

Isobutyl acetate

Other names:	2-METHYL-1-PROPYL ACETATE 2-METHYLPROPYL ESTER ACETIC ACID 2-Methyl-1-propanol, acetate 2-Methylpropyl acetate 2-Methylpropyl ethanoate Acetate d'isobutyle Acetic acid, 2-methylpropyl ester Acetic acid, isobutyl ester ISOBUTYL ETHANOATE Isobutyl acetate fcc Isobutylester kyseliny octove NSC 8035 UN 1213 ethanoic acid, isobutyl ester i-Butyl acetate «beta»-Methylpropyl ethanoate Â«betaÂ»-Methylpropyl ethanoate
Inchi:	InChI=1S/C6H12O2/c1-5(2)4-8-6(3)7/h5H,4H2,1-3H3
InchiKey:	GJRQTCIYDGXPES-UHFFFAOYSA-N
Formula:	C6H12O2
SMILES:	CC(=O)OCC(C)C
Mol. weight [g/mol]:	116.16
CAS:	110-19-0

Physical Properties

Property code	Value	Unit	Source
af	0.4550		KDB
aigt	695.93	K	KDB
chl	-3534.00	kJ/mol	NIST Webbook
dm	1.90	debye	KDB
fll	2.40	% in Air	KDB
flu	10.50	% in Air	KDB
fpc	302.59	K	KDB
fpo	289.82	K	KDB
gf	-236.72	kJ/mol	Joback Method
hf	-495.50	kJ/mol	KDB
hfus	10.56	kJ/mol	Joback Method

hvap	35.90 ± 0.04	kJ/mol	NIST Webbook
ie	9.97	eV	NIST Webbook
log10ws	-1.21		Aqueous Solubility Prediction Method
log10ws	-1.21		Estimated Solubility Method
logp	1.205		Crippen Method
mcvol	102.840	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=1)		KDB
pc	3180.00 ± 60.79	kPa	NIST Webbook
pc	3010.00 ± 20.00	kPa	NIST Webbook
pc	3160.00	kPa	KDB
rhoc	281.10 ± 8.13	kg/m3	NIST Webbook
rinpol	741.00		NIST Webbook
rinpol	771.00		NIST Webbook
rinpol	780.00		NIST Webbook
rinpol	753.00		NIST Webbook
rinpol	750.00		NIST Webbook
rinpol	748.00		NIST Webbook
rinpol	746.00		NIST Webbook
rinpol	730.00		NIST Webbook
rinpol	749.00		NIST Webbook
rinpol	758.00		NIST Webbook
rinpol	748.00		NIST Webbook
rinpol	755.00		NIST Webbook
rinpol	750.00		NIST Webbook
rinpol	754.00		NIST Webbook
rinpol	759.00		NIST Webbook
rinpol	762.00		NIST Webbook
rinpol	762.00		NIST Webbook
rinpol	759.00		NIST Webbook
rinpol	758.00		NIST Webbook
rinpol	749.00		NIST Webbook
rinpol	781.00		NIST Webbook
rinpol	758.00		NIST Webbook
rinpol	753.00		NIST Webbook
rinpol	772.00		NIST Webbook
rinpol	767.00		NIST Webbook
rinpol	753.00		NIST Webbook
rinpol	758.00		NIST Webbook
rinpol	768.00		NIST Webbook
rinpol	750.00		NIST Webbook
rinpol	772.00		NIST Webbook
rinpol	750.00		NIST Webbook

rinpol	768.00	NIST Webbook
rinpol	781.00	NIST Webbook
rinpol	772.00	NIST Webbook
rinpol	771.00	NIST Webbook
rinpol	782.00	NIST Webbook
rinpol	780.00	NIST Webbook
rinpol	730.00	NIST Webbook
rinpol	758.00	NIST Webbook
rinpol	764.00	NIST Webbook
rinpol	764.00	NIST Webbook
rinpol	758.00	NIST Webbook
rinpol	754.00	NIST Webbook
rinpol	744.00	NIST Webbook
rinpol	743.00	NIST Webbook
rinpol	745.00	NIST Webbook
rinpol	744.00	NIST Webbook
rinpol	758.00	NIST Webbook
rinpol	770.00	NIST Webbook
rinpol	760.00	NIST Webbook
rinpol	760.00	NIST Webbook
rinpol	764.00	NIST Webbook
rinpol	757.00	NIST Webbook
rinpol	779.50	NIST Webbook
rinpol	767.00	NIST Webbook
rinpol	770.00	NIST Webbook
rinpol	770.00	NIST Webbook
rinpol	749.00	NIST Webbook
rinpol	734.00	NIST Webbook
rinpol	766.00	NIST Webbook
rinpol	757.00	NIST Webbook
rinpol	771.00	NIST Webbook
rinpol	768.00	NIST Webbook
rinpol	776.00	NIST Webbook
rinpol	763.00	NIST Webbook
rinpol	786.00	NIST Webbook
rinpol	780.00	NIST Webbook
rinpol	782.00	NIST Webbook
rinpol	749.00	NIST Webbook
rinpol	755.00	NIST Webbook
rinpol	749.00	NIST Webbook
rinpol	748.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	746.00	NIST Webbook

rinpol	747.00	NIST Webbook
rinpol	754.00	NIST Webbook
rinpol	754.00	NIST Webbook
rinpol	754.45	NIST Webbook
rinpol	748.70	NIST Webbook
rinpol	749.80	NIST Webbook
rinpol	752.10	NIST Webbook
rinpol	748.40	NIST Webbook
rinpol	745.30	NIST Webbook
rinpol	770.00	NIST Webbook
rinpol	755.00	NIST Webbook
rinpol	755.00	NIST Webbook
rinpol	755.00	NIST Webbook
rinpol	756.00	NIST Webbook
rinpol	779.00	NIST Webbook
rinpol	768.00	NIST Webbook
rinpol	753.00	NIST Webbook
rinpol	759.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	781.00	NIST Webbook
rinpol	746.00	NIST Webbook
rinpol	757.70	NIST Webbook
rinpol	758.98	NIST Webbook
rinpol	757.00	NIST Webbook
rinpol	749.70	NIST Webbook
rinpol	757.20	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	768.00	NIST Webbook
rinpol	758.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	762.00	NIST Webbook
rinpol	764.00	NIST Webbook
rinpol	763.00	NIST Webbook
rinpol	764.00	NIST Webbook
rinpol	763.00	NIST Webbook
rinpol	758.00	NIST Webbook
rinpol	760.00	NIST Webbook
rinpol	764.00	NIST Webbook
rinpol	750.00	NIST Webbook
rinpol	783.00	NIST Webbook
rinpol	788.00	NIST Webbook
rinpol	753.00	NIST Webbook
rinpol	767.20	NIST Webbook
rinpol	741.00	NIST Webbook

ripol	775.00	NIST Webbook
ripol	1011.00	NIST Webbook
ripol	1025.00	NIST Webbook
ripol	984.00	NIST Webbook
ripol	1023.00	NIST Webbook
ripol	1023.00	NIST Webbook
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ripol	1020.00	NIST Webbook
ripol	1000.00	NIST Webbook
ripol	1020.00	NIST Webbook
ripol	1047.00	NIST Webbook
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ripol	987.00	NIST Webbook
ripol	1020.00	NIST Webbook
ripol	1020.00	NIST Webbook
ripol	1017.00	NIST Webbook
ripol	985.00	NIST Webbook
ripol	1024.00	NIST Webbook
ripol	976.00	NIST Webbook
ripol	1012.00	NIST Webbook
ripol	1012.00	NIST Webbook
ripol	1020.00	NIST Webbook
ripol	1019.00	NIST Webbook
ripol	1014.00	NIST Webbook
ripol	1014.00	NIST Webbook
ripol	1011.00	NIST Webbook
ripol	1010.00	NIST Webbook
ripol	1017.00	NIST Webbook
ripol	1009.00	NIST Webbook
ripol	1009.00	NIST Webbook
ripol	1005.00	NIST Webbook
ripol	1005.00	NIST Webbook
ripol	1007.00	NIST Webbook
ripol	1014.00	NIST Webbook
ripol	1005.00	NIST Webbook
ripol	1000.00	NIST Webbook
ripol	1005.00	NIST Webbook
ripol	992.00	NIST Webbook
ripol	988.00	NIST Webbook
ripol	988.00	NIST Webbook
ripol	998.00	NIST Webbook
ripol	1000.00	NIST Webbook
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ripol	1016.00	NIST Webbook
ripol	1018.00	NIST Webbook
ripol	1002.00	NIST Webbook
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ripol	1009.00	NIST Webbook
ripol	1009.00	NIST Webbook
ripol	1011.00	NIST Webbook
ripol	1019.00	NIST Webbook
ripol	1013.00	NIST Webbook
ripol	1012.00	NIST Webbook
ripol	993.00	NIST Webbook
ripol	1014.00	NIST Webbook
ripol	986.00	NIST Webbook
ripol	989.00	NIST Webbook
ripol	1027.00	NIST Webbook
ripol	1007.00	NIST Webbook
ripol	1002.00	NIST Webbook
ripol	1022.00	NIST Webbook
ripol	1029.00	NIST Webbook
ripol	1031.00	NIST Webbook
ripol	1000.00	NIST Webbook
ripol	1017.00	NIST Webbook
ripol	1025.00	NIST Webbook
ripol	1029.00	NIST Webbook
ripol	1020.00	NIST Webbook
ripol	1018.00	NIST Webbook
ripol	1033.00	NIST Webbook
ripol	1009.00	NIST Webbook
ripol	1025.00	NIST Webbook
ripol	1005.00	NIST Webbook

tb	389.75	K	Measurement and Correlation of Isobaric Vapor-Liquid Equilibrium for Binary Systems of Allyl Alcohol with Isobutyl Acetate, Butyl Acetate, and Butyl Propionate at 101.3 kPa
tb	389.70	K	KDB
tb	389.44	K	Isobaric VLE at 0.6 MPa for binary systems isobutyl acetate + ethanol, + 1-propanol or + 2-propanol
tb	389.55	K	Vapour-liquid equilibrium measurements and extractive distillation process design for separation of azeotropic mixture (dimethyl carbonate + ethanol)
tb	389.90	K	Isobaric Vapor Liquid Equilibrium for the Binary and Ternary System with Isobutyl Alcohol, Isobutyl Acetate and Dimethyl Sulfoxide at 101.3 kPa
tb	389.55	K	Isobaric Vapor-Liquid Equilibrium Measurements for Separation of Azeotrope (Methanol + Methyl Acetate)
tc	561.00	K	KDB
tc	560.80 ± 0.60	K	NIST Webbook
tc	561.50 ± 2.00	K	NIST Webbook
tc	569.00 ± 5.00	K	NIST Webbook
tf	176.10 ± 0.60	K	NIST Webbook
tf	240.15 ± 0.50	K	NIST Webbook
tf	176.05	K	NIST Webbook
tf	174.25	K	Aqueous Solubility Prediction Method
tf	174.30	K	KDB
vc	0.414	m ³ /kmol	KDB
zc	0.2804710		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	255.87	J/mol×K	594.22	Joback Method
cpg	219.89	J/mol×K	473.09	Joback Method
cpg	229.39	J/mol×K	503.38	Joback Method

cpg	238.55	J/molxK	533.66	Joback Method
cpg	247.38	J/molxK	563.94	Joback Method
cpg	210.06	J/molxK	442.81	Joback Method
cpg	199.90	J/molxK	412.53	Joback Method
cpl	240.20	J/molxK	290.00	NIST Webbook
dvisc	0.0046134	Paxs	214.54	Joback Method
dvisc	0.0011317	Paxs	280.54	Joback Method
dvisc	0.0006998	Paxs	313.53	Joback Method
dvisc	0.0004742	Paxs	346.53	Joback Method
dvisc	0.0003438	Paxs	379.53	Joback Method
dvisc	0.0020807	Paxs	247.54	Joback Method
dvisc	0.0002624	Paxs	412.53	Joback Method
hvapt	39.20	kJ/mol	359.00	NIST Webbook
hvapt	39.80	kJ/mol	321.50	NIST Webbook
hvapt	39.90	kJ/mol	349.50	NIST Webbook
pvap	101.30	kPa	389.55	Vapour-liquid equilibrium measurements and extractive distillation process design for separation of azeotropic mixture (dimethyl carbonate + ethanol)
rfi	1.39020		293.15	Measurement and Correlation of Phase Equilibria for Isobutyl Acetate + {Ethanol or Methanol} + Water at 303.15 and 323.15 K
rfi	1.39050		293.15	Isobaric Vapor Liquid Equilibrium for Binary Systems of Thioglycolic Acid with Water, Butyl Acetate, Butyl Formate, and Isobutyl Acetate at 101.3 kPa
rfi	1.38760		298.15	Study of liquid liquid equilibrium of the systems isobutyl acetate + acetic acid +water and isobutyl alcohol + acetic acid +water at different temperatures

rfi	1.38760	298.15	Liquid liquid equilibria of the systems isobutyl acetate + isobutyl alcohol + water and isobutyl acetate + isobutyl alcohol + glycerol at different temperatures
rfi	1.38760	298.15	Vapor liquid equilibria in the ternary system isobutyl alcohol + isobutyl acetate + butyl propionate and the binary systems isobutyl alcohol + butyl propionate, isobutyl acetate + butyl propionate at 101.3 kPa
rfi	1.38760	298.15	Phase equilibria in the ternary system isobutyl alcohol + isobutyl acetate + 1-hexanol and the binary systems isobutyl alcohol + 1-hexanol, isobutyl acetate + 1-hexanol at 101.3 kPa
rfi	1.38760	298.15	Phase equilibria in the systems isobutyl alcohol + N,N-dimethylformamide, isobutyl acetate + N,N-dimethylformamide and isobutyl alcohol + isobutyl acetate + N,N-dimethylformamide at 101.3 kPa
rfi	1.38780	298.20	Tie-line data for the aqueous solutions of phenol with organic solvents at T = 298.2 K
rfi	1.38760	298.15	Isobaric vapor-liquid equilibria for the binary systems isobutyl alcohol + isobutyl acetate and tert-butyl alcohol + tert-butyl acetate at 20 and 101.3 kPa

rho1	849.39	kg/m3	313.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
rho1	871.30	kg/m3	293.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
rho1	875.00	kg/m3	293.00	KDB
srf	0.02	N/m	298.15	Excess Molar Volumes and Surface Tensions of 1,2,4-Trimethylbenzene and 1,3,5-Trimethylbenzene with Isopropyl Acetate and Isobutyl Acetate at (298.15, 308.15, and 313.15) K
srf	0.02	N/m	308.15	Excess Molar Volumes and Surface Tensions of 1,2,4-Trimethylbenzene and 1,3,5-Trimethylbenzene with Isopropyl Acetate and Isobutyl Acetate at (298.15, 308.15, and 313.15) K
srf	0.02	N/m	313.15	Excess Molar Volumes and Surface Tensions of 1,2,4-Trimethylbenzene and 1,3,5-Trimethylbenzene with Isopropyl Acetate and Isobutyl Acetate at (298.15, 308.15, and 313.15) K

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbp	361.00	K	39.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	367.41	K	49.98	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	372.89	K	59.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	377.39	K	70.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	381.58	K	80.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	385.54	K	90.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	389.37	K	100.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil

tbp	392.35	K	110.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	395.26	K	120.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	398.16	K	130.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	400.84	K	140.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	403.64	K	150.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.50519e+01
Coeff. B	-3.64415e+03
Coeff. C	-4.07290e+01
Temperature range (K), min.	287.55
Temperature range (K), max.	414.85

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C*\ln(T) + D*T^2$

Coeff. A	9.01223e+01
Coeff. B	-7.87047e+03
Coeff. C	-1.11424e+01
Coeff. D	7.93342e-06
Temperature range (K), min.	174.30
Temperature range (K), max.	561.00

Sources

Solution thermodynamics of simvastatin in pure solvents and binary mixtures: NIST WebBook

<https://www.doi.org/10.1016/j.fluid.2015.07.055>

<http://webbook.nist.gov/cgi/cbook.cgi?ID=C110190&Units=SI>

Phase equilibria in the ternary system isobutyl alcohol + isobutyl acetate + hexan-1-ol. Vapor-liquid equilibrium systems. Mixtures of acetates in the isobutyl acetate-hexan-1-ol system at 0.1 kPa. Different solvents:

<https://www.doi.org/10.1016/j.fluid.2005.06.019>

Excess Molar Volumes and Surface Tensions of 1,2,4-Trimethylbenzene and 1,3,5-Trimethylbenzene with Water, Propionic Acid, Isobutyl Acetate, and Isobutyl Alcohol. Binary and Ternary Vapor-Liquid Equilibrium Measurements and Extractive Distillation Process Design for Aqueous Mixtures of Propionic Acid and Isobutyl Acetate from (299.73 to 308.15) K.

<https://www.doi.org/10.1021/acs.jced.6b00221>

<https://www.doi.org/10.1016/j.fluid.2012.06.011>

<https://www.doi.org/10.1021/je800046k>

<https://www.doi.org/10.1016/j.tca.2012.04.020>

<https://www.doi.org/10.1021/je060321b>

<https://www.doi.org/10.1016/j.jct.2019.01.027>

<https://www.doi.org/10.1016/j.jct.2010.01.001>

<https://www.doi.org/10.1021/je101319f>

Phase equilibria in the systems isobutyl alcohol + isobutyl acetate + N,N-dimethylformamide (DMF) at 0.1 kPa: acetate + butyl propionate and the binary systems isobutyl alcohol + butyl propionate, isobutyl acetate + butyl propionate. Equilibrium for CO₂-Based Mixtures at the Vapor-Liquid Equilibria of Water + Prop-2-enoic Acid + Isobutyl Acetate at Different Temperatures: the isoalkyl acetate in supercritical liquid-liquid equilibria of the systems isobutyl acetate + isobutyl alcohol + isobutyl acetate for the binary and ternary systems with isobutyl acetate and n-butyl alcohol + isobutyl acetate and n-butyl alcohol + isobutyl acetate at 0.1 kPa. Vapor Pressure: Liquid-liquid equilibrium determination and thermodynamics modeling for isobaric Vapor-Liquid Equilibrium for Binary Systems of Thioglycolic Acid with Water, Butyric Acid, and Aspirin in Pure Solvents Using Reduced Binary Measurements and Correlation of Isobaric Vapor-Liquid Equilibrium for Binary Systems of Thioglycolic Acid with Organic Solvents and Isobutyl Acetate, n-Butyric Acid, Ethyl Acetate, and n-Propylamine. Data: N,N-Dimethylformamide, and Acetone Solubility Prediction Method: Aqueous Dataset

https://en.wikipedia.org/wiki/Joback_method

<https://www.doi.org/10.1016/j.fluid.2005.03.014>

<https://www.doi.org/10.1021/acs.jced.8b00807>

<https://www.doi.org/10.1016/j.fluid.2005.09.015>

<https://www.thermo.com/files/research/kdb/mol/mol1080.mol>

<https://www.doi.org/10.1021/je501023n>

<https://www.doi.org/10.1021/je2003226>

<https://www.doi.org/10.1016/j.fluid.2013.12.026>

<https://www.doi.org/10.1016/j.fluid.2008.01.010>

<https://www.doi.org/10.1021/acs.jced.7b00241>

<https://www.doi.org/10.1016/j.fluid.2004.10.022>

<https://www.doi.org/10.1016/j.fluid.2012.06.013>

<https://www.sciencedirect.com/book/9780128029992/the-yaws-handbook-of-vapor-pressure>

<https://www.doi.org/10.1016/j.fluid.2017.11.010>

<https://www.doi.org/10.1021/acs.jced.6b00686>

<https://www.doi.org/10.1021/acs.jced.5b00746>

<https://www.doi.org/10.1021/acs.jced.7b01024>

<https://www.doi.org/10.1016/j.jct.2012.10.028>

<https://www.doi.org/10.1021/je800428r>

<https://www.thermo.com/research/kdb/hcprop/showprop.php?cmpid=1080>

Aqueous Dataset

<http://onschallenge.wikispaces.com/file/view/AqueousDataset002.xlsx/351826032/AqueousDataset002.xlsx>

Measurement and Correlation of Phase Equilibria for Isobutyl Acetate + Isobutyl Alcohol + Water at 100.15, 115, 130, and 145 °C <https://www.doi.org/10.1021/acs.jced.6b00949>

Investigation of the Ternary Liquid-Liquid Equilibrium for acetic acid + water + propyl acetate by gas-liquid extraction: Preparation of Protocatechuic Acetate Using Di-(2-ethylhexyl)phosphoric Acid <https://www.doi.org/10.1016/j.fluid.2011.03.006>

Isobutyl Acetate-Liquid Equilibrium of the Ternary System: Ethyl acetate + acetic acid + water <https://www.doi.org/10.1021/acs.jced.7b00797>

Measurement of Isobutyl Alcohol + Acetic Acid + Water at Different Temperatures: Measurement and Thermodynamic Modelling of Ternary Liquid-Liquid Equilibrium <https://www.doi.org/10.1016/j.fluid.2008.07.001>

Liquid-Liquid Equilibrium for the Ternary System: Acetic Acid + Water + Butyl Methacrylate <http://pubs.acs.org/doi/abs/10.1021/ci9903071>

Measurement of the Ternary System: 2-Methyl Propyl Acetate + Water + Isobutyl Alcohol at 304.15 K, 332.15 K, and 360.15 K <https://www.doi.org/10.1016/j.jct.2017.06.015>

Acetic Acid + Isobutyl Alcohol + Isobutyl Acetate: A New Ternary System <https://www.doi.org/10.1021/je6005746>

Measurement of the Ternary System: Acetic Acid + Water + 2-Methyl Propyl Acetate at 304.15 K, 332.15 K, and 360.15 K <http://link.springer.com/article/10.1007/BF02311772>

Acetic Acid + Isobutyl Alcohol + Isobutyl Acetate: A New Ternary System <https://www.doi.org/10.1021/je800120p>

Measurement of the Ternary System: Acetic Acid + Isobutyl Alcohol + Isobutyl Acetate <https://www.doi.org/10.1016/j.fluid.2018.02.003>

Measurement of the Ternary System: Acetic Acid + Isobutyl Alcohol + Isobutyl Acetate <https://www.doi.org/10.1016/j.fluid.2009.03.006>

Measurement of the Ternary System: Acetic Acid + Isobutyl Alcohol + Isobutyl Acetate http://pubs.acs.org/doi/suppl/10.1021/ci034243x/suppl_file/ci034243xsi20040112_053635.txt

Liquid-Liquid Equilibrium of Isobutyl Acetate + Isobutyl Alcohol + Imidazolium-Based Ionic Liquids at 298.15 and 308.15 K <https://www.doi.org/10.1021/acs.jced.8b01045>

Legend

af:	Acentric Factor
aignt:	Autoignition Temperature
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
fl:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpc:	Flash Point (Closed Cup Method)
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
hf:	Enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index

rhoc:	Critical density
rhoL:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tbp:	Boiling point at given pressure
tc:	Critical Temperature
tf:	Normal melting (fusion) point
vc:	Critical Volume
zc:	Critical Compressibility

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