

Acetic acid, 2-methylpropyl ester

Other names:	2-METHYLPROPYL ESTER ACETIC ACID 2-Methyl-1-propanol, acetate 2-Methyl-1-propyl acetate 2-Methylpropyl acetate 2-methylpropyl ethanoate Acetate d'isobutyle Isobutyl acetate fcc Isobutylester kyseliny octove NSC 8035 UN 1213 acetic acid, isobutyl ester ethanoic acid, isobutyl ester i-Butyl acetate isobutyl acetate isobutyl ethanoate «beta»-Methylpropyl ethanoate
Inchi:	InChI=1S/C6H12O2/c1-5(2)4-8-6(3)7/h5H,4H2,1-3H3
InchiKey:	GJRQTCIYDGXPES-UHFFFAOYSA-N
Formula:	C6H12O2
SMILES:	CC(=O)OCC(C)C
Mol. weight [g/mol]:	116.16
CAS:	110-19-0

Physical Properties

Property code	Value	Unit	Source
af	0.4550		KDB
aigt	695.93	K	KDB
chl	-3534.00	kJ/mol	NIST Webbook
dm	1.90	debye	KDB
fil	2.40	% in Air	KDB
flu	10.50	% in Air	KDB
fpc	302.59	K	KDB
fpo	289.82	K	KDB
gf	-236.72	kJ/mol	Joback Method
hf	-495.50	kJ/mol	KDB
hfus	10.56	kJ/mol	Joback Method
hvap	35.90 ± 0.04	kJ/mol	NIST Webbook

ie	9.97	eV	NIST Webbook
log10ws	-1.21		Estimated Solubility Method
log10ws	-1.21		Aqueous Solubility Prediction Method
logp	1.206		Crippen Method
mcvol	102.840	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=1)		KDB
pc	3010.00 ± 20.00	kPa	NIST Webbook
pc	3160.00	kPa	KDB
pc	3180.00 ± 60.79	kPa	NIST Webbook
rhoc	281.10 ± 8.13	kg/m3	NIST Webbook
rinpol	758.00		NIST Webbook
rinpol	782.00		NIST Webbook
rinpol	741.00		NIST Webbook
rinpol	741.00		NIST Webbook
rinpol	781.00		NIST Webbook
rinpol	779.00		NIST Webbook
rinpol	756.00		NIST Webbook
rinpol	755.00		NIST Webbook
rinpol	755.00		NIST Webbook
rinpol	755.00		NIST Webbook
rinpol	770.00		NIST Webbook
rinpol	745.30		NIST Webbook
rinpol	748.40		NIST Webbook
rinpol	749.70		NIST Webbook
rinpol	752.10		NIST Webbook
rinpol	749.80		NIST Webbook
rinpol	748.70		NIST Webbook
rinpol	754.45		NIST Webbook
rinpol	754.00		NIST Webbook
rinpol	754.00		NIST Webbook
rinpol	747.00		NIST Webbook
rinpol	746.00		NIST Webbook
rinpol	750.00		NIST Webbook
rinpol	750.00		NIST Webbook
rinpol	748.00		NIST Webbook
rinpol	749.00		NIST Webbook
rinpol	749.00		NIST Webbook
rinpol	782.00		NIST Webbook
rinpol	780.00		NIST Webbook
rinpol	786.00		NIST Webbook
rinpol	763.00		NIST Webbook
rinpol	776.00		NIST Webbook

rinpol	768.00	NIST Webbook
rinpol	771.00	NIST Webbook
rinpol	757.00	NIST Webbook
rinpol	766.00	NIST Webbook
rinpol	734.00	NIST Webbook
rinpol	749.00	NIST Webbook
rinpol	770.00	NIST Webbook
rinpol	770.00	NIST Webbook
rinpol	767.00	NIST Webbook
rinpol	779.50	NIST Webbook
rinpol	757.00	NIST Webbook
rinpol	764.00	NIST Webbook
rinpol	760.00	NIST Webbook
rinpol	760.00	NIST Webbook
rinpol	770.00	NIST Webbook
rinpol	753.00	NIST Webbook
rinpol	744.00	NIST Webbook
rinpol	745.00	NIST Webbook
rinpol	743.00	NIST Webbook
rinpol	744.00	NIST Webbook
rinpol	754.00	NIST Webbook
rinpol	758.00	NIST Webbook
rinpol	764.00	NIST Webbook
rinpol	764.00	NIST Webbook
rinpol	758.00	NIST Webbook
rinpol	730.00	NIST Webbook
rinpol	780.00	NIST Webbook
rinpol	767.20	NIST Webbook
rinpol	771.00	NIST Webbook
rinpol	772.00	NIST Webbook
rinpol	781.00	NIST Webbook
rinpol	768.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	772.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	768.00	NIST Webbook
rinpol	758.00	NIST Webbook
rinpol	753.00	NIST Webbook
rinpol	767.00	NIST Webbook
rinpol	772.00	NIST Webbook
rinpol	753.00	NIST Webbook
rinpol	758.00	NIST Webbook
rinpol	775.00	NIST Webbook
rinpol	749.00	NIST Webbook

rinpol	758.00	NIST Webbook
rinpol	759.00	NIST Webbook
rinpol	762.00	NIST Webbook
rinpol	762.00	NIST Webbook
rinpol	759.00	NIST Webbook
rinpol	754.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	755.00	NIST Webbook
rinpol	748.00	NIST Webbook
rinpol	758.00	NIST Webbook
rinpol	749.00	NIST Webbook
rinpol	746.00	NIST Webbook
rinpol	748.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	753.00	NIST Webbook
rinpol	730.00	NIST Webbook
rinpol	781.00	NIST Webbook
rinpol	768.00	NIST Webbook
rinpol	753.00	NIST Webbook
rinpol	759.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	746.00	NIST Webbook
rinpol	780.00	NIST Webbook
rinpol	771.00	NIST Webbook
rinpol	788.00	NIST Webbook
rinpol	783.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	764.00	NIST Webbook
rinpol	760.00	NIST Webbook
rinpol	758.00	NIST Webbook
rinpol	763.00	NIST Webbook
rinpol	764.00	NIST Webbook
rinpol	763.00	NIST Webbook
rinpol	764.00	NIST Webbook
rinpol	762.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	758.00	NIST Webbook
rinpol	768.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	757.20	NIST Webbook
rinpol	755.00	NIST Webbook
rinpol	757.00	NIST Webbook
rinpol	758.98	NIST Webbook
rinpol	757.70	NIST Webbook

ripol	1002.00	NIST Webbook
ripol	1010.00	NIST Webbook
ripol	1032.00	NIST Webbook
ripol	1025.00	NIST Webbook
ripol	984.00	NIST Webbook
ripol	1023.00	NIST Webbook
ripol	1023.00	NIST Webbook
ripol	1023.00	NIST Webbook
ripol	1020.00	NIST Webbook
ripol	1000.00	NIST Webbook
ripol	1020.00	NIST Webbook
ripol	1020.00	NIST Webbook
ripol	987.00	NIST Webbook
ripol	1020.00	NIST Webbook
ripol	1020.00	NIST Webbook
ripol	1017.00	NIST Webbook
ripol	985.00	NIST Webbook
ripol	1024.00	NIST Webbook
ripol	976.00	NIST Webbook
ripol	1012.00	NIST Webbook
ripol	1012.00	NIST Webbook
ripol	1020.00	NIST Webbook
ripol	1019.00	NIST Webbook
ripol	1047.00	NIST Webbook
ripol	1014.00	NIST Webbook
ripol	1014.00	NIST Webbook
ripol	1011.00	NIST Webbook
ripol	1010.00	NIST Webbook
ripol	1017.00	NIST Webbook
ripol	1009.00	NIST Webbook
ripol	1009.00	NIST Webbook
ripol	1005.00	NIST Webbook
ripol	1005.00	NIST Webbook
ripol	1025.00	NIST Webbook
ripol	1011.00	NIST Webbook
ripol	1025.00	NIST Webbook
ripol	1013.00	NIST Webbook
ripol	1033.00	NIST Webbook
ripol	1018.00	NIST Webbook
ripol	1020.00	NIST Webbook
ripol	1029.00	NIST Webbook
ripol	1005.00	NIST Webbook
ripol	1017.00	NIST Webbook
ripol	1000.00	NIST Webbook

ripol	1031.00		NIST Webbook
ripol	1029.00		NIST Webbook
ripol	1022.00		NIST Webbook
ripol	1002.00		NIST Webbook
ripol	1007.00		NIST Webbook
ripol	1027.00		NIST Webbook
ripol	989.00		NIST Webbook
ripol	986.00		NIST Webbook
ripol	1014.00		NIST Webbook
ripol	993.00		NIST Webbook
ripol	1012.00		NIST Webbook
ripol	1013.00		NIST Webbook
ripol	1019.00		NIST Webbook
ripol	1011.00		NIST Webbook
ripol	1009.00		NIST Webbook
ripol	1009.00		NIST Webbook
ripol	1012.00		NIST Webbook
ripol	1007.00		NIST Webbook
ripol	1018.00		NIST Webbook
ripol	1016.00		NIST Webbook
ripol	1034.00		NIST Webbook
ripol	1014.00		NIST Webbook
ripol	1012.00		NIST Webbook
ripol	1009.00		NIST Webbook
ripol	1009.00		NIST Webbook
ripol	1035.00		NIST Webbook
ripol	985.00		NIST Webbook
ripol	1015.00		NIST Webbook
ripol	1004.00		NIST Webbook
ripol	1032.00		NIST Webbook
ripol	1008.00		NIST Webbook
ripol	1000.00		NIST Webbook
ripol	1009.00		NIST Webbook
ripol	1000.00		NIST Webbook
ripol	998.00		NIST Webbook
ripol	988.00		NIST Webbook
ripol	988.00		NIST Webbook
ripol	992.00		NIST Webbook
ripol	1005.00		NIST Webbook
ripol	1000.00		NIST Webbook
ripol	1005.00		NIST Webbook
tb	390.40 ± 0.50	K	NIST Webbook
tb	389.70	K	KDB
tb	389.20 ± 1.50	K	NIST Webbook

tb	390.40	K	NIST Webbook
tb	389.44	K	Isobaric VLE at 0.6 MPa for binary systems isobutyl acetate + ethanol, + 1-propanol or + 2-propanol
tb	389.55	K	Vapour-liquid equilibrium measurements and extractive distillation process design for separation of azeotropic mixture (dimethyl carbonate + ethanol)
tb	389.90	K	Isobaric Vapor Liquid Equilibrium for the Binary and Ternary System with Isobutyl Alcohol, Isobutyl Acetate and Dimethyl Sulfoxide at 101.3 kPa
tb	389.75	K	Measurement and Correlation of Isobaric Vapor-Liquid Equilibrium for Binary Systems of Allyl Alcohol with Isobutyl Acetate, Butyl Acetate, and Butyl Propionate at 101.3 kPa
tb	390.00	K	NIST Webbook
tb	390.20 ± 0.50	K	NIST Webbook
tb	389.55	K	Isobaric Vapor-Liquid Equilibrium Measurements for Separation of Azeotrope (Methanol + Methyl Acetate)
tb	389.00 ± 3.00	K	NIST Webbook
tb	390.45	K	NIST Webbook
tb	390.15 ± 1.00	K	NIST Webbook
tb	385.15 ± 2.00	K	NIST Webbook
tb	390.55 ± 2.00	K	NIST Webbook
tb	388.90 ± 1.50	K	NIST Webbook
tb	390.00 ± 2.00	K	NIST Webbook
tb	388.90 ± 1.00	K	NIST Webbook
tb	391.15 ± 2.00	K	NIST Webbook
tb	390.30 ± 1.50	K	NIST Webbook
tb	388.85 ± 2.00	K	NIST Webbook
tb	389.65 ± 2.00	K	NIST Webbook
tb	390.40 ± 0.40	K	NIST Webbook
tb	389.40 ± 2.00	K	NIST Webbook
tb	390.40 ± 0.50	K	NIST Webbook
tb	390.35 ± 2.00	K	NIST Webbook
tb	389.25 ± 2.00	K	NIST Webbook
tb	390.00 ± 2.00	K	NIST Webbook
tb	390.55 ± 0.50	K	NIST Webbook
tb	390.60 ± 0.50	K	NIST Webbook

tb	390.25 ± 2.00	K	NIST Webbook
tb	387.90 ± 2.00	K	NIST Webbook
tc	561.00	K	KDB
tc	560.80 ± 0.60	K	NIST Webbook
tc	561.50 ± 2.00	K	NIST Webbook
tc	569.00 ± 5.00	K	NIST Webbook
tf	174.30	K	KDB
tf	174.25	K	Aqueous Solubility Prediction Method
tf	176.05	K	NIST Webbook
tf	176.10 ± 0.60	K	NIST Webbook
tf	240.15 ± 0.50	K	NIST Webbook
vc	0.414	m3/kmol	KDB
zc	0.2804710		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	199.90	J/mol×K	412.53	Joback Method
cpg	255.87	J/mol×K	594.22	Joback Method
cpg	247.38	J/mol×K	563.94	Joback Method
cpg	238.55	J/mol×K	533.66	Joback Method
cpg	229.39	J/mol×K	503.38	Joback Method
cpg	219.89	J/mol×K	473.09	Joback Method
cpg	210.06	J/mol×K	442.81	Joback Method
cpl	240.20	J/mol×K	290.00	NIST Webbook
dvisc	0.0046134	Pa×s	214.54	Joback Method
dvisc	0.0002624	Pa×s	412.53	Joback Method
dvisc	0.0003438	Pa×s	379.53	Joback Method
dvisc	0.0004742	Pa×s	346.53	Joback Method
dvisc	0.0006998	Pa×s	313.53	Joback Method
dvisc	0.0011317	Pa×s	280.54	Joback Method
dvisc	0.0020807	Pa×s	247.54	Joback Method
hvapt	39.80	kJ/mol	321.50	NIST Webbook
hvapt	39.20	kJ/mol	359.00	NIST Webbook
hvapt	39.90	kJ/mol	349.50	NIST Webbook

pvap	101.30	kPa	389.55	Vapour-liquid equilibrium measurements and extractive distillation process design for separation of azeotropic mixture (dimethyl carbonate + ethanol)
rfi	1.38760		298.15	Phase equilibria in the ternary system isobutyl alcohol + isobutyl acetate + 1-hexanol and the binary systems isobutyl alcohol + 1-hexanol, isobutyl acetate + 1-hexanol at 101.3 kPa
rfi	1.38760		298.15	Liquid liquid equilibria of the systems isobutyl acetate + isobutyl alcohol + water and isobutyl acetate + isobutyl alcohol + glycerol at different temperatures
rfi	1.39020		293.15	Measurement and Correlation of Phase Equilibria for Isobutyl Acetate + {Ethanol or Methanol} + Water at 303.15 and 323.15 K
rfi	1.38760		298.15	Isobaric vapor-liquid equilibria for the binary systems isobutyl alcohol + isobutyl acetate and tert-butyl alcohol + tert-butyl acetate at 20 and 101.3 kPa

rfi	1.38760		298.15	Phase equilibria in the systems isobutyl alcohol +N,N-dimethylformamide, isobutyl acetate +N,N-dimethylformamide and isobutyl alcohol + isobutyl acetate +N,N-dimethylformamide at 101.3 kPa
rfi	1.39050		293.15	Isobaric Vapor Liquid Equilibrium for Binary Systems of Thioglycolic Acid with Water, Butyl Acetate, Butyl Formate, and Isobutyl Acetate at 101.3 kPa
rfi	1.38760		298.15	Vapor liquid equilibria in the ternary system isobutyl alcohol + isobutyl acetate + butyl propionate and the binary systems isobutyl alcohol + butyl propionate, isobutyl acetate + butyl propionate at 101.3 kPa
rfi	1.38780		298.20	Tie-line data for the aqueous solutions of phenol with organic solvents at T = 298.2 K
rfi	1.38760		298.15	Study of liquid liquid equilibrium of the systems isobutyl acetate + acetic acid +water and isobutyl alcohol + acetic acid +water at different temperatures
rhoI	875.00	kg/m3	293.00	KDB
rhoI	849.39	kg/m3	313.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa

rhoI	871.30	kg/m3	293.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
srf	0.02	N/m	308.15	Excess Molar Volumes and Surface Tensions of 1,2,4-Trimethylbenzene and 1,3,5-Trimethylbenzene with Isopropyl Acetate and Isobutyl Acetate at (298.15, 308.15, and 313.15) K
srf	0.02	N/m	298.15	Excess Molar Volumes and Surface Tensions of 1,2,4-Trimethylbenzene and 1,3,5-Trimethylbenzene with Isopropyl Acetate and Isobutyl Acetate at (298.15, 308.15, and 313.15) K
srf	0.02	N/m	313.15	Excess Molar Volumes and Surface Tensions of 1,2,4-Trimethylbenzene and 1,3,5-Trimethylbenzene with Isopropyl Acetate and Isobutyl Acetate at (298.15, 308.15, and 313.15) K

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
---------------	-------	------	----------------	--------

tbp	361.00	K	39.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	367.41	K	49.98	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	372.89	K	59.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	377.39	K	70.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	381.58	K	80.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	385.54	K	90.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	389.37	K	100.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	392.35	K	110.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	395.26	K	120.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	

tdp	398.16	K	130.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tdp	400.84	K	140.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tdp	403.64	K	150.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.50519e+01
Coeff. B	-3.64415e+03
Coeff. C	-4.07290e+01
Temperature range (K), min.	287.55
Temperature range (K), max.	414.85

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C*\ln(T) + D*T^2$
Coeff. A	9.01223e+01
Coeff. B	-7.87047e+03
Coeff. C	-1.11424e+01
Coeff. D	7.93342e-06
Temperature range (K), min.	174.30
Temperature range (K), max.	561.00

Sources

Estimated Solubility Method:

Solution thermodynamics of simvastatin in pure solvents and binary solvent mixtures
Solubility of Naphthalene in Isobutyl Acetate, n-Butyric Acid, Ethyl Acetate, and Methyl Ethyl Ketone
Nonidealities of Benzene-Carboxylic Acids in Isobutyl Acetate and n-Butyric Acid-Liquid Equilibrium Measurements for Separation of Amino Acids from Organic Solutions
Solubility of phenol with organic solvents at T = 298.15 K
Solubility of Benzoic Acid and Aspirin in Pure Solvents Using Focused Beam Reflective Measurement

Isobaric Vapor Liquid Equilibrium for the Binary and Ternary System with Isobutyl Alcohol + Isobutyl Acetate and Systems Acetic Acid + Water + Butyl Alcohol and Acetic Acid + Water + Isobutyl Alcohol for Ternary Liquid + Vapor Equilibrium for Ternary Liquid + Vapor at 101.3 K, 200.0 kPa and 308.15 K. Thermodynamic Properties of Organic Compounds and Organic Solutions with Their Resolved Long-Chain Aliphatic Alcohol and the Gas Phase as a Function of Temperature. Binary systems isobutyl acetate + ethanol, + Liquid-Liquid Equilibrium of Isobutyl Acetate + Isobutyl Alcohol + Propanol or 2-propanol. Solubility of Based on Liquids at 298.15 and 308.15 K: Isobaric Vapor Liquid Equilibrium for Binary Systems of Thioglycolic Acid + Water, Butyl Acetate, Butyl Methacrylate and Correlation of Phase Equilibrium of Isobutyl Acetate at 101.3 kPa and of Methanol + Water at 303.15 and 323.15 K: KDB:

Vapor liquid equilibria in the ternary system isobutyl alcohol + isobutyl acetate + butyl propionate and the binary systems isobutyl alcohol + butyl propionate, isobutyl acetate + butyl propionate at 101.3 kPa:

Isobaric vapor-liquid equilibria for the binary systems isobutyl alcohol + isobutyl acetate and tert-butyl alcohol + isobutyl acetate at 20 and 101.3 kPa: Liquid-liquid equilibria of the systems isobutyl acetate + isobutyl alcohol and tert-butyl alcohol + isobutyl alcohol and isobutyl alcohol + isobutyl acetate in water + (isobutyl acetate + isobutyl acetate): Dioxide + Isopropyl, Isobutyl, and German Methods:

(Liquid + liquid) equilibria in ternary aqueous mixtures of phosphoric acid measurement and correlation at 298.2 K: Isobaric Vapor-Liquid Equilibrium for Base Determination of Binary Vapor-Liquid Equilibrium of CO₂-Based and Non-CO₂-Based Acidic Aqueous Phases of Water + Prop-2-enoic Acid + Isobutyl Binadate at Different Temperatures of the Water - Propionic Acid - Isobutyl Acetate and Equilibrium of Benzyl and Methyls of Acetates in the Direct Esterification of Propionic Acid Using Di-(2-ethylhexyl)phosphoric Acid from Molar Ratios of Acetic Acid and Benzyl 2,4-Trimethylbenzene and 1,3,5-Trimethylbenzene of the Esters of Isobutyl and Propionic Acid at (298.15, 308.15 and 313.15) K: acetic acid + water at different temperatures:

http://pubs.acs.org/doi/suppl/10.1021/ci034243x/suppl_file/ci034243xsi20040112_053635.txt

<https://www.doi.org/10.1016/j.fluid.2015.07.055>

<https://www.doi.org/10.1021/je800428r>

<https://www.doi.org/10.1021/je101319f>

<https://www.doi.org/10.1021/acs.jced.8b00807>

<https://www.doi.org/10.1016/j.jct.2012.10.028>

<https://www.doi.org/10.1021/acs.jced.5b00746>

https://en.wikipedia.org/wiki/Joback_method

<https://www.doi.org/10.1021/acs.jced.7b00241>

<https://www.doi.org/10.1021/je6005746>

<https://www.doi.org/10.1016/j.ijct.2017.06.015>

<https://www.doi.org/10.1021/je050368h>

<https://www.doi.org/10.1016/j.fluid.2012.06.013>

<https://www.doi.org/10.1021/acs.jced.8b01045>

<https://www.doi.org/10.1016/j.fluid.2012.06.011>

<https://www.doi.org/10.1021/acs.jced.6b00686>

<https://www.doi.org/10.1021/acs.jced.6b00949>

<https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=1080>

<https://www.chemic.org/files/research/kdb/mol/mol1080.mol>

<https://www.doi.org/10.1016/j.fluid.2005.09.015>

<http://link.springer.com/article/10.1007/BF02311772>

<http://onschallenge.wikispaces.com/file/view/AqueousDataset002.xlsx/351826032/AqueousDataset002.xlsx>

<http://webbook.nist.gov/cgi/cbook.cgi?ID=C110190&Units=SI>

<https://www.doi.org/10.1016/j.fluid.2004.10.022>

<https://www.sciencedirect.com/book/9780128029992/the-yaws-handbook-of-vapor-pressure>

<https://www.doi.org/10.1016/j.fluid.2008.01.010>

<https://www.doi.org/10.1016/j.fluid.2011.03.006>

<https://www.doi.org/10.1021/ie060321b>

<http://pubs.acs.org/doi/abs/10.1021/cj990307l>

<https://www.doi.org/10.1016/j.ijct.2010.01.001>

<https://www.doi.org/10.1021/acs.jced.7b01024>

<https://www.doi.org/10.1021/ie501023n>

<https://www.doi.org/10.1021/je2003226>

<https://www.doi.org/10.1016/j.tca.2012.04.020>

<https://www.doi.org/10.1021/acs.jced.6b00221><https://www.doi.org/10.1021/acs.jced.7b00797>

<https://www.doi.org/10.1021/je800046k>

<https://www.doi.org/10.1016/j.fluid.2008.07.001>

Liquid-liquid equilibrium determination and thermodynamics modeling for <https://www.doi.org/10.1016/j.fluid.2017.11.010>
 Vapor-liquid equilibrium from its <https://www.doi.org/10.1016/j.jct.2019.01.027>
 measurements and extractive <https://www.doi.org/10.1016/j.fluid.2005.03.014>
 distillation process design for <https://www.doi.org/10.1016/j.fluid.2013.12.026>
 isobutyl alcohol-oleotropic mixture <https://www.doi.org/10.1016/j.fluid.2009.03.006>
 Phase equilibria and thermodynamic <https://www.doi.org/10.1016/j.fluid.2018.02.003>
 properties of the binary system <https://www.doi.org/10.1016/j.fluid.2005.06.019>
 acetic acid + isobutyl acetate + <https://www.doi.org/10.1021/je800120p>
 isobutyl alcohol (1) + isobutyl acetate <https://www.doi.org/10.1021/je800120p>
 + N,N-dimethylformamide at 101.3 kPa: <https://www.doi.org/10.1021/je800120p>
 Solubility and limiting activity <https://www.doi.org/10.1021/je800120p>
 coefficient of simvastatin in different <https://www.doi.org/10.1021/je800120p>
 liquid solvents <https://www.doi.org/10.1021/je800120p>
 Equilibrium data for <https://www.doi.org/10.1021/je800120p>
 ternary systems of water + acetic acid + <https://www.doi.org/10.1021/je800120p>
 acetone at 203.2 and 303.2 K <https://www.doi.org/10.1021/je800120p>
 Phase equilibria in the ternary system <https://www.doi.org/10.1021/je800120p>
 isobutyl alcohol + isobutyl acetate + <https://www.doi.org/10.1021/je800120p>
 2-butanone and the binary systems <https://www.doi.org/10.1021/je800120p>
 Acetate, n-Propyl Acetate, Isobutyl <https://www.doi.org/10.1021/je800120p>
 Acetate, n-Propyl Acetate, Isobutyl <https://www.doi.org/10.1021/je800120p>
 Acetate, Isobutyl Acetate, tert-Butyl <https://www.doi.org/10.1021/je800120p>
 Acetate, and 2-Butanone, between (285 <https://www.doi.org/10.1021/je800120p>
 and 323) K <https://www.doi.org/10.1021/je800120p>

Legend

af:	Acentric Factor
aigt:	Autoignition Temperature
chl:	Standard liquid enthalpy of combustion
cp _g :	Ideal gas heat capacity
c _p _l :	Liquid phase heat capacity
dm:	Dipole Moment
d _{visc} :	Dynamic viscosity
fl:	Lower Flammability Limit
flu:	Upper Flammability Limit
f _{pc} :	Flash Point (Closed Cup Method)
f _{po} :	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
hf:	Enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
h _{vap} :	Enthalpy of vaporization at standard conditions
h _{vapt} :	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log ₁₀ ws:	Log10 of Water solubility in mol/l
log _p :	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
p _{vap} :	Vapor pressure
r _{fi} :	Refractive Index
rhoc:	Critical density
rho _l :	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices

srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tbp:	Boiling point at given pressure
tc:	Critical Temperature
tf:	Normal melting (fusion) point
vc:	Critical Volume
zc:	Critical Compressibility

Latest version available from:

<https://www.cheméo.com/cid/23-647-8/Acetic-acid-2-methylpropyl-ester.pdf>

Generated by Cheméo on 2026-07-21 20:18:31.417472855 +0000 UTC m=+176207.259358231.

Cheméo (<https://www.cheméo.com>) is the biggest free database of chemical and physical data for the process industry.