

1-Butanol

Other names:	1-Butyl alcohol
	1-Hydroxybutane
	Alcool butylique
	Butan-1-ol
	Butanol
	Butanol-1
	Butanolen
	Butanolo
	Butyl alcohol
	Butyl hydroxide
	Butylowy alkohol
	Butyric alcohol
	CCS 203
	Hemostyp
	METHYLOLPROPANE
	N-BUTYL ALCOHOL
	NSC 62782
	Propylcarbinol
	Propylmethanol
	Rcra waste number U031
	n-Butan-1-ol
	n-Butanol
	n-C4H9OH
Inchi:	InChI=1S/C4H10O/c1-2-3-4-5/h5H,2-4H2,1H3
InchiKey:	LRHPLDYGQMQRHN-UHFFFAOYSA-N
Formula:	C4H10O
SMILES:	CCCCO
Mol. weight [g/mol]:	74.12
CAS:	71-36-3

Physical Properties

Property code	Value	Unit	Source
af	0.5930		KDB
affp	789.20	kJ/mol	NIST Webbook
aigt	616.48	K	KDB
basg	758.90	kJ/mol	NIST Webbook

chl	-2674.90 ± 0.84	kJ/mol	NIST Webbook
chl	-2677.40 ± 0.63	kJ/mol	NIST Webbook
chl	-2676.01 ± 0.24	kJ/mol	NIST Webbook
chl	-2675.61 ± 0.45	kJ/mol	NIST Webbook
chl	-2670.44	kJ/mol	NIST Webbook
chl	-2676.00	kJ/mol	NIST Webbook
chl	-2640.00 ± 120.00	kJ/mol	NIST Webbook
chl	-2676.18 ± 0.24	kJ/mol	NIST Webbook
chl	-2670.77	kJ/mol	NIST Webbook
chl	-2670.40 ± 0.42	kJ/mol	NIST Webbook
dm	1.80	debye	KDB
dvisc	0.0025383	Pa×s	Densities and Viscosities of Binary Liquid Mixtures of Trichloroethylene and Tetrachloroethylene with Some Polar and Nonpolar Solvents
dvisc	0.0025650	Pa×s	Thermodynamic properties of binary liquid mixtures of diethylenetriamine with alcohols at different temperatures
dvisc	0.0025730	Pa×s	Study of densities, viscosities, and speeds of sound of binary liquid mixtures of butan-1-ol with n-alkanes (C6, C8, and C10) at T = (298.15, 303.15, and 308.15) K
fil	1.40	% in Air	KDB
flu	11.20	% in Air	KDB
fpc	309.26	K	KDB
fpo	302.04	K	KDB
gf	-150.90	kJ/mol	KDB
gyrad	3.2250		KDB
hf	-275.28 ± 0.53	kJ/mol	NIST Webbook
hf	-280.00 ± 0.92	kJ/mol	NIST Webbook
hf	-273.50 ± 0.70	kJ/mol	NIST Webbook
hf	-277.00 ± 1.50	kJ/mol	NIST Webbook
hf	-281.40	kJ/mol	NIST Webbook
hf	-278.20	kJ/mol	NIST Webbook
hf	-274.90	kJ/mol	KDB
hf	-274.40	kJ/mol	NIST Webbook
hf	-275.60	kJ/mol	NIST Webbook
hf	-277.30 ± 3.00	kJ/mol	NIST Webbook
hf	-280.50 ± 0.40	kJ/mol	NIST Webbook
hf	-274.90 ± 0.30	kJ/mol	NIST Webbook
hf	-275.80	kJ/mol	NIST Webbook
hf	-274.70 ± 0.30	kJ/mol	NIST Webbook

hfl	-329.60	kJ/mol	NIST Webbook
hfl	-327.18 ± 0.24	kJ/mol	NIST Webbook
hfl	-325.80 ± 0.67	kJ/mol	NIST Webbook
hfl	-328.40 ± 0.84	kJ/mol	NIST Webbook
hfl	-332.80 ± 0.42	kJ/mol	NIST Webbook
hfl	-327.58 ± 0.52	kJ/mol	NIST Webbook
hfl	-327.01 ± 0.24	kJ/mol	NIST Webbook
hfus	10.20	kJ/mol	Joback Method
hvap	41.18	kJ/mol	Joback Method
ie	10.64 ± 0.07	eV	NIST Webbook
ie	10.10 ± 0.05	eV	NIST Webbook
ie	9.99 ± 0.05	eV	NIST Webbook
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ie	10.37	eV	NIST Webbook
ie	10.09 ± 0.02	eV	NIST Webbook
log10ws	0.00		Aqueous Solubility Prediction Method
log10ws	0.00		Estimated Solubility Method
logp	0.779		Crippen Method
mcvol	73.090	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=1)		KDB
pc	4413.00	kPa	NIST Webbook
pc	4423.00	kPa	NIST Webbook
pc	4415.00	kPa	NIST Webbook
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pc	4418.00 ± 20.00	kPa	NIST Webbook
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pc	4413.00	kPa	NIST Webbook
rhoc	271.29 ± 1.48	kg/m3	NIST Webbook
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ripol	1164.00	NIST Webbook
ripol	1140.00	NIST Webbook
ripol	1138.00	NIST Webbook
ripol	1163.00	NIST Webbook
ripol	1120.00	NIST Webbook
ripol	1133.33	NIST Webbook
ripol	1178.00	NIST Webbook
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ripol	1135.00	NIST Webbook
ripol	1142.00	NIST Webbook
ripol	1145.00	NIST Webbook
ripol	1153.00	NIST Webbook
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ripol	1137.00	NIST Webbook
ripol	1134.00	NIST Webbook
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ripol	1145.00	NIST Webbook
ripol	1145.90	NIST Webbook
ripol	1125.00	NIST Webbook
ripol	1157.00	NIST Webbook
ripol	1153.00	NIST Webbook
ripol	1128.00	NIST Webbook
ripol	1113.00	NIST Webbook
ripol	1160.00	NIST Webbook
ripol	1175.00	NIST Webbook
ripol	1164.00	NIST Webbook
ripol	1150.00	NIST Webbook
ripol	1150.00	NIST Webbook
ripol	1113.00	NIST Webbook
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ripol	1160.00	NIST Webbook
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ripol	1143.00	NIST Webbook
ripol	1152.00	NIST Webbook
ripol	1138.00	NIST Webbook
ripol	1136.00	NIST Webbook
ripol	1115.00	NIST Webbook
ripol	1137.00	NIST Webbook
ripol	1152.00	NIST Webbook
ripol	1118.00	NIST Webbook
ripol	1120.00	NIST Webbook
ripol	1178.00	NIST Webbook
ripol	1135.00	NIST Webbook
ripol	1135.08	NIST Webbook
ripol	1129.04	NIST Webbook
ripol	1130.99	NIST Webbook
ripol	1133.33	NIST Webbook
ripol	1131.00	NIST Webbook
ripol	1153.00	NIST Webbook
ripol	1124.00	NIST Webbook
ripol	1148.00	NIST Webbook
ripol	1104.00	NIST Webbook
ripol	1126.00	NIST Webbook
ripol	1178.00	NIST Webbook
ripol	1146.00	NIST Webbook
ripol	1147.50	NIST Webbook
ripol	1120.00	NIST Webbook

ripol	1128.00		NIST Webbook
ripol	1133.00		NIST Webbook
sg	361.98	J/mol×K	NIST Webbook
sl	228.00	J/mol×K	NIST Webbook
sl	225.73	J/mol×K	NIST Webbook
sl	251.90	J/mol×K	NIST Webbook
tb	390.95 ± 0.50	K	NIST Webbook
tb	390.03 ± 1.50	K	NIST Webbook
tb	390.00 ± 1.50	K	NIST Webbook
tb	390.65 ± 0.50	K	NIST Webbook
tb	390.17 ± 0.20	K	NIST Webbook
tb	389.15 ± 2.00	K	NIST Webbook
tb	389.65 ± 0.50	K	NIST Webbook
tb	389.65 ± 2.50	K	NIST Webbook
tb	390.65 ± 0.30	K	NIST Webbook
tb	390.90 ± 0.50	K	NIST Webbook
tb	389.65 ± 1.00	K	NIST Webbook
tb	390.25 ± 0.20	K	NIST Webbook
tb	390.75 ± 0.50	K	NIST Webbook
tb	390.86 ± 0.05	K	NIST Webbook
tb	389.55 ± 0.70	K	NIST Webbook
tb	390.75 ± 0.30	K	NIST Webbook
tb	390.65 ± 0.30	K	NIST Webbook
tb	390.25 ± 0.20	K	NIST Webbook
tb	390.80 ± 0.50	K	NIST Webbook
tb	390.85 ± 0.50	K	NIST Webbook
tb	390.65 ± 0.50	K	NIST Webbook
tb	390.00 ± 1.50	K	NIST Webbook
tb	390.60 ± 0.50	K	NIST Webbook
tb	390.48	K	Phase Equilibrium (VLE, LLE, and VLE) Data of the Ternary System: Ionic Liquid [OMIM][PF6] + Butan-1-ol + Butyl Acetate
tb	391.00 ± 0.30	K	NIST Webbook
tb	390.70 ± 0.70	K	NIST Webbook
tb	389.75 ± 0.50	K	NIST Webbook
tb	390.95 ± 0.20	K	NIST Webbook
tb	390.90 ± 0.20	K	NIST Webbook
tb	389.40 ± 1.00	K	NIST Webbook
tb	390.80 ± 0.50	K	NIST Webbook
tb	390.88	K	KDB

tb	390.83	K	Experimental Determination of Densities and Isobaric Vapor Liquid Equilibria of Methyl Acetate and Ethyl Acetate with Alcohols (C3 and C4) at 0.3 MPa
tb	390.75	K	Excess molar volumes of ternary mixtures of 1,3-dichlorobenzene and methyl ethyl ketone with 1-alkanols at 303.15K
tb	390.12	K	Vapor liquid equilibria for the binary mixtures of 2,3-butanediol with n-butanol, n-butyl acetate, and ethyl acetate at 101.3 kPa
tb	390.85	K	Measurement and correlation of binary vapor liquid equilibria of isomeric butanols with 1,4-dioxane
tb	390.12	K	Liquid liquid equilibria of water + 2,3-butanediol + 1-butanol at T = 298.15 K, T = 308.15K and T = 318.15K
tb	390.65	K	Isobaric VLE data for the system of butan-1-ol + butylethanoate + 1-butyl-3-methylimidazoliumbis[(trifluoromethyl)sulfonyl]phosphonate
tb	390.82	K	Isobaric vapor-liquid equilibrium for the binary systems of 1-butanol +Poly methoxy methylal (n=2), and 1-butanol +Poly methoxy methylal (n=3) at 101.3 kPa
tb	390.80	K	Solubility and tie-line data for ternary aqueous mixtures of cyclopentanol with organic solvents at T = 298.2 K: Experiments and NRTL model
tb	390.84	K	Isobaric vapor liquid equilibrium for the binary systems of 1-propanol + 1-(methoxymethoxy)-butane and 1-butanol + 1-(methoxymethoxy)-butane at 101.3 kPa
tb	390.40	K	Isothermal and isobaric (vapour + liquid) equilibria of (alpha-pinene + n-butanol + n-octane)
tb	390.82	K	Isobaric Vapor Liquid Equilibrium for Two Binary Systems (n-Butanol + 1,4-Butanediol and .gamma.-Butyrolactone + 1,4-Butanediol) at p = (30.0, 50.0, and 70.0) kPa

tb	390.79	K	Isobaric Vapor Liquid Equilibrium for the Binary Systems of sec-Butyl Acetate + n-Butyl Alcohol, Isobutyl Alcohol, or tert-Butyl Alcohol at 101.3 kPa
tb	390.78	K	Isobaric Vapor Liquid Equilibrium for Three Binary Systems of Acetaldehyde + Ethanol, Ethyl Acetate, 1-Butanol at 101.3 kPa
tb	390.83	K	Measurement and Modelization of VLE for Butyl Acetate with Methanol, Ethanol, 1-Propanol, and 1-Butanol. Experimental Data at 0.15 MPa
tb	390.75	K	Vapor-Liquid Equilibrium for Binary of 1-Butanol + N,N-Dimethylacetamide and Methyl Isobutyl Ketone + N,N-Dimethylacetamide at 101.3 kPa
tb	390.91	K	Isobaric Phase Equilibria of Diethyl Carbonate with Five Alcohols at 101.3 kPa
tb	390.86	K	Measurement and Correlation of Excess Molar Enthalpies for Ethylene Glycol + Alkanol Systems at the Temperatures (298.15, 308.15, and 323.15) K
tb	390.65	K	Vapor Liquid Equilibrium at p/kPa = 101.3 of the Binary Mixtures of Ethenyl Acetate with Methanol and Butan-1-ol
tb	390.65 ± 0.50	K	NIST Webbook
tb	390.49	K	Vapor Liquid Equilibria Measurements for the Nine n-Alkane/Ketone Pairs Comprising 2-, 3-, and 4-Heptanone with n-Octane, n-Nonane, and n-Decane
tb	390.85	K	Vapor-Liquid Equilibrium Behaviors of Vanillin in 1-Butanol, 2-Butanol, and 2-Methyl-1-propanol
tb	390.85	K	Vapor-Liquid Equilibrium Behaviors of 3-Ethoxy-4-hydroxybenzaldehyde in Alcohol

tb	390.81	K	Vapor Liquid Equilibrium Behaviors of 5-Methyl-2-(1-methylethyl)phenol in Alcohol
tb	390.95	K	Isobaric Vapor-Liquid Equilibria of Heptane + 1-Butanol and Heptane + 1-Pentanol Systems at (53.3 and 91.3) kPa
tb	390.77 ± 0.07	K	NIST Webbook
tb	390.70 ± 0.40	K	NIST Webbook
tb	390.80 ± 0.10	K	NIST Webbook
tb	390.80 ± 0.25	K	NIST Webbook
tb	390.75 ± 0.40	K	NIST Webbook
tb	390.40	K	NIST Webbook
tb	391.00	K	NIST Webbook
tb	390.85 ± 0.25	K	NIST Webbook
tb	390.92 ± 0.10	K	NIST Webbook
tb	390.75 ± 0.30	K	NIST Webbook
tb	390.90	K	NIST Webbook
tb	390.85 ± 0.40	K	NIST Webbook
tb	390.85 ± 0.30	K	NIST Webbook
tb	450.74 ± 0.10	K	NIST Webbook
tb	390.15 ± 0.40	K	NIST Webbook
tb	389.85 ± 0.40	K	NIST Webbook
tb	390.80 ± 0.40	K	NIST Webbook
tb	390.10 ± 0.50	K	NIST Webbook
tb	390.65 ± 0.30	K	NIST Webbook
tb	390.55 ± 0.08	K	NIST Webbook
tb	390.80 ± 0.40	K	NIST Webbook
tb	390.80 ± 0.30	K	NIST Webbook
tb	390.80 ± 0.30	K	NIST Webbook
tb	391.20 ± 0.30	K	NIST Webbook
tb	390.51 ± 0.20	K	NIST Webbook
tb	390.90 ± 0.30	K	NIST Webbook
tb	390.75 ± 0.30	K	NIST Webbook
tb	391.00 ± 0.40	K	NIST Webbook
tb	390.35 ± 0.30	K	NIST Webbook
tb	390.90 ± 0.30	K	NIST Webbook
tb	390.85	K	NIST Webbook
tb	390.75 ± 0.30	K	NIST Webbook
tb	391.00 ± 0.15	K	NIST Webbook
tb	390.80 ± 0.50	K	NIST Webbook
tb	390.20 ± 2.00	K	NIST Webbook
tb	390.87 ± 0.50	K	NIST Webbook
tb	390.85 ± 0.30	K	NIST Webbook
tb	390.85 ± 0.40	K	NIST Webbook

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tb	390.67 ± 0.20	K	NIST Webbook
tb	390.95 ± 0.20	K	NIST Webbook
tb	390.85 ± 0.40	K	NIST Webbook
tb	389.15 ± 2.00	K	NIST Webbook
tb	390.85	K	NIST Webbook
tb	390.15 ± 0.50	K	NIST Webbook
tb	390.85 ± 0.50	K	NIST Webbook
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tb	390.65 ± 1.00	K	NIST Webbook
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tb	390.15 ± 1.00	K	NIST Webbook
tb	380.15 ± 2.00	K	NIST Webbook
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tb	389.65 ± 1.00	K	NIST Webbook
tb	389.90 ± 1.00	K	NIST Webbook
tb	390.55 ± 0.05	K	NIST Webbook
tb	390.85 ± 0.30	K	NIST Webbook
tb	391.25 ± 0.50	K	NIST Webbook
tb	390.95 ± 0.30	K	NIST Webbook
tb	391.00 ± 0.40	K	NIST Webbook
tb	390.95 ± 0.50	K	NIST Webbook
tb	390.80 ± 0.50	K	NIST Webbook
tb	390.00 ± 1.00	K	NIST Webbook

tb	390.82 ± 0.25	K	NIST Webbook
tb	390.95 ± 0.30	K	NIST Webbook
tb	390.75 ± 0.30	K	NIST Webbook
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tb	390.65 ± 1.00	K	NIST Webbook
tb	390.95 ± 0.30	K	NIST Webbook
tb	390.85 ± 0.50	K	NIST Webbook
tb	390.15 ± 1.00	K	NIST Webbook
tb	390.85 ± 0.50	K	NIST Webbook
tb	390.75 ± 0.50	K	NIST Webbook
tb	390.85 ± 0.50	K	NIST Webbook
tb	388.90 ± 2.00	K	NIST Webbook
tb	390.15 ± 1.00	K	NIST Webbook
tb	390.87 ± 0.05	K	NIST Webbook
tb	390.85 ± 0.50	K	NIST Webbook
tb	391.15 ± 0.50	K	NIST Webbook
tb	390.00 ± 3.00	K	NIST Webbook
tb	389.65 ± 1.00	K	NIST Webbook
tb	391.15 ± 1.00	K	NIST Webbook
tb	390.86 ± 0.10	K	NIST Webbook
tb	390.40 ± 0.10	K	NIST Webbook
tb	390.84 ± 0.10	K	NIST Webbook
tb	390.50 ± 0.50	K	NIST Webbook
tb	390.55 ± 0.50	K	NIST Webbook
tb	390.57 ± 0.20	K	NIST Webbook
tb	390.90 ± 0.30	K	NIST Webbook
tb	390.90 ± 0.25	K	NIST Webbook
tb	390.30 ± 0.30	K	NIST Webbook
tb	390.45 ± 0.50	K	NIST Webbook
tb	390.40 ± 0.50	K	NIST Webbook
tb	390.90 ± 0.40	K	NIST Webbook
tb	391.15 ± 0.20	K	NIST Webbook
tb	389.30 ± 1.00	K	NIST Webbook
tb	355.70 ± 0.50	K	NIST Webbook
tc	563.00	K	KDB
tc	560.30	K	NIST Webbook
tc	561.20	K	NIST Webbook
tc	560.10 ± 0.20	K	NIST Webbook
tc	562.92	K	NIST Webbook
tc	560.20	K	NIST Webbook
tc	564.20	K	NIST Webbook
tc	560.20	K	NIST Webbook
tc	563.05	K	NIST Webbook
tc	561.00 ± 2.00	K	NIST Webbook

tc	563.01	K	NIST Webbook
tc	562.20 ± 0.40	K	NIST Webbook
tc	562.20 ± 0.30	K	NIST Webbook
tc	562.20 ± 0.30	K	NIST Webbook
tc	562.20 ± 0.20	K	NIST Webbook
tc	562.90	K	NIST Webbook
tc	562.40	K	NIST Webbook
tc	562.40 ± 0.60	K	NIST Webbook
tc	562.40 ± 0.60	K	NIST Webbook
tc	563.60	K	NIST Webbook
tc	563.00 ± 0.30	K	NIST Webbook
tc	563.00	K	Measurement of Critical Properties for Binary and Ternary Mixtures Containing n-Butanol and n-Alkane
tc	562.20 ± 0.40	K	NIST Webbook
tf	193.15 ± 5.00	K	NIST Webbook
tf	183.30	K	KDB
tf	183.63	K	Aqueous Solubility Prediction Method
tf	183.85	K	NIST Webbook
tf	184.00 ± 2.00	K	NIST Webbook
tf	193.65 ± 1.00	K	NIST Webbook
tf	183.35 ± 0.20	K	NIST Webbook
tf	183.85	K	NIST Webbook
tf	192.55 ± 0.50	K	NIST Webbook
tf	183.70	K	Phase equilibria of didecyldimethylammonium nitrate ionic liquid with water and organic solvents
tt	184.51	K	KDB
tt	184.54 ± 0.02	K	NIST Webbook
tt	184.51 ± 0.05	K	NIST Webbook
tt	183.90 ± 0.20	K	NIST Webbook
vc	0.274	m3/kmol	KDB
vc	0.274	m3/kmol	NIST Webbook
zc	0.2583670		KDB
zra	0.25		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	149.26 ± 0.79	J/mol×K	431.05	NIST Webbook

cpg	151.60 ± 0.79	J/mol×K	441.15	NIST Webbook
cpg	140.93 ± 0.79	J/mol×K	395.25	NIST Webbook
cpg	137.88	J/mol×K	398.15	NIST Webbook
cpg	143.00 ± 0.79	J/mol×K	404.15	NIST Webbook
cpg	144.16 ± 0.79	J/mol×K	409.15	NIST Webbook
cpg	142.06	J/mol×K	413.15	NIST Webbook
cpg	189.31 ± 0.79	J/mol×K	603.35	NIST Webbook
cpg	181.20 ± 0.79	J/mol×K	568.45	NIST Webbook
cpg	175.97 ± 0.79	J/mol×K	545.95	NIST Webbook
cpg	169.95 ± 0.79	J/mol×K	520.05	NIST Webbook
cpg	162.55 ± 0.79	J/mol×K	488.25	NIST Webbook
cpg	155.88 ± 0.79	J/mol×K	459.55	NIST Webbook
cpg	152.66	J/mol×K	453.15	NIST Webbook
cpg	146.58 ± 0.79	J/mol×K	419.55	NIST Webbook
cpg	147.42	J/mol×K	433.15	NIST Webbook
cpl	175.97	J/mol×K	298.15	NIST Webbook
cpl	173.80	J/mol×K	293.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	189.10	J/mol×K	323.00	NIST Webbook
cpl	215.50	J/mol×K	302.60	NIST Webbook
cpl	183.30	J/mol×K	298.00	NIST Webbook
cpl	175.30	J/mol×K	294.00	NIST Webbook
cpl	180.30	J/mol×K	303.00	NIST Webbook
cpl	177.03	J/mol×K	298.15	NIST Webbook
cpl	179.50	J/mol×K	301.20	NIST Webbook
cpl	181.60	J/mol×K	303.50	NIST Webbook
cpl	174.30	J/mol×K	293.15	NIST Webbook
cpl	177.08	J/mol×K	298.15	NIST Webbook
cpl	176.69	J/mol×K	298.15	NIST Webbook
cpl	174.50	J/mol×K	298.00	NIST Webbook
cpl	177.18	J/mol×K	298.15	NIST Webbook
cpl	192.20	J/mol×K	321.05	NIST Webbook
cpl	177.70	J/mol×K	298.00	NIST Webbook
cpl	176.67	J/mol×K	298.15	NIST Webbook
cpl	176.86	J/mol×K	298.15	NIST Webbook
cpl	208.40	J/mol×K	338.15	Isobaric heat capacity of nanostructured liquids with potential use as lubricants

cpl	204.10	J/mol×K	333.15	Isobaric heat capacity of nanostructured liquids with potential use as lubricants
cpl	200.10	J/mol×K	328.15	Isobaric heat capacity of nanostructured liquids with potential use as lubricants
cpl	196.00	J/mol×K	323.15	Isobaric heat capacity of nanostructured liquids with potential use as lubricants
cpl	191.40	J/mol×K	318.15	Isobaric heat capacity of nanostructured liquids with potential use as lubricants
cpl	187.80	J/mol×K	313.15	Isobaric heat capacity of nanostructured liquids with potential use as lubricants
cpl	184.50	J/mol×K	308.15	Isobaric heat capacity of nanostructured liquids with potential use as lubricants
cpl	181.10	J/mol×K	303.15	Isobaric heat capacity of nanostructured liquids with potential use as lubricants
cpl	177.90	J/mol×K	298.15	Isobaric heat capacity of nanostructured liquids with potential use as lubricants
cpl	174.10	J/mol×K	293.15	Isobaric heat capacity of nanostructured liquids with potential use as lubricants
cpl	171.00	J/mol×K	288.15	Isobaric heat capacity of nanostructured liquids with potential use as lubricants

cpl	168.00	J/mol×K	283.15	Isobaric heat capacity of nanostructured liquids with potential use as lubricants
cpl	222.54	J/mol×K	353.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	218.10	J/mol×K	348.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	213.57	J/mol×K	343.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	209.16	J/mol×K	338.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	204.72	J/mol×K	333.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature

cpl	200.40	J/mol×K	328.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	196.13	J/mol×K	323.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	192.10	J/mol×K	318.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	188.02	J/mol×K	313.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	184.28	J/mol×K	308.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
cpl	180.61	J/mol×K	303.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature

cpl	177.10	J/mol×K	298.15	Molar heat capacities for (1-butanol + 1,4-butanediol, 2,3-butanediol, 1,2-butanediol, and 2-methyl-2,4-pentanediol) as function of temperature
dvisc	0.0022962	Pa×s	303.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0014140	Pa×s	323.15	Densities and Viscosities of Naphthalen-1-ol, Naphthalen-2-ol, and 1-Aminonaphthalene in the Solvents of Ethanol, Propan-1-ol, and Butan-1-ol
dvisc	0.0017690	Pa×s	313.15	Densities and Viscosities of Naphthalen-1-ol, Naphthalen-2-ol, and 1-Aminonaphthalene in the Solvents of Ethanol, Propan-1-ol, and Butan-1-ol
dvisc	0.0022600	Pa×s	303.15	Densities and Viscosities of Naphthalen-1-ol, Naphthalen-2-ol, and 1-Aminonaphthalene in the Solvents of Ethanol, Propan-1-ol, and Butan-1-ol
dvisc	0.0029290	Pa×s	293.15	Densities and Viscosities of Naphthalen-1-ol, Naphthalen-2-ol, and 1-Aminonaphthalene in the Solvents of Ethanol, Propan-1-ol, and Butan-1-ol

dvisc	0.0011430	Pa×s	333.15	Densities and Viscosities of Naphthalen-1-ol, Naphthalen-2-ol, and 1-Aminonaphthalene in the Solvents of Ethanol, Propan-1-ol, and Butan-1-ol
dvisc	0.0029530	Pa×s	293.15	Density, Viscosity, and Isobaric Heat Capacity of the Mixture (1-Butanol + 1-Hexene)
dvisc	0.0017442	Pa×s	313.15	Molecular interactions in binary mixtures of formamide with 1-butanol, 2-butanol, 1,3-butanediol and 1,4-butanediol at different temperatures: An ultrasonic and viscometric study
dvisc	0.0022630	Pa×s	303.15	Density, Viscosity, and Isobaric Heat Capacity of the Mixture (1-Butanol + 1-Hexene)
dvisc	0.0017690	Pa×s	313.15	Density, Viscosity, and Isobaric Heat Capacity of the Mixture (1-Butanol + 1-Hexene)
dvisc	0.0038220	Pa×s	283.15	Density and Viscosity of the Binary Systems Ethanol + Butan-1-ol, + Pentan-1-ol, + Heptan-1-ol, + Octan-1-ol, + Nonan-1-ol, + Decan-1-ol at 0.1 MPa and Temperatures from 283.15 K to 313.15 K

dvisc	0.0028590	Pa×s	293.15	Density and Viscosity of the Binary Systems Ethanol + Butan-1-ol, + Pentan-1-ol, + Heptan-1-ol, + Octan-1-ol, + Nonan-1-ol, + Decan-1-ol at 0.1 MPa and Temperatures from 283.15 K to 313.15 K
dvisc	0.0025580	Pa×s	298.15	Density and Viscosity of the Binary Systems Ethanol + Butan-1-ol, + Pentan-1-ol, + Heptan-1-ol, + Octan-1-ol, + Nonan-1-ol, + Decan-1-ol at 0.1 MPa and Temperatures from 283.15 K to 313.15 K
dvisc	0.0022360	Pa×s	303.15	Density and Viscosity of the Binary Systems Ethanol + Butan-1-ol, + Pentan-1-ol, + Heptan-1-ol, + Octan-1-ol, + Nonan-1-ol, + Decan-1-ol at 0.1 MPa and Temperatures from 283.15 K to 313.15 K
dvisc	0.0017360	Pa×s	313.15	Density and Viscosity of the Binary Systems Ethanol + Butan-1-ol, + Pentan-1-ol, + Heptan-1-ol, + Octan-1-ol, + Nonan-1-ol, + Decan-1-ol at 0.1 MPa and Temperatures from 283.15 K to 313.15 K

dvisc	0.0033748	Pa×s	288.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0029446	Pa×s	293.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0025809	Pa×s	298.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0022719	Pa×s	303.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0020081	Pa×s	308.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0017820	Pa×s	313.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K

dvisc	0.0015872	Pa×s	318.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0014188	Pa×s	323.15	Densities, Viscosities and Refractive Indices of the Ternary Mixture Dimethyladipate + 2-Butanone + 1-Butanol at T = (288.15 to 323.15) K
dvisc	0.0025730	Pa×s	298.15	Temperature and Composition Dependence of the Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of 1-Butanol with Hexadecane and Squalane
dvisc	0.0020253	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0019810	Pa×s	308.15	Temperature and Composition Dependence of the Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of 1-Butanol with Hexadecane and Squalane
dvisc	0.0029420	Pa×s	293.15	Viscosities and Densities of Binary Mixtures of (N-Acetylmorpholine + Alkanols) from (293.15 to 323.15) K

dvisc	0.0022750	Pa×s	303.15	Viscosities and Densities of Binary Mixtures of (N-Acetylmorpholine + Alkanols) from (293.15 to 323.15) K
dvisc	0.0016840	Pa×s	313.15	Viscosities and Densities of Binary Mixtures of (N-Acetylmorpholine + Alkanols) from (293.15 to 323.15) K
dvisc	0.0010980	Pa×s	323.15	Viscosities and Densities of Binary Mixtures of (N-Acetylmorpholine + Alkanols) from (293.15 to 323.15) K
dvisc	0.0025880	Pa×s	298.15	Densities and Viscosities of Binary Mixtures of Cyclopropanecarboxylic Acid with Methanol, Ethanol, Propan-1-ol, and Butan-1-ol at Different Temperatures
dvisc	0.0019910	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of Cyclopropanecarboxylic Acid with Methanol, Ethanol, Propan-1-ol, and Butan-1-ol at Different Temperatures
dvisc	0.0015953	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K

dvisc	0.0014170	Pa×s	323.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0012714	Pa×s	328.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0011381	Pa×s	333.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0010275	Pa×s	338.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0009306	Pa×s	343.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0015550	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of Cyclopropanecarboxylic Acid with Methanol, Ethanol, Propan-1-ol, and Butan-1-ol at Different Temperatures

dvisc	0.0012280	Pa×s	328.15	Densities and Viscosities of Binary Mixtures of Cyclopropanecarboxylic Acid with Methanol, Ethanol, Propan-1-ol, and Butan-1-ol at Different Temperatures
dvisc	0.0009810	Pa×s	338.15	Densities and Viscosities of Binary Mixtures of Cyclopropanecarboxylic Acid with Methanol, Ethanol, Propan-1-ol, and Butan-1-ol at Different Temperatures
dvisc	0.0029410	Pa×s	293.15	Densities, Viscosities, and Excess Molar Enthalpies of 2-Pyrrolidone + Butanol Isomers at T) (293.15, 298.15, and 303.15) K
dvisc	0.0022750	Pa×s	303.15	Temperature and Composition Dependence of the Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of 1-Butanol with Hexadecane and Squalane
dvisc	0.0025720	Pa×s	298.15	Densities, Viscosities, and Excess Molar Enthalpies of 2-Pyrrolidone + Butanol Isomers at T) (293.15, 298.15, and 303.15) K
dvisc	0.0022750	Pa×s	303.15	Densities, Viscosities, and Excess Molar Enthalpies of 2-Pyrrolidone + Butanol Isomers at T) (293.15, 298.15, and 303.15) K

dvisc	0.0029401	Pa×s	293.15	Densities and Viscosities of exo-Tetrahydrodicyclopentadiene + n-Butanol and exo-Tetrahydrodicyclopentadiene + n-Pentanol at Temperatures of (293.15 to 313.15) K
dvisc	0.0025612	Pa×s	298.15	Densities and Viscosities of exo-Tetrahydrodicyclopentadiene + n-Butanol and exo-Tetrahydrodicyclopentadiene + n-Pentanol at Temperatures of (293.15 to 313.15) K
dvisc	0.0022866	Pa×s	303.15	Densities and Viscosities of exo-Tetrahydrodicyclopentadiene + n-Butanol and exo-Tetrahydrodicyclopentadiene + n-Pentanol at Temperatures of (293.15 to 313.15) K
dvisc	0.0029380	Pa×s	293.15	Viscosities and densities for binary mixtures of N-methylpiperazine with methanol, ethanol, n-propanol, iso-propanol, n-butanol and iso-butanol at 293.15, 298.15 and 303.15K
dvisc	0.0025720	Pa×s	298.15	Viscosities and densities for binary mixtures of N-methylpiperazine with methanol, ethanol, n-propanol, iso-propanol, n-butanol and iso-butanol at 293.15, 298.15 and 303.15K

dvisc	0.0022710	Pa×s	303.15	Viscosities and densities for binary mixtures of N-methylpiperazine with methanol, ethanol, n-propanol, iso-propanol, n-butanol and iso-butanol at 293.15, 298.15 and 303.15K
dvisc	0.0029356	Pa×s	293.15	Molecular interactions in binary mixtures of formamide with 1-butanol, 2-butanol, 1,3-butanediol and 1,4-butanediol at different temperatures: An ultrasonic and viscometric study
dvisc	0.0025416	Pa×s	298.15	Molecular interactions in binary mixtures of formamide with 1-butanol, 2-butanol, 1,3-butanediol and 1,4-butanediol at different temperatures: An ultrasonic and viscometric study
dvisc	0.0022751	Pa×s	303.15	Molecular interactions in binary mixtures of formamide with 1-butanol, 2-butanol, 1,3-butanediol and 1,4-butanediol at different temperatures: An ultrasonic and viscometric study
dvisc	0.0019978	Pa×s	308.15	Molecular interactions in binary mixtures of formamide with 1-butanol, 2-butanol, 1,3-butanediol and 1,4-butanediol at different temperatures: An ultrasonic and viscometric study

dvisc	0.0017954	Pa×s	313.15	Densities and Viscosities of Binary Mixtures of n-Butanol with 2-Butanol, Isobutanol, and tert-Butanol from (303.15 to 343.15) K
dvisc	0.0015712	Pa×s	318.15	Molecular interactions in binary mixtures of formamide with 1-butanol, 2-butanol, 1,3-butanediol and 1,4-butanediol at different temperatures: An ultrasonic and viscometric study
dvisc	0.0020104	Pa×s	308.15	Densities and Viscosities for Binary Mixtures of the Ionic Liquid N-Ethyl Piperazinium Propionate with n-Alcohols at Several Temperatures
dvisc	0.0025710	Pa×s	298.15	Viscosity, density, and speed of sound of methylcyclopentane with primary and secondary alcohols at T = (293.15, 298.15, and 303.15) K
dvisc	0.0022550	Pa×s	303.15	Viscosity, density, and speed of sound of methylcyclopentane with primary and secondary alcohols at T = (293.15, 298.15, and 303.15) K

dvisc	0.0025850	Pa×s	298.15	Densities, viscosities, and ultrasonic velocity studies of binary mixtures of trichloromethane with methanol, ethanol, propan-1-ol, and butan-1-ol at T=(298.15 and 308.15) K
dvisc	0.0020120	Pa×s	308.15	Densities, viscosities, and ultrasonic velocity studies of binary mixtures of trichloromethane with methanol, ethanol, propan-1-ol, and butan-1-ol at T=(298.15 and 308.15) K
dvisc	0.0029410	Pa×s	293.15	Dynamic viscosities of binary mixtures of cycloalkanes with primary alcohols at T = (293.15, 298.15, and 303.15) K: New UNIFAC-VISCO interaction parameters
dvisc	0.0025710	Pa×s	298.15	Dynamic viscosities of binary mixtures of cycloalkanes with primary alcohols at T = (293.15, 298.15, and 303.15) K: New UNIFAC-VISCO interaction parameters
dvisc	0.0022550	Pa×s	303.15	Dynamic viscosities of binary mixtures of cycloalkanes with primary alcohols at T = (293.15, 298.15, and 303.15) K: New UNIFAC-VISCO interaction parameters

dvisc	0.0038794	Pa×s	283.15	Density and viscosity of 1-butyl-3-methylimidazolium nitrate with ethanol, 1-propanol, or 1-butanol at several temperatures
dvisc	0.0033911	Pa×s	288.15	Density and viscosity of 1-butyl-3-methylimidazolium nitrate with ethanol, 1-propanol, or 1-butanol at several temperatures
dvisc	0.0030100	Pa×s	293.15	Density and viscosity of 1-butyl-3-methylimidazolium nitrate with ethanol, 1-propanol, or 1-butanol at several temperatures
dvisc	0.0026062	Pa×s	298.15	Density and viscosity of 1-butyl-3-methylimidazolium nitrate with ethanol, 1-propanol, or 1-butanol at several temperatures
dvisc	0.0023147	Pa×s	303.15	Density and viscosity of 1-butyl-3-methylimidazolium nitrate with ethanol, 1-propanol, or 1-butanol at several temperatures
dvisc	0.0020655	Pa×s	308.15	Density and viscosity of 1-butyl-3-methylimidazolium nitrate with ethanol, 1-propanol, or 1-butanol at several temperatures
dvisc	0.0018476	Pa×s	313.15	Density and viscosity of 1-butyl-3-methylimidazolium nitrate with ethanol, 1-propanol, or 1-butanol at several temperatures

dvisc	0.0016597	Pa×s	318.15	Density and viscosity of 1-butyl-3-methylimidazolium nitrate with ethanol, 1-propanol, or 1-butanol at several temperatures	
dvisc	0.0014952	Pa×s	323.15	Density and viscosity of 1-butyl-3-methylimidazolium nitrate with ethanol, 1-propanol, or 1-butanol at several temperatures	
dvisc	0.0013567	Pa×s	328.15	Density and viscosity of 1-butyl-3-methylimidazolium nitrate with ethanol, 1-propanol, or 1-butanol at several temperatures	
dvisc	0.0012435	Pa×s	333.15	Density and viscosity of 1-butyl-3-methylimidazolium nitrate with ethanol, 1-propanol, or 1-butanol at several temperatures	
dvisc	0.0029410	Pa×s	293.15	Properties of pure 1-methylimidazolium acetate ionic liquid and its binary mixtures with alcohols	
dvisc	0.0025730	Pa×s	298.15	Properties of pure 1-methylimidazolium acetate ionic liquid and its binary mixtures with alcohols	
dvisc	0.0022640	Pa×s	303.15	Properties of pure 1-methylimidazolium acetate ionic liquid and its binary mixtures with alcohols	

dvisc	0.0020020	Pa×s	308.15	Properties of pure 1-methylimidazolium acetate ionic liquid and its binary mixtures with alcohols
dvisc	0.0017880	Pa×s	313.15	Properties of pure 1-methylimidazolium acetate ionic liquid and its binary mixtures with alcohols
dvisc	0.0029590	Pa×s	293.15	Viscosities of binary mixtures containing 1-butanol + 2,2,4-trimethylpentane or + 1,2,4-trimethylbenzene at high pressures for the thermophysical characterization of biofuels
dvisc	0.0017940	Pa×s	313.15	Viscosities of binary mixtures containing 1-butanol + 2,2,4-trimethylpentane or + 1,2,4-trimethylbenzene at high pressures for the thermophysical characterization of biofuels
dvisc	0.0011543	Pa×s	333.15	Viscosities of binary mixtures containing 1-butanol + 2,2,4-trimethylpentane or + 1,2,4-trimethylbenzene at high pressures for the thermophysical characterization of biofuels
dvisc	0.0007837	Pa×s	353.15	Viscosities of binary mixtures containing 1-butanol + 2,2,4-trimethylpentane or + 1,2,4-trimethylbenzene at high pressures for the thermophysical characterization of biofuels

dvisc	0.0014060	Pa×s	323.15	Thermophysical properties of 1,2,4-trimethylbenzene in admixtures with 1-butanol or 2-butanol at high pressures
dvisc	0.0011340	Pa×s	333.15	Thermophysical properties of 1,2,4-trimethylbenzene in admixtures with 1-butanol or 2-butanol at high pressures
dvisc	0.0022820	Pa×s	303.15	Viscosities and Densities of Binary Mixtures of 1,4-Dioxane, Carbon Tetrachloride, and Butanol at 303.15 K, 308.15 K, and 313.15 K
dvisc	0.0019073	Pa×s	308.15	Viscosities and Densities of Binary Mixtures of 1,4-Dioxane, Carbon Tetrachloride, and Butanol at 303.15 K, 308.15 K, and 313.15 K
dvisc	0.0018947	Pa×s	308.15	Viscosities and Densities of Binary Mixtures of 1,4-Dioxane, Carbon Tetrachloride, and Butanol at 303.15 K, 308.15 K, and 313.15 K
dvisc	0.0016813	Pa×s	313.15	Viscosities and Densities of Binary Mixtures of 1,4-Dioxane, Carbon Tetrachloride, and Butanol at 303.15 K, 308.15 K, and 313.15 K
dvisc	0.0026180	Pa×s	298.15	Excess Molar Volumes and Viscosity Deviations of Binary Mixtures of 2,4,6-Trimethyl-1,3,5-trioxane + Ethanol, 1-Propanol, and 1-Butanol at (298.15, 303.15, and 308.15) K

dvisc	0.0022970	Pa×s	303.15	Excess Molar Volumes and Viscosity Deviations of Binary Mixtures of 2,4,6-Trimethyl-1,3,5-trioxane + Ethanol, 1-Propanol, and 1-Butanol at (298.15, 303.15, and 308.15) K
dvisc	0.0020320	Pa×s	308.15	Excess Molar Volumes and Viscosity Deviations of Binary Mixtures of 2,4,6-Trimethyl-1,3,5-trioxane + Ethanol, 1-Propanol, and 1-Butanol at (298.15, 303.15, and 308.15) K
dvisc	0.0033460	Pa×s	288.15	Densities and Viscosities of Binary Mixtures of 1-Chlorobutane with Butanol Isomers at Several Temperatures
dvisc	0.0025600	Pa×s	298.15	Densities and Viscosities of Binary Mixtures of 1-Chlorobutane with Butanol Isomers at Several Temperatures
dvisc	0.0019910	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of 1-Chlorobutane with Butanol Isomers at Several Temperatures
dvisc	0.0015690	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of 1-Chlorobutane with Butanol Isomers at Several Temperatures

dvisc	0.0038690	Pa×s	283.15	Excess Enthalpy, Density, Viscosity, and Speed of Sound for the Mixture Tetrahydropyran + 1-Butanol at (283.15, 298.15 and, 313.15) K
dvisc	0.0025609	Pa×s	298.15	Excess Enthalpy, Density, Viscosity, and Speed of Sound for the Mixture Tetrahydropyran + 1-Butanol at (283.15, 298.15 and, 313.15) K
dvisc	0.0017567	Pa×s	313.15	Excess Enthalpy, Density, Viscosity, and Speed of Sound for the Mixture Tetrahydropyran + 1-Butanol at (283.15, 298.15 and, 313.15) K
dvisc	0.0025640	Pa×s	298.15	Viscosities, Densities, and Ultrasonic Velocities of Binary Mixtures of Ethylbenzene with Ethanol, 1-Propanol, and 1-Butanol at (298.15 and 308.15)K
dvisc	0.0020000	Pa×s	308.15	Viscosities, Densities, and Ultrasonic Velocities of Binary Mixtures of Ethylbenzene with Ethanol, 1-Propanol, and 1-Butanol at (298.15 and 308.15)K
dvisc	0.0033460	Pa×s	288.15	Densities and Viscosities of Binary Mixtures of 1-Bromobutane with Butanol Isomers at Several Temperatures

dvisc	0.0025600	Pa×s	298.15	Densities and Viscosities of Binary Mixtures of 1-Bromobutane with Butanol Isomers at Several Temperatures
dvisc	0.0019910	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of 1-Bromobutane with Butanol Isomers at Several Temperatures
dvisc	0.0015690	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of 1-Bromobutane with Butanol Isomers at Several Temperatures
dvisc	0.0022740	Pa×s	303.15	Densities, Viscosities, and Ultrasonic Velocity Studies of Binary Mixtures of Chloroform with Propan-1-ol and Butan-1-ol at (303.15 and 313.15) K
dvisc	0.0017830	Pa×s	313.15	Densities, Viscosities, and Ultrasonic Velocity Studies of Binary Mixtures of Chloroform with Propan-1-ol and Butan-1-ol at (303.15 and 313.15) K
dvisc	0.0025660	Pa×s	298.15	Density and Viscosity for Ethyl 3-Ethoxypropionate + Methacrylic Acid, + Benzyl Methacrylate, and + 2-Hydroxyethyl Methacrylate

dvisc	0.0022650	Pa×s	303.15	Density and Viscosity for Ethyl 3-Ethoxypropionate + Methacrylic Acid, + Benzyl Methacrylate, and + 2-Hydroxyethyl Methacrylate
dvisc	0.0019980	Pa×s	308.15	Density and Viscosity for Ethyl 3-Ethoxypropionate + Methacrylic Acid, + Benzyl Methacrylate, and + 2-Hydroxyethyl Methacrylate
dvisc	0.0017780	Pa×s	313.15	Density and Viscosity for Ethyl 3-Ethoxypropionate + Methacrylic Acid, + Benzyl Methacrylate, and + 2-Hydroxyethyl Methacrylate
dvisc	0.0038690	Pa×s	283.15	Excess Enthalpy, Density, Speed of Sound, and Viscosity for 2-Methyltetrahydrofuran + 1-Butanol at (283.15, 298.15, and, 313.15) K
dvisc	0.0025609	Pa×s	298.15	Excess Enthalpy, Density, Speed of Sound, and Viscosity for 2-Methyltetrahydrofuran + 1-Butanol at (283.15, 298.15, and, 313.15) K
dvisc	0.0017567	Pa×s	313.15	Excess Enthalpy, Density, Speed of Sound, and Viscosity for 2-Methyltetrahydrofuran + 1-Butanol at (283.15, 298.15, and, 313.15) K

dvisc	0.0029630	Pa×s	293.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0026190	Pa×s	298.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0022980	Pa×s	303.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0017860	Pa×s	313.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method

dvisc	0.0014210	Pa×s	323.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0011370	Pa×s	333.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0009200	Pa×s	343.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0007590	Pa×s	353.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method

dvisc	0.0006300	Pa×s	363.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0032860	Pa×s	288.15	Densities and Viscosities of Binary Mixtures of 1-Butanol with Methacrylic Acid, Benzyl Methacrylate, and 2-Hydroxyethyl Methacrylate between 288.15 K and 318.15 K
dvisc	0.0025660	Pa×s	298.15	Densities and Viscosities of Binary Mixtures of 1-Butanol with Methacrylic Acid, Benzyl Methacrylate, and 2-Hydroxyethyl Methacrylate between 288.15 K and 318.15 K
dvisc	0.0019980	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of 1-Butanol with Methacrylic Acid, Benzyl Methacrylate, and 2-Hydroxyethyl Methacrylate between 288.15 K and 318.15 K
dvisc	0.0015500	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of 1-Butanol with Methacrylic Acid, Benzyl Methacrylate, and 2-Hydroxyethyl Methacrylate between 288.15 K and 318.15 K

dvisc	0.0025768	Pa×s	298.15	Densities and Viscosities for Binary Mixtures of the Ionic Liquid N-Ethyl Piperazinium Propionate with n-Alcohols at Several Temperatures
dvisc	0.0022719	Pa×s	303.15	Densities and Viscosities for Binary Mixtures of the Ionic Liquid N-Ethyl Piperazinium Propionate with n-Alcohols at Several Temperatures
dvisc	0.0029410	Pa×s	293.15	Viscosity, density, and speed of sound of methylcyclopentane with primary and secondary alcohols at T = (293.15, 298.15, and 303.15) K
dvisc	0.0017856	Pa×s	313.15	Densities and Viscosities for Binary Mixtures of the Ionic Liquid N-Ethyl Piperazinium Propionate with n-Alcohols at Several Temperatures
dvisc	0.0017673	Pa×s	313.15	Densities and Viscosities of exo-Tetrahydrodicyclopentadiene + n-Butanol and exo-Tetrahydrodicyclopentadiene + n-Pentanol at Temperatures of (293.15 to 313.15) K
econd	8.00e-05	S/m	318.15	Electrical Conductivity of Caprolactam Tetrabutylammonium Bromide Ionic Liquids in Aqueous and Alcohol Binary Systems

econd	6.90e-05	S/m	313.15	Electrical Conductivity of Caprolactam Tetrabutylammonium Bromide Ionic Liquids in Aqueous and Alcohol Binary Systems	
econd	6.58e-05	S/m	308.15	Electrical Conductivity of Caprolactam Tetrabutylammonium Bromide Ionic Liquids in Aqueous and Alcohol Binary Systems	
econd	5.55e-05	S/m	303.15	Electrical Conductivity of Caprolactam Tetrabutylammonium Bromide Ionic Liquids in Aqueous and Alcohol Binary Systems	
econd	4.40e-05	S/m	298.15	Electrical Conductivity of Caprolactam Tetrabutylammonium Bromide Ionic Liquids in Aqueous and Alcohol Binary Systems	
hfust	9.37	kJ/mol	184.50	NIST Webbook	
hfust	9.28	kJ/mol	183.90	NIST Webbook	
hfust	9.28	kJ/mol	183.90	NIST Webbook	
hfust	9.28	kJ/mol	183.90	NIST Webbook	
hvapt	48.30	kJ/mol	363.50	NIST Webbook	
hvapt	49.50 ± 0.10	kJ/mol	333.00	NIST Webbook	
hvapt	49.00	kJ/mol	360.00	NIST Webbook	
hvapt	47.20	kJ/mol	374.00	NIST Webbook	
hvapt	37.40	kJ/mol	530.00	NIST Webbook	
hvapt	41.90	kJ/mol	458.00	NIST Webbook	
hvapt	43.80	kJ/mol	410.00	NIST Webbook	
hvapt	45.40	kJ/mol	386.50	NIST Webbook	
hvapt	51.60	kJ/mol	230.00	NIST Webbook	
hvapt	41.90	kJ/mol	481.50	NIST Webbook	
hvapt	50.10	kJ/mol	368.00	NIST Webbook	
hvapt	45.30	kJ/mol	387.50	NIST Webbook	
hvapt	45.30	kJ/mol	383.50	NIST Webbook	
hvapt	49.90	kJ/mol	352.50	NIST Webbook	
hvapt	20.80	kJ/mol	523.00	NIST Webbook	

hvapt	29.60	kJ/mol	473.00	NIST Webbook
hvapt	38.20	kJ/mol	423.00	NIST Webbook
hvapt	46.00	kJ/mol	373.00	NIST Webbook
hvapt	43.29	kJ/mol	390.90	NIST Webbook
hvapt	43.09	kJ/mol	390.60	KDB
hvapt	48.60 ± 0.10	kJ/mol	343.00	NIST Webbook
hvapt	47.50 ± 0.10	kJ/mol	353.00	NIST Webbook
hvapt	46.40 ± 0.10	kJ/mol	363.00	NIST Webbook
hvapt	55.00	kJ/mol	346.00	NIST Webbook
hvapt	53.00	kJ/mol	343.00	NIST Webbook
hvapt	45.40 ± 0.10	kJ/mol	381.00	NIST Webbook
hvapt	43.10 ± 0.10	kJ/mol	391.00	NIST Webbook
hvapt	42.10	kJ/mol	491.00	NIST Webbook
hvapt	46.60	kJ/mol	380.00	NIST Webbook
hvapt	48.30	kJ/mol	352.00	NIST Webbook
hvapt	47.20 ± 0.10	kJ/mol	356.00	NIST Webbook
kvisc	0.0000032	m2/s	298.15	Viscosities of Binary Mixtures of Isomeric Butanols or Isomeric Chlorobutanes with 2-Methyltetrahydrofuran
kvisc	0.0000022	m2/s	313.15	Viscosities of Binary Mixtures of Isomeric Butanols or Isomeric Chlorobutanes with 2-Methyltetrahydrofuran
pvap	53.33	kPa	373.74	Isobaric Vapor-Liquid Equilibria for Tetrahydropyran and Alcohol Systems
pvap	3.60	kPa	318.40	Vapor-Liquid Equilibrium for 1-Butanol + 1-Butene at (318.4 and 364.5) K and Vapor-Liquid Equilibrium of 1-Butanol + 2-Methylpropane, + n-Butane and 1-Butene + 2-Methylpropane at 318.4 K

pvap	3.60	kPa	318.35	Vapor-Liquid Equilibrium for 1-Butanol + 1-Butene at (318.4 and 364.5) K and Vapor-Liquid Equilibrium of 1-Butanol + 2-Methylpropane, + n-Butane and 1-Butene + 2-Methylpropane at 318.4 K
pvap	3.90	kPa	318.35	Vapor-Liquid Equilibrium for 1-Butanol + 1-Butene at (318.4 and 364.5) K and Vapor-Liquid Equilibrium of 1-Butanol + 2-Methylpropane, + n-Butane and 1-Butene + 2-Methylpropane at 318.4 K
pvap	98.66	kPa	390.04	Isobaric Vapor-Liquid Equilibria for Tetrahydropyran and Alcohol Systems
pvap	93.32	kPa	388.49	Isobaric Vapor-Liquid Equilibria for Tetrahydropyran and Alcohol Systems
pvap	36.30	kPa	364.52	Vapor-Liquid Equilibrium for 1-Butanol + 1-Butene at (318.4 and 364.5) K and Vapor-Liquid Equilibrium of 1-Butanol + 2-Methylpropane, + n-Butane and 1-Butene + 2-Methylpropane at 318.4 K
pvap	1.83	kPa	308.15	Isothermal Vapor-Liquid Equilibrium of (1-Butanol + 1,8-Cineole) at 10 Temperatures between (278.15 and 323.15) K

pvap	36.90	kPa	364.50	Vapour liquid equilibrium for the systems butane + methanol, +2-propanol, +1-butanol, +2-butanol, +2-methyl-2-propanol at 364.5K
pvap	101.30	kPa	390.65	Isobaric VLE data for the system of butan-1-ol + butylethanoate + 1-butyl-3-methylimidazoliumbis[(trifluoromethyl)sulfonyl]imide
pvap	2.51	kPa	313.15	Isothermal vapor liquid equilibrium and molar excess Gibbs energies of two ternary systems containing either 1-butanol or 2-butanol + 1-hexene + methylbenzene at 313.15 K
pvap	1.79	kPa	308.15	(Vapour + liquid) equilibria of (1-butanol + benzene, or toluene, or o-, or m-, or p-xylene) at T = 308.15 K
pvap	0.91	kPa	298.15	(Vapour + liquid) equilibrium and excess Gibbs functions of ternary mixtures containing 1-butanol or 2-butanol, n-hexane, and 1-chlorobutane at T = 298.15 K
pvap	25.30	kPa	356.35	Isobaric (vapour + liquid) equilibria for the (1-propanol + 1-butanol) binary mixture at (53.3 and 91.3) kPa
pvap	29.30	kPa	359.45	Isobaric (vapour + liquid) equilibria for the (1-propanol + 1-butanol) binary mixture at (53.3 and 91.3) kPa

pvap	33.50	kPa	362.95	Isobaric (vapour + liquid) equilibria for the (1-propanol + 1-butanol) binary mixture at (53.3 and 91.3) kPa
pvap	42.80	kPa	368.60	Isobaric (vapour + liquid) equilibria for the (1-propanol + 1-butanol) binary mixture at (53.3 and 91.3) kPa
pvap	52.50	kPa	373.45	Isobaric (vapour + liquid) equilibria for the (1-propanol + 1-butanol) binary mixture at (53.3 and 91.3) kPa
pvap	61.20	kPa	377.30	Isobaric (vapour + liquid) equilibria for the (1-propanol + 1-butanol) binary mixture at (53.3 and 91.3) kPa
pvap	72.80	kPa	381.90	Isobaric (vapour + liquid) equilibria for the (1-propanol + 1-butanol) binary mixture at (53.3 and 91.3) kPa
pvap	84.90	kPa	386.05	Isobaric (vapour + liquid) equilibria for the (1-propanol + 1-butanol) binary mixture at (53.3 and 91.3) kPa
pvap	105.30	kPa	391.95	Isobaric (vapour + liquid) equilibria for the (1-propanol + 1-butanol) binary mixture at (53.3 and 91.3) kPa
pvap	120.10	kPa	395.80	Isobaric (vapour + liquid) equilibria for the (1-propanol + 1-butanol) binary mixture at (53.3 and 91.3) kPa

pvap	2.48	kPa	313.15	Vapour-liquid equilibria of binary and ternary mixtures containing 1-butanol, 2,2,4-trimethylpentane and 1-hexene at T = 313.15 K
pvap	34.47	kPa	363.20	(Vapour + liquid) equilibria, (VLE) excess molar enthalpies and infinite dilution activity coefficients of selected binary systems involving n-hexyl pyridinium bis(trifluoromethylsulphonyl)imide ionic liquid: Experimental and predictions using modified UNIFAC (Dortmund)
pvap	14.44	kPa	343.39	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	13.71	kPa	343.36	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	13.52	kPa	343.20	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	21.03	kPa	352.70	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	32.09	kPa	360.58	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube

pvap	4.74	kPa	323.90	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.95	kPa	324.80	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	8.38	kPa	334.32	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	8.09	kPa	333.51	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.98	kPa	324.91	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	2.61	kPa	314.81	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	2.60	kPa	314.76	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	2.67	kPa	314.75	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	1.96	kPa	310.26	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube

pvap	1.90	kPa	310.29	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	1.46	kPa	305.59	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	1.92	kPa	310.16	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	1.09	kPa	301.02	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	1.91	kPa	310.29	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.62	kPa	323.50	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.91	kPa	324.57	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.87	kPa	324.59	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube

pvap	12.79	kPa	341.78	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.48	kPa	322.58	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.85	kPa	324.28	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.52	kPa	322.69	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.33	kPa	322.07	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.69	kPa	323.67	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.75	kPa	323.78	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	79.99	kPa	384.26	Isobaric Vapor-Liquid Equilibria for Tetrahydropyran and Alcohol Systems
pvap	4.15	kPa	321.34	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube

pvap	4.19	kPa	321.34	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.54	kPa	323.09	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	2.50	kPa	314.76	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	4.79	kPa	324.18	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube
pvap	101.47	kPa	390.69	Vapor-Liquid Equilibrium of Binary Mixtures Containing Isopropyl Acetate and Alkanols at 101.32 kPa
pvap	127.02	kPa	397.19	Vapor-Liquid Equilibrium of Binary Mixtures Containing Isopropyl Acetate and Alkanols at 101.32 kPa
pvap	152.42	kPa	402.79	Vapor-Liquid Equilibrium of Binary Mixtures Containing Isopropyl Acetate and Alkanols at 101.32 kPa
pvap	177.83	kPa	407.58	Vapor-Liquid Equilibrium of Binary Mixtures Containing Isopropyl Acetate and Alkanols at 101.32 kPa
pvap	203.23	kPa	411.88	Vapor-Liquid Equilibrium of Binary Mixtures Containing Isopropyl Acetate and Alkanols at 101.32 kPa

pvap	228.64	kPa	415.88	Vapor-Liquid Equilibrium of Binary Mixtures Containing Isopropyl Acetate and Alkanols at 101.32 kPa
pvap	85.00	kPa	385.75	Experimental Vapor-Liquid Equilibria and Thermodynamic Modeling of the Methanol + n-Heptane and 1-Butanol + Aniline Binary Systems
pvap	0.56	kPa	293.15	Dibutyl Citrate Synthesis, Physicochemical Characterization, and Px Data in Mixtures with Butanol
pvap	0.84	kPa	298.15	Dibutyl Citrate Synthesis, Physicochemical Characterization, and Px Data in Mixtures with Butanol
pvap	1.23	kPa	303.15	Dibutyl Citrate Synthesis, Physicochemical Characterization, and Px Data in Mixtures with Butanol
pvap	1.76	kPa	308.15	Dibutyl Citrate Synthesis, Physicochemical Characterization, and Px Data in Mixtures with Butanol
pvap	2.44	kPa	313.15	Dibutyl Citrate Synthesis, Physicochemical Characterization, and Px Data in Mixtures with Butanol
pvap	3.33	kPa	318.15	Dibutyl Citrate Synthesis, Physicochemical Characterization, and Px Data in Mixtures with Butanol

pvap	4.35	kPa	323.15	Dibutyl Citrate Synthesis, Physicochemical Characterization, and Px Data in Mixtures with Butanol
pvap	5.33	kPa	328.15	Dibutyl Citrate Synthesis, Physicochemical Characterization, and Px Data in Mixtures with Butanol
pvap	101.30	kPa	390.75	Vapor-Liquid Equilibrium for Binary of 1-Butanol + N,N-Dimethylacetamide and Methyl Isobutyl Ketone + N,N-Dimethylacetamide at 101.3 kPa
pvap	2.70	kPa	314.19	Vapor-Liquid Equilibrium Studies for Systems Containing n-Butylisocyanate at Temperatures between 323.15 K and 371.15 K
pvap	4.49	kPa	323.20	Vapor-Liquid Equilibrium Studies for Systems Containing n-Butylisocyanate at Temperatures between 323.15 K and 371.15 K
pvap	10.38	kPa	338.21	Vapor-Liquid Equilibrium Studies for Systems Containing n-Butylisocyanate at Temperatures between 323.15 K and 371.15 K
pvap	12.89	kPa	342.17	Vapor-Liquid Equilibrium Studies for Systems Containing n-Butylisocyanate at Temperatures between 323.15 K and 371.15 K

pvap	21.44	kPa	352.81	Vapor-Liquid Equilibrium Studies for Systems Containing n-Butylisocyanate at Temperatures between 323.15 K and 371.15 K
pvap	31.52	kPa	361.24	Vapor-Liquid Equilibrium Studies for Systems Containing n-Butylisocyanate at Temperatures between 323.15 K and 371.15 K
pvap	49.26	kPa	371.94	Vapor-Liquid Equilibrium Studies for Systems Containing n-Butylisocyanate at Temperatures between 323.15 K and 371.15 K
pvap	1.00	kPa	298.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data
pvap	1.32	kPa	303.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data
pvap	1.84	kPa	308.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data

pvap	2.54	kPa	313.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data
pvap	3.45	kPa	318.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data
pvap	4.65	kPa	323.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data
pvap	6.17	kPa	328.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data
pvap	8.10	kPa	333.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data

pvap	10.56	kPa	338.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data
pvap	13.60	kPa	343.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data
pvap	17.37	kPa	348.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data
pvap	21.98	kPa	353.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data
pvap	27.65	kPa	358.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data

pvap	34.41	kPa	363.15	Vapor-Pressure Measurements of Liquid Solutions at Different Temperatures: Apparatus for Use over an Extended Temperature Range and Some New Data
pvap	833.00	kPa	468.15	Isothermal Vapor-Liquid Equilibria for the n-Pentane + 1-Butanol and n-Pentane + 2-Butanol Systems near the Critical Region of the Mixtures
pvap	1182.00	kPa	483.15	Isothermal Vapor-Liquid Equilibria for the n-Pentane + 1-Butanol and n-Pentane + 2-Butanol Systems near the Critical Region of the Mixtures
pvap	1558.00	kPa	498.15	Isothermal Vapor-Liquid Equilibria for the n-Pentane + 1-Butanol and n-Pentane + 2-Butanol Systems near the Critical Region of the Mixtures
pvap	2027.00	kPa	513.15	Isothermal Vapor-Liquid Equilibria for the n-Pentane + 1-Butanol and n-Pentane + 2-Butanol Systems near the Critical Region of the Mixtures

pvap	4.61	kPa	323.15	Vapor-Liquid Equilibria and HE for Binary Systems of Dimethyl Ether (DME) with C1-C4 Alkan-1-ols at 323.15 K and Liquid-Liquid Equilibria for Ternary System of DME + Methanol + Water at 313.15 K
pvap	0.20	kPa	278.15	Isothermal Vapor-Liquid Equilibrium of (1-Butanol + 1,8-Cineole) at 10 Temperatures between (278.15 and 323.15) K
pvap	0.31	kPa	283.15	Isothermal Vapor-Liquid Equilibrium of (1-Butanol + 1,8-Cineole) at 10 Temperatures between (278.15 and 323.15) K
pvap	0.45	kPa	288.15	Isothermal Vapor-Liquid Equilibrium of (1-Butanol + 1,8-Cineole) at 10 Temperatures between (278.15 and 323.15) K
pvap	0.66	kPa	293.15	Isothermal Vapor-Liquid Equilibrium of (1-Butanol + 1,8-Cineole) at 10 Temperatures between (278.15 and 323.15) K
pvap	0.94	kPa	298.15	Isothermal Vapor-Liquid Equilibrium of (1-Butanol + 1,8-Cineole) at 10 Temperatures between (278.15 and 323.15) K
pvap	1.32	kPa	303.15	Isothermal Vapor-Liquid Equilibrium of (1-Butanol + 1,8-Cineole) at 10 Temperatures between (278.15 and 323.15) K

pvap	66.66	kPa	379.43	Isobaric Vapor-Liquid Equilibria for Tetrahydropyran and Alcohol Systems
pvap	2.53	kPa	313.15	Isothermal Vapor-Liquid Equilibrium of (1-Butanol + 1,8-Cineole) at 10 Temperatures between (278.15 and 323.15) K
pvap	3.44	kPa	318.15	Isothermal Vapor-Liquid Equilibrium of (1-Butanol + 1,8-Cineole) at 10 Temperatures between (278.15 and 323.15) K
pvap	4.54	kPa	323.15	Isothermal Vapor-Liquid Equilibrium of (1-Butanol + 1,8-Cineole) at 10 Temperatures between (278.15 and 323.15) K
pvap	60.00	kPa	376.78	Isobaric Vapor Liquid Equilibria for the 1-Propanol + Ethylene Glycol Monopropyl Ether and 1-Butanol + Ethylene Glycol Monopropyl Ether Systems
pvap	80.00	kPa	384.28	Isobaric Vapor Liquid Equilibria for the 1-Propanol + Ethylene Glycol Monopropyl Ether and 1-Butanol + Ethylene Glycol Monopropyl Ether Systems
pvap	100.00	kPa	390.28	Isobaric Vapor Liquid Equilibria for the 1-Propanol + Ethylene Glycol Monopropyl Ether and 1-Butanol + Ethylene Glycol Monopropyl Ether Systems

pvap	101.30	kPa	390.65	Vapor Liquid Equilibrium at p/kPa = 101.3 of the Binary Mixtures of Ethenyl Acetate with Methanol and Butan-1-ol
pvap	8.39	kPa	333.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	110.26	kPa	393.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	101.30	kPa	390.48	Phase Equilibrium (VLE, LLE, and VLLE) Data of the Ternary System: Ionic Liquid [OMIM][PF6] + Butan-1-ol + Butyl Acetate
pvap	101.30	kPa	390.49	Vapor Liquid Equilibria Measurements for the Nine n-Alkane/Ketone Pairs Comprising 2-, 3-, and 4-Heptanone with n-Octane, n-Nonane, and n-Decane
pvap	40.00	kPa	366.76	Isobaric Vapor-Liquid Equilibria for Tetrahydropyran and Alcohol Systems
pvap	4.54	kPa	323.14	Thermogravimetric measurement of evaporation: Data analysis based on the Stefan tube

rfi	1.39523	303.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.39686	298.15	Liquid-Liquid Equilibrium in Binary System [bmim][PF6] + 1-Butanol
rfi	1.39300	308.15	Densities, Excess Molar Volumes, and Refractive Properties of the Binary Mixtures of the Amino Acid Ionic Liquid [bmim][Gly] with 1-Butanol or Isopropanol at T = (298.15 to 313.15) K
rfi	1.39500	303.15	Densities, Excess Molar Volumes, and Refractive Properties of the Binary Mixtures of the Amino Acid Ionic Liquid [bmim][Gly] with 1-Butanol or Isopropanol at T = (298.15 to 313.15) K
rfi	1.39700	298.15	Densities, Excess Molar Volumes, and Refractive Properties of the Binary Mixtures of the Amino Acid Ionic Liquid [bmim][Gly] with 1-Butanol or Isopropanol at T = (298.15 to 313.15) K
rfi	1.39730	298.15	Excess Molar Enthalpies of 2-Methyl-2-butanol (1) + 1-Alkanols (C1-C5) (2) at 298.15 K

rfi	1.39730	298.15	Volumetric Behavior of Carbon Dioxide + Butan-1-ol Mixtures at 313.15 K
rfi	1.39740	298.15	Excess Molar Enthalpies of Benzyl Alcohol + Alkanols (C1-C6) and Their Correlations at 298.15 K and Ambient Pressure
rfi	1.39100	313.15	Densities, Excess Molar Volumes, and Refractive Properties of the Binary Mixtures of the Amino Acid Ionic Liquid [bmim][Gly] with 1-Butanol or Isopropanol at T = (298.15 to 313.15) K
rfi	1.39930	293.15	Liquid-Liquid Equilibria of Water + 3-Hydroxy-2-butanone + 1-Butanol
rfi	1.39730	298.15	Isothermal Vapor Liquid Equilibrium Data of Propan-1-ol + 2,2,4-Trimethylpentane and Butan-1-ol + 2,2,4-Trimethylpentane at 318.15 K
rfi	1.39730	298.15	Density, Viscosity, and Refractive Index Properties for the Binary Mixtures of n-Butylammonium Acetate Ionic Liquid + Alkanols at Several Temperatures
rfi	1.39930	293.20	Vapor Liquid Equilibrium Data for Binary Systems of 1-Methyl-4-(1-methylethenyl)-cyclohexene + {Ethanol, Propan-1-ol, Propan-2-ol, Butan-1-ol, Pentan-1-ol, or Hexan-1-ol} at 40 kPa

rfi	1.39930	293.20	Vapor Liquid Equilibrium Data for Binary Systems of 1H-Pyrrole with Butan-1-ol, Propan-1-ol, or Pentan-1-ol
rfi	1.39720	298.15	Vapor Liquid Equilibria, Excess Enthalpy, and Excess Volume of Binary Mixtures Containing an Alcohol (1-Butanol, 2-Butanol, or 2-Methyl-2-butanol) and 2-Ethoxy-2-methylbutane
rfi	1.39920	293.15	Vapor Liquid Equilibrium Data for 1-Methyl-2-Pyrrolidone + (1-Butanol or 1-Hexene or Water) Binary Mixtures
rfi	1.39920	293.15	Vapor Liquid Equilibrium Data for Binary Systems of n-Dodecane + {Propan-1-ol, Butan-1-ol, 2-Methylpropan-1-ol} at 40 kPa
rfi	1.39928	293.15	Ternary Liquid Liquid Equilibrium Data for the Water + Acetonitrile + {Butan-1-ol or 2-Methylpropan-1-ol} Systems at (303.2, 323.2, 343.2) K and 1 atm
rfi	1.39726	298.15	Experimental Liquid-Liquid Equilibria of 1-Alkyl-3-methylimidazolium Hexafluorophosphate with 1-Alcohols
rfi	1.39600	298.15	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa

rfi	1.39970	293.15	Densities, Excess Molar Volumes, and Isobaric Thermal Expansibilities for 1,2-Ethanediol + 1-Butanol, or 1-Hexanol, or 1-Octanol in the Temperature Range from (293.15 to 313.15) K
rfi	1.39780	298.15	Densities, Excess Molar Volumes, and Isobaric Thermal Expansibilities for 1,2-Ethanediol + 1-Butanol, or 1-Hexanol, or 1-Octanol in the Temperature Range from (293.15 to 313.15) K
rfi	1.39940	293.15	Refractive Indices and Deviations in Refractive Indices for Binary Mixtures of Formamide + 1-Butanol, + 2-Butanol, + 1,3-Butanediol, and + 1,4-Butanediol at Temperatures from (293.15 to 318.15) K
rfi	1.39740	298.15	Refractive Indices and Deviations in Refractive Indices for Binary Mixtures of Formamide + 1-Butanol, + 2-Butanol, + 1,3-Butanediol, and + 1,4-Butanediol at Temperatures from (293.15 to 318.15) K

rfi

1.39530

303.15

Refractive
Indices and
Deviations in
Refractive
Indices for Binary
Mixtures of
Formamide +
1-Butanol, +
2-Butanol, +
1,3-Butanediol,
and +
1,4-Butanediol at
Temperatures
from (293.15 to
318.15) K

rfi

1.39330

308.15

Refractive
Indices and
Deviations in
Refractive
Indices for Binary
Mixtures of
Formamide +
1-Butanol, +
2-Butanol, +
1,3-Butanediol,
and +
1,4-Butanediol at
Temperatures
from (293.15 to
318.15) K

rfi

1.39130

313.15

Refractive
Indices and
Deviations in
Refractive
Indices for Binary
Mixtures of
Formamide +
1-Butanol, +
2-Butanol, +
1,3-Butanediol,
and +
1,4-Butanediol at
Temperatures
from (293.15 to
318.15) K

rfi

1.38930

318.15

Refractive
Indices and
Deviations in
Refractive
Indices for Binary
Mixtures of
Formamide +
1-Butanol, +
2-Butanol, +
1,3-Butanediol,
and +
1,4-Butanediol at
Temperatures
from (293.15 to
318.15) K

rfi	1.39720	298.15	Effect of Pressure on the Static Relative Permittivities of Alkan-1-ols at 298.15 K
rfi	1.39740	298.15	Excess Molar Enthalpies of 1,2-Propanediol + Alkan-1-ols (C1-C6) and Their Correlations at 298.15 K and Ambient Pressure (81.5 kPa)
rfi	1.39370	308.15	Density, Viscosity, Refractive Index, and Speed of Sound for Binary Mixtures of 1,4-Dioxane with Different Organic Liquids at (298.15, 303.15, and 308.15) K
rfi	1.39550	303.15	Density, Viscosity, Refractive Index, and Speed of Sound for Binary Mixtures of 1,4-Dioxane with Different Organic Liquids at (298.15, 303.15, and 308.15) K
rfi	1.39830	298.15	Density, Viscosity, Refractive Index, and Speed of Sound for Binary Mixtures of 1,4-Dioxane with Different Organic Liquids at (298.15, 303.15, and 308.15) K
rfi	1.39730	298.15	Density, Surface Tension, and Refractive Index of Octane + 1-Alkanol Mixtures at T) 298.15 K.

rfi	1.39920	293.15	Limiting Activity Coefficients by Comparative Tensimetry: 1-Propanol and 1-Butanol in Heptane and in Octane
rfi	1.39320	308.15	Excess Molar Volumes, Viscosities, and Refractive Indexes for Binary Mixtures of 1-Chlorobutane with Four Alcohols at T = (288.15, 298.15 and 308.15) K
rfi	1.39720	298.15	Excess Molar Volumes, Viscosities, and Refractive Indexes for Binary Mixtures of 1-Chlorobutane with Four Alcohols at T = (288.15, 298.15 and 308.15) K
rfi	1.40100	288.15	Excess Molar Volumes, Viscosities, and Refractive Indexes for Binary Mixtures of 1-Chlorobutane with Four Alcohols at T = (288.15, 298.15 and 308.15) K
rfi	1.39740	298.15	Bubble-Temperature Measurements on Some Binary Mixtures Formed by Tetrahydrofuran or Amyl Alcohol with Hydrocarbons, Chlorohydrocarbons, or Butanols at (94.6 or 95.8) kPa

rfi	1.39800	298.15	Bubble Temperatures of the Binary Mixtures of Dimethylcarbonate with Some Alcohols at 95.8 kPa
rfi	1.39890	293.15	Solubility Data for Roflumilast and Maraviroc in Various Solvents between T = (278.2-323.2) K
rfi	1.39860	293.15	Solid-Liquid Equilibrium Measurements for Posaconazole and Voriconazole in Several Solvents between T = 278.2 and 323.2 K Using Differential Thermal Analysis/Thermal Gravimetric Analysis
rfi	1.39890	293.15	Isothermal Vapor-Liquid Equilibrium Measurements for the Pentan-2-one + Propan-1-ol/Butan-1-ol System within 342-363 K
rfi	1.39318	308.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.39940	293.15	Liquid Liquid Equilibrium Data of Water + Butyric Acid + {Butanal or n-Butanol} Ternary Systems at 293.15, 308.15, and 323.15 K

rfi	1.38688	323.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.38901	318.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.39110	313.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.39318	308.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K

rfi	1.39523	303.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.39730	298.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.39932	293.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K
rfi	1.40135	288.15	Experimental Determination and Modeling of Densities, Refractive Indices of the Binary Mixtures of Dimethylphthalate (or Dimethyladipate) + 1-Butanol, or + 2-Butanol, or + 2-Butanone at T = (288.15 to 323.15) K

rfi	1.38688	323.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.38901	318.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.39110	313.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.39460	303.15	Measurements of the Properties of Binary Mixtures of Dimethylsulphoxide (DMSO) with 1-Alkanols (C4, C6, C7) at 303.15K
rfi	1.39730	298.15	Isobaric Vapor Liquid Equilibria of 1-Butanol p-Xylene System1
rfi	1.39930	293.15	Vapor liquid equilibria and excess volumes of the binary systems ethanol + ethyl lactate, isopropanol + isopropyl lactate and n-butanol + n-butyl lactate at 101.325 kPa

rfi	1.39740	298.15	Activity coefficients of the binary mixtures of a-cresol or p-cresol with C1-C4 aliphatic alcohols near ambient pressure
rfi	1.39760	298.15	Isobaric vapor-liquid equilibria for the binary systems 1-propyl alcohol + dipropyl ether and 1-butyl alcohol + dibutyl ether at 20 and 101.3 kPa
rfi	1.39732	298.15	Isobaric vapour liquid equilibria for the binary systems 4-methyl-2-pentanone + 1-butanol and + 2-butanol at 20 and 101.3 kPa
rfi	1.39740	298.15	Excess molar volumes, excess molar enthalpies and refractive index deviations for binary mixtures of propan-1-ol, butan-1-ol and pentan-1-ol with 2,2,4-trimethylpentane at 298.15 K
rfi	1.40130	288.20	Experimental and calculated liquid-liquid equilibrium data for water + furfural + solvents
rfi	1.39520	303.20	Experimental and calculated liquid-liquid equilibrium data for water + furfural + solvents
rfi	1.38920	318.20	Experimental and calculated liquid-liquid equilibrium data for water + furfural + solvents

rfi	1.39950	298.15	Investigation on vapor liquid equilibrium for 2-propanol + 1-butanol + 1-pentanol at 101.3 kPa
rfi	1.39830	293.20	Liquid-liquid equilibrium data for systems containing of formic acid, water, and primary normal alcohols at T = 298.2 K
rfi	1.39730	298.15	Isobaric (vapor+liquid) equilibrium for n-propyl acetate with 1-butanol or 2-butanol. Binary mixtures at 0.15 and 0.6 MPa
rfi	1.39886	298.15	Atmospheric densities and interfacial tensions for 1-alkanol (1-butanol to 1-octanol) + water and ether (MTBE, ETBE, DIPE, TAME and THP) + water demixed mixtures.
rfi	1.39700	298.15	Excess molar volumes and partial molar volumes for (propionitrile + an alkanol) at T = 298.15 K and p = 0.1 MPa
rfi	1.39970	293.15	Measurement and Correlation of the Solubilities of m-Phthalic Acid in Monobasic Alcohols

rfi	1.39590	303.15	Physico-chemical and excess properties of the binary mixtures of methylcyclohexane + ethanol, + propan-1-ol, + propan-2-ol, + butan-1-ol, + 2-methyl-1-propanol, or 3-methyl-1-butanol at T = (298.15, 303.15, and 308.15) K
rfi	1.39400	308.15	Physico-chemical and excess properties of the binary mixtures of methylcyclohexane + ethanol, + propan-1-ol, + propan-2-ol, + butan-1-ol, + 2-methyl-1-propanol, or 3-methyl-1-butanol at T = (298.15, 303.15, and 308.15) K
rfi	1.39680	298.15	Thermodynamic properties of (tetradecane + benzene, + toluene, + chlorobenzene, + bromobenzene, + anisole) binary mixtures at T = (298.15, 303.15, and 308.15) K
rfi	1.39440	303.15	Thermodynamic properties of (tetradecane + benzene, + toluene, + chlorobenzene, + bromobenzene, + anisole) binary mixtures at T = (298.15, 303.15, and 308.15) K
rfi	1.39230	308.15	Thermodynamic properties of (tetradecane + benzene, + toluene, + chlorobenzene, + bromobenzene, + anisole) binary mixtures at T = (298.15, 303.15, and 308.15) K

rfi	1.39740	298.15	(Vapor + liquid) equilibria of the binary mixtures of m-cresol with C1 C4 aliphatic alcohols at 95.5 kPa
rfi	1.39680	298.15	Thermodynamic interactions in binary mixtures of anisole with ethanol, propan-1-ol, propan-2-ol, butan-1-ol, pentan-1-ol, and 3-methylbutan-1-ol at T = (298.15, 303.15, and 308.15) K
rfi	1.39440	303.15	Thermodynamic interactions in binary mixtures of anisole with ethanol, propan-1-ol, propan-2-ol, butan-1-ol, pentan-1-ol, and 3-methylbutan-1-ol at T = (298.15, 303.15, and 308.15) K
rfi	1.39230	308.15	Thermodynamic interactions in binary mixtures of anisole with ethanol, propan-1-ol, propan-2-ol, butan-1-ol, pentan-1-ol, and 3-methylbutan-1-ol at T = (298.15, 303.15, and 308.15) K
rfi	1.39740	298.15	Excess Gibbs free energies of the binary mixtures of acetonitrile with butanols at 94.83 kPa

rfi	1.39479	303.15	Density, viscosity, refractive index, excess molar enthalpy, viscosity, and refractive index deviations for the (1-butanol + 2-butanone) binary system at T = 303 K. A new adiabatic calorimeter for heat of mixing
rfi	1.39729	298.15	Thermophysical properties of the binary mixtures (1,8-cineole + 1-alkanol) at T = (298.15 and 313.15) K and at atmospheric pressure
rfi	1.39114	313.15	Thermophysical properties of the binary mixtures (1,8-cineole + 1-alkanol) at T = (298.15 and 313.15) K and at atmospheric pressure
rfi	1.39640	298.15	Application of the ERAS model to volumetric properties of binary mixtures of banana oil with primary and secondary alcohols (C1- C4) at different temperatures
rfi	1.39620	303.15	Experimental study on the calorimetric data of cyclohexanol with alkanols (C1-C4) and correlation with Wilson, NRTL and UNIQUAC models at 300 K

rfi	1.39747	298.15	Densities, speeds of sound, and refractive indices for binary mixtures of 1-butyl-3-methylimidazolium methyl sulphate ionic liquid with alcohols at T = (298.15, 303.15, 308.15, and 313.15) K
rfi	1.39549	303.15	Densities, speeds of sound, and refractive indices for binary mixtures of 1-butyl-3-methylimidazolium methyl sulphate ionic liquid with alcohols at T = (298.15, 303.15, 308.15, and 313.15) K
rfi	1.39342	308.15	Densities, speeds of sound, and refractive indices for binary mixtures of 1-butyl-3-methylimidazolium methyl sulphate ionic liquid with alcohols at T = (298.15, 303.15, 308.15, and 313.15) K
rfi	1.39138	313.15	Densities, speeds of sound, and refractive indices for binary mixtures of 1-butyl-3-methylimidazolium methyl sulphate ionic liquid with alcohols at T = (298.15, 303.15, 308.15, and 313.15) K
rfi	1.39720	298.15	Properties of pure n-butylammonium nitrate ionic liquid and its binary mixtures of with alcohols at T = (293.15 to 313.15) K

rfi	1.39733	298.15	Volumetric behaviour of the (2,2,4-trimethylpentane + methylbenzene + butan-1-ol) ternary system and its binary sub-systems within the temperature range (298.15-328.15) K
rfi	1.39720	298.15	Thermodynamic and acoustic properties of binary mixtures of 1-butanol with 1,2-butanediol. The comparison with the results for 1,3-, and 1,4-butanediol
rfi	1.39680	298.20	Tie line data for the (water + butyric acid + n-butyl alcohol or amyl alcohol) at T = (298.2, 308.2, and 318.2) K and (water + butyric acid + isoamyl alcohol) at T = 298.2 K
rfi	1.39733	298.15	Volumetric behavior of the ternary system (methyl tert-butyl ether + methylbenzene + butan-1-ol) and its binary sub-system (methyl tert-butyl ether + butan-1-ol) within the temperature range (298.15 to 328.15) K
rfi	1.39930	293.15	Separation of water/butan-1-ol with ionic liquids in ternary liquid-liquid phase equilibrium

rfi	1.40135	288.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.39932	293.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.39730	298.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.39700	298.15	Experimental Binary VLE Data of Morpholine with 1-Butanol and 3-Methyl-1-butanol Systems
rfi	1.39830	298.15	Physico-chemical and excess properties of the binary mixtures of methylcyclohexane + ethanol, + propan-1-ol, + propan-2-ol, + butan-1-ol, + 2-methyl-1-propanol, or 3-methyl-1-butanol at T = (298.15, 303.15, and 308.15) K

rhoI	805.80	kg/m3	298.15	Apparent Molal Volumes and Viscosity B-Coefficients of Acetyl Salicylic Acid (2-Acetoxy Benzoic Acid) Solutions in Higher Alcohols at Different Temperatures
rhoI	805.87	kg/m3	298.15	Binary Liquid-Liquid Equilibrium (LLE) for Methyl tert-Amyl Ether (TAME) + Water from (288.15 to 313.15) K and Ternary LLE for Systems of TAME + C1-C4 Alcohols + Water at 298.15 K
rhoI	805.85	kg/m3	298.15	Binary Liquid-Liquid Equilibrium (LLE) for Dibutyl Ether (DBE) + Water from (288.15 to 318.15) K and Ternary LLE for Systems of DBE + C1 less than C4 Alcohols + Water at 298.15 K
rhoI	805.76	kg/m3	298.15	Liquid Liquid Equilibrium for Ternary Systems of Propyl Vinyl Ether + C3 or C4 Alcohols + Water at 298.15 K and Excess Molar Enthalpies for Ternary and Constituent Binary Systems of Propyl Vinyl Ether + Ethanol + Isooctane at 303.15 K
rhoI	805.92	kg/m3	298.15	Densities and Excess Molar Volumes of N-Methylmorpholine + 1-Alkanol Systems at 298.15 K

rhoI	790.27	kg/m3	318.15	Thermodynamic Properties of 1-Butyl-3-methylpyridinium Tetrafluoroborate and Its Mixtures with Water and Alkanols
rhoI	805.95	kg/m3	298.15	Thermodynamic Properties of 1-Butyl-3-methylpyridinium Tetrafluoroborate and Its Mixtures with Water and Alkanols
rhoI	786.25	kg/m3	323.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	790.24	kg/m3	318.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	794.19	kg/m3	313.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	798.10	kg/m3	308.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rhoI	801.97	kg/m3	303.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform

rho	805.81	kg/m ³	298.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rho	809.61	kg/m ³	293.15	Speed of sound, density and related thermodynamic excess properties of binary mixtures of butan-2-one with C1-C4 nalkanols and chloroform
rho	786.29	kg/m ³	323.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rho	790.28	kg/m ³	318.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rho	794.22	kg/m ³	313.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rho	798.12	kg/m ³	308.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rho	801.99	kg/m ³	303.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rho	805.84	kg/m ³	298.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rho	809.66	kg/m ³	293.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols

rhoI	813.46	kg/m3	288.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rhoI	778.01	kg/m3	333.15	Densities, Refractive Indices, Viscosities, and Spectroscopic Study of 1-Amino-2-propanol + 1-Butanol and + 2-Butanol Solutions at (288.15 to 333.15) K
rhoI	782.12	kg/m3	328.15	Densities, Refractive Indices, Viscosities, and Spectroscopic Study of 1-Amino-2-propanol + 1-Butanol and + 2-Butanol Solutions at (288.15 to 333.15) K
rhoI	786.18	kg/m3	323.15	Densities, Refractive Indices, Viscosities, and Spectroscopic Study of 1-Amino-2-propanol + 1-Butanol and + 2-Butanol Solutions at (288.15 to 333.15) K
rhoI	790.18	kg/m3	318.15	Densities, Refractive Indices, Viscosities, and Spectroscopic Study of 1-Amino-2-propanol + 1-Butanol and + 2-Butanol Solutions at (288.15 to 333.15) K

rhoI	794.13	kg/m3	313.15	Densities, Refractive Indices, Viscosities, and Spectroscopic Study of 1-Amino-2-propanol + 1-Butanol and + 2-Butanol Solutions at (288.15 to 333.15) K
rhoI	798.04	kg/m3	308.15	Densities, Refractive Indices, Viscosities, and Spectroscopic Study of 1-Amino-2-propanol + 1-Butanol and + 2-Butanol Solutions at (288.15 to 333.15) K
rhoI	801.91	kg/m3	303.15	Densities, Refractive Indices, Viscosities, and Spectroscopic Study of 1-Amino-2-propanol + 1-Butanol and + 2-Butanol Solutions at (288.15 to 333.15) K
rhoI	805.75	kg/m3	298.15	Densities, Refractive Indices, Viscosities, and Spectroscopic Study of 1-Amino-2-propanol + 1-Butanol and + 2-Butanol Solutions at (288.15 to 333.15) K
rhoI	809.56	kg/m3	293.15	Densities, Refractive Indices, Viscosities, and Spectroscopic Study of 1-Amino-2-propanol + 1-Butanol and + 2-Butanol Solutions at (288.15 to 333.15) K

rhoI	813.35	kg/m3	288.15	Densities, Refractive Indices, Viscosities, and Spectroscopic Study of 1-Amino-2-propanol + 1-Butanol and + 2-Butanol Solutions at (288.15 to 333.15) K
rhoI	778.16	kg/m3	333.15	Densities and Viscosities of Diaminotoluene with Water, Ethanol, Propan-1-ol, and Butan-1-ol from (293.15 to 333.15) K
rhoI	786.32	kg/m3	323.15	Densities and Viscosities of Diaminotoluene with Water, Ethanol, Propan-1-ol, and Butan-1-ol from (293.15 to 333.15) K
rhoI	794.27	kg/m3	313.15	Densities and Viscosities of Diaminotoluene with Water, Ethanol, Propan-1-ol, and Butan-1-ol from (293.15 to 333.15) K
rhoI	802.04	kg/m3	303.15	Densities and Viscosities of Diaminotoluene with Water, Ethanol, Propan-1-ol, and Butan-1-ol from (293.15 to 333.15) K
rhoI	809.69	kg/m3	293.15	Densities and Viscosities of Diaminotoluene with Water, Ethanol, Propan-1-ol, and Butan-1-ol from (293.15 to 333.15) K

rhoI	786.21	kg/m3	323.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure
rhoI	790.18	kg/m3	318.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure
rhoI	794.10	kg/m3	313.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure
rhoI	797.99	kg/m3	308.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure
rhoI	801.86	kg/m3	303.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure

rhoI	805.70	kg/m3	298.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure	
rhoI	809.53	kg/m3	293.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure	
rhoI	805.71	kg/m3	298.15	Thermophysical Properties of the Pure Ionic Liquid 1-Butyl-1-methylpyrrolidinium Dicyanamide and Its Binary Mixtures with Alcohols	
rhoI	809.50	kg/m3	293.15	Isobaric vapor liquid equilibrium for the binary systems of 1-butanol with o-xylene, m-xylene, p-xylene, and ethylbenzene at 101.33 kPa	
rhoI	805.71	kg/m3	298.15	ACSExcess Molar Enthalpies of Mixtures of (+-)-Linalool with Several Alkanols	
rhoI	805.95	kg/m3	298.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Ethylenediamine with Alcohols at T = (293.15 to 313.15) K	

rhoI	805.80	kg/m3	298.15	Surface Tensions of the Ternary Mixtures Containing an Isomeric Butanol + n-Hexane + 1-Chlorobutane at 298.15 K
rhoI	778.03	kg/m3	333.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhoI	782.48	kg/m3	328.15	Excess Molar Volumes of 1,3-Diethyl Propanedioate with Methanol, Ethanol, Propan-1-ol, Propan-2-ol, Butan-2-ol, 2-Methyl-propan-1-ol, and Pentan-1-ol at T = (288.15, 298.15, 313.15, and 328.15) K
rhoI	794.49	kg/m3	313.15	Excess Molar Volumes of 1,3-Diethyl Propanedioate with Methanol, Ethanol, Propan-1-ol, Propan-2-ol, Butan-2-ol, 2-Methyl-propan-1-ol, and Pentan-1-ol at T = (288.15, 298.15, 313.15, and 328.15) K
rhoI	806.14	kg/m3	298.15	Excess Molar Volumes of 1,3-Diethyl Propanedioate with Methanol, Ethanol, Propan-1-ol, Propan-2-ol, Butan-2-ol, 2-Methyl-propan-1-ol, and Pentan-1-ol at T = (288.15, 298.15, 313.15, and 328.15) K

rhoI	813.77	kg/m3	288.15	Excess Molar Volumes of 1,3-Diethyl Propanedioate with Methanol, Ethanol, Propan-1-ol, Propan-2-ol, Butan-2-ol, 2-Methyl-propan-1-ol, and Pentan-1-ol at T = (288.15, 298.15, 313.15, and 328.15) K
rhoI	801.90	kg/m3	303.00	Fluid-Phase Behavior of {1-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl) Imide, [C6mim][NTf2], + C2-C8 n-Alcohol} Mixtures: Liquid-Liquid Equilibrium and Excess Volumes
rhoI	801.90	kg/m3	303.00	Fluid-Phase Behavior of {1-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl) Imide, [C6mim][NTf2], + C2-C8 n-Alcohol} Mixtures: Liquid-Liquid Equilibrium and Excess Volumes
rhoI	805.70	kg/m3	298.00	Fluid-Phase Behavior of {1-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl) Imide, [C6mim][NTf2], + C2-C8 n-Alcohol} Mixtures: Liquid-Liquid Equilibrium and Excess Volumes
rhoI	805.70	kg/m3	298.00	Fluid-Phase Behavior of {1-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl) Imide, [C6mim][NTf2], + C2-C8 n-Alcohol} Mixtures: Liquid-Liquid Equilibrium and Excess Volumes

rhoI	809.60	kg/m3	293.00	Fluid-Phase Behavior of {1-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl) Imide, [C6mim][NTf2], + C2-C8 n-Alcohol} Mixtures: Liquid-Liquid Equilibrium and Excess Volumes	
rhoI	809.60	kg/m3	293.00	Fluid-Phase Behavior of {1-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl) Imide, [C6mim][NTf2], + C2-C8 n-Alcohol} Mixtures: Liquid-Liquid Equilibrium and Excess Volumes	
rhoI	806.04	kg/m3	298.15	Measurement and Correlation of Vapor-Liquid Equilibria at T) 333.15 K and Excess Molar Volumes at T) 298.15 K for Ethanol + Dimethyl Carbonate (DMC), DMC + 1-Propanol, and DMC + 1-Butanol	
rhoI	805.80	kg/m3	298.15	Excess Molar Volumes and Surface Tensions of 1,2,4-Trimethylbenzene and 1,3,5-Trimethylbenzene with 1-Butanol, 2-Methyl-1-propanol, 2-Butanol, and 2-Methyl-2-propanol at 298.15 K	
rhoI	805.90	kg/m3	298.15	Dynamic Viscosities of Diethyl Carbonate with Linear and Secondary Alcohols at Several Temperatures	
rhoI	810.00	kg/m3	293.00	KDB	

rhoI	806.14	kg/m3	298.15	Speeds of Sound and Isentropic Compressibilities in Binary Mixtures of 2-Propanol with Several 1-Alkanols at 298.15K
rhoI	813.37	kg/m3	288.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)
rhoI	809.57	kg/m3	293.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)
rhoI	805.76	kg/m3	298.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)

rhoI	801.92	kg/m3	303.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)
rhoI	798.05	kg/m3	308.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)
rhoI	794.15	kg/m3	313.15	Temperature Dependence of Densities and Excess Molar Volumes of the Ternary Mixture (1-Butanol + Chloroform + Benzene) and its Binary Constituents (1-Butanol + Chloroform and 1-Butanol + Benzene)
rhoI	813.41	kg/m3	288.15	Volumetric Properties, Viscosities, and Refractive Indices of the Binary Systems 1-Butanol + PEG 200, + PEG 400, and + TEGDME
rhoI	809.62	kg/m3	293.15	Volumetric Properties, Viscosities, and Refractive Indices of the Binary Systems 1-Butanol + PEG 200, + PEG 400, and + TEGDME

rhoI	805.80	kg/m3	298.15	Volumetric Properties, Viscosities, and Refractive Indices of the Binary Systems 1-Butanol + PEG 200, + PEG 400, and + TEGDME
rhoI	801.96	kg/m3	303.15	Volumetric Properties, Viscosities, and Refractive Indices of the Binary Systems 1-Butanol + PEG 200, + PEG 400, and + TEGDME
rhoI	798.09	kg/m3	308.15	Volumetric Properties, Viscosities, and Refractive Indices of the Binary Systems 1-Butanol + PEG 200, + PEG 400, and + TEGDME
rhoI	794.18	kg/m3	313.15	Volumetric Properties, Viscosities, and Refractive Indices of the Binary Systems 1-Butanol + PEG 200, + PEG 400, and + TEGDME
rhoI	790.23	kg/m3	318.15	Volumetric Properties, Viscosities, and Refractive Indices of the Binary Systems 1-Butanol + PEG 200, + PEG 400, and + TEGDME
rhoI	786.23	kg/m3	323.15	Volumetric Properties, Viscosities, and Refractive Indices of the Binary Systems 1-Butanol + PEG 200, + PEG 400, and + TEGDME
rhoI	782.17	kg/m3	328.15	Volumetric Properties, Viscosities, and Refractive Indices of the Binary Systems 1-Butanol + PEG 200, + PEG 400, and + TEGDME

rhoI	778.06	kg/m3	333.15	Volumetric Properties, Viscosities, and Refractive Indices of the Binary Systems 1-Butanol + PEG 200, + PEG 400, and + TEGDME
rhoI	805.60	kg/m3	298.15	Densities, Ultrasonic Speeds, and Excess Properties of Binary Mixtures of Diethylene Glycol with 1-Butanol, 2-Butanol, and 1,4-Butanediol at Different Temperatures
rhoI	801.90	kg/m3	303.15	Densities, Ultrasonic Speeds, and Excess Properties of Binary Mixtures of Diethylene Glycol with 1-Butanol, 2-Butanol, and 1,4-Butanediol at Different Temperatures
rhoI	798.20	kg/m3	308.15	Densities, Ultrasonic Speeds, and Excess Properties of Binary Mixtures of Diethylene Glycol with 1-Butanol, 2-Butanol, and 1,4-Butanediol at Different Temperatures
rhoI	794.50	kg/m3	313.15	Densities, Ultrasonic Speeds, and Excess Properties of Binary Mixtures of Diethylene Glycol with 1-Butanol, 2-Butanol, and 1,4-Butanediol at Different Temperatures

rhoI	805.80	kg/m3	298.15	Revision of the volumetric method for measurements of liquid liquid equilibria in binary systems
rhoI	805.74	kg/m3	298.15	Excess molar volumes and excess molar enthalpies of binary and ternary mixtures of (ethanol or 1-butanol), triethylamine and n-hexane
rhoI	802.10	kg/m3	303.15	Viscous synergy and antagonism and isentropic compressibility of ternary mixtures containing 1,3-dioxolane, water and monoalkanols at 303.15K
rhoI	817.15	kg/m3	283.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhoI	813.38	kg/m3	288.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhoI	809.59	kg/m3	293.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine

rhoI	805.77	kg/m3	298.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhoI	801.92	kg/m3	303.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhoI	798.05	kg/m3	308.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhoI	794.14	kg/m3	313.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhoI	790.19	kg/m3	318.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine

rhoI	786.19	kg/m3	323.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhoI	782.14	kg/m3	328.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhoI	805.67	kg/m3	298.15	Mixing Properties for the Ternary Mixture Methyl tert-Butyl Ether + 1-Butanol + Decane at 298.15 K
rhoI	805.71	kg/m3	298.15	Excess molar enthalpy of 1-alkanol + 1-octene mixtures at 298.15K Experimental results and theoretical description by means of the ERAS and TB models
rhoI	813.37	kg/m3	288.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules

rhoI	809.57	kg/m3	293.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules
rhoI	805.76	kg/m3	298.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules
rhoI	801.92	kg/m3	303.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules
rhoI	798.05	kg/m3	308.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules
rhoI	794.15	kg/m3	313.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules

rhoI	805.78	kg/m3	298.15	Liquid liquid equilibria for the binary system of di-isopropyl ether (DIPE) +water in between 288.15 and 323.15K and the ternary systems of DIPE +water + C1 C4 alcohols at 298.15K
rhoI	813.60	kg/m3	288.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhoI	805.98	kg/m3	298.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhoI	794.34	kg/m3	313.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhoI	782.32	kg/m3	328.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa

rhoI	774.03	kg/m3	338.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhoI	765.48	kg/m3	348.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhoI	805.78	kg/m3	298.15	Phase behaviour of ionic liquid 1-butyl-1-methylpyrrolidinium tris(pentafluoroethyl)trifluorophosphate with alcohols, water and aromatic hydrocarbons
rhoI	805.88	kg/m3	298.20	Liquid-liquid equilibrium data for ternary systems of water + lactic acid + C4-C7 alcohols at 298.2 K and atmospheric pressure
rhoI	805.99	kg/m3	298.15	Thermodynamic and spectral investigations of binary liquid mixtures of 2-butoxy ethanol with alcohols at temperature range of 293.15-313.15 K
rhoI	805.50	kg/m3	298.15	Solubility of androstenedione in lower alcohols
rhoI	810.00	kg/m3	293.15	Liquid-liquid equilibrium of 1-butanol + water +tri-n-butyl phosphate + ammonium chloride system

rhoI	807.96	kg/m3	298.20	Phase equilibria of (water + propionic acid or butyric acid + 2-methoxy-2-methylpropane) ternary systems at 298.2 K and 323.2 K	
rhoI	805.20	kg/m3	298.15	Liquid-liquid equilibria for the ternary system containing 1-Butanol + methoxy(methoxymethoxy)methane + water at temperatures of 303.15, 323.15 and 343.15 K	
rhoI	806.01	kg/m3	298.20	Isothermal vapor-liquid equilibria, excess molar volume and the deviation of refractive indices for binary mixtures of 1-butanol, 1-hexanol, 3-methyl-1-butanol and butyl acetate	
rhoI	806.27	kg/m3	298.15	Effect of composition and temperature variations on thermophysical properties of binary and ternary mixtures of 1-ethyl-3-methylimidazolium ethylsulfate with 1-butanol and /or methanol	
rhoI	802.42	kg/m3	303.15	Effect of composition and temperature variations on thermophysical properties of binary and ternary mixtures of 1-ethyl-3-methylimidazolium ethylsulfate with 1-butanol and /or methanol	

rhoI	798.54	kg/m3	308.15	Effect of composition and temperature variations on thermophysical properties of binary and ternary mixtures of 1-ethyl-3-methylimidazolium ethylsulfate with 1-butanol and /or methanol
rhoI	794.62	kg/m3	313.15	Effect of composition and temperature variations on thermophysical properties of binary and ternary mixtures of 1-ethyl-3-methylimidazolium ethylsulfate with 1-butanol and /or methanol
rhoI	790.65	kg/m3	318.15	Effect of composition and temperature variations on thermophysical properties of binary and ternary mixtures of 1-ethyl-3-methylimidazolium ethylsulfate with 1-butanol and /or methanol
rhoI	786.64	kg/m3	323.15	Effect of composition and temperature variations on thermophysical properties of binary and ternary mixtures of 1-ethyl-3-methylimidazolium ethylsulfate with 1-butanol and /or methanol

rhoI	805.98	kg/m3	298.15	A systematic study on volumetric and transport properties of binary systems 1-propanol + n-hexadecane, 1-butanol + n-hexadecane and 1-propanol + ethyl oleate at different temperatures: Experimental and modeling
rhoI	802.13	kg/m3	303.15	A systematic study on volumetric and transport properties of binary systems 1-propanol + n-hexadecane, 1-butanol + n-hexadecane and 1-propanol + ethyl oleate at different temperatures: Experimental and modeling
rhoI	798.25	kg/m3	308.15	A systematic study on volumetric and transport properties of binary systems 1-propanol + n-hexadecane, 1-butanol + n-hexadecane and 1-propanol + ethyl oleate at different temperatures: Experimental and modeling
rhoI	805.77	kg/m3	298.15	Isobaric vapor-liquid equilibrium, density and speed of sound of binary mixtures 2,2,4-trimethylpentane + 1-butanol or dibutyl ether (DBE) at 101.3 kPa

rho1	809.38	kg/m3	293.20	Liquid-liquid equilibrium data and thermophysical properties for ternary systems composed of water, acetic acid and different solvents
rho1	793.78	kg/m3	313.20	Liquid-liquid equilibrium data and thermophysical properties for ternary systems composed of water, acetic acid and different solvents
rho1	805.82	kg/m3	298.15	Excess molar heat capacities for (1-butanol+1,3-butanediol) at temperatures from (285 to 353) K
rho1	805.80	kg/m3	298.15	Bubble point temperatures of the binary mixtures of nitrobenzene with C1 C4 aliphatic alcohols at 94.95 kPa
rho1	817.18	kg/m3	283.15	Excess molar volumes of binary mixtures of 1,3-dimethylimidazolidin-2-one with an alkan-1-ol at the temperatures 283.15 K, 298.15 K, and 313.15 K
rho1	805.79	kg/m3	298.15	Excess molar volumes of binary mixtures of 1,3-dimethylimidazolidin-2-one with an alkan-1-ol at the temperatures 283.15 K, 298.15 K, and 313.15 K
rho1	794.18	kg/m3	313.15	Excess molar volumes of binary mixtures of 1,3-dimethylimidazolidin-2-one with an alkan-1-ol at the temperatures 283.15 K, 298.15 K, and 313.15 K

rhoI	809.52	kg/m3	293.15	Densities and volumetric properties of (N-(2-hydroxyethyl)morpholine + ethanol, + 1-propanol, + 2-propanol, + 1-butanol, and + 2-butanol) at (293.15, 298.15, 303.15, 313.15, and 323.15) K	
rhoI	805.88	kg/m3	298.15	Densities and volumetric properties of (N-(2-hydroxyethyl)morpholine + ethanol, + 1-propanol, + 2-propanol, + 1-butanol, and + 2-butanol) at (293.15, 298.15, 303.15, 313.15, and 323.15) K	
rhoI	801.99	kg/m3	303.15	Densities and volumetric properties of (N-(2-hydroxyethyl)morpholine + ethanol, + 1-propanol, + 2-propanol, + 1-butanol, and + 2-butanol) at (293.15, 298.15, 303.15, 313.15, and 323.15) K	
rhoI	794.34	kg/m3	313.15	Densities and volumetric properties of (N-(2-hydroxyethyl)morpholine + ethanol, + 1-propanol, + 2-propanol, + 1-butanol, and + 2-butanol) at (293.15, 298.15, 303.15, 313.15, and 323.15) K	
rhoI	786.67	kg/m3	323.15	Densities and volumetric properties of (N-(2-hydroxyethyl)morpholine + ethanol, + 1-propanol, + 2-propanol, + 1-butanol, and + 2-butanol) at (293.15, 298.15, 303.15, 313.15, and 323.15) K	

rhoI	805.64	kg/m3	298.15	Apparent molar volumes and compressibilities of tetrabutyl-ammonium bromide in organic solvents
rhoI	805.60	kg/m3	298.15	Volumetric and surface properties of pure ionic liquid n-octyl-pyridinium nitrate and its binary mixture with alcohol
rhoI	805.77	kg/m3	298.15	Effect of temperature and composition on the density, viscosity, surface tension, and thermodynamic properties of binary mixtures of N-octylisoquinolinium bis{(trifluoromethyl)sulfonyl}imide with alcohols
rhoI	798.06	kg/m3	308.15	Effect of temperature and composition on the density, viscosity, surface tension, and thermodynamic properties of binary mixtures of N-octylisoquinolinium bis{(trifluoromethyl)sulfonyl}imide with alcohols
rhoI	790.19	kg/m3	318.15	Effect of temperature and composition on the density, viscosity, surface tension, and thermodynamic properties of binary mixtures of N-octylisoquinolinium bis{(trifluoromethyl)sulfonyl}imide with alcohols

rhoI	782.15	kg/m3	328.15	Effect of temperature and composition on the density, viscosity, surface tension, and thermodynamic properties of binary mixtures of N-octylisoquinolinium bis{(trifluoromethyl)sulfonyl}imide with alcohols
rhoI	773.89	kg/m3	338.15	Effect of temperature and composition on the density, viscosity, surface tension, and thermodynamic properties of binary mixtures of N-octylisoquinolinium bis{(trifluoromethyl)sulfonyl}imide with alcohols
rhoI	798.06	kg/m3	298.15	Extraction of butan-1-ol from water with ionic liquids at T = 308.15 K
rhoI	805.85	kg/m3	298.15	Isothermal (vapour + liquid) equilibria for binary mixtures of diisopropyl ether with (methanol, or ethanol, or 1-butanol): Experimental data, correlations, and predictions
rhoI	809.89	kg/m3	293.15	Thermodynamics of 1-alkanol + linear polyether mixtures
rhoI	806.47	kg/m3	298.15	Thermodynamics of 1-alkanol + linear polyether mixtures
rhoI	802.22	kg/m3	303.15	Thermodynamics of 1-alkanol + linear polyether mixtures

rhoI	809.54	kg/m3	293.15	Osmotic and apparent molar properties of binary mixtures alcohol + 1-butyl-3-methylimidazolium trifluoromethanesulfonate ionic liquid
rhoI	798.01	kg/m3	308.15	Osmotic and apparent molar properties of binary mixtures alcohol + 1-butyl-3-methylimidazolium trifluoromethanesulfonate ionic liquid
rhoI	786.15	kg/m3	323.15	Osmotic and apparent molar properties of binary mixtures alcohol + 1-butyl-3-methylimidazolium trifluoromethanesulfonate ionic liquid
rhoI	805.70	kg/m3	298.15	Density and surface tension of pure ionic liquid 1-butyl-3-methylimidazolium L-lactate and its binary mixture with alcohol and water
rhoI	798.00	kg/m3	308.15	Density and surface tension of pure ionic liquid 1-butyl-3-methylimidazolium L-lactate and its binary mixture with alcohol and water
rhoI	790.10	kg/m3	318.15	Density and surface tension of pure ionic liquid 1-butyl-3-methylimidazolium L-lactate and its binary mixture with alcohol and water

rhoI	805.95	kg/m3	298.15	FT-IR studies on excess thermodynamic properties of binary liquid mixtures o-chlorotoluene with 1-propanol, 1-butanol, 1-pentanol, 1-hexanol and 1-heptanol at different temperatures
rhoI	802.11	kg/m3	303.15	FT-IR studies on excess thermodynamic properties of binary liquid mixtures o-chlorotoluene with 1-propanol, 1-butanol, 1-pentanol, 1-hexanol and 1-heptanol at different temperatures
rhoI	798.24	kg/m3	308.15	FT-IR studies on excess thermodynamic properties of binary liquid mixtures o-chlorotoluene with 1-propanol, 1-butanol, 1-pentanol, 1-hexanol and 1-heptanol at different temperatures
rhoI	804.00	kg/m3	303.15	Study of molecular interactions in the mixtures of some primary alcohols with equimolar mixture of 1-propanol and alkylbenzoates at T = 303.15 K
rhoI	786.32	kg/m3	323.15	Osmotic coefficients and apparent molar volumes of 1-hexyl-3-methylimidazolium trifluoromethanesulfonate ionic liquid in alcohols

rhoI	809.81	kg/m3	293.15	Molecular interactions in binary mixtures of 1-butoxy-2-propanol with alcohols at different temperatures: A thermophysical and spectroscopic approach
rhoI	805.99	kg/m3	298.15	Molecular interactions in binary mixtures of 1-butoxy-2-propanol with alcohols at different temperatures: A thermophysical and spectroscopic approach
rhoI	802.14	kg/m3	303.15	Molecular interactions in binary mixtures of 1-butoxy-2-propanol with alcohols at different temperatures: A thermophysical and spectroscopic approach
rhoI	798.26	kg/m3	308.15	Molecular interactions in binary mixtures of 1-butoxy-2-propanol with alcohols at different temperatures: A thermophysical and spectroscopic approach
rhoI	794.38	kg/m3	313.15	Molecular interactions in binary mixtures of 1-butoxy-2-propanol with alcohols at different temperatures: A thermophysical and spectroscopic approach

rhoI	805.79	kg/m3	298.15	A combined experimental and computational investigation of excess molar enthalpies of (nitrobenzene + alkanol) mixtures
rhoI	805.50	kg/m3	298.15	Solubility and solution thermodynamics of sorbic acid in eight pure organic solvents
rhoI	809.80	kg/m3	293.15	Isothermal (vapour + liquid) equilibrium and thermophysical properties for (1-butyl-3-methylimidazolium iodide + 1-butanol) binary system
rhoI	805.90	kg/m3	298.15	Isothermal (vapour + liquid) equilibrium and thermophysical properties for (1-butyl-3-methylimidazolium iodide + 1-butanol) binary system
rhoI	798.20	kg/m3	308.15	Isothermal (vapour + liquid) equilibrium and thermophysical properties for (1-butyl-3-methylimidazolium iodide + 1-butanol) binary system
rhoI	809.72	kg/m3	293.15	Properties of pure 1,1,3,3-tetramethylguanidine imidazole ionic liquid and its binary mixtures with alcohols at T = (293.15 to 313.15) K
rhoI	805.92	kg/m3	298.15	Properties of pure 1,1,3,3-tetramethylguanidine imidazole ionic liquid and its binary mixtures with alcohols at T = (293.15 to 313.15) K

rhoI	802.08	kg/m3	303.15	Properties of pure 1,1,3,3-tetramethylguanidine imidazole ionic liquid and its binary mixtures with alcohols at T = (293.15 to 313.15) K
rhoI	798.21	kg/m3	308.15	Properties of pure 1,1,3,3-tetramethylguanidine imidazole ionic liquid and its binary mixtures with alcohols at T = (293.15 to 313.15) K
rhoI	794.30	kg/m3	313.15	Properties of pure 1,1,3,3-tetramethylguanidine imidazole ionic liquid and its binary mixtures with alcohols at T = (293.15 to 313.15) K
rhoI	805.79	kg/m3	298.15	Measurements and equation-of-state modelling of thermodynamic properties of binary mixtures of 1-butyl-1-methylpyrrolidinium tetracyanoborate ionic liquid with molecular compounds
rhoI	806.10	kg/m3	298.15	Solubility and solution thermodynamics of thymol in six pure organic solvents
rhoI	817.10	kg/m3	283.15	Ionic association and conductance of [emim][BF4] and [bmim][BF4] in 1-butanol in a wide range of temperature
rhoI	813.34	kg/m3	288.15	Ionic association and conductance of [emim][BF4] and [bmim][BF4] in 1-butanol in a wide range of temperature

rhoI	809.55	kg/m3	293.15	Ionic association and conductance of [emim][BF4] and [bmim][BF4] in 1-butanol in a wide range of temperature
rhoI	805.74	kg/m3	298.15	Ionic association and conductance of [emim][BF4] and [bmim][BF4] in 1-butanol in a wide range of temperature
rhoI	801.90	kg/m3	303.15	Ionic association and conductance of [emim][BF4] and [bmim][BF4] in 1-butanol in a wide range of temperature
rhoI	798.03	kg/m3	308.15	Ionic association and conductance of [emim][BF4] and [bmim][BF4] in 1-butanol in a wide range of temperature
rhoI	794.13	kg/m3	313.15	Ionic association and conductance of [emim][BF4] and [bmim][BF4] in 1-butanol in a wide range of temperature
rhoI	790.18	kg/m3	318.15	Ionic association and conductance of [emim][BF4] and [bmim][BF4] in 1-butanol in a wide range of temperature
rhoI	809.75	kg/m3	293.15	(Liquid + liquid) equilibria of four alcohol-water systems containing 1,8-cineole at T = 298.15 K
rhoI	809.82	kg/m3	293.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures

rhoI	806.00	kg/m3	298.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhoI	802.15	kg/m3	303.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhoI	798.28	kg/m3	308.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhoI	794.37	kg/m3	313.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhoI	790.43	kg/m3	318.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhoI	786.44	kg/m3	323.15	Thermodynamic and spectroscopic interpretation of molecular interactions of nicotine + alcohol binary mixtures
rhoI	778.01	kg/m3	333.15	Densities and Viscosities of Ternary System n-Dodecane (1) + Bicyclohexyl (2) + n-Butanol (3) and Corresponding Binaries at T = (293.15 to 333.15) K

rhoI	809.52	kg/m3	293.15	Thermodynamic and spectroscopic properties of binary mixtures of n-butylammonium butanoate ionic liquid with alcohols at T = (293.15-313.15) K
rhoI	805.71	kg/m3	298.15	Thermodynamic and spectroscopic properties of binary mixtures of n-butylammonium butanoate ionic liquid with alcohols at T = (293.15-313.15) K
rhoI	801.87	kg/m3	303.15	Thermodynamic and spectroscopic properties of binary mixtures of n-butylammonium butanoate ionic liquid with alcohols at T = (293.15-313.15) K
rhoI	798.00	kg/m3	308.15	Thermodynamic and spectroscopic properties of binary mixtures of n-butylammonium butanoate ionic liquid with alcohols at T = (293.15-313.15) K
rhoI	794.10	kg/m3	313.15	Thermodynamic and spectroscopic properties of binary mixtures of n-butylammonium butanoate ionic liquid with alcohols at T = (293.15-313.15) K

rhoI	809.49	kg/m3	293.15	Investigation on molecular interactions of antibiotics in alcohols using volumetric and acoustic studies at different temperatures	
rhoI	805.65	kg/m3	298.15	Investigation on molecular interactions of antibiotics in alcohols using volumetric and acoustic studies at different temperatures	
rhoI	803.68	kg/m3	303.15	Investigation on molecular interactions of antibiotics in alcohols using volumetric and acoustic studies at different temperatures	
rhoI	800.50	kg/m3	308.15	Investigation on molecular interactions of antibiotics in alcohols using volumetric and acoustic studies at different temperatures	
rhoI	794.11	kg/m3	313.15	Investigation on molecular interactions of antibiotics in alcohols using volumetric and acoustic studies at different temperatures	
rhoI	806.00	kg/m3	298.00	Comparative study of physical properties of binary mixtures of halogen free ionic liquids with alcohols	
rhoI	802.00	kg/m3	303.00	Comparative study of physical properties of binary mixtures of halogen free ionic liquids with alcohols	

rhoI	798.00	kg/m3	308.00	Comparative study of physical properties of binary mixtures of halogen free ionic liquids with alcohols	
rhoI	794.00	kg/m3	313.00	Comparative study of physical properties of binary mixtures of halogen free ionic liquids with alcohols	
rhoI	805.81	kg/m3	298.20	Liquid-liquid equilibrium in systems used for the production of 5-hydroxymethylfurfural from biomass using alcohols as solvents	
rhoI	809.50	kg/m3	293.15	Measurement and correlation of isobaric vapour-liquid equilibria for binary systems of 1-(methoxymethoxy)-2-methyl-propane with 1-butanol and isobutanol at 101.33 kPa	
rhoI	817.11	kg/m3	283.15	Excess molar enthalpies of R-fenchone + butan-1-ol or + pentan-1-ol. Modeling with COSMO-RS and UNIFAC	
rhoI	805.72	kg/m3	298.15	Excess molar enthalpies of R-fenchone + butan-1-ol or + pentan-1-ol. Modeling with COSMO-RS and UNIFAC	
rhoI	794.40	kg/m3	313.15	Excess molar enthalpies of R-fenchone + butan-1-ol or + pentan-1-ol. Modeling with COSMO-RS and UNIFAC	

rhoI	782.11	kg/m3	328.15	Excess molar enthalpies of R-fenchone + butan-1-ol or + pentan-1-ol. Modeling with COSMO-RS and UNIFAC
rhoI	809.53	kg/m3	293.15	Intermolecular interactions in binary mixtures of 2-diethylethanolamine with 1-propanol and 1-butanol at different temperatures
rhoI	802.00	kg/m3	303.15	Intermolecular interactions in binary mixtures of 2-diethylethanolamine with 1-propanol and 1-butanol at different temperatures
rhoI	794.70	kg/m3	313.15	Intermolecular interactions in binary mixtures of 2-diethylethanolamine with 1-propanol and 1-butanol at different temperatures
rhoI	810.00	kg/m3	293.15	Density, speed of sound and refractive index of mixtures containing 2-phenoxyethanol with propanol or butanol at various temperatures
rhoI	802.00	kg/m3	303.15	Density, speed of sound and refractive index of mixtures containing 2-phenoxyethanol with propanol or butanol at various temperatures

rhoI	794.00	kg/m3	313.15	Density, speed of sound and refractive index of mixtures containing 2-phenoxyethanol with propanol or butanol at various temperatures
rhoI	787.00	kg/m3	323.15	Density, speed of sound and refractive index of mixtures containing 2-phenoxyethanol with propanol or butanol at various temperatures
rhoI	806.00	kg/m3	298.15	Density, speed of sound and refractive index of mixtures containing 2-phenoxyethanol with propanol or butanol at various temperatures
rhoI	809.77	kg/m3	293.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa
rhoI	805.92	kg/m3	298.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa
rhoI	802.00	kg/m3	303.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa
rhoI	798.14	kg/m3	308.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa

rhoI	794.24	kg/m3	313.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa	
rhoI	790.20	kg/m3	318.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa	
rhoI	786.21	kg/m3	323.15	Volumetric properties of monoethanolamine and alcohol binary mixtures at different temperatures and 0.1 MPa	
rhoI	817.18	kg/m3	283.15	Volumetric and sound speed study of aqueous 1-butanol liquid mixtures at different temperatures	
rhoI	813.40	kg/m3	288.15	Volumetric and sound speed study of aqueous 1-butanol liquid mixtures at different temperatures	
rhoI	809.60	kg/m3	293.15	Volumetric and sound speed study of aqueous 1-butanol liquid mixtures at different temperatures	
rhoI	805.78	kg/m3	298.15	Volumetric and sound speed study of aqueous 1-butanol liquid mixtures at different temperatures	
rhoI	801.94	kg/m3	303.15	Volumetric and sound speed study of aqueous 1-butanol liquid mixtures at different temperatures	

rhoI	801.91	kg/m3	303.15	Vapor-liquid equilibrium and excess properties of the binary mixtures formed by ethyl isobutyrate and n-alkanols
rhoI	786.62	kg/m3	323.15	Vapor-liquid equilibrium and excess properties of the binary mixtures formed by ethyl isobutyrate and n-alkanols
rhoI	805.75	kg/m3	298.15	Excess molar enthalpies of methyl isobutyl ketone (MIBK) with alkan-1-ols (C1-C6) and their correlations at 298.15 K
rhoI	801.98	kg/m3	303.15	Excess molar enthalpies and heat capacities of dimethyl sulfoxide + seven normal alkanols at 303.15K and atmospheric pressure
rhoI	801.92	kg/m3	303.15	Studies of viscosities of dilute solutions of alkylamines in non-electrolyte solvents III. Alkylamines in butanols 303.15K
rhoI	801.90	kg/m3	303.15	Volumetric and transport properties of ternary mixtures containing 1-alkanol + ethyl ethanoate + cyclohexane at 303.15 K: Experimental data, correlation and prediction by ERAS model
rhoI	809.50	kg/m3	298.15	Topological investigations of the molecular species and molecular interactions that characterize pyrrolidin-2-one + lower alkanol mixtures

rhoI	813.37	kg/m3	288.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K
rhoI	809.57	kg/m3	293.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K
rhoI	805.76	kg/m3	298.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K
rhoI	801.92	kg/m3	303.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K

rhoI	798.05	kg/m3	308.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K
rhoI	794.15	kg/m3	313.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K
rhoI	790.23	kg/m3	318.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K
rhoI	786.24	kg/m3	323.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K
rhoI	809.78	kg/m3	293.15	Excess molar volumes of Diisopropylamine + (C1-C5) Alkan-1-ols: application of the ERAS model and cubic EOS

rhoI	806.05	kg/m3	298.15	Excess molar volumes of Diisopropylamine + (C1-C5) Alkan-1-ols: application of the ERAS model and cubic EOS
rhoI	802.03	kg/m3	303.15	Excess molar volumes of Diisopropylamine + (C1-C5) Alkan-1-ols: application of the ERAS model and cubic EOS
rhoI	794.12	kg/m3	313.15	Excess molar volumes of Diisopropylamine + (C1-C5) Alkan-1-ols: application of the ERAS model and cubic EOS
rhoI	805.90	kg/m3	298.15	Thermodynamics of mixtures containing amines. XVI. CE pm of 1-butanol, 1-octanol or 1-decanol + benzylamine systems at (298.15, 308.15, 318.15 and 333.15) K
rhoI	817.21	kg/m3	283.15	Effects of alkyl group and temperature on the interactions between furfural and alcohol: Insight from density and sound velocity studies
rhoI	809.65	kg/m3	293.15	Effects of alkyl group and temperature on the interactions between furfural and alcohol: Insight from density and sound velocity studies

rhoI	802.00	kg/m3	303.15	Effects of alkyl group and temperature on the interactions between furfural and alcohol: Insight from density and sound velocity studies	
rhoI	794.21	kg/m3	313.15	Effects of alkyl group and temperature on the interactions between furfural and alcohol: Insight from density and sound velocity studies	
rhoI	805.76	kg/m3	298.15	Experimental and theoretical excess molar properties of imidazolium based ionic liquids with isomers of butanol	
rhoI	798.05	kg/m3	308.15	Experimental and theoretical excess molar properties of imidazolium based ionic liquids with isomers of butanol	
rhoI	790.21	kg/m3	318.15	Experimental and theoretical excess molar properties of imidazolium based ionic liquids with isomers of butanol	
rhoI	809.78	kg/m3	293.15	Density, Speed of Sound, Viscosity, Excess Properties, and Prigogine Flory Patterson (PFP) Theory of Binary Mixtures of Amine and Alcohols	

rhoI	805.95	kg/m3	298.15	Density, Speed of Sound, Viscosity, Excess Properties, and Prigogine Flory Patterson (PFP) Theory of Binary Mixtures of Amine and Alcohols
rhoI	802.10	kg/m3	303.15	Density, Speed of Sound, Viscosity, Excess Properties, and Prigogine Flory Patterson (PFP) Theory of Binary Mixtures of Amine and Alcohols
rhoI	798.23	kg/m3	308.15	Density, Speed of Sound, Viscosity, Excess Properties, and Prigogine Flory Patterson (PFP) Theory of Binary Mixtures of Amine and Alcohols
rhoI	794.31	kg/m3	313.15	Density, Speed of Sound, Viscosity, Excess Properties, and Prigogine Flory Patterson (PFP) Theory of Binary Mixtures of Amine and Alcohols
rhoI	802.01	kg/m3	303.15	Density, Refractive Index, and Sound Velocity for the Binary Mixtures of Tri-n-Butyl Phosphate and n-Butanol between 303.15 K and 323.15 K
rhoI	798.14	kg/m3	308.15	Density, Refractive Index, and Sound Velocity for the Binary Mixtures of Tri-n-Butyl Phosphate and n-Butanol between 303.15 K and 323.15 K

rhoI	794.22	kg/m3	313.15	Density, Refractive Index, and Sound Velocity for the Binary Mixtures of Tri-n-Butyl Phosphate and n-Butanol between 303.15 K and 323.15 K
rhoI	790.28	kg/m3	318.15	Density, Refractive Index, and Sound Velocity for the Binary Mixtures of Tri-n-Butyl Phosphate and n-Butanol between 303.15 K and 323.15 K
rhoI	786.29	kg/m3	323.15	Density, Refractive Index, and Sound Velocity for the Binary Mixtures of Tri-n-Butyl Phosphate and n-Butanol between 303.15 K and 323.15 K
rhoI	809.84	kg/m3	293.15	Density and Excess Molar Volumes of 1-Butanol + Methanol + Electrolyte Systems in the Temperature Range (293.15 308.15) K
rhoI	806.03	kg/m3	298.15	Density and Excess Molar Volumes of 1-Butanol + Methanol + Electrolyte Systems in the Temperature Range (293.15 308.15) K
rhoI	802.19	kg/m3	303.15	Density and Excess Molar Volumes of 1-Butanol + Methanol + Electrolyte Systems in the Temperature Range (293.15 308.15) K

rhoI	798.38	kg/m3	308.15	Density and Excess Molar Volumes of 1-Butanol + Methanol + Electrolyte Systems in the Temperature Range (293.15 308.15) K
rhoI	807.96	kg/m3	298.15	Tie-Line Data for Aqueous Mixtures of Butyric Acid with Diisopropyl Ether at Various Temperatures
rhoI	806.00	kg/m3	298.15	Thermodynamics of 1,3-dimethylurea in eight alcohols
rhoI	817.07	kg/m3	283.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	813.32	kg/m3	288.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	809.55	kg/m3	293.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa

rhoI	805.76	kg/m3	298.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	801.94	kg/m3	303.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	798.09	kg/m3	308.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	794.20	kg/m3	313.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	790.27	kg/m3	318.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa

rhoI	786.30	kg/m3	323.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	782.27	kg/m3	328.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	778.18	kg/m3	333.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	774.03	kg/m3	338.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	769.80	kg/m3	343.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa

rhoI	765.49	kg/m3	348.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	761.12	kg/m3	353.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	756.64	kg/m3	358.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	752.08	kg/m3	363.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhoI	805.94	kg/m3	298.15	Isobaric Vapor Liquid Equilibrium for Two Binary Systems (Methanol + Dibutyl Carbonate) and (n-Butanol + Dibutyl Carbonate) at p = 40.0, 70.0, and 100.0 kPa

rhoI	805.75	kg/m3	298.15	Physical Properties of the Pure Deep Eutectic Solvent, [ChCl]:[Lev] (1:2) DES, and Its Binary Mixtures with Alcohols
rhoI	798.06	kg/m3	308.15	Physical Properties of the Pure Deep Eutectic Solvent, [ChCl]:[Lev] (1:2) DES, and Its Binary Mixtures with Alcohols
rhoI	790.22	kg/m3	318.15	Physical Properties of the Pure Deep Eutectic Solvent, [ChCl]:[Lev] (1:2) DES, and Its Binary Mixtures with Alcohols
rhoI	801.92	kg/m3	303.15	Isobaric Vapor Liquid Equilibrium for the Binary Systems Dimethyl Disulfide + C1 C4 n-Alkanol at 40.000 and 101.325 kPa
rhoI	809.50	kg/m3	298.15	Measurement and Correlation of Isobaric Vapor Liquid Equilibrium for Binary Systems of 1-(Ethoxymethoxy)-2-methyl-propane with Isobutyl Alcohol or 1-Butanol at 101.33 kPa
rhoI	809.01	kg/m3	293.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Butanol, + Isobutyl Alcohol, or + 2-Butanol from 293.15 to 333.15 K at 0.1 MPa

rhoI	805.87	kg/m3	298.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Butanol, + Isobutyl Alcohol, or + 2-Butanol from 293.15 to 333.15 K at 0.1 MPa
rhoI	802.06	kg/m3	303.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Butanol, + Isobutyl Alcohol, or + 2-Butanol from 293.15 to 333.15 K at 0.1 MPa
rhoI	798.18	kg/m3	308.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Butanol, + Isobutyl Alcohol, or + 2-Butanol from 293.15 to 333.15 K at 0.1 MPa
rhoI	794.26	kg/m3	313.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Butanol, + Isobutyl Alcohol, or + 2-Butanol from 293.15 to 333.15 K at 0.1 MPa
rhoI	790.30	kg/m3	318.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Butanol, + Isobutyl Alcohol, or + 2-Butanol from 293.15 to 333.15 K at 0.1 MPa

rhoI	786.29	kg/m3	323.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Butanol, + Isobutyl Alcohol, or + 2-Butanol from 293.15 to 333.15 K at 0.1 MPa
rhoI	782.02	kg/m3	328.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Butanol, + Isobutyl Alcohol, or + 2-Butanol from 293.15 to 333.15 K at 0.1 MPa
rhoI	777.81	kg/m3	333.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Butanol, + Isobutyl Alcohol, or + 2-Butanol from 293.15 to 333.15 K at 0.1 MPa
rhoI	805.98	kg/m3	298.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa
rhoI	802.16	kg/m3	303.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa

rhoI	798.28	kg/m3	308.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa
rhoI	794.37	kg/m3	313.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa
rhoI	790.42	kg/m3	318.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa
rhoI	786.41	kg/m3	323.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa

rhoI	782.25	kg/m3	328.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa
rhoI	778.09	kg/m3	333.15	Densities and Viscosities for Binary Liquid Mixtures of Butan-1-ol + Propane-1,2-diol, + Butane-1,2-diol and 2-Methylpropan-1-ol + Propane-1,2-diol, + Butane-1,2-diol from 298.15 to 333.15 K at 0.1 MPa
rhoI	809.50	kg/m3	293.15	Three Binary Azeotropic Systems for 1-(Methoxymethoxy)-propane, 1-(Ethoxymethoxy)-propane, and Methoxy(methoxymethoxy)methane with Three Alcohols at 101.33 kPa: Experimental Data, Correlation, and Purification
rhoI	805.88	kg/m3	298.15	Liquid-Liquid Equilibrium for Ternary Systems, Water + 5-Hydroxymethylfurfural + (1-Butanol, Isobutanol, Methyl Isobutyl Ketone), at 313.15, 323.15, and 333.15 K
rhoI	809.50	kg/m3	293.15	Densities and Viscosities of Ternary System n-Dodecane (1) + Bicyclohexyl (2) + n-Butanol (3) and Corresponding Binaries at T = (293.15 to 333.15) K

rhoI	805.70	kg/m3	298.15	Densities and Viscosities of Ternary System n-Dodecane (1) + Bicyclohexyl (2) + n-Butanol (3) and Corresponding Binaries at T = (293.15 to 333.15) K
rhoI	801.87	kg/m3	303.15	Densities and Viscosities of Ternary System n-Dodecane (1) + Bicyclohexyl (2) + n-Butanol (3) and Corresponding Binaries at T = (293.15 to 333.15) K
rhoI	798.00	kg/m3	308.15	Densities and Viscosities of Ternary System n-Dodecane (1) + Bicyclohexyl (2) + n-Butanol (3) and Corresponding Binaries at T = (293.15 to 333.15) K
rhoI	794.10	kg/m3	313.15	Densities and Viscosities of Ternary System n-Dodecane (1) + Bicyclohexyl (2) + n-Butanol (3) and Corresponding Binaries at T = (293.15 to 333.15) K
rhoI	790.15	kg/m3	318.15	Densities and Viscosities of Ternary System n-Dodecane (1) + Bicyclohexyl (2) + n-Butanol (3) and Corresponding Binaries at T = (293.15 to 333.15) K
rhoI	786.16	kg/m3	323.15	Densities and Viscosities of Ternary System n-Dodecane (1) + Bicyclohexyl (2) + n-Butanol (3) and Corresponding Binaries at T = (293.15 to 333.15) K

rhoI	782.12	kg/m3	328.15	Densities and Viscosities of Ternary System n-Dodecane (1) + Bicyclohexyl (2) + n-Butanol (3) and Corresponding Binaries at T = (293.15 to 333.15) K
rhoI	805.80	kg/m3	298.15	Experimental study on the calorimetric data of 2-butoxyethanol with aliphatic alcohols (C1-C4) and correlation with the Wilson, NRTL and UNIQUAC models at T = 298 K
rhoI	806.00	kg/m3	298.15	Isobaric Vapor-Liquid Equilibrium for the Binary Systems of 2-Butanol + 2-(Methoxymethoxy)-butane and 1-Butanol + 2-(Methoxymethoxy)-butane at 101.3 kPa
sfust	50.46	J/mol×K	183.90	NIST Webbook
sfust	50.79	J/mol×K	184.50	NIST Webbook
speedsl	1212.00	m/s	308.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene
speedsl	1191.40	m/s	313.15	Excess Enthalpy, Density, and Speed of Sound for the Mixtures α-Pinene + 1-Butanol or 2-Butanol at (283.15, 298.15, and 313.15) K

speedsl	1240.70	m/s	298.15	Excess Enthalpy, Density, and Speed of Sound for the Mixtures α -Pinene + 1-Butanol or 2-Butanol at (283.15, 298.15, and 313.15) K
speedsl	1292.20	m/s	283.15	Excess Enthalpy, Density, and Speed of Sound for the Mixtures α -Pinene + 1-Butanol or 2-Butanol at (283.15, 298.15, and 313.15) K
speedsl	1241.60	m/s	298.15	Compressibility Studies of Binary Solutions Involving Water as a Solute in Nonaqueous Solvents at T) 298.15 K
speedsl	1244.00	m/s	298.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene
speedsl	1172.12	m/s	318.15	Thermodynamic Properties of dodecane + 1-butanol and + 2-butanol systems
speedsl	1205.50	m/s	308.15	Thermodynamic Properties of dodecane + 1-butanol and + 2-butanol systems

speedsl	1239.29	m/s	298.15	Thermodynamic Properties of dodecane + 1-butanol and + 2-butanol systems
speedsl	1273.51	m/s	288.15	Thermodynamic Properties of dodecane + 1-butanol and + 2-butanol systems
speedsl	1308.19	m/s	278.15	Thermodynamic Properties of dodecane + 1-butanol and + 2-butanol systems
speedsl	1170.00	m/s	318.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K
speedsl	1189.20	m/s	313.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K
speedsl	1207.60	m/s	308.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K
speedsl	1225.80	m/s	303.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K

speedsl	1242.60	m/s	298.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K
speedsl	1262.40	m/s	293.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K
speedsl	1282.20	m/s	288.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K
speedsl	1156.90	m/s	323.15	Acoustic, volumetric and osmotic properties of binary mixtures containing the ionic liquid 1-butyl-3-methylimidazolium dicyanamide mixed with primary and secondary alcohols
speedsl	1206.50	m/s	308.15	Acoustic, volumetric and osmotic properties of binary mixtures containing the ionic liquid 1-butyl-3-methylimidazolium dicyanamide mixed with primary and secondary alcohols

speedsl	1256.70	m/s	293.15	Acoustic, volumetric and osmotic properties of binary mixtures containing the ionic liquid 1-butyl-3-methylimidazolim dicyanamide mixed with primary and secondary alcohols
speedsl	1241.30	m/s	298.15	Ultrasonic speeds and isentropic compressibilities of {difurylmethane + (C1 C6) n-alkanol} binary mixtures at T = 298.15 K
speedsl	1239.80	m/s	298.15	Excess enthalpy, density, and speed of sound determination for the ternary mixture (methyl tert-butyl ether + 1-butanol + n-hexane)
speedsl	1205.90	m/s	308.15	Excess enthalpy, density, and speed of sound determination for the ternary mixture (methyl tert-butyl ether + 1-butanol + n-hexane)
speedsl	1222.70	m/s	303.15	Excess enthalpy, density, and speed of sound determination for the ternary mixture (methyl tert-butyl ether + 1-butanol + n-hexane)
speedsl	1257.00	m/s	293.15	Excess enthalpy, density, and speed of sound determination for the ternary mixture (methyl tert-butyl ether + 1-butanol + n-hexane)

speedsl	1273.70	m/s	288.15	Excess enthalpy, density, and speed of sound determination for the ternary mixture (methyl tert-butyl ether + 1-butanol + n-hexane)	
speedsl	1256.30	m/s	293.15	Acoustic and Thermophysical Properties of Binary Liquid Mixtures of Primary Butanols with Hexane and Cyclohexane at 293.15 K	
srf	0.02	N/m	303.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol	
srf	0.02	N/m	303.15	Study of the Temperature Dependence of Surface Tensions of Some Alkanol + Hexane Mixtures	
srf	0.02	N/m	313.15	Study of the Temperature Dependence of Surface Tensions of Some Alkanol + Hexane Mixtures	
srf	0.02	N/m	298.00	Surface Tension and Density of Pure Ionic Liquids and Some Binary Mixtures with 1-Propanol and 1-Butanol	
srf	0.03	N/m	293.20	KDB	
srf	0.02	N/m	298.15	Study of the Temperature Dependence of Surface Tensions of Some Alkanol + Hexane Mixtures	
srf	0.02	N/m	293.15	Study of the Temperature Dependence of Surface Tensions of Some Alkanol + Hexane Mixtures	

srf	0.03	N/m	288.15	Study of the Temperature Dependence of Surface Tensions of Some Alkanol + Hexane Mixtures	
srf	0.02	N/m	308.15	Study of the Temperature Dependence of Surface Tensions of Some Alkanol + Hexane Mixtures	
srf	0.03	N/m	283.15	Study of the Temperature Dependence of Surface Tensions of Some Alkanol + Hexane Mixtures	
srf	0.02	N/m	308.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol	
srf	0.02	N/m	298.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol	
srf	0.02	N/m	293.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol	
srf	0.02	N/m	288.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol	
srf	0.02	N/m	293.15	Density and Surface Tension of Binary Mixtures of Acetonitrile + 1-Alkanol at 293.15 K	
srf	0.02	N/m	323.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol	
srf	0.02	N/m	318.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol	

srf	0.02	N/m	313.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol
srf	0.02	N/m	308.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol
srf	0.02	N/m	303.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol
srf	0.02	N/m	298.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol
srf	0.02	N/m	298.15	Concentration Dependence of Surface Tension for Very Dilute Aqueous Solutions of Organic Non-Electrolytes
srf	0.02	N/m	333.20	Surface tension and interfacial compositions of binary glycerol/alcohol mixtures
srf	0.02	N/m	323.20	Surface tension and interfacial compositions of binary glycerol/alcohol mixtures
srf	0.02	N/m	313.20	Surface tension and interfacial compositions of binary glycerol/alcohol mixtures
srf	0.02	N/m	303.20	Surface tension and interfacial compositions of binary glycerol/alcohol mixtures
srf	0.02	N/m	293.20	Surface tension and interfacial compositions of binary glycerol/alcohol mixtures

srf	0.02	N/m	328.15	Study of surface tension and surface properties of binary systems of DMSO with long chain alcohols at various temperatures	
srf	0.02	N/m	318.15	Study of surface tension and surface properties of binary systems of DMSO with long chain alcohols at various temperatures	
srf	0.02	N/m	308.15	Study of surface tension and surface properties of binary systems of DMSO with long chain alcohols at various temperatures	
srf	0.02	N/m	298.15	Study of surface tension and surface properties of binary systems of DMSO with long chain alcohols at various temperatures	
srf	0.02	N/m	288.15	Study of surface tension and surface properties of binary systems of DMSO with long chain alcohols at various temperatures	
srf	0.02	N/m	293.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol	

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
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tbp	390.65	K	101.40	Isobaric Vapor Liquid Equilibrium Data for the 1,2-Dichloroethane-1-Butanol System
tbp	386.45	K	86.71	Isobaric Vapor Liquid Equilibrium Data for the 1,2-Dichloroethane-1-Butanol System
tbp	384.35	K	80.04	Isobaric Vapor Liquid Equilibrium Data for the 1,2-Dichloroethane-1-Butanol System
tbp	382.05	K	73.37	Isobaric Vapor Liquid Equilibrium Data for the 1,2-Dichloroethane-1-Butanol System
tbp	379.65	K	66.66	Isobaric Vapor Liquid Equilibrium Data for the 1,2-Dichloroethane-1-Butanol System
tbp	376.95	K	59.97	Isobaric Vapor Liquid Equilibrium Data for the 1,2-Dichloroethane-1-Butanol System

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.47969e+01
Coeff. B	-2.95887e+03
Coeff. C	-9.99030e+01
Temperature range (K), min.	303.83
Temperature range (K), max.	411.84

Information	Value
Property code	pvap

Equation	$\ln(P_{vp}) = A + B/T + C \cdot \ln(T) + D \cdot T^2$
Coeff. A	8.67221e+01
Coeff. B	-9.12750e+03
Coeff. C	-9.88261e+00
Coeff. D	1.42848e-06
Temperature range (K), min.	183.85
Temperature range (K), max.	563.00

Datasets

Molar heat capacity at constant pressure, J/K/mol

Temperature, K - Liquid	Pressure, kPa - Liquid	Molar heat capacity at constant pressure, J/K/mol - Liquid
273.15	100.00	159.50
273.15	5000.00	158.70
273.15	10000.00	158.40
273.15	15000.00	158.20
273.15	20000.00	157.90
273.15	25000.00	157.20
293.15	100.00	175.20
293.15	5000.00	173.90
293.15	10000.00	172.80
293.15	15000.00	173.50
293.15	20000.00	172.10
293.15	25000.00	171.70
313.15	100.00	190.40
313.15	5000.00	189.80
313.15	10000.00	189.00
313.15	15000.00	187.60
313.15	20000.00	186.70
313.15	25000.00	186.00
333.15	100.00	206.60
333.15	5000.00	206.50
333.15	10000.00	204.90
333.15	15000.00	202.00
333.15	20000.00	200.70
333.15	25000.00	199.90

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
298.15	81.50	0.0025720
Reference		https://www.doi.org/10.1016/j.jct.2016.12.036

Refractive index (Na D-line)

Pressure, kPa - Liquid	Temperature, K - Liquid	Refractive index (Na D-line) - Liquid
100.00	298.15	1.3975
Reference		https://www.doi.org/10.1016/j.jct.2016.01.012

Temperature, K	Pressure, kPa	Refractive index (Na D-line)
294.15	100.00	1.39782
Reference		https://www.doi.org/10.1021/acs.jced.5b01024

Mass density, kg/m3

Temperature, K - Gas	Pressure, kPa - Gas	Mass density, kg/m3 - Gas
528.31	2642.00	113.76
539.69	3127.00	113.76
543.30	3315.00	113.76
546.79	3456.00	113.76
548.15	3531.00	113.76
551.66	3610.00	113.76
558.64	3788.00	113.76
574.48	4178.00	113.76
590.87	4586.00	113.76

605.17	4925.00	113.76
616.28	5197.00	113.76
531.38	2775.00	167.7
543.89	3315.00	167.7
550.45	3647.00	167.7
555.53	3893.00	167.7
557.65	4020.00	167.7
562.14	4275.00	167.7
569.15	4559.00	167.7
580.80	5000.00	167.7
593.16	5452.00	167.7
604.17	5852.00	167.7
616.27	6275.00	167.7
533.03	2834.00	203.9
548.49	3579.00	203.9
555.70	3941.00	203.9
559.33	4118.00	203.9
563.04	4340.00	203.9
568.44	4598.00	203.9
577.73	5059.00	203.9
588.79	5613.00	203.9
600.42	6162.00	203.9
614.97	6834.00	203.9

Reference

<https://www.doi.org/10.1016/j.fluid.2012.09.026>

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
293.15	100.00	809.5
293.15	10000.00	816.4
293.15	20000.00	822.9
293.15	30000.00	828.9
293.15	40000.00	834.5
293.15	50000.00	839.8
293.15	60000.00	844.7
293.15	70000.00	849.6
293.15	80000.00	854.2
293.15	90000.00	858.5
293.15	100000.00	862.9
293.15	110000.00	866.7

293.15	120000.00	870.8
293.15	130000.00	874.4
293.15	140000.00	878.1
303.15	100.00	802.0
303.15	10000.00	809.4
303.15	20000.00	816.0
303.15	30000.00	822.3
303.15	40000.00	828.0
303.15	50000.00	833.6
303.15	60000.00	838.7
303.15	70000.00	843.6
303.15	80000.00	848.3
303.15	90000.00	852.7
303.15	100000.00	857.0
303.15	110000.00	861.2
303.15	120000.00	865.0
303.15	130000.00	868.9
303.15	140000.00	872.6
313.15	100.00	794.1
313.15	10000.00	801.6
313.15	20000.00	809.1
313.15	30000.00	815.4
313.15	40000.00	821.4
313.15	50000.00	827.2
313.15	60000.00	832.6
313.15	70000.00	837.8
313.15	80000.00	842.6
313.15	90000.00	847.3
313.15	100000.00	851.6
313.15	110000.00	856.0
313.15	120000.00	860.1
313.15	130000.00	864.0
313.15	140000.00	867.9
323.15	100.00	786.5
323.15	10000.00	794.5
323.15	20000.00	801.7
323.15	30000.00	808.5
323.15	40000.00	815.0
323.15	50000.00	821.0
323.15	60000.00	826.5
323.15	70000.00	831.5
323.15	80000.00	836.3
323.15	90000.00	841.1
323.15	100000.00	845.8

323.15	110000.00	850.1
323.15	120000.00	854.3
323.15	130000.00	858.3
323.15	140000.00	862.1
333.15	100.00	778.3
333.15	10000.00	786.8
333.15	20000.00	794.6
333.15	30000.00	801.7
333.15	40000.00	808.4
333.15	50000.00	814.6
333.15	60000.00	820.3
333.15	70000.00	825.6
333.15	80000.00	830.8
333.15	90000.00	836.0
333.15	100000.00	840.5
333.15	110000.00	844.9
333.15	120000.00	849.0
333.15	130000.00	853.2
333.15	140000.00	857.0
343.15	100.00	769.9
343.15	10000.00	779.0
343.15	20000.00	787.1
343.15	30000.00	794.4
343.15	40000.00	801.3
343.15	50000.00	807.8
343.15	60000.00	813.6
343.15	70000.00	819.3
343.15	80000.00	824.6
343.15	90000.00	829.5
343.15	100000.00	834.4
343.15	110000.00	838.9
343.15	120000.00	843.3
343.15	130000.00	847.5
343.15	140000.00	851.6
353.15	100.00	760.9
353.15	10000.00	770.6
353.15	20000.00	779.2
353.15	30000.00	787.1
353.15	40000.00	794.3
353.15	50000.00	800.9
353.15	60000.00	807.7
353.15	70000.00	813.2
353.15	80000.00	818.9
353.15	90000.00	823.9

353.15	100000.00	828.8
353.15	110000.00	833.5
353.15	120000.00	838.1
353.15	130000.00	842.1
353.15	140000.00	846.5
363.15	100.00	751.9
363.15	10000.00	762.6
363.15	20000.00	771.7
363.15	30000.00	780.1
363.15	40000.00	787.4
363.15	50000.00	794.3
363.15	60000.00	800.9
363.15	70000.00	807.0
363.15	80000.00	812.5
363.15	90000.00	817.9
363.15	100000.00	822.9
363.15	110000.00	827.7
363.15	120000.00	832.4
363.15	130000.00	836.8
363.15	140000.00	841.0
373.15	100.00	742.4
373.15	10000.00	753.4
373.15	20000.00	763.3
373.15	30000.00	772.2
373.15	40000.00	780.0
373.15	50000.00	787.2
373.15	60000.00	793.8
373.15	70000.00	800.2
373.15	80000.00	805.8
373.15	90000.00	811.5
373.15	100000.00	817.0
373.15	110000.00	821.9
373.15	120000.00	826.3
373.15	130000.00	831.0
373.15	140000.00	835.3
383.15	100.00	732.2
383.15	10000.00	744.7
383.15	20000.00	754.6
383.15	30000.00	764.3
383.15	40000.00	772.2
383.15	50000.00	779.6
383.15	60000.00	786.6
383.15	70000.00	793.2
383.15	80000.00	799.1

383.15	90000.00	804.9
383.15	100000.00	810.3
383.15	110000.00	815.4
383.15	120000.00	820.4
383.15	130000.00	825.0
383.15	140000.00	829.6
393.15	10000.00	735.3
393.15	20000.00	746.4
393.15	30000.00	755.9
393.15	40000.00	764.9
393.15	50000.00	772.3
393.15	60000.00	779.6
393.15	70000.00	786.3
393.15	80000.00	792.8
393.15	90000.00	798.8
393.15	100000.00	804.3
393.15	110000.00	809.7
393.15	120000.00	814.7
393.15	130000.00	819.3
393.15	140000.00	823.9
403.15	10000.00	725.6
403.15	20000.00	737.3
403.15	30000.00	747.7
403.15	40000.00	756.9
403.15	50000.00	765.4
403.15	60000.00	772.8
403.15	70000.00	779.9
403.15	80000.00	786.5
403.15	90000.00	792.6
403.15	100000.00	798.5
403.15	110000.00	803.9
403.15	120000.00	809.1
403.15	130000.00	814.1
403.15	140000.00	819.3

Reference

<https://www.doi.org/10.1016/j.fluid.2010.11.020>

Temperature, K	Pressure, kPa	Mass density, kg/m3
313.10	1013.00	794.97
313.10	2008.00	795.76
313.10	3007.00	796.55
313.10	3990.00	797.33
313.10	5000.00	798.11

313.10	6014.00	798.9
313.10	7006.00	799.69
313.10	8016.00	800.47
313.10	9008.00	801.23
313.10	9996.00	801.97
313.10	11012.00	802.72
313.10	12008.00	803.48
313.10	13036.00	804.23
313.10	14009.00	804.93
313.10	15034.00	805.67
313.10	16014.00	806.36
313.10	17013.00	807.07
313.10	18011.00	807.76
313.10	19027.00	808.46
313.10	20015.00	809.14
313.10	21034.00	809.84
313.10	22060.00	810.53
313.10	23039.00	811.19
313.10	24049.00	811.9
313.10	25048.00	812.56
323.08	1040.00	787.23
323.08	2043.00	788.06
323.08	3005.00	788.88
323.08	4009.00	789.7
323.08	5014.00	790.53
323.08	6024.00	791.38
323.08	7062.00	792.21
323.08	8033.00	792.99
323.08	9025.00	793.79
323.08	10008.00	794.58
323.08	11020.00	795.36
323.08	12027.00	796.15
323.08	13044.00	796.95
323.08	14035.00	797.69
323.08	15055.00	798.46
323.08	16063.00	799.21
323.08	17039.00	799.93
323.08	18057.00	800.67
323.08	18995.00	801.37
323.08	20045.00	802.11
323.08	21090.00	802.85
323.08	22039.00	803.52
323.08	23078.00	804.27
323.08	24010.00	804.94

323.08	25055.00	805.68
332.95	1095.00	779.28
332.95	2064.00	780.15
332.95	3035.00	781.02
332.95	4039.00	781.89
332.95	5007.00	782.76
332.95	6035.00	783.65
332.95	7048.00	784.53
332.95	8021.00	785.37
332.95	9035.00	786.23
332.95	10030.00	787.06
332.95	11057.00	787.9
332.95	12026.00	788.71
332.95	13041.00	789.54
332.95	14034.00	790.33
332.95	15074.00	791.16
332.95	16022.00	791.89
332.95	16957.00	792.61
332.95	18103.00	793.49
332.95	19053.00	794.22
332.95	20044.00	794.97
332.95	21090.00	795.75
332.95	21974.00	796.4
332.95	22960.00	797.13
332.95	24014.00	797.92
332.95	25045.00	798.67
342.89	1021.00	771.26
342.89	2060.00	772.26
342.89	3051.00	773.2
342.89	4044.00	774.13
342.89	5014.00	775.03
342.89	6024.00	775.96
342.89	7050.00	776.88
342.89	8037.00	777.76
342.89	9052.00	778.65
342.89	10057.00	779.53
342.89	11053.00	780.38
342.89	12027.00	781.22
342.89	13077.00	782.09
342.89	14026.00	782.86
342.89	15080.00	783.73
342.89	16028.00	784.48
342.89	17031.00	785.27
342.89	18020.00	786.04

342.89	19009.00	786.8
342.89	20030.00	787.58
342.89	21066.00	788.35
342.89	21978.00	789.03
342.89	23061.00	789.83
342.89	24031.00	790.55
342.89	25045.00	791.3
352.76	1033.00	762.72
352.76	2075.00	763.8
352.76	3038.00	764.75
352.76	4004.00	765.74
352.76	5017.00	766.75
352.76	6042.00	767.75
352.76	7041.00	768.72
352.76	8024.00	769.64
352.76	9042.00	770.61
352.76	10044.00	771.56
352.76	11026.00	772.44
352.76	12073.00	773.4
352.76	13002.00	774.25
352.76	14050.00	775.17
352.76	15000.00	776.03
352.76	15999.00	776.89
352.76	17008.00	777.76
352.76	18066.00	778.65
352.76	19002.00	779.43
352.76	20014.00	780.28
352.76	21043.00	781.12
352.76	22024.00	781.94
352.76	23025.00	782.75
352.76	24015.00	783.56
352.76	25100.00	784.44
362.68	1031.00	753.17
362.68	2065.00	754.33
362.68	3038.00	755.4
362.68	4026.00	756.45
362.68	5050.00	757.54
362.68	6018.00	758.55
362.68	6995.00	759.56
362.68	8100.00	760.7
362.68	9002.00	761.62
362.68	10021.00	762.62
362.68	10995.00	763.58
362.68	12059.00	764.62

362.68	13056.00	765.56
362.68	14029.00	766.47
362.68	15024.00	767.42
362.68	16010.00	768.33
362.68	17020.00	769.25
362.68	18041.00	770.16
362.68	19031.00	771.05
362.68	20045.00	771.93
362.68	21016.00	772.76
362.68	22022.00	773.64

Reference

<https://www.doi.org/10.1016/j.jct.2006.07.009>

Temperature, K	Pressure, kPa	Mass density, kg/m3
278.15	100.00	820.9
278.15	1000.00	821.6
278.15	5000.00	824.4
278.15	10000.00	827.7
278.15	15000.00	830.9
278.15	20000.00	834.0
278.15	25000.00	837.0
278.15	30000.00	839.9
278.15	35000.00	842.7
278.15	40000.00	845.4
278.15	45000.00	848.1
278.15	50000.00	850.7
278.15	55000.00	853.2
278.15	60000.00	855.6
288.15	100.00	813.5
288.15	1000.00	814.1
288.15	5000.00	817.0
288.15	10000.00	820.5
288.15	15000.00	823.9
288.15	20000.00	827.2
288.15	25000.00	830.3
288.15	30000.00	833.2
288.15	35000.00	836.2
288.15	40000.00	839.0
288.15	45000.00	841.7
288.15	50000.00	844.4
288.15	55000.00	846.8
288.15	60000.00	849.4
298.15	100.00	805.8

298.15	1000.00	806.6
298.15	5000.00	809.6
298.15	10000.00	813.3
298.15	15000.00	816.8
298.15	20000.00	820.2
298.15	25000.00	823.5
298.15	30000.00	826.6
298.15	35000.00	829.6
298.15	40000.00	832.6
298.15	45000.00	835.4
298.15	50000.00	838.2
298.15	55000.00	840.9
298.15	60000.00	843.3
308.15	100.00	798.0
308.15	1000.00	798.8
308.15	5000.00	802.0
308.15	10000.00	805.9
308.15	15000.00	809.5
308.15	20000.00	813.0
308.15	25000.00	816.4
308.15	30000.00	819.7
308.15	35000.00	822.8
308.15	40000.00	825.9
308.15	45000.00	828.8
308.15	50000.00	831.7
308.15	55000.00	834.5
308.15	60000.00	837.0
318.15	100.00	790.3
318.15	1000.00	791.1
318.15	5000.00	794.5
318.15	10000.00	798.5
318.15	15000.00	802.4
318.15	20000.00	805.6
318.15	25000.00	809.5
318.15	30000.00	812.9
318.15	35000.00	816.1
318.15	40000.00	819.3
318.15	45000.00	822.4
318.15	50000.00	825.3
318.15	55000.00	828.2
318.15	60000.00	830.9
328.15	100.00	782.3
328.15	1000.00	783.1
328.15	5000.00	786.7

328.15	10000.00	790.9
328.15	15000.00	795.0
328.15	20000.00	798.8
328.15	25000.00	802.4
328.15	30000.00	806.0
328.15	35000.00	809.4
328.15	40000.00	812.7
328.15	45000.00	815.8
328.15	50000.00	818.9
328.15	55000.00	821.8
328.15	60000.00	824.6
338.15	100.00	774.0
338.15	1000.00	774.9
338.15	5000.00	778.7
338.15	10000.00	783.2
338.15	15000.00	787.4
338.15	20000.00	791.4
338.15	25000.00	795.3
338.15	30000.00	799.0
338.15	35000.00	802.5
338.15	40000.00	805.9
338.15	45000.00	809.2
338.15	50000.00	812.4
338.15	55000.00	815.4
338.15	60000.00	818.4
348.15	100.00	765.6
348.15	1000.00	766.3
348.15	5000.00	770.5
348.15	10000.00	775.3
348.15	15000.00	779.8
348.15	20000.00	784.0
348.15	25000.00	788.0
348.15	30000.00	791.8
348.15	35000.00	795.6
348.15	40000.00	799.1
348.15	45000.00	802.5
348.15	50000.00	805.8
348.15	55000.00	809.0
348.15	60000.00	811.9
358.15	100.00	756.6
358.15	1000.00	757.7
358.15	5000.00	761.7
358.15	10000.00	767.0
358.15	15000.00	771.7

358.15	20000.00	776.2
358.15	25000.00	780.4
358.15	30000.00	784.4
358.15	35000.00	788.3
358.15	40000.00	792.0
358.15	45000.00	795.5
358.15	50000.00	799.0
358.15	55000.00	802.3
358.15	60000.00	805.3

Reference

<https://www.doi.org/10.1016/j.jct.2011.10.023>

Pressure, kPa	Temperature, K	Mass density, kg/m3
100.00	302.90	802.0
1020.00	302.90	802.7
2010.00	302.90	803.4
3010.00	302.90	804.1
4000.00	302.90	804.9
5010.00	302.90	805.7
6000.00	302.90	806.4
7020.00	302.90	807.2
8010.00	302.90	807.9
9020.00	302.90	808.7
10020.00	302.90	809.4
100.00	323.10	785.6
1010.00	323.10	786.6
2020.00	323.10	787.5
3010.00	323.10	788.3
4000.00	323.10	789.2
5020.00	323.10	790.0
6020.00	323.10	790.9
7000.00	323.10	791.7
8010.00	323.10	792.5
9020.00	323.10	793.3
10020.00	323.10	794.2

Reference

<https://www.doi.org/10.1016/j.jct.2013.08.007>

Temperature, K	Pressure, kPa	Mass density, kg/m3
298.15	100.00	805.95

Reference

<https://www.doi.org/10.1016/j.jct.2018.07.013>

Temperature, K	Pressure, kPa	Mass density, kg/m3
298.15	81.50	806.07
Reference		https://www.doi.org/10.1021/acs.jced.5b00162

Temperature, K	Pressure, kPa	Mass density, kg/m3
283.63	80.00	817.19
283.64	1000.00	817.88
283.63	5000.00	820.7
283.66	10000.00	824.01
283.66	20000.00	830.39
283.65	30000.00	836.43
283.64	40000.00	842.03
283.64	60000.00	852.39
283.65	80000.00	861.72
283.64	100000.00	870.33
303.45	100.00	801.81
303.45	1000.00	802.54
303.46	5000.00	805.65
303.46	10000.00	809.35
303.47	20000.00	816.29
303.47	30000.00	822.84
303.47	40000.00	828.87
303.47	60000.00	839.95
303.48	80010.00	849.82
303.48	100000.00	858.94
323.26	100.00	786.36
323.25	1000.00	787.19
323.26	5000.00	790.63
323.27	10000.00	794.68
323.27	20000.00	802.33
323.27	30000.00	809.41
323.28	40000.00	816.0
323.28	60000.00	827.77
323.28	80000.00	838.31
323.28	100000.00	847.65
343.03	100.00	769.54
343.03	1000.00	770.45
343.04	5000.00	774.32
343.04	10000.00	778.88
343.05	20000.00	787.37

343.05	30000.00	795.06
343.05	40000.00	802.13
343.05	60000.00	814.83
343.05	80000.00	826.08
343.05	100000.00	836.2
362.68	100.00	752.67
362.68	1000.00	753.64
362.69	5000.00	758.03
362.69	10000.00	763.16
362.69	20000.00	772.56
362.68	30000.00	781.04
362.70	40000.00	788.67
362.70	60000.00	802.36
362.71	80000.00	814.44
362.71	100000.00	825.18

Reference

<https://www.doi.org/10.1021/acs.jced.7b00176>

Temperature, K	Pressure, kPa	Mass density, kg/m3
298.12	2010.00	806.8
298.12	3910.00	808.2
298.12	6020.00	809.8
298.12	8030.00	811.2
298.12	9910.00	812.5
298.13	13010.00	814.6
298.12	16020.00	816.6
298.12	19030.00	818.5
298.12	22000.00	820.4
298.12	25020.00	822.3
298.12	28000.00	824.0
298.12	30010.00	825.1
303.15	2010.00	803.3
303.15	4000.00	804.8
303.15	5980.00	806.3
303.15	8010.00	807.8
303.15	9990.00	809.2
303.15	12990.00	811.3
303.15	15990.00	813.3
303.16	19000.00	815.3
303.15	22010.00	817.3
303.15	25010.00	819.1
303.15	27970.00	820.9
303.15	29990.00	822.1

313.16	1990.00	795.5
313.16	3980.00	797.1
313.16	5990.00	798.7
313.16	7980.00	800.2
313.15	10020.00	801.8
313.15	12980.00	803.9
313.16	15980.00	806.1
313.16	19010.00	808.2
313.15	22020.00	810.2
313.15	25010.00	812.2
313.16	27990.00	814.1
313.16	29990.00	815.3
323.14	2000.00	787.9
323.14	3920.00	789.6
323.14	6030.00	791.3
323.14	8000.00	792.9
323.14	10020.00	794.5
323.14	13040.00	796.9
323.14	16050.00	799.2
323.14	19000.00	801.3
323.14	21990.00	803.4
323.14	24970.00	805.5
323.14	28000.00	807.5
323.14	29970.00	808.8

Reference

<https://www.doi.org/10.1021/acs.jced.8b00812>

Temperature, K	Pressure, kPa	Mass density, kg/m3
293.15	100.00	809.28
293.15	5000.00	813.04
293.15	10000.00	816.54
293.15	15000.00	819.83
293.15	20000.00	822.97
293.15	25000.00	826.0
293.15	30000.00	828.99
293.15	35000.00	831.99
303.15	100.00	801.9
303.15	5000.00	806.0
303.15	10000.00	809.77
303.15	15000.00	813.26
303.15	20000.00	816.52
303.15	25000.00	819.61
303.15	30000.00	822.58

303.15	35000.00	825.48
313.15	100.00	794.32
313.15	5000.00	798.42
313.15	10000.00	802.22
313.15	15000.00	805.8
313.15	20000.00	809.2
313.15	25000.00	812.49
313.15	30000.00	815.73
313.15	35000.00	818.97

Reference

<https://www.doi.org/10.1021/acs.jced.8b00975>

Temperature, K	Pressure, kPa	Mass density, kg/m3
283.15	550.80	818.14
283.15	11959.00	825.705
283.15	18047.00	829.455
283.15	32971.00	838.117
283.15	62025.00	852.74
283.15	267.60	817.937
283.15	2020.20	819.134
283.15	7034.80	822.538
283.15	9991.90	824.485
283.15	15011.00	827.609
283.15	25044.00	833.615
283.15	28046.00	835.368
283.15	32970.00	838.092
283.15	34960.00	839.141
283.15	37943.00	840.737
283.15	44940.00	844.325
283.15	49996.00	846.902
283.15	51982.00	847.942
283.15	57949.00	850.826
283.15	991.30	818.415
283.15	2914.80	819.722
283.15	4946.50	821.145
283.15	9021.60	823.807
283.15	34017.00	838.557
283.15	40004.00	841.811
283.15	42058.00	842.896
283.15	54965.00	849.358
283.15	64998.00	854.215
283.15	878.60	818.388
283.15	20045.00	830.642

283.15	30052.00	836.501
283.15	48022.00	845.954
283.15	59996.00	851.847
283.15	22057.00	831.928
283.16	65971.00	854.69
283.16	101.20	817.825
288.15	882.70	814.204
288.15	2917.80	815.651
288.15	9018.60	819.847
288.15	10040.00	820.583
288.15	20693.00	827.38
288.15	32084.00	834.074
288.15	37993.00	837.311
288.15	40041.00	838.449
288.15	44979.00	841.064
288.15	52032.00	844.696
288.15	55077.00	846.251
288.15	61974.00	849.542
288.15	64942.00	850.93
288.15	391.30	813.84
288.15	66025.00	851.488
288.15	7088.80	818.541
288.15	12072.00	821.91
288.15	17968.00	825.72
288.15	78.50	813.612
288.15	25002.00	829.984
288.15	28026.00	831.832
288.15	30035.00	832.896
288.15	33050.00	834.714
288.15	34036.00	835.152
288.15	50068.00	843.734
288.15	554.40	813.953
288.15	2057.50	815.033
288.15	5041.40	817.16
288.15	15001.00	823.877
288.15	20068.00	826.976
288.15	22020.00	828.211
288.15	35077.00	835.674
288.15	42023.00	839.459
288.15	989.10	814.282
288.15	48045.00	842.655
288.15	58004.00	847.666
288.15	59988.00	848.618
293.15	33151.00	832.036

293.15	28066.00	829.163
293.15	58072.00	845.282
293.15	825.10	811.053
293.15	66045.00	849.224
293.15	21987.00	825.417
293.15	27986.00	829.06
293.15	35000.00	833.078
293.15	45068.00	838.658
293.15	1971.70	811.916
293.15	3060.60	812.72
293.15	5011.00	814.074
293.15	9042.10	816.992
293.15	91.10	810.528
293.15	10036.00	817.626
293.15	11947.00	818.963
293.15	14941.00	820.924
293.15	34099.00	832.526
293.15	40081.00	835.959
293.15	42099.00	837.008
293.15	54966.00	843.81
293.16	1045.20	811.221
293.16	7096.80	815.616
293.16	17889.00	822.832
293.16	19992.00	824.147
293.16	24983.00	827.251
293.16	29976.00	830.11
293.16	32232.00	831.521
293.16	476.40	810.81
293.16	38027.00	834.783
293.16	48022.00	840.192
293.16	50085.00	841.31
293.16	52032.00	842.308
293.16	60018.00	846.257
293.16	64991.00	848.649
293.16	305.20	810.686
293.16	61962.00	847.209
298.15	33113.00	828.365
298.15	45021.00	835.052
298.15	55016.00	840.375
298.15	65018.00	845.412
298.15	10107.00	813.67
298.15	38097.00	831.213
298.15	40161.00	832.357
298.15	57931.00	841.819

298.15	59914.00	842.826
298.15	22004.00	821.641
298.15	50068.00	837.797
298.15	62036.00	843.934
298.15	5067.60	810.04
298.15	305.40	806.45
298.15	42029.00	833.462
298.15	1980.90	807.747
298.15	48107.00	836.745
298.15	3167.80	808.637
298.15	7065.30	811.55
298.15	854.50	806.874
298.15	20128.00	820.445
298.15	25081.00	823.55
298.15	33924.00	828.845
298.15	98.10	806.282
298.15	42359.00	833.614
298.16	9120.90	813.012
298.16	11970.00	814.957
298.16	15220.00	817.234
298.16	17984.00	819.076
298.16	28040.00	825.42
298.16	30089.00	826.686
298.16	32030.00	827.814
298.16	35217.00	829.575
298.16	52020.00	838.835
298.16	493.70	806.599
298.16	1012.60	806.992
298.16	66118.00	845.919
303.15	498.90	802.435
303.15	32862.00	824.267
303.15	34081.00	824.9
303.15	39904.00	828.27
303.15	1977.60	803.554
303.15	52073.00	834.942
303.15	55075.00	836.525
303.15	57989.00	838.099
303.15	64988.00	841.599
303.15	33112.00	824.372
303.15	304.10	802.278
303.15	62052.00	840.165
303.15	4930.40	805.792
303.15	42014.00	829.398
303.15	44896.00	831.035

303.15	50065.00	833.864
303.15	979.10	802.787
303.15	19974.00	816.207
303.15	21920.00	817.555
303.15	31958.00	823.711
303.15	34980.00	825.355
303.15	59979.00	839.13
303.15	66030.00	842.119
303.15	11975.00	810.901
303.15	900.60	802.733
303.15	15044.00	812.956
303.15	24992.00	819.44
303.15	37951.00	827.164
303.15	47951.00	832.781
303.16	10014.00	809.449
303.16	18021.00	814.973
303.16	27933.00	821.256
303.16	29990.00	822.537
303.16	8858.20	808.638
303.16	2964.90	804.3
303.16	100.00	802.125
303.16	7045.60	807.335
308.15	12009.00	807.267
308.15	803.30	798.75
308.15	17850.00	811.315
308.15	21988.00	814.131
308.15	27955.00	817.999
308.15	32886.00	820.911
308.15	1916.70	799.642
308.15	4990.20	802.048
308.15	2980.70	800.489
308.15	19930.00	812.759
308.15	25012.00	816.144
308.15	31929.00	820.41
308.15	32941.00	821.059
308.15	37971.00	823.987
308.15	54982.00	833.542
308.15	9863.10	805.692
308.15	40011.00	825.154
308.15	8864.30	804.962
308.15	494.10	798.504
308.15	58009.00	835.036
308.15	1039.50	798.954
308.15	29906.00	819.191

308.15	34011.00	821.636
308.15	45017.00	828.081
308.15	50044.00	830.856
308.15	61985.00	837.136
308.15	64981.00	838.691
308.15	41998.00	826.392
308.15	48033.00	829.748
308.15	51977.00	831.933
308.15	6964.90	803.548
308.15	274.30	798.317
308.15	60030.00	836.098
308.16	15069.00	809.4
308.16	34949.00	822.224
308.16	85.20	798.155
308.16	66088.00	839.237
313.15	17921.00	807.72
313.15	24862.00	812.41
313.15	15059.00	805.716
313.15	19932.00	809.082
313.15	10209.00	802.164
313.15	6921.80	799.704
313.15	12020.00	803.525
313.15	5111.80	798.292
313.15	27869.00	814.438
313.15	29957.00	815.731
313.15	54924.00	830.321
313.15	32980.00	817.674
313.15	33981.00	818.214
313.15	2109.70	795.902
313.15	41978.00	822.973
313.15	59932.00	832.96
313.15	1088.80	795.074
313.15	32107.00	817.091
313.15	33002.00	817.783
313.15	38127.00	820.76
313.15	47880.00	826.39
313.15	103.10	794.254
313.15	52097.00	828.677
313.15	62004.00	834.048
313.15	66113.00	836.222
313.15	22058.00	810.55
313.15	316.00	794.433
313.15	9210.70	801.445
313.15	35045.00	818.819

313.15	44946.00	824.676
313.15	3137.00	796.707
313.15	58082.00	831.994
313.15	569.60	794.643
313.15	64954.00	835.652
313.16	860.70	794.888
313.16	39997.00	821.817
313.16	50021.00	827.556
318.15	11896.00	799.896
318.15	66028.00	833.327
318.15	33016.00	814.458
318.15	37838.00	817.415
318.15	59923.00	830.12
318.15	2933.20	792.866
318.15	8989.00	797.678
318.15	44884.00	821.648
318.15	72.70	790.456
318.15	18102.00	804.461
318.15	47944.00	823.402
318.15	150.10	790.516
318.15	57972.00	829.016
318.15	336.30	790.675
318.15	22094.00	807.257
318.15	29998.00	812.541
318.15	19985.00	805.78
318.15	40093.00	818.817
318.15	1105.70	791.334
318.15	54944.00	827.433
318.15	10075.00	798.523
318.15	1929.10	792.026
318.15	65022.00	832.785
318.16	27909.00	811.139
318.16	31957.00	813.824
318.16	891.00	791.16
318.16	34110.00	815.009
318.16	35048.00	815.63
318.16	6926.70	796.098
318.16	41996.00	819.89
318.16	5020.80	794.556
318.16	49950.00	824.565
318.16	14800.00	802.072
318.16	52037.00	825.741
318.16	61930.00	831.241
318.16	24873.00	809.191

318.16	590.90	790.894
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323.15	58045.00	825.293
323.15	17981.00	800.333
323.15	2006.90	787.814
323.15	54964.00	823.594
323.15	60050.00	826.448
323.15	64999.00	829.093
323.15	35113.00	811.773
323.15	9029.90	793.564
323.15	2966.60	788.632
323.15	48025.00	819.642
323.15	95.00	786.145
323.15	52114.00	821.994
323.15	20038.00	801.815
323.15	4996.20	790.328
323.15	34081.00	811.155
323.15	24993.00	805.264
323.15	7042.10	792.001
323.15	15111.00	798.229
323.15	62131.00	827.565
323.15	32079.00	809.955
323.15	37953.00	813.623
323.15	528.40	786.535
323.15	10090.00	794.392
323.15	42011.00	816.075
323.15	21995.00	803.198
323.15	994.20	786.944
323.15	11914.00	795.8
323.16	30055.00	808.674
323.16	27958.00	807.28
323.16	33067.00	810.61
323.16	40047.00	814.861
323.16	44937.00	817.856
323.16	920.70	786.888
323.16	66131.00	829.687
328.15	33066.00	807.772
328.15	35030.00	808.989
328.15	38010.00	810.915
328.15	44953.00	815.144
328.15	47978.00	816.959
328.15	49927.00	818.128
328.15	54947.00	821.045

328.15	59991.00	823.77
328.15	27979.00	804.324
328.15	61982.00	824.89
328.15	65032.00	826.439
328.15	66046.00	826.965
328.15	5013.40	786.446
328.15	2996.70	784.66
328.15	24924.00	802.164
328.15	57939.00	822.658
328.15	994.10	782.825
328.15	39969.00	812.181
328.15	34013.00	808.285
328.15	41959.00	813.311
328.15	289.90	782.179
328.15	51997.00	819.32
328.15	32060.00	807.104
328.15	29958.00	805.68
328.15	33107.00	807.703
328.15	9017.00	789.881
328.15	97.90	781.987
328.15	10040.00	790.727
328.15	897.50	782.733
328.15	6974.90	788.15
328.15	1988.80	783.741
328.16	20279.00	798.799
328.16	12210.00	792.522
328.16	18061.00	797.122
328.16	22013.00	800.057
328.16	15055.00	794.783
328.16	501.00	782.371
333.15	34086.00	805.827
333.15	37894.00	808.332
333.15	4997.40	783.921
333.15	47936.00	814.509
333.15	51953.00	816.927
333.15	58057.00	820.5
333.15	32067.00	804.524
333.15	62049.00	822.689
333.15	35075.00	806.492
333.15	40111.00	809.759
333.15	30016.00	803.156
333.15	22034.00	797.567
333.15	66005.00	824.853
333.15	44974.00	812.823

333.15	45490.00	813.093
333.15	49920.00	815.727
333.15	54876.00	818.691
333.15	7002.40	785.686
333.15	59993.00	821.547
333.15	64970.00	824.293
333.15	10210.00	788.367
333.15	41947.00	810.938
333.15	9032.00	787.401
333.15	532.60	779.903
333.15	28040.00	801.782
333.15	1987.20	781.249
333.15	897.80	780.245
333.15	3023.40	782.177
333.15	15008.00	792.251
333.16	303.50	779.691
333.16	25027.00	799.667
333.16	12011.00	789.847
333.16	20036.00	796.123
333.16	1003.00	780.346
333.16	17992.00	794.568
333.16	87.70	779.482
333.16	33073.00	805.134
338.15	25026.00	796.362
338.15	22041.00	794.077
338.15	14885.00	788.349
338.15	35012.00	803.345
338.15	52127.00	814.375
338.15	60014.00	819.058
338.15	65012.00	821.872
338.15	66057.00	822.451
338.15	47971.00	811.881
338.15	57940.00	817.865
338.15	32882.00	801.907
338.15	10034.00	784.276
338.15	44978.00	809.926
338.15	19927.00	792.473
338.15	49999.00	813.099
338.15	898.50	775.911
338.15	41990.00	808.025
338.15	5018.60	779.821
338.15	309.80	775.333
338.15	2936.10	777.859
338.15	29994.00	799.911

338.15	39987.00	806.717
338.15	17956.00	790.925
338.15	80.90	775.106
338.15	33937.00	802.603
338.15	561.60	775.578
338.15	1014.10	776.019
338.16	2000.20	776.987
338.16	6917.30	781.55
338.16	11959.00	785.981
338.16	27976.00	798.446
338.16	54992.00	816.085
338.16	31949.00	801.318
338.16	62074.00	820.252
338.16	37962.00	805.345
338.16	9046.90	783.457
338.16	67534.00	823.221
343.15	1017.70	770.563
343.15	52026.00	808.534
343.15	4994.80	774.313
343.15	30082.00	794.441
343.15	297.30	769.853
343.15	911.70	770.459
343.15	65070.00	815.911
343.15	44927.00	804.186
343.15	33097.00	796.546
343.15	520.30	770.07
343.15	2332.50	771.83
343.15	2968.30	772.434
343.15	61967.00	814.212
343.15	10060.00	778.847
343.15	6976.60	776.117
343.15	47908.00	806.033
343.15	1994.60	771.497
343.15	73.70	769.631
343.15	12025.00	780.506
343.15	59944.00	813.181
343.15	19985.00	786.983
343.15	66059.00	816.518
343.15	17975.00	785.398
343.15	9002.60	777.941
343.15	28045.00	793.012
343.15	40012.00	801.058
343.15	25091.00	790.858
343.15	14928.00	782.929

343.15	35030.00	797.771
343.15	50059.00	807.349
343.15	22033.00	788.56
343.15	32170.00	795.891
343.15	41972.00	802.307
343.15	37943.00	799.701
343.16	34034.00	797.101
343.16	54919.00	810.24
343.16	57986.00	812.021
348.15	49950.00	804.611
348.15	88.80	765.578
348.15	3051.10	768.513
348.15	859.80	766.355
348.15	64942.00	813.608
348.15	5094.00	770.529
348.15	40026.00	798.192
348.15	47915.00	803.304
348.15	22163.00	785.27
348.15	66153.00	814.319
348.15	1974.90	767.461
348.15	35045.00	794.751
348.15	57945.00	809.531
348.15	52167.00	805.991
348.15	20111.00	783.649
348.15	55022.00	807.759
348.15	33959.00	793.985
348.15	30149.00	791.333
348.15	32161.00	792.797
348.15	462.20	765.945
348.15	14792.00	779.258
348.15	974.20	766.465
348.15	37937.00	796.729
348.15	10025.00	775.087
348.15	60030.00	810.761
348.15	42066.00	799.57
348.15	28080.00	789.8
348.16	7050.20	772.352
348.16	45051.00	801.465
348.16	32942.00	793.364
348.16	9003.20	774.145
348.16	291.70	765.77
348.16	62063.00	811.961
348.16	17899.00	781.843
348.16	25100.00	787.55

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353.15	21894.00	781.405
353.15	4963.90	766.051
353.15	17977.00	778.173
353.15	336.00	761.273
353.15	40143.00	795.172
353.15	19937.00	779.792
353.15	29936.00	787.797
353.15	12128.00	772.98
353.15	52082.00	803.184
353.15	10005.00	771.015
353.15	45002.00	798.55
353.15	48029.00	800.525
353.15	926.00	761.914
353.15	7000.90	768.126
353.15	32961.00	790.048
353.15	37913.00	793.571
353.15	1016.40	762.008
353.15	50145.00	801.944
353.15	34945.00	791.423
353.15	60098.00	808.146
353.15	14954.00	775.544
353.15	42067.00	796.559
353.15	65063.00	811.071
353.15	2992.10	764.106
353.15	31876.00	789.263
353.15	86.20	760.995
353.15	24908.00	783.869
353.15	27850.00	786.199
353.15	9062.30	770.136
353.15	57980.00	806.879
353.15	55132.00	805.077
353.15	572.60	761.533
353.16	2113.40	763.181
353.16	62043.00	809.275
353.16	33964.00	790.701
353.16	66024.00	811.636
358.15	60043.00	804.453
358.15	17041.00	772.871
358.15	32793.00	786.01
358.15	50038.00	798.154
358.15	926.80	756.64
358.15	31978.00	785.37
358.15	4930.00	760.98

358.15	52081.00	799.474
358.15	37872.00	789.731
358.15	55073.00	801.393
358.15	62067.00	805.674
358.15	28035.00	782.278
358.15	33850.00	786.716
358.15	17965.00	773.738
358.15	66109.00	808.067
358.15	47958.00	796.761
358.15	40037.00	791.31
358.15	35027.00	787.554
358.15	64986.00	807.407
358.15	22175.00	777.415
358.15	14905.00	770.903
358.15	1013.90	756.732
358.15	12137.00	768.259
358.15	42100.00	792.749
358.15	25059.00	779.849
358.15	3021.20	758.947
358.15	508.40	756.19
358.15	57918.00	803.161
358.15	10073.00	766.29
358.15	264.10	755.935
358.15	30002.00	783.844
358.16	2083.90	757.886
358.16	95.10	755.754
358.16	45054.00	794.81
358.16	9030.20	765.202
358.16	20162.00	775.665
358.16	6993.50	763.142
363.15	50050.00	794.458
363.15	34000.00	783.178
363.15	54940.00	797.589
363.15	37919.00	786.081
363.15	31961.00	781.745
363.15	4979.20	757.84
363.15	11971.00	764.806
363.15	47947.00	793.03
363.15	27993.00	778.673
363.15	94.00	752.456
363.15	35028.00	783.945
363.15	42016.00	788.986
363.15	59980.00	800.724
363.15	30062.00	780.285

363.15	17973.00	770.255
363.15	33033.00	782.563
363.15	57917.00	799.479
363.15	601.70	753.061
363.15	892.90	753.404
363.15	19940.00	771.991
363.15	39916.00	787.488
363.15	52023.00	795.718
363.15	334.00	752.741
363.15	2940.40	755.648
363.15	961.60	753.487
363.15	1986.00	754.594
363.15	64924.00	803.734
363.15	66088.00	804.418
363.15	1034.70	753.567
363.15	9959.50	762.855
363.15	62043.00	802.008
363.15	14936.00	767.534
363.15	24872.00	776.146
363.16	8964.80	761.886
363.16	21933.00	773.696
363.16	44987.00	791.029
363.16	6920.20	759.821

Reference

<https://www.doi.org/10.1021/je5010214>

Temperature, K	Pressure, kPa	Mass density, kg/m3
313.08	1006.00	795.22
313.08	2017.00	796.08
313.08	3007.00	796.85
313.08	4010.00	797.64
313.08	5016.00	798.44
313.08	6017.00	799.22
313.08	7011.00	800.0
313.08	8006.00	800.77
313.08	9019.00	801.53
313.08	10008.00	802.27
313.08	11014.00	803.01
313.08	12016.00	803.73
313.08	13016.00	804.46
313.08	14013.00	805.18
313.08	15010.00	805.91
313.08	16003.00	806.58

313.08	16999.00	807.29
313.08	17999.00	807.98
313.08	19024.00	808.67
313.08	20005.00	809.33
313.08	21013.00	810.09
313.08	22003.00	810.75
313.08	23024.00	811.41
313.08	24027.00	812.09
313.08	24234.00	812.21
323.05	999.00	787.38
323.05	2026.00	788.22
323.05	3007.00	789.03
323.05	4024.00	789.91
323.05	5012.00	790.75
323.05	6016.00	791.57
323.05	7023.00	792.4
323.05	8004.00	793.16
323.05	9009.00	793.98
323.05	10007.00	794.78
323.05	11004.00	795.57
323.05	11995.00	796.32
323.05	13007.00	797.09
323.05	14022.00	797.85
323.05	14989.00	798.63
323.05	16006.00	799.33
323.05	16998.00	800.1
323.05	18001.00	800.84
323.05	19025.00	801.56
323.05	19993.00	802.28
323.05	21032.00	803.06
323.05	22006.00	803.74
323.05	22993.00	804.41
323.05	24012.00	805.16
323.05	24418.00	805.43
332.93	1013.00	779.33
332.93	2026.00	780.27
332.93	3014.00	781.21
332.93	4006.00	782.04
332.93	5000.00	782.91
332.93	6013.00	783.78
332.93	6997.00	784.6
332.93	8003.00	785.5
332.93	9005.00	786.32
332.93	10001.00	787.17

332.93	10996.00	787.97
332.93	12003.00	788.8
332.93	12993.00	789.62
332.93	14001.00	790.38
332.93	15016.00	791.22
332.93	15998.00	791.96
332.93	16999.00	792.72
332.93	18009.00	793.53
332.93	18986.00	794.29
332.93	20043.00	795.08
332.93	21056.00	795.87
332.93	22040.00	796.59
332.93	23009.00	797.3
332.93	24001.00	798.04
332.93	24515.00	798.46
342.86	1026.00	770.92
342.86	2007.00	771.87
342.86	3003.00	772.85
342.86	4051.00	773.84
342.86	5008.00	774.72
342.86	6023.00	775.59
342.86	7010.00	776.55
342.86	8000.00	777.42
342.86	9001.00	778.28
342.86	10005.00	779.2
342.86	11006.00	780.06
342.86	12010.00	780.9
342.86	13033.00	781.77
342.86	14017.00	782.62
342.86	15001.00	783.45
342.86	16009.00	784.29
342.86	17016.00	785.14
342.86	17991.00	785.93
342.86	19023.00	786.79
342.86	19999.00	787.57
342.86	21000.00	788.37
342.86	22003.00	789.15
342.86	22989.00	789.91
342.86	24004.00	790.69
342.86	24621.00	791.2
352.79	1020.00	762.66
352.79	2014.00	763.68
352.79	3007.00	764.68
352.79	3998.00	765.67

352.79	4998.00	766.69
352.79	5997.00	767.68
352.79	7006.00	768.64
352.79	8005.00	769.61
352.79	9007.00	770.53
352.79	9997.00	771.44
352.79	11008.00	772.38
352.79	12000.00	773.26
352.79	13043.00	774.22
352.79	14002.00	775.11
352.79	15000.00	775.98
352.79	16000.00	776.85
352.79	16992.00	777.72
352.79	17988.00	778.56
352.79	18994.00	779.41
352.79	20012.00	780.22
352.79	21003.00	781.04
352.79	22010.00	781.87
352.79	22971.00	782.68
352.79	24021.00	783.49
352.79	24573.00	783.95
362.67	1043.00	753.5
362.67	2116.00	754.77
362.67	3026.00	755.74
362.67	4013.00	756.82
362.67	5024.00	757.87
362.67	6047.00	758.93
362.67	7014.00	759.93
362.67	8012.00	760.98
362.67	9025.00	762.03
362.67	10015.00	762.94
362.67	11002.00	763.92
362.67	12002.00	764.89
362.67	13011.00	765.86
362.67	14011.00	766.84
362.67	15014.00	767.7
362.67	16006.00	768.67
362.67	17009.00	769.58
362.67	18008.00	770.48
362.67	18993.00	771.37
362.67	19990.00	772.21
362.67	21007.00	773.1
362.67	21997.00	773.96
362.67	23014.00	774.89

362.67	24000.00	775.58
362.67	24563.00	776.12
Reference		https://www.doi.org/10.1021/je700261b

Speed of sound, m/s

Temperature, K - Liquid	Pressure, kPa - Liquid	Speed of sound, m/s - Liquid
253.15	108.00	1399.203
253.15	5065.00	1423.053
253.15	10086.00	1446.233
253.15	15035.00	1468.319
253.15	20115.00	1490.177
253.15	25062.00	1510.75
253.15	30526.00	1532.696
273.15	103.00	1326.117
273.15	5008.00	1351.87
273.15	10094.00	1377.167
273.15	15185.00	1401.443
273.15	20115.00	1424.124
273.15	25088.00	1446.132
273.15	30170.00	1467.891
293.15	104.00	1256.423
293.15	5067.00	1284.566
293.15	10144.00	1311.663
293.15	15081.00	1336.897
293.15	20094.00	1361.485
293.15	25087.00	1384.998
293.15	30176.00	1408.068
313.15	100.00	1189.161
313.15	5050.00	1219.204
313.15	10082.00	1248.164
313.15	15167.00	1275.967
313.15	20187.00	1302.165
313.15	25473.00	1328.5
313.15	30162.00	1351.047
333.15	99.00	1122.893
333.15	5055.00	1155.491
333.15	10099.00	1186.761
333.15	15058.00	1215.841
333.15	20149.00	1244.214

333.15	25167.00	1270.825
333.15	30276.00	1296.753
353.15	100.00	1056.353
353.15	5013.00	1091.582
353.15	10032.00	1125.304
353.15	15066.00	1157.065
353.15	20085.00	1186.968
353.15	25075.00	1215.14
353.15	30204.00	1242.721

Reference

<https://www.doi.org/10.1016/j.jct.2015.10.006>

Temperature, K	Pressure, kPa	Speed of sound, m/s
250.00	67.00	1411.8
218.17	100.00	1536.6
249.99	100.00	1412.0
300.04	101.00	1234.1
350.11	104.00	1067.1
400.14	145.00	891.2
449.96	576.00	696.4
350.11	911.00	1073.1
400.14	933.00	898.8
300.03	1100.00	1240.0
218.25	1111.00	1540.5
449.96	1176.00	704.8
499.96	1636.00	472.8
400.14	1839.00	907.3
449.96	2010.00	716.0
249.99	2060.00	1421.4
350.11	2067.00	1081.4
218.26	2129.00	1544.8
300.03	2196.00	1246.4
499.96	2336.00	490.0
350.11	4569.00	1099.0
400.14	4864.00	934.6
499.96	4923.00	544.0
249.99	5075.00	1435.7
300.03	5369.00	1264.5
218.31	5399.00	1558.2
499.96	7243.00	586.7
249.98	9057.00	1453.9
350.11	9077.00	1129.2
400.12	9483.00	973.3

449.96	9527.00	803.9
218.28	9570.00	1575.2
300.03	9681.00	1288.1
499.96	9870.00	626.9
499.95	19314.00	741.4
218.22	19695.00	1614.9
300.03	20060.00	1341.4
350.11	20660.00	1199.6
400.14	20722.00	1055.9
449.96	21165.00	910.4
249.98	22437.00	1511.7
499.91	25968.00	806.2
400.14	36029.00	1150.7
217.92	39005.00	1685.4
449.96	39912.00	1043.3
300.03	40032.00	1432.5
499.95	40048.00	918.1
250.01	40124.00	1581.1
350.10	40651.00	1303.9
249.98	58985.00	1648.4
400.14	59027.00	1269.1
300.02	59057.00	1509.0
350.10	59555.00	1388.7
218.12	59881.00	1753.2
449.96	59899.00	1156.8
499.96	60162.00	1045.7
400.14	79223.00	1357.8
249.98	79282.00	1714.5
300.02	79463.00	1582.8
449.96	79678.00	1251.8
218.18	79839.00	1813.2
499.96	80004.00	1149.3
350.09	80590.00	1472.2

Reference

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Sources

Isobaric VLE data for the system of butan-1-ol + butylethanoate + butylpropanoate + butyldimethylphosphite

Solubility and Thermodynamics of Betaine in Different Pure Solvents and Binary Organic Solvents at Different Temperatures:

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Solubility Modeling and Solvent Effect of 2-Amino-6-chloropurine in Twelve Neat Solvents: of the solubility, dissolution enthalpy and entropy of solution of 6-chloropurine Hydrogen Sulfate Formanil) in Different Solvents: Thermodynamic equilibrium of hydroxyacetic acid in pure and binary solvent systems; osity of 1-butyl-3-methylimidazolium nitrate with various Meas preparation and Correlation of 3-Oxapentane-1,2-Dione Organic Vapor-Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry; Determination of a Wilson Thermodynamic Modeling of 2-Methyl-2-butanol and its binary mixtures with ethyl formate and ethyl acetate; solubilities of 1-butylmethane + 2-butylpropanol in diethylether liquid T phase equilibria in 1-butanol, oleic acid, water and n-heptane mixtures: Determination of Solid-Liquid Equilibrium and Correlation of the Self-Diffusion Coefficients of Seven Monoalcohols and Two Different Binary Ternary Mixtures and Alcohol Systems: Properties of pure 1-methylimidazolium acetate ionic liquid and its binary mixtures; Determination and Thermodynamic Mixing Properties of Determination and Modeling of Acid in Chloroform Solubility in Several Pure Solvents from 298.15 to 303.15 K: Compressibilities in Binary Mixtures of Determination and Correlation of Solubility and Thermodynamic Properties of Trans-stilbene in Alcohol in Methanol Ethanol 1-Propanol 253.15 Methylcyclopentanediol Tetrahydrofuran, model of thermodynamic properties density and refractive index coefficients aliphatic alcohols of ethanol and propanol hydrocarbons sulfur dioxide in dimethyl sulfoxide (DMSO), MPB, and Water in Ionic Liquid [BMIM][SCN] using 1-Butyl-3-methylimidazolium Tetrafluoroborate ([M][TfPB]) Volumes of N-methylmorpholine Diurethane of Systems Gases and Crystal Structure: mixtures of some primary alcohols with 2-hydroxy-2-methylpropane and solubility of 2-nitrobenzaldehyde in different solvents at a constant temperature 177.15 K: manual sampling method developed with experimental data consisting of benzoic acid in C₆H₅Alcohol Solubilities of 2-Methyl-2-butanol (1) + 1-Alkanols Part II (2) at 298.15 K liquid equilibria for binary systems of propanol/CaCl₂ and Octanol/CaCl₂: coefficients at infinite dilution measurements for organic solutes and volatility measurement and Thermodynamic Model Correlation of Vapor-Liquid Equilibria for Monofluoroalkanes, Difluoroalkanes and Chloroalkanes Vapor-Liquid Equilibrium for Solubility Measurements and Thermodynamic Functions of propane Determination and Correlation of Equilibrium Vapor Pressures of pure and binary mixtures for the consideration of alcohols /bmim]PF₆ at different temperatures by Differential Scanning Calorimetry: Determination of the Self-Diffusion Coefficients of 1-butyl-3-methylimidazolium hexafluorophosphate in water and several other solvents Measurement and correlation of solubility of Tetracycline hydrochloride in binary and ternary systems Modeling of Sulfanilamide in 12 Mono Solvents and binary mixtures of mono- and binary mixtures of 2-thio-1,3-dioxane in lower molecular enthalpies of ethylformate and (1-propanol, 2-propanol and 1-butanol, 2-butanol, properties of neat mixtures (298.15 and 308.15) K and p = 35 kPa in 1-methyl-3-imidazolium trifluoromethanesulfonate ionic liquid:

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Measurement and correlation of the solubility of

Thermodynamic behavior of alkyl lactate-alkanol systems:

Physical properties of systems of interest to the edible oil industry:

Acoustic and thermodynamic model for binary liquid mixtures of fatty acids

Activity coefficients at infinite dilution of alcohols in binary mixtures

Physical properties for binary mixtures of alcohols and water

On the interactions between furfural and alcohols

Thermodynamic properties of mixtures containing ionic liquids

Solubility of L-ascorbic acid in eight organic solvents

Extraction of Oxalic Acid from Dilute Aqueous Solutions by Methylene Chloride

Effect of Temperature and Solvent Effects on the Solubility of Oxalic Acid in 15 Organic Solvents

Density and surface tension of pure ionic liquid

Solubility of methylimidazolium L-lactate in chloroform, nitrobenzene, and p-toluenesulfonic acid

Measurement of the effect of temperature and composition on the effect of pressure

Correlation of Solubilities of Asiaticoside in Water, Methanol, Ethanol, and Propylene Glycol

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Saturated Solubility and Thermodynamic Evaluation of Surface Tension in the Ternary Mixtures Containing the Ternary Substances by the Gravimetric Method at 298.15 K: 2-pentanol ternary system at 0.019 kPa and correlation of solubility and solution thermodynamics by using the equilibrium for Ternary Systems - Butanol + n-Hexane + Polyethylene Glycol in Binary System in Ethanol, 1-Propanol, 1-Butanol, Benzene, and Decalene as Solvents, and Excess Activity Coefficients and Activity Ratios Between 23°C and 36°C in Hexane and Butanol of solubility and solution thermodynamics by using the gravimetric method at different pressures (vacuum) and ethanol difference between carbon dioxide + 1-butanol at temperatures from (293.15 to 323.15) K; thermodynamic functions of saturated vapor pressure based on activity coefficients at infinite dilution molar volumes of Di-n-propylamine, tri(n-butyl)phosphine, methyl phosphonates of the type AS (n-butyl)-alkoxide (S1-C6) and Their Correlations of 298.15 K and Ambient Temperatures Database); Mutual diffusion coefficients of n-butanol + n-heptane and n-pentanol + n-heptane from liquid phase equilibria for the binary systems of tert-butanol + diethyl malic acid and tert-butanol + tetrahydrofuran and their relation to thermodynamic models for solid liquid equilibrium of the pure and mixture organic substances at different temperatures limiting activity coefficient of simvastatin in different organic solvents; Equilibrium Behaviors of 5-Methyl-2-(1-methylethyl)phenol in Measurement and Correlation of Solubilities of Luteolin in Organic Solvents at Different Temperatures; Propanediol with Methanol, Ethanol, Methylpropanediol, tert-butanol solubility and mixing properties of malonic acid in the non-aqueous organic solvent phase equilibria study of the binary systems in hexyloquinoline and transport properties of (tert-butylamino)imide + acetonitrile in organic mixtures of organic solvents and ethyl alcohol + water) measurement of water/butan-1-ol with ionic liquids in ternary liquid-liquid phase equilibria and activity coefficients at infinite dilution for Excess Enthalpy, Density and Speed of Sound for the Mixtures of Pinene + Heptanediol, 1-Butanol + 2-Pentanol, 2-Pentanol + 1-Butanol and Extraction on Investigation of Limiting of Activity Coefficients Form III) in Different Solvents from (275 to 343) Kobaric vapor-liquid equilibria for water + n-propanol + n-butanol ternary system and osmotic pressure study on infinite dilution activity coefficients of liquid-liquid equilibrium of water / ionic liquid butanediol + 1-butanol at T = 298.15 K; butanol + propanediol in different organic solvents; Solubility of 4-methyl-2-nitroaniline in fourteen organic solvents from T = (273.15 to 313.15) K; van Raaij mixing measurements of activity coefficients at infinite dilution in various organic solvents in water; Water as a Solute in Non-Aqueous and Overcritical Solvent Liquid-Liquid Equilibrium of 1-butanol + water + methanol at 298.15 K solubility and behaviour of poly(propylene glycol) - Ammonia and butanol solvents in binary mixtures and their coefficients at increases in temperature and composition; Equilibria of Binary Mixtures Containing 1-Butanol and Atheromycin at 313.15 K on solubility and liquid-liquid phase behaviour for 2,2,2-trifluoroethanol + cyclohexane + 1-butanol at three temperatures and pressure 101.3 kPa;

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Tetrafluoroborate Using Gas Liquid
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Solubility Measurement and Thermodynamic Model Correlation and Activity Coefficients at Infinite Dilution of Alkanols in the Ionic Liquids 1-Butyl-3-methylimidazolium Hexafluorophosphate, Determination and Correlation of Solubilities of (S)-Indoline-2-carboxylic Acid in Organic Properties of Binary Liquid Mixtures of 1-methylpiperidinium Hexafluorophosphate Excess Enthalpy and Excess Volume of Binary Mixtures Containing an Alcohol Physicochemical Characterization, and Solubility Data of 1-methylpiperidinium Binary Systems (n-propanol + 1-methoxyethoxy) butane and 1-Butanol + 1-Methoxyethoxy)- Liquid-Liquid Equilibria and 1-Butanol + Water Binary Phase Behavior of Solutions of Density, Refractive Index, and Sound Velocity for the Binary Mixtures of 1-methylpiperidinium Hexafluorophosphate and Water between 303.15 K and 323.15 K for organic solutes and water in the ionic liquid 1-(2-methoxyethyl)-1-methylpiperidinium trifluoromethylphosphate:

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Legend

af:	Acentric Factor
affp:	Proton affinity
aigt:	Autoignition Temperature
basg:	Gas basicity
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
econd:	Electrical conductivity
fl:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpc:	Flash Point (Closed Cup Method)
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hvap:	Enthalpy of vaporization at standard conditions

hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
kvisc:	Kinematic viscosity
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhog:	Gas Density
rhof:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sg:	Molar entropy at standard conditions
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tbp:	Boiling point at given pressure
tc:	Critical Temperature
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility
zra:	Rackett Parameter

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