## 1,4-Butanediol

Other names: 1,4-BD

1,4-BUTYLENE GLYCOL

1,4-Dihydroxybutane

1,4-Tetramethylene glycol

**BDO** 

Butane diol-1,4 Butane-1,4-diol Butanediol

Butylene glycol Dabco BDO Diol 14B NSC 406696

SUCOL B

TETRAMETHYLENE GLYCOL

Tetramethylene 1,4-diol

**Inchi:** InChl=1S/C4H10O2/c5-3-1-2-4-6/h5-6H,1-4H2

InchiKey: WERYXYBDKMZEQL-UHFFFAOYSA-N

 Formula:
 C4H10O2

 SMILES:
 OCCCCO

 Mol. weight [g/mol]:
 90.12

 CAS:
 110-63-4

### **Physical Properties**

Property code	Value	Unit	Source
affp	871.70	kJ/mol	NIST Webbook
affp	$884.30 \pm 0.50$	kJ/mol	NIST Webbook
affp	915.60	kJ/mol	NIST Webbook
affp	875.00	kJ/mol	NIST Webbook
basg	854.90	kJ/mol	NIST Webbook
basg	852.90 ± 0.50	kJ/mol	NIST Webbook
basg	843.50	kJ/mol	NIST Webbook
basg	841.20	kJ/mol	NIST Webbook
chl	-2495.50 ± 5.70	kJ/mol	NIST Webbook
chl	-2499.90 ± 2.00	kJ/mol	NIST Webbook

gf         -290.84         kJ/mol         Joback Method           hf         -426.00 ± 5.70         kJ/mol         NIST Webbook           hf         -427.00 ± 3.00         kJ/mol         NIST Webbook           hfl         -503.00 ± 2.00         kJ/mol         NIST Webbook           hfl         -505.30 ± 5.70         kJ/mol         NIST Webbook           hfus         14.29         kJ/mol         Joback Method           hvap         57.86         kJ/mol         Joback Method           log10ws         -0.02         Crippen Method           logp         -0.249         Crippen Method           mcvol         78.960         ml/mol         McGowan Method           nfpaf         %Id(float64=1)         KDB           nfpah         %Id(float64=1)         KDB           pc         6220.00 ± 150.00         kPa         NIST Webbook           rinpol         900.00         NIST Webbook           rinpol         912.40         NIST Webbook           rinpol         900.00         NIST Webbook	cpl	203.79	J/mol×K	Molar heat capacities for {isomer of butanediol + methanol} as function of mixture composition and temperature
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	gf	-290.84	kJ/mol	Joback Method
hfl         -503.00 ± 2.00         kJ/mol         NIST Webbook           hfl         -505.30 ± 5.70         kJ/mol         NIST Webbook           hfus         14.29         kJ/mol         Joback Method           hvap         57.86         kJ/mol         Joback Method           log10ws         -0.02         Crippen Method           logp         -0.249         Crippen Method           mcvol         78.960         ml/mol         McGowan Method           nfpaf         %!d(float64=1)         KDB           nfpah         %!d(float64=1)         KDB           pc         6220.00 ± 150.00         kPa         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         912.40         NIST Webbook		-426.00 ± 5.70	kJ/mol	NIST Webbook
hfl         -505.30 ± 5.70         kJ/mol         NIST Webbook           hfus         14.29         kJ/mol         Joback Method           hvap         57.86         kJ/mol         Joback Method           log10ws         -0.02         Crippen Method           logp         -0.249         Crippen Method           mcvol         78.960         ml/mol         McGowan Method           nfpaf         %!d(float64=1)         KDB           nfpah         %!d(float64=1)         KDB           pc         6220.00 ± 150.00         kPa         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         912.40         NIST Webbook	hf	-427.00 ± 3.00	kJ/mol	NIST Webbook
hfus         14.29         kJ/mol         Joback Method           hvap         57.86         kJ/mol         Joback Method           log10ws         -0.02         Crippen Method           logp         -0.249         Crippen Method           mcvol         78.960         ml/mol         McGowan Method           nfpaf         %!d(float64=1)         KDB           nfpah         %!d(float64=1)         KDB           pc         6220.00 ± 150.00         kPa         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         900.00         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         912.40         NIST Webbook	hfl	-503.00 ± 2.00	kJ/mol	NIST Webbook
hvap         57.86         kJ/mol         Joback Method           log10ws         -0.02         Crippen Method           logp         -0.249         Crippen Method           mcvol         78.960         ml/mol         McGowan Method           nfpaf         %!d(float64=1)         KDB           nfpah         %!d(float64=1)         KDB           pc         6220.00 ± 150.00         kPa         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         900.00         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         912.40         NIST Webbook	hfl	-505.30 ± 5.70	kJ/mol	NIST Webbook
log10ws         -0.02         Crippen Method           logp         -0.249         Crippen Method           mcvol         78.960         ml/mol         McGowan Method           nfpaf         %!d(float64=1)         KDB           nfpah         %!d(float64=1)         KDB           pc         6220.00 ± 150.00         kPa         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         900.00         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         912.40         NIST Webbook	hfus	14.29	kJ/mol	Joback Method
logp         -0.249         Crippen Method           mcvol         78.960         ml/mol         McGowan Method           nfpaf         %!d(float64=1)         KDB           nfpah         %!d(float64=1)         KDB           pc         6220.00 ± 150.00         kPa         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         900.00         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         912.40         NIST Webbook	hvap	57.86	kJ/mol	Joback Method
mcvol         78.960         ml/mol         McGowan Method           nfpaf         %!d(float64=1)         KDB           nfpah         %!d(float64=1)         KDB           pc         6220.00 ± 150.00         kPa         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         900.00         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         912.40         NIST Webbook	log10ws	-0.02		Crippen Method
nfpaf         %!d(float64=1)         KDB           nfpah         %!d(float64=1)         KDB           pc         6220.00 ± 150.00         kPa         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         912.40         NIST Webbook	logp	-0.249		Crippen Method
nfpah         %!d(float64=1)         KDB           pc         6220.00 ± 150.00         kPa         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         900.00         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         912.40         NIST Webbook	mcvol	78.960	ml/mol	McGowan Method
pc         6220.00 ± 150.00         kPa         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         900.00         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         912.40         NIST Webbook	nfpaf	%!d(float64=1)		KDB
rinpol         922.00         NIST Webbook           rinpol         900.00         NIST Webbook           rinpol         922.00         NIST Webbook           rinpol         912.40         NIST Webbook	nfpah	%!d(float64=1)		KDB
rinpol 900.00 NIST Webbook rinpol 922.00 NIST Webbook rinpol 912.40 NIST Webbook	рс	6220.00 ± 150.00	kPa	NIST Webbook
rinpol 922.00 NIST Webbook rinpol 912.40 NIST Webbook	rinpol	922.00		NIST Webbook
rinpol 912.40 NIST Webbook	rinpol	900.00		NIST Webbook
	rinpol	922.00		NIST Webbook
rinpol 900.00 NIST Webbook	·	912.40		NIST Webbook
·	rinpol	900.00		NIST Webbook
rinpol 912.40 NIST Webbook	rinpol	912.40		NIST Webbook
rinpol 931.00 NIST Webbook	rinpol	931.00		NIST Webbook
ripol 1870.00 NIST Webbook	ripol	1870.00		NIST Webbook
ripol 1911.00 NIST Webbook	ripol	1911.00		NIST Webbook
ripol 1861.00 NIST Webbook	ripol	1861.00		NIST Webbook
ripol 1890.00 NIST Webbook	ripol	1890.00		NIST Webbook
ripol 1911.00 NIST Webbook	ripol	1911.00		NIST Webbook
sl 223.40 J/mol×K NIST Webbook	sl	223.40	J/mol×K	NIST Webbook
tb 502.88 ± 0.05 K NIST Webbook	tb	502.88 ± 0.05	K	NIST Webbook
tb 501.15 K Isobaric Vapor-Liquid Equilibrium for Binary System of Tetrahydrofuran + 1,4-Butanediol and gamma-Butyrolactone at 50.0 and 70.0 kPa	tb	501.15	K	Equilibrium for Binary System of Tetrahydrofuran + 1,4-Butanediol and gamma-Butyrolactone at
tb 503.15 ± 2.00 K NIST Webbook	tb	503.15 ± 2.00	K	NIST Webbook
tb 501.15 ± 1.00 K NIST Webbook	tb	501.15 ± 1.00	K	NIST Webbook
tb 501.05 K Isobaric Vapor Liquid Equilibrium for Two Binary Systems (n-Butanol + 1,4-Butanediol and .gammaButyrolactone + 1,4-Butanediol) at p = (30.0, 50.0, and 70.0) kPa	tb	501.05	K	Equilibrium for Two Binary Systems (n-Butanol + 1,4-Butanediol and .gammaButyrolactone + 1,4-Butanediol) at p =
tb 501.15 ± 2.00 K NIST Webbook	tb	501.15 ± 2.00	K	NIST Webbook
tb 503.20 K NIST Webbook	tb	503.20	K	NIST Webbook

tc	727.00 ± 3.00	K	NIST Webbook
tc	728.00	К	Critical temperatures and pressures of straight-chain alkanediols (C3 to C12)
tf	289.40 ± 1.20	K	NIST Webbook
tf	294.05 ± 0.60	K	NIST Webbook
tf	355.40 ± 1.00	K	NIST Webbook
tf	292.80 ± 0.50	K	NIST Webbook
tf	289.90 ± 3.00	K	NIST Webbook
tf	292.15 ± 2.00	K	NIST Webbook
tf	292.40 ± 0.70	K	NIST Webbook
tt	293.38 ± 0.10	K	NIST Webbook
tt	293.58 ± 0.02	K	NIST Webbook
tt	289.90 ± 0.10	K	NIST Webbook
tt	293.58 ± 0.05	K	NIST Webbook
VC	0.297	m3/kmol	Joback Method

# **Temperature Dependent Properties**

Property code	Value	Unit	Temperature [K	[] Source	
cpg	202.87	J/mol×K	607.39	Joback Method	
cpg	208.17	J/mol×K	633.81	Joback Method	
cpg	197.36	J/mol×K	580.97	Joback Method	
cpg	191.63	J/mol×K	554.54	Joback Method	
cpg	185.68	J/mol×K	528.12	Joback Method	
cpg	179.49	J/mol×K	501.70	Joback Method	
cpg	173.07	J/mol×K	475.28	Joback Method	
cpl	230.33	J/mol×K	342.65 alp	Heat Capacities of Some Liquid cha,omega-Alkanedi within the Temperature Range between (293.15 and 353.15) K	ols
cpl	229.34	J/mol×K	341.15 alp	Heat Capacities of Some Liquid cha,omega-Alkanedi within the Temperature Range between (293.15 and 353.15) K	ols

срІ	231.32	J/mol×K	344.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	232.32	J/mol×K	345.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	233.32	J/mol×K	347.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	234.32	J/mol×K	348.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	235.34	J/mol×K	350.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
срІ	203.82	J/mol×K	299.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	236.35	J/mol×K	351.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	228.36	J/mol×K	339.65	Heat Capacities
				of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	227.38	J/mol×K	338.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	226.41	J/mol×K	336.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	225.45	J/mol×K	335.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	224.49	J/mol×K	333.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	223.53	J/mol×K	332.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	222.58	J/mol×K	330.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	221.64	J/mol×K	329.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	220.70	J/mol×K	327.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	219.76	J/mol×K	326.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	218.83	J/mol×K	324.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	217.91	J/mol×K	323.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	216.99	J/mol×K	321.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
срІ	216.08	J/mol×K	320.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	215.17	J/mol×K	318.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K  Heat Capacities
				of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	213.36	J/mol×K	315.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	212.47	J/mol×K	314.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	211.58	J/mol×K	312.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	210.70	J/mol×K	311.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	209.82	J/mol×K	309.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	208.95	J/mol×K	308.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	214.55	J/mol <b>×</b> K	318.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	208.08	J/mol×K	306.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	207.22	J/mol <b>×</b> K	305.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	206.36	J/mol×K	303.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	205.51	J/mol×K	302.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	204.67	J/mol×K	300.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	178.00	J/mol×K	297.79	NIST Webbook

cpl	200.39	J/mol×K	293.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	203.06	J/mol×K	298.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	205.82	J/mol×K	303.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	208.65	J/mol×K	308.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	211.57	J/mol×K	313.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	203.27	J/mol×K	298.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

cpl	217.61	J/mol×K	323.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	220.72	J/mol×K	328.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	223.90	J/mol×K	333.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	227.12	J/mol×K	338.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	230.40	J/mol×K	343.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	233.72	J/mol×K	348.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature

cpl	237.07	J/mol×K	353.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	200.51	J/mol×K	293.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	201.33	J/mol×K	294.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
срІ	202.16	J/mol×K	296.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	202.99	J/mol×K	297.65	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K
cpl	200.10	J/mol×K	298.15	NIST Webbook
cpl	237.38	J/mol×K	353.15	Heat Capacities of Some Liquid alpha,omega-Alkanediols within the Temperature Range between (293.15 and 353.15) K

dvisc	0.0727454	Paxs	298.15	Molecular interactions in binary mixtures of formamide with 1-butanol, 2-butanol, 1,3-butanediol and 1,4-butanediol at different temperatures: An ultrasonic and viscometric study	
dvisc	0.0568860	Paxs	303.15	Molecular interactions in binary mixtures of formamide with 1-butanol, 2-butanol, 1,3-butanediol and 1,4-butanediol at different temperatures: An ultrasonic and viscometric study	
dvisc	0.0448850	Paxs	308.15	Molecular interactions in binary mixtures of formamide with 1-butanol, 2-butanol, 1,3-butanediol and 1,4-butanediol at different temperatures: An ultrasonic and viscometric study	
dvisc	0.0358106	Paxs	313.15	Molecular interactions in binary mixtures of formamide with 1-butanol, 2-butanol, 1,3-butanediol and 1,4-butanediol at different temperatures: An ultrasonic and viscometric study	
dvisc	0.0290542	Paxs	318.15	Molecular interactions in binary mixtures of formamide with 1-butanol, 2-butanol, 1,3-butanediol and 1,4-butanediol at different temperatures: An ultrasonic and viscometric study	

dvisc	0.0972620	Paxs	293.15 Molecular interactions in binary mixtures of formamide with 1-butanol, 2-butanol, 1,3-butanediol and 1,4-butanediol at different temperatures: An ultrasonic and viscometric study
hfust	18.70	kJ/mol	293.60 NIST Webbook
hfust	18.70	kJ/mol	293.60 NIST Webbook
hfust	18.70	kJ/mol	293.58 NIST Webbook
hvapt	77.10	kJ/mol	298.15 Vaporization Enthalpies of the r,o-Alkanediols by Correlation Gas Chromatography
hvapt	72.00	kJ/mol	445.00 NIST Webbook
hvapt	77.00 ± 2.00	kJ/mol	419.00 NIST Webbook
pvap	0.04	kPa	341.20 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.06	kPa	346.30 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method

pvap	0.05	kPa	343.60 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.05	kPa	343.60 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.05	kPa	343.20 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.07	kPa	348.20 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.04	kPa	339.60 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method

pvap	0.04	kPa	339.60 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.03	kPa	338.20 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.02	kPa	335.20 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.07	kPa	348.60 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method

pvap	0.01	kPa	329.20 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.07	kPa	348.60 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.08	kPa	351.20 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.10	kPa	353.20 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.10	kPa	353.60 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method

pvap	0.10	kPa	353.60 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.12	kPa	356.20 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.14	kPa	358.60 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.14	kPa	358.60 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method

pvap	0.17	kPa	361.20 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.19	kPa	363.20 Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
pvap	0.66	kPa	383.15  Vapor-Liquid Equilibria on Seven Binary Systems: Ethylene Oxide + 2-Methylpropane; Acetophenone + Phenol; cis-1,3-Dichloropropene + 1,2-Dichloropropane; 1,5-Hexadiene + Allyl Chloride; Isopropyl Acetate + Acetonitrile; Vinyl Chloride + Methyl Chloride; and 1,4-Butanediol + c-Butyrolactone
pvap	0.14	kPa	358.30 Thermodynamic Properties of Mixtures Containing lonic Liquids. Activity Coefficients of Ethers and Alcohols in 1-Methyl-3-Ethyl-Imidazolium Bis(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method

pvap	0.02	kPa		Thermodynamic Properties of Mixtures Containing Ionic Liquids. Activity Coefficients of Ethers and Alcohols in Iethyl-3-Ethyl-Imidazolium s(trifluoromethyl-sulfonyl) Imide Using the Transpiration Method
rfi	1.43520		318.15	Refractive Indices and Deviations in Refractive Indices for Binary Mixtures of Formamide + 1-Butanol, + 2-Butanol, + 1,3-Butanediol, and + 1,4-Butanediol at Temperatures from (293.15 to 318.15) K
rfi	1.44470		298.15	The effect of temperature and pressure on acoustic and thermodynamic properties of 1,4-butanediol. The comparison with 1,2- and 1,3-butanediols
rfi	1.44570		298.20	A thermodynamic study of solute solvent interactions through dielectric properties of the mixtures consisting of 1,4-butanediol, 1-octanol, and 1,4-dioxane at different temperatures
rfi	1.44220		308.20	A thermodynamic study of solute solvent interactions through dielectric properties of the mixtures consisting of 1,4-butanediol, 1-octanol, and 1,4-dioxane at different temperatures

rfi	1.44170	308.20	A thermodynamic study of solute solvent interactions through dielectric properties of the mixtures consisting of 1,4-butanediol, 1-octanol, and 1,4-dioxane at different temperatures	
rfi	1.43860	318.20	A thermodynamic study of solute solvent interactions through dielectric properties of the mixtures consisting of 1,4-butanediol, 1-octanol, and 1,4-dioxane at different temperatures	
rfi	1.44420	298.15	Densities, Dynamic Viscosities, Speeds of Sound, and Relative Permittivities for Water + Alkanediols (Propane-1,2- and -1,3-diol and Butane-1,2-, -1,3-, -1,4-, and -2,3-Diol) at Different Temperatures	
rfi	1.44510	293.15	Refractive Indices and Deviations in Refractive Indices for Binary Mixtures of Formamide + 1-Butanol, + 2-Butanol, + 1,3-Butanediol, and + 1,4-Butanediol at Temperatures from (293.15 to 318.15) K	

rfi	1.44310	298.15	Refractive Indices and Deviations in Refractive Indices for Binary Mixtures of Formamide + 1-Butanol, + 2-Butanol, + 1,3-Butanediol, and + 1,4-Butanediol at Temperatures from (293.15 to 318.15) K	
rfi	1.44110	303.15	Refractive Indices and Deviations in Refractive Indices for Binary Mixtures of Formamide + 1-Butanol, + 2-Butanol, + 1,3-Butanediol, and + 1,4-Butanediol at Temperatures from (293.15 to 318.15) K	
rfi	1.43910	308.15	Refractive Indices and Deviations in Refractive Indices for Binary Mixtures of Formamide + 1-Butanol, + 2-Butanol, + 1,3-Butanediol, and + 1,4-Butanediol at Temperatures from (293.15 to 318.15) K	
rfi	1.43720	313.15	Refractive Indices and Deviations in Refractive Indices for Binary Mixtures of Formamide + 1-Butanol, + 2-Butanol, + 1,3-Butanediol, and + 1,4-Butanediol at Temperatures from (293.15 to 318.15) K	

rhol	1009.60	kg/m3	303.15	Densities, Ultrasonic Speeds, and Excess Properties of Binary Mixtures of Diethylene Glycol with 1-Butanol, 2-Butanol, and 1,4-Butanediol at Different Temperatures	
rhol	1012.60	kg/m3	298.15	Densities, Ultrasonic Speeds, and Excess Properties of Binary Mixtures of Diethylene Glycol with 1-Butanol, 2-Butanol, and 1,4-Butanediol at Different Temperatures	
rhol	997.80	kg/m3	323.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K	
rhol	1006.70	kg/m3	308.15	Densities, Ultrasonic Speeds, and Excess Properties of Binary Mixtures of Diethylene Glycol with 1-Butanol, 2-Butanol, and 1,4-Butanediol at Different Temperatures	
rhol	1003.70	kg/m3	313.15	Densities, Ultrasonic Speeds, and Excess Properties of Binary Mixtures of Diethylene Glycol with 1-Butanol, 2-Butanol, and 1,4-Butanediol at Different Temperatures	

rhol	1022.21	kg/m3	283.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	
rhol	1016.11	kg/m3	293.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	
rhol	1013.06	kg/m3	298.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	
rhol	1009.99	kg/m3	303.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	
rhol	1003.85	kg/m3	313.15	Excess volumes and excess heat capacities for alkanediol + water systems in the temperature interval (283.15-313.15) K	
rhol	1003.95	kg/m3	308.15	Effect of placement of hydroxyl groups in isomeric butanediol on the behaviour of thermophysical and spectroscopic properties of pyrrolidin-2-one	

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rhol	1003.95	kg/m3	308.15	A comparative study of thermophysical and spectroscopic properties in mixtures of isomeric butanediol and N,N-dimethylformamide
rhol	1003.95	kg/m3	308.15	Thermodynamic, transport, and spectroscopic studies for mixtures of isomeric butanediol and N-methyl-2-pyrrolidinone
rhol	1003.95	kg/m3	308.15	Effect of B-cyclodextrin on the behaviour of thermophysical and spectroscopic properties of binary mixtures of (isomeric butanediol + pyrrolidin-2-one)
rhol	1013.90	kg/m3	298.15	Investigation on some thermophysical properties of poly(ethylene glycol) binary mixtures at different temperatures
rhol	1010.60	kg/m3	303.15	Investigation on some thermophysical properties of poly(ethylene glycol) binary mixtures at different temperatures
rhol	1007.50	kg/m3	308.15	Investigation on some thermophysical properties of poly(ethylene glycol) binary mixtures at different temperatures

rhol	1012.80	kg/m3	298.15	Acoustic and	
	.0.2.00	g.me	255115	volumetric study of renewable oxygenated fuel additives at (298.15-323.15) K: Isomeric butanediols with ethylbutyrate	
rhol	1009.77	kg/m3	303.15	Acoustic and volumetric study of renewable oxygenated fuel additives at (298.15-323.15) K: Isomeric butanediols with ethylbutyrate	
rhol	1006.74	kg/m3	308.15	Acoustic and volumetric study of renewable oxygenated fuel additives at (298.15-323.15) K: Isomeric butanediols with ethylbutyrate	
rhol	1003.70	kg/m3	313.15	Acoustic and volumetric study of renewable oxygenated fuel additives at (298.15-323.15) K: Isomeric butanediols with ethylbutyrate	
rhol	1000.67	kg/m3	318.15	Acoustic and volumetric study of renewable oxygenated fuel additives at (298.15-323.15) K: Isomeric butanediols with ethylbutyrate	
rhol	997.63	kg/m3	323.15	Acoustic and volumetric study of renewable oxygenated fuel additives at (298.15-323.15) K: Isomeric butanediols with ethylbutyrate	

rhol	1012.96	kg/m3	298.15	Isobaric Vapor Liquid Equilibrium for Two Binary Systems, (3-Methyl-1-butanol + 1,4-Butanediol) and (Hexylene Glycol + 1,4-Butanediol), at p = 40.0, 60.0, and 80.0 kPa	
rhol	1015.76	kg/m3	293.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	
rhol	1012.68	kg/m3	298.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	
rhol	1009.54	kg/m3	303.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	
rhol	1006.43	kg/m3	308.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	
rhol	1003.37	kg/m3	313.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	
rhol	1000.45	kg/m3	318.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	

rhol	997.14	kg/m3	323.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	
rhol	994.02	kg/m3	328.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	
rhol	990.93	kg/m3	333.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	
rhol	987.93	kg/m3	338.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	
rhol	984.81	kg/m3	343.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	
rhol	981.70	kg/m3	348.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	
rhol	978.59	kg/m3	353.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	

rhol	972.71	kg/m3	363.15	Excess Molar Volume, Viscosity, and Heat Capacity for the Mixtures of 1,4-Butanediol + Water at Different Temperatures	
rhol	1013.04	kg/m3		Isobaric Vapor-Liquid Equilibrium for Four Binary Systems of Ethane-1,2-diol, Butane-1,4-diol, 2-(2- vdroxyethoxy)ethan-1 and 2-[2-(2- coxyethoxy)ethoxy]eth at 10.0 kPa, 20.0 kPa and 40.0 kPa	
rhol	1016.37	kg/m3	293.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol,	
				1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K	
rhol	1013.04	kg/m3	298.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol,	
				and + Ethane-1,2-diol from (293.15 to 328.15) K	
rhol	1009.96	kg/m3	303.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol	
				+ 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K	

rhol	1006.75	kg/m3	308.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K	
rhol	1003.55	kg/m3	313.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K	
rhol	1000.72	kg/m3	318.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K	
rhol	994.41	kg/m3	328.15	Densities and Excess Molar Volumes for Binary Mixtures of 1,4-Butanediol + 1,2-Propanediol, + 1,3-Propanediol, and + Ethane-1,2-diol from (293.15 to 328.15) K	
sfust	63.72	J/mol×K	293.58	NIST Webbook	

# **Pressure Dependent Properties**

Property code	Value	Unit	Pressure [kPa]	Source
FIUDGILY COUG	value	Ullit	FIC33UIC INFAI	Jouite

K 1.30 NIST Webbook tbrp 393.20

### **Correlations**

Information	Value

Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)
Coeff. A	1.61683e+01
Coeff. B	-4.88254e+03
Coeff. C	-8.04700e+01
Temperature range (K), min.	387.92
Temperature range (K), max.	530.19

Information	Value
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Property code	pvap
Equation	$ln(Pvp) = A + B/T + C*ln(T) + D*T^2$
Coeff. A	5.07189e+01
Coeff. B	-9.72020e+03
Coeff. C	-4.35830e+00
Coeff. D	1.55136e-06
Temperature range (K), min.	293.05
Temperature range (K), max.	667.00

#### Sources

Thermodynamics of phase transfer for polar molecules from alkanes to deep

**Eure**ctic solvents:

70.0) kPa:

Solubility of Etoricoxib in Aqueous Solutions of 1,4-Butanediol, Malbiocents அவர்கள் இருக்கும் Solubility of Etoricoxib in Aqueous

Excess volumes and excess heat capacities for alkanediol + water

Sessitives fire field the fire field that the field that the fire field and is single the drawn of a queous activity coefficients of aqueous some of a queous some of the properties of a queous some of the properties of a queous actudy of the properties of the .gamma.-Butyrolactone + 1,4-Butanediol) at p = (30.0, 50.0, and

https://www.doi.org/10.1016/j.fluid.2017.05.008

https://www.cheric.org/files/research/kdb/mol/mol916.mol

https://www.doi.org/10.1021/acs.jced.5b00201 https://www.doi.org/10.1016/j.jct.2007.04.011

https://www.chemeo.com/doc/models/crippen\_log10ws

https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=916

https://www.doi.org/10.1016/j.fluid.2013.06.041

https://www.doi.org/10.1021/je8008792

https://www.doi.org/10.1021/acs.jced.6b00088

#### **Crippen Method:**

Isobaric Vapor Liquid Equilibrium for Two Binary Systems,
Two Binary Systems,
Pennetrias Ubutaanoi Spendiaanediol)
System Report the college of Binace Mixing the properties of Binace Mixing the properties of Binace Mixing the properties of System of Syst ฟิลิโนฟัชชิดดิติเร่าtion and temperature:

Liquid phase behavior of hexafluorophosphate ionic liquids with Measurement and thermodynamic modeling of ternary (liquid + liquid) Accompanitive state and the meaning of ternary (liquid + liquid) Accompanitive state and the meaning of ternary (liquid + liquid) Accompanitive state and the meaning of ternary (liquid + liquid) Accompanitive state and the meaning of ternary (liquid + liquid) Accompanitive state and the meaning of ternary (liquid + liquid) Accompanitive state and the meaning of ternary (liquid + liquid) Accompanitive state and the meaning of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures of the excess molar volume of ternary mixtures containing scharic varieties of the excess molar volume of ternary mixtures of the excess molar volume of ternary mixtures of the excess molar volume of ternary mixtures of the excess molar volume of terna Liquid phase behavior of for Binary Mixtures of 1,4-Butanediol + The Propagation, 4 กุมระคณธุลาณ https://www.doi.org/10.1016/j.jct.2009.06.006 A thermodynamic study of solute solvent interactions through dielectric befraetive brunes and lesvestions ing of reflective broices for Binary Mixtures of Density and Wixtures of Density and Section of Section

Densities, Dynamic Viscosities, Speeds https://www.doi.org/10.1021/je0340755 Densities, Dynamic Viscosities, Speeds of Sound, and Relative Permittivities investigation in the investigation of excess mixtures of (isomeric butanediol + pyrrolidin-2-one):

Haker26 Math Based Ionic Liquids:

http://pubs.acs.org/doi/abs/10.1021/ci990307l

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https://www.doi.org/10.1021/acs.jced.9b00283

https://en.wikipedia.org/wiki/Joback\_method

### Legend

**affp:** Proton affinity **basg:** Gas basicity

**chl:** Standard liquid enthalpy of combustion

cpg: Ideal gas heat capacitycpl: Liquid phase heat capacity

dvisc: Dynamic viscosity

gf: Standard Gibbs free energy of formationhf: Enthalpy of formation at standard conditions

**hfl:** Liquid phase enthalpy of formation at standard conditions

hfus: Enthalpy of fusion at standard conditions hfust: Enthalpy of fusion at a given temperature

hvap: Enthalpy of vaporization at standard conditions hvapt: Enthalpy of vaporization at a given temperature

log10ws:Log10 of Water solubility in mol/llogp:Octanol/Water partition coefficientmcvol:McGowan's characteristic volume

nfpaf: NFPA Fire Rating
nfpah: NFPA Health Rating
pc: Critical Pressure
pvap: Vapor pressure
rfi: Refractive Index
rhol: Liquid Density

rinpol: Non-polar retention indices ripol: Polar retention indices

**sfust:** Entropy of fusion at a given temperature

sl: Liquid phase molar entropy at standard conditions

tb: Normal Boiling Point Temperaturetbrp: Boiling point at reduced pressure

tc: Critical Temperature

tf: Normal melting (fusion) pointtt: Triple Point Temperature

vc: Critical Volume

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https://www.chemeo.com/cid/29-232-2/1-4-Butanediol.pdf

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