

# Benzene, (trifluoromethyl)-

<b>Other names:</b>	(Trifluoromethyl)benzene .alpha.,.alpha.,.alpha.-trifluorotoluene 1,1,1-TRIFLUOROTOLUENE ALPHA,ALPHA,ALPHA-TRIFLUOROTOLUENE BENZENYL FLUORIDE BENZOTRIFLUORIDE Benzylidyne fluoride Benzyltrifluoride NSC 8038 Phenylfluoroform Toluene, «alpha»,«alpha»,«alpha»-trifluoro- Toluene, Â«alphaÂ»,Â«alphaÂ»,Â«alphaÂ»-trifluoro- Trifluoro(phenyl)methane Trifluoromethylbenzene UN 2338 USAF MA-16 «alpha»,«alpha»,«alpha»-Trifluorotoluene Â«alphaÂ»,Â«alphaÂ»,Â«alphaÂ»-Trifluorotoluene
<b>Inchi:</b>	InChI=1S/C7H5F3/c8-7(9,10)6-4-2-1-3-5-6/h1-5H
<b>InchiKey:</b>	GETTZEONDQJALK-UHFFFAOYSA-N
<b>Formula:</b>	C7H5F3
<b>SMILES:</b>	FC(F)(F)c1ccccc1
<b>Mol. weight [g/mol]:</b>	146.11
<b>CAS:</b>	98-08-8

## Physical Properties

Property code	Value	Unit	Source
chl	-3369.30 ± 0.50	kJ/mol	NIST Webbook
chl	-3390.50	kJ/mol	NIST Webbook
ea	0.00	eV	NIST Webbook
gf	-461.12	kJ/mol	Joback Method
hf	-581.03	kJ/mol	NIST Webbook
hfl	-620.45	kJ/mol	NIST Webbook
hfus	9.75	kJ/mol	Joback Method
hvap	37.10	kJ/mol	NIST Webbook
hvap	37.67	kJ/mol	NIST Webbook
hvap	37.60	kJ/mol	NIST Webbook

ie	9.86	eV	NIST Webbook
ie	9.69 ± 0.00	eV	NIST Webbook
ie	9.69 ± 0.03	eV	NIST Webbook
ie	9.70	eV	NIST Webbook
ie	9.68	eV	NIST Webbook
ie	9.69 ± 0.01	eV	NIST Webbook
ie	9.69 ± 0.01	eV	NIST Webbook
ie	9.68 ± 0.02	eV	NIST Webbook
log10ws	-2.51		Estimated Solubility Method
log10ws	-2.51		Aqueous Solubility Prediction Method
logp	2.705		Crippen Method
mcvol	91.040	ml/mol	McGowan Method
pc	3564.27	kPa	Joback Method
rinpol	700.00		NIST Webbook
rinpol	656.30		NIST Webbook
rinpol	656.40		NIST Webbook
rinpol	696.00		NIST Webbook
sl	271.50	J/molxK	NIST Webbook
tb	374.50 ± 0.50	K	NIST Webbook
tb	375.20	K	NIST Webbook
tb	375.19 ± 0.20	K	NIST Webbook
tb	375.70	K	Phase diagrams of (vapour + liquid) equilibrium for binary mixtures of a,a,a-trifluorotoluene with ethanol, or benzene, or chloroform at pressure 101.4 kPa
tb	375.20 ± 0.40	K	NIST Webbook
tb	375.40 ± 1.00	K	NIST Webbook
tb	376.61	K	KDB
tb	375.00	K	NIST Webbook
tb	375.20	K	NIST Webbook
tc	559.90	K	NIST Webbook
tf	244.78	K	Aqueous Solubility Prediction Method
tf	244.00 ± 0.02	K	NIST Webbook
tt	244.14 ± 0.07	K	NIST Webbook
tt	244.14 ± 0.02	K	NIST Webbook
vc	0.362	m <sup>3</sup> /kmol	Joback Method

# Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	205.09	J/molxK	507.64	Joback Method
cpg	195.99	J/molxK	475.93	Joback Method
cpg	186.19	J/molxK	444.23	Joback Method
cpg	175.67	J/molxK	412.52	Joback Method
cpg	221.37	J/molxK	571.05	Joback Method
cpg	213.54	J/molxK	539.34	Joback Method
cpg	164.39	J/molxK	380.82	Joback Method
cpl	188.45	J/molxK	298.15	NIST Webbook
hfust	11.99	kJ/mol	242.00	NIST Webbook
hfust	13.77	kJ/mol	244.00	NIST Webbook
hfust	13.78	kJ/mol	244.14	NIST Webbook
hsubt	54.40	kJ/mol	227.50	NIST Webbook
hvapt	35.60	kJ/mol	370.50	NIST Webbook
hvapt	38.50	kJ/mol	314.00	NIST Webbook
hvapt	32.63	kJ/mol	375.20	NIST Webbook
hvapt	39.10	kJ/mol	308.00	NIST Webbook
hvapt	32.60 ± 0.10	kJ/mol	375.00	NIST Webbook
hvapt	34.10 ± 0.10	kJ/mol	353.00	NIST Webbook
hvapt	35.40 ± 0.10	kJ/mol	334.00	NIST Webbook
hvapt	32.40	kJ/mol	495.00	NIST Webbook
hvapt	35.70	kJ/mol	370.50	NIST Webbook
hvapt	35.90	kJ/mol	353.50	NIST Webbook
hvapt	31.60	kJ/mol	500.00	NIST Webbook
rfi	1.41320		298.15	Study of Vapor-Liquid Equilibrium for Binary Mixtures (Chloroform + 2,2,2-Trifluoroethanol) and (r,r,r-Trifluorotoluene + 2,2,2-Trifluoroethanol) at Pressure 102 kPa

rho1	1182.18	kg/m3	298.15	Volumetric properties of binary and ternary mixtures of diisopropyl ether, a,a,a-trifluorotoluene, 2,2,2-trifluoroethanol, and ethanol at a temperature 298.15 K and pressure 101 kPa
sfust	56.45	J/molxK	244.14	NIST Webbook

## Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.42129e+01
Coeff. B	-3.14473e+03
Coeff. C	-4.72370e+01
Temperature range (K), min.	244.14
Temperature range (K), max.	400.52

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C \cdot \ln(T) + D \cdot T^2$
Coeff. A	5.19443e+01
Coeff. B	-5.93323e+03
Coeff. C	-5.37094e+00
Coeff. D	2.26368e-06
Temperature range (K), min.	244.14
Temperature range (K), max.	565.00

## Sources

KDB Pure (Korean Thermophysical Properties Databank):  
KDB:

<https://www.thermopedia.com/research/kdb/hcprop/showprop.php?cmpid=1694>

<https://www.thermopedia.com/files/research/kdb/mol/mol1694.mol>

Estimated Solubility Method:

[http://pubs.acs.org/doi/suppl/10.1021/ci034243x/suppl\\_file/ci034243xsi20040112\\_053635.txt](http://pubs.acs.org/doi/suppl/10.1021/ci034243x/suppl_file/ci034243xsi20040112_053635.txt)

Study of Vapor-Liquid Equilibrium for Binary Mixtures (Chloroform + 2,2,2-Trifluoroethanol) and (r,r,r-Trifluorotoluene + 2,2,2-Trifluoroethanol) at Pressure 102 kPa:

<https://www.doi.org/10.1021/je700103k>

<b>Joback Method:</b>	<a href="https://en.wikipedia.org/wiki/Joback_method">https://en.wikipedia.org/wiki/Joback_method</a>
<b>The Yaws Handbook of Vapor Pressure:</b>	<a href="https://www.sciencedirect.com/book/9780128029992/the-yaws-handbook-of-vapor-pressure">https://www.sciencedirect.com/book/9780128029992/the-yaws-handbook-of-vapor-pressure</a>
<b>KDB Vapor Pressure Data:</b>	<a href="https://www.thermo.com/research/kdb/hcprop/showprop.php?cmpid=1694">https://www.thermo.com/research/kdb/hcprop/showprop.php?cmpid=1694</a>
<b>Solubilities and Phase Equilibria for Ternary Solutions of alpha, alpha, alpha-trifluoroethane, Water, and Propan-1-ol at 298.15 K and Pressure of 0.101325 MPa:</b>	<a href="https://www.doi.org/10.1021/je600526x">https://www.doi.org/10.1021/je600526x</a>
<b>Phase Diagrams of (vapour + liquid) equilibrium for binary mixtures of 2,2,2-trifluoroethane, water, and ethanol at a temperature of 298.15 K and pressure of 101.325 kPa:</b>	<a href="https://www.doi.org/10.1016/j.jct.2006.09.006">https://www.doi.org/10.1016/j.jct.2006.09.006</a>
<b>Phase Diagrams of (vapour + liquid) equilibrium for binary mixtures of 2,2,2-trifluoroethane, water, and ethanol at a temperature of 298.15 K and pressure of 101.325 kPa:</b>	<a href="http://link.springer.com/article/10.1007/BF02311772">http://link.springer.com/article/10.1007/BF02311772</a>
<b>Phase Diagrams of (vapour + liquid) equilibrium for binary mixtures of 2,2,2-trifluoroethane, water, and ethanol at a temperature of 298.15 K and pressure of 101.325 kPa:</b>	<a href="https://www.doi.org/10.1016/j.jct.2006.09.004">https://www.doi.org/10.1016/j.jct.2006.09.004</a>
<b>Phase Diagrams of (vapour + liquid) equilibrium for binary mixtures of 2,2,2-trifluoroethane, water, and ethanol at a temperature of 298.15 K and pressure of 101.325 kPa:</b>	<a href="http://pubs.acs.org/doi/abs/10.1021/ci9903071">http://pubs.acs.org/doi/abs/10.1021/ci9903071</a>
<b>Phase Diagrams of (vapour + liquid) equilibrium for binary mixtures of 2,2,2-trifluoroethane, water, and ethanol at a temperature of 298.15 K and pressure of 101.325 kPa:</b>	<a href="https://www.doi.org/10.1016/j.jct.2007.09.002">https://www.doi.org/10.1016/j.jct.2007.09.002</a>
<b>Phase Diagrams of (vapour + liquid) equilibrium for binary mixtures of 2,2,2-trifluoroethane, water, and ethanol at a temperature of 298.15 K and pressure of 101.325 kPa:</b>	<a href="http://webbook.nist.gov/cgi/cbook.cgi?ID=C98088&amp;Units=SI">http://webbook.nist.gov/cgi/cbook.cgi?ID=C98088&amp;Units=SI</a>
<b>Aqueous Solubility Prediction Method:</b>	<a href="http://onschallenge.wikispaces.com/file/view/AqueousDataset002.xlsx/351826032/AqueousDataset002.xlsx">http://onschallenge.wikispaces.com/file/view/AqueousDataset002.xlsx/351826032/AqueousDataset002.xlsx</a>

## Legend

<b>chl:</b>	Standard liquid enthalpy of combustion
<b>cpg:</b>	Ideal gas heat capacity
<b>cpl:</b>	Liquid phase heat capacity
<b>ea:</b>	Electron affinity
<b>gf:</b>	Standard Gibbs free energy of formation
<b>hf:</b>	Enthalpy of formation at standard conditions
<b>hfl:</b>	Liquid phase enthalpy of formation at standard conditions
<b>hfus:</b>	Enthalpy of fusion at standard conditions
<b>hfust:</b>	Enthalpy of fusion at a given temperature
<b>hsubt:</b>	Enthalpy of sublimation at a given temperature
<b>hvap:</b>	Enthalpy of vaporization at standard conditions
<b>hvapt:</b>	Enthalpy of vaporization at a given temperature
<b>ie:</b>	Ionization energy
<b>log10ws:</b>	Log10 of Water solubility in mol/l
<b>logp:</b>	Octanol/Water partition coefficient
<b>mcvol:</b>	McGowan's characteristic volume
<b>pc:</b>	Critical Pressure
<b>pvap:</b>	Vapor pressure
<b>rfi:</b>	Refractive Index
<b>rhoL:</b>	Liquid Density
<b>rinpol:</b>	Non-polar retention indices
<b>sfust:</b>	Entropy of fusion at a given temperature
<b>sl:</b>	Liquid phase molar entropy at standard conditions
<b>tb:</b>	Normal Boiling Point Temperature
<b>tc:</b>	Critical Temperature
<b>tf:</b>	Normal melting (fusion) point
<b>tt:</b>	Triple Point Temperature

**vc:** Critical Volume

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