

Thiophene, 2-ethyl-

Other names:	2-Ethylthiophene 2-Ethylthiophenol
Inchi:	InChI=1S/C6H8S/c1-2-6-4-3-5-7-6/h3-5H,2H2,1H3
InchiKey:	JCCCMAAJYSNBPR-UHFFFAOYSA-N
Formula:	C6H8S
SMILES:	CCc1cccs1
Mol. weight [g/mol]:	112.19
CAS:	872-55-9

Physical Properties

Property code	Value	Unit	Source
hvap	39.70 ± 0.90	kJ/mol	NIST Webbook
ie	8.67 ± 0.05	eV	NIST Webbook
ie	8.80 ± 0.20	eV	NIST Webbook
ie	8.57	eV	NIST Webbook
log10ws	-2.59		Aqueous Solubility Prediction Method
logp	2.310		Crippen Method
mcvol	92.290	ml/mol	McGowan Method
rinpol	872.00		NIST Webbook
rinpol	850.00		NIST Webbook
rinpol	850.00		NIST Webbook
rinpol	845.00		NIST Webbook
rinpol	905.00		NIST Webbook
rinpol	871.00		NIST Webbook
rinpol	846.00		NIST Webbook
rinpol	847.00		NIST Webbook
rinpol	871.00		NIST Webbook
rinpol	880.00		NIST Webbook
rinpol	870.00		NIST Webbook
rinpol	870.00		NIST Webbook
rinpol	872.00		NIST Webbook
rinpol	905.00		NIST Webbook
rinpol	868.00		NIST Webbook
rinpol	871.00		NIST Webbook
rinpol	861.00		NIST Webbook
rinpol	844.00		NIST Webbook

ripol	844.00		NIST Webbook
ripol	869.00		NIST Webbook
ripol	874.00		NIST Webbook
ripol	837.00		NIST Webbook
ripol	850.00		NIST Webbook
ripol	847.00		NIST Webbook
ripol	874.00		NIST Webbook
ripol	845.00		NIST Webbook
ripol	846.00		NIST Webbook
ripol	845.00		NIST Webbook
ripol	846.00		NIST Webbook
ripol	868.00		NIST Webbook
ripol	871.00		NIST Webbook
ripol	861.00		NIST Webbook
ripol	851.00		NIST Webbook
ripol	845.00		NIST Webbook
ripol	1179.00		NIST Webbook
ripol	1177.00		NIST Webbook
ripol	1167.00		NIST Webbook
ripol	1161.00		NIST Webbook
ripol	1162.00		NIST Webbook
ripol	1179.00		NIST Webbook
ripol	1170.00		NIST Webbook
ripol	1170.00		NIST Webbook
ripol	1191.00		NIST Webbook
ripol	1185.00		NIST Webbook
ripol	1183.00		NIST Webbook
ripol	1162.00		NIST Webbook
ripol	1173.00		NIST Webbook
ripol	1180.00		NIST Webbook
ripol	1182.00		NIST Webbook
ripol	1172.00		NIST Webbook
ripol	1182.00		NIST Webbook
ripol	1177.00		NIST Webbook
ripol	1180.00		NIST Webbook
tb	407.15	K	Isobaric vapor-liquid equilibrium for binary system of 2-ethylthiophene + n-octane at 101.33 kPa
tb	407.14	K	Phase equilibria of three binary systems containing 2,5-dimethylthiophene and 2-ethylthiophene in hydrocarbons
tb	407.20	K	NIST Webbook
tb	406.15 ± 2.00	K	NIST Webbook
tb	407.00 ± 4.00	K	NIST Webbook

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
hvapt	39.70	kJ/mol	353.50	NIST Webbook
pvap	101.33	kPa	407.15	Isobaric vapor-liquid equilibrium for binary system of 2-ethylthiophene + n-octane at 101.33 kPa
pvap	101.33	kPa	407.14	Phase equilibria of three binary systems containing 2,5-dimethylthiophene and 2-ethylthiophene in hydrocarbons
pvap	33.26	kPa	373.10	Phase Equilibria on Four Binary Systems: 1,2-Dichloroethane + trans-1,2-Dichloroethylene, 1-Octene + 2-Methyl Thiophene, 2-Ethyl Thiophene + 2,2,4-Trimethylpentane, and Cyclopropanecarbonitrile + Water
pvap	111.40	kPa	413.15	Phase Equilibria on Four Binary Systems: 1,2-Dichloroethane + trans-1,2-Dichloroethylene, 1-Octene + 2-Methyl Thiophene, 2-Ethyl Thiophene + 2,2,4-Trimethylpentane, and Cyclopropanecarbonitrile + Water

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.42303e+01
Coeff. B	-3.34101e+03
Coeff. C	-5.96100e+01
Temperature range (K), min.	299.23
Temperature range (K), max.	434.21

Datasets

Mass density, kg/m³

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m ³ - Liquid
283.15	100.00	1003.44
288.15	100.00	998.47
293.15	100.00	993.45
298.15	100.00	988.39
303.15	100.00	983.42
308.15	100.00	978.38
313.15	100.00	973.34
318.15	100.00	968.32
323.15	100.00	963.21
328.15	100.00	958.12
333.15	100.00	952.99
338.15	100.00	947.86
283.15	2000.00	1004.84
288.15	2000.00	999.91
293.15	2000.00	994.92
298.15	2000.00	989.91
303.15	2000.00	984.97
308.15	2000.00	979.99
313.15	2000.00	975.0
318.15	2000.00	970.02

323.15	2000.00	964.97
328.15	2000.00	959.94
333.15	2000.00	954.85
338.15	2000.00	949.78
283.15	5000.00	1007.0
288.15	5000.00	1002.13
293.15	5000.00	997.2
298.15	5000.00	992.26
303.15	5000.00	987.39
308.15	5000.00	982.48
313.15	5000.00	977.54
318.15	5000.00	972.64
323.15	5000.00	967.69
328.15	5000.00	962.71
333.15	5000.00	957.72
338.15	5000.00	952.72
283.15	7000.00	1008.42
288.15	7000.00	1003.59
293.15	7000.00	998.7
298.15	7000.00	993.8
303.15	7000.00	988.98
308.15	7000.00	984.11
313.15	7000.00	979.22
318.15	7000.00	974.36
323.15	7000.00	969.44
328.15	7000.00	964.53
333.15	7000.00	959.58
338.15	7000.00	954.65
283.15	10000.00	1010.51
288.15	10000.00	1005.73
293.15	10000.00	1000.9
298.15	10000.00	996.05
303.15	10000.00	991.3
308.15	10000.00	986.49
313.15	10000.00	981.68
318.15	10000.00	976.86
323.15	10000.00	972.03
328.15	10000.00	967.18
333.15	10000.00	962.31
338.15	10000.00	957.46
283.15	15000.00	1013.9
288.15	15000.00	1009.2
293.15	15000.00	1004.46
298.15	15000.00	999.7

303.15	15000.00	995.04
308.15	15000.00	990.33
313.15	15000.00	985.61
318.15	15000.00	980.93
323.15	15000.00	976.2
328.15	15000.00	971.45
333.15	15000.00	966.72
338.15	15000.00	961.97
283.15	20000.00	1017.18
288.15	20000.00	1012.57
293.15	20000.00	1007.92
298.15	20000.00	1003.24
303.15	20000.00	998.67
308.15	20000.00	994.05
313.15	20000.00	989.42
318.15	20000.00	984.83
323.15	20000.00	980.22
328.15	20000.00	975.56
333.15	20000.00	970.93
338.15	20000.00	966.32
283.15	25000.00	1020.37
288.15	25000.00	1015.82
293.15	25000.00	1011.25
298.15	25000.00	1006.67
303.15	25000.00	1002.17
308.15	25000.00	997.63
313.15	25000.00	993.09
318.15	25000.00	988.58
323.15	25000.00	984.06
328.15	25000.00	979.5
333.15	25000.00	974.97
338.15	25000.00	970.44
283.15	30000.00	1023.45
288.15	30000.00	1018.97
293.15	30000.00	1014.49
298.15	30000.00	1009.97
303.15	30000.00	1005.54
308.15	30000.00	1001.09
313.15	30000.00	996.63
318.15	30000.00	992.22
323.15	30000.00	987.78
328.15	30000.00	983.31
333.15	30000.00	978.86
338.15	30000.00	974.41

283.15	35000.00	1026.45
288.15	35000.00	1022.04
293.15	35000.00	1017.62
298.15	35000.00	1013.18
303.15	35000.00	1008.81
308.15	35000.00	1004.45
313.15	35000.00	1000.06
318.15	35000.00	995.71
323.15	35000.00	991.35
328.15	35000.00	986.98
333.15	35000.00	982.61
338.15	35000.00	978.26
283.15	40000.00	1029.36
288.15	40000.00	1025.03
293.15	40000.00	1020.67
298.15	40000.00	1016.3
303.15	40000.00	1012.0
308.15	40000.00	1007.68
313.15	40000.00	1003.38
318.15	40000.00	999.11
323.15	40000.00	994.81
328.15	40000.00	990.51
333.15	40000.00	986.22
338.15	40000.00	981.96
283.15	45000.00	1032.2
288.15	45000.00	1027.9
293.15	45000.00	1023.61
298.15	45000.00	1019.31
303.15	45000.00	1015.07
308.15	45000.00	1010.84
313.15	45000.00	1006.6
318.15	45000.00	1002.39
323.15	45000.00	998.17
328.15	45000.00	993.94
333.15	45000.00	989.73
338.15	45000.00	985.53
283.15	50000.00	1034.96
288.15	50000.00	1030.72
293.15	50000.00	1026.49
298.15	50000.00	1022.24
303.15	50000.00	1018.07
308.15	50000.00	1013.88
313.15	50000.00	1009.71
318.15	50000.00	1005.57

323.15	50000.00	1001.41
328.15	50000.00	997.24
333.15	50000.00	993.09
338.15	50000.00	988.98
283.15	55000.00	1037.65
288.15	55000.00	1033.47
293.15	55000.00	1029.29
298.15	55000.00	1025.1
303.15	55000.00	1020.99
308.15	55000.00	1016.86
313.15	55000.00	1012.75
318.15	55000.00	1008.66
323.15	55000.00	1004.56
328.15	55000.00	1000.47
333.15	55000.00	996.39
338.15	55000.00	992.31
283.15	60000.00	1040.28
288.15	60000.00	1036.14
293.15	60000.00	1032.01
298.15	60000.00	1027.87
303.15	60000.00	1023.81
308.15	60000.00	1019.74
313.15	60000.00	1015.69
318.15	60000.00	1011.66
323.15	60000.00	1007.62
328.15	60000.00	1003.58
333.15	60000.00	999.56
338.15	60000.00	995.56
283.15	65000.00	1042.84
288.15	65000.00	1038.73
293.15	65000.00	1034.65
298.15	65000.00	1030.59
303.15	65000.00	1026.56
308.15	65000.00	1022.56
313.15	65000.00	1018.54
318.15	65000.00	1014.56
323.15	65000.00	1010.59
328.15	65000.00	1006.6
333.15	65000.00	1002.62
338.15	65000.00	998.71

Reference

<https://www.doi.org/10.1021/acs.jced.8b00153>

Sources

Phase equilibria of three binary systems containing 1,5-dimethylthiophene and 2-ethylthiophene in hydrocarbons: Crippen Method:

<https://www.doi.org/10.1016/j.fluid.2015.09.030>

<http://link.springer.com/article/10.1007/BF02311772>

<http://pubs.acs.org/doi/abs/10.1021/ci990307l>

Phase Equilibria on Four Binary Systems: 1,2-Dichloroethane + trans-1,2-Dichloroethylene, 1-Octene + 2-Methyl Thiophene, 2-Ethyl Thiophene + 2,2,4-Trimethylpentane, and

<https://www.doi.org/10.1021/je050473r>

Cyclopropanecarbonitrile + Water: Isobaric vapor-liquid equilibrium for binary system of 2-ethylthiophene + 2-ethylfuran

<http://webbook.nist.gov/cgi/cbook.cgi?ID=C872559&Units=SI>

Pressure: Comparative Study of the Thermophysical Properties of 2-Ethylthiophene and 2-Ethylfuran:

<http://onschallenge.wikispaces.com/file/view/AqueousDataset002.xlsx/351826032/AqueousDa>

<https://www.doi.org/10.1016/j.fluid.2014.07.010>

<https://www.sciencedirect.com/book/9780128029992/the-yaws-handbook-of-vapor-pressure>

<https://www.doi.org/10.1021/acs.jced.8b00153>

Legend

h _{vap} :	Enthalpy of vaporization at standard conditions
h _{vapt} :	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log ₁₀ ws:	Log ₁₀ of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
m _{cvol} :	McGowan's characteristic volume
p _{vap} :	Vapor pressure
ρ _{ol} :	Liquid Density
rin _{pol} :	Non-polar retention indices
rip _{ol} :	Polar retention indices
tb:	Normal Boiling Point Temperature

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