

# Tetraethylene glycol

<b>Other names:</b>	1,11-Dihydroxy-3,6,9-trioxaundecane 1,11-undecanediol, 3,6,9-trioxa- 2,2'-(Oxybis(ethyleneoxy))diethanol 2-(2-[2-(2-Hydroxyethoxy)ethoxy]ethoxy)ethanol 3,6,9-Trioxaundecan-1,11-diol 3,6,9-Trioxaundecane-1,11-diol 3,6,9-trioxa-1,11-undecanediol Ethanol, 2,2'-(oxybis(ethyleneoxy))di- Ethanol, 2,2'-[oxybis(2,1-ethanediyl)]bis- Hi-Dry NSC 1262 PEG-4 Tetraglycol ethanol, 2,2'-[oxybis(2,1-ethanediyl)]-
<b>Inchi:</b>	InChI=1S/C8H18O5/c9-1-3-11-5-7-13-8-6-12-4-2-10/h9-10H,1-8H2
<b>InchiKey:</b>	UWHCKJMYHZGTIT-UHFFFAOYSA-N
<b>Formula:</b>	C8H18O5
<b>SMILES:</b>	OCCOCCOCOCOCO
<b>Mol. weight [g/mol]:</b>	194.23
<b>CAS:</b>	112-60-7

## Physical Properties

Property code	Value	Unit	Source
chl	-4738.80 ± 4.60	kJ/mol	NIST Webbook
gf	-572.16	kJ/mol	Joback Method
hf	-909.57	kJ/mol	Joback Method
hfl	-981.70 ± 4.60	kJ/mol	NIST Webbook
hfus	28.22	kJ/mol	Joback Method
hvap	73.99	kJ/mol	Joback Method
log10ws	1.04		Crippen Method
logp	-0.979		Crippen Method
mcvol	152.930	ml/mol	McGowan Method
pc	3200.00 ± 100.00	kPa	NIST Webbook
rinpol	1515.40		NIST Webbook
rinpol	1515.40		NIST Webbook
rinpol	1507.00		NIST Webbook
tb	587.20	K	NIST Webbook

tb	601.20	K	NIST Webbook
tc	762.00 ± 20.00	K	NIST Webbook
tc	800.00 ± 30.00	K	NIST Webbook
tc	814.00	K	Critical temperatures and pressures of ethylene glycols
tf	263.75 ± 0.70	K	NIST Webbook
tf	269.05	K	NIST Webbook
vc	0.576	m3/kmol	Joback Method

## Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	457.15	J/mol×K	740.27	Joback Method
cpg	418.43	J/mol×K	634.06	Joback Method
cpg	474.22	J/mol×K	793.37	Joback Method
cpg	448.03	J/mol×K	713.72	Joback Method
cpg	438.54	J/mol×K	687.16	Joback Method
cpg	428.67	J/mol×K	660.61	Joback Method
cpg	465.88	J/mol×K	766.82	Joback Method
cpl	438.50	J/mol×K	333.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	430.90	J/mol×K	313.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	443.60	J/mol×K	343.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	449.10	J/mol×K	353.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	428.50	J/mol×K	303.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)

cpl	419.20	J/mol×K	298.00	NIST Webbook
cpl	434.70	J/mol×K	323.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	428.80	J/mol×K	298.00	NIST Webbook
dvisc	0.0000264	Paxs	589.76	Joback Method
dvisc	0.0000148	Paxs	634.06	Joback Method
dvisc	0.0002920	Paxs	456.85	Joback Method
dvisc	0.0037933	Paxs	368.25	Joback Method
dvisc	0.0001138	Paxs	501.15	Joback Method
dvisc	0.0000517	Paxs	545.46	Joback Method
dvisc	0.0009170	Paxs	412.55	Joback Method
hvapt	99.00 ± 10.00	kJ/mol	273.00	NIST Webbook
hvapt	92.20	kJ/mol	503.50	NIST Webbook
rfi	1.45710		293.15	Infinite Dilution Activity Coefficients of Hydrocarbons in Triethylene Glycol and Tetraethylene Glycol
rhol	1132.10	kg/m3	283.15	Thermophysical properties of glycols and glymes
rhol	1103.20	kg/m3	323.15	Thermophysical properties of glycols and glymes
rhol	1099.20	kg/m3	328.15	Thermophysical properties of glycols and glymes
rhol	1095.30	kg/m3	333.15	Thermophysical properties of glycols and glymes
rhol	1091.30	kg/m3	338.15	Thermophysical properties of glycols and glymes
rhol	1087.30	kg/m3	343.15	Thermophysical properties of glycols and glymes
rhol	1083.40	kg/m3	348.15	Thermophysical properties of glycols and glymes

rhol	1079.40	kg/m3	353.15	Thermophysical properties of glycols and glymes
rhol	1075.30	kg/m3	358.15	Thermophysical properties of glycols and glymes
rhol	1071.30	kg/m3	363.15	Thermophysical properties of glycols and glymes
rhol	1067.30	kg/m3	368.15	Thermophysical properties of glycols and glymes
rhol	1063.20	kg/m3	373.15	Thermophysical properties of glycols and glymes
rhol	1107.20	kg/m3	318.15	Thermophysical properties of glycols and glymes
rhol	1128.10	kg/m3	288.15	Thermophysical properties of glycols and glymes
rhol	1124.10	kg/m3	293.15	Thermophysical properties of glycols and glymes
rhol	1111.10	kg/m3	313.15	Thermophysical properties of glycols and glymes
rhol	1116.10	kg/m3	303.15	Thermophysical properties of glycols and glymes
rhol	1112.20	kg/m3	308.15	Thermophysical properties of glycols and glymes
rhol	1108.20	kg/m3	313.15	Thermophysical properties of glycols and glymes
rhol	1100.20	kg/m3	323.15	Thermophysical properties of glycols and glymes
rhol	1092.20	kg/m3	333.15	Thermophysical properties of glycols and glymes
rhol	1084.30	kg/m3	343.15	Thermophysical properties of glycols and glymes

rhol	1112.28	kg/m3	308.15	Excess Molar Enthalpies of Binary Mixtures Containing Glycols or Polyglycols + Dimethyl Sulfoxide at 308.15 K
rhol	1120.09	kg/m3	298.15	Thermodynamic Study of Binary Mixtures Containing Glycols or Polyethylene Glycols + Benzyl Alcohol at 308.15 K
rhol	1112.31	kg/m3	308.15	Thermodynamic Study of Binary Mixtures Containing Glycols or Polyethylene Glycols + Benzyl Alcohol at 308.15 K
rhol	1120.09	kg/m3	298.15	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Glycols or Poly(Ethylene Glycols) and 2-Phenylethyl Alcohol at 308.15 K and Atmospheric Pressure
rhol	1112.32	kg/m3	308.50	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Ethers and Benzyl Alcohol at 308.15 K and Atmospheric Pressure
rhol	1115.10	kg/m3	308.15	Thermophysical properties of glycols and glymes
rhol	1119.10	kg/m3	303.15	Thermophysical properties of glycols and glymes

rhol	1123.10	kg/m3	298.15	Thermophysical properties of glycols and glymes
rhol	1127.10	kg/m3	293.15	Thermophysical properties of glycols and glymes
rhol	1131.20	kg/m3	288.15	Thermophysical properties of glycols and glymes
rhol	1112.28	kg/m3	308.15	Excess molar enthalpies of binary mixtures containing ethylene glycols or poly(ethylene glycols) + ethyl alcohol at 308.15K and atmospheric pressure
rhol	1092.05	kg/m3	333.15	Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures in a wide temperature range
rhol	1096.04	kg/m3	328.15	Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures in a wide temperature range
rhol	1100.02	kg/m3	323.15	Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures in a wide temperature range
rhol	1104.01	kg/m3	318.15	Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures in a wide temperature range
rhol	1107.98	kg/m3	313.15	Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures in a wide temperature range

rhol	1111.96	kg/m3	308.15	Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures in a wide temperature range
rhol	1115.94	kg/m3	303.15	Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures in a wide temperature range
rhol	1127.88	kg/m3	288.15	Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures in a wide temperature range
rhol	1131.85	kg/m3	283.15	Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures in a wide temperature range
rhol	1135.81	kg/m3	278.15	Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures in a wide temperature range
rhol	1086.00	kg/m3	343.15	Vapour pressures and densities of the mixed-solvent desiccants (glycols + water + salts)
rhol	1093.00	kg/m3	333.15	Vapour pressures and densities of the mixed-solvent desiccants (glycols + water + salts)
rhol	1100.00	kg/m3	323.15	Vapour pressures and densities of the mixed-solvent desiccants (glycols + water + salts)
rhol	1108.00	kg/m3	313.15	Vapour pressures and densities of the mixed-solvent desiccants (glycols + water + salts)

rhol	1116.00	kg/m3	303.15	Vapour pressures and densities of the mixed-solvent desiccants (glycols + water + salts)
rhol	1123.90	kg/m3	293.15	Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures in a wide temperature range
rhol	1120.10	kg/m3	298.15	Thermophysical properties of glycols and glymes
rhol	1119.92	kg/m3	298.15	Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures in a wide temperature range
tcondl	0.19	W/mxK	328.20	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.19	W/mxK	318.30	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.19	W/mxK	308.20	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols

tcondl	0.18	W/mxK	298.20	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.19	W/mxK	338.20	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols

## Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C*\ln(T) + D*T^2$
Coeff. A	2.51044e+02
Coeff. B	-2.43857e+04
Coeff. C	-3.27566e+01
Coeff. D	1.19079e-05
Temperature range (K), min.	268.15
Temperature range (K), max.	722.00

## Datasets

### Mass density, kg/m<sup>3</sup>

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m <sup>3</sup> - Liquid
283.13	100.00	1132.0
283.13	1000.00	1132.4
283.13	2000.00	1132.8
283.13	5000.00	1134.1

283.13	7000.00	1135.0
283.13	10000.00	1136.4
283.13	12000.00	1137.2
283.13	16000.00	1138.9
283.13	20000.00	1140.6
283.13	25000.00	1142.8
283.13	30000.00	1144.8
283.13	35000.00	1146.9
283.13	40000.00	1148.8
283.13	45000.00	1150.7
283.13	50000.00	1152.6
283.13	55000.00	1154.5
283.13	60000.00	1156.3
283.13	65000.00	1158.2
283.13	70000.00	1159.9
283.13	75000.00	1161.7
283.13	80000.00	1163.3
283.13	85000.00	1165.1
283.13	90000.00	1166.7
283.13	95000.00	1168.4
293.11	100.00	1123.8
293.11	1000.00	1124.2
293.11	2000.00	1124.7
293.11	5000.00	1126.1
293.11	7000.00	1127.0
293.11	10000.00	1128.4
293.11	12000.00	1129.2
293.11	16000.00	1131.1
293.11	20000.00	1132.8
293.11	25000.00	1134.9
293.11	30000.00	1137.1
293.11	35000.00	1139.0
293.11	40000.00	1141.1
293.11	45000.00	1143.1
293.11	50000.00	1145.1
293.11	55000.00	1147.0
293.11	60000.00	1148.9
293.11	65000.00	1150.8
293.11	70000.00	1152.6
293.11	75000.00	1154.4
293.11	80000.00	1156.2
293.11	85000.00	1157.9
293.11	90000.00	1159.6
293.11	95000.00	1161.3

303.13	100.00	1115.8
303.13	1000.00	1116.1
303.13	2000.00	1116.7
303.13	5000.00	1118.1
303.13	7000.00	1119.1
303.13	10000.00	1120.5
303.13	12000.00	1121.4
303.13	16000.00	1123.3
303.13	20000.00	1125.0
303.13	25000.00	1127.3
303.13	30000.00	1129.5
303.13	35000.00	1131.6
303.13	40000.00	1133.7
303.13	45000.00	1135.7
303.13	50000.00	1137.7
303.13	55000.00	1139.7
303.13	60000.00	1141.7
303.13	65000.00	1143.6
303.13	70000.00	1145.5
303.13	75000.00	1147.4
303.13	80000.00	1149.1
303.13	85000.00	1150.8
303.13	90000.00	1152.6
303.13	95000.00	1154.4
313.22	100.00	1107.8
313.22	1000.00	1108.1
313.22	2000.00	1108.6
313.22	5000.00	1110.1
313.22	7000.00	1111.1
313.22	10000.00	1112.6
313.22	12000.00	1113.6
313.22	16000.00	1115.5
313.22	20000.00	1117.3
313.22	25000.00	1119.7
313.22	30000.00	1121.9
313.22	35000.00	1124.1
313.22	40000.00	1126.3
313.22	45000.00	1128.4
313.22	50000.00	1130.4
313.22	55000.00	1132.5
313.22	60000.00	1134.5
313.22	65000.00	1136.5
313.22	70000.00	1138.4
313.22	75000.00	1140.3

313.22	80000.00	1142.2
313.22	85000.00	1144.0
313.22	90000.00	1145.8
313.22	95000.00	1147.7
323.20	100.00	1099.8
323.20	1000.00	1100.1
323.20	2000.00	1100.6
323.20	5000.00	1102.2
323.20	7000.00	1103.2
323.20	10000.00	1104.7
323.20	12000.00	1105.6
323.20	16000.00	1107.7
323.20	20000.00	1109.6
323.20	25000.00	1111.9
323.20	30000.00	1114.3
323.20	35000.00	1116.6
323.20	40000.00	1118.8
323.20	45000.00	1121.0
323.20	50000.00	1123.2
323.20	55000.00	1125.5
323.20	60000.00	1127.4
323.20	65000.00	1129.4
323.20	70000.00	1131.3
323.20	75000.00	1133.3
323.20	80000.00	1135.2
323.20	85000.00	1137.1
323.20	90000.00	1139.0
323.20	95000.00	1140.7
333.20	100.00	1091.8
333.20	1000.00	1092.3
333.20	2000.00	1092.9
333.20	5000.00	1094.5
333.20	7000.00	1095.6
333.20	10000.00	1097.1
333.20	12000.00	1098.1
333.20	16000.00	1100.2
333.20	20000.00	1102.2
333.20	25000.00	1104.6
333.20	30000.00	1107.1
333.20	35000.00	1109.4
333.20	40000.00	1111.7
333.20	45000.00	1113.9
333.20	50000.00	1116.2
333.20	55000.00	1118.4

333.20	60000.00	1120.5
333.20	65000.00	1122.5
333.20	70000.00	1124.6
333.20	75000.00	1126.6
333.20	80000.00	1128.5
333.20	85000.00	1130.4
333.20	90000.00	1132.2
333.20	95000.00	1134.1
343.17	100.00	1084.0
343.17	1000.00	1084.4
343.17	2000.00	1085.0
343.17	5000.00	1086.7
343.17	7000.00	1087.7
343.17	10000.00	1089.4
343.17	12000.00	1090.4
343.17	16000.00	1092.5
343.17	20000.00	1094.6
343.17	25000.00	1097.1
343.17	30000.00	1099.7
343.17	35000.00	1102.1
343.17	40000.00	1104.5
343.17	45000.00	1106.8
343.17	50000.00	1109.1
343.17	55000.00	1111.3
343.17	60000.00	1113.5
343.17	65000.00	1115.7
343.17	70000.00	1117.7
343.17	75000.00	1119.8
343.17	80000.00	1121.9
343.17	85000.00	1123.8
343.17	90000.00	1125.8
343.17	95000.00	1127.6
353.13	100.00	1075.9
353.13	1000.00	1076.4
353.13	2000.00	1076.9
353.13	5000.00	1078.7
353.13	7000.00	1079.9
353.13	10000.00	1081.6
353.13	12000.00	1082.8
353.13	16000.00	1084.9
353.13	20000.00	1087.1
353.13	25000.00	1089.8
353.13	30000.00	1092.3
353.13	35000.00	1094.9

353.13	40000.00	1097.3
353.13	45000.00	1099.8
353.13	50000.00	1102.1
353.13	55000.00	1104.3
353.13	60000.00	1106.6
353.13	65000.00	1108.9
353.13	70000.00	1111.0
353.13	75000.00	1113.2
353.13	80000.00	1115.2
353.13	85000.00	1117.2
353.13	90000.00	1119.2
353.13	95000.00	1121.1
363.20	100.00	1067.8
363.20	1000.00	1068.4
363.20	2000.00	1069.0
363.20	5000.00	1070.8
363.20	7000.00	1072.0
363.20	10000.00	1073.7
363.20	12000.00	1074.9
363.20	16000.00	1077.1
363.20	20000.00	1079.5
363.20	25000.00	1082.3
363.20	30000.00	1084.8
363.20	35000.00	1087.5
363.20	40000.00	1089.9
363.20	45000.00	1092.4
363.20	50000.00	1094.8
363.20	55000.00	1097.2
363.20	60000.00	1099.5
363.20	65000.00	1101.8
363.20	70000.00	1104.0
363.20	75000.00	1106.2
363.20	80000.00	1108.4
363.20	85000.00	1110.4
363.20	90000.00	1112.5
363.20	95000.00	1114.4

Reference

<https://www.doi.org/10.1016/j.fluid.2017.01.003>

Temperature, K	Pressure, kPa	Mass density, kg/m <sup>3</sup>
283.15	100.00	1130.1
283.15	100.00	1130.1
283.15	630.00	1130.3

283.15	1170.00	1130.2
283.15	1640.00	1130.8
283.15	2110.00	1131.0
283.15	3060.00	1131.4
283.15	5060.00	1132.2
283.15	7000.00	1133.1
283.15	9990.00	1134.3
283.15	14800.00	1136.3
283.15	19770.00	1138.4
283.15	24630.00	1140.4
283.15	29550.00	1142.3
283.15	34530.00	1144.2
283.15	39370.00	1146.1
283.15	44340.00	1147.9
283.15	49210.00	1149.7
283.15	54130.00	1151.5
283.15	59040.00	1153.3
283.15	63940.00	1155.0
283.15	68790.00	1156.7
293.15	100.00	1122.0
293.15	100.00	1122.0
293.15	570.00	1122.2
293.15	1090.00	1122.4
293.15	1480.00	1122.6
293.15	2030.00	1122.8
293.15	3030.00	1123.3
293.15	5050.00	1124.2
293.15	7090.00	1125.1
293.15	9890.00	1126.3
293.15	14910.00	1128.5
293.15	19720.00	1130.5
293.15	24600.00	1132.6
293.15	29670.00	1134.6
293.15	34600.00	1136.6
293.15	39380.00	1138.5
293.15	44310.00	1140.4
293.15	49240.00	1142.3
293.15	54080.00	1144.1
293.15	58950.00	1145.9
293.15	63910.00	1147.7
293.15	68760.00	1149.4
303.15	100.00	1114.0
303.15	100.00	1114.0
303.15	630.00	1114.2

303.15	1200.00	1114.5
303.15	1610.00	1114.7
303.15	2120.00	1114.9
303.15	3090.00	1115.4
303.15	5080.00	1116.3
303.15	7050.00	1117.2
303.15	10000.00	1118.5
303.15	14920.00	1120.8
303.15	19740.00	1122.9
303.15	24580.00	1125.0
303.15	29520.00	1127.1
303.15	34410.00	1129.1
303.15	39420.00	1131.2
303.15	44270.00	1133.1
303.15	49210.00	1135.1
303.15	54140.00	1136.9
303.15	59090.00	1138.8
303.15	63880.00	1140.6
303.15	68800.00	1142.4
313.15	100.00	1106.0
313.15	100.00	1106.0
313.15	570.00	1106.3
313.15	1110.00	1106.5
313.15	1570.00	1106.7
313.15	2100.00	1107.0
313.15	3080.00	1107.5
313.15	5070.00	1108.4
313.15	7000.00	1109.4
313.15	9960.00	1110.7
313.15	14830.00	1113.0
313.15	19730.00	1115.2
313.15	24720.00	1117.5
313.15	29640.00	1119.6
313.15	34400.00	1121.8
313.15	39380.00	1123.8
313.15	44210.00	1125.9
313.15	49240.00	1127.8
313.15	54040.00	1129.8
313.15	59030.00	1131.7
313.15	63920.00	1133.6
313.15	68770.00	1135.4
323.15	100.00	1098.0
323.15	100.00	1098.0
323.15	590.00	1098.3

323.15	1180.00	1098.5
323.15	1580.00	1098.8
323.15	2100.00	1099.0
323.15	3000.00	1099.5
323.15	5060.00	1100.5
323.15	7010.00	1101.5
323.15	9930.00	1102.9
323.15	14900.00	1105.3
323.15	19770.00	1107.6
323.15	24760.00	1110.0
323.15	29530.00	1112.1
323.15	34470.00	1114.4
323.15	39440.00	1116.5
323.15	44180.00	1118.6
323.15	49200.00	1120.6
323.15	54100.00	1122.7
323.15	58970.00	1124.6
323.15	63800.00	1126.5
323.15	68790.00	1128.4
333.15	100.00	1090.1
333.15	100.00	1090.1
333.15	660.00	1090.4
333.15	1170.00	1090.6
333.15	1590.00	1090.8
333.15	2110.00	1091.1
333.15	3020.00	1091.6
333.15	5110.00	1092.7
333.15	6990.00	1093.7
333.15	9900.00	1095.1
333.15	14860.00	1097.7
333.15	19730.00	1100.0
333.15	23990.00	1102.6
333.15	29600.00	1104.7
333.15	34450.00	1107.1
333.15	39370.00	1109.2
333.15	44310.00	1111.5
333.15	49120.00	1113.5
333.15	54060.00	1115.6
333.15	59100.00	1117.7
333.15	63900.00	1119.7
333.15	68790.00	1121.6
343.15	100.00	1082.1
343.15	100.00	1082.1
343.15	720.00	1082.5

343.15	1090.00	1082.7
343.15	1600.00	1082.9
343.15	2060.00	1083.2
343.15	3100.00	1083.7
343.15	5040.00	1084.8
343.15	6870.00	1085.8
343.15	9930.00	1087.4
343.15	14830.00	1090.0
343.15	19790.00	1092.5
343.15	24630.00	1095.0
343.15	29580.00	1097.4
343.15	34440.00	1099.7
343.15	39430.00	1102.1
343.15	44410.00	1104.4
343.15	49170.00	1106.5
343.15	54160.00	1108.6
343.15	58970.00	1110.7
343.15	63920.00	1112.8
343.15	68720.00	1114.7
353.15	100.00	1074.1
353.15	100.00	1074.1
353.15	560.00	1074.4
353.15	1190.00	1074.7
353.15	1660.00	1075.0
353.15	2160.00	1075.3
353.15	3100.00	1075.8
353.15	5040.00	1076.9
353.15	6910.00	1078.0
353.15	10040.00	1079.7
353.15	14770.00	1082.3
353.15	19790.00	1085.0
353.15	24570.00	1087.5
353.15	29460.00	1090.0
353.15	34560.00	1092.5
353.15	39340.00	1094.8
353.15	44310.00	1097.2
353.15	49190.00	1099.5
353.15	54020.00	1101.6
353.15	59160.00	1103.9
353.15	63870.00	1106.0
353.15	68800.00	1108.0
363.15	100.00	1066.1
363.15	100.00	1066.1
363.15	650.00	1066.5

363.15	1150.00	1066.7
363.15	1550.00	1067.0
363.15	2070.00	1067.2
363.15	3090.00	1067.9
363.15	5060.00	1069.0
363.15	7010.00	1070.2
363.15	9860.00	1071.8
363.15	14820.00	1074.7
363.15	19750.00	1077.4
363.15	24740.00	1080.1
363.15	29560.00	1082.6
363.15	34540.00	1085.2
363.15	39360.00	1087.6
363.15	44280.00	1090.1
363.15	49130.00	1092.3
363.15	54040.00	1094.7
363.15	59030.00	1097.0
363.15	63900.00	1099.1
363.15	68810.00	1101.6

Reference

<https://www.doi.org/10.1016/j.fluid.2018.09.026>

## Sources

### NIST Webbook:

<http://webbook.nist.gov/cgi/cbook.cgi?ID=C112607&Units=SI>

### Molar heat capacity of several aqueous solutions of KDB (hydroxymethyl)methyl-3-amino]propanesulfonic acid (TAPS) + glycol: Volumetric and acoustic studies on (tetraethylene glycol + water) mixtures Joback Method temperature range:

<https://www.doi.org/10.1016/j.tca.2012.04.006>

### Liquid-Liquid Equilibria of Ternary Systems Sulfide + Octane + Solvents at Different Pressure: Coefficients of Hydrocarbons in Triethylene Glycol Theoretical Properties: characterization of ternary system Viscosity of liquid diethylene (T4EG) + triethylene (T3EG) + tetraethylene glycol solutio Mixed-vapor high pressures using a organic solvate of some glycols: KDB Vapor Pressure Data:

<https://www.cheric.org/files/research/kdb/mol/mol928.mol>

<https://www.doi.org/10.1016/j.jct.2015.02.007>

[https://en.wikipedia.org/wiki/Joback\\_method](https://en.wikipedia.org/wiki/Joback_method)

<https://www.doi.org/10.1021/je800340v>

<https://www.doi.org/10.1021/je020196d>

<https://www.doi.org/10.1016/j.jct.2012.12.011>

<https://www.doi.org/10.1016/j.fluid.2018.09.026>

<https://www.doi.org/10.1016/j.fluid.2009.07.002>

<https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=928>

<https://pubs.acs.org/doi/abs/10.1021/ci990307l>

<https://www.doi.org/10.1021/je900802d>

<https://www.doi.org/10.1021/acs.jced.5b00662>

<https://www.doi.org/10.1021/je049943s>

<https://www.doi.org/10.1016/j.jct.2008.12.003>

<https://www.doi.org/10.1016/j.jct.2010.04.014>

### Crippen Method:

### Solubility Comparison of Bis(2-hydroxyethyl) Ether and Theoretical properties of glycols and glycols Modification by Ethyl Oxalyl Ester Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Glycols + water (partial densities of the mixed solvent, viscosities of glycols and densities and vapor pressures of mixed-solvent desiccant systems containing {glycol (diethylene, or triethylene, or tetraethylene glycol) + salt (magnesium chloride) + water}:

<b>Molar heat capacities of some aqueous 2-amino-2-hydroxymethyl-1,3-propanediol</b>	<a href="https://www.doi.org/10.1016/j.jct.2012.02.022">https://www.doi.org/10.1016/j.jct.2012.02.022</a>
<b>Heat capacities of the mixed-solvents desiccants (glycols +water + salts):</b>	<a href="https://www.doi.org/10.1016/j.tca.2009.01.008">https://www.doi.org/10.1016/j.tca.2009.01.008</a>
<b>Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Water and One or Several Mixed Solvent Desiccants Containing Glycol + Water</b>	<a href="https://www.doi.org/10.1021/je0504212">https://www.doi.org/10.1021/je0504212</a>
<b>The Thermodynamic Study of Binary Mixtures Containing Glycols or Polyethylene Glycols at Intermediate Weight and Size on the Solubility of Compounds Molar Viscosities and Partial Molar Isentropic Compressions of Four Polyethyleneglycols at Intermediate Temperatures and Pressures of Ethylene Glycols at Temperatures T = (278 to 343) K and Atmospheric Pressure:</b>	<a href="https://www.doi.org/10.1016/j.fluid.2011.12.018">https://www.doi.org/10.1016/j.fluid.2011.12.018</a>
<b>Excess Molar Enthalpies of Binary Mixtures Containing Glycols or Polyols and Dimethyl Sulphide at Liquid-Liquid Equilibrium Data of the Application of the Multi-Current Transient-Flow Wire Technique to Glycols: New Measurements of the Thermal Properties of Glycols:</b>	<a href="https://www.doi.org/10.1021/acs.jced.5b00498">https://www.doi.org/10.1021/acs.jced.5b00498</a>
<b>Excess molar enthalpies of binary mixtures containing ethylene glycols or Measurements and Modeling of Enthalpic Vapors-Liquids Equilibrium Water: Glycols:</b>	<a href="https://www.doi.org/10.1016/j.fluid.2018.05.011">https://www.doi.org/10.1016/j.fluid.2018.05.011</a>
	<a href="http://link.springer.com/article/10.1007/BF02311772">http://link.springer.com/article/10.1007/BF02311772</a>
	<a href="https://www.doi.org/10.1021/je034007i">https://www.doi.org/10.1021/je034007i</a>
	<a href="https://www.doi.org/10.1021/je034128i">https://www.doi.org/10.1021/je034128i</a>
	<a href="https://www.doi.org/10.1007/s10765-005-5568-4">https://www.doi.org/10.1007/s10765-005-5568-4</a>
	<a href="https://www.doi.org/10.1016/j.fluid.2017.01.003">https://www.doi.org/10.1016/j.fluid.2017.01.003</a>
	<a href="https://www.chemeo.com/doc/models/crippen_log10ws">https://www.chemeo.com/doc/models/crippen_log10ws</a>
	<a href="https://www.doi.org/10.1016/j.tca.2005.01.064">https://www.doi.org/10.1016/j.tca.2005.01.064</a>
	<a href="https://www.doi.org/10.1021/acs.jced.7b00945">https://www.doi.org/10.1021/acs.jced.7b00945</a>

## Legend

<b>chl:</b>	Standard liquid enthalpy of combustion
<b>cpg:</b>	Ideal gas heat capacity
<b>cpl:</b>	Liquid phase heat capacity
<b>dvisc:</b>	Dynamic viscosity
<b>gf:</b>	Standard Gibbs free energy of formation
<b>hf:</b>	Enthalpy of formation at standard conditions
<b>hfl:</b>	Liquid phase enthalpy of formation at standard conditions
<b>hfus:</b>	Enthalpy of fusion at standard conditions
<b>hvap:</b>	Enthalpy of vaporization at standard conditions
<b>hvapt:</b>	Enthalpy of vaporization at a given temperature
<b>log10ws:</b>	Log10 of Water solubility in mol/l
<b>logp:</b>	Octanol/Water partition coefficient
<b>mcvol:</b>	McGowan's characteristic volume
<b>pc:</b>	Critical Pressure
<b>pvap:</b>	Vapor pressure
<b>rfi:</b>	Refractive Index
<b>rhol:</b>	Liquid Density
<b>rinpolt:</b>	Non-polar retention indices
<b>tb:</b>	Normal Boiling Point Temperature
<b>tc:</b>	Critical Temperature
<b>tcondl:</b>	Liquid thermal conductivity
<b>tf:</b>	Normal melting (fusion) point

**vc:**

Critical Volume

Latest version available from:

<https://www.chemeo.com/cid/37-677-0/Tetraethylene-glycol.pdf>

Generated by Cheméo on 2024-04-17 23:17:04.152191068 +0000 UTC m=+15685073.072768380.

Cheméo (<https://www.chemeo.com>) is the biggest free database of chemical and physical data for the process industry.