1,2-Ethanediol

Other names:	1,2-Dihydroxyethane
	1,2-Ethandiol
	1,2-Ethylene glycol
	146AR
	2-Hydroxyethanol
	Aethylenglykol
	Aliphatic diol
	Athylenglykol
	Dihydroxyethane
	Dowtherm SR 1
	ETHTLENE DIHYDRATE
	ETHYLENE GLYCOL
	Ethane-1,2-diol
	Ethanediol
	Ethylene alcohol
	Ethylene dihydrate
	Ethylene gycol
	Fridex
	GLYCOL ALCOHOL
	Glycol
	Glygen
	HOCH2CH2OH
	Ilexan E
	Lutrol 9
	M.e.g.
	MEG 100
	Macrogol 400 BPC
	Monoethylene glycol
	NSC 93876
	Norkool
	Ramp
	Tescol
	Ucar 17
	Union Carbide XL 54 Type I De-icing Fluid
	Zerex
Inchi:	InChI=1S/C2H6O2/c3-1-2-4/h3-4H,1-2H2
InchiKey:	LYCAIKOWRPUZTN-UHFFFAOYSA-N
Formula:	C2H6O2
SMILES:	OCCO
Mol. weight [g/mol]:	62.07

CAS: 107-21-1

Physical Properties

Property code	Value	Unit	Source
affp	815.90	kJ/mol	NIST Webbook
aigt	685.93	K	KDB
basg	773.60	kJ/mol	NIST Webbook
dm	2.20	debye	KDB
dvisc	0.0169000	Pa×s	Viscosity, thermal and electrical conductivity of silicon dioxide - ethylene glycol transparent nanofluids: An experimental studies
fll	3.20	% in Air	KDB
fpc	388.71	K	KDB
fpo	384.26	K	KDB
gf	-304.70	kJ/mol	KDB
gyrad	2.4700		KDB
hf	-394.40 ± 2.80	kJ/mol	NIST Webbook
hf	-388.00 ± 2.00	kJ/mol	NIST Webbook
hf	-389.30	kJ/mol	NIST Webbook
hf	-389.60	kJ/mol	KDB
hf	-387.50	kJ/mol	NIST Webbook
hf	-390.30	kJ/mol	NIST Webbook
hfl	-455.60 ± 0.80	kJ/mol	NIST Webbook
hfl	-460.00 ± 2.80	kJ/mol	NIST Webbook
hfl	-454.90 ± 0.30	kJ/mol	NIST Webbook
hfl	-453.10 ± 1.20	kJ/mol	NIST Webbook
hfl	-455.85	kJ/mol	NIST Webbook
hfus	9.11	kJ/mol	Joback Method
hvap	65.60 ± 0.30	kJ/mol	NIST Webbook
hvap	63.80	kJ/mol	NIST Webbook
hvap	63.60	kJ/mol	NIST Webbook
hvap	67.60	kJ/mol	NIST Webbook
hvap	68.20 ± 0.80	kJ/mol	NIST Webbook
hvap	66.10 ± 0.30	kJ/mol	NIST Webbook
hvap	65.60 ± 0.30	kJ/mol	NIST Webbook
hvap	66.00 ± 0.20	kJ/mol	NIST Webbook
hvap	66.20	kJ/mol	NIST Webbook
hvap	63.40 ± 0.10	kJ/mol	NIST Webbook
hvap	65.60	kJ/mol	NIST Webbook

hvap	65.40 ± 0.30	kJ/mol	NIST Webbook
hvap	63.70 ± 0.10	kJ/mol	NIST Webbook
ie	10.16	eV	NIST Webbook
ie	10.55	eV	NIST Webbook
ie	10.55	eV	NIST Webbook
ie	10.50	eV	NIST Webbook
log10ws	0.08		Aqueous Solubility Prediction Method
logp	-1.029		Crippen Method
mcvol	50.780	ml/mol	McGowan Method
nfpaf	%!d(float64=1)		KDB
nfpah	%!d(float64=1)		KDB
pc	13100.00 ± 1000.00	kPa	NIST Webbook
pc	9000.00 ± 100.00	kPa	NIST Webbook
pc	8200.00 ± 200.00	kPa	NIST Webbook
pc	7700.00	kPa	KDB
rinpol	726.00		NIST Webbook
rinpol	726.00		NIST Webbook
rinpol	670.00		NIST Webbook
rinpol	702.00		NIST Webbook
rinpol	659.00		NIST Webbook
rinpol	705.00		NIST Webbook
rinpol	672.00		NIST Webbook
rinpol	710.00		NIST Webbook
rinpol	712.00		NIST Webbook
rinpol	670.00		NIST Webbook
ripol	1667.00		NIST Webbook
ripol	1635.00		NIST Webbook
ripol	1660.00		NIST Webbook
ripol	1660.00		NIST Webbook
ripol	1660.00		NIST Webbook
ripol	1621.00		NIST Webbook
ripol	1670.00		NIST Webbook
ripol	1695.00		NIST Webbook
ripol	1635.00		NIST Webbook
ripol	1652.00		NIST Webbook
sg	311.84	J/mol×K	NIST Webbook
sl	179.50	J/mol×K	NIST Webbook
sl	166.90	J/mol×K	NIST Webbook
tb	470.63	K	(Vapour + liquid) equilibria in the ternary system (acetonitrile + n-propanol + ethylene glycol) and corresponding binary systems at 101.3 kPa

tb	470.47	K	Vapor Liquid Equilibria for Three Binary Systems of N-Methylethanolamine, N-Methyldiethanolamine, and Ethylene Glycol at P = (40.0, 30.0, and 20.0) kPa
tb	470.22	K	Investigation on Thermodynamics in Separation for Ethylene Glycol + Neopentyl Glycol System by Azeotropic Distillation
tb	470.32	K	Separation of azeotrope (allyl alcohol + water): Isobaric vapour-liquid phase equilibrium measurements and extractive distillation
tb	470.49	K	KDB
tb	469.15	K	Cosolvent Selection for Benzene-Cyclohexane Separation in Extractive Distillation
tb	470.38	K	Measurement and Correlation of Excess Molar Enthalpies for Ethylene Glycol + Alkanol Systems at the Temperatures (298.15, 308.15, and 323.15) K
tc	645.00 ± 30.00	K	NIST Webbook
tc	718.00 ± 1.00	K	NIST Webbook
tc	720.00 ± 4.00	K	NIST Webbook
tc	718.00	K	KDB
tc	720.00 ± 1.00	K	NIST Webbook
tc	790.00 ± 30.00	K	NIST Webbook
tf	261.70 ± 1.00	K	NIST Webbook
tf	259.25 ± 0.50	K	NIST Webbook
tf	260.15 ± 0.50	K	NIST Webbook
tf	260.45	K	NIST Webbook
tf	260.46 ± 0.05	K	NIST Webbook
tf	260.00	K	KDB
tf	262.00 ± 1.50	K	NIST Webbook
tf	260.55 ± 0.40	K	NIST Webbook
tf	259.95 ± 0.50	K	NIST Webbook
tf	260.55 ± 0.25	K	NIST Webbook
tt	260.80 ± 0.30	K	NIST Webbook
tt	260.60 ± 0.20	K	NIST Webbook
tt	260.60 ± 0.20	K	NIST Webbook
tt	256.60 ± 0.20	K	NIST Webbook
vc	0.185	m3/kmol	Joback Method
zra	0.25		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	121.88	J/mol×K	589.28	Joback Method
cpg	118.53	J/mol×K	562.65	Joback Method
cpg	115.05	J/mol×K	536.02	Joback Method
cpg	111.44	J/mol×K	509.40	Joback Method
cpg	107.68	J/mol×K	482.77	Joback Method
cpg	103.79	J/mol×K	456.15	Joback Method
cpg	99.75	J/mol×K	429.52	Joback Method
cpl	145.60	J/mol×K	293.40	NIST Webbook
cpl	148.87	J/mol×K	298.00	NIST Webbook
cpl	147.30	J/mol×K	298.00	NIST Webbook
cpl	150.33	J/mol×K	298.15	NIST Webbook
cpl	150.60	J/mol×K	301.20	NIST Webbook
cpl	145.20	J/mol×K	303.00	NIST Webbook
cpl	149.60	J/mol×K	298.15	NIST Webbook
cpl	149.30	J/mol×K	298.00	NIST Webbook
cpl	149.80	J/mol×K	298.00	NIST Webbook
cpl	167.32	J/mol×K	353.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	166.83	J/mol×K	351.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	166.35	J/mol×K	350.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	165.86	J/mol×K	348.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	165.38	J/mol×K	347.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	164.90	J/mol×K	345.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	164.42	J/mol×K	344.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	163.93	J/mol×K	342.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	163.45	J/mol×K	341.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	162.97	J/mol×K	339.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	162.49	J/mol×K	338.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	162.00	J/mol×K	336.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	161.52	J/mol×K	335.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	161.04	J/mol×K	333.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	160.56	J/mol×K	332.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	160.08	J/mol×K	330.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	159.60	J/mol×K	329.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	159.11	J/mol×K	327.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	158.63	J/mol×K	326.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	158.15	J/mol×K	324.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	157.67	J/mol×K	323.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	157.19	J/mol×K	321.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	156.71	J/mol×K	320.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	156.23	J/mol×K	318.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	155.75	J/mol×K	317.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	155.27	J/mol×K	315.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	153.83	J/mol×K	311.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	152.40	J/mol×K	306.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	152.88	J/mol×K	308.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	155.23	J/mol×K	333.15	Specific Heat Capacities of Two Functional Ionic Liquids and Two Functional Deep Eutectic Solvents for the Absorption of SO2
cpl	158.58	J/mol×K	343.15	Specific Heat Capacities of Two Functional Ionic Liquids and Two Functional Deep Eutectic Solvents for the Absorption of SO2

cpl	161.31	J/mol×K	353.15	Specific Heat Capacities of Two Functional Ionic Liquids and Two Functional Deep Eutectic Solvents for the Absorption of SO2
cpl	164.85	J/mol×K	363.15	Specific Heat Capacities of Two Functional Ionic Liquids and Two Functional Deep Eutectic Solvents for the Absorption of SO2
cpl	148.10	J/mol×K	293.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	149.40	J/mol×K	293.00	NIST Webbook
cpl	154.79	J/mol×K	314.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	150.96	J/mol×K	302.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	150.48	J/mol×K	300.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	153.36	J/mol×K	309.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	151.92	J/mol×K	305.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	150.01	J/mol×K	299.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	149.69	J/mol×K	298.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	148.57	J/mol×K	294.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	151.44	J/mol×K	303.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	149.05	J/mol×K	296.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	149.53	J/mol×K	297.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	154.31	J/mol×K	312.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	151.57	J/mol×K	323.15	Specific Heat Capacities of Two Functional Ionic Liquids and Two Functional Deep Eutectic Solvents for the Absorption of SO2
dvisc	0.0052400	Pa×s	333.10	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0031300	Pa×s	353.05	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0020600	Pa×s	372.15	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0014400	Pa×s	392.45	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K

dvisc	0.0010700	Pa×s	412.25	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K	
dvisc	0.0008670	Pa×s	428.30	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K	
dvisc	0.0097400	Pa×s	313.05	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K	
dvisc	0.0148200	Pa×s	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures	
dvisc	0.0191000	Pa×s	295.55	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K	

dvisc	0.0041030	Pa×s	343.15	Viscosity of binary mixtures of 1-ethyl-3-methylimidazolium tetrafluoroborate ionic liquid with four organic solvents
dvisc	0.0094440	Pa×s	313.15	Excess Molar Volumes and Viscosities of Binary Mixtures of p-Cresol with Ethylene Glycol and Methanol at Different Temperature and Atmospheric Pressure
dvisc	0.0079720	Pa×s	318.15	Excess Molar Volumes and Viscosities of Binary Mixtures of p-Cresol with Ethylene Glycol and Methanol at Different Temperature and Atmospheric Pressure
dvisc	0.0067940	Pa×s	323.15	Excess Molar Volumes and Viscosities of Binary Mixtures of p-Cresol with Ethylene Glycol and Methanol at Different Temperature and Atmospheric Pressure
dvisc	0.0053300	Pa×s	333.15	Viscosity of binary mixtures of 1-ethyl-3-methylimidazolium tetrafluoroborate ionic liquid with four organic solvents
dvisc	0.0038790	Pa×s	343.15	Excess Molar Volumes and Viscosities of Binary Mixtures of p-Cresol with Ethylene Glycol and Methanol at Different Temperature and Atmospheric Pressure

dvisc	0.0030580	Pa×s	353.15	Excess Molar Volumes and Viscosities of Binary Mixtures of p-Cresol with Ethylene Glycol and Methanol at Different Temperature and Atmospheric Pressure	
dvisc	0.0111930	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of m-Cresol with Ethylene Glycol or Methanol over Several Temperatures	
dvisc	0.0094440	Pa×s	313.15	Densities and Viscosities of Binary Mixtures of m-Cresol with Ethylene Glycol or Methanol over Several Temperatures	
dvisc	0.0079720	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of m-Cresol with Ethylene Glycol or Methanol over Several Temperatures	
dvisc	0.0067940	Pa×s	323.15	Densities and Viscosities of Binary Mixtures of m-Cresol with Ethylene Glycol or Methanol over Several Temperatures	
dvisc	0.0050650	Pa×s	333.15	Densities and Viscosities of Binary Mixtures of m-Cresol with Ethylene Glycol or Methanol over Several Temperatures	
dvisc	0.0038790	Pa×s	343.15	Densities and Viscosities of Binary Mixtures of m-Cresol with Ethylene Glycol or Methanol over Several Temperatures	

dvisc	0.0030580	Pa×s	353.15	Densities and Viscosities of Binary Mixtures of m-Cresol with Ethylene Glycol or Methanol over Several Temperatures
dvisc	0.0163876	Pa×s	298.15	Densities, Viscosities, and Sound Speeds of Some Acetate Salts in Binary Mixtures of Tetrahydrofuran and Methanol at (303.15, 313.15, and 323.15) K
dvisc	0.0107719	Pa×s	308.15	Densities, Viscosities, and Sound Speeds of Some Acetate Salts in Binary Mixtures of Tetrahydrofuran and Methanol at (303.15, 313.15, and 323.15) K
dvisc	0.0071210	Pa×s	323.15	Viscosity of binary mixtures of 1-ethyl-3-methylimidazolium tetrafluoroborate ionic liquid with four organic solvents
dvisc	0.0077029	Pa×s	318.15	Densities, Viscosities, and Sound Speeds of Some Acetate Salts in Binary Mixtures of Tetrahydrofuran and Methanol at (303.15, 313.15, and 323.15) K
dvisc	0.0167950	Pa×s	298.15	Density, Viscosity, and Excess Properties for 1,2-Diaminoethane + 1,2-Ethanediol at (298.15, 303.15, and 308.15) K
dvisc	0.0133960	Pa×s	303.15	Density, Viscosity, and Excess Properties for 1,2-Diaminoethane + 1,2-Ethanediol at (298.15, 303.15, and 308.15) K

dvisc	0.0113330	Pa×s	308.15	Density, Viscosity, and Excess Properties for 1,2-Diaminoethane + 1,2-Ethanediol at (298.15, 303.15, and 308.15) K
dvisc	0.0174000	Pa×s	298.15	Densities and Viscosities of Propane-1,2,3-triol + Ethane-1,2-diol at T = (298.15 to 338.15) K
dvisc	0.0138000	Pa×s	303.15	Densities and Viscosities of Propane-1,2,3-triol + Ethane-1,2-diol at T = (298.15 to 338.15) K
dvisc	0.0115000	Pa×s	308.15	Densities and Viscosities of Propane-1,2,3-triol + Ethane-1,2-diol at T = (298.15 to 338.15) K
dvisc	0.0094200	Pa×s	313.15	Densities and Viscosities of Propane-1,2,3-triol + Ethane-1,2-diol at T = (298.15 to 338.15) K
dvisc	0.0081000	Pa×s	318.15	Densities and Viscosities of Propane-1,2,3-triol + Ethane-1,2-diol at T = (298.15 to 338.15) K
dvisc	0.0069500	Pa×s	323.15	Densities and Viscosities of Propane-1,2,3-triol + Ethane-1,2-diol at T = (298.15 to 338.15) K
dvisc	0.0059600	Pa×s	328.15	Densities and Viscosities of Propane-1,2,3-triol + Ethane-1,2-diol at T = (298.15 to 338.15) K
dvisc	0.0052200	Pa×s	333.15	Densities and Viscosities of Propane-1,2,3-triol + Ethane-1,2-diol at T = (298.15 to 338.15) K

dvisc	0.0045300	Pa×s	338.15	Densities and Viscosities of Propane-1,2,3-triol + Ethane-1,2-diol at T = (298.15 to 338.15) K
dvisc	0.0154081	Pa×s	298.15	Densities, Viscosities, and Volumetric Properties of Binary Mixtures of 1,2-Propanediol + 1-Heptanol or 1-Hexanol and 1,2-Ethanediol + 2-Butanol or 2-Propanol at T = (298.15, 303.15, and 308.15) K
dvisc	0.0127314	Pa×s	303.15	Densities, Viscosities, and Volumetric Properties of Binary Mixtures of 1,2-Propanediol + 1-Heptanol or 1-Hexanol and 1,2-Ethanediol + 2-Butanol or 2-Propanol at T = (298.15, 303.15, and 308.15) K
dvisc	0.0106614	Pa×s	308.15	Densities, Viscosities, and Volumetric Properties of Binary Mixtures of 1,2-Propanediol + 1-Heptanol or 1-Hexanol and 1,2-Ethanediol + 2-Butanol or 2-Propanol at T = (298.15, 303.15, and 308.15) K
dvisc	0.0100100	Pa×s	313.15	Viscosity of binary mixtures of 1-ethyl-3-methylimidazolium tetrafluoroborate ionic liquid with four organic solvents

dvisc	0.0050650	Pa×s	333.15	Excess Molar Volumes and Viscosities of Binary Mixtures of p-Cresol with Ethylene Glycol and Methanol at Different Temperature and Atmospheric Pressure
dvisc	0.0143300	Pa×s	303.15	Viscosity of binary mixtures of 1-ethyl-3-methylimidazolium tetrafluoroborate ionic liquid with four organic solvents
dvisc	0.0174100	Pa×s	298.15	Viscosity of binary mixtures of 1-ethyl-3-methylimidazolium tetrafluoroborate ionic liquid with four organic solvents
dvisc	0.0214400	Pa×s	293.15	Viscosity of binary mixtures of 1-ethyl-3-methylimidazolium tetrafluoroborate ionic liquid with four organic solvents
dvisc	0.0006520	Pa×s	464.40	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0009600	Pa×s	421.70	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure

dvisc	0.0014190	Pa×s	395.55	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure	
dvisc	0.0018150	Pa×s	380.82	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure	
dvisc	0.0023900	Pa×s	365.70	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure	
dvisc	0.0035170	Pa×s	349.24	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure	
dvisc	0.0049490	Pa×s	334.87	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure	

dvisc	0.0104780	Pa×s	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
dvisc	0.0099250	Pa×s	312.46	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0211000	Pa×s	293.15	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0032420	Pa×s	353.15	Viscosity of binary mixtures of 1-ethyl-3-methylimidazolium tetrafluoroborate ionic liquid with four organic solvents
dvisc	0.0111930	Pa×s	308.15	Excess Molar Volumes and Viscosities of Binary Mixtures of p-Cresol with Ethylene Glycol and Methanol at Different Temperature and Atmospheric Pressure

econd	1.68e-04	S/m	343.15	Permittivity and electrical conductivity of copper oxide nanofluid (12 nm) in water at different temperatures	
econd	1.21e-04	S/m	333.15	Permittivity and electrical conductivity of copper oxide nanofluid (12 nm) in water at different temperatures	
econd	8.00e-05	S/m	323.15	Permittivity and electrical conductivity of copper oxide nanofluid (12 nm) in water at different temperatures	
econd	4.60e-05	S/m	313.15	Permittivity and electrical conductivity of copper oxide nanofluid (12 nm) in water at different temperatures	
econd	0.00	S/m	303.15	Micellar Properties and Related Thermodynamic Parameters of the 14-6-14, 2Br-Gemini Surfactant in Water + Organic Solvent Mixed Media	
econd	1.50e-05	S/m	293.15	Permittivity and electrical conductivity of copper oxide nanofluid (12 nm) in water at different temperatures	
econd	2.90e-05	S/m	303.15	Permittivity and electrical conductivity of copper oxide nanofluid (12 nm) in water at different temperatures	
hfust	9.96	kJ/mol	260.60	NIST Webbook	
hfust	11.60	kJ/mol	260.80	NIST Webbook	
hfust	9.96	kJ/mol	260.60	NIST Webbook	

hfust	11.62	kJ/mol	260.80	NIST Webbook
hvapt	57.30	kJ/mol	436.50	NIST Webbook
hvapt	62.50	kJ/mol	390.50	NIST Webbook
hvapt	65.20	kJ/mol	398.00	NIST Webbook
hvapt	57.40	kJ/mol	385.50	NIST Webbook
hvapt	63.90	kJ/mol	298.15	Vaporization Enthalpies of the r,o-Alkanediols by Correlation Gas Chromatography
hvapt	52.51	kJ/mol	470.50	KDB
hvapt	62.40 ± 4.00	kJ/mol	345.50	NIST Webbook
hvapt	61.10	kJ/mol	427.00	NIST Webbook
hvapt	64.00	kJ/mol	398.00	NIST Webbook
hvapt	61.90 ± 6.30	kJ/mol	273.00	NIST Webbook
hvapt	61.10	kJ/mol	383.00	NIST Webbook
hvapt	68.00 ± 2.00	kJ/mol	409.00	NIST Webbook
pvap	10.02	kPa	406.25	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa
pvap	20.00	kPa	420.74	Isobaric Vapor Liquid Equilibrium for the Binary System (Ethane-1,2-diol + Butan-1,2-diol) at (20, 30, and 40) kPa
pvap	3.47	kPa	384.50	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	1.95	kPa	373.40	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K

pvap	1.48	kPa	367.90	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	0.90	kPa	359.20	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	0.45	kPa	347.90	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	0.28	kPa	340.20	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	0.20	kPa	335.20	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	0.20	kPa	334.50	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	0.12	kPa	328.20	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K

pvap	0.11	kPa	326.10	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	0.08	kPa	322.10	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	0.06	kPa	318.80	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	0.06	kPa	316.50	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	0.04	kPa	312.60	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	0.03	kPa	307.70	Vapor Pressure Measurements of Hydroxyacetaldehyde and Hydroxyacetone in the Temperature Range (273 to 356) K
pvap	30.00	kPa	432.29	Isobaric Vapor Liquid Equilibrium for the Binary System (Ethane-1,2-diol + Butan-1,2-diol) at (20, 30, and 40) kPa

pvap	40.00	kPa	440.15	Isobaric Vapor Liquid Equilibrium for the Binary System (Ethane-1,2-diol + Butan-1,2-diol) at (20, 30, and 40) kPa
pvap	11.34	kPa	408.25	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures
pvap	9.20	kPa	404.05	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures
pvap	7.14	kPa	397.25	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures
pvap	6.01	kPa	394.56	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures

pvap	5.33	kPa	391.45	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures
pvap	4.40	kPa	388.10	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures
pvap	3.57	kPa	384.45	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures
pvap	2.66	kPa	378.95	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures
pvap	2.13	kPa	374.45	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures

pvap	1.69	kPa	369.25	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures
pvap	0.90	kPa	355.15	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures
pvap	0.48	kPa	345.00	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures
pvap	0.25	kPa	336.45	Determination and Modeling of Isobaric Vapor Liquid Equilibria for the Methylcarbamate + Methyl-N-phenyl Carbamate System at Different Pressures
pvap	101.30	kPa	470.47	Vapor Liquid Equilibria for Three Binary Systems of N-Methylethanolamine, N-Methyldiethanolamine, and Ethylene Glycol at P = (40.0, 30.0, and 20.0) kPa

pvap	20.00	kPa	422.75	Vapor Liquid Equilibria for Three Binary Systems of N-Methylethanolamine, N-Methyldiethanolamine, and Ethylene Glycol at P = (40.0, 30.0, and 20.0) kPa
pvap	30.00	kPa	433.66	Vapor Liquid Equilibria for Three Binary Systems of N-Methylethanolamine, N-Methyldiethanolamine, and Ethylene Glycol at P = (40.0, 30.0, and 20.0) kPa
pvap	40.00	kPa	441.66	Vapor Liquid Equilibria for Three Binary Systems of N-Methylethanolamine, N-Methyldiethanolamine, and Ethylene Glycol at P = (40.0, 30.0, and 20.0) kPa
pvap	20.00	kPa	422.80	Vapor Liquid Equilibria for Three Binary Systems of N-Methylethanolamine, N-Methyldiethanolamine, and Ethylene Glycol at P = (40.0, 30.0, and 20.0) kPa
pvap	30.00	kPa	433.71	Vapor Liquid Equilibria for Three Binary Systems of N-Methylethanolamine, N-Methyldiethanolamine, and Ethylene Glycol at P = (40.0, 30.0, and 20.0) kPa
pvap	40.00	kPa	441.70	Vapor Liquid Equilibria for Three Binary Systems of N-Methylethanolamine, N-Methyldiethanolamine, and Ethylene Glycol at P = (40.0, 30.0, and 20.0) kPa

pvap	10.00	kPa	406.09	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa	
pvap	15.37	kPa	416.45	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa	
pvap	13.85	kPa	413.85	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa	
pvap	12.85	kPa	411.85	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa	
pvap	12.41	kPa	411.15	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa	

pvap	11.42	kPa	409.30	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa
pvap	9.85	kPa	405.85	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa
pvap	8.37	kPa	402.15	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa
pvap	7.87	kPa	400.78	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa
pvap	6.08	kPa	395.25	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa

pvap	4.89	kPa	390.75	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa	
pvap	4.78	kPa	389.95	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa	
pvap	4.51	kPa	389.12	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa	
pvap	3.92	kPa	386.15	Isobaric Vapor Liquid Equilibria for the Binary Mixtures Composed of Ethylene Glycol, 1,2-Propylene Glycol, 1,2-Butanediol, and 1,3-Butanediol at 10.00 kPa	
pvap	100.40	kPa	470.02	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems	

pvap	98.66	kPa	469.48	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	93.32	kPa	467.62	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	86.66	kPa	465.18	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	79.99	kPa	462.58	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	73.33	kPa	459.79	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	66.66	kPa	456.78	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	60.00	kPa	453.52	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems

pvap	53.33	kPa	449.93	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	46.66	kPa	445.96	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	33.33	kPa	436.37	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	26.66	kPa	430.26	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	20.00	kPa	422.78	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	13.33	kPa	412.81	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	101.32	kPa	469.15	Cosolvent Selection for Benzene-Cyclohexane Separation in Extractive Distillation

pvap	1.24	kPa	363.60	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.92	kPa	358.60	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.68	kPa	353.60	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.49	kPa	348.60	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.36	kPa	343.60	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method

pvap	0.27	kPa	339.60	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.22	kPa	336.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.18	kPa	333.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.15	kPa	331.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method

pvap	0.11	kPa	326.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.08	kPa	323.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.07	kPa	320.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.06	kPa	318.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.05	kPa	316.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method

pvap	0.04	kPa	313.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.03	kPa	310.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.03	kPa	308.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.02	kPa	306.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method

pvap	0.02	kPa	303.20	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.77	kPa	353.15	Isothermal Vapor-Liquid Equilibrium and Excess Enthalpy Data for the Binary Systems Water + 1,2-Ethanediol and Propene + Acetophenone
pvap	0.22	kPa	333.15	Isothermal Vapor-Liquid Equilibrium and Excess Enthalpy Data for the Binary Systems Water + 1,2-Ethanediol and Propene + Acetophenone
pvap	101.30	kPa	470.22	Investigation on Thermodynamics in Separation for Ethylene Glycol + Neopentyl Glycol System by Azeotropic Distillation
pvap	40.00	kPa	441.50	Isobaric Vapor-Liquid Equilibria for Ethanol + Water + Ethylene Glycol and Its Constituent Three Binary Systems
pvap	0.12	kPa	328.10	Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method

rfi	1.43090	298.15	Densities, Excess Molar Volumes, and Isobaric Thermal Expansibilities for 1,2-Ethanediol + 1-Butanol, or 1-Hexanol, or 1-Octanol in the Temperature Range from (293.15 to 313.15) K
rfi	1.43060	298.15	Liquid liquid equilibria of the systems dipropyl ether + n-propanol +water and dipropyl ether + n-propanol + ethylene glycol at different temperatures
rfi	1.43040	298.15	Density and refractive index in mixtures of ionic liquids and organic solvents: Correlations and predictions
rfi	1.43070	298.15	Thermodynamic and transport properties of (1,2-ethanediol + 1-nonanol) at temperatures from (298.15 to 313.15) K
rfi	1.43180	293.15	Experimental Vapor-Liquid Equilibrium Data for Binary Mixtures of Methyldiethanolamine in Water and Ethylene Glycol under Vacuum
rfi	1.43159	298.15	Phase Equilibrium Involving Xylose, Water, and Ethylene Glycol or 1,2-Propylene Glycol at Different Temperatures

rfi	1.43070	298.15	Density, Viscosity, Refractive Index, and Speed of Sound in the Binary Mixtures of 1,4-Dioxane + Ethanediol, + Hexane, + Tributylamine, or + Triethylamine at (298.15, 303.15, and 308.15) K	
rfi	1.42690	303.15	Density, Viscosity, Refractive Index, and Speed of Sound in the Binary Mixtures of 1,4-Dioxane + Ethanediol, + Hexane, + Tributylamine, or + Triethylamine at (298.15, 303.15, and 308.15) K	
rfi	1.42460	308.15	Density, Viscosity, Refractive Index, and Speed of Sound in the Binary Mixtures of 1,4-Dioxane + Ethanediol, + Hexane, + Tributylamine, or + Triethylamine at (298.15, 303.15, and 308.15) K	
rfi	1.43280	293.15	Isobaric Vapor - Liquid Equilibria for the Ternary System of 2-Methyl-1-butanol, 3-Methyl-1-butanol, and Ethylene Glycol at 101.3 kPa	
rfi	1.43184	293.15	Liquid-Liquid Equilibria of (Limonene + Linalool + Ethylene Glycol or Diethylene Glycol or Triethylene Glycol or 1,2-Propylene Glycol) Ternary Systems	

rfi	1.43230		293.15	Densities, Excess Molar Volumes, and Isobaric Thermal Expansibilities for 1,2-Ethanediol + 1-Butanol, or 1-Hexanol, or 1-Octanol in the Temperature Range from (293.15 to 313.15) K	
rhol	1073.70	kg/m3	348.15	Measurements and correlations of solubility of N2O in and density, viscosity of partially CO2 loaded water-lean amino acid salts	
rhol	1088.83	kg/m3	328.15	Volume-related solvation and pair interaction parameters for dilute solutions of urea and tetramethylurea in ethylene glycol between 288.15 K and 328.15 K: A comparative analysis	
rhol	1102.93	kg/m3	308.15	Excess molar enthalpies of binary mixtures containing ethylene glycols or poly(ethylene glycols) + ethyl alcohol at 308.15K and atmospheric pressure	
rhol	1106.00	kg/m3	303.15	Thermodynamic study on some alkanediol solutions: measurement and molecular modeling	
rhol	1102.70	kg/m3	308.15	Thermodynamic study on some alkanediol solutions: measurement and molecular modeling	

rhol	1109.70	kg/m3	298.15	Thermodynamic study on some alkanediol solutions: measurement and molecular modeling
rhol	1118.20	kg/m3	288.15	Thermophysical properties of glycols and glymes
rhol	1114.60	kg/m3	293.15	Thermophysical properties of glycols and glymes
rhol	1111.10	kg/m3	298.15	Thermophysical properties of glycols and glymes
rhol	1107.60	kg/m3	303.15	Thermophysical properties of glycols and glymes
rhol	1104.10	kg/m3	308.15	Thermophysical properties of glycols and glymes
rhol	1100.50	kg/m3	313.15	Thermophysical properties of glycols and glymes
rhol	1097.00	kg/m3	318.15	Thermophysical properties of glycols and glymes
rhol	1093.40	kg/m3	323.15	Thermophysical properties of glycols and glymes
rhol	1089.80	kg/m3	328.15	Thermophysical properties of glycols and glymes
rhol	1086.20	kg/m3	333.15	Thermophysical properties of glycols and glymes
rhol	1082.60	kg/m3	338.15	Thermophysical properties of glycols and glymes
rhol	1078.90	kg/m3	343.15	Thermophysical properties of glycols and glymes
rhol	1075.20	kg/m3	348.15	Thermophysical properties of glycols and glymes

rhol	1071.50	kg/m3	353.15	Thermophysical properties of glycols and glymes
rhol	1067.80	kg/m3	358.15	Thermophysical properties of glycols and glymes
rhol	1064.00	kg/m3	363.15	Thermophysical properties of glycols and glymes
rhol	1060.20	kg/m3	368.15	Thermophysical properties of glycols and glymes
rhol	1056.40	kg/m3	373.15	Thermophysical properties of glycols and glymes
rhol	1120.20	kg/m3	283.15	Thermophysical properties of glycols and glymes
rhol	1116.80	kg/m3	288.15	Thermophysical properties of glycols and glymes
rhol	1113.30	kg/m3	293.15	Thermophysical properties of glycols and glymes
rhol	1109.80	kg/m3	298.15	Thermophysical properties of glycols and glymes
rhol	1106.30	kg/m3	303.15	Thermophysical properties of glycols and glymes
rhol	1102.70	kg/m3	308.15	Thermophysical properties of glycols and glymes
rhol	1077.50	kg/m3	343.15	Measurements and correlations of solubility of N2O in and density, viscosity of partially CO2 loaded water-lean amino acid salts
rhol	1092.10	kg/m3	323.15	Thermophysical properties of glycols and glymes

rhol	1084.80	kg/m3	333.15	Thermophysical properties of glycols and glymes
rhol	1077.50	kg/m3	343.15	Thermophysical properties of glycols and glymes
rhol	1127.05	kg/m3	273.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1120.50	kg/m3	283.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1113.84	kg/m3	293.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1107.07	kg/m3	303.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1100.19	kg/m3	313.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1093.20	kg/m3	323.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1086.11	kg/m3	333.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1078.91	kg/m3	343.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1071.60	kg/m3	353.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1064.18	kg/m3	363.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	1120.00	kg/m3	283.15	Density and Viscosity of the Nonaqueous and Aqueous Mixtures of Methyldiethanolamine and Monoethylene Glycol at Temperatures from 283.15 to 353.15 K

rhol	1109.90	kg/m3	298.15	Density and Viscosity of the Nonaqueous and Aqueous Mixtures of Methyldiethanolamine and Monoethylene Glycol at Temperatures from 283.15 to 353.15 K
rhol	1099.10	kg/m3	313.15	Density and Viscosity of the Nonaqueous and Aqueous Mixtures of Methyldiethanolamine and Monoethylene Glycol at Temperatures from 283.15 to 353.15 K
rhol	1091.60	kg/m3	323.15	Density and Viscosity of the Nonaqueous and Aqueous Mixtures of Methyldiethanolamine and Monoethylene Glycol at Temperatures from 283.15 to 353.15 K
rhol	1085.00	kg/m3	333.15	Density and Viscosity of the Nonaqueous and Aqueous Mixtures of Methyldiethanolamine and Monoethylene Glycol at Temperatures from 283.15 to 353.15 K
rhol	1077.60	kg/m3	343.15	Density and Viscosity of the Nonaqueous and Aqueous Mixtures of Methyldiethanolamine and Monoethylene Glycol at Temperatures from 283.15 to 353.15 K

rhol	1070.10	kg/m3	353.15	Density and Viscosity of the Nonaqueous and Aqueous Mixtures of Methyldiethanolamine and Monoethylene Glycol at Temperatures from 283.15 to 353.15 K
rhol	1113.70	kg/m3	293.15	Excess Molar Volumes, Viscosities, and Heat Capacities for the Mixtures of Ethylene Glycol + Water from 273.15 K to 353.15 K
rhol	1103.20	kg/m3	303.15	Excess Molar Volumes, Viscosities, and Heat Capacities for the Mixtures of Ethylene Glycol + Water from 273.15 K to 353.15 K
rhol	1093.60	kg/m3	313.15	Excess Molar Volumes, Viscosities, and Heat Capacities for the Mixtures of Ethylene Glycol + Water from 273.15 K to 353.15 K
rhol	1084.70	kg/m3	323.15	Excess Molar Volumes, Viscosities, and Heat Capacities for the Mixtures of Ethylene Glycol + Water from 273.15 K to 353.15 K
rhol	1076.40	kg/m3	333.15	Excess Molar Volumes, Viscosities, and Heat Capacities for the Mixtures of Ethylene Glycol + Water from 273.15 K to 353.15 K

rhol	1067.50	kg/m3	343.15	Excess Molar Volumes, Viscosities, and Heat Capacities for the Mixtures of Ethylene Glycol + Water from 273.15 K to 353.15 K
rhol	1060.00	kg/m3	353.15	Excess Molar Volumes, Viscosities, and Heat Capacities for the Mixtures of Ethylene Glycol + Water from 273.15 K to 353.15 K
rhol	1102.93	kg/m3	308.15	Excess Molar Enthalpies of Binary Mixtures Containing Glycols or Polyglycols + Dimethyl Sulfoxide at 308.15 K
rhol	1109.80	kg/m3	298.15	Thermodynamic Study of Binary Mixtures Containing Glycols or Polyethylene Glycols + Benzyl Alcohol at 308.15 K
rhol	1102.93	kg/m3	308.15	Thermodynamic Study of Binary Mixtures Containing Glycols or Polyethylene Glycols + Benzyl Alcohol at 308.15 K
rhol	1109.80	kg/m3	298.15	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Glycols or Poly(Ethylene Glycols) and 2-Phenylethyl Alcohol at 308.15 K and Atmospheric Pressure

rhol	1102.93	kg/m3	308.15	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Glycols or Poly(Ethylene Glycols) and 2-Phenylethyl Alcohol at 308.15 K and Atmospheric Pressure
rhol	1123.77	kg/m3	278.15	Densities and Volumetric Properties of Ethylene Glycol + Dimethylsulfoxide Mixtures at Temperatures of (278.15 to 323.15) K and Pressures of (0.1 to 100) MPa
rhol	1116.83	kg/m3	288.15	Densities and Volumetric Properties of Ethylene Glycol + Dimethylsulfoxide Mixtures at Temperatures of (278.15 to 323.15) K and Pressures of (0.1 to 100) MPa
rhol	1109.83	kg/m3	298.15	Densities and Volumetric Properties of Ethylene Glycol + Dimethylsulfoxide Mixtures at Temperatures of (278.15 to 323.15) K and Pressures of (0.1 to 100) MPa
rhol	1102.81	kg/m3	308.15	Densities and Volumetric Properties of Ethylene Glycol + Dimethylsulfoxide Mixtures at Temperatures of (278.15 to 323.15) K and Pressures of (0.1 to 100) MPa

rhol	1092.12	kg/m3	323.15	Densities and Volumetric Properties of Ethylene Glycol + Dimethylsulfoxide Mixtures at Temperatures of (278.15 to 323.15) K and Pressures of (0.1 to 100) MPa	
rhol	1109.60	kg/m3	298.15	Solubility of Carbonyl Sulfide in Aqueous Solutions of Ethylene Glycol at Temperatures from (308.15 K to 323.15) K	
rhol	1109.90	kg/m3	298.15	Liquid-Liquid Equilibrium in Ternary Systems Containing Ethylene Glycol, Monofunctional Benzene Derivative, and Ethyl Acetate	
rhol	1119.29	kg/m3	283.15	Densities and Excess Properties of Primary Amines in Alcoholic Solutions	
rhol	1112.37	kg/m3	293.15	Densities and Excess Properties of Primary Amines in Alcoholic Solutions	
rhol	1105.39	kg/m3	303.15	Densities and Excess Properties of Primary Amines in Alcoholic Solutions	
rhol	1098.34	kg/m3	313.15	Densities and Excess Properties of Primary Amines in Alcoholic Solutions	
rhol	1091.21	kg/m3	323.15	Densities and Excess Properties of Primary Amines in Alcoholic Solutions	

rhol	1083.99	kg/m3	333.15	Densities and Excess Properties of Primary Amines in Alcoholic Solutions
rhol	1076.65	kg/m3	343.15	Densities and Excess Properties of Primary Amines in Alcoholic Solutions
rhol	1098.90	kg/m3	313.15	Solubilities of CO2 in, and Densities and Viscosities of, the Piperazine + 1-Ethyl-3-methyl-imidazolium Acetate + H2O System
rhol	1091.70	kg/m3	323.15	Solubilities of CO2 in, and Densities and Viscosities of, the Piperazine + 1-Ethyl-3-methyl-imidazolium Acetate + H2O System
rhol	1084.20	kg/m3	333.15	Solubilities of CO2 in, and Densities and Viscosities of, the Piperazine + 1-Ethyl-3-methyl-imidazolium Acetate + H2O System
rhol	1078.10	kg/m3	343.15	Solubilities of CO2 in, and Densities and Viscosities of, the Piperazine + 1-Ethyl-3-methyl-imidazolium Acetate + H2O System
rhol	1113.45	kg/m3	293.15	Density and Refractive Index of Binary Mixtures of Two 1-Alkyl-3-methylimidazolium Ionic Liquids with 1,4-Dioxane and Ethylene Glycol
rhol	1109.96	kg/m3	298.15	Density and Refractive Index of Binary Mixtures of Two 1-Alkyl-3-methylimidazolium Ionic Liquids with 1,4-Dioxane and Ethylene Glycol

rhol	1106.45	kg/m3	303.15	Density and Refractive Index of Binary Mixtures of Two 1-Alkyl-3-methylimidazolium Ionic Liquids with 1,4-Dioxane and Ethylene Glycol
rhol	1099.38	kg/m3	313.15	Density and Refractive Index of Binary Mixtures of Two 1-Alkyl-3-methylimidazolium Ionic Liquids with 1,4-Dioxane and Ethylene Glycol
rhol	1092.24	kg/m3	323.15	Density and Refractive Index of Binary Mixtures of Two 1-Alkyl-3-methylimidazolium Ionic Liquids with 1,4-Dioxane and Ethylene Glycol
rhol	1085.00	kg/m3	333.15	Density and Refractive Index of Binary Mixtures of Two 1-Alkyl-3-methylimidazolium Ionic Liquids with 1,4-Dioxane and Ethylene Glycol
rhol	1077.65	kg/m3	343.15	Density and Refractive Index of Binary Mixtures of Two 1-Alkyl-3-methylimidazolium Ionic Liquids with 1,4-Dioxane and Ethylene Glycol
rhol	1070.17	kg/m3	353.15	Density and Refractive Index of Binary Mixtures of Two 1-Alkyl-3-methylimidazolium Ionic Liquids with 1,4-Dioxane and Ethylene Glycol
rhol	1107.92	kg/m3	298.15	Isobaric Vapor-Liquid Equilibrium for Four Binary Systems of Ethane-1,2-diol, Butane-1,4-diol, 2-(2-Hydroxyethoxy)ethan-1-ol and 2-[2-(2-Hydroxyethoxy)ethoxy]ethanol at 10.0 kPa, 20.0 kPa and 40.0 kPa

rhol	1110.20	kg/m3	298.15	Solubility Properties and Spectral Characterization of Dilute SO2 in Binary Mixtures of Urea + Ethylene Glycol	
rhol	1106.60	kg/m3	303.15	Solubility Properties and Spectral Characterization of Dilute SO2 in Binary Mixtures of Urea + Ethylene Glycol	
rhol	1103.00	kg/m3	308.15	Solubility Properties and Spectral Characterization of Dilute SO2 in Binary Mixtures of Urea + Ethylene Glycol	
rhol	1099.30	kg/m3	313.15	Solubility Properties and Spectral Characterization of Dilute SO2 in Binary Mixtures of Urea + Ethylene Glycol	
rhol	1095.80	kg/m3	318.15	Solubility Properties and Spectral Characterization of Dilute SO2 in Binary Mixtures of Urea + Ethylene Glycol	
rhol	1109.82	kg/m3	298.15	Isobaric Vapor Liquid Equilibrium for Two Binary Systems{Propane-1,2-diol + Ethane-1,2-diol and Propane-1,2-diol + Butane-1,2-diol} at p = (10.0, 20.0, and 40.0) kPa	

rhol	1113.55	kg/m3	293.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhol	1109.86	kg/m3	298.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhol	1106.82	kg/m3	303.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhol	1103.20	kg/m3	308.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhol	1099.80	kg/m3	313.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K

rhol	1096.23	kg/m3	318.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhol	1092.59	kg/m3	323.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhol	1088.66	kg/m3	328.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K
rhol	1109.71	kg/m3	298.15	Surface Properties of Binary Mixtures of Ethylene Glycol with a Series of Aliphatic Alcohols (1-Pentanol, 1-Hexanol, and 1-Heptanol)
rhol	1121.00	kg/m3	293.15	Interfacial Properties, Densities, and Contact Angles of Task Specific Ionic Liquids
rhol	1081.20	kg/m3	338.15	Measurements and correlations of solubility of N2O in and density, viscosity of partially CO2 loaded water-lean amino acid salts

rhol	1084.80	kg/m3	333.15	Measurements and correlations of solubility of N2O in and density, viscosity of partially CO2 loaded water-lean amino acid salts	
rhol	1088.40	kg/m3	328.15	Measurements and correlations of solubility of N2O in and density, viscosity of partially CO2 loaded water-lean amino acid salts	
rhol	1092.10	kg/m3	323.15	Measurements and correlations of solubility of N2O in and density, viscosity of partially CO2 loaded water-lean amino acid salts	
rhol	1095.60	kg/m3	318.15	Measurements and correlations of solubility of N2O in and density, viscosity of partially CO2 loaded water-lean amino acid salts	
rhol	1099.20	kg/m3	313.15	Measurements and correlations of solubility of N2O in and density, viscosity of partially CO2 loaded water-lean amino acid salts	
rhol	1102.70	kg/m3	308.15	Measurements and correlations of solubility of N2O in and density, viscosity of partially CO2 loaded water-lean amino acid salts	
rhol	1106.30	kg/m3	303.15	Measurements and correlations of solubility of N2O in and density, viscosity of partially CO2 loaded water-lean amino acid salts	

rhol	1103.19	kg/m3	308.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhol	1106.71	kg/m3	303.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhol	1110.22	kg/m3	298.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhol	1113.72	kg/m3	293.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhol	1077.50	kg/m3	343.15	Density and refractive index measurements of transition-temperature mixture (deep eutectic analogues) based on potassium carbonate with dual hydrogen bond donors for CO2 capture
rhol	1081.20	kg/m3	338.15	Density and refractive index measurements of transition-temperature mixture (deep eutectic analogues) based on potassium carbonate with dual hydrogen bond donors for CO2 capture

rhol	1084.90	kg/m3	333.15	Density and refractive index measurements of transition-temperature mixture (deep eutectic analogues) based on potassium carbonate with dual hydrogen bond donors for CO2 capture
rhol	1088.50	kg/m3	328.15	Density and refractive index measurements of transition-temperature mixture (deep eutectic analogues) based on potassium carbonate with dual hydrogen bond donors for CO2 capture
rhol	1092.10	kg/m3	323.15	Density and refractive index measurements of transition-temperature mixture (deep eutectic analogues) based on potassium carbonate with dual hydrogen bond donors for CO2 capture
rhol	1099.20	kg/m3	313.15	Density and refractive index measurements of transition-temperature mixture (deep eutectic analogues) based on potassium carbonate with dual hydrogen bond donors for CO2 capture
rhol	1102.80	kg/m3	308.15	Density and refractive index measurements of transition-temperature mixture (deep eutectic analogues) based on potassium carbonate with dual hydrogen bond donors for CO2 capture

rhol	1106.30	kg/m3	303.15	Density and refractive index measurements of transition-temperature mixture (deep eutectic analogues) based on potassium carbonate with dual hydrogen bond donors for CO2 capture
rhol	1109.80	kg/m3	298.15	Density and refractive index measurements of transition-temperature mixture (deep eutectic analogues) based on potassium carbonate with dual hydrogen bond donors for CO2 capture
rhol	1113.30	kg/m3	293.15	Density and refractive index measurements of transition-temperature mixture (deep eutectic analogues) based on potassium carbonate with dual hydrogen bond donors for CO2 capture
rhol	1106.00	kg/m3	303.15	Thermodynamic and transport properties of acetonitrile + alkanediols liquid mixtures at different temperatures, experimental measurements and modeling
rhol	1109.00	kg/m3	298.15	Thermodynamic and transport properties of acetonitrile + alkanediols liquid mixtures at different temperatures, experimental measurements and modeling

rhol	1113.00	kg/m3	293.15	Thermodynamic and transport properties of acetonitrile + alkanediols liquid mixtures at different temperatures, experimental measurements and modeling
rhol	1110.00	kg/m3	298.15	Activity coefficients at infinite dilution of hydrocarbons in glycols: Experimental data and thermodynamic modeling with the GCA-EoS
rhol	1095.80	kg/m3	318.15	Solubility for dilute sulfur dioxide in binary mixtures of N,N-dimethylformamide + Ethylene Glycol at T = 308.15 Kand p = 122.66 kPa
rhol	1099.30	kg/m3	313.15	Solubility for dilute sulfur dioxide in binary mixtures of N,N-dimethylformamide + Ethylene Glycol at T = 308.15 Kand p = 122.66 kPa
rhol	1103.00	kg/m3	308.15	Solubility for dilute sulfur dioxide in binary mixtures of N,N-dimethylformamide + Ethylene Glycol at T = 308.15 Kand p = 122.66 kPa
rhol	1106.60	kg/m3	303.15	Solubility for dilute sulfur dioxide in binary mixtures of N,N-dimethylformamide + Ethylene Glycol at T = 308.15 Kand p = 122.66 kPa

rhol	1110.20	kg/m3	298.15	Solubility for dilute sulfur dioxide in binary mixtures of N,N-dimethylformamide + Ethylene Glycol at T = 308.15 Kand p = 122.66 kPa
rhol	1102.70	kg/m3	308.15	Investigation on some thermophysical properties of poly(ethylene glycol) binary mixtures at different temperatures
rhol	1106.00	kg/m3	303.15	Investigation on some thermophysical properties of poly(ethylene glycol) binary mixtures at different temperatures
rhol	1109.70	kg/m3	298.15	Investigation on some thermophysical properties of poly(ethylene glycol) binary mixtures at different temperatures
rhol	1088.56	kg/m3	328.15	Viscosity and density data for the ternary system water(1) ethanol(2) ethylene glycol(3) between 298.15 K and 328.15 K
rhol	1092.16	kg/m3	323.15	Viscosity and density data for the ternary system water(1) ethanol(2) ethylene glycol(3) between 298.15 K and 328.15 K
rhol	1095.75	kg/m3	318.15	Viscosity and density data for the ternary system water(1) ethanol(2) ethylene glycol(3) between 298.15 K and 328.15 K

rhol	1099.31	kg/m3	313.15	Viscosity and density data for the ternary system water(1) ethanol(2) ethylene glycol(3) between 298.15 K and 328.15 K
rhol	1102.86	kg/m3	308.15	Viscosity and density data for the ternary system water(1) ethanol(2) ethylene glycol(3) between 298.15 K and 328.15 K
rhol	1106.38	kg/m3	303.15	Viscosity and density data for the ternary system water(1) ethanol(2) ethylene glycol(3) between 298.15 K and 328.15 K
rhol	1109.89	kg/m3	298.15	Viscosity and density data for the ternary system water(1) ethanol(2) ethylene glycol(3) between 298.15 K and 328.15 K
rhol	1102.90	kg/m3	308.15	Molecular interactions of a,x-alkanediols in pyrrolidin-2-one: Thermophysical and spectroscopic measurements
rhol	1102.90	kg/m3	308.15	Structural and interactional studies of homologous series of a,x-alkanediols in N,N-dimethylformamide
rhol	1113.23	kg/m3	293.15	Transport properties of 2:2 symmetrical electrolytes in (water + ethylene glycol) binary mixtures at T = 293.15 K

rhol	1103.30	kg/m3	308.15	Liquid-liquid phase equilibrium for ternary mixtures of formamide (or ethylene glycol, or monoethanolamine) + indole + 2-methylnaphthalene at 308.15 K
rhol	1095.69	kg/m3	318.15	Effect of structural alteration of ionic liquid on their bulk and molecular level interactions with ethylene glycol
rhol	1099.26	kg/m3	313.15	Effect of structural alteration of ionic liquid on their bulk and molecular level interactions with ethylene glycol
rhol	1102.80	kg/m3	308.15	Effect of structural alteration of ionic liquid on their bulk and molecular level interactions with ethylene glycol
rhol	1106.33	kg/m3	303.15	Effect of structural alteration of ionic liquid on their bulk and molecular level interactions with ethylene glycol
rhol	1109.85	kg/m3	298.15	Effect of structural alteration of ionic liquid on their bulk and molecular level interactions with ethylene glycol
rhol	1113.35	kg/m3	293.15	Effect of structural alteration of ionic liquid on their bulk and molecular level interactions with ethylene glycol

rhol	1116.84	kg/m3	288.15	Effect of structural alteration of ionic liquid on their bulk and molecular level interactions with ethylene glycol	
rhol	1099.07	kg/m3	313.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	
rhol	1106.23	kg/m3	303.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	
rhol	1109.79	kg/m3	298.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	
rhol	1113.34	kg/m3	293.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	
rhol	1120.39	kg/m3	283.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	

rhol	1092.14	kg/m3	323.15	Liquid phase PVTx properties of binary mixtures of (water + ethylene glycol) in the range from 278.15 to 323.15 K and from 0.1 to 100 MPa. I. Experimental results, partial and excess thermodynamics properties	
rhol	1102.84	kg/m3	308.15	Liquid phase PVTx properties of binary mixtures of (water + ethylene glycol) in the range from 278.15 to 323.15 K and from 0.1 to 100 MPa. I. Experimental results, partial and excess thermodynamics properties	
rhol	1109.88	kg/m3	298.15	Liquid phase PVTx properties of binary mixtures of (water + ethylene glycol) in the range from 278.15 to 323.15 K and from 0.1 to 100 MPa. I. Experimental results, partial and excess thermodynamics properties	
rhol	1116.85	kg/m3	288.15	Liquid phase PVTx properties of binary mixtures of (water + ethylene glycol) in the range from 278.15 to 323.15 K and from 0.1 to 100 MPa. I. Experimental results, partial and excess thermodynamics properties	

rhol	1123.80	kg/m3	278.15	Liquid phase PVTx properties of binary mixtures of (water + ethylene glycol) in the range from 278.15 to 323.15 K and from 0.1 to 100 MPa. I. Experimental results, partial and excess thermodynamics properties
rhol	1109.90	kg/m3	298.15	Phase equilibria for the ternary systems ethanol, water + ethylene glycol or + glycerol at 101.3 kPa
rhol	1120.70	kg/m3	295.00	New device for fast measuring surface tension, density and viscosity of liquids
rhol	1109.90	kg/m3	298.15	Binary liquid liquid equilibrium in the systems containing monofunctional benzene derivates and 1,2-ethanediol
rhol	1109.90	kg/m3	298.15	Revision of the volumetric method for measurements of liquid liquid equilibria in binary systems
rhol	1099.30	kg/m3	313.15	Volumetric Properties of Binary Mixtures of 2,4,6-Trimethylpyridine with 1,2-Ethanediol, Methanol, and Water, and the Association Energies of the O-H***N Bonded Complexes

rhol	1102.84	kg/m3	308.15	Volumetric Properties of Binary Mixtures of 2,4,6-Trimethylpyridine with 1,2-Ethanediol, Methanol, and Water, and the Association Energies of the O-H***N Bonded Complexes
rhol	1106.36	kg/m3	303.15	Volumetric Properties of Binary Mixtures of 2,4,6-Trimethylpyridine with 1,2-Ethanediol, Methanol, and Water, and the Association Energies of the O-H***N Bonded Complexes
rhol	1109.87	kg/m3	298.14	Volumetric Properties of Binary Mixtures of 2,4,6-Trimethylpyridine with 1,2-Ethanediol, Methanol, and Water, and the Association Energies of the O-H***N Bonded Complexes
rhol	1113.37	kg/m3	293.15	Volumetric Properties of Binary Mixtures of 2,4,6-Trimethylpyridine with 1,2-Ethanediol, Methanol, and Water, and the Association Energies of the O-H***N Bonded Complexes
rhol	1116.86	kg/m3	288.15	Volumetric Properties of Binary Mixtures of 2,4,6-Trimethylpyridine with 1,2-Ethanediol, Methanol, and Water, and the Association Energies of the O-H***N Bonded Complexes

rhol	1120.32	kg/m3	283.15	Volumetric Properties of Binary Mixtures of 2,4,6-Trimethylpyridine with 1,2-Ethanediol, Methanol, and Water, and the Association Energies of the O-H***N Bonded Complexes
rhol	1124.48	kg/m3	277.15	Volumetric Properties of Binary Mixtures of 2,4,6-Trimethylpyridine with 1,2-Ethanediol, Methanol, and Water, and the Association Energies of the O-H***N Bonded Complexes
rhol	1125.17	kg/m3	276.15	Volumetric Properties of Binary Mixtures of 2,4,6-Trimethylpyridine with 1,2-Ethanediol, Methanol, and Water, and the Association Energies of the O-H***N Bonded Complexes
rhol	1114.00	kg/m3	293.00	KDB
rhol	1096.00	kg/m3	318.15	Volume-related solvation and pair interaction parameters for dilute solutions of urea and tetramethylurea in ethylene glycol between 288.15 K and 328.15 K: A comparative analysis
rhol	1103.08	kg/m3	308.15	Volume-related solvation and pair interaction parameters for dilute solutions of urea and tetramethylurea in ethylene glycol between 288.15 K and 328.15 K: A comparative analysis

rhol	1110.08	kg/m3	298.15	Volume-related solvation and pair interaction parameters for dilute solutions of urea and tetramethylurea in ethylene glycol between 288.15 K and 328.15 K: A comparative analysis	
rhol	1117.01	kg/m3	288.15	Volume-related solvation and pair interaction parameters for dilute solutions of urea and tetramethylurea in ethylene glycol between 288.15 K and 328.15 K: A comparative analysis	
rhol	1084.84	kg/m3	333.15	Solubilities of CO2 in, densities and kinematic viscosities of poly(propylene glycol) diglycidyl ether and poly(ethylene glycol) monooleate	
rhol	1092.07	kg/m3	323.15	Solubilities of CO2 in, densities and kinematic viscosities of poly(propylene glycol) diglycidyl ether and poly(ethylene glycol) monooleate	
rhol	1099.20	kg/m3	313.15	Solubilities of CO2 in, densities and kinematic viscosities of poly(propylene glycol) diglycidyl ether and poly(ethylene glycol) monooleate	
rhol	1106.26	kg/m3	303.15	Solubilities of CO2 in, densities and kinematic viscosities of poly(propylene glycol) diglycidyl ether and poly(ethylene glycol) monooleate	

rhol	1113.25	kg/m3	293.15	Solubilities of CO2 in, densities and kinematic viscosities of poly(propylene glycol) diglycidyl ether and poly(ethylene glycol) monooleate
rhol	1120.35	kg/m3	283.15	Solubilities of CO2 in, densities and kinematic viscosities of poly(propylene glycol) diglycidyl ether and poly(ethylene glycol) monooleate
rhol	1127.43	kg/m3	273.15	Solubilities of CO2 in, densities and kinematic viscosities of poly(propylene glycol) diglycidyl ether and poly(ethylene glycol) monooleate
rhol	1070.00	kg/m3	353.15	Measurements and correlations of solubility of N2O in and density, viscosity of partially CO2 loaded water-lean amino acid salts
rhol	1095.70	kg/m3	318.15	Density and refractive index measurements of transition-temperature mixture (deep eutectic analogues) based on potassium carbonate with dual hydrogen bond donors for CO2 capture
rhol	1099.20	kg/m3	313.15	Thermophysical properties of glycols and glymes
sfust	38.21	J/mol×K	260.60	NIST Webbook
sfust	44.57	J/mol×K	260.80	NIST Webbook

speedsl	1656.10	m/s	298.15	Volumetric and compressibility properties of liquid water as a solute in glycolic, propylene carbonate, and tetramethylurea solutions at T = 298.15 K
speedsl	1654.38	m/s	298.15	Densities, Speeds of Sound, and Isentropic Compressibilities for Binary Mixtures of 1,2-Ethanediol with 2-Ethyl-1-hexanol, 1-Heptanol, or Ethanol at the Temperature 298.15 K and Densities for Mixtures of 1,2-Ethanediol with 1-Nonanol at the Temperatures (293.15 and 298.15) K
srf	0.05	N/m	308.15	Surface Tension of Binary Mixtures of Ethanol + Ethylene glycol from 20 to 50 oC
srf	0.05	N/m	293.20	KDB
srf	0.05	N/m	283.15	Surface tension of non-ideal binary and ternary liquid mixtures at various temperatures and p = 81.5 kPa
srf	0.05	N/m	308.15	Gas-Liquid Equilibrium Data for a Mixture Gas of Sulfur Dioxide + Nitrogen with Ethylene Glycol Aqueous Solutions at 298.15 K and 123.15 kPa
srf	0.05	N/m	293.15	Surface Tension of Binary Mixtures of Ethanol + Ethylene glycol from 20 to 50 oC

srf	0.05	N/m	308.15	Surface tension of non-ideal binary and ternary liquid mixtures at various temperatures and p = 81.5 kPa
srf	0.05	N/m	298.15	Surface Tension of Binary Mixtures of Ethanol + Ethylene glycol from 20 to 50 oC
srf	0.05	N/m	323.15	Gas-Liquid Equilibrium Data for a Mixture Gas of Sulfur Dioxide + Nitrogen with Ethylene Glycol Aqueous Solutions at 298.15 K and 123.15 kPa
srf	0.05	N/m	318.15	Gas-Liquid Equilibrium Data for a Mixture Gas of Sulfur Dioxide + Nitrogen with Ethylene Glycol Aqueous Solutions at 298.15 K and 123.15 kPa
srf	0.05	N/m	313.15	Gas-Liquid Equilibrium Data for a Mixture Gas of Sulfur Dioxide + Nitrogen with Ethylene Glycol Aqueous Solutions at 298.15 K and 123.15 kPa
srf	0.05	N/m	298.15	Surface tension of non-ideal binary and ternary liquid mixtures at various temperatures and p = 81.5 kPa
srf	0.05	N/m	323.15	Surface Tensions of Dilute Solutions of Cycloheptanol in Ethylene Glycol
srf	0.05	N/m	303.15	Surface Tension of Binary Mixtures of Ethanol + Ethylene glycol from 20 to 50 oC

srf	0.05	N/m	313.15	Surface Tensions of Dilute Solutions of Cycloheptanol in Ethylene Glycol
srf	0.05	N/m	308.15	Surface Tensions of Dilute Solutions of Cycloheptanol in Ethylene Glycol
srf	0.05	N/m	303.15	Surface Tensions of Dilute Solutions of Cycloheptanol in Ethylene Glycol
srf	0.05	N/m	298.15	Surface Tensions of Dilute Solutions of Cycloheptanol in Ethylene Glycol
srf	0.05	N/m	293.15	Surface Tensions of Dilute Solutions of Cycloheptanol in Ethylene Glycol
srf	0.05	N/m	298.15	Concentration Dependence of Surface Tension for Very Dilute Aqueous Solutions of Organic Non-Electrolytes
srf	0.05	N/m	323.15	Surface Properties of Pure Liquids and Binary Liquid Mixtures of Ethylene Glycol + Methylcyclohexanols
srf	0.05	N/m	318.15	Surface Properties of Pure Liquids and Binary Liquid Mixtures of Ethylene Glycol + Methylcyclohexanols
srf	0.05	N/m	313.15	Surface Properties of Pure Liquids and Binary Liquid Mixtures of Ethylene Glycol + Methylcyclohexanols
srf	0.05	N/m	308.15	Surface Properties of Pure Liquids and Binary Liquid Mixtures of Ethylene Glycol + Methylcyclohexanols

srf	0.05	N/m	303.15	Surface Properties of Pure Liquids and Binary Liquid Mixtures of Ethylene Glycol + Methylcyclohexanols
srf	0.05	N/m	298.15	Surface Properties of Pure Liquids and Binary Liquid Mixtures of Ethylene Glycol + Methylcyclohexanols
srf	0.05	N/m	293.15	Surface Properties of Pure Liquids and Binary Liquid Mixtures of Ethylene Glycol + Methylcyclohexanols
srf	0.05	N/m	323.15	Equilibrium Surface Tensions of Benzyl Alcohol + Ethylene Glycol Mixtures
srf	0.05	N/m	318.15	Equilibrium Surface Tensions of Benzyl Alcohol + Ethylene Glycol Mixtures
srf	0.05	N/m	313.15	Equilibrium Surface Tensions of Benzyl Alcohol + Ethylene Glycol Mixtures
srf	0.05	N/m	308.15	Equilibrium Surface Tensions of Benzyl Alcohol + Ethylene Glycol Mixtures
srf	0.05	N/m	303.15	Equilibrium Surface Tensions of Benzyl Alcohol + Ethylene Glycol Mixtures
srf	0.05	N/m	298.15	Equilibrium Surface Tensions of Benzyl Alcohol + Ethylene Glycol Mixtures
srf	0.05	N/m	293.15	Equilibrium Surface Tensions of Benzyl Alcohol + Ethylene Glycol Mixtures
srf	0.05	N/m	323.15	Surface Tension of Binary Mixtures of Ethanol + Ethylene glycol from 20 to 50 oC

srf	0.05	N/m	318.15	Surface Tension of Binary Mixtures of Ethanol + Ethylene glycol from 20 to 50 oC	
srf	0.05	N/m	313.15	Surface Tension of Binary Mixtures of Ethanol + Ethylene glycol from 20 to 50 oC	
srf	0.05	N/m	318.15	Surface Tensions of Dilute Solutions of Cycloheptanol in Ethylene Glycol	
tcondl	0.25	W/m×K	303.15	An experimental study on thermal conductivity enhancement of DI water-EG based ZnO(CuO)/graphene wrapped carbon nanotubes nanofluids	
tcondl	0.26	W/m×K	323.15	Thermal conductivity enhancement of ethylene glycol and water with graphene nanoplatelets	
tcondl	0.25	W/m×K	293.15	Measurement of the thermal conductivity of SiO2 nanofluids with an optimized transient hot wire method	
tcondl	0.26	W/m×K	313.15	Thermal conductivity enhancement of ethylene glycol and water with graphene nanoplatelets	
tcondl	0.25	W/m×K	303.15	Thermal conductivity enhancement of ethylene glycol and water with graphene nanoplatelets	

tcondl	0.24	W/m×K	298.15	Experimental studies on viscosity, thermal and electrical conductivity of aluminum nitride ethylene glycol (AlN-EG) nanofluids
tcondl	0.27	W/m×K	343.15	Thermal conductivity of dry anatase and rutile nano-powders and ethylene and propylene glycol-based TiO2 nanofluids
tcondl	0.26	W/m×K	323.15	Thermal conductivity of dry anatase and rutile nano-powders and ethylene and propylene glycol-based TiO2 nanofluids
tcondl	0.25	W/m×K	303.15	Thermal conductivity of dry anatase and rutile nano-powders and ethylene and propylene glycol-based TiO2 nanofluids
tcondl	0.24	W/m×K	283.15	Thermal conductivity of dry anatase and rutile nano-powders and ethylene and propylene glycol-based TiO2 nanofluids
tcondl	0.26	W/m×K	343.15	Thermophysical profile of ethylene glycol-based ZnO nanofluids
tcondl	0.25	W/m×K	323.15	Thermophysical profile of ethylene glycol-based ZnO nanofluids
tcondl	0.25	W/m×K	303.15	Thermophysical profile of ethylene glycol-based ZnO nanofluids

tcondl	0.24	W/m×K	283.15	Thermophysical profile of ethylene glycol-based ZnO nanofluids	
tcondl	0.25	W/m×K	298.15	An experimental study on thermal conductivity enhancement of DI water-EG based ZnO(CuO)/graphene wrapped carbon nanotubes nanofluids	
tcondl	0.26	W/m×K	328.30	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols	
tcondl	0.26	W/m×K	308.15	An experimental study on thermal conductivity enhancement of DI water-EG based ZnO(CuO)/graphene wrapped carbon nanotubes nanofluids	
tcondl	0.25	W/m×K	318.30	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols	
tcondl	0.25	W/m×K	308.10	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols	

tcondl	0.25	W/m×K	298.20	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.26	W/m×K	313.15	An experimental study on thermal conductivity enhancement of DI water-EG based ZnO(CuO)/graphene wrapped carbon nanotubes nanofluids
tcondl	0.26	W/m×K	318.15	An experimental study on thermal conductivity enhancement of DI water-EG based ZnO(CuO)/graphene wrapped carbon nanotubes nanofluids
tcondl	0.26	W/m×K	338.30	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.26	W/m×K	323.15	An experimental study on thermal conductivity enhancement of DI water-EG based ZnO(CuO)/graphene wrapped carbon nanotubes nanofluids
tdiff	9.84e-08	m2/s	298.15	Temperature controlled photoacoustic device for thermal diffusivity measurements of liquids and nanofluids

tdiff	9.42e-08	m2/s	338.15	Temperature controlled photoacoustic device for thermal diffusivity measurements of liquids and nanofluids
tdiff	9.49e-08	m2/s	328.15	Temperature controlled photoacoustic device for thermal diffusivity measurements of liquids and nanofluids
tdiff	9.68e-08	m2/s	318.15	Temperature controlled photoacoustic device for thermal diffusivity measurements of liquids and nanofluids
tdiff	9.73e-08	m2/s	308.15	Temperature controlled photoacoustic device for thermal diffusivity measurements of liquids and nanofluids
vols	8.99e-04	m3/kg	295.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.03e-04	m3/kg	301.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	9.03e-04	m3/kg	302.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.04e-04	m3/kg	303.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.04e-04	m3/kg	304.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.05e-04	m3/kg	305.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.06e-04	m3/kg	306.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	9.06e-04	m3/kg	307.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.07e-04	m3/kg	308.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.07e-04	m3/kg	309.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.08e-04	m3/kg	310.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.08e-04	m3/kg	311.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	9.09e-04	m3/kg	312.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.10e-04	m3/kg	313.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.95e-04	m3/kg	288.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.95e-04	m3/kg	288.21	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.99e-04	m3/kg	294.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	8.98e-04	m3/kg	293.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.98e-04	m3/kg	292.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.97e-04	m3/kg	291.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.96e-04	m3/kg	290.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.96e-04	m3/kg	289.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	8.95e-04	m3/kg	288.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.94e-04	m3/kg	286.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.94e-04	m3/kg	285.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.93e-04	m3/kg	284.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.93e-04	m3/kg	283.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	8.92e-04	m3/kg	282.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.91e-04	m3/kg	281.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.91e-04	m3/kg	280.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.90e-04	m3/kg	279.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.90e-04	m3/kg	278.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	8.89e-04	m3/kg	277.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.89e-04	m3/kg	276.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.88e-04	m3/kg	275.14	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.88e-04	m3/kg	274.14	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.95e-04	m3/kg	288.22	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	9.02e-04	m3/kg	300.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.02e-04	m3/kg	299.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.01e-04	m3/kg	298.16	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.00e-04	m3/kg	297.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	9.00e-04	m3/kg	296.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

vols	8.87e-04	m3/kg	273.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture
vols	8.95e-04	m3/kg	287.15	Volumetric Properties of Pressure-Transmitting Fluids up to 350 MPa: Water, Ethanol, Ethylene Glycol, Propylene Glycol, Castor Oil, Silicon Oil, and Some of Their Binary Mixture

Correlations

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)
Coeff. A	2.03109e+01
Coeff. B	-7.24361e+03
Coeff. C	-8.90400e+00
Temperature range (K), min.	370.66
Temperature range (K), max.	623.15

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/T + C*ln(T) + D*T^2
Coeff. A	1.91425e+02
Coeff. B	-1.47686e+04
Coeff. C	-2.59977e+01
Coeff. D	2.06233e-05
Temperature range (K), min.	260.15
Temperature range (K), max.	645.00

Datasets

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
293.15	98.00	0.0211000
293.15	49030.00	0.0267500
293.15	98060.00	0.0334200
293.15	147100.00	0.0411900
293.15	196130.00	0.0503300
293.15	245160.00	0.0604300
312.46	98.00	0.0099250
312.46	98060.00	0.0148200
312.49	49030.00	0.0122400
312.49	147100.00	0.0176400
312.65	245160.00	0.0246900
334.87	98.00	0.0049490
335.00	49030.00	0.0059520
335.30	98060.00	0.0070310
335.35	245160.00	0.0111500
335.43	147100.00	0.0082340
335.45	196130.00	0.0096080
349.24	98.00	0.0035170
349.50	49030.00	0.0041570
349.65	98060.00	0.0048900
349.67	147100.00	0.0056880
349.80	196130.00	0.0065410
349.91	245160.00	0.0074540
365.70	98.00	0.0023900
366.10	49030.00	0.0028160
366.15	98060.00	0.0033020
366.37	147100.00	0.0038120
366.48	196130.00	0.0043440
366.80	245160.00	0.0048890
380.15	98060.00	0.0025580
380.82	98.00	0.0018720
381.00	49030.00	0.0022070
381.20	196130.00	0.0033450
381.27	147100.00	0.0029320
381.30	245160.00	0.0037840

395.55	98.00	0.0014190
395.60	49030.00	0.0016730
395.61	98060.00	0.0019360
395.65	147100.00	0.0022140
395.73	196130.00	0.0025010
395.80	245160.00	0.0028110
421.70	98.00	0.0009600
421.71	49030.00	0.0011740
421.80	98060.00	0.0013450
421.90	147100.00	0.0015210
422.00	196130.00	0.0017160
422.00	245160.00	0.0018980
464.40	98.00	0.0006520
464.47	98060.00	0.0009700
464.53	196130.00	0.0012030
464.53	245160.00	0.0013560
464.54	147100.00	0.0011100
464.60	49030.00	0.0008770

Reference *https://www.doi.org/10.1016/j.fluid.2011.11.022*

Pressure, kPa	Temperature, K	Viscosity, Pa*s
101.30	308.15	0.0105900

Reference *https://www.doi.org/10.1021/je020178w*

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
283.11	100.00	1120.2
283.11	1000.00	1120.5
283.11	2000.00	1120.9
283.11	5000.00	1122.1
283.11	7000.00	1123.0
283.11	10000.00	1124.3
283.11	12000.00	1125.1
283.11	16000.00	1126.7
283.11	20000.00	1128.2
283.11	25000.00	1130.1
283.11	30000.00	1132.0

283.11	35000.00	1133.9
283.11	40000.00	1135.7
283.11	45000.00	1137.5
283.11	50000.00	1139.3
283.11	55000.00	1141.0
283.11	60000.00	1142.9
283.11	65000.00	1144.5
283.11	70000.00	1146.1
283.11	75000.00	1147.8
283.11	80000.00	1149.4
283.11	85000.00	1151.1
283.11	90000.00	1152.6
283.11	95000.00	1154.2
293.13	100.00	1113.0
293.13	1000.00	1113.4
293.13	2000.00	1113.9
293.13	5000.00	1115.1
293.13	7000.00	1116.0
293.13	10000.00	1117.2
293.13	12000.00	1118.0
293.13	16000.00	1119.8
293.13	20000.00	1121.3
293.13	25000.00	1123.3
293.13	30000.00	1125.3
293.13	35000.00	1127.1
293.13	40000.00	1129.0
293.13	45000.00	1130.7
293.13	50000.00	1132.7
293.13	55000.00	1134.5
293.13	60000.00	1136.3
293.13	65000.00	1138.0
293.13	70000.00	1139.7
293.13	75000.00	1141.3
293.13	80000.00	1143.1
293.13	85000.00	1144.6
293.13	90000.00	1146.3
293.13	95000.00	1147.8
303.13	100.00	1106.0
303.13	1000.00	1106.4
303.13	2000.00	1106.8
303.13	5000.00	1108.2
303.13	7000.00	1109.2
303.13	10000.00	1110.4
303.13	12000.00	1111.2

303.13	16000.00	1112.9
303.13	20000.00	1114.6
303.13	25000.00	1116.6
303.13	30000.00	1118.6
303.13	35000.00	1120.7
303.13	40000.00	1122.6
303.13	45000.00	1124.5
303.13	50000.00	1126.2
303.13	55000.00	1128.0
303.13	60000.00	1129.8
303.13	65000.00	1131.7
303.13	70000.00	1133.4
303.13	75000.00	1135.2
303.13	80000.00	1136.9
303.13	85000.00	1138.4
303.13	90000.00	1140.1
303.13	95000.00	1141.7
313.16	100.00	1099.1
313.16	1000.00	1099.4
313.16	2000.00	1099.8
313.16	5000.00	1101.2
313.16	7000.00	1102.1
313.16	10000.00	1103.5
313.16	12000.00	1104.2
313.16	16000.00	1106.1
313.16	20000.00	1107.8
313.16	25000.00	1109.8
313.16	30000.00	1111.8
313.16	35000.00	1113.8
313.16	40000.00	1115.9
313.16	45000.00	1117.9
313.16	50000.00	1119.8
313.16	55000.00	1121.5
313.16	60000.00	1123.4
313.16	65000.00	1125.2
313.16	70000.00	1127.0
313.16	75000.00	1128.8
313.16	80000.00	1130.6
313.16	85000.00	1132.3
313.16	90000.00	1133.9
313.16	95000.00	1135.5
323.15	100.00	1092.0
323.15	1000.00	1092.3
323.15	2000.00	1092.9

323.15	5000.00	1094.2
323.15	7000.00	1095.2
323.15	10000.00	1096.5
323.15	12000.00	1097.4
323.15	16000.00	1099.3
323.15	20000.00	1100.9
323.15	25000.00	1103.1
323.15	30000.00	1105.2
323.15	35000.00	1107.3
323.15	40000.00	1109.3
323.15	45000.00	1111.3
323.15	50000.00	1113.3
323.15	55000.00	1115.1
323.15	60000.00	1117.1
323.15	65000.00	1119.1
323.15	70000.00	1120.9
323.15	75000.00	1122.7
323.15	80000.00	1124.4
323.15	85000.00	1126.2
323.15	90000.00	1127.8
323.15	95000.00	1129.5
333.18	100.00	1084.7
333.18	1000.00	1085.1
333.18	2000.00	1085.6
333.18	5000.00	1087.1
333.18	7000.00	1088.0
333.18	10000.00	1089.5
333.18	12000.00	1090.4
333.18	16000.00	1092.2
333.18	20000.00	1094.0
333.18	25000.00	1096.3
333.18	30000.00	1098.4
333.18	35000.00	1100.4
333.18	40000.00	1102.6
333.18	45000.00	1104.5
333.18	50000.00	1106.4
333.18	55000.00	1108.5
333.18	60000.00	1110.6
333.18	65000.00	1112.5
333.18	70000.00	1114.3
333.18	75000.00	1116.2
333.18	80000.00	1118.0
333.18	85000.00	1119.7
333.18	90000.00	1121.5

333.18	95000.00	1123.1
343.16	100.00	1077.3
343.16	1000.00	1077.8
343.16	2000.00	1078.3
343.16	5000.00	1080.0
343.16	7000.00	1080.9
343.16	10000.00	1082.3
343.16	12000.00	1083.1
343.16	16000.00	1085.1
343.16	20000.00	1086.9
343.16	25000.00	1089.3
343.16	30000.00	1091.5
343.16	35000.00	1093.7
343.16	40000.00	1095.8
343.16	45000.00	1097.8
343.16	50000.00	1100.0
343.16	55000.00	1102.0
343.16	60000.00	1104.0
343.16	65000.00	1106.1
343.16	70000.00	1108.0
343.16	75000.00	1109.8
343.16	80000.00	1111.7
343.16	85000.00	1113.5
343.16	90000.00	1115.3
343.16	95000.00	1117.0
353.18	100.00	1069.9
353.18	1000.00	1070.5
353.18	2000.00	1071.0
353.18	5000.00	1072.5
353.18	7000.00	1073.5
353.18	10000.00	1075.0
353.18	12000.00	1076.0
353.18	16000.00	1078.0
353.18	20000.00	1079.9
353.18	25000.00	1082.2
353.18	30000.00	1084.5
353.18	35000.00	1086.8
353.18	40000.00	1089.0
353.18	45000.00	1091.0
353.18	50000.00	1093.2
353.18	55000.00	1095.4
353.18	60000.00	1097.4
353.18	65000.00	1099.4
353.18	70000.00	1101.3

353.18	75000.00	1103.2
353.18	80000.00	1105.2
353.18	85000.00	1106.9
353.18	90000.00	1108.8
353.18	95000.00	1110.6
363.18	100.00	1062.4
363.18	1000.00	1062.8
363.18	2000.00	1063.4
363.18	5000.00	1065.0
363.18	7000.00	1066.0
363.18	10000.00	1067.6
363.18	12000.00	1068.6
363.18	16000.00	1070.6
363.18	20000.00	1072.5
363.18	25000.00	1075.0
363.18	30000.00	1077.4
363.18	35000.00	1079.6
363.18	40000.00	1082.0
363.18	45000.00	1084.2
363.18	50000.00	1086.2
363.18	55000.00	1088.4
363.18	60000.00	1090.5
363.18	65000.00	1092.6
363.18	70000.00	1094.5
363.18	75000.00	1096.6
363.18	80000.00	1098.5
363.18	85000.00	1100.4
363.18	90000.00	1102.3
363.18	95000.00	1104.1

Reference *https://www.doi.org/10.1016/j.fluid.2017.01.003*

Pressure, kPa	Temperature, K	Mass density, kg/m3
100.00	298.15	1112.1

Reference *https://www.doi.org/10.1016/j.fluid.2017.05.024*

Temperature, K	Pressure, kPa	Mass density, kg/m3
278.15	100.00	1122.4
278.15	1000.00	1122.6
278.15	5000.00	1124.1
278.15	10000.00	1126.0

278.15	15000.00	1127.8
278.15	20000.00	1129.6
278.15	25000.00	1131.4
278.15	30000.00	1133.1
278.15	35000.00	1134.8
278.15	40000.00	1136.6
278.15	45000.00	1138.2
278.15	50000.00	1139.9
278.15	55000.00	1141.6
278.15	60000.00	1143.3
288.15	100.00	1115.8
288.15	1000.00	1116.0
288.15	5000.00	1117.6
288.15	10000.00	1119.5
288.15	15000.00	1121.5
288.15	20000.00	1123.3
288.15	25000.00	1125.2
288.15	30000.00	1127.0
288.15	35000.00	1128.8
288.15	40000.00	1130.6
288.15	45000.00	1132.3
288.15	50000.00	1134.1
288.15	55000.00	1135.7
288.15	60000.00	1137.4
298.15	100.00	1109.0
298.15	1000.00	1109.2
298.15	5000.00	1110.9
298.15	10000.00	1112.9
298.15	15000.00	1114.9
298.15	20000.00	1116.8
298.15	25000.00	1118.7
298.15	30000.00	1120.6
298.15	35000.00	1122.4
298.15	40000.00	1124.3
298.15	45000.00	1126.1
298.15	50000.00	1127.8
298.15	55000.00	1129.6
298.15	60000.00	1131.3
308.15	100.00	1102.2
308.15	1000.00	1102.4
308.15	5000.00	1104.1
308.15	10000.00	1106.1
308.15	15000.00	1108.2
308.15	20000.00	1110.1

308.15	25000.00	1112.1
308.15	30000.00	1114.0
308.15	35000.00	1115.9
308.15	40000.00	1117.7
308.15	45000.00	1119.6
308.15	50000.00	1121.4
308.15	55000.00	1123.2
308.15	60000.00	1125.0
318.15	100.00	1095.2
318.15	1000.00	1095.4
318.15	5000.00	1097.1
318.15	10000.00	1099.2
318.15	15000.00	1101.3
318.15	20000.00	1103.3
318.15	25000.00	1105.3
318.15	30000.00	1107.3
318.15	35000.00	1109.3
318.15	40000.00	1111.2
318.15	45000.00	1113.1
318.15	50000.00	1115.0
318.15	55000.00	1116.8
318.15	60000.00	1118.6
328.15	100.00	1088.2
328.15	1000.00	1088.3
328.15	5000.00	1090.2
328.15	10000.00	1092.3
328.15	15000.00	1094.4
328.15	20000.00	1096.5
328.15	25000.00	1098.6
328.15	30000.00	1100.6
328.15	35000.00	1102.6
328.15	40000.00	1104.6
328.15	45000.00	1106.5
328.15	50000.00	1108.4
328.15	55000.00	1110.3
328.15	60000.00	1112.1
338.15	100.00	1080.9
338.15	1000.00	1081.2
338.15	5000.00	1083.1
338.15	10000.00	1085.4
338.15	15000.00	1087.6
338.15	20000.00	1089.8
338.15	25000.00	1091.9
338.15	30000.00	1094.0

338.15	35000.00	1096.0
338.15	40000.00	1097.9
338.15	45000.00	1099.9
338.15	50000.00	1101.9
338.15	55000.00	1103.9
338.15	60000.00	1105.8
348.15	100.00	1073.6
348.15	1000.00	1073.9
348.15	5000.00	1075.8
348.15	10000.00	1078.1
348.15	15000.00	1080.4
348.15	20000.00	1082.7
348.15	25000.00	1084.9
348.15	30000.00	1087.0
348.15	35000.00	1089.2
348.15	40000.00	1091.3
348.15	45000.00	1093.4
348.15	50000.00	1095.3
348.15	55000.00	1097.3
348.15	60000.00	1099.4
358.15	100.00	1066.1
358.15	1000.00	1066.2
358.15	5000.00	1068.2
358.15	10000.00	1070.7
358.15	15000.00	1073.1
358.15	20000.00	1075.4
358.15	25000.00	1077.8
358.15	30000.00	1079.9
358.15	35000.00	1082.1
358.15	40000.00	1084.3
358.15	45000.00	1086.5
358.15	50000.00	1088.6
358.15	55000.00	1090.7
358.15	60000.00	1092.7

Reference *https://www.doi.org/10.1016/j.jct.2012.08.014*

Temperature, K	Pressure, kPa	Mass density, kg/m3
293.15	101.13	1105.0

Reference *https://www.doi.org/10.1021/acs.jced.9b00134*

Speed of sound, m/s

Temperature, K - Liquid	Pressure, kPa - Liquid	Speed of sound, m/s - Liquid
273.15	99.00	1713.847
273.15	5204.00	1727.491
273.15	10344.00	1740.939
273.15	15152.00	1753.194
273.15	20194.00	1765.939
273.15	25132.00	1778.134
273.15	30171.00	1789.896
293.15	99.00	1665.836
293.15	5051.00	1679.764
293.15	10070.00	1693.534
293.15	15176.00	1707.192
293.15	20158.00	1720.201
293.15	25108.00	1732.878
293.15	30024.00	1745.294
313.15	100.00	1618.547
313.15	5031.00	1633.093
313.15	10028.00	1647.339
313.15	15117.00	1661.696
313.15	20088.00	1675.281
313.15	25102.00	1688.742
313.15	29983.00	1701.571
333.15	99.00	1570.742
333.15	5054.00	1586.116
333.15	10048.00	1601.104
333.15	15067.00	1615.849
333.15	20106.00	1630.289
333.15	25103.00	1644.305
333.15	29958.00	1657.658
353.15	100.00	1521.783
353.15	5079.00	1538.084
353.15	10048.00	1553.832
353.15	15054.00	1569.282
353.15	20071.00	1584.393
353.15	25078.00	1599.138
353.15	29995.00	1613.263

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Liquid-Liquid Equilibria for Monoethylene Glycol + Hexane and 2,2,4-Trimethylpentane, Water + Hexane and 2,2,4-Trimethylpentane, Monoethylene Glycol + Water + Hexane, and Monoethylene Glycol + Water + 2,2,4-Trimethylpentane in the Temperature Range between T = 283.15 K and T = 323.15 K:

https://www.doi.org/10.1021/je900295u

Legend

affp:	Proton affinity
aigt:	Autoignition Temperature
basg:	Gas basicity
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
econd:	Electrical conductivity
fll:	Lower Flammability Limit
fpc:	Flash Point (Closed Cup Method)
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sg:	Molar entropy at standard conditions
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
tb:	Normal Boiling Point Temperature

tc:	Critical Temperature
tcondl:	Liquid thermal conductivity
tdiff:	Thermal diffusivity
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
vols:	Specific Volume
zra:	Rackett Parameter