p-Xylene

Other names:	1,4-Dimethylbenzene
	1,4-Xylene
	1,4-dimethyl-benzene (p-xylene)
	4-Methyltoluene
	Benzene, 1,4-dimethyl-
	Chromar
	NSC 72419
	Scintillar
	p-Dimethylbenzene
	p-Methyltoluene
	p-Xylol
	para-Xylene
Inchi:	InChI=1S/C8H10/c1-7-3-5-8(2)6-4-7/h3-6H,1-2H3
InchiKey:	URLKBWYHVLBVBO-UHFFFAOYSA-N
Formula:	C8H10
SMILES:	Cc1ccc(C)cc1
Mol. weight [g/mol]:	106.17
CAS:	106-42-3

Physical Properties

Property code	Value	Unit	Source
af	0.3200		KDB
affp	790.50 ± 1.10	kJ/mol	NIST Webbook
affp	794.40	kJ/mol	NIST Webbook
affp	793.70	kJ/mol	NIST Webbook
aigt	738.71	K	KDB
basg	766.90	kJ/mol	NIST Webbook
basg	771.30 ± 1.40	kJ/mol	NIST Webbook
basg	766.80	kJ/mol	NIST Webbook
chl	-4552.86 ± 0.92	kJ/mol	NIST Webbook
chl	-4551.44 ± 0.50	kJ/mol	NIST Webbook
chl	-4565.90	kJ/mol	NIST Webbook
chl	-4551.70	kJ/mol	NIST Webbook
cpl	181.73	J/mol×K	Thermodynamics of mixtures involving some (benzene derivatives + benzonitrile)
dm	0.10	debye	KDB

dvisc	0.0006090	Pa×s	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of o-Xylene, m-Xylene, p-Xylene, and Isopropylbenzene with 2-Butanone at 298.15 K
dvisc	0.0006090	Pa×s	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of o-Xylene, m-Xylene, p-Xylene, and Isopropylbenzene with 4-Methylpentan-2-one at 298.15 K
ea	0.00 ± 0.00	eV	NIST Webbook
ep	44.20	J/mol×K	NIST Webbook
fll	1.10	% in Air	KDB
flu	6.60	% in Air	KDB
fpo	300.37	K	KDB
gf	121.20	kJ/mol	KDB
gyrad	3.7960		KDB
hcg	4552.86	kJ/mol	KDB
hcn	4332.784	kJ/mol	KDB
hf	17.90 ± 1.00	kJ/mol	NIST Webbook
hf	17.96	kJ/mol	KDB
hfl	-24.40 ± 1.00	kJ/mol	NIST Webbook
hfus	10.13	kJ/mol	Joback Method
hvap	36.34	kJ/mol	Joback Method
ie	8.45 ± 0.01	eV	NIST Webbook
ie	8.48	eV	NIST Webbook
ie	8.44	eV	NIST Webbook
ie	8.60 ± 0.03	eV	NIST Webbook
ie	8.45	eV	NIST Webbook
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ie	8.52 ± 0.01	eV	NIST Webbook
ie	8.44 ± 0.05	eV	NIST Webbook
ie	8.44 ± 0.02	eV	NIST Webbook
ie	8.37 ± 0.02	eV	NIST Webbook
log10ws	-2.77		Aqueous Solubility Prediction Method
log10ws	-2.77		Estimated Solubility Method
logp	2.303		Crippen Method
mcvol	99.820	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=2)		KDB
pc	3510.70 ± 5.00	kPa	NIST Webbook

pc	3343.73 ± 151.99	kPa	NIST Webbook
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pc	3617.50 ± 100.00	kPa	NIST Webbook
pc	3510.00 ± 20.00	kPa	NIST Webbook
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ripol	1139.00	NIST Webbook
ripol	1164.00	NIST Webbook
ripol	1117.00	NIST Webbook
ripol	1137.00	NIST Webbook
ripol	1137.00	NIST Webbook
ripol	1117.00	NIST Webbook
ripol	1154.20	NIST Webbook
ripol	1142.00	NIST Webbook
ripol	1165.00	NIST Webbook
ripol	1129.00	NIST Webbook
ripol	1180.00	NIST Webbook
ripol	1142.00	NIST Webbook
ripol	1136.00	NIST Webbook
ripol	1156.00	NIST Webbook
ripol	1178.00	NIST Webbook
ripol	1170.00	NIST Webbook
ripol	1163.00	NIST Webbook

ripol	1182.00		NIST Webbook
ripol	1189.00		NIST Webbook
ripol	1118.60		NIST Webbook
ripol	1134.80		NIST Webbook
ripol	1169.20		NIST Webbook
ripol	1143.00		NIST Webbook
ripol	1169.77		NIST Webbook
ripol	1145.24		NIST Webbook
ripol	1149.89		NIST Webbook
ripol	1129.00		NIST Webbook
ripol	1138.90		NIST Webbook
ripol	1134.00		NIST Webbook
sl	253.10	J/mol×K	NIST Webbook
sl	247.15	J/mol×K	NIST Webbook
sl	243.51	J/mol×K	NIST Webbook
tb	411.52	K	KDB
tb	411.21	K	Investigation on Thermodynamics in Separation for Ethylene Glycol + Neopentyl Glycol System by Azeotropic Distillation
tb	411.45	K	Vapour-liquid equilibrium measurements and extractive distillation process design for separation of azeotropic mixture (dimethyl carbonate + ethanol)
tb	411.45	K	Separation of azeotrope (2,2,3,3-tetrafluoro-1-propanol + water): Isobaric vapour-liquid phase equilibrium measurements and azeotropic distillation
tb	411.40	K	Isobaric vapor-liquid equilibrium for the binary mixtures of nonane with cyclohexane, toluene, m-xylene, or p-xylene at 101.3 kPa
tb	411.49	K	Isobaric Vapor-Liquid Equilibrium Measurements for Separation of Azeotrope (Methanol + Methyl Acetate)
tb	411.37	K	Isobaric Vapor-Liquid Equilibium for the Binary Systems of Methyl Formate with o-Xylene, m-Xylene, p-Xylene, and Ethylbenzene at 101.33 kPa

tb	411.23	K	Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures of Ethanol, Methylcyclohexane and p-Xylene
tc	616.20	K	KDB
tf	285.90	K	Aqueous Solubility Prediction Method
tf	286.30	K	KDB
tt	286.40 ± 0.01	K	NIST Webbook
tt	286.30 ± 0.30	K	NIST Webbook
vc	0.378	m3/kmol	KDB
vc	0.378	m3/kmol	NIST Webbook
zc	0.2590380		KDB
zra	0.26		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	211.09 ± 0.42	J/mol×K	523.15	NIST Webbook
cpg	166.52 ± 0.33	J/mol×K	398.15	NIST Webbook
cpg	175.82 ± 0.35	J/mol×K	423.15	NIST Webbook
cpg	189.10 ± 1.70	J/mol×K	463.00	NIST Webbook
cpg	178.20 ± 1.70	J/mol×K	428.00	NIST Webbook
cpg	185.40 ± 0.37	J/mol×K	448.15	NIST Webbook
cpg	194.17 ± 0.39	J/mol×K	473.15	NIST Webbook
cpg	202.92 ± 0.41	J/mol×K	498.15	NIST Webbook
cpg	163.20 ± 1.70	J/mol×K	393.00	NIST Webbook
cpl	182.56	J/mol×K	298.15	Isobaric molar heat capacities of the ternary system dimethyl carbonate + p-xylene + n-decane
cpl	198.70	J/mol×K	336.00	NIST Webbook
cpl	186.15	J/mol×K	308.15	Isobaric molar heat capacities of the ternary system dimethyl carbonate + p-xylene + n-decane
cpl	182.22	J/mol×K	298.15	NIST Webbook

cpl	178.86	J/mol×K	288.15	Isobaric molar heat capacities of the ternary system dimethyl carbonate + p-xylene + n-decane
cpl	183.65	J/mol×K	298.15	NIST Webbook
cpl	181.94	J/mol×K	298.15	NIST Webbook
cpl	181.79	J/mol×K	298.15	NIST Webbook
cpl	181.55	J/mol×K	298.15	NIST Webbook
cpl	181.70	J/mol×K	298.15	NIST Webbook
cpl	181.60	J/mol×K	298.00	NIST Webbook
cpl	184.90	J/mol×K	298.00	NIST Webbook
cpl	183.76	J/mol×K	298.15	NIST Webbook
cpl	180.30	J/mol×K	299.00	NIST Webbook
cpl	176.60	J/mol×K	303.00	NIST Webbook
cpl	181.90	J/mol×K	298.15	NIST Webbook
dvisc	0.0003809	Pa×s	343.15	Densities and Viscosities of N-Formylmorpholine (NFM) + p-Xylene, + o-Xylene, + m-Xylene at Different Temperatures and Atmospheric Pressure
dvisc	0.0005730	Pa×s	303.15	Volumetric and Viscometric Behavior of the Binary System: (Hexan-1-ol + p-Xylene)
dvisc	0.0005120	Pa×s	313.15	Volumetric and Viscometric Behavior of the Binary System: (Hexan-1-ol + p-Xylene)
dvisc	0.0004610	Pa×s	323.15	Volumetric and Viscometric Behavior of the Binary System: (Hexan-1-ol + p-Xylene)
dvisc	0.0005410	Pa×s	308.15	Density and Viscosity of the Binary Mixtures of Hexan-1-ol with Isomeric Xylenes at T = (308.15 and 318.15) K and Atmospheric Pressure

dvisc	0.0004860	Pa×s	318.15	Density and Viscosity of the Binary Mixtures of Hexan-1-ol with Isomeric Xylenes at T = (308.15 and 318.15) K and Atmospheric Pressure
dvisc	0.0006120	Pa×s	298.15	Densities and Viscosities of N-Formylmorpholine (NFM) + p-Xylene, + o-Xylene, + m-Xylene at Different Temperatures and Atmospheric Pressure
dvisc	0.0005756	Pa×s	303.15	Densities and Viscosities of N-Formylmorpholine (NFM) + p-Xylene, + o-Xylene, + m-Xylene at Different Temperatures and Atmospheric Pressure
dvisc	0.0005140	Pa×s	313.15	Densities and Viscosities of N-Formylmorpholine (NFM) + p-Xylene, + o-Xylene, + m-Xylene at Different Temperatures and Atmospheric Pressure
dvisc	0.0004641	Pa×s	323.15	Densities and Viscosities of N-Formylmorpholine (NFM) + p-Xylene, + o-Xylene, + m-Xylene at Different Temperatures and Atmospheric Pressure

dvisc	0.0004171	Pa×s	333.15	Densities and Viscosities of N-Formylmorpholine (NFM) + p-Xylene, + o-Xylene, + m-Xylene at Different Temperatures and Atmospheric Pressure
dvisc	0.0005760	Pa×s	303.15	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene with Anisole at (288.15, 293.15, 298.15, and 303.15) K
dvisc	0.0003487	Pa×s	353.15	Densities and Viscosities of N-Formylmorpholine (NFM) + p-Xylene, + o-Xylene, + m-Xylene at Different Temperatures and Atmospheric Pressure
dvisc	0.0005726	Pa×s	303.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0005374	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K

dvisc	0.0006110	Pa×s	298.15	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene with Anisole at (288.15, 293.15, 298.15, and 303.15) K
dvisc	0.0004882	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0004595	Pa×s	323.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0004439	Pa×s	328.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K

dvisc	0.0006500	Pa×s	293.15	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene with Anisole at (288.15, 293.15, 298.15, and 303.15) K
dvisc	0.0005660	Pa×s	303.15	Thermophysical Properties of Isoamyl Acetate or Methyl Benzoate + Hydrocarbon Binary Mixtures, at (303.15 and 313.15) K
dvisc	0.0005170	Pa×s	313.15	Thermophysical Properties of Isoamyl Acetate or Methyl Benzoate + Hydrocarbon Binary Mixtures, at (303.15 and 313.15) K
dvisc	0.0006090	Pa×s	298.15	Densities and Viscosities of Binary Mixtures of Methyl 4-Chlorobutyrate with Aromatic Hydrocarbons at T) (298.15 to 318.15) K
dvisc	0.0005410	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of Methyl 4-Chlorobutyrate with Aromatic Hydrocarbons at T) (298.15 to 318.15) K
dvisc	0.0004840	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of Methyl 4-Chlorobutyrate with Aromatic Hydrocarbons at T) (298.15 to 318.15) K

dvisc	0.0007010	Pa×s	288.15	Viscosities, Densities, and Speeds of Sound of Binary Mixtures of Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene with Anisole at (288.15, 293.15, 298.15, and 303.15) K
dvisc	0.0003382	Pa×s	353.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0003783	Pa×s	343.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0004298	Pa×s	333.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0004599	Pa×s	323.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures

dvisc	0.0005080	Pa×s	313.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0005715	Pa×s	303.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0006162	Pa×s	298.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0005170	Pa×s	313.15	Viscosity, Density, and Refractive Index of Some (Ester + Hydrocarbon) Binary Mixtures at 303.15 K and 313.15 K
dvisc	0.0005660	Pa×s	303.15	Viscosity, Density, and Refractive Index of Some (Ester + Hydrocarbon) Binary Mixtures at 303.15 K and 313.15 K
dvisc	0.0004599	Pa×s	323.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Sulfolane with Benzene, Toluene, Ethylbenzene, p-Xylene, o-Xylene, and m-Xylene at 303.15 and 323.15 K and Atmospheric Pressure

dvisc	0.0005715	Pa×s	303.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Sulfolane with Benzene, Toluene, Ethylbenzene, p-Xylene, o-Xylene, and m-Xylene at 303.15 and 323.15 K and Atmospheric Pressure
dvisc	0.0006078	Pa×s	298.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Sulfolane with Benzene, Toluene, Ethylbenzene, p-Xylene, o-Xylene, and m-Xylene at 303.15 and 323.15 K and Atmospheric Pressure
dvisc	0.0006130	Pa×s	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for CmH2m+1(OCH2CH2)nOH (m) 1 or 2 or 4 andn) 1) + Benzene, + Toluene, + (o-, m-, and p-) Xylenes, + Ethylbenzene, and + Cyclohexane
dvisc	0.0004610	Pa×s	323.15	Viscometric Studies of Molecular Interactions in Binary Liquid Mixtures of Isomeric Xylenes with Methanol

dvisc	0.0004860	Pa×s	318.15	Viscometric Studies of Molecular Interactions in Binary Liquid Mixtures of Isomeric Xylenes with Methanol
dvisc	0.0005140	Pa×s	313.15	Viscometric Studies of Molecular Interactions in Binary Liquid Mixtures of Isomeric Xylenes with Methanol
dvisc	0.0006110	Pa×s	298.15	Ultrasonic and viscometric study of molecular interactions in binary mixtures of aniline with 1-propanol, 2-propanol, 2-methyl-1-propanol, and 2-methyl-2-propanol at different temperatures
dvisc	0.0005420	Pa×s	308.15	Viscometric Studies of Molecular Interactions in Binary Liquid Mixtures of Isomeric Xylenes with Methanol
dvisc	0.0005740	Pa×s	303.15	Viscometric Studies of Molecular Interactions in Binary Liquid Mixtures of Isomeric Xylenes with Methanol
dvisc	0.0004912	Pa×s	318.15	Ultrasonic and viscometric study of molecular interactions in binary mixtures of aniline with 1-propanol, 2-propanol, 2-methyl-1-propanol, and 2-methyl-2-propanol at different temperatures

dvisc	0.0005501	Pa×s	308.15	Ultrasonic and viscometric study of molecular interactions in binary mixtures of aniline with 1-propanol, 2-propanol, 2-methyl-1-propanol, and 2-methyl-2-propanol at different temperatures
dvisc	0.0005400	Pa×s	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for CmH2m+1(OCH2CH2)nOH (m) 1 or 2 or 4 andn) 1) + Benzene, + Toluene, + (o-, m-, and p-) Xylenes, + Ethylbenzene, and + Cyclohexane
dvisc	0.0005178	Pa×s	313.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0004189	Pa×s	333.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
hfust	17.11	kJ/mol	286.39	NIST Webbook
hfust	17.11	kJ/mol	286.30	NIST Webbook
hfust	17.11	kJ/mol	286.30	NIST Webbook
hfust	16.93	kJ/mol	286.30	NIST Webbook
hfust	17.10	kJ/mol	286.30	NIST Webbook

hfust	17.12	kJ/mol	286.40	NIST Webbook
hsubt	60.80	kJ/mol	286.00	NIST Webbook
hsubt	59.40	kJ/mol	266.50	NIST Webbook
hvapt	35.67	kJ/mol	411.50	NIST Webbook
hvapt	35.98	kJ/mol	411.40	KDB
hvapt	42.57	kJ/mol	298.00	Enthalpies of Vaporization and Vapor Pressures of Some Deuterated Hydrocarbons. Liquid-Vapor Pressure Isotope Effects
hvapt	40.30	kJ/mol	353.00	NIST Webbook
hvapt	37.30	kJ/mol	437.00	NIST Webbook
hvapt	36.10	kJ/mol	506.50	NIST Webbook
hvapt	36.20	kJ/mol	583.50	NIST Webbook
hvapt	42.40	kJ/mol	369.50	NIST Webbook
hvapt	36.00 ± 0.10	kJ/mol	411.00	NIST Webbook
hvapt	34.50 ± 0.10	kJ/mol	436.00	NIST Webbook
hvapt	30.50 ± 0.10	kJ/mol	484.00	NIST Webbook
hvapt	24.70 ± 0.10	kJ/mol	540.00	NIST Webbook
hvapt	37.30	kJ/mol	395.00	NIST Webbook
hvapt	41.60	kJ/mol	323.00	NIST Webbook
hvapt	40.10	kJ/mol	372.50	NIST Webbook
pvap	97.30	kPa	410.00	Vapor-Liquid Equilibria and Excess Properties of the Binary System Vinyl Acetate + p-Xylene
pvap	16.85	kPa	355.15	Vapour-liquid equilibrium for tripropylene glycol + aromatic hydrocarbons binary systems: Experimental data and regression
pvap	20.30	kPa	360.15	Vapour-liquid equilibrium for tripropylene glycol + aromatic hydrocarbons binary systems: Experimental data and regression

pvap	24.30	kPa	365.15	Vapour-liquid equilibrium for tripropylene glycol + aromatic hydrocarbons binary systems: Experimental data and regression
pvap	1.12	kPa	298.15	(Vapour + liquid) equilibria of (1-butanol + benzene, or toluene, or o-, or m-, or p-xylene) at T = 308.15 K
pvap	101.30	kPa	411.45	Separation of azeotrope (2,2,3,3-tetrafluoro-1-propanol + water): Isobaric vapour-liquid phase equilibrium measurements and azeotropic distillation
pvap	101.30	kPa	411.45	Vapour-liquid equilibrium measurements and extractive distillation process design for separation of azeotropic mixture (dimethyl carbonate + ethanol)
pvap	101.30	kPa	411.21	Investigation on Thermodynamics in Separation for Ethylene Glycol + Neopentyl Glycol System by Azeotropic Distillation
pvap	93.13	kPa	408.37	Refractive Index and Vapor-Liquid Equilibrium Data for the Binary Systems of Anisole with Xylene Isomers at 93.13 kPa
pvap	97.30	kPa	410.00	Isobaric Vapor-Liquid Equilibria at 97.3 kPa and Excess Properties at (303.15, 308.15, and 313.15) K of Binary Mixture of p-Xylene + Decane

pvap	13.90	kPa	350.15	Vapour-liquid equilibrium for tripropylene glycol + aromatic hydrocarbons binary systems: Experimental data and regression
pvap	40.00	kPa	379.85	Isobaric Vapor Liquid Equilibria for Binary Systems Comprising 1-Chloro-2-ethylhexane, 2-Ethyl-1-hexanol, p-Xylene, and N-Methylpyrrolidone (NMP) at 40.0 kPa
pvap	100.04	kPa	410.78	Isobaric Vapor Liquid Equilibrium for Binary Systems of 2,2,4-Trimethylpentane with o-Xylene, m-Xylene, p-Xylene, and Ethylbenzene at 250 kPa
pvap	105.00	kPa	412.63	Isobaric Vapor Liquid Equilibrium for Binary Systems of 2,2,4-Trimethylpentane with o-Xylene, m-Xylene, p-Xylene, and Ethylbenzene at 250 kPa
pvap	124.93	kPa	419.48	Isobaric Vapor Liquid Equilibrium for Binary Systems of 2,2,4-Trimethylpentane with o-Xylene, m-Xylene, p-Xylene, and Ethylbenzene at 250 kPa
pvap	174.88	kPa	433.57	Isobaric Vapor Liquid Equilibrium for Binary Systems of 2,2,4-Trimethylpentane with o-Xylene, m-Xylene, p-Xylene, and Ethylbenzene at 250 kPa

pvap	199.86	kPa	439.37	Isobaric Vapor Liquid Equilibrium for Binary Systems of 2,2,4-Trimethylpentane with o-Xylene, m-Xylene, p-Xylene, and Ethylbenzene at 250 kPa
pvap	224.86	kPa	444.66	Isobaric Vapor Liquid Equilibrium for Binary Systems of 2,2,4-Trimethylpentane with o-Xylene, m-Xylene, p-Xylene, and Ethylbenzene at 250 kPa
pvap	250.04	kPa	449.56	Isobaric Vapor Liquid Equilibrium for Binary Systems of 2,2,4-Trimethylpentane with o-Xylene, m-Xylene, p-Xylene, and Ethylbenzene at 250 kPa
pvap	250.00	kPa	449.60	Isobaric Vapor Liquid Equilibrium for Binary Systems of 2,2,4-Trimethylpentane with o-Xylene, m-Xylene, p-Xylene, and Ethylbenzene at 250 kPa
pvap	11.39	kPa	345.15	Vapour-liquid equilibrium for tripropylene glycol + aromatic hydrocarbons binary systems: Experimental data and regression
pvap	92.43	kPa	408.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression

pvap	80.87	kPa	403.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	60.79	kPa	393.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	44.56	kPa	383.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	32.04	kPa	373.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	22.80	kPa	363.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	19.04	kPa	358.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression

pvap	6.85	kPa	333.15	Vapor liquid equilibria and density measurement for binary mixtures of o-xylene + NMF, m-xylene +NMF and p-xylene +NMF at 333.15 K, 343.15 K and 353.15 K from 0 kPa to 101.3 kPa
pvap	10.63	kPa	343.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	7.00	kPa	333.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	4.42	kPa	323.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	2.49	kPa	313.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	1.56	kPa	303.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression

pvap	101.30	kPa	411.40	Isobaric vapor-liquid equilibrium for the binary mixtures of nonane with cyclohexane, toluene, m-xylene, or p-xylene at 101.3 kPa
pvap	15.61	kPa	353.15	Vapor liquid equilibria and density measurement for binary mixtures of o-xylene + NMF, m-xylene +NMF and p-xylene +NMF at 333.15 K, 343.15 K and 353.15 K from 0 kPa to 101.3 kPa
pvap	10.50	kPa	343.15	Vapor liquid equilibria and density measurement for binary mixtures of o-xylene + NMF, m-xylene +NMF and p-xylene +NMF at 333.15 K, 343.15 K and 353.15 K from 0 kPa to 101.3 kPa
pvap	15.72	kPa	353.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
rfi	1.49850		288.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K
rfi	1.49321		298.15	Effect of an Ionic Liquid (IL) Cation on the Ternary System (IL + p-Xylene + Hexane) at T= 298.15 K

rfi	1.49290	298.15	Densities, Excess Molar Volumes, Viscosity, and Refractive Indices of Binary Mixtures of Ethanoic Acid and Trichloroethylene with Dimethylbenzenes at Different Temperatures	
rfi	1.49300	298.15	Isobaric Vapor-Liquid Equilibria for the Binary Mixtures of Styrene with Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene	
rfi	1.49250	298.15	Liquid-liquid equilibria for mixtures of (Furfural + an Aromatic hydrocarbon + an alkane) at T=298.15 K	
rfi	1.49220	293.15	Volumetric properties of binary mixtures of tributylamine with benzene derivatives and comparison with ERAS model results at temperatures from (293.15 to 333.15) K	
rfi	1.48580	293.15	Activity coefficients and excess Gibbs free energy of some binary mixtures formed by p-cresol at 95.23 kPa	
rfi	1.49580	298.15	A study of densities and volumetric properties of binary mixtures of N-methyl-2-pyrrolidone with xylene at different temperatures and atmospheric pressure	

rfi	1.49580	298.15	Densities and volumetric properties of binary mixtures of xylene with N,N-dimethylformamide at different temperatures
rfi	1.49590	293.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K
rfi	1.49150	303.15	Excess molar volumes and refractive indices of (methoxybenzene + benzene, or toluene, or o-xylene, or m-xylene, or p-xylene, or mesitylene) binary mixtures between T = (288.15 to 303.15) K
rfi	1.49330	298.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K
rfi	1.49070	303.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K
rfi	1.48810	308.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K

rfi	1.48550	313.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K	
rfi	1.48300	318.15	Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K	
rfi	1.49850	288.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K	
rfi	1.49590	293.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K	

rfi	1.49330	298.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K
rfi	1.49070	303.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K
rfi	1.48810	308.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K
rfi	1.48550	313.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K

rfi	1.48300	318.15	Densities, Refractive Indices, and Excess Properties of Binary Mixtures of 1,4-Dioxane with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from (288.15 to 318.15) K
rfi	1.50040	293.15	Solubilities of Methyldiphenylphosphine Oxide in Selected Solvents
rfi	1.49312	298.15	Density, Speed of Sound, and Refractive Index for Binary Mixtures Containing Cycloalkanes with o-Xylene, m-Xylene, p-Xylene, and Mesitylene at T = (298.15 and 313.15) K
rfi	1.48444	313.15	Density, Speed of Sound, and Refractive Index for Binary Mixtures Containing Cycloalkanes with o-Xylene, m-Xylene, p-Xylene, and Mesitylene at T = (298.15 and 313.15) K
rfi	1.48580	293.15	Bubble points of some binary mixtures formed by o-cresol at 95.75 kPa

rfi	1.49290	298.15	Excess molar volumes and refractive indices of (methoxybenzene + benzene, or toluene, or o-xylene, or m-xylene, or p-xylene, or mesitylene) binary mixtures between T = (288.15 to 303.15) K	
rfi	1.49580	293.15	Excess molar volumes and refractive indices of (methoxybenzene + benzene, or toluene, or o-xylene, or m-xylene, or p-xylene, or mesitylene) binary mixtures between T = (288.15 to 303.15) K	
rfi	1.49830	288.15	Excess molar volumes and refractive indices of (methoxybenzene + benzene, or toluene, or o-xylene, or m-xylene, or p-xylene, or mesitylene) binary mixtures between T = (288.15 to 303.15) K	
rfi	1.48670	308.15	Excess and deviation properties for the binary mixtures of methylcyclohexane with benzene, toluene, p-xylene, mesitylene, and anisole at T = (298.15, 303.15, and 308.15) K	

rfi	1.48930	303.15	Excess and deviation properties for the binary mixtures of methylcyclohexane with benzene, toluene, p-xylene, mesitylene, and anisole at T = (298.15, 303.15, and 308.15) K
rfi	1.49260	298.15	Excess and deviation properties for the binary mixtures of methylcyclohexane with benzene, toluene, p-xylene, mesitylene, and anisole at T = (298.15, 303.15, and 308.15) K
rfi	1.49330	298.15	(Vapor + liquid) equilibria of binary mixtures formed by iso-octane with a variety of compounds at 95.8 kPa
rfi	1.49577	293.15	A study of densities and volumetric properties of binary mixtures containing nitrobenzene at T = (293.15 to 353.15) K
rfi	1.49577	293.15	Densities and volumetric properties of a (xylene + dimethyl sulfoxide) at temperature from (293.15 to 353.15) K
rfi	1.49577	293.10	Volumetric properties of (cyclohexanone + a xylene) at temperature between (293.15 and 353.15) K

rfi	1.49321		298.15	Separation of aromatic hydrocarbons from alkanes using ammonium ionic liquid C2NTf2 at T = 298.15K
rfi	1.49325		298.15	KDB
rfi	1.49298		298.15	Effect of Temperature on the Change of Refractive Index on Mixing for Butyl Acetate + Aromatic Hydrocarbons
rfi	1.49325		298.15	Isobaric Vapor Liquid Equilibria of 1-Butanol p-Xylene System1
rfi	1.49330		298.15	Bubble temperature measurements on the binary mixtures formed by decane with a variety of compounds at 95.8 kPa
rfi	1.48790		308.15	Topological and thermodynamic investigations of molecular interactions in binary mixtures: Molar excess volumes and molar excess enthalpies
rfi	1.48580		293.15	Excess Gibbs' energies of the binary mixtures formed by N,N-dimethylformamide with xylenes and cresols at 95.1 kPa
rhol	852.28	kg/m3	303.15	Excess volumes and partial molar volumes of binary mixtures of 1,2-propanediol carbonate with xylene in the temperature range of (293.15 to 353.15) K

rhol	834.74	kg/m3	323.15	Thermodynamic characterization of binary mixtures of poly(propylene glycol) 425 with toluene and o-, m- and p-xylenes
rhol	856.51	kg/m3	298.15	Surface Tension Deviations and Excess Molar Volumes on the Ternary System Propyl Propanoate + Hexane + p-Xylene at 298.15 K
rhol	858.63	kg/m3	298.15	Molar Excess Volumes and Excess Isentropic Compressibilities of {2-Methylaniline (i) + Benzene (j) + Methylbenzene}, {2-Methylaniline (i) + Benzene (j) + 1,2-Dimethylbenzene (k)}, and {2-Methylaniline (i) + Benzene (j) + 1,4-Dimethylbenzene (k)} at T = 308.15 K
rhol	856.58	kg/m3	298.15	Molar Excess Volumes and Excess Isentropic Compressibilities of Ternary Mixtures of o-Toluidine
rhol	856.54	kg/m3	298.15	Vapor Liquid Equilibrium for 2-Methyl-1-butanol + Ethylbenzene + Xylene Isomers at 101.33 kPa
rhol	856.65	kg/m3	298.15	Evaluation of the Performance of Four Solvents for the Liquid Liquid Extraction of Acrylic Acid from Water

rhol	861.21	kg/m3	293.15	Isobaric vapor liquid equilibium for the binary systerms of 1-butanol with o-xylene, m-xylene, p-xylene, and ethylbenzene at 101.33 kPa
rhol	856.67	kg/m3	298.15	Excess Molar Volumes of 2,4,6,8-Tetramethylcyclotetrasiloxane with Benzene, Toluene, and Xylene at T = (288.15, 298.15, and 308.15) K
rhol	856.68	kg/m3	298.15	Ebulliometric Determination and Prediction of Vapor Liquid Equilibria for Binary Mixtures of Ethanol and Ethyl Hexanoate
rhol	856.85	kg/m3	298.15	Excess Molar Volumes and Surface Tensions of Xylene with Isopropyl Ether or Methyl tert-Butyl Ether at 298.15 K
rhol	856.85	kg/m3	298.15	Excess Molar Volumes and Surface Tensions of Xylene with Acetone or 2-Butanone at 298.15 K
rhol	856.70	kg/m3	298.15	Excess Molar Enthalpies for Dimethyl Carbonate with o-Xylene, m-Xylene, p-Xylene, Ethylbenzene or Ethyl Benzoate at 298.15 K and 10.2 MPa
rhol	856.70	kg/m3	298.15	Excess Molar Entalpies of Dimethyl Carbonate with o-Xylene, m-Xylene, p-Xylene, Ethylbenzene, or Ethyl Benzoate at 298.15 K

rhol	856.50	kg/m3	298.15	Determination and Correlation of Liquid-Liquid Equilibria Data for Water + Cyclohexanol + (Mesityl Oxide, Toluene, and p-Xylene) Ternary Systems at Different Temperatures
rhol	856.54	kg/m3	298.15	Isobaric Vapor Liquid Equilibrium for the Binary Systems of Diethyl Carbonate with Xylene Isomers and Ethylbenzene at 101.33 kPa
rhol	856.63	kg/m3	298.15	Liquid Liquid Equilibria, Equilibrium Phase Densities, and Refractive Indices for the Quaternary Mixtures Containing 2-Propanol or 2-Methyl-2-Propanol of Fuel Oxygenate at T = 298.15 and 318.15 K
rhol	825.88	kg/m3	333.15	Thermodynamic characterization of binary mixtures of poly(propylene glycol) 425 with toluene and o-, m- and p-xylenes
rhol	830.32	kg/m3	328.15	Thermodynamic characterization of binary mixtures of poly(propylene glycol) 425 with toluene and o-, m- and p-xylenes
rhol	839.14	kg/m3	318.15	Thermodynamic characterization of binary mixtures of poly(propylene glycol) 425 with toluene and o-, m- and p-xylenes

rhol	843.53	kg/m3	313.15	Thermodynamic characterization of binary mixtures of poly(propylene glycol) 425 with toluene and o-, m- and p-xylenes	
rhol	847.91	kg/m3	308.15	Thermodynamic characterization of binary mixtures of poly(propylene glycol) 425 with toluene and o-, m- and p-xylenes	
rhol	852.27	kg/m3	303.15	Thermodynamic characterization of binary mixtures of poly(propylene glycol) 425 with toluene and o-, m- and p-xylenes	
rhol	856.63	kg/m3	298.15	Thermodynamic characterization of binary mixtures of poly(propylene glycol) 425 with toluene and o-, m- and p-xylenes	
rhol	860.97	kg/m3	293.15	Thermodynamic characterization of binary mixtures of poly(propylene glycol) 425 with toluene and o-, m- and p-xylenes	
rhol	865.31	kg/m3	288.15	Thermodynamic characterization of binary mixtures of poly(propylene glycol) 425 with toluene and o-, m- and p-xylenes	
rhol	847.88	kg/m3	308.15	Acoustic and thermodynamic properties of binary mixtures of 1-nonanol with o-xylene, m-xylene, p-xylene, ethylbenzene and mesitylene at T = (298.15 and 308.15) K	

rhol	856.61	kg/m3	298.15	Acoustic and thermodynamic properties of binary mixtures of 1-nonanol with o-xylene, m-xylene, p-xylene, ethylbenzene and mesitylene at T = (298.15 and 308.15) K
rhol	856.62	kg/m3	298.15	Effect of temperature and composition on the density, refractive index, and excess quantities of binary mixtures of 2,4,6,8-tetramethyl-2,4,6,8-tetraethenylcyclotetrasiloxane with aromatic hydrocarbons
rhol	830.39	kg/m3	328.15	Effect of temperature and composition on the density, refractive index, and excess quantities of binary mixtures of 2,4,6,8-tetramethyl-2,4,6,8-tetraethenylcyclotetrasiloxane with aromatic hydrocarbons
rhol	839.21	kg/m3	318.15	Effect of temperature and composition on the density, refractive index, and excess quantities of binary mixtures of 2,4,6,8-tetramethyl-2,4,6,8-tetraethenylcyclotetrasiloxane with aromatic hydrocarbons

rhol	847.97	kg/m3	308.15	Effect of temperature and composition on the density, refractive index, and excess quantities of binary mixtures of 2,4,6,8-tetramethyl-2,4,6,8- tetraethenylcyclotetrasiloxane with aromatic hydrocarbons
rhol	865.30	kg/m3	288.15	Effect of temperature and composition on the density, refractive index, and excess quantities of binary mixtures of 2,4,6,8-tetramethyl-2,4,6,8- tetraethenylcyclotetrasiloxane with aromatic hydrocarbons
rhol	809.07	kg/m3	353.15	Excess volumes and partial molar volumes of binary mixtures of 1,2-propanediol carbonate with xylene in the temperature range of (293.15 to 353.15) K
rhol	817.66	kg/m3	343.15	Excess volumes and partial molar volumes of binary mixtures of 1,2-propanediol carbonate with xylene in the temperature range of (293.15 to 353.15) K
rhol	826.27	kg/m3	333.15	Excess volumes and partial molar volumes of binary mixtures of 1,2-propanediol carbonate with xylene in the temperature range of (293.15 to 353.15) K

rhol	834.92	kg/m3	323.15	Excess volumes and partial molar volumes of binary mixtures of 1,2-propanediol carbonate with xylene in the temperature range of (293.15 to 353.15) K
rhol	843.58	kg/m3	313.15	Excess volumes and partial molar volumes of binary mixtures of 1,2-propanediol carbonate with xylene in the temperature range of (293.15 to 353.15) K
rhol	861.00	kg/m3	293.00	KDB
rhol	856.51	kg/m3	298.15	Experimental Study of the Dynamic Viscosity Deviations in the Binary Systems: Hexane + Ethylbenzene, + o-Xylene, + m-Xylene, + p-Xylene at 298.15 K
rhol	856.58	kg/m3	298.15	Thermodynamic Properties of Ternary Liquid Mixtures of 2-Pyrrolidinone with Aromatic Hydrocarbons
rhol	865.52	kg/m3	288.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K

rhol	861.17	kg/m3	293.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K	
rhol	856.82	kg/m3	298.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K	
rhol	852.47	kg/m3	303.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K	
rhol	848.12	kg/m3	308.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K	

rhol	843.77	kg/m3	313.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K
rhol	839.42	kg/m3	318.15	Densities and Volumetric Properties of Binary Mixtures of Butyl Acrylate with Benzene, Toluene, o-Xylene, m-Xylene, p-Xylene, and Mesitylene at Temperatures from 288.15 K to 318.15 K
rhol	856.71	kg/m3	298.15	Isobaric vapor-liquid equilibrium of binary systems of decane with p-, o-, m-xylene at 20 kPa
rhol	856.71	kg/m3	298.15	Isobaric vapor-liquid equilibrium data of the binary systems of octane with p, o, m-xylene at 20 kPa
rhol	856.71	kg/m3	298.15	Isobaric vapor-liquid equilibrium for n-undecane + p-, o-, m-xylene at 10 kPa
rhol	856.78	kg/m3	298.15	Liquid liquid equilibria in the ternary systems {hexadecane + BTX aromatics + 2-methoxyethanol or acetonitrile} at 298.15 K

rhol	856.50	kg/m3	298.15	Isobaric vapor-liquid equilibrium of the binary system sec-butyl acetate + para-xylene and the quaternary system methyl acetate + para-xylene + sec-butyl acetate + acetic acid at 101.3 kPa
rhol	861.00	kg/m3	293.15	Excess volumes and partial molar volumes of binary mixtures of 1,2-propanediol carbonate with xylene in the temperature range of (293.15 to 353.15) K
rhol	861.20	kg/m3	293.10	Vapor-Liquid Equilibria Data for Binary Systems of Ethylbenzene + Xylene Isomers at 100.65 kPa
sfust	59.73	J/mol×K	286.30	NIST Webbook
sfust	59.75	J/mol×K	286.39	NIST Webbook
sfust	59.77	J/mol×K	286.40	NIST Webbook
sfust	59.14	J/mol×K	286.30	NIST Webbook
speedsl	1287.30	m/s	303.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods
speedsl	1285.42	m/s	303.15	Influence of temperature on thermodynamics of ethers + xylenes
speedsl	1275.64	m/s	305.65	Influence of temperature on thermodynamics of ethers + xylenes

speedsl	1266.13	m/s	308.15	Influence of temperature on thermodynamics of ethers + xylenes	
speedsl	1256.41	m/s	310.65	Influence of temperature on thermodynamics of ethers + xylenes	
speedsl	1246.85	m/s	313.15	Influence of temperature on thermodynamics of ethers + xylenes	
speedsl	1237.60	m/s	315.65	Influence of temperature on thermodynamics of ethers + xylenes	
speedsl	1310.00	m/s	298.15	Isentropic Compressibilities Changes of Mixing of Tetrahydropyran and Aromatic Hydrocarbons Ternary Mixtures at 308.15 K	
speedsl	1220.47	m/s	320.65	Influence of temperature on thermodynamics of ethers + xylenes	
speedsl	1211.00	m/s	323.15	Influence of temperature on thermodynamics of ethers + xylenes	
speedsl	1328.40	m/s	293.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods	

speedsl	1307.40	m/s	298.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods
speedsl	1295.34	m/s	300.65	Influence of temperature on thermodynamics of ethers + xylenes
speedsl	1267.60	m/s	308.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods
speedsl	1248.30	m/s	313.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods
speedsl	1347.94	m/s	288.15	Influence of temperature on thermodynamics of ethers + xylenes
speedsl	1229.80	m/s	318.15	Physicochemical study of intermolecular interactions in 1,4-dioxane + aromatic hydrocarbons binary mixtures at different temperatures by using ultrasonic and viscometric methods

speedsl	1308.00	m/s	298.15	Densities, Excess Molar Volumes at T = (298.15 to 313.15) K, Speeds of Sound, Excess Isentropic Compressibilities, Relative Permittivities and Deviations in Molar Polarizations at T = (298.15 and 308.15) K for Methyl Methacrylate + 2-Butoxyethanol or + Dibutyl Ether + Benzene, + Toluene and + p-Xylene
speedsl	1276.00	m/s	308.15	Densities, Excess Molar Volumes at T = (298.15 to 313.15) K, Speeds of Sound, Excess Isentropic Compressibilities, Relative Permittivities and Deviations in Molar Polarizations at T = (298.15 and 308.15) K for Methyl Methacrylate + 2-Butoxyethanol or + Dibutyl Ether + Benzene, + Toluene and + p-Xylene
speedsl	1314.00	m/s	298.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene

speedsl	1272.00	m/s	308.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene
speedsl	1330.00	m/s	293.15	Densities, Speeds of Sound, and Isentropic Compressibilities of Binary Mixtures of {Alkan-1-ols + 1,2-Dimethylbenzene, or 1,3-Dimethylbenzene, or 1,4-Dimethylbenzene, or Ethylbenzene} at (293.15, 303.15, and 313.15) K
speedsl	1249.00	m/s	313.15	Densities, Speeds of Sound, and Isentropic Compressibilities of Binary Mixtures of {Alkan-1-ols + 1,2-Dimethylbenzene, or 1,3-Dimethylbenzene, or 1,4-Dimethylbenzene, or Ethylbenzene} at (293.15, 303.15, and 313.15) K
speedsl	1305.39	m/s	298.15	Influence of temperature on thermodynamics of ethers + xylenes
speedsl	1336.86	m/s	290.65	Influence of temperature on thermodynamics of ethers + xylenes

speedsl	1315.60	m/s	295.65	Influence of temperature on thermodynamics of ethers + xylenes
speedsl	1326.13	m/s	293.15	Influence of temperature on thermodynamics of ethers + xylenes
speedsl	1289.00	m/s	303.15	Densities, Speeds of Sound, and Isentropic Compressibilities of Binary Mixtures of {Alkan-1-ols + 1,2-Dimethylbenzene, or 1,3-Dimethylbenzene, or 1,4-Dimethylbenzene, or Ethylbenzene} at (293.15, 303.15, and 313.15) K
speedsl	1228.14	m/s	318.15	Influence of temperature on thermodynamics of ethers + xylenes
srf	0.03	N/m	308.15	Excess thermodynamic functions derived from densities and surface tensions of (p- or o-xylene + ethylene glycol dimethyl ether) between the temperatures (298.15 and 308.15) K
srf	0.03	N/m	298.15	Densities and Surface Tensions of Propyl Acetate + Xylenes or + Ethylbenzene from (298.15 to 308.15) K
srf	0.03	N/m	303.15	Densities and Surface Tensions of Propyl Acetate + Xylenes or + Ethylbenzene from (298.15 to 308.15) K

srf	0.03	N/m	308.15	Densities and Surface Tensions of Propyl Acetate + Xylenes or + Ethylbenzene from (298.15 to 308.15) K
srf	0.03	N/m	303.15	Excess thermodynamic functions derived from densities and surface tensions of (p- or o-xylene + ethylene glycol dimethyl ether) between the temperatures (298.15 and 308.15) K
srf	0.03	N/m	298.15	Excess thermodynamic functions derived from densities and surface tensions of (p- or o-xylene + ethylene glycol dimethyl ether) between the temperatures (298.15 and 308.15) K
srf	0.03	N/m	298.15	Surface tension, density, and speed of sound for the ternary mixture {diethyl carbonate + p-xylene + decane}
srf	0.03	N/m	293.20	KDB
srf	0.03	N/m	298.15	Analysis of Surface Tension, Density, and Speed of Sound for the Ternary Mixture Dimethyl Carbonate + p-Xylene + n-Octane
srf	0.03	N/m	308.15	Surface Tension of Dialkyl Carbonates + (Alkanes or 1,4-Dimethylbenzene) and 1,4-Dimethylbenzene + Alkanes Binary Mixtures at T = 308.15 K

srf	0.03	N/m	298.15	Experimental and theoretical surface tension deviations in the binary systems propyl propanoate + o-, m- and p-xylene at 298.15K
tcondl	0.12	W/m×K	311.71	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	311.94	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	312.11	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	328.75	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

tcondl	0.13	W/m×K	294.44	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	329.16	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.13	W/m×K	294.03	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.13	W/m×K	287.73	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.13	W/m×K	287.55	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

tcondl	0.13	W/m×K	287.33	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.13	W/m×K	294.27	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	328.99	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tfp	286.45	K	100.00	Activity coefficient at infinite dilution, azeotropic data, excess enthalpies and solid liquid-equilibria for binary systems of alkanes and aromatics with esters

Correlations

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)
Coeff. A	1.44593e+01
Coeff. B	-3.57809e+03
Coeff. C	-4.79200e+01
Temperature range (K), min.	286.41
Temperature range (K), max.	439.06

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/T + C*ln(T) + D*T^2
Coeff. A	7.95572e+01
Coeff. B	-7.63795e+03
Coeff. C	-9.52735e+00
Coeff. D	5.74897e-06
Temperature range (K), min.	286.41
Temperature range (K), max.	616.26

Datasets

Refractive index (Na D-line)

Pressure, kPa - Liquid	Temperature, K - Liquid	Refractive index (Na D-line) - Liquid
93.00	298.15	1.4929

Reference *https://www.doi.org/10.1021/acs.jced.7b00372*

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
293.15	100.00	862.7
293.15	1000.00	863.3
293.15	3000.00	864.7
293.15	5000.00	865.9
293.15	10000.00	869.6
293.15	15000.00	873.0
293.15	20000.00	876.3
293.15	25000.00	879.6
303.15	100.00	852.9
303.15	1000.00	853.8
303.15	3000.00	855.3
303.15	5000.00	856.9
303.15	10000.00	860.6
303.15	15000.00	864.3
303.15	20000.00	867.6
303.15	25000.00	871.0
303.15	30000.00	874.3
303.15	35000.00	877.4
303.15	40000.00	880.3
303.15	50000.00	886.3
303.15	60000.00	892.5
313.15	100.00	843.6
313.15	1000.00	844.7
313.15	3000.00	846.5
313.15	5000.00	848.1
313.15	10000.00	852.0
313.15	15000.00	855.8
313.15	20000.00	859.5
313.15	25000.00	863.0
313.15	30000.00	866.4
313.15	35000.00	869.6
313.15	40000.00	872.8
313.15	50000.00	879.1
313.15	60000.00	884.5
323.15	100.00	835.7
323.15	1000.00	836.7
323.15	3000.00	838.5
323.15	5000.00	840.2
323.15	10000.00	844.5
323.15	15000.00	848.4
323.15	20000.00	852.3
323.15	25000.00	855.7
323.15	30000.00	859.2

323.15	35000.00	862.6
323.15	40000.00	866.1
323.15	50000.00	872.8
323.15	60000.00	878.1
333.15	100.00	827.0
333.15	1000.00	827.8
333.15	3000.00	829.7
333.15	5000.00	831.5
333.15	10000.00	835.9
333.15	15000.00	840.0
333.15	20000.00	844.1
333.15	25000.00	847.9
333.15	30000.00	851.6
333.15	35000.00	855.0
333.15	40000.00	858.8
333.15	50000.00	865.1
333.15	60000.00	871.1
343.15	100.00	817.8
343.15	1000.00	818.8
343.15	3000.00	820.6
343.15	5000.00	823.0
343.15	10000.00	827.2
343.15	15000.00	831.7
343.15	20000.00	836.3
343.15	25000.00	840.0
343.15	30000.00	843.9
343.15	35000.00	847.6
343.15	40000.00	851.0
343.15	50000.00	858.0
343.15	60000.00	864.1
353.15	100.00	808.7
353.15	1000.00	809.6
353.15	3000.00	811.5
353.15	5000.00	813.6
353.15	10000.00	818.1
353.15	15000.00	822.8
353.15	20000.00	827.6
353.15	25000.00	831.5
353.15	30000.00	835.8
353.15	35000.00	839.8
353.15	40000.00	843.4
353.15	50000.00	850.6
353.15	60000.00	856.9
363.15	100.00	799.5

363.15	1000.00	800.7
363.15	3000.00	802.9
363.15	5000.00	805.3
363.15	10000.00	810.2
363.15	15000.00	815.5
363.15	20000.00	819.9
363.15	25000.00	824.1
363.15	30000.00	828.5
363.15	35000.00	832.7
363.15	40000.00	836.7
363.15	50000.00	844.0
363.15	60000.00	850.8

Reference *https://www.doi.org/10.1016/j.fluid.2017.11.021*

Temperature, K	Pressure, kPa	Mass density, kg/m3
288.15	100.00	864.9
298.15	100.00	856.2
308.15	100.00	847.5
288.15	5000.00	868.3
298.15	5000.00	860.2
308.15	5000.00	851.4
288.15	10000.00	871.8
298.15	10000.00	863.5
308.15	10000.00	855.2
288.15	20000.00	878.1
298.15	20000.00	870.1
308.15	20000.00	862.1
288.15	30000.00	884.0
298.15	30000.00	876.5
308.15	30000.00	868.6
288.15	40000.00	889.7
298.15	40000.00	882.2
308.15	40000.00	874.8

Reference *https://www.doi.org/10.1016/j.jct.2013.09.039*

Speed of sound, m/s

Temperature, K - Liquid	Pressure, kPa - Liquid	Speed of sound, m/s - Liquid

305.99	1000.00	1281.77
306.07	2050.00	1287.1
306.02	2050.00	1287.22
305.93	3690.00	1296.49
306.00	4900.00	1302.49
305.98	5250.00	1304.38
306.05	6960.00	1312.94
306.03	9400.00	1325.57
306.00	13840.00	1347.72
306.07	16500.00	1360.11
306.06	19900.00	1376.19
306.07	24630.00	1397.78
306.14	26930.00	1407.8
306.18	28370.00	1413.93
306.10	29650.00	1419.72
306.00	30490.00	1423.77
305.99	35160.00	1443.56
305.97	40270.00	1464.54
305.98	45030.00	1483.47
305.98	50870.00	1505.99
323.56	210.00	1206.43
323.57	490.00	1208.1
323.54	1060.00	1211.51
323.57	2600.00	1220.4
323.58	5070.00	1234.53
323.54	6060.00	1240.28
323.58	6090.00	1240.29
323.59	7490.00	1248.03
323.57	10070.00	1262.13
323.58	11110.00	1267.65
323.53	11470.00	1269.76
323.60	15130.00	1288.59
323.59	17890.00	1302.54
323.55	18570.00	1306.1
323.57	20900.00	1317.51
323.59	25130.00	1337.71
323.59	30210.00	1361.29
323.52	30290.00	1361.83
323.48	34540.00	1381.14
323.58	34830.00	1382.01
323.57	39580.00	1402.7
323.47	41260.00	1410.19
323.54	44230.00	1422.37
323.57	44830.00	1424.72

323.54	45010.00	1425.56
323.49	46870.00	1433.42
323.51	49380.00	1443.5
323.47	49810.00	1445.32
323.48	54770.00	1464.84
323.48	55430.00	1467.39
323.47	59650.00	1483.53
323.51	65910.00	1506.74
335.99	280.00	1158.02
335.99	570.00	1159.79
335.98	1230.00	1163.95
335.98	2630.00	1172.56
335.98	5600.00	1190.42
336.00	10270.00	1217.21
335.99	10300.00	1217.47
336.01	14980.00	1243.1
335.99	20370.00	1271.42
336.01	20750.00	1273.3
336.00	24830.00	1293.84
336.00	30890.00	1322.99
336.06	31080.00	1323.64
336.00	34840.00	1341.19
336.02	40670.00	1367.23
336.05	41270.00	1369.78
336.03	41380.00	1370.31
335.98	45230.00	1387.08
335.97	50590.00	1409.56
335.95	55000.00	1427.54
335.96	61040.00	1451.3
335.95	65380.00	1467.88
348.25	40.00	1108.83
348.32	1270.00	1116.85
348.30	2110.00	1122.26
348.27	2120.00	1122.47
348.29	2590.00	1125.51
348.28	4090.00	1135.15
348.32	8600.00	1162.9
348.32	8900.00	1164.69
348.35	10880.00	1176.32
348.37	14620.00	1197.72
348.36	15220.00	1201.14
348.36	20050.00	1227.6
348.45	24930.00	1252.9
348.43	29340.00	1275.02

348.43	33900.00	1297.21
348.43	39830.00	1324.82
348.42	45170.00	1348.71
348.42	49930.00	1369.38
348.42	54750.00	1389.61
348.39	59820.00	1410.34
348.41	59890.00	1410.6
348.37	60580.00	1413.43
348.39	64180.00	1427.64
348.40	64670.00	1429.6
355.98	270.00	1081.04
355.95	490.00	1082.63
355.94	920.00	1085.65
355.95	2620.00	1097.05
355.98	5370.00	1115.13
355.96	10930.00	1149.89
355.89	12280.00	1158.25
355.92	15640.00	1177.67
355.94	20950.00	1207.26
355.95	25050.00	1229.15
355.95	31130.00	1260.21
356.05	34600.00	1276.89
356.02	41360.00	1308.87
356.02	45060.00	1325.7
356.08	50520.00	1349.51
356.04	54960.00	1368.53
356.00	59390.00	1387.08
355.98	65160.00	1410.32
373.59	240.00	1014.61
373.58	570.00	1017.06
373.55	950.00	1020.07
373.53	2520.00	1031.71
373.54	2530.00	1031.73
373.53	5450.00	1052.49
373.60	10260.00	1084.6
373.61	14920.00	1114.21
373.60	19750.00	1143.36
373.62	20290.00	1146.4
373.63	24920.00	1172.65
373.60	29800.00	1199.11
373.60	29850.00	1199.31
373.60	35000.00	1226.08
373.62	39790.00	1249.82
373.62	40800.00	1254.88

373.57	44340.00	1271.77
373.58	49640.00	1296.23
373.63	54980.00	1319.83
373.62	58970.00	1337.14
373.61	59070.00	1337.54
373.64	64880.00	1361.68
398.20	220.00	923.76
398.21	500.00	926.17
398.22	1040.00	930.76
398.25	2490.00	942.77
398.24	5190.00	964.55
398.25	10300.00	1002.89
398.26	12650.00	1019.53
398.24	15110.00	1036.53
398.25	19720.00	1066.63
398.22	20010.00	1068.47
398.22	24890.00	1098.56
398.20	29920.00	1127.9
398.25	31220.00	1135.23
398.24	31220.00	1135.21
398.21	34890.00	1155.44
398.19	37260.00	1168.3
398.20	37270.00	1168.29
398.20	40070.00	1182.91
398.21	44950.00	1207.53
398.23	50040.00	1232.26
398.20	54810.00	1254.71
398.20	60130.00	1278.81
398.21	64730.00	1298.96
422.73	190.00	834.7
422.72	550.00	838.3
422.75	780.00	840.37
422.74	1230.00	844.88
422.65	2630.00	858.44
422.57	5690.00	886.27
422.74	9190.00	915.48
422.75	10020.00	922.14
422.70	14830.00	959.38
422.75	19940.00	995.75
422.75	24810.00	1028.16
422.73	28590.00	1052.11
422.75	29890.00	1060.03
422.77	34850.00	1089.33
422.77	40720.00	1122.29

422.74	44830.00	1144.36
422.72	50170.00	1171.8
422.73	54780.00	1194.57
422.76	59900.00	1218.69
422.75	64580.00	1240.21
447.07	300.00	748.43
447.07	580.00	751.73
447.02	1020.00	756.94
446.94	5130.00	800.91
447.01	7300.00	821.88
446.99	10180.00	848.37
446.99	14830.00	887.97
447.00	19890.00	927.32
447.03	22500.00	946.32
447.02	24900.00	963.22
447.09	30510.00	1000.66
447.13	35270.00	1030.41
447.12	40150.00	1059.45
447.13	45010.00	1086.93
447.08	49880.00	1113.32
447.11	54450.00	1136.99
447.13	59760.00	1163.32
447.08	64750.00	1187.32

Reference *https://www.doi.org/10.1016/j.jct.2019.03.022*

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
293.04	100.00	0.0006444
293.04	1000.00	0.0006494
293.04	5000.00	0.0006720
293.04	10000.00	0.0006997
293.03	15000.00	0.0007277
293.03	20000.00	0.0007569
293.03	25000.00	0.0007883
293.03	30000.00	0.0008186
302.86	100.00	0.0005762
302.86	1000.00	0.0005804
302.87	5000.00	0.0005995
302.87	10000.00	0.0006244

302.88	15000.00	0.0006499
302.88	20000.00	0.0006747
302.88	25000.00	0.0007023
302.89	30000.00	0.0007274
312.76	100.00	0.0005150
312.76	1000.00	0.0005186
312.77	5000.00	0.0005356
312.77	10000.00	0.0005575
312.76	15000.00	0.0005806
312.76	20000.00	0.0006027
312.76	25000.00	0.0006263
312.76	30000.00	0.0006494
322.62	100.00	0.0004653
322.63	1000.00	0.0004689
322.64	5000.00	0.0004833
322.64	10000.00	0.0005038
322.64	15000.00	0.0005240
322.64	20000.00	0.0005442
322.64	25000.00	0.0005653
322.65	30000.00	0.0005861
332.58	100.00	0.0004206
332.58	1000.00	0.0004237
332.58	5000.00	0.0004383
332.58	10000.00	0.0004564
332.58	15000.00	0.0004745
332.58	20000.00	0.0004930
332.58	25000.00	0.0005109
332.57	30000.00	0.0005304
342.27	100.00	0.0003815
342.27	1000.00	0.0003842
342.28	5000.00	0.0003977
342.28	10000.00	0.0004144
342.29	15000.00	0.0004314
342.28	20000.00	0.0004482
342.29	25000.00	0.0004649
342.29	30000.00	0.0004833
352.21	100.00	0.0003483
352.21	1000.00	0.0003507
352.20	5000.00	0.0003634
352.20	10000.00	0.0003791
352.20	15000.00	0.0003945
352.20	20000.00	0.0004111
352.20	25000.00	0.0004263
352.20	30000.00	0.0004423

362.73	100.00	0.0003194
362.74	1000.00	0.0003217
362.75	5000.00	0.0003331
362.76	10000.00	0.0003467
362.76	15000.00	0.0003616
362.77	20000.00	0.0003756
362.81	25000.00	0.0003915
362.82	30000.00	0.0004050
372.71	100.00	0.0002936
372.71	1000.00	0.0002960
372.71	5000.00	0.0003061
372.70	10000.00	0.0003203
372.70	15000.00	0.0003341
372.69	20000.00	0.0003480
372.69	25000.00	0.0003614
372.69	30000.00	0.0003752

Reference *https://www.doi.org/10.1016/j.jct.2015.11.027*

Temperature, K	Pressure, kPa	Viscosity, Pa*s
313.15	100.00	0.0004990
313.15	800.00	0.0005029
313.15	1600.00	0.0005100
313.15	2400.00	0.0005160
313.15	3200.00	0.0005210
333.15	100.00	0.0004090
333.15	800.00	0.0004120
333.15	1600.00	0.0004140
333.15	2400.00	0.0004170
333.15	3200.00	0.0004190
353.15	100.00	0.0003400
353.15	800.00	0.0003460
353.15	1600.00	0.0003500
353.15	2400.00	0.0003560
353.15	3200.00	0.0003610
373.15	100.00	0.0002920
373.15	800.00	0.0002970
373.15	1600.00	0.0003000
373.15	2400.00	0.0003030
373.15	3200.00	0.0003050
393.15	800.00	0.0002540
393.15	1600.00	0.0002580
393.15	2400.00	0.0002620

393.15	3200.00	0.0002660
413.15	800.00	0.0002210
413.15	1600.00	0.0002230
413.15	2400.00	0.0002260
413.15	3200.00	0.0002280
433.15	800.00	0.0001920
433.15	1600.00	0.0001970
433.15	2400.00	0.0002010
433.15	3200.00	0.0002060
453.15	800.00	0.0001680
453.15	1600.00	0.0001700
453.15	2400.00	0.0001720
453.15	3200.00	0.0001750
473.15	1600.00	0.0001590
473.15	2400.00	0.0001630
473.15	3200.00	0.0001670

Reference *https://www.doi.org/10.1021/je800635g*

Sources

Acoustic and thermodynamic properties of binary mixtures of 1-nonanol with o-xylene, m-xylene, p-xylene, ethylbenzene and mesitylene at T = (298.15 and 308.15) K:	https://www.doi.org/10.1016/j.jct.2012.10.023
Experimental and theoretically study of interaction between organic compounds and tricyanomethanide based ionic liquids:	https://www.doi.org/10.1016/j.jct.2014.12.027
Isothermal (liquid + liquid) equilibrium data at T = 313.15 K and isobaric (vapor + liquid + liquid) equilibrium data at 101.3 kPa for the ternary system (water + 1-butanol + p-xylene):	https://www.doi.org/10.1016/j.jct.2014.07.021
Volumetric and Viscometric Behavior of the Binary System: (Hexan-1-ol + p-Xylene)	https://www.doi.org/10.1021/je100390b
Activity coefficients at infinite dilution and physicochemical properties for organic solutes and water in the ionic liquid 4-(3-hydroxypropyl)-4-methylmorpholinium bis(trifluoromethylsulfonyl)-amide:	https://www.doi.org/10.1016/j.jct.2015.02.024
Bubble points of some binary mixtures formed by o-cresol at 95.75 kPa:	https://www.doi.org/10.1016/j.fluid.2005.09.012
Activity Coefficients at Infinite Dilution of Alkanes, Alkenes, and Alkyl Benzenes in 1-Ethyl-3-methylimidazolium Diethylphosphate Using Gas-Liquid Chromatography	https://www.doi.org/10.1021/je200266f
Activity coefficients at infinite dilution and physicochemical properties for organic solutes and water in the ionic liquid 1-(2-methoxyethyl)-1-methylpiperidinium trifluorotris(perfluoroethyl)phosphate:	https://www.doi.org/10.1016/j.jct.2012.08.016
Isobaric vapor-liquid equilibrium for n-undecane + p-, o-, m-xylene at 10 kPa:	https://www.doi.org/10.1016/j.fluid.2013.10.012
Bubble temperature measurements on the binary mixtures formed by decane with a variety of compounds at 95.8 kPa:	https://www.doi.org/10.1016/j.fluid.2004.10.027
Gas-liquid chromatography measurements of activity coefficients at infinite dilution of hydrocarbons and alkanols in 1-alkyl-3-methylimidazolium bis(oxalato)borate:	https://www.doi.org/10.1016/j.fluid.2010.08.016
Determination and correlation of solubility of 2,2',4,4',6,6'-hexanitro-1,1'-biphenyl and 2,2',2'',4,4',4'',6,6',6''-Nonanitro-1,1':3',1''-terphenyl in six pure solvents:	https://www.doi.org/10.1016/j.fluid.2018.03.021
Dortmund Data Bank Vapor-Liquid Equilibrium Data:	http://www.ddbst.com/en/EED/VLE/VLE%20Acetonitrile%3Bp-Xylene.php
Activity coefficient at infinite dilution, azeotropic data, excess enthalpies and solid liquid-equilibria for binary systems of alkanes and aromatics with esters:	https://www.doi.org/10.1016/j.fluid.2004.12.005
Isobaric Vapor-Liquid Equilibrium for the Binary Systems of Methyl Formate with o-Xylene, m-Xylene, p-Xylene, and Ethylbenzene at 101.33 kPa:	https://www.doi.org/10.1021/je200974r
Separation of water/butan-1-ol based on activity coefficients at infinite dilution in 1,3-didecyl-2-methylimidazolium dicyanamide ionic liquid:	https://www.doi.org/10.1016/j.jct.2017.10.003
Study of Ether-, Alcohol-, or Cyano-Functionalized Ionic Liquids Using Inverse Gas Chromatography:	https://www.doi.org/10.1021/je900838a
Viscosity, Density, and Refractive Index of Some (Ester + Hydrocarbon) Binary Mixtures at 303.15 K and 313.15 K:	https://www.doi.org/10.1021/je0400052
Refractive Indices of Binary Mixtures of Tetrahydrofuran with Aromatic Hydrocarbon at Temperatures from (288.15 to 318.15) K:	https://www.doi.org/10.1021/je700564c
Thermodynamics and activity coefficients at infinite dilution for organic solutes, water and diols in the ionic liquid choline bis(trifluoromethylsulfonyl)imide:	https://www.doi.org/10.1016/j.jct.2014.04.024

Elimination of Tar in Biomass Gasification Process: Liquid Liquid Equilibrium of Ternary Systems {Water + Solvent (p-Xylene and Methyl Hexadecanoate) + Model Molecules of Tar (Thiophene, Pyridine, Naphthalene, Phenanthrene, and Anthracene)}:	https://www.doi.org/10.1021/acs.jced.6b00857
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Densities, Excess Molar Volumes, Viscosity, and Refractive Indices of Binary Mixtures of Ethanoic Acid and Trichloroethylene with Cyclohexane, Toluene, or Dimethylbenzenes at Different Temperatures:	https://www.doi.org/10.1021/je201211f
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Activity Coefficients at Infinite Dilution Measurements for Organic Solutes and Water in the Ionic Liquid 1-Butyl-3-methylpyridinium Trifluoromethanesulfonate	https://www.doi.org/10.1021/je1000582
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Liquid-liquid equilibria for ternary systems polyoxymethylene dimethyl ethers	https://www.doi.org/10.1016/j.jct.2016.05.016
Physical properties of + water: 3-methyl-N-butylpyridinium tricyanomethanide and ternary LLE data with an aromatic and an aliphatic hydrocarbon at T = (303.2 and 328.2) K	https://www.doi.org/10.1016/j.fluid.2011.05.002
Gas-liquid chromatography measurements of activity coefficients	https://www.doi.org/10.1016/j.jct.2010.01.004
Evaluation of the Performance of Trigeminal Tricationic Ionic Liquids for Separation Problems	https://www.doi.org/10.1021/je201129y
Excess molar enthalpies, density, and speed of sound for the ternary mixture {diethyl carbonate + p-xylene + decane}	https://www.doi.org/10.1016/j.jct.2008.12.010
Activity coefficients at infinite dilution, physicochemical and thermodynamic properties for organic solutes and water in the ionic liquid	https://www.doi.org/10.1016/j.jct.2015.05.022
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Activity coefficients at infinite dilution and physicochemical properties for organic solutes and water in the ionic liquid 1-(2-methoxyethyl)-1-methylpyrrolidinium bis(trifluoromethylsulfonyl)-amide:	https://www.doi.org/10.1016/j.jct.2012.03.015

Legend

af:	Acentric Factor
affp:	Proton affinity
aigt:	Autoignition Temperature
basg:	Gas basicity
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
ea:	Electron affinity
ep:	Protonation entropy at 298K
fll:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hcg:	Heat of Combustion, Gross form
hcn:	Heat of Combustion, Net Form
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hsubt:	Enthalpy of sublimation at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume

nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tc:	Critical Temperature
tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
tfp:	Melting point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility
zra:	Rackett Parameter