) equilibrium at subatmospheric pressures of binary (1,2-propanediol + 1,3-propanediol) system: Measurement and modeling:	https://www.doi.org/10.1016/j.jct.2016.01.019
Solubility of Lamotrigine, Diazepam, Clonazepam, and Phenobarbital in Propylene Glycol + Water Mixtures at 298.15 K:	https://www.doi.org/10.1021/je800931z
Vapor Liquid Equilibria for Water + Propylene Glycols Binary Systems: Experimental Data and Regression:	https://www.doi.org/10.1021/je4009014
Viscosities, Densities, and Refractive Indices of Aqueous Propane-1,3-diol:	https://www.doi.org/10.1021/acs.jced.8b00403
Densities, viscosities, and refractive indices of the binary systems (PEG200 + 1,2-propanediol, +1,3-propanediol) and (PEG400 + 1,2-propanediol, +1,3-propanediol) at (288.15 to 333.15) K and atmospheric pressure:	https://www.doi.org/10.1016/j.jct.2012.07.024
Solubility of (Z)-N-Cyclohexyl-2-(2-hydroxybenzylidine) hydrazine Carbothioamide in Different Pure Solvents at (298.15 to 338.15) K:	https://www.doi.org/10.1021/je5003708
Molar heat capacity of several aqueous solutions of n-[tris(hydroxymethyl)methyl]-3-amino]-propanesulfonic acid (TAPS) + glycol: Measurements and modeling:	https://www.doi.org/10.1016/j.tca.2012.04.006

McGowan Method:	http://link.springer.com/article/10.1007/BF02311772
Thermophysical Properties of Ternary Systems Potassium Formate + Propylene Glycol/Glycerol + Water:	https://www.doi.org/10.1021/acs.jced.8b00742
Equilibrium solubility of sodium 2,4-diaminobenzene sulfonate in liquid mixtures (methanol + water, isopropanol + water, and 1,2-propanediol + water) from 273.15 K to 323.15 K:	https://www.doi.org/10.1016/j.jct.2016.04.004
Solubilities of Carbon Dioxide in Eutectic Mixtures of Choline Chloride and Dihydric Alcohols:	https://www.doi.org/10.1021/je400884v
Volumetric and compressibility properties of liquid water as a solute in glycolic, propylene carbonate, and tetramethylurea solutions at T = 298.15 K:	https://www.doi.org/10.1016/j.jct.2007.05.010
Correlation of Solubility of Bioactive Compound Reserpine in Eight Green Solvents at (298.15 to 338.15) K:	https://www.doi.org/10.1021/je500893g
Experimental determination and modeling of excess molar volumes, viscosities and refractive indices of the binary systems (pyridine + 1-propanol, + 1,2-propanediol, + 1,3-propanediol, and + glycerol). New UNIFAC-VISCO parameters determination:	https://www.doi.org/10.1016/j.jct.2012.06.031
Solubility of Valdecoxib in the Presence of Glyceryl, Propylene Glycol, and Polyethylene Glycol 400 at (298.15 to 318.15) K:	https://www.doi.org/10.1021/je050190z
Heat Capacity of Several Mixed Solvent Desiccants Containing Glycol + Water + NaCl:	https://www.doi.org/10.1016/j.tca.2012.02.017
Thermal conductivity of dry anatase and rutile nano-powders and ethylene and propylene glycol-based TiO2 nanofluids:	https://www.doi.org/10.1016/j.jct.2014.12.001
Solubility and Modeling of Hesperidin in Cosolvent Mixtures of Ethanol, Isopropanol, Propylene Glycol, and n-Propanol + Water:	https://www.doi.org/10.1021/acs.jced.7b00948
Solubility of 1H-1,2,4-Triazole in Ethanol, 1-Propanol, 2-Propanol, 1,2-Propanediol, Ethyl Formate, Methyl Acetate, Ethyl Acetate, and Butyl Acetate at (283 to 363) K:	https://www.doi.org/10.1021/je060452c
Measurement and correlation of the (p, rho, T) behavior of liquid propylene glycol at temperatures from (272.7 to 393.0) K and pressures up to 91.4 MPa:	https://www.doi.org/10.1016/j.jct.2018.10.016
Joback Method:	https://en.wikipedia.org/wiki/Joback_method
Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K:	https://www.doi.org/10.1021/je700499d
Excess volumes and excess heat capacities of {1,2-alkanediol + [illegible]} mixtures and ionic volumes in these systems:	https://www.doi.org/10.1016/j.fluid.2015.05.016
Solubility and dissolution thermodynamics of N'-(4-chlorophenyl)-2-(pyridin-4-ylcarbonyl)hydrazinecarbothioamide in PG + water cosolvent mixtures at (298.15 to 338.15) K:	https://www.doi.org/10.1016/j.tca.2014.08.013
Enthalpies of solution of l-threonine in aqueous alcohol solutions:	https://www.doi.org/10.1016/j.tca.2005.08.031
Vapor-Liquid Equilibrium for Propylene Glycol + 2-(2-Hexyloxyethoxy)ethanol and 1-Methyl-2-pyrrolidone + 1-Methoxypropan-2-ol:	https://www.doi.org/10.1021/je034096z
Solubilities of Menadione Sodium Bisulfite in Water + (Methanol, Ethanol, 1-Propanol, 2-Propanol, 1,2-Propanediol, and Glycerin, Respectively) from (297.67 to 337.76) K:	https://www.doi.org/10.1021/je800022j
Solubility and Thermodynamic Analysis of Tenoxicam in Different Pure Solvents at Different Temperatures:	https://www.doi.org/10.1021/acs.jced.5b00382
Density and vapor pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water):	https://www.doi.org/10.1016/j.jct.2014.08.005
Solubility of Acetylsalicylic Acid in Ethanol, Acetone, Propylene Glycol, and 2-Propanol:	https://www.doi.org/10.1021/je7005693
Solubility of Bioactive Compound Hesperidin in Six Pure Solvents at (298.15 to 333.15) K:	https://www.doi.org/10.1021/je500206w
Heat capacities of the mixed-solvents desiccants (glycols +water + salts):	https://www.doi.org/10.1016/j.tca.2009.01.008
KDB Vapor Pressure Data:	https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=910
Solubility of daidzein in propylene glycol plus water cosolvent mixtures:	https://www.doi.org/10.1016/j.fluid.2013.12.024
Measurement and correlation of excess molar enthalpy for(1,2-propanediol, or 1,3-propanediol, or 1,4-butanediol + water) at the temperatures (298.15, 328.15, and 348.15) K:	https://www.doi.org/10.1016/j.jct.2005.06.018
Study of the Acoustic and Thermodynamic Properties of 1,2- and 1,3-Propanediol by Means of High-Pressure Speed of Sound Measurements at Temperatures from (293 to 318) K and Pressures up to 101 MPa:	https://www.doi.org/10.1021/je7004374
Volume effects for binary mixtures of propane-1,2-diol with methanol, hexan-1-ol or octan-1-ol:	https://www.doi.org/10.1016/j.jct.2012.12.003
Vapor-liquid equilibrium for propylene glycols binary systems: Experimental data and regression:	https://www.doi.org/10.1016/j.fluid.2014.09.015
Solubility of rosuvastatin calcium in different neat solvents at different temperatures:	https://www.doi.org/10.1016/j.jct.2015.11.019
Phase Equilibrium Involving Xylose, Water, and Ethylene Glycol or 1,2-Propylene Glycol at Different Temperatures:	https://www.doi.org/10.1021/acs.jced.8b01128
KDB Pure (Korean Thermophysical Properties Databank):	https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=910
Solubility of 3-Ethyl-5-methyl-(4RS)-2-((2-aminoethoxy)methyl)-4-(2-chlorophenyl)-1,4-dihydro-6-methyl-3,5-pyridinedicarboxylate Monobenzenesulfonate (Amlodipine Besylate) in Ethanol + Water and Propane-1,2-diol + Water Mixtures at Various Temperatures :	https://www.doi.org/10.1021/je3005672
Solubility of CO2 in methanol, ethanol, 1,2-propanediol and glycerol from 283.15 K to 373.15 K and up to 6.0 MPa:	https://www.doi.org/10.1016/j.jct.2019.05.003
The Yaws Handbook of Vapor Pressure:	https://www.sciencedirect.com/book/9780128029992/the-yaws-handbook-of-vapor-pressure
Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15–313.15) K:	https://www.doi.org/10.1016/j.fluid.2013.06.041
Thermodynamic and transport properties of acetonitrile + alkanediols liquid mixtures at different temperatures: experimental measurements and modeling:	https://www.doi.org/10.1016/j.jct.2017.06.004
Densities, Dynamic Viscosities, Speeds of Sound, and Relative Permittivities for Water + Alkanediols (Propane-1,2- and -1,3-diol and Butane-1,2-, -1,3-, -1,4-, and -2,3-Diol) at Different Temperatures:	https://www.doi.org/10.1021/je0340755
Measurement and Correlation of Tadalafil Solubility in Five Pure Solvents at (298.15 to 333.15) K:	https://www.doi.org/10.1021/je400982r
Solubilities of 2-Methyl-1,4-naphthoquinone in Water + (Methanol, Ethanol, 1-Propanol, 2-Propanol, 1,2-Propanediol, and Glycerin, Respectively) from (293.15 to 337.92) K:	https://www.doi.org/10.1021/je7002989
Enthalpies of dilution of formamide in aqueous alcohol solutions at 298.15K:	https://www.doi.org/10.1016/j.tca.2007.10.006

Phase Equilibrium and Physical Properties for the Purification of Propylene Carbonate (PC) and 1,2-Butylene Oxide (1,2-BO):	https://www.doi.org/10.1021/je100803e
Densities, surface tensions, and isobaric vapor–liquid equilibria for the mixtures of 2-propanol, water, and 1,2-propanediol:	https://www.doi.org/10.1016/j.fluid.2014.12.040
Liquid–liquid equilibrium data for binary systems containing o-dichlorobenzene and nitrobenzene:	https://www.doi.org/10.1016/j.fluid.2014.11.012
Measurement and correlation of the solubility of florfenicol in binary 1,2-propanediol + water mixtures from 293.15 to 318.25 K:	https://www.doi.org/10.1016/j.fluid.2013.09.020
Partial molar volumes of organic solutes in water XV. Polyhydric alcohols derived from ethane and propane at temperatures from 298.15 to 393.15 K and at pressures up to 30 MPa:	https://www.doi.org/10.1016/j.jct.2005.08.015
Solubility of N-(4-Chlorophenyl)-2-(pyridin-4-ylcarbonyl)hydrazinecarbothioamide in Selected Monosolvents and Binary Solvents at (298.15 to 333.15) K:	https://www.doi.org/10.1021/je500457p
Thermodynamic and spectroscopic investigation of molecular interactions of thiourea + alcohol binary mixtures:	https://www.doi.org/10.1016/j.jct.2016.07.005
Solubility and thermodynamic function of a bioactive compound bergenin in various pharmaceutically acceptable neat solvents at different temperatures:	https://www.doi.org/10.1016/j.jct.2016.05.003
NIST Webbook:	http://webbook.nist.gov/cgi/cbook.cgi?ID=C57556&Units=SI
Solubility of sulfapyridine in propylene glycol + water mixtures and correlation with the Jouyban Acree model:	https://www.doi.org/10.1016/j.fluid.2012.12.017
Solid–Liquid Equilibria of 1-Ethyl-3-methylimidazolium Hexafluorophosphate + Polyols:	https://www.doi.org/10.1021/je301265w
Solubilities of Isonicotinic Acid in (Methanol, Ethanol, 1-Propanol, 2-Propanol, and 1,2-Propanediol, Respectively) from (289.65 to 358.75) K:	https://www.doi.org/10.1021/je800824h

Legend

chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
gf:	Standard Gibbs free energy of formation
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
speedsl:	Speed of sound in fluid
tb:	Normal Boiling Point Temperature
tc:	Critical Temperature
tcondl:	Liquid thermal conductivity

tf:	Normal melting (fusion) point
vc:	Critical Volume
vols:	Specific Volume
zc:	Critical Compressibility