

2-Butanone

Other names:	2-Butanal
	2-Oxobutane
	2-butanone (MEK)
	2-butanone (MEK; methyl ethyl ketone)
	3-Butanone
	Acetone, methyl-
	Aethylmethylketon
	Butan-2-one
	Butanone
	Butanone 2
	C2H5COCH3
	Ethyl methyl cetone
	Ethyl methyl ketone
	Ethylmethylketon
	Ketone, ethyl methyl
	Ketone, methyl ethyl
	MEK
	METHYL ACETONE
	Meetco
	Methyl ethyl ketone
	Metiletilchetone
	Metyloetyloketon
	Rcra waste number U159
	UN 1193
Inchi:	InChI=1S/C4H8O/c1-3-4(2)5/h3H2,1-2H3
InchiKey:	ZWEHNKRNPVVGH-UHFFFAOYSA-N
Formula:	C4H8O
SMILES:	CCC(C)=O
Mol. weight [g/mol]:	72.11
CAS:	78-93-3

Physical Properties

Property code	Value	Unit	Source
af	0.3200		KDB
affp	827.30	kJ/mol	NIST Webbook
aigt	789.26	K	KDB

basg	795.50	kJ/mol	NIST Webbook
chl	-2436.30 ± 1.50	kJ/mol	NIST Webbook
chl	-2444.20	kJ/mol	NIST Webbook
chl	-2438.40	kJ/mol	NIST Webbook
dm	3.30	debye	KDB
dvisc	0.0003730	Paxs	Excess Molar Volumes and Viscosity Deviations of Binary Liquid Mixtures of 1,3-Dioxolane and 1,4-Dioxane with Butyl Acetate, Butyric Acid, Butylamine, and 2-Butanone at 298.15 K
dvisc	0.0003760	Paxs	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of o-Xylene, m-Xylene, p-Xylene, and Isopropylbenzene with 2-Butanone at 298.15 K
dvisc	0.0004011	Paxs	Densities and Viscosities of Binary Liquid Mixtures of Trichloroethylene and Tetrachloroethylene with Some Polar and Nonpolar Solvents
dvisc	0.0003880	Paxs	A volumetric and viscosity study for the binary mixtures of 1-hexyl-3-methylimidazolium tetrafluoroborate with some molecular solvents
ea	9.99e-04	eV	NIST Webbook
fll	1.80	% in Air	KDB
flu	11.50	% in Air	KDB
fpc	267.59	K	KDB
fpo	266.48	K	KDB
gf	-146.20	kJ/mol	KDB
hf	-238.60 ± 0.84	kJ/mol	NIST Webbook
hf	-238.70 ± 0.96	kJ/mol	NIST Webbook
hf	-238.10	kJ/mol	NIST Webbook
hf	-238.50	kJ/mol	KDB
hfl	-279.00	kJ/mol	NIST Webbook
hfl	-273.30 ± 1.20	kJ/mol	NIST Webbook
hfus	7.71	kJ/mol	Joback Method
hvap	35.51 ± 0.08	kJ/mol	NIST Webbook
hvap	34.73	kJ/mol	NIST Webbook
hvap	34.92	kJ/mol	NIST Webbook
hvap	34.50 ± 0.10	kJ/mol	NIST Webbook
hvap	34.80 ± 0.10	kJ/mol	NIST Webbook
hvap	32.00 ± 0.01	kJ/mol	NIST Webbook
ie	9.50 ± 0.10	eV	NIST Webbook
ie	9.54 ± 0.03	eV	NIST Webbook

ie	9.55 ± 0.03	eV	NIST Webbook
ie	9.48 ± 0.02	eV	NIST Webbook
ie	9.51	eV	NIST Webbook
ie	9.49	eV	NIST Webbook
ie	9.54 ± 0.01	eV	NIST Webbook
ie	9.52	eV	NIST Webbook
ie	9.54 ± 0.03	eV	NIST Webbook
ie	9.53 ± 0.01	eV	NIST Webbook
ie	9.53 ± 0.01	eV	NIST Webbook
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ie	9.70	eV	NIST Webbook
ie	9.52	eV	NIST Webbook
ie	9.52 ± 0.04	eV	NIST Webbook
ie	9.53 ± 0.01	eV	NIST Webbook
ie	9.56	eV	NIST Webbook
ie	9.54 ± 0.01	eV	NIST Webbook
ie	9.46	eV	NIST Webbook
log10ws	0.52		Aqueous Solubility Prediction Method
log10ws	0.52		Estimated Solubility Method
logp	0.985		Crippen Method
mcvol	68.790	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=1)		KDB
pc	4166.00 ± 15.00	kPa	NIST Webbook
pc	4166.00 ± 3.00	kPa	NIST Webbook
pc	4207.00	kPa	KDB
pc	4165.80 ± 20.68	kPa	NIST Webbook
pc	4390.00 ± 202.65	kPa	NIST Webbook
pc	4166.00 ± 3.00	kPa	NIST Webbook
pc	4150.00 ± 34.50	kPa	NIST Webbook
pc	3998.00 ± 202.65	kPa	NIST Webbook
pc	4207.00 ± 10.00	kPa	NIST Webbook
rhoc	269.68 ± 15.14	kg/m3	NIST Webbook
rhoc	251.65 ± 4.33	kg/m3	NIST Webbook
rinpol	575.00		NIST Webbook
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ripol	914.00		NIST Webbook
sl	239.00	J/molxK	NIST Webbook
sl	241.40	J/molxK	NIST Webbook
sl	238.82	J/molxK	NIST Webbook
tb	352.65 ± 0.50	K	NIST Webbook
tb	351.75 ± 1.00	K	NIST Webbook
tb	353.75 ± 1.00	K	NIST Webbook
tb	351.15 ± 4.00	K	NIST Webbook
tb	354.15 ± 2.00	K	NIST Webbook
tb	352.75 ± 1.00	K	NIST Webbook
tb	352.74	K	KDB
tb	352.85	K	Excess molar volumes of ternary mixtures of 1,3-dichlorobenzene and methyl ethyl ketone with 1-alkanols at 303.15K
tb	352.68	K	Measurements and correlation of vapour liquid equilibria of 2-butanone and hydrocarbons binary systems at two different pressures

tb	352.72	K	Isobaric vapor-liquid equilibrium for 2-butanone + ethanol + phosphate-based ionic liquids at 101.3 kPa
tb	352.69	K	Excess enthalpies and (vapour + liquid) equilibrium data for the binary mixtures of dimethylsulphoxide with ketones
tb	352.72	K	Isobaric Vapor-Liquid Equilibrium for 2-Butanone + Ethanol System Containing Different Ionic Liquids at 101.3 kPa
tb	352.78	K	Measurement of Isobaric Vapor - Liquid Equilibria of Dimethyl Carbonate with Acetone, 2-Butanone and 2-Pentanone at 101.3 kPa and Density and Speed of Sound at 298.15 K
tb	352.68	K	Liquid-Liquid and Vapor-Liquid-Liquid Equilibrium of the 2-Butanone + 2-Butanol + Water System
tb	352.71 ± 0.10	K	NIST Webbook
tb	352.75 ± 0.20	K	NIST Webbook
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tb	352.72 ± 0.30	K	NIST Webbook
tb	351.75 ± 1.00	K	NIST Webbook
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tb	351.15 ± 2.00	K	NIST Webbook
tb	352.70 ± 0.30	K	NIST Webbook
tb	352.95 ± 1.00	K	NIST Webbook

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tb	352.75 ± 0.25	K	NIST Webbook
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tb	351.40 ± 1.00	K	NIST Webbook
tb	350.65 ± 2.00	K	NIST Webbook
tb	352.80 ± 0.30	K	NIST Webbook
tb	352.40 ± 1.00	K	NIST Webbook
tc	535.77 ± 0.30	K	NIST Webbook
tc	536.78	K	KDB
tc	536.80	K	NIST Webbook
tc	535.77 ± 0.20	K	NIST Webbook
tc	535.77 ± 0.20	K	NIST Webbook
tc	535.77 ± 0.20	K	NIST Webbook
tc	533.00 ± 3.00	K	NIST Webbook
tc	533.70 ± 3.00	K	NIST Webbook
tc	535.70 ± 0.39	K	NIST Webbook
tc	536.78 ± 0.20	K	NIST Webbook
tf	186.50	K	Aqueous Solubility Prediction Method
tf	186.55 ± 0.30	K	NIST Webbook
tf	186.00 ± 2.00	K	NIST Webbook
tf	186.25 ± 0.30	K	NIST Webbook
tf	186.46 ± 0.01	K	NIST Webbook
tf	186.42 ± 0.02	K	NIST Webbook
tf	186.85	K	NIST Webbook
tf	186.48	K	KDB
tf	186.80 ± 0.20	K	NIST Webbook
tt	186.50 ± 0.01	K	NIST Webbook
tt	186.10 ± 0.10	K	NIST Webbook
tt	186.48 ± 0.03	K	NIST Webbook
tt	186.40 ± 0.06	K	NIST Webbook
tt	186.47 ± 0.04	K	NIST Webbook
vc	0.267	m3/kmol	KDB
zc	0.2516810		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	113.43 ± 0.23	J/mol×K	347.15	NIST Webbook
cpg	115.65 ± 0.17	J/mol×K	358.79	NIST Webbook
cpg	118.70 ± 0.18	J/mol×K	371.90	NIST Webbook
cpg	119.03 ± 0.24	J/mol×K	372.15	NIST Webbook
cpg	121.75 ± 0.18	J/mol×K	385.60	NIST Webbook
cpg	124.39 ± 0.25	J/mol×K	397.15	NIST Webbook
cpg	124.60 ± 0.19	J/mol×K	399.55	NIST Webbook
cpg	126.98 ± 0.19	J/mol×K	410.70	NIST Webbook
cpg	131.71 ± 0.26	J/mol×K	432.15	NIST Webbook
cpg	138.62 ± 0.28	J/mol×K	467.15	NIST Webbook
cpl	162.20	J/mol×K	303.15	NIST Webbook
cpl	159.00	J/mol×K	298.15	NIST Webbook
cpl	158.40	J/mol×K	298.15	NIST Webbook
cpl	158.40	J/mol×K	298.15	NIST Webbook
cpl	158.41	J/mol×K	298.15	NIST Webbook
cpl	158.40	J/mol×K	298.10	NIST Webbook
cpl	159.20	J/mol×K	298.15	NIST Webbook
cpl	158.70	J/mol×K	298.15	NIST Webbook
cpl	158.00	J/mol×K	293.00	NIST Webbook
cpl	158.91	J/mol×K	298.15	NIST Webbook
cpl	157.91	J/mol×K	298.15	NIST Webbook
cpl	160.70	J/mol×K	297.00	NIST Webbook
cpl	160.70	J/mol×K	297.00	NIST Webbook
dvisc	0.0003168	Paxs	323.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0003167	Paxs	323.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K

dvisc	0.0003303	Paxs	318.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0003461	Paxs	313.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0004306	Paxs	288.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0003793	Paxs	303.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0003793	Paxs	303.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0003962	Paxs	298.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K

dvisc	0.0003962	Paxs	298.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0004136	Paxs	293.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0004306	Paxs	288.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0003030	Paxs	323.15	Densities and Viscosities of the Binary Mixtures of Phenylmethanol with 2-Butanone
dvisc	0.0003160	Paxs	318.15	Densities and Viscosities of the Binary Mixtures of Phenylmethanol with 2-Butanone
dvisc	0.0003300	Paxs	313.15	Densities and Viscosities of the Binary Mixtures of Phenylmethanol with 2-Butanone
dvisc	0.0002545	Paxs	313.15	Densities and Viscosities of Binary Liquid Mixtures of 2-Butanone with Branched Alcohols at (293.15 to 313.15) K
dvisc	0.0003450	Paxs	308.15	Densities and Viscosities of the Binary Mixtures of Phenylmethanol with 2-Butanone

dvisc	0.0003620	Paxs	303.15	Densities and Viscosities of the Binary Mixtures of Phenylmethanol with 2-Butanone
dvisc	0.0003600	Paxs	303.15	Dynamic Viscosities of the Binary Systems Cyclohexane and Cyclopentane with Acetone, Butanone, or 2-Pentanone at Three Temperatures T) (293.15, 298.15, and 303.15) K
dvisc	0.0003520	Paxs	308.15	Densities and viscosities of binary mixtures of ethylmethylketone and 2-alkanols; application of the ERAS model and cubic EOS
dvisc	0.0003780	Paxs	298.15	Dynamic Viscosities of the Binary Systems Cyclohexane and Cyclopentane with Acetone, Butanone, or 2-Pentanone at Three Temperatures T) (293.15, 298.15, and 303.15) K
dvisc	0.0003440	Paxs	308.15	Density and Viscosity of Ketones with Toluene at Different Temperatures and at Atmospheric Pressure
dvisc	0.0003653	Paxs	303.15	Density and Viscosity of Ketones with Toluene at Different Temperatures and at Atmospheric Pressure

dvisc	0.0003856	Paxs	298.15	Density and Viscosity of Ketones with Toluene at Different Temperatures and at Atmospheric Pressure
dvisc	0.0002601	Paxs	308.15	Densities and Viscosities of Binary Liquid Mixtures of 2-Butanone with Branched Alcohols at (293.15 to 313.15) K
dvisc	0.0003680	Paxs	303.15	Densities and viscosities of binary mixtures of ethylmethylketone and 2-alkanols; application of the ERAS model and cubic EOS
dvisc	0.0002666	Paxs	303.15	Densities and Viscosities of Binary Liquid Mixtures of 2-Butanone with Branched Alcohols at (293.15 to 313.15) K
dvisc	0.0002828	Paxs	298.15	Densities and Viscosities of Binary Liquid Mixtures of 2-Butanone with Branched Alcohols at (293.15 to 313.15) K
dvisc	0.0003956	Paxs	293.15	Densities and Viscosities of Binary Liquid Mixtures of 2-Butanone with Branched Alcohols at (293.15 to 313.15) K

dvisc	0.0003980	Paxs	293.15	Dynamic Viscosities of the Binary Systems Cyclohexane and Cyclopentane with Acetone, Butanone, or 2-Pentanone at Three Temperatures T) (293.15, 298.15, and 303.15) K
dvisc	0.0003303	Paxs	318.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0003461	Paxs	313.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0003626	Paxs	308.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0003980	Paxs	293.15	Physical properties of the binary systems methylcyclopentane with ketones (acetone, butanone and 2-pentanone) at T = (293.15, 298.15, and 303.15) K. New UNIFAC-VISCO interaction parameters

dvisc	0.0003780	Paxs	298.15	Physical properties of the binary systems methylcyclopentane with ketones (acetone, butanone and 2-pentanone) at T = (293.15, 298.15, and 303.15) K. New UNIFAC-VISCO interaction parameters
dvisc	0.0003600	Paxs	303.15	Physical properties of the binary systems methylcyclopentane with ketones (acetone, butanone and 2-pentanone) at T = (293.15, 298.15, and 303.15) K. New UNIFAC-VISCO interaction parameters
dvisc	0.0003856	Paxs	298.15	Excess parameter studies on the binary mixtures of toluene with ketones at different temperatures
dvisc	0.0003653	Paxs	303.15	Excess parameter studies on the binary mixtures of toluene with ketones at different temperatures
dvisc	0.0003440	Paxs	308.15	Excess parameter studies on the binary mixtures of toluene with ketones at different temperatures
dvisc	0.0003810	Paxs	298.15	Densities and viscosities of binary mixtures of ethylmethylketone and 2-alkanols; application of the ERAS model and cubic EOS

dvisc	0.0003626	Paxs	308.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0004136	Paxs	293.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0003390	Paxs	313.15	Densities and viscosities of binary mixtures of ethylmethylketone and 2-alkanols; application of the ERAS model and cubic EOS
hfust	8.44	kJ/mol	186.48	NIST Webbook
hfust	8.38	kJ/mol	186.47	NIST Webbook
hfust	8.44	kJ/mol	186.50	NIST Webbook
hfust	8.44	kJ/mol	186.50	NIST Webbook
hfust	8.48	kJ/mol	186.10	NIST Webbook
hvapt	32.30 ± 0.10	kJ/mol	338.00	NIST Webbook
hvapt	30.00 ± 0.10	kJ/mol	370.00	NIST Webbook
hvapt	30.50 ± 0.10	kJ/mol	363.00	NIST Webbook
hvapt	31.30 ± 0.10	kJ/mol	352.00	NIST Webbook
hvapt	33.90	kJ/mol	342.00	NIST Webbook
hvapt	33.80	kJ/mol	315.00	NIST Webbook
hvapt	35.60	kJ/mol	310.00	NIST Webbook
hvapt	33.90	kJ/mol	339.00	NIST Webbook
hvapt	31.10	kJ/mol	505.00	NIST Webbook
hvapt	31.60	kJ/mol	438.00	NIST Webbook
hvapt	32.50	kJ/mol	378.00	NIST Webbook
hvapt	34.60	kJ/mol	318.00	NIST Webbook
hvapt	33.80 ± 0.10	kJ/mol	314.00	NIST Webbook
hvapt	31.21	kJ/mol	352.60	KDB
hvapt	31.30	kJ/mol	352.80	NIST Webbook

pvap	101.30	kPa	352.68	Measurements and correlation of vapour liquid equilibria of 2-butanone and hydrocarbons binary systems at two different pressures
pvap	30.00	kPa	319.95	Measurements and correlation of vapour liquid equilibria of 2-butanone and hydrocarbons binary systems at two different pressures
pvap	101.30	kPa	352.72	Isobaric vapor-liquid equilibrium for 2-butanone + ethanol + phosphate-based ionic liquids at 101.3 kPa
pvap	94.00	kPa	350.25	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	101.30	kPa	352.72	Isobaric Vapor-Liquid Equilibrium for 2-Butanone + Ethanol System Containing Different Ionic Liquids at 101.3 kPa
pvap	15.74	kPa	303.15	Density, Viscosity, Vapor-Liquid Equilibrium, Excess Molar Volume, Viscosity Deviation, and Their Correlations for the Chloroform + 2-Butanone Binary System
pvap	20.00	kPa	309.65	Measurements and correlation of vapour liquid equilibria of 2-butanone and hydrocarbons binary systems at two different pressures

rfi	1.37879	293.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.36565	318.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.36294	323.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.37910	293.15	Isothermal Vapor-Liquid Equilibrium Measurements of Butan-2-one + 2-Methyl-propan-1-ol/Pentan-1-ol
rfi	1.37900	293.15	Solid-Liquid Equilibrium Measurements for Posaconazole and Voriconazole in Several Solvents between T = 278.2 and 323.2 K Using Differential Thermal Analysis/Thermal Gravimetric Analysis

rfi	1.37870	293.15	Solubility Data for Roflumilast and Maraviroc in Various Solvents between T = (278.2-323.2) K
rfi	1.37690	298.15	Bubble-Temperature Measurements on Some Binary Mixtures Formed by Tetrahydrofuran or Amyl Alcohol with Hydrocarbons, Chlorohydrocarbons, or Butanols at (94.6 or 95.8) kPa
rfi	1.37623	298.15	Densities and Viscosities for Binary and Ternary Mixtures of Ethanol, 2-Butanone, and 2,2,4-Trimethylpentane at T = (298.15, 308.15, and 318.15) K
rfi	1.37879	293.15	Thermodynamic Properties of Ionic Liquids in Organic Solvents from (293.15 to 303.15) K
rfi	1.37618	298.15	Thermodynamic Properties of Ionic Liquids in Organic Solvents from (293.15 to 303.15) K
rfi	1.37355	303.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.37618	298.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures

rfi	1.37102	308.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.37604	298.15	Properties of ionic liquid HMIMPF ₆ with carbonates, ketones and alkyl acetates
rfi	1.37614	298.15	Isobaric vapour liquid equilibria for binary systems of 2-butanone with ethanol, 1-propanol, and 2-propanol at 20 and 101.3 kPa
rfi	1.37623	298.15	Vapor liquid equilibria for binary and ternary mixtures of ethanol, 2-butanone, and 2,2,4-trimethylpentane at 101.3 kPa
rfi	1.37355	303.15	Thermodynamic Properties of Ionic Liquids in Organic Solvents from (293.15 to 303.15) K
rfi	1.37690	298.15	(Vapor + liquid) equilibrium of binary mixtures formed by N,N-dimethyl formamide with some compounds at 95.1 kPa
rfi	1.37880	293.15	Solubilities of Phosphorus-Containing Compounds in Selected Solvents

rfi	1.37880	293.15	Isothermal Vapor Liquid Equilibrium Data for the Butan-2-one + Methanol or Ethanol Systems Using a Static-Analytic Microcell
rfi	1.37618	298.15	Ternary Liquid-Liquid Equilibria Ethanol + 2-Butanone + 1-Butyl-3-methylimidazolium Hexafluorophosphate, 2-Propanol + 2-Butanone + 1-Butyl-3-methylimidazolium Hexafluorophosphate, and 2-Butanone + 2-Propanol + 1,3-Dimethylimidazolium Methyl Sulfate at 298.15 K
rfi	1.37930	298.15	Isobaric Vapor Liquid Equilibria for Binary Systems of Acetone + Isopropenyl Acetate, 2-Butanone + Isopropenyl Acetate, and Isopropenyl Acetate + Acetylacetone at 101.3 kPa
rfi	1.37610	298.15	Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures of Ethanol and 2-Propanol with 2-Butanone and Butyl Propionate at 101.3 kPa
rfi	1.37366	303.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K

rfi	1.37631	298.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.37892	293.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.38153	288.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.37700	298.15	Excess molar volumes and ultrasonic studies of N-methyl-2-pyrrolidone with ketones at T = 303.15 K

rfi	1.37383	303.15	Density, viscosity, refractive index, excess molar enthalpy, viscosity, and refractive index deviations for the (1-butanol + 2-butanone) binary system at T = 303 K. A new adiabatic calorimeter for heat of mixing
rfi	1.37500	298.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of Methyl Ethyl Ketone + Pentanol Isomers at Different Temperatures
rfi	1.37000	308.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of Methyl Ethyl Ketone + Pentanol Isomers at Different Temperatures
rfi	1.36834	313.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.36570	318.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of Methyl Ethyl Ketone + Pentanol Isomers at Different Temperatures

rhoI	800.30	kg/m3	298.15	Liquid-liquid equilibria for the pseudo-ternary system {aqueous sulfuric acid solution + methyl ethyl ketone or methyl isopropyl ketone + phosphonium-based ionic liquids} at 298.15 K and atmospheric pressure
rhoI	794.63	kg/m3	303.15	Excess molar volumes of (1-chlorobutane +heptane + 2-butanone or 2-pentanone) at 288.15 , 303.15 and 313.15 K . Measurements and correlations.
rhoI	784.01	kg/m3	313.15	Excess molar volumes of (1-chlorobutane +heptane + 2-butanone or 2-pentanone) at 288.15 , 303.15 and 313.15 K . Measurements and correlations.
rhoI	810.26	kg/m3	288.15	Volumetric properties of binary liquid mixtures of ketones with chloroalkanes at different temperatures and atmospheric pressure
rhoI	805.06	kg/m3	293.15	Volumetric properties of binary liquid mixtures of ketones with chloroalkanes at different temperatures and atmospheric pressure
rhoI	794.57	kg/m3	303.15	Volumetric properties of binary liquid mixtures of ketones with chloroalkanes at different temperatures and atmospheric pressure

rhoI	789.27	kg/m3	308.15	Volumetric properties of binary liquid mixtures of ketones with chloroalkanes at different temperatures and atmospheric pressure
rhoI	783.95	kg/m3	313.15	Volumetric properties of binary liquid mixtures of ketones with chloroalkanes at different temperatures and atmospheric pressure
rhoI	799.83	kg/m3	298.15	Volumetric properties of binary liquid mixtures of ketones with chloroalkanes at different temperatures and atmospheric pressure
rhoI	799.70	kg/m3	298.15	Isobaric Vapor Liquid Equilibrium for the Binary Systems of sec-Butyl Acetate + Methyl Ethyl Ketone, 2-Methoxyethanol, or 1,2-Dimethoxyethane at 101.3 kPa
rhoI	799.62	kg/m3	298.15	Excess Molar Volumes and Surface Tensions of Xylene with Acetone or 2-Butanone at 298.15 K
rhoI	794.60	kg/m3	303.15	Viscometric Behavior of Binary Mixtures of Butan-2-one with Benzene at T = (303.15, 313.15, and 323.15) K

rhoI	784.00	kg/m3	313.15	Viscometric Behavior of Binary Mixtures of Butan-2-one with Benzene at T = (303.15, 313.15, and 323.15) K
rhoI	773.30	kg/m3	323.15	Viscometric Behavior of Binary Mixtures of Butan-2-one with Benzene at T = (303.15, 313.15, and 323.15) K
rhoI	799.97	kg/m3	298.15	Thermodynamics of Ketone + Amine Mixtures. Part VIII. Molar Excess Enthalpies at 298.15 K for n-Alkanone + Aniline or + N-Methylaniline Systems
rhoI	804.97	kg/m3	293.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	799.74	kg/m3	298.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	794.47	kg/m3	303.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform

rhoI	789.18	kg/m3	308.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	783.85	kg/m3	313.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	778.48	kg/m3	318.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	773.09	kg/m3	323.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	804.83	kg/m3	293.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	799.60	kg/m3	298.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform

rhoI	794.33	kg/m3	303.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	789.04	kg/m3	308.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	783.72	kg/m3	313.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	778.36	kg/m3	318.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	772.97	kg/m3	323.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	804.90	kg/m3	293.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform

rhoI	799.68	kg/m3	298.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	794.41	kg/m3	303.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	789.12	kg/m3	308.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	783.80	kg/m3	313.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	778.44	kg/m3	318.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	773.04	kg/m3	323.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform

rhoI	805.17	kg/m3	293.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	799.94	kg/m3	298.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	794.67	kg/m3	303.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	789.38	kg/m3	308.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	794.60	kg/m3	303.15	Volumetric Behavior of the Binary Mixtures of Methyl Ethyl Ketone with n-Hexane, Cyclohexane, and Benzene at T) (303.15, 313.15, and 323.15) K
rhoI	784.00	kg/m3	313.15	Volumetric Behavior of the Binary Mixtures of Methyl Ethyl Ketone with n-Hexane, Cyclohexane, and Benzene at T) (303.15, 313.15, and 323.15) K

rhoI	773.30	kg/m3	323.15	Volumetric Behavior of the Binary Mixtures of Methyl Ethyl Ketone with n-Hexane, Cyclohexane, and Benzene at T) (303.15, 313.15, and 323.15) K
rhoI	799.71	kg/m3	303.15	Excess Molar Enthalpies and Vapor-Liquid Equilibrium for N-Methyl-2-pyrrolidone with Ketones
rhoI	799.69	kg/m3	303.15	Studies of viscosities of dilute solutions of alkylamine in non-electrolyte solvents. II. Haloalkanes and other polar solvents
rhoI	794.55	kg/m3	303.15	Thermodynamics of amide + ketone mixtures. 1. Volumetric, speed of sound and refractive index data for N,N-dimethylformamide + 2-alkanone systems at several temperatures
rhoI	799.78	kg/m3	298.15	Thermodynamics of amide + ketone mixtures. 1. Volumetric, speed of sound and refractive index data for N,N-dimethylformamide + 2-alkanone systems at several temperatures
rhoI	805.06	kg/m3	293.15	Thermodynamics of amide + ketone mixtures. 1. Volumetric, speed of sound and refractive index data for N,N-dimethylformamide + 2-alkanone systems at several temperatures

rhoI	799.60	kg/m3	298.15	Volumetric and optical properties for some (2-butanone + chloroalkane) binary mixtures at T = 298.15 K
rhoI	799.97	kg/m3	298.15	Thermodynamics of (ketone + amine) mixtures. Part XI. Excess molar enthalpies at T = 298.15 K for the (1-propanol + N,N,N-triethylamine + 2-butanone) system
rhoI	786.94	kg/m3	313.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhoI	792.45	kg/m3	308.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhoI	797.88	kg/m3	303.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhoI	803.24	kg/m3	298.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K

rhoI	808.64	kg/m3	293.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhoI	794.50	kg/m3	303.15	Excess molar volumes and ultrasonic studies of dimethylsulphoxide with ketones at T = 303.15 K
rhoI	799.75	kg/m3	298.15	Excess molar enthalpies and volumes of binary mixtures of nonafluorobutylmethylether with ketones at T = 298.15 K
rhoI	799.80	kg/m3	293.15	(Vapour + liquid) equilibria for (2-ethoxypropene + acetone) and (2-ethoxypropene + butanone)
rhoI	802.03	kg/m3	298.15	Quaternary isothermal vapor-liquid equilibrium of the model biofuel 2-butanone + n-heptane + tetrahydrofuran + cyclohexane using Raman spectroscopic characterization

rhoI	800.87	kg/m3	298.15	Experimental measurements and modelling of volumetric properties, refractive index and viscosity of binary systems of ethyl lactate with methyl ethyl ketone, toluene and n-methyl-2-pyrrolidone at 288.15 323.15 K and atmospheric pressure. New UNIFAC VISCO and ASOG VISCO interaction parameters
rhoI	799.97	kg/m3	298.15	Thermodynamics of ketone + amine mixtures. Part X. Excess molarenthalpies at 298.15 K for N,N,N-triethylamine + 2-alkanone systems.Characterization of tertiary amine + 2-alkanone, and of amino-ketone + n-alkane mixtures in terms of DISQUAC
rhoI	799.97	kg/m3	298.15	Thermodynamics of ketone + amine mixtures. Part IX. Excess molar enthalpies at 298.15K for dipropylamine, or dibutylamine + 2-alkanone systems and modeling of linear or aromatic amine + 2-alkanone mixtures in terms of DISQUAC and ERAS
rhoI	800.30	kg/m3	313.15	Effect of temperature on ultrasonic velocity and thermodynamic parameters of bisphenol-C-formaldehyde-acrylate resin solutions

rhoI	800.10	kg/m3	308.15	Effect of temperature on ultrasonic velocity and thermodynamic parameters of bisphenol-C-formaldehyde-acrylate resin solutions
rhoI	802.50	kg/m3	303.15	Effect of temperature on ultrasonic velocity and thermodynamic parameters of bisphenol-C-formaldehyde-acrylate resin solutions
rhoI	805.00	kg/m3	293.00	KDB
rhoI	810.33	kg/m3	288.15	Excess molar volumes of (1-chlorobutane +heptane + 2-butanone or 2-pentanone) at 288.15 , 303.15 and 313.15 K . Measurements and correlations.
sfust	45.25	J/molxK	186.48	NIST Webbook
sfust	44.98	J/molxK	186.47	NIST Webbook
sfust	45.59	J/molxK	186.10	NIST Webbook
speedsl	1192.00	m/s	298.15	Vapor liquid equilibria for systems of diethyl carbonate and ketones and determination of group interaction parameters for the UNIFAC and ASOG methods
speedsl	1212.30	m/s	293.15	Thermodynamics of ketone + amine mixtures Part IV. Volumetric and speed of sound data at (293.15; 298.15 and 303.15 K) for 2-butanone +dipropylamine, +dibutylamine or +triethylamine systems

speedsl	1170.80	m/s	303.15	Thermodynamics of ketone + amine mixtures Part IV. Volumetric and speed of sound data at (293.15; 298.15 and 303.15 K) for 2-butanone +dipropylamine, +dibutylamine or +triethylamine systems
speedsl	1212.00	m/s	293.15	Thermodynamics of Ketone + Amine Mixtures. Part III. Volumetric and Speed of Sound Data at (293.15, 298.15, and 303.15) K for 2-Butanone + Aniline, + N-Methylaniline, or + Pyridine Systems
speedsl	1190.80	m/s	298.15	Thermodynamics of Ketone + Amine Mixtures. Part III. Volumetric and Speed of Sound Data at (293.15, 298.15, and 303.15) K for 2-Butanone + Aniline, + N-Methylaniline, or + Pyridine Systems
speedsl	1170.60	m/s	303.15	Thermodynamics of Ketone + Amine Mixtures. Part III. Volumetric and Speed of Sound Data at (293.15, 298.15, and 303.15) K for 2-Butanone + Aniline, + N-Methylaniline, or + Pyridine Systems

speedsl	1178.00	m/s	303.15	Densities and Speeds of Sound for Binary Liquid Mixtures of Thiolane-I,I-dioxide with Butanone, Pentan-2-one, Pentan-3-one, and 4-Methyl-pentan-2-one at T = (303.15 or 308.15 or 313.15) K
speedsl	1191.00	m/s	298.15	Thermodynamics of ketone + amine mixtures Part IV. Volumetric and speed of sound data at (293.15; 298.15 and 303.15 K) for 2-butanone +dipropylamine, +dibutylamine or +triethylamine systems
speedsl	1136.00	m/s	313.15	Densities and Speeds of Sound for Binary Liquid Mixtures of Thiolane-I,I-dioxide with Butanone, Pentan-2-one, Pentan-3-one, and 4-Methyl-pentan-2-one at T = (303.15 or 308.15 or 313.15) K
speedsl	1158.00	m/s	308.15	Densities and Speeds of Sound for Binary Liquid Mixtures of Thiolane-I,I-dioxide with Butanone, Pentan-2-one, Pentan-3-one, and 4-Methyl-pentan-2-one at T = (303.15 or 308.15 or 313.15) K
srf	0.02	N/m	298.20	KDB
srf	0.02	N/m	298.15	Concentration Dependence of Surface Tension for Very Dilute Aqueous Solutions of Organic Non-Electrolytes

tcondl	0.14	W/m×K	344.54	Thermal Conductivity of Some Oxygenated Fuels and Additives in the Saturated Liquid Phase
tcondl	0.14	W/m×K	323.96	Thermal Conductivity of Some Oxygenated Fuels and Additives in the Saturated Liquid Phase
tcondl	0.14	W/m×K	334.71	Thermal Conductivity of Some Oxygenated Fuels and Additives in the Saturated Liquid Phase
tcondl	0.14	W/m×K	314.26	Thermal Conductivity of Some Oxygenated Fuels and Additives in the Saturated Liquid Phase
tcondl	0.13	W/m×K	354.33	Thermal Conductivity of Some Oxygenated Fuels and Additives in the Saturated Liquid Phase
tcondl	0.13	W/m×K	364.46	Thermal Conductivity of Some Oxygenated Fuels and Additives in the Saturated Liquid Phase
tcondl	0.13	W/m×K	374.56	Thermal Conductivity of Some Oxygenated Fuels and Additives in the Saturated Liquid Phase

tcondl	0.15	W/m×K	305.02	Thermal Conductivity of Some Oxygenated Fuels and Additives in the Saturated Liquid Phase
tcondl	0.15	W/m×K	294.42	Thermal Conductivity of Some Oxygenated Fuels and Additives in the Saturated Liquid Phase
tcondl	0.15	W/m×K	284.48	Thermal Conductivity of Some Oxygenated Fuels and Additives in the Saturated Liquid Phase

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.45436e+01
Coeff. B	-3.04648e+03
Coeff. C	-4.60570e+01
Temperature range (K), min.	259.76
Temperature range (K), max.	376.05

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C \cdot \ln(T) + D \cdot T^2$
Coeff. A	6.69787e+01
Coeff. B	-6.16017e+03
Coeff. C	-7.78365e+00
Coeff. D	6.13927e-06
Temperature range (K), min.	186.48
Temperature range (K), max.	535.50

Datasets

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
308.15	101.30	0.0003160
Reference		https://www.doi.org/10.1021/je8003723

Sources

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<https://www.doi.org/10.1016/j.jct.2009.01.006>
<https://www.doi.org/10.1016/j.jct.2016.10.006>
<https://www.doi.org/10.1021/acs.jced.9b00406>
<https://www.doi.org/10.1021/je200195q>
<https://www.doi.org/10.1021/acs.jced.8b00663>
<https://www.doi.org/10.1021/je5007696>
<https://www.doi.org/10.1016/j.fluid.2019.03.023>
<https://www.doi.org/10.1016/j.tca.2010.09.004>
<https://www.doi.org/10.1021/je0504109>
<https://www.doi.org/10.1016/j.jct.2011.09.028>
<https://www.doi.org/10.1021/acs.jced.9b00341>
<https://www.doi.org/10.1021/je201129y>
<https://www.doi.org/10.1016/j.fluid.2007.08.006>
<https://www.doi.org/10.1016/j.jct.2013.05.035>
<https://www.doi.org/10.1021/je100472t>
<https://www.doi.org/10.1016/j.jct.2017.05.013>
<https://www.doi.org/10.1021/je0498762>
<https://www.doi.org/10.1021/je049655w>
<https://www.doi.org/10.1021/je100998r>
<https://www.doi.org/10.1021/acs.jced.8b01014>
<https://www.doi.org/10.1016/j.fluid.2018.01.019>
<https://www.doi.org/10.1021/je9006585>
imidazolium-1-yl)
<https://www.doi.org/10.1016/j.jct.2015.08.017>
<https://www.doi.org/10.1021/acs.jced.9b00243>
<https://www.doi.org/10.1021/je100341q>

[illegible]

<https://www.doi.org/10.1021/je034137r>
<https://www.doi.org/10.1016/j.fluid.2015.04.017>
<https://www.doi.org/10.1021/je1011604>
<https://www.doi.org/10.1021/je060150a>
<https://www.doi.org/10.1016/j.jct.2014.04.004>
<https://www.doi.org/10.1021/je200150r>
<https://www.doi.org/10.1021/acs.jced.8b00235>
<https://www.doi.org/10.1016/j.jct.2010.12.027>
<https://www.doi.org/10.1021/je100030j>
<https://www.doi.org/10.1016/j.jct.2004.11.007>
<https://www.doi.org/10.1021/je100125x>
<https://www.doi.org/10.1016/j.jct.2013.10.017>
<https://www.doi.org/10.1021/acs.jced.8b00600>
<https://www.doi.org/10.1016/j.jct.2017.02.017>
<https://www.doi.org/10.1021/je400065j>
<https://www.doi.org/10.1016/j.jct.2005.08.002>
<https://www.doi.org/10.1016/j.tca.2004.08.013>
<https://www.doi.org/10.1016/j.fluid.2014.06.021>
<https://www.doi.org/10.1021/je900523k>
<https://www.doi.org/10.1021/acs.jced.9b00179>
<https://www.doi.org/10.1016/j.jct.2006.03.003>
<https://www.doi.org/10.1016/j.fluid.2009.03.008>
<https://www.doi.org/10.1016/j.jct.2016.11.029>
<https://www.doi.org/10.1021/je200822w>
<https://www.doi.org/10.1021/acs.jced.5b01058>
<https://www.doi.org/10.1021/acs.jced.8b00430>
<https://www.doi.org/10.1021/je900547w>
<http://link.springer.com/article/10.1007/BF02311772>
<https://www.doi.org/10.1021/je800883b>
<https://www.doi.org/10.1021/je9003178>
<https://www.doi.org/10.1016/j.jct.2016.09.033>
<https://www.doi.org/10.1016/j.fluid.2014.01.043>
<https://www.doi.org/10.1016/j.jct.2005.04.010>
<https://www.doi.org/10.1021/je5007604>
<https://www.doi.org/10.1016/j.fluid.2006.11.011>
<https://www.doi.org/10.1016/j.jct.2012.09.017>
<https://www.doi.org/10.1016/j.jct.2017.04.019>
<https://www.doi.org/10.1021/acs.jced.8b00552>
<https://www.doi.org/10.1021/je800571y>
<https://www.doi.org/10.1021/je200637v>
<https://www.doi.org/10.1021/acs.jced.6b00230>
<https://www.doi.org/10.1016/j.jct.2016.10.037>
<https://www.cheric.org/files/research/kdb/mol/mol1192.mol>

[illegible]

<https://www.doi.org/10.1021/je400029t>

<https://www.doi.org/10.1016/j.fluid.2018.05.023>

<https://www.doi.org/10.1016/j.fluid.2012.06.011>

<https://www.doi.org/10.1021/je1010054>

Imide
<https://www.doi.org/10.1021/acs.iced.7b00316>

<https://www.doi.org/10.1016/j.fluid.2014.11.020>

<https://www.doi.org/10.1016/j.fluid.2007.02.027>

<https://www.doi.org/10.1021/je049875+>

<https://www.doi.org/10.1021/acs.iced.9b00710>

<https://www.doi.org/10.1016/j.ijct.2016.09.012>

<https://www.doi.org/10.1021/acs.iced.7b01011>

<https://www.doi.org/10.1016/j.itca.2012.04.001>

<https://www.doi.org/10.1021/ie800754w>

<https://www.doi.org/10.1021/je030122h>

<https://www.doi.org/10.1016/j.fluid.2007.06.001>

<http://onschallenge.wikispaces.com/file/view/AqueousDataset003.xlsx/351826032/AqueousDataset003.xlsx>

<https://www.doi.org/10.1021/acs.iced.7b00783>

<https://www.doi.org/10.1021/acs.iced.8b01226>

<https://www.doi.org/10.1021/je034203n>

<https://www.doi.org/10.1016/j.ijct.2016.11.033>

<https://www.doi.org/10.1016/j.fluid.2013.03.054>

<http://pubs.acs.org/doi/abs/10.1021/ci000303l>

<https://www.doi.org/10.1021/jc0405042>

<https://www.doi.org/10.1016/j.ijet.2004.08.002>

<https://www.doi.org/10.1016/j.ijet.2016.08.036>

<https://www.doi.org/10.1021/la200603a>

<https://www.doi.org/10.1016/j.ijet.2016.03.016>

<https://www.doi.org/10.1031/acs.joc.5b00310>

<https://www.doi.org/10.1001/jc3006054>

<https://www.doi.org/10.1001/ja.024.11762>

"10-11-1964" 000007

mium)

<https://doi.org/10.1001/jama.2019.10211>

111 112 113 114 115 116 117 118 119 120 121 122 123 124 125 126 127 128 129 130 131 132 133 134 135 136 137 138 139 140 141 142 143 144 145 146 147 148 149 150 151 152 153 154 155 156 157 158 159 160 161 162 163 164 165 166 167 168 169 170 171 172 173 174 175 176 177 178 179 180 181 182 183 184 185 186 187 188 189 190 191 192 193 194 195 196 197 198 199 200 201 202 203 204 205 206 207 208 209 210 211 212 213 214 215 216 217 218 219 220 221 222 223 224 225 226 227 228 229 230 231 232 233 234 235 236 237 238 239 240 241 242 243 244 245 246 247 248 249 250 251 252 253 254 255 256 257 258 259 260 261 262 263 264 265 266 267 268 269 270 271 272 273 274 275 276 277 278 279 280 281 282 283 284 285 286 287 288 289 290 291 292 293 294 295 296 297 298 299 300 301 302 303 304 305 306 307 308 309 310 311 312 313 314 315 316 317 318 319 320 321 322 323 324 325 326 327 328 329 330 331 332 333 334 335 336 337 338 339 340 341 342 343 344 345 346 347 348 349 350 351 352 353 354 355 356 357 358 359 360 361 362 363 364 365 366 367 368 369 370 371 372 373 374 375 376 377 378 379 380 381 382 383 384 385 386 387 388 389 390 391 392 393 394 395 396 397 398 399 400 401 402 403 404 405 406 407 408 409 410 411 412 413 414 415 416 417 418 419 420 421 422 423 424 425 426 427 428 429 430 431 432 433 434 435 436 437 438 439 440 441 442 443 444 445 446 447 448 449 450 451 452 453 454 455 456 457 458 459 460 461 462 463 464 465 466 467 468 469 470 471 472 473 474 475 476 477 478 479 480 481 482 483 484 485 486 487 488 489 490 491 492 493 494 495 496 497 498 499 500 501 502 503 504 505 506 507 508 509 510 511 512 513 514 515 516 517 518 519 520 521 522 523 524 525 526 527 528 529 530 531 532 533 534 535 536 537 538 539 540 541 542 543 544 545 546 547 548 549 550 551 552 553 554 555 556 557 558 559 560 561 562 563 564 565 566 567 568 569 570 571 572 573 574 575 576 577 578 579 580 581 582 583 584 585 586 587 588 589 590 591 592 593 594 595 596 597 598 599 600 601 602 603 604 605 606 607 608 609 610 611 612 613 614 615 616 617 618 619 620 621 622 623 624 625 626 627 628 629 630 631 632 633 634 635 636 637 638 639 640 641 642 643 644 645 646 647 648 649 650 651 652 653 654 655 656 657 658 659 660 661 662 663 664 665 666 667 668 669 670 671 672 673 674 675 676 677 678 679 680 681 682 683 684 685 686 687 688 689 690 691 692 693 694 695 696 697 698 699 700 701 702 703 704 705 706 707 708 709 710 711 712 713 714 715 716 717 718 719 720 721 722 723 724 725 726 727 728 729 730 731 732 733 734 735 736 737 738 739 740 741 742 743 744 745 746 747 748 749 750 751 752 753 754 755 756 757 758 759 760 761 762 763 764 765 766 767 768 769 770 771 772 773 774 775 776 777 778 779 780 781 782 783 784 785 786 787 788 789 790 791 792 793 794 795 796 797 798 799 800 801 802 803 804 805 806 807 808 809 810 811 812 813 814 815 816 817 818 819 820 821 822 823 824 825 826 827 828 829 830 831 832 833 834 835 836 837 838 839 840 841 842 843 844 845 846 847 848 849 850 851 852 853 854 855 856 857 858 859 860 861 862 863 864 865 866 867 868 869 870 871 872 873 874 875 876 877 878 879 880 881 882 883 884 885 886 887 888 889 890 891 892 893 894 895 896 897 898 899 900 901 902 903 904 905 906 907 908 909 910 911 912 913 914 915 916 917 918 919 920 921 922 923 924 925 926 927 928 929 930 931 932 933 934 935 936 937 938 939 940 941 942 943 944 945 946 947 948 949 950 951 952 953 954 955 956 957 958 959 960 961 962 963 964 965 966 967 968 969 970 971 972 973 974 975 976 977 978 979 980 981 982 983 984 985 986 987 988 989 990 991 992 993 994 995 996 997 998 999 1000

<https://www.industry.gov.au/publications/industry-2020-2021>

<http://www.fishbase.org/ViewPage.do?portalId=32&pageId=3233>

<https://www.doi.org/10.1016/j.joule.2017.05.002>

<https://www.doi.org/10.1016/j.jmoldi.2019.05.003>

<https://www.industry.gov.au/publications/industry-2020-2021>

<https://www.ascl.org/10.1016/j.joi.2007.08.005>

<https://doi.org/10.1021/acs.joc.7b00071>

<https://www.doi.org/10.1021/joc50037c>

<https://www.doi.org/10.1016/j.tca.2012.04.001>

<https://www.doi.org/10.1021/jc050141f>

[illegible]

<https://www.doi.org/10.1021/je900262t>

<https://www.doi.org/10.1021/ie049955d>

<https://www.sciencedirect.com/book/9780128029992/the-vaws-handbook-of-vapor-pressure>

<https://www.doi.org/10.1016/j.jct.2007.01.004>

<https://www.doi.org/10.1016/j.ijct.2016.07.043>

<https://www.doi.org/10.1016/j.fluid.2018.06.003>

http://pubs.acs.org/doi/suppl/10.1021/ci034243x/suppl_file/ci034243xsi20040112_053635.txt

<https://www.doi.org/10.1016/j.fluid.2008.06.004>

<https://www.doi.org/10.1016/j.fluid.2007.06.005>

<https://www.doi.org/10.1021/je050110r>

<https://www.doi.org/10.1016/j.fluid.2005.02.006>

<https://www.doi.org/10.1016/j.fluid.2010.10.008>

<https://www.doi.org/10.1021/ie049793l>

<https://www.doi.org/10.1016/j.fluid.2006.04.010>

<https://www.doi.org/10.1016/j.ijct.2007.06.009>

<https://www.doi.org/10.1021/je060033f>

<https://www.doi.org/10.1016/j.fluid.2016.02.031>

<https://www.doi.org/10.1016/j.ijct.2005.10.001>

<https://www.doi.org/10.1016/j.ijct.2015.03.013>

<https://www.doi.org/10.1016/j.ijct.2009.12.008>

<https://www.doi.org/10.1016/j.ijct.2019.05.011>

<https://www.doi.org/10.1021/ie9010954>

<https://www.doi.org/10.1016/j.fluid.2015.08.003>

<https://www.doi.org/10.1021/acs.iced.8b00190>

<https://www.doi.org/10.1021/ie900826n>

<https://www.doi.org/10.1031/jc0497000>

<https://www.doi.org/10.1031/jc4001894>

<https://www.doi.org/10.1031/cas-icod.8b00003>

<https://www.doi.org/10.1021/jc800246y>

<https://www.doi.org/10.1021/ie060005g>

<https://www.doi.org/10.1021/jc800120n>

<https://www.doi.org/10.1021/jc060403d>

<https://www.doi.org/10.1016/j.jst.2015.03.002>

<https://www.doi.org/10.1001/ja.101030m>

<https://www.doi.org/10.1016/j.tsc.2018.01.012>

<https://www.doi.org/10.1001/ajph.2019.0352>

11. // 11.10.1991/ 11.10.1991

11. // 10 1010 / i : 0010 10 005

11. "11-10-1961" 11-10-1961

14. "11-11-1994" 000000

11. "The first step in the process of creating a new product is to identify a market need." (100%)

Figure 10. The "1000" series.

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Liquid-Liquid and Vapor-Liquid-Liquid Equilibrium of the 2-Butanone + 2-Aminopropanes at infinite dilution of organic solutes in the ionic liquid *1*-butyl-3-methylimidazolium hexafluorophosphate using gas liquid chromatography at 134.15, 152.15, 170.15, 188.15, 206.15, 224.15, 242.15, 260.15, 278.15, 296.15, 314.15, 332.15, 350.15, 368.15, 386.15, 404.15, 422.15, 440.15, 458.15, 476.15, 494.15, 512.15, 530.15, 548.15, 566.15, 584.15, 602.15, 620.15, 638.15, 656.15, 674.15, 692.15, 710.15, 728.15, 746.15, 764.15, 782.15, 800.15, 818.15, 836.15, 854.15, 872.15, 890.15, 908.15, 926.15, 944.15, 962.15, 980.15, 998.15, 1016.15, 1034.15, 1052.15, 1070.15, 1088.15, 1106.15, 1124.15, 1142.15, 1160.15, 1178.15, 1196.15, 1214.15, 1232.15, 1250.15, 1268.15, 1286.15, 1304.15, 1322.15, 1340.15, 1358.15, 1376.15, 1394.15, 1412.15, 1430.15, 1448.15, 1466.15, 1484.15, 1502.15, 1520.15, 1538.15, 1556.15, 1574.15, 1592.15, 1610.15, 1628.15, 1646.15, 1664.15, 1682.15, 1700.15, 1718.15, 1736.15, 1754.15, 1772.15, 1790.15, 1808.15, 1826.15, 1844.15, 1862.15, 1880.15, 1898.15, 1916.15, 1934.15, 1952.15, 1970.15, 1988.15, 2006.15, 2024.15, 2042.15, 2060.15, 2078.15, 2096.15, 2114.15, 2132.15, 2150.15, 2168.15, 2186.15, 2204.15, 2222.15, 2240.15, 2258.15, 2276.15, 2294.15, 2312.15, 2330.15, 2348.15, 2366.15, 2384.15, 2402.15, 2420.15, 2438.15, 2456.15, 2474.15, 2492.15, 2510.15, 2528.15, 2546.15, 2564.15, 2582.15, 2600.15, 2618.15, 2636.15, 2654.15, 2672.15, 2690.15, 2708.15, 2726.15, 2744.15, 2762.15, 2780.15, 2798.15, 2816.15, 2834.15, 2852.15, 2870.15, 2888.15, 2906.15, 2924.15, 2942.15, 2960.15, 2978.15, 2996.15, 3014.15, 3032.15, 3050.15, 3068.15, 3086.15, 3104.15, 3122.15, 3140.15, 3158.15, 3176.15, 3194.15, 3212.15, 3230.15, 3248.15, 3266.15, 3284.15, 3302.15, 3320.15, 3338.15, 3356.15, 3374.15, 3392.15, 3410.15, 3428.15, 3446.15, 3464.15, 3482.15, 3500.15, 3518.15, 3536.15, 3554.15, 3572.15, 3590.15, 3608.15, 3626.15, 3644.15, 3662.15, 3680.15, 3698.15, 3716.15, 3734.15, 3752.15, 3770.15, 3788.15, 3806.15, 3824.15, 3842.15, 3860.15, 3878.15, 3896.15, 3914.15, 3932.15, 3950.15, 3968.15, 3986.15, 4004.15, 4022.15, 4040.15, 4058.15, 4076.15, 4094.15, 4112.15, 4130.15, 4148.15, 4166.15, 4184.15, 4202.15, 4220.15, 4238.15, 4256.15, 4274.15, 4292.15, 4310.15, 4328.15, 4346.15, 4364.15, 4382.15, 4400.15, 4418.15, 4436.15, 4454.15, 4472.15, 4490.15, 4508.15, 4526.15, 4544.15, 4562.15, 4580.15, 4598.15, 4616.15, 4634.15, 4652.15, 4670.15, 4688.15, 4706.15, 4724.15, 4742.15, 4760.15, 4778.15, 4796.15, 4814.15, 4832.15, 4850.15, 4868.15, 4886.15, 4904.15, 4922.15, 4940.15, 4958.15, 4976.15, 4994.15, 5012.15, 5030.15, 5048.15, 5066.15, 5084.15, 5102.15, 5120.15, 5138.15, 5156.15, 5174.15, 5192.15, 5210.15, 5228.15, 5246.15, 5264.15, 5282.15, 5300.15, 5318.15, 5336.15, 5354.15, 5372.15, 5390.15, 5408.15, 5426.15, 5444.15, 5462.15, 5480.15, 5498.15, 5516.15, 5534.15, 5552.15, 5570.15, 5588.15, 5606.15, 5624.15, 5642.15, 5660.15, 5678.15, 5696.15, 5714.15, 5732.15, 5750.15, 5768.15, 5786.15, 5804.15, 5822.15, 5840.15, 5858.15, 5876.15, 5894.15, 5912.15, 5930.15, 5948.15, 5966.15, 5984.15, 6002.15, 6020.15, 6038.15, 6056.15, 6074.15, 6092.15, 6110.15, 6128.15, 6146.15, 6164.15, 6182.15, 6200.15, 6218.15, 6236.15, 6254.15, 6272.15, 6290.15, 6308.15, 6326.15, 6344.15, 6362.15, 6380.15, 6398.15, 6416.15, 6434.15, 6452.15, 6470.15, 6488.15, 6506.15, 6524.15, 6542.15, 6560.15, 6578.15, 6596.15, 6614.15, 6632.15, 6650.15, 6668.15, 6686.15, 6704.15, 6722.15, 6740.15, 6758.15, 6776.15, 6794.15, 6812.15, 6830.15, 6848.15, 6866.15, 6884.15, 6902.15, 6920.15, 6938.15, 6956.15, 6974.15, 6992.15, 7010.15, 7028.15, 7046.15, 7064.15, 7082.15, 7100.15, 7118.15, 7136.15, 7154.15, 7172.15, 7190.15, 7208.15, 7226.15, 7244.15, 7262.15, 7280.15, 7298.15, 7316.15, 7334.15, 7352.15, 7370.15, 7388.15, 7406.15, 7424.15, 7442.15, 7460.15, 7478.15, 7496.15, 7514.15, 7532.15, 7550.15, 7568.15, 7586.15, 7604.15, 7622.15, 7640.15, 7658.15, 7676.15, 7694.15, 7712.15, 7730.15, 7748.15, 7766.15, 7784.15, 7802.15, 7820.15, 7838.15, 7856.15, 7874.15, 7892.15, 7910.15, 7928.15, 7946.15, 7964.15, 7982.15, 8000.15, 8018.15, 8036.15, 8054.15, 8072.15, 8090.15, 8108.15, 8126.15, 8144.15, 8162.15, 8180.15, 8198.15, 8216.15, 8234.15, 8252.15, 8270.1

<https://www.doi.org/10.1021/je1004643>

<https://www.doi.org/10.1016/j.ijct.2010.12.019>

<https://www.doi.org/10.1016/j.ijct.2009.08.012>

<https://www.doi.org/10.1016/j.ijct.2016.07.001>

<https://www.doi.org/10.1016/j.ijct.2016.07.013>

<https://www.doi.org/10.1021/ie7004038>

<https://www.doi.org/10.1016/j.fluid.2013.07.037>

<https://www.doi.org/10.1016/j.ijct.2010.12.020>

<https://www.doi.org/10.1021/ie8003723>

<http://webbook.nist.gov/cgi/lookup.cgi?ID=C78933&Units=SI>

<https://www.doi.org/10.1016/j.ijct.2007.04.004>

<https://www.doi.org/10.1016/j.ijct.2005.07.020>

<https://www.doi.org/10.1021/ie301062a>

<https://www.doi.org/10.1021/acs.jced.7b00288>

<https://www.doi.org/10.1016/j.ijct.2016.08.034>

<https://www.doi.org/10.1021/ie900056u>

<https://www.doi.org/10.1016/j.ijct.2013.05.030>

<https://www.doi.org/10.1016/j.fluid.2009.13.030>

<https://www.doi.org/10.1016/j.ijct.2008.03.011>

<https://www.doi.org/10.1021/ie049818a>

<https://www.doi.org/10.1031/acs-iacd.9b00854>

<https://www.doi.org/10.1016/j.ijet.2016.11.014>

<https://www.doi.org/10.1016/j.ijat.2017.03.008>

<https://www.doi.org/10.1016/j.fluid.2011.05.004>

<https://www.doi.org/10.1031/jc800658v>

<https://www.ehrii.org/research/kdh/beprep/ebewprep.php?ampid=1102>

<https://www.doi.org/10.1021/jc500050n>

<http://www.doi.org/10.1016/j.jst.2013.01.004>

<https://www.ehrii.org/research/ldh/harper/chowharp.php?ampid=1400>

<https://www.doi.org/10.1016/j.jst.2007.02.002>

1001-1004

<https://doi.org/10.1016/j.jmb.2019.03.010>

<https://doi.org/10.1016/j.fluc.2021.01.011>

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11. "1991/1992" 171-225, 199

100-11176-11189 (100-10100"/5") 110017-10001

http://www.elsevier.com/locate/jmb

<https://www.doi.org/10.1016/j.jmbs.2016.05.001>

<https://www.astron.gy/foros2/?action=profile&id=33>

<https://www.washingtonpost.com/archive/local/2017/05/01/2017-05-01/>

<https://www.aom.org/for-rez/press-room>

<https://www.ncbi.nlm.nih.gov/pmc/articles/PMC6116216/>

Solubility of methylphosphonic acid in selected organic solvents: <https://www.doi.org/10.1016/j.fluid.2015.01.009>
 Solubility Modeling and Solvent Effect for Flubendazole in 12 Neat Solvents: <https://www.doi.org/10.1021/acs.jced.8b01126>
 Quaternary isothermal vapor-liquid equilibrium of the model biofuel <https://www.doi.org/10.1016/j.fluid.2018.04.009>
 Vapor-liquid equilibrium for systems of <https://www.doi.org/10.1016/j.fluid.2005.06.024>
 diethyl carbonate and ketones and <https://www.doi.org/10.1016/j.jct.2012.02.033>
 diethyl carbonate and ketones using <https://www.doi.org/10.1016/j.jct.2016.06.033>
 Relativistic pseudopotential calculation: <https://www.doi.org/10.1016/j.jct.2016.12.028>
 parameters for the Lennard-Jones and <https://www.doi.org/10.1021/je050544m>
 Lennard-Jones 12-6 potential systems <https://www.doi.org/10.1021/acs.jced.6b00725>
 in (water + diethyl carbonate) with <https://www.doi.org/10.1021/acs.jced.6b00725>
 acetone or 2-butanone and flazoles in <https://www.doi.org/10.1021/acs.jced.6b00725>
 nine pure organic solvents and liquid <https://www.doi.org/10.1021/acs.jced.6b00725>
 mixture coefficients at infinite dilution <https://www.doi.org/10.1021/acs.jced.6b00725>
 from the 1,2-methyldiazolium <https://www.doi.org/10.1021/acs.jced.6b00725>
 ionic vapor-liquid liquid phase <https://www.doi.org/10.1021/acs.jced.6b00725>
 external measurements of three <https://www.doi.org/10.1021/acs.jced.6b00725>
 ternary Water + 2-Butanone + Aliphatic <https://www.doi.org/10.1021/acs.jced.6b00725>
 Alcohol (Ethanol, 1-Propanol, <https://www.doi.org/10.1021/acs.jced.6b00725>
 2-Propanol) Systems at 101.3 kPa:

Legend

af:	Acentric Factor
affp:	Proton affinity
aignt:	Autoignition Temperature
basg:	Gas basicity
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
ea:	Electron affinity
fl:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpc:	Flash Point (Closed Cup Method)
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
vpap:	Vapor pressure

rfi:	Refractive Index
rhoc:	Critical density
rhof:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tc:	Critical Temperature
tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility

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