Butanoic acid, ethyl ester

Other names:	BUTYRIC ESTER
	Butyric acid, ethyl ester
	ETHYL BUTANOATE
	ETHYL BUTYRATE
	ETHYL N-BUTYRATE
	Ethyl ester of butanoic acid
	Ethyl n-butanoate
	NSC 8857
	UN 1180
	ethyl 1-butyrate
	ethyl butanoate (ethyl butyrate)
	n-Butyric acid ethyl ester
Inchi:	InChI=1S/C6H12O2/c1-3-5-6(7)8-4-2/h3-5H2,1-2H3
InchiKey:	OBNCKNCVKJNDBV-UHFFFAOYSA-N
Formula:	C6H12O2
SMILES:	CCCC(=O)OCC
Mol. weight [g/mol]:	116.16
CAS:	105-54-4

Physical Properties

Property code	Value	Unit	Source
af	0.4610		KDB
chl	-3539.00	kJ/mol	NIST Webbook
chl	-3545.00	kJ/mol	NIST Webbook
dm	1.80	debye	KDB
gf	-234.28	kJ/mol	Joback Method
hf	-485.00 ± 1.00	kJ/mol	NIST Webbook
hfl	-528.40 ± 0.79	kJ/mol	NIST Webbook
hfus	14.08	kJ/mol	Joback Method
hvap	36.90 ± 0.04	kJ/mol	NIST Webbook
hvap	44.00 ± 1.00	kJ/mol	NIST Webbook
hvap	43.40	kJ/mol	NIST Webbook
hvap	42.71	kJ/mol	NIST Webbook
hvap	42.68 ± 0.10	kJ/mol	NIST Webbook
hvap	42.00 ± 0.10	kJ/mol	NIST Webbook
hvap	42.00 ± 0.10	kJ/mol	NIST Webbook
hvap	43.70 ± 1.30	kJ/mol	NIST Webbook

log10ws	-1.28		Aqueous Solubility Prediction Method
logp	1.350		Crippen Method
mcvol	102.840	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
pc	3064.00 ± 151.99	kPa	NIST Webbook
pc	3060.00	kPa	KDB
rhoc	276.46 ± 9.99	kg/m3	NIST Webbook
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tb	392.15 ± 1.00	K	NIST Webbook
tb	388.65 ± 5.00	K	NIST Webbook
tb	393.15 ± 1.00	K	NIST Webbook
tb	394.55 ± 1.00	K	NIST Webbook
tb	393.15 ± 1.00	K	NIST Webbook
tb	393.00 ± 1.00	K	NIST Webbook
tb	394.70 ± 0.50	K	NIST Webbook
tb	394.15 ± 1.00	K	NIST Webbook
tb	394.50 ± 2.00	K	NIST Webbook
tb	391.90 ± 1.00	K	NIST Webbook
tb	394.70 ± 0.50	K	NIST Webbook
tb	394.35 ± 0.40	K	NIST Webbook
tb	393.40 ± 0.50	K	NIST Webbook
tb	393.30 ± 0.50	K	NIST Webbook
tb	393.20 ± 0.50	K	NIST Webbook
tb	393.35 ± 0.50	K	NIST Webbook
tb	393.45 ± 1.00	K	NIST Webbook
tb	391.65 ± 1.00	K	NIST Webbook
tb	392.15 ± 2.00	K	NIST Webbook
tb	394.90 ± 0.30	K	NIST Webbook
tb	393.15 ± 1.00	K	NIST Webbook

tb	393.40 ± 1.00	K	NIST Webbook
tb	394.65 ± 1.00	K	NIST Webbook
tb	392.15 ± 1.00	K	NIST Webbook
tb	393.10 ± 1.00	K	NIST Webbook
tb	393.15 ± 1.00	K	NIST Webbook
tc	577.50 ± 6.00	K	NIST Webbook
tc	568.80 ± 0.60	K	NIST Webbook
tc	569.98	K	Development of a Predictive Equation of State for CO2 + Ethyl Ester Mixtures Based on Critical Points Measurements
tc	566.00	K	KDB
tc	566.00 ± 2.00	K	NIST Webbook
tc	558.70 ± 10.00	K	NIST Webbook
tf	170.65 ± 0.70	K	NIST Webbook
tf	175.00	K	KDB
tf	175.30 ± 0.30	K	NIST Webbook
tf	178.90	K	Aqueous Solubility Prediction Method
vc	0.421	m3/kmol	KDB
zc	0.2737480		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	219.25	J/mol×K	472.16	Joback Method
cpg	228.47	J/mol×K	501.76	Joback Method
cpg	237.38	J/mol×K	531.36	Joback Method
cpg	245.98	J/mol×K	560.96	Joback Method
cpg	254.27	J/mol×K	590.55	Joback Method
cpg	199.87	J/mol×K	412.97	Joback Method
cpg	209.71	J/mol×K	442.57	Joback Method
cpl	220.10	J/mol×K	297.20	NIST Webbook
cpl	228.00	J/mol×K	298.15	NIST Webbook
cpl	229.70	J/mol×K	290.00	NIST Webbook
cpl	220.10	J/mol×K	297.20	NIST Webbook
dvisc	0.0004200	Pa×s	333.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters

dvisc	0.0006200	Pa×s	298.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0005830	Pa×s	303.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0006620	Pa×s	293.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0005190	Pa×s	313.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003820	Pa×s	343.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004910	Pa×s	318.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004650	Pa×s	323.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004420	Pa×s	328.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0005490	Pa×s	308.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004000	Pa×s	338.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
hvapt	41.80	kJ/mol	324.00	NIST Webbook

hvapt	39.40	kJ/mol	382.50	NIST Webbook
hvapt	40.20	kJ/mol	362.50	NIST Webbook
hvapt	42.10 ± 0.10	kJ/mol	323.00	NIST Webbook
hvapt	48.30	kJ/mol	333.50	NIST Webbook
hvapt	35.47	kJ/mol	394.60	NIST Webbook
pvap	57.52	kPa	375.67	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	65.03	kPa	379.48	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	67.53	kPa	380.68	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	70.00	kPa	381.82	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	72.52	kPa	382.96	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	75.01	kPa	384.07	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	77.51	kPa	385.13	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	79.99	kPa	386.19	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	60.00	kPa	376.95	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane

pvap	85.02	kPa	388.21	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	87.54	kPa	389.17	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	89.98	kPa	390.12	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	92.53	kPa	391.06	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	94.92	kPa	391.95	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	97.45	kPa	392.83	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	100.01	kPa	393.71	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	101.31	kPa	394.13	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	82.52	kPa	387.22	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	55.03	kPa	374.31	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane

pvap	52.51	kPa	372.86	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	50.01	kPa	371.44	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	47.51	kPa	369.87	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	45.03	kPa	368.24	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	42.51	kPa	366.66	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	40.04	kPa	364.86	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	37.52	kPa	363.04	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	35.02	kPa	361.08	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	32.51	kPa	359.00	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	30.03	kPa	356.76	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane

pvap	27.50	kPa	354.39	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	25.00	kPa	351.83	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	22.50	kPa	348.97	Solvent Effects on Vapor Liquid Equilibria of the Binary System 1-Hexene + n-Hexane
pvap	60.00	kPa	377.21	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	60.00	kPa	377.23	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	35.41	kPa	361.56	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	50.00	kPa	371.33	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	54.40	kPa	373.83	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	58.98	kPa	376.28	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	65.75	kPa	379.65	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane

pvap	77.20	kPa	384.82	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	84.14	kPa	387.65	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	90.84	kPa	390.23	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	100.40	kPa	393.63	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	40.41	kPa	365.24	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	101.30	kPa	393.78	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
rfi	1.38980		298.15	Measurements and Correlations of the Isobaric Vapor Liquid Equilibria of Binary Mixtures and Excess Properties for Mixtures Containing an Alkyl (Methyl, Ethyl) Butanoate with an Alkane (Heptane, Nonane) at 101.3 kPa
rfi	1.38990		293.15	Vapor liquid equilibria of carbon dioxide with isopropyl acetate, diethyl carbonate and ethyl butyrate at elevated pressures

rfi	1.38950		298.15	Thermodynamic study of (alkyl esters + a,x-alkyl dihalides) I: HE and V E for 25 binary mixtures {xCu-1H2u-1CO2C2H5 + (1-x)a,x-ClCH2(CH2)v-2CH2Cl}, where u = 1 to 5, a = 1 and v = x = 2 to 6	
rhol	847.00	kg/m3	323.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols	
rhol	879.00	kg/m3	293.00	KDB	
rhol	879.18	kg/m3	293.20	Modeling extraction equilibria of butyric acid distributed between water and tri-n-butyl amine/diluent or tri-n-butyl phosphate/diluent system: Extension of the LSER approach	
rhol	874.31	kg/m3	298.15	Acoustic and volumetric study of renewable oxygenated fuel additives at (298.15-323.15) K: Isomeric butanediols with ethylbutyrate	
rhol	868.85	kg/m3	303.15	Acoustic and volumetric study of renewable oxygenated fuel additives at (298.15-323.15) K: Isomeric butanediols with ethylbutyrate	
rhol	863.40	kg/m3	308.15	Acoustic and volumetric study of renewable oxygenated fuel additives at (298.15-323.15) K: Isomeric butanediols with ethylbutyrate	

rhol	857.94	kg/m3	313.15	Acoustic and volumetric study of renewable oxygenated fuel additives at (298.15-323.15) K: Isomeric butanediols with ethylbutyrate
rhol	852.49	kg/m3	318.15	Acoustic and volumetric study of renewable oxygenated fuel additives at (298.15-323.15) K: Isomeric butanediols with ethylbutyrate
rhol	847.03	kg/m3	323.15	Acoustic and volumetric study of renewable oxygenated fuel additives at (298.15-323.15) K: Isomeric butanediols with ethylbutyrate
rhol	884.16	kg/m3	288.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rhol	878.90	kg/m3	293.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rhol	873.62	kg/m3	298.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rhol	868.33	kg/m3	303.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rhol	863.02	kg/m3	308.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rhol	857.70	kg/m3	313.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols

rhol	852.36	kg/m3	318.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols
rhol	868.21	kg/m3	303.15	Densities, Viscosities, and Surface and Interfacial Tensions of the Ternary Mixture Water + Ethyl Butyrate + Methanol at 303.15 K.
tcondl	0.15	W/m×K	268.57	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	273.61	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	278.63	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	283.58	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	288.65	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	293.58	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	298.53	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase

tcondl	0.13	W/m×K	303.56	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.12	W/m×K	363.52	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.12	W/m×K	358.57	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.12	W/m×K	353.36	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.12	W/m×K	348.54	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.12	W/m×K	343.51	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.12	W/m×K	338.50	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.12	W/m×K	333.46	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	328.48	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	323.42	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase

tcondl	0.13	W/m×K	318.61	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	313.49	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	308.67	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase

Correlations

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)
Coeff. A	1.49602e+01
Coeff. B	-3.54866e+03
Coeff. C	-5.08630e+01
Temperature range (K), min.	292.72
Temperature range (K), max.	418.65

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/T + C*ln(T) + D*T^2
Coeff. A	6.66105e+01
Coeff. B	-6.89506e+03
Coeff. C	-7.55898e+00
Coeff. D	4.55093e-06
Temperature range (K), min.	175.15
Temperature range (K), max.	571.00

Datasets

Mass density, kg/m3

Pressure, kPa - Liquid	Temperature, K - Liquid	Mass density, kg/m3 - Liquid
100.00	298.15	873.3
100.00	303.15	868.1
100.00	308.15	862.6
100.00	313.15	857.3
100.00	318.15	851.9
100.00	323.15	846.7
100.00	328.15	841.4
100.00	333.15	835.8
100.00	338.15	830.3
100.00	343.15	824.8
100.00	348.15	819.1
100.00	353.15	813.5
100.00	363.15	799.9
100.00	373.15	788.5
100.00	383.15	776.9
100.00	393.15	765.1
1000.00	298.15	874.1
1000.00	303.15	868.9
1000.00	308.15	863.5
1000.00	313.15	858.2
1000.00	318.15	852.8
1000.00	323.15	847.4
1000.00	328.15	842.0
1000.00	333.15	837.0
1000.00	338.15	831.5
1000.00	343.15	825.9
1000.00	348.15	820.3
1000.00	353.15	814.7
1000.00	363.15	801.4
1000.00	373.15	790.1
1000.00	383.15	778.6
1000.00	393.15	766.9
2000.00	298.15	875.0
2000.00	303.15	869.8
2000.00	308.15	864.4
2000.00	313.15	859.1
2000.00	318.15	853.8
2000.00	323.15	848.4
2000.00	328.15	843.3

2000.00	333.15	838.1
2000.00	338.15	832.6
2000.00	343.15	827.1
2000.00	348.15	821.6
2000.00	353.15	816.1
2000.00	363.15	803.0
2000.00	373.15	791.7
2000.00	383.15	780.4
2000.00	393.15	768.8
3000.00	298.15	875.9
3000.00	303.15	870.7
3000.00	308.15	865.3
3000.00	313.15	860.1
3000.00	318.15	854.8
3000.00	323.15	849.5
3000.00	328.15	844.5
3000.00	333.15	839.2
3000.00	338.15	833.8
3000.00	343.15	828.3
3000.00	348.15	822.9
3000.00	353.15	817.4
3000.00	363.15	804.5
3000.00	373.15	793.4
3000.00	383.15	782.2
3000.00	393.15	770.8
3100.00	298.15	876.0
3100.00	303.15	870.7
3100.00	308.15	865.4
3100.00	313.15	860.2
3100.00	318.15	854.9
3100.00	323.15	849.6
3100.00	328.15	844.6
3100.00	333.15	839.3
3100.00	338.15	833.9
3100.00	343.15	828.4
3100.00	348.15	823.0
3100.00	353.15	817.5
3100.00	363.15	804.7
3100.00	373.15	793.6
3100.00	383.15	782.4
3100.00	393.15	771.0
5000.00	298.15	877.5
5000.00	303.15	872.4
5000.00	308.15	867.1

5000.00	313.15	861.9
5000.00	318.15	856.7
5000.00	323.15	851.7
5000.00	328.15	846.6
5000.00	333.15	841.2
5000.00	338.15	835.9
5000.00	343.15	830.7
5000.00	348.15	825.1
5000.00	353.15	819.8
5000.00	363.15	807.9
5000.00	373.15	796.8
5000.00	383.15	785.5
5000.00	393.15	774.5
10000.00	298.15	881.5
10000.00	303.15	876.5
10000.00	308.15	871.4
10000.00	313.15	866.3
10000.00	318.15	861.3
10000.00	323.15	856.7
10000.00	328.15	851.5
10000.00	333.15	846.3
10000.00	338.15	841.2
10000.00	343.15	836.2
10000.00	348.15	830.9
10000.00	353.15	825.7
10000.00	363.15	814.4
10000.00	373.15	804.0
10000.00	383.15	793.5
10000.00	393.15	783.1
15000.00	298.15	885.3
15000.00	303.15	880.4
15000.00	308.15	875.5
15000.00	313.15	870.5
15000.00	318.15	865.8
15000.00	323.15	861.1
15000.00	328.15	856.2
15000.00	333.15	851.1
15000.00	338.15	846.2
15000.00	343.15	841.4
15000.00	348.15	836.2
15000.00	353.15	831.2
15000.00	363.15	820.7
15000.00	373.15	810.8
15000.00	383.15	800.8

15000.00	393.15	790.9
20000.00	298.15	889.0
20000.00	303.15	884.1
20000.00	308.15	879.4
20000.00	313.15	874.5
20000.00	318.15	869.9
20000.00	323.15	865.4
20000.00	328.15	860.5
20000.00	333.15	855.6
20000.00	338.15	850.8
20000.00	343.15	846.1
20000.00	348.15	841.1
20000.00	353.15	836.3
20000.00	363.15	826.7
20000.00	373.15	817.2
20000.00	383.15	807.5
20000.00	393.15	798.0
25000.00	298.15	892.5
25000.00	303.15	887.8
25000.00	308.15	883.1
25000.00	313.15	878.4
25000.00	318.15	874.1
25000.00	323.15	869.4
25000.00	328.15	864.8
25000.00	333.15	860.1
25000.00	338.15	855.5
25000.00	343.15	850.1
25000.00	348.15	846.0
25000.00	353.15	841.4
25000.00	363.15	832.4
25000.00	373.15	823.1
25000.00	383.15	813.8
25000.00	393.15	804.6
30000.00	298.15	896.9
30000.00	303.15	892.3
30000.00	308.15	887.8
30000.00	313.15	883.2
30000.00	318.15	879.0
30000.00	323.15	874.5
30000.00	328.15	870.0
30000.00	333.15	865.4
30000.00	338.15	861.0
30000.00	343.15	855.7
30000.00	348.15	851.8

30000.00	353.15	847.4
30000.00	363.15	837.7
30000.00	373.15	828.7
30000.00	383.15	819.6
30000.00	393.15	810.7
35000.00	298.15	901.4
35000.00	303.15	896.9
35000.00	308.15	892.5
35000.00	313.15	888.1
35000.00	318.15	884.1
35000.00	323.15	879.7
35000.00	328.15	875.3
35000.00	333.15	870.8
35000.00	338.15	866.5
35000.00	343.15	861.8
35000.00	348.15	857.7
35000.00	353.15	853.4
35000.00	363.15	842.7
35000.00	373.15	834.0
35000.00	383.15	825.2
35000.00	393.15	816.6

Reference *https://www.doi.org/10.1021/je800251v*

Sources

Development of a Predictive Equation of State for CO2 + Ethyl Ester Mixtures Based on Critical Points Measurements: https://www.doi.org/10.1021/je5002494

Density, Viscosity, and Refractive Index Data for a Ternary System of Wine Congeners (Ethyl Butyrate + Diethyl Succinate + Isobutanol) in the Temperature Range from (288.15 to 323.15) K at Atmospheric Pressure: https://www.doi.org/10.1021/acs.jced.6b00640

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Legend

af:	Acentric Factor
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
gf:	Standard Gibbs free energy of formation
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
tb:	Normal Boiling Point Temperature
tc:	Critical Temperature

tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
vc:	Critical Volume
zc:	Critical Compressibility