

# Butane, 1,4-dichloro-

<b>Other names:</b>	1,4-Dichlorobutane TETRAMETHYLENE CHLORIDE
<b>Inchi:</b>	InChI=1S/C4H8Cl2/c5-3-1-2-4-6/h1-4H2
<b>InchiKey:</b>	KJDRSWPQXHESDQ-UHFFFAOYSA-N
<b>Formula:</b>	C4H8Cl2
<b>SMILES:</b>	C1CCCC1
<b>Mol. weight [g/mol]:</b>	127.01
<b>CAS:</b>	110-56-5

## Physical Properties

Property code	Value	Unit	Source
chl	-2534.80 ± 1.90	kJ/mol	NIST Webbook
gf	-41.06	kJ/mol	Joback Method
hf	-183.40 ± 1.90	kJ/mol	NIST Webbook
hfl	-229.50	kJ/mol	NIST Webbook
hfl	-229.80 ± 1.90	kJ/mol	NIST Webbook
hfus	14.51	kJ/mol	Joback Method
hvap	33.27	kJ/mol	Joback Method
ie	11.03	eV	NIST Webbook
log10ws	-1.80		Crippen Method
logp	2.244		Crippen Method
mcvol	91.700	ml/mol	McGowan Method
pc	3560.02	kPa	Joback Method
rinpol	874.00		NIST Webbook
rinpol	874.00		NIST Webbook
rinpol	874.00		NIST Webbook
rinpol	874.00		NIST Webbook
rinpol	894.10		NIST Webbook
rinpol	898.10		NIST Webbook
rinpol	895.00		NIST Webbook
rinpol	867.40		NIST Webbook
tb	428.15	K	KDB
tc	547.67	K	Joback Method
tf	234.50 ± 0.40	K	NIST Webbook
vc	0.357	m <sup>3</sup> /kmol	Joback Method

# Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	156.05	J/molxK	426.41	Joback Method
cpg	149.02	J/molxK	396.09	Joback Method
cpg	169.22	J/molxK	487.04	Joback Method
cpg	181.25	J/molxK	547.67	Joback Method
cpg	175.37	J/molxK	517.35	Joback Method
cpg	162.78	J/molxK	456.72	Joback Method
cpg	141.67	J/molxK	365.78	Joback Method
cpl	184.00	J/molxK	298.15	NIST Webbook
cpl	183.59	J/molxK	298.15	NIST Webbook
dvisc	0.0041179	Paxs	194.68	Joback Method
dvisc	0.0004401	Paxs	337.26	Joback Method
dvisc	0.0005835	Paxs	308.75	Joback Method
dvisc	0.0008192	Paxs	280.23	Joback Method
dvisc	0.0012422	Paxs	251.71	Joback Method
dvisc	0.0020950	Paxs	223.20	Joback Method
dvisc	0.0003469	Paxs	365.78	Joback Method
hvapt	43.40	kJ/mol	380.50	NIST Webbook
pvap	2.21	kPa	323.15	Excess molar enthalpies and (vapour + liquid) equilibria for mixtures containing N,N-dialkylamides and a,x-dichloroalkanes
pvap	2.21	kPa	323.15	Excess enthalpies and isothermal (vapour + liquid) equilibria of (1-methyl-2-pyrrolidone + 1-chloroalkane or +,?-dichloroalkane) mixtures
rfi	1.45190		298.15	Isothermal (vapour + liquid) equilibria and excess Gibbs free energies in some binary (cyclopentanone + chloroalkane) mixtures at temperatures from 298.15 K to 318.15 K

rfi	1.45200		298.15	Thermodynamic study of (alkyl esters + a,x-alkyl dihalides) I: HE and V E for 25 binary mixtures $\{x\text{Cu-1H}_2\text{u-1CO}_2\text{C}_2\text{H}_5 + (1-x)\text{a,x-ClCH}_2(\text{CH}_2)_v\text{-2CH}_2\text{Cl}\}$ , where $u = 1$ to $5$ , $a = 1$ and $v = x = 2$ to $6$
rfi	1.45220		298.15	Isothermal (vapour + liquid) equilibria for (nitromethane or nitroethane + 1,4-dichlorobutane) binary systems at temperatures between (343.15 and 363.15) K
rhol	1112.00	kg/m <sup>3</sup>	318.15	Volumetric Study for the Binary Nitromethane with Chloroalkane Mixtures at Temperatures in the Range (298.15 to 318.15) K
rhol	1133.94	kg/m <sup>3</sup>	298.15	Volumetric Study for the Binary Nitromethane with Chloroalkane Mixtures at Temperatures in the Range (298.15 to 318.15) K
rhol	1123.00	kg/m <sup>3</sup>	308.15	Volumetric Study for the Binary Nitromethane with Chloroalkane Mixtures at Temperatures in the Range (298.15 to 318.15) K
rhol	1132.50	kg/m <sup>3</sup>	298.15	Densities and Excess Molar Volumes of the Binary Mixtures of Cyclopentanone with Chloroalkanes at $T = (288.15, 298.15, 308.15, \text{ and } 318.15) \text{ K}$

rho	1121.54	kg/m <sup>3</sup>	308.15	Densities and Excess Molar Volumes of the Binary Mixtures of Cyclopentanone with Chloroalkanes at T = (288.15, 298.15, 308.15, and 318.15) K
rho	1143.43	kg/m <sup>3</sup>	288.15	Densities and Excess Molar Volumes of the Binary Mixtures of Cyclopentanone with Chloroalkanes at T = (288.15, 298.15, 308.15, and 318.15) K
rho	1110.61	kg/m <sup>3</sup>	318.15	Densities and Excess Molar Volumes of the Binary Mixtures of Cyclohexanone with Chloroalkanes at Temperatures between (288.15 and 318.15) K
rho	1121.61	kg/m <sup>3</sup>	308.15	Densities and Excess Molar Volumes of the Binary Mixtures of Cyclohexanone with Chloroalkanes at Temperatures between (288.15 and 318.15) K
rho	1132.57	kg/m <sup>3</sup>	298.15	Densities and Excess Molar Volumes of the Binary Mixtures of Cyclohexanone with Chloroalkanes at Temperatures between (288.15 and 318.15) K

rhoI	1110.54	kg/m3	318.15	Densities and Excess Molar Volumes of the Binary Mixtures of Cyclopentanone with Chloroalkanes at T = (288.15, 298.15, 308.15, and 318.15) K
rhoI	1143.49	kg/m3	288.15	Densities and Excess Molar Volumes of the Binary Mixtures of Cyclohexanone with Chloroalkanes at Temperatures between (288.15 and 318.15) K
rhoI	1135.00	kg/m3	298.15	Volumetric and optical properties for some (2-butanone + chloroalkane) binary mixtures at T = 298.15 K
speedsl	1251.00	m/s	308.15	Speeds of sound, isentropic compressibilities and refractive indices for some binary mixtures of nitromethane with chloroalkane at temperatures from 298.15 to 318.15 K. Comparison with theories
speedsl	1215.66	m/s	318.15	Speeds of sound, isentropic compressibilities and refractive indices for some binary mixtures of nitromethane with chloroalkane at temperatures from 298.15 to 318.15 K. Comparison with theories

speedsl	1286.64	m/s	298.15	Speeds of sound, isentropic compressibilities and refractive indices for some binary mixtures of nitromethane with chloroalkane at temperatures from 298.15 to 318.15 K. Comparison with theories
srf	0.03	N/m	303.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.03	N/m	298.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.03	N/m	293.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.03	N/m	313.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.03	N/m	308.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes

## Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.62874e+01
Coeff. B	-4.19096e+03
Coeff. C	-5.08480e+01
Temperature range (K), min.	312.79
Temperature range (K), max.	432.68

Information

Value

Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C \cdot \ln(T) + D \cdot T^2$
Coeff. A	7.77758e+01
Coeff. B	-7.95407e+03
Coeff. C	-9.14431e+00
Coeff. D	4.66169e-06
Temperature range (K), min.	235.85
Temperature range (K), max.	641.00

## Datasets

### Mass density, kg/m<sup>3</sup>

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m <sup>3</sup> - Liquid
288.15	100.00	1143.7
288.15	500.00	1144.1
288.15	1000.00	1144.5
288.15	1500.00	1144.8
288.15	2000.00	1145.2
288.15	2500.00	1145.5
288.15	3000.00	1145.9
288.15	3600.00	1146.4
288.15	4100.00	1146.7
288.15	4600.00	1147.0
288.15	5100.00	1147.4
288.15	5600.00	1147.7
288.15	6100.00	1148.1
288.15	6600.00	1148.5
288.15	7100.00	1148.9
288.15	7600.00	1149.2
288.15	8100.00	1149.5
288.15	8600.00	1149.9
288.15	9200.00	1150.3
288.15	9600.00	1150.7
288.15	10100.00	1151.0
288.15	10600.00	1151.3
288.15	11100.00	1151.7
288.15	11600.00	1152.0
288.15	12100.00	1152.4

288.15	12600.00	1152.7
288.15	13100.00	1153.1
288.15	13500.00	1153.3
288.15	14200.00	1153.8
288.15	14700.00	1154.1
288.15	15200.00	1154.4
288.15	15700.00	1154.8
288.15	16300.00	1155.2
288.15	16800.00	1155.6
288.15	17300.00	1155.9
288.15	17800.00	1156.2
288.15	18300.00	1156.5
288.15	18800.00	1156.8
288.15	19100.00	1157.1
288.15	19700.00	1157.4
288.15	20200.00	1157.8
298.15	100.00	1133.7
298.15	500.00	1134.0
298.15	1000.00	1134.4
298.15	1500.00	1134.8
298.15	2000.00	1135.2
298.15	2500.00	1135.6
298.15	3100.00	1136.1
298.15	3600.00	1136.4
298.15	4100.00	1136.8
298.15	4600.00	1137.2
298.15	5100.00	1137.6
298.15	5600.00	1137.9
298.15	6100.00	1138.4
298.15	6600.00	1138.7
298.15	7100.00	1139.1
298.15	7600.00	1139.4
298.15	8100.00	1139.8
298.15	8600.00	1140.2
298.15	9200.00	1140.6
298.15	9600.00	1141.0
298.15	10100.00	1141.4
298.15	10700.00	1141.8
298.15	11100.00	1142.1
298.15	11600.00	1142.4
298.15	12100.00	1142.8
298.15	12600.00	1143.2
298.15	13100.00	1143.6
298.15	13600.00	1143.9



298.15	14100.00	1144.2
298.15	14700.00	1144.6
298.15	15200.00	1145.0
298.15	15700.00	1145.4
298.15	16200.00	1145.8
298.15	16700.00	1146.1
298.15	17200.00	1146.5
298.15	17800.00	1146.9
298.15	18300.00	1147.2
298.15	18800.00	1147.6
298.15	19200.00	1147.9
298.15	19700.00	1148.2
298.15	20200.00	1148.7
308.15	100.00	1122.3
308.15	500.00	1122.7
308.15	1000.00	1123.1
308.15	1500.00	1123.5
308.15	2000.00	1123.9
308.15	2500.00	1124.3
308.15	3100.00	1124.8
308.15	3600.00	1125.2
308.15	4100.00	1125.6
308.15	4600.00	1126.0
308.15	5100.00	1126.4
308.15	5600.00	1126.9
308.15	6100.00	1127.2
308.15	6600.00	1127.5
308.15	7100.00	1128.0
308.15	7600.00	1128.4
308.15	8100.00	1128.8
308.15	8600.00	1129.2
308.15	9200.00	1129.6
308.15	9600.00	1130.0
308.15	10100.00	1130.4
308.15	10600.00	1130.9
308.15	11100.00	1131.2
308.15	11600.00	1131.5
308.15	12100.00	1131.9
308.15	12600.00	1132.4
308.15	13100.00	1132.6
308.15	13600.00	1133.1
308.15	14100.00	1133.5
308.15	14700.00	1133.9
308.15	15100.00	1134.2

308.15	15700.00	1134.6
308.15	16200.00	1135.0
308.15	16700.00	1135.3
308.15	17200.00	1135.7
308.15	17800.00	1136.1
308.15	18300.00	1136.5
308.15	18800.00	1136.8
308.15	19200.00	1137.2
308.15	19700.00	1137.6
308.15	20200.00	1138.0
318.15	100.00	1112.0
318.15	500.00	1112.4
318.15	1000.00	1112.8
318.15	1500.00	1113.2
318.15	2000.00	1113.7
318.15	2500.00	1114.1
318.15	3100.00	1114.7
318.15	3500.00	1115.0
318.15	4100.00	1115.5
318.15	4600.00	1115.9
318.15	5100.00	1116.3
318.15	5600.00	1116.8
318.15	6100.00	1117.3
318.15	6600.00	1117.7
318.15	7100.00	1118.1
318.15	7600.00	1118.4
318.15	8100.00	1118.9
318.15	8600.00	1119.3
318.15	9200.00	1119.8
318.15	9600.00	1120.2
318.15	10100.00	1120.6
318.15	10600.00	1121.0
318.15	11100.00	1121.4
318.15	11600.00	1121.8
318.15	12100.00	1122.1
318.15	12600.00	1122.6
318.15	13000.00	1123.0
318.15	13600.00	1123.3
318.15	14200.00	1123.9
318.15	14700.00	1124.4
318.15	15200.00	1124.7
318.15	15700.00	1125.1
318.15	16300.00	1125.4
318.15	16800.00	1126.0

318.15	17300.00	1126.3
318.15	17800.00	1126.5
318.15	18300.00	1127.0
318.15	18800.00	1127.4
318.15	19200.00	1127.7
318.15	19700.00	1128.0
318.15	20200.00	1128.4

Reference

<https://www.doi.org/10.1021/je700339f>**Temperature, K****Pressure, kPa****Mass density, kg/m<sup>3</sup>**

298.15

100.00

1133.7

Reference

<https://www.doi.org/10.1021/je7003758>

## Sources

Crippen Method:

<http://pubs.acs.org/doi/abs/10.1021/ci9903071>

Densities and Excess Molar Volumes of the Binary Mixtures of Cyclopentanone with Chloroalkanes at 298.15 K and Vapor-Liquid Equilibria for the Mixtures of Chloroalkanes with Cyclopentanone and Vapor-Liquid Equilibria of Nitromethane with Cyclopentanone

<https://www.doi.org/10.1021/je901052w>

The Yaws Handbook of Vapor Pressure:

<https://www.doi.org/10.1016/j.jct.2007.06.017>

Densities and Excess Molar Volumes of the Binary Mixtures of Cyclohexanone with Chloroalkanes at 298.15 K and Vapor-Liquid Equilibria of Nitromethane with Cyclohexanone

<https://www.doi.org/10.1016/j.jct.2008.01.024>

N,N-Dimethylformamide or N,N-Dimethylacetamide + 1,2-Dichloroalkane

<http://webbook.nist.gov/cgi/cbook.cgi?ID=C110565&Units=SI>

Thermodynamic study of (alkyl esters + a,x-alkyl dihalides) III. HE m and VE m for 20 binary mixtures

<https://www.sciencedirect.com/book/9780128029992/the-yaws-handbook-of-vapor-pressure>

Thermodynamic study of (alkyl esters + a,x-alkyl dihalides) VII. HE m and VE m for 20 binary mixtures (x Cu, 1 H<sub>2</sub>O)

<https://www.doi.org/10.1021/je900404r>

Volumetric study for the binary mixtures of nitromethane with chloroalkane

<https://www.doi.org/10.1021/je700339f>

Using the COSMO-RS methodology:

<http://link.springer.com/article/10.1007/BF02311772>

Thermodynamic study of (alkyl esters + a,x-alkyl dihalides) V. Hex and Vex for 20 binary mixtures

[https://www.chemeo.com/doc/models/crippen\\_log10ws](https://www.chemeo.com/doc/models/crippen_log10ws)

Speed of sound, entropic compressibility and refractive indices for binary mixtures of chloroalkane with nitromethane

<https://www.doi.org/10.1016/j.jct.2005.11.003>

Thermodynamic study of (alkyl esters + a,x-alkyl dihalides) VI. HE m and VE m for 20 binary mixtures (x Cu, 1 H<sub>2</sub>O)

<https://www.doi.org/10.1016/j.jct.2018.12.042>

Thermodynamic study of (alkyl esters + a,x-alkyl dihalides) v-2CH<sub>2</sub>Cl, where v = 1 to 4, x = Y and Z

<https://www.doi.org/10.1016/j.jct.2008.10.007>

Volumetric and optical properties for some (2-butanone + chloroalkane) binary mixtures at T = 298.15 K:

[https://en.wikipedia.org/wiki/Joback\\_method](https://en.wikipedia.org/wiki/Joback_method)<https://www.doi.org/10.1021/je3013342><https://www.thermopedia.com/doc/thermophys/prop/1604.html><https://www.thermopedia.com/doc/thermophys/prop/1604.html><https://www.doi.org/10.1016/j.jct.2006.10.008><https://www.doi.org/10.1016/j.fluid.2014.10.004><https://www.doi.org/10.1016/j.jct.2012.06.033><https://www.doi.org/10.1016/j.jct.2005.03.020><https://www.thermopedia.com/doc/thermophys/prop/1604.html><https://www.thermopedia.com/doc/thermophys/prop/1604.html><https://www.doi.org/10.1016/j.jct.2014.04.004><https://www.doi.org/10.1016/j.jct.2014.04.004>

Heat Capacities of  
alpha,omega-Dichloroalkanes at  
Densities and Normal  
Compressibilities at Pressures up to 20  
MPa  
Thermal Systems+ liquid) equilibria  
and Gibbs free energies in  
some binary (cyclopentane,  
chloroalkane) or P, U-Dichloroalkane:  
chloroalkane) mixtures at temperatures  
from 298.15 K to 318.15 K:

<https://www.doi.org/10.1021/je020042y>

<https://www.doi.org/10.1021/je7003758>

<https://www.doi.org/10.1016/j.jct.2007.03.008>

## Legend

<b>chl:</b>	Standard liquid enthalpy of combustion
<b>cpg:</b>	Ideal gas heat capacity
<b>cpl:</b>	Liquid phase heat capacity
<b>dvisc:</b>	Dynamic viscosity
<b>gf:</b>	Standard Gibbs free energy of formation
<b>hf:</b>	Enthalpy of formation at standard conditions
<b>hfl:</b>	Liquid phase enthalpy of formation at standard conditions
<b>hfus:</b>	Enthalpy of fusion at standard conditions
<b>hvap:</b>	Enthalpy of vaporization at standard conditions
<b>hvapt:</b>	Enthalpy of vaporization at a given temperature
<b>ie:</b>	Ionization energy
<b>log10ws:</b>	Log10 of Water solubility in mol/l
<b>logp:</b>	Octanol/Water partition coefficient
<b>mcvol:</b>	McGowan's characteristic volume
<b>pc:</b>	Critical Pressure
<b>pvap:</b>	Vapor pressure
<b>rfi:</b>	Refractive Index
<b>rho:</b>	Liquid Density
<b>rinpol:</b>	Non-polar retention indices
<b>speedsl:</b>	Speed of sound in fluid
<b>srf:</b>	Surface Tension
<b>tb:</b>	Normal Boiling Point Temperature
<b>tc:</b>	Critical Temperature
<b>tf:</b>	Normal melting (fusion) point
<b>vc:</b>	Critical Volume

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