Acetic acid, butyl ester

Other names:	1-Acetoxybutane
	1-Butanol, acetate
	1-Butyl acetate
	Acetate de butyle
	Acetic acid butyl ester
	Acetic acid n-butyl ester
	BUTYL ACETATE
	BUTYL ETHANOATE
	Butile
	Butile(acetati di)
	Butyl ester of acetic acid
	Butyl ester, acetic acid
	Butylacetat
	Butylacetaten
	Butyle
	Butyle (acetate de)
	Butylester kyseliny octove
	CH3COO(CH2)3CH3
	N-BUTYL ACETATE
	NSC 9298
	UN 1123
	ethanoic acid, butyl ester
	n-Butyl ethanoate
Inchi:	InChI=1S/C6H12O2/c1-3-4-5-8-6(2)7/h3-5H2,1-2H3
InchiKey:	DKPFZGUDAPQIHT-UHFFFAOYSA-N
Formula:	C6H12O2
SMILES:	CCCCOC(C)=O
Mol. weight [g/mol]:	116.16
CAS:	123-86-4

Physical Properties

Property code	Value	Unit	Source
af	0.4170		KDB
aigt	677.59	K	KDB
chl	-3467.00	kJ/mol	NIST Webbook
chl	-3543.00	kJ/mol	NIST Webbook

dm	1.80	debye	KDB
dvisc	0.0006680	Pa×s	Excess Molar Volumes and Viscosity Deviations of Binary Liquid Mixtures of 1,3-Dioxolane and 1,4-Dioxane with Butyl Acetate, Butyric Acid, Butylamine, and 2-Butanone at 298.15 K
fll	1.70	% in Air	KDB
flu	7.60	% in Air	KDB
fpc	310.37	K	KDB
fpo	297.04	K	KDB
gf	-234.28	kJ/mol	Joback Method
gyrad	4.1700		KDB
hf	-566.00	kJ/mol	NIST Webbook
hf	-486.80	kJ/mol	KDB
hfl	-609.60	kJ/mol	NIST Webbook
hfus	14.08	kJ/mol	Joback Method
hvap	43.70 ± 0.20	kJ/mol	NIST Webbook
hvap	41.00 ± 0.50	kJ/mol	NIST Webbook
hvap	43.10	kJ/mol	NIST Webbook
hvap	42.70	kJ/mol	NIST Webbook
hvap	43.60 ± 0.50	kJ/mol	NIST Webbook
hvap	42.40	kJ/mol	NIST Webbook
hvap	37.50	kJ/mol	NIST Webbook
hvap	43.89	kJ/mol	NIST Webbook
hvap	43.60 ± 0.20	kJ/mol	NIST Webbook
hvap	43.60 ± 0.20	kJ/mol	NIST Webbook
ie	9.92 ± 0.05	eV	NIST Webbook
ie	10.01	eV	NIST Webbook
ie	9.56 ± 0.03	eV	NIST Webbook
ie	10.02 ± 0.05	eV	NIST Webbook
ie	10.17	eV	NIST Webbook
log10ws	-1.24		Aqueous Solubility Prediction Method
logp	1.350		Crippen Method
mcvol	102.840	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=1)		KDB
pc	3100.00 ± 101.32	kPa	NIST Webbook
pc	3140.00	kPa	KDB
pc	3090.00 ± 20.00	kPa	NIST Webbook
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tb	399.40 ± 0.50	K	NIST Webbook
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tb	399.20	K	KDB
tb	399.11	K	Vapor liquid equilibria for the binary mixtures of 2,3-butanediol with n-butanol, n-butyl acetate, and ethyl acetate at 101.3 kPa
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tb	399.65 ± 0.25	K	NIST Webbook
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tb	399.11	K	Liquid Liquid Equilibria of Water + 2,3-Butanediol + Butyl Acetate at T) 298.15 K, T) 308.15 K, and T) 318.15 K
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tf	195.00	K	KDB
tf	196.35 ± 0.30	K	NIST Webbook
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tt	196.03 ± 0.10	K	NIST Webbook
tt	196.12 ± 0.05	K	NIST Webbook
vc	0.400	m3/kmol	KDB
zc	0.2609000		KDB
zra	0.26		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	237.38	J/mol×K	531.36	Joback Method
cpg	245.98	J/mol×K	560.96	Joback Method
cpg	199.87	J/mol×K	412.97	Joback Method
cpg	209.71	J/mol×K	442.57	Joback Method
cpg	219.25	J/mol×K	472.16	Joback Method
cpg	228.47	J/mol×K	501.76	Joback Method
cpg	254.27	J/mol×K	590.55	Joback Method
cpl	242.30	J/mol×K	292.50	NIST Webbook
cpl	242.30	J/mol×K	292.50	NIST Webbook
cpl	228.11	J/mol×K	298.35	NIST Webbook
cpl	225.11	J/mol×K	298.15	NIST Webbook
cpl	228.40	J/mol×K	298.15	NIST Webbook
dvisc	0.0005300	Pa×s	318.15	Binary mixtures of ([C4mim][NTf2] + molecular organic solvents): Thermophysical, acoustic and transport properties at various compositions and temperatures
dvisc	0.0005000	Pa×s	323.15	Binary mixtures of ([C4mim][NTf2] + molecular organic solvents): Thermophysical, acoustic and transport properties at various compositions and temperatures

dvisc	0.0006740	Pa×s	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
dvisc	0.0005940	Pa×s	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
dvisc	0.0006280	Pa×s	303.15	Density and Viscosity for a Binary Mixture of cis-3-Hexenyl Formate, Butyl Acetate, trans-2-Hexenyl Acetate, and cis-3-Hexenyl Acetate with Ethanol at Several Temperatures
dvisc	0.0007320	Pa×s	293.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0005700	Pa×s	313.15	Binary mixtures of ([C4mim][NTf2] + molecular organic solvents): Thermophysical, acoustic and transport properties at various compositions and temperatures

dvisc	0.0005800	Pa×s	308.15	Binary mixtures of ([C4mim][NTf2] + molecular organic solvents): Thermophysical, acoustic and transport properties at various compositions and temperatures	
dvisc	0.0006400	Pa×s	303.15	Binary mixtures of ([C4mim][NTf2] + molecular organic solvents): Thermophysical, acoustic and transport properties at various compositions and temperatures	
dvisc	0.0005460	Pa×s	313.15	Density and Viscosity for a Binary Mixture of cis-3-Hexenyl Formate, Butyl Acetate, trans-2-Hexenyl Acetate, and cis-3-Hexenyl Acetate with Ethanol at Several Temperatures	
dvisc	0.0006860	Pa×s	298.15	Density and Viscosity of Binary Mixtures of n-Butyl Acetate with Ketones at (298.15, 303.15, 308.15, and 313.15) K	
dvisc	0.0006700	Pa×s	298.15	Binary mixtures of ([C4mim][NTf2] + molecular organic solvents): Thermophysical, acoustic and transport properties at various compositions and temperatures	

dvisc	0.0006250	Pa×s	303.15	Density and Viscosity of Binary Mixtures of n-Butyl Acetate with Ketones at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0005890	Pa×s	308.15	Density and Viscosity of Binary Mixtures of n-Butyl Acetate with Ketones at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0005450	Pa×s	313.15	Density and Viscosity of Binary Mixtures of n-Butyl Acetate with Ketones at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0006072	Pa×s	303.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K
dvisc	0.0006770	Pa×s	298.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0006280	Pa×s	303.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters

dvisc	0.0005687	Pa×s	308.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K
dvisc	0.0005850	Pa×s	308.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0005460	Pa×s	313.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0005120	Pa×s	318.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004810	Pa×s	323.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004530	Pa×s	328.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004280	Pa×s	333.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004050	Pa×s	338.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters

dvisc	0.0007320	Pa×s	293.15	Density and Viscosity for a Binary Mixture of cis-3-Hexenyl Formate, Butyl Acetate, trans-2-Hexenyl Acetate, and cis-3-Hexenyl Acetate with Ethanol at Several Temperatures
dvisc	0.0003840	Pa×s	343.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0005340	Pa×s	313.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K
hvapt	40.60 ± 0.10	kJ/mol	343.00	NIST Webbook
hvapt	37.50	kJ/mol	398.00	NIST Webbook
hvapt	39.40 ± 0.10	kJ/mol	358.00	NIST Webbook
hvapt	41.70 ± 0.10	kJ/mol	328.00	NIST Webbook
hvapt	43.00 ± 0.10	kJ/mol	313.00	NIST Webbook
hvapt	41.30	kJ/mol	365.00	NIST Webbook
hvapt	40.80	kJ/mol	365.50	NIST Webbook
hvapt	40.50	kJ/mol	370.00	NIST Webbook
hvapt	36.28	kJ/mol	399.20	NIST Webbook
pvap	67.70	kPa	385.64	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	275.00	kPa	437.80	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa

pvap	297.00	kPa	440.65	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	295.00	kPa	440.81	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	342.00	kPa	447.05	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	377.00	kPa	451.67	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	382.00	kPa	452.25	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	407.00	kPa	455.22	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	420.00	kPa	456.75	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa

pvap	457.00	kPa	460.69	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	480.00	kPa	463.25	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	492.00	kPa	464.05	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	542.00	kPa	469.05	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	592.00	kPa	473.70	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	615.00	kPa	475.55	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	637.00	kPa	477.25	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa

pvap	641.00	kPa	477.55	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	670.00	kPa	479.95	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	692.00	kPa	481.70	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	712.00	kPa	483.15	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	747.00	kPa	485.75	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	790.00	kPa	488.85	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	807.00	kPa	489.95	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa

pvap	842.00	kPa	492.48	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa	
pvap	885.00	kPa	495.15	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa	
pvap	915.00	kPa	496.95	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa	
pvap	947.00	kPa	498.95	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa	
pvap	970.00	kPa	500.35	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa	
pvap	990.00	kPa	501.65	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa	
pvap	997.00	kPa	501.95	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa	

pvap	998.00	kPa	502.15	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1005.00	kPa	502.45	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1012.00	kPa	502.85	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1050.00	kPa	505.05	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1092.00	kPa	507.35	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1107.00	kPa	508.25	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1135.00	kPa	509.73	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa

pvap	1187.00	kPa	512.35	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1225.00	kPa	514.25	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1267.00	kPa	516.35	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1307.00	kPa	518.35	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1357.00	kPa	520.65	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1395.00	kPa	522.45	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1447.00	kPa	524.75	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa

pvap	1472.00	kPa	525.85	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1501.00	kPa	527.15	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1537.00	kPa	528.65	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1577.00	kPa	530.35	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	1602.00	kPa	531.45	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	40.29	kPa	369.66	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	41.48	kPa	370.49	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	42.64	kPa	371.19	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	44.02	kPa	372.26	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	45.37	kPa	373.05	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	46.58	kPa	373.83	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	48.12	kPa	374.87	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	49.58	kPa	375.76	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	50.55	kPa	376.36	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	52.07	kPa	377.33	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	53.38	kPa	378.11	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	54.37	kPa	378.59	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	56.01	kPa	379.52	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	57.30	kPa	380.35	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	58.69	kPa	381.07	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	60.07	kPa	381.84	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	61.43	kPa	382.55	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	62.61	kPa	383.04	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	64.03	kPa	383.86	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	65.43	kPa	384.46	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	66.73	kPa	385.13	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	260.00	kPa	435.40	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	69.74	kPa	386.53	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	70.74	kPa	387.08	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	72.02	kPa	387.58	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	73.29	kPa	388.24	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	74.70	kPa	388.78	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	76.06	kPa	389.46	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	77.65	kPa	390.04	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	78.73	kPa	390.60	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	80.42	kPa	391.29	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	81.38	kPa	391.73	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	82.99	kPa	392.35	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	83.42	kPa	392.55	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	86.83	kPa	393.89	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	87.98	kPa	394.26	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	89.08	kPa	394.68	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	90.72	kPa	395.39	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	91.92	kPa	395.76	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	93.38	kPa	396.37	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	94.72	kPa	396.86	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	96.04	kPa	397.26	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	97.26	kPa	397.70	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	98.80	kPa	398.30	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	100.02	kPa	398.75	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	101.32	kPa	399.18	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	102.59	kPa	399.56	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	104.16	kPa	400.13	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	106.99	kPa	401.02	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	108.04	kPa	401.45	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	109.22	kPa	401.76	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	110.79	kPa	402.25	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	112.04	kPa	402.73	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	113.10	kPa	403.02	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	220.00	kPa	428.55	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	116.02	kPa	403.97	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	117.33	kPa	404.32	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	118.57	kPa	404.70	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	120.05	kPa	405.20	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	121.55	kPa	405.59	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	122.71	kPa	405.99	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	124.36	kPa	406.47	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	125.41	kPa	406.72	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	126.49	kPa	407.04	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	128.01	kPa	407.47	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	129.32	kPa	407.84	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	130.79	kPa	408.31	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	132.03	kPa	408.66	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	133.33	kPa	408.96	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	134.61	kPa	409.37	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	136.01	kPa	409.70	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	137.57	kPa	410.13	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	138.47	kPa	410.36	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	140.29	kPa	410.86	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	141.19	kPa	411.08	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	142.69	kPa	411.53	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	144.17	kPa	411.88	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	145.56	kPa	412.24	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	146.81	kPa	412.59	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	148.01	kPa	412.90	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	149.35	kPa	413.19	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	150.84	kPa	413.61	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	152.16	kPa	413.93	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	153.49	kPa	414.27	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	154.57	kPa	414.48	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	155.86	kPa	414.80	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol

pvap	157.54	kPa	415.25	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	158.72	kPa	415.49	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	159.80	kPa	415.75	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	161.46	kPa	416.19	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	162.90	kPa	416.51	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	164.01	kPa	416.74	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	29.77	kPa	361.65	Determination and Prediction of Vapor Liquid Equilibria for a System Containing Water + Butyl Acetate + Cyclohexane + Ethanol

pvap	58.85	kPa	381.35	Determination and Prediction of Vapor Liquid Equilibria for a System Containing Water + Butyl Acetate + Cyclohexane + Ethanol
pvap	87.65	kPa	394.25	Determination and Prediction of Vapor Liquid Equilibria for a System Containing Water + Butyl Acetate + Cyclohexane + Ethanol
pvap	44.71	kPa	373.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	195.63	kPa	423.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	42.55	kPa	373.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	188.81	kPa	423.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	191.33	kPa	423.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation

pvap	583.23	kPa	473.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation	
pvap	101.30	kPa	399.15	Phase Equilibrium (VLE, LLE, and VLLE) Data of the Ternary System: Ionic Liquid [OMIM][PF6] + Butan-1-ol + Butyl Acetate	
pvap	217.00	kPa	427.54	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa	
pvap	195.00	kPa	423.56	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa	
pvap	155.00	kPa	414.72	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa	
pvap	127.00	kPa	407.93	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa	
pvap	97.50	kPa	398.20	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa	

pvap	92.00	kPa	395.97	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	86.50	kPa	393.22	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	82.00	kPa	393.08	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	79.50	kPa	391.24	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	76.50	kPa	389.14	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	66.50	kPa	385.97	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	60.50	kPa	383.00	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa

pvap	56.50	kPa	379.96	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	56.00	kPa	379.26	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	51.50	kPa	376.35	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	45.50	kPa	372.26	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	41.50	kPa	369.76	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	34.00	kPa	363.70	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	30.00	kPa	362.02	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa

pvap	25.00	kPa	355.56	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	21.00	kPa	351.77	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	17.00	kPa	346.66	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	12.50	kPa	335.89	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	8.50	kPa	328.98	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	60.00	kPa	381.99	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	60.00	kPa	382.01	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	29.92	kPa	361.85	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane

pvap	32.95	kPa	364.47	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	41.42	kPa	370.90	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	45.02	kPa	373.32	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	56.43	kPa	380.10	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	60.15	kPa	382.08	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	72.71	kPa	388.06	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	80.09	kPa	391.20	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	88.69	kPa	394.58	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	99.03	kPa	398.35	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	101.30	kPa	399.09	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane

pvap	101.30	kPa	399.15	Isobaric VLE data for the system of butan-1-ol + butylethanoate + 1-butyl-3-methylimidazoliumbis[(trifluoromethyl)sulfonyl]imide
pvap	37.00	kPa	367.03	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
pvap	114.64	kPa	403.56	Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol
pvap	74.50	kPa	387.78	Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol. Binary Systems at 0.15 and 0.6 MPa
rfi	1.39510		293.15	Liquid-liquid equilibrium for the ternary system water + 2-methyl-1-propanol + butyl acetate and water + 2-methyl-2-propanol + butyl acetate at (298.15 and 323.15) K
rfi	1.39175		298.15	Vapor-Liquid Equilibrium Data for Binary Mixtures of Dimethyl Carbonate with Methyl Acetate, Ethyl Acetate, n-Propyl Acetate, Isopropyl Acetate, n-Butyl Acetate, and Isoamyl Acetate at 93.13 kPa
rfi	1.39160		298.15	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa

rfi	1.39191	298.15	Isobaric Vapor-Liquid Equilibria for the Binary Systems Benzene + Methyl Ethanoate, Benzene + Butyl Ethanoate, and Benzene + Methyl Heptanoate at 101.31kPa
rfi	1.39191	298.15	Densities, speeds of sound, and refractive indices of the ternary mixtures (toluene + methyl acetate + butyl acetate) and (toluene + methyl acetate + methyl heptanoate) at 298.15 K
rfi	1.39180	298.15	Molecular interactions in (2,4,6-trimethyl-1,3,5-trioxane + n-alkyl acetates) at T=(298.15, 303.15, and 308.15) K
rfi	1.38960	303.15	Densities, speeds of sound, isentropic compressibilities, refractive indexes, and viscosities of tetrahydrofuran with haloalkane or alkyl ethanoate at T = 303.15 K
rfi	1.39180	298.15	Thermodynamic study of (alkyl esters + a,x-alkyl dihalides)III. HE m and V E m for 20 binary mixtures {xCu-1H2u-1CO2C4H9 + (1 - x)a,x-ClCH2(CH2)v-2CH2Cl}, where u = 1 to 4, a = 1 and v = x = 2 to 6
rfi	1.39190	298.15	Properties of ionic liquid HMIMPF6 with carbonates, ketones and alkyl acetates

rfi	1.39400		293.15	Isobaric Vapor Liquid Equilibrium for Binary Systems of Thioglycolic Acid with Water, Butyl Acetate, Butyl Formate, and Isobutyl Acetate at 101.3 kPa	
rfi	1.38250		318.15	Thermodynamic properties of (an ester + an alkane). XVI. Experimental HEm and V Em values and a new correlation method for (an alkyl ethanoate + an n-alkane) at 318.15 K	
rfi	1.39080		308.15	Topological and thermodynamic investigations of molecular interactions in binary mixtures: Molar excess volumes and molar excess enthalpies	
rfi	1.39180		298.15	Densities, Excess Molar Volumes, Viscosities, and Refractive Indices of Binary Mixtures of n-Butyl Acetate with 1-Chloroalkanes (C4 C8) at 298.15 K	
rfi	1.39176		298.15	Effect of Temperature on the Change of Refractive Index on Mixing for Butyl Acetate + Aromatic Hydrocarbons	
rhol	860.49	kg/m3	313.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates	

rhol	865.70	kg/m3	308.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model	
rhol	860.50	kg/m3	313.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model	
rhol	855.30	kg/m3	318.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model	
rhol	870.90	kg/m3	303.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model	
rhol	881.54	kg/m3	293.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)	
rhol	876.40	kg/m3	298.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)	
rhol	871.24	kg/m3	303.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)	
rhol	866.05	kg/m3	308.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)	

rhol	860.84	kg/m3	313.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)	
rhol	850.10	kg/m3	323.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model	
rhol	876.38	kg/m3	298.15	Surface Tension and Surface Properties of Binary Mixtures of 1,4-Dioxane or N,N-Dimethyl Formamide with n-Alkyl Acetates	
rhol	859.86	kg/m3	313.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures	
rhol	876.00	kg/m3	298.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model	
rhol	881.10	kg/m3	293.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model	
rhol	873.10	kg/m3	298.15	Liquid Liquid Equilibria for the Ternary System n-Butyl Acetate + Pyrocatechol + Water at Different Temperatures at 101.3 kPa	

rhol	875.60	kg/m3	298.40	Vapor Liquid Equilibrium at 350 K, Excess Molar Enthalpies at 298 K, and Excess Molar Volumes at 298 K of Binary Mixtures Containing Ethyl Acetate, Butyl Acetate, and 2-Butanol	
rhol	871.28	kg/m3	303.15	Studies of viscosities of dilute solutions of alkylamine in non-electrolyte solvents. II. Haloalkanes and other polar solvents	
rhol	875.80	kg/m3	298.15	Measurement and correlation of solubility and solution thermodynamics of 1,3-dimethylurea in different solvents from T = (288.15 to 328.15) K	
rhol	850.03	kg/m3	323.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates	
rhol	855.27	kg/m3	318.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates	
rhol	865.68	kg/m3	308.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates	

rhol	865.08	kg/m3	308.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhol	870.27	kg/m3	303.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhol	875.45	kg/m3	298.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhol	880.61	kg/m3	293.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhol	870.86	kg/m3	303.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhol	875.80	kg/m3	298.20	Phase equilibria of (water + butyric acid + butyl acetate) ternary systems at different temperatures
rhol	871.07	kg/m3	303.15	Excess Volumes and Excess Isentropic Compressibilities of Binary Liquid Mixtures of Trichloroethylene with Esters at 303.15 K
rhol	898.00	kg/m3	273.00	KDB

rhol	849.75	kg/m3	323.15	Liquid-Liquid Equilibria, Density, Viscosity, and Surface and Interfacial Tension of the System Water + n-Butyl Acetate + 1-Propanol at 323.15 K and Atmospheric Pressure
rhol	876.00	kg/m3	298.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhol	881.13	kg/m3	293.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhol	876.38	kg/m3	298.15	Experimental and theoretical study of surface tension of binary mixtures of (n-alkyl acetates + heptane, benzene, and toluene)
rhol	881.38	kg/m3	293.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
rhol	876.26	kg/m3	298.20	Isothermal vapor-liquid equilibria, excess molar volume and the deviation of refractive indices for binary mixtures of 1-butanol, 1-hexanol, 3-methyl-1-butanol and butyl acetate

rhol	860.06	kg/m3	313.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
speedsl	1233.32	m/s	288.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K
speedsl	1150.00	m/s	308.15	Densities, Sound Speed, and IR Studies of (Methanol + 1-Acetoxybutane) and (Methanol + 1,1-Dimethylethyl Ester) at (298.15, 303.15, 308.15, and 313.15) K
speedsl	1173.00	m/s	303.15	Densities, Sound Speed, and IR Studies of (Methanol + 1-Acetoxybutane) and (Methanol + 1,1-Dimethylethyl Ester) at (298.15, 303.15, 308.15, and 313.15) K
speedsl	1151.35	m/s	308.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K

speedsl	1171.79	m/s	303.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K	
speedsl	1192.35	m/s	298.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K	
speedsl	1213.05	m/s	293.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K	
speedsl	1131.00	m/s	313.15	Densities, Sound Speed, and IR Studies of (Methanol + 1-Acetoxybutane) and (Methanol + 1,1-Dimethylethyl Ester) at (298.15, 303.15, 308.15, and 313.15) K	
speedsl	1190.00	m/s	298.15	Densities, Sound Speed, and IR Studies of (Methanol + 1-Acetoxybutane) and (Methanol + 1,1-Dimethylethyl Ester) at (298.15, 303.15, 308.15, and 313.15) K	

srf	0.02	N/m	298.15	Surface Tension Data of Aqueous Binary Mixtures of Methyl, Ethyl, Propyl, and Butyl Acetates at 298.15 K	
srf	0.02	N/m	313.15	Densities, surface tensions, and derived surface thermodynamics properties of (trimethylbenzene + propyl acetate, or butyl acetate) from T = 298.15 K to 313.15 K	
srf	0.02	N/m	308.15	Densities, surface tensions, and derived surface thermodynamics properties of (trimethylbenzene + propyl acetate, or butyl acetate) from T = 298.15 K to 313.15 K	
srf	0.02	N/m	303.15	Densities, surface tensions, and derived surface thermodynamics properties of (trimethylbenzene + propyl acetate, or butyl acetate) from T = 298.15 K to 313.15 K	
srf	0.02	N/m	298.15	Densities, surface tensions, and derived surface thermodynamics properties of (trimethylbenzene + propyl acetate, or butyl acetate) from T = 298.15 K to 313.15 K	

Correlations

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)

Coeff. A	1.46670e+01
Coeff. B	-3.49621e+03
Coeff. C	-5.10730e+01
Temperature range (K), min.	294.21
Temperature range (K), max.	424.78

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/T + C*ln(T) + D*T^2
Coeff. A	8.07098e+01
Coeff. B	-7.79009e+03
Coeff. C	-9.58507e+00
Coeff. D	5.19348e-06
Temperature range (K), min.	199.65
Temperature range (K), max.	579.15

Datasets

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
298.15	100.00	875.7
298.15	1000.00	876.3
298.15	2000.00	877.2
298.15	3000.00	878.0
298.15	3100.00	878.1
298.15	5000.00	879.9
298.15	10000.00	883.8
298.15	15000.00	887.6
298.15	20000.00	891.3
298.15	25000.00	894.9
298.15	30000.00	899.1
298.15	35000.00	903.7
303.15	100.00	870.4
303.15	1000.00	871.1
303.15	2000.00	872.0
303.15	3000.00	872.9
303.15	3100.00	873.0

303.15	5000.00	874.7
303.15	10000.00	878.8
303.15	15000.00	882.8
303.15	20000.00	886.5
303.15	25000.00	890.2
303.15	30000.00	894.4
303.15	35000.00	899.1
308.15	100.00	865.1
308.15	1000.00	865.9
308.15	2000.00	866.9
308.15	3000.00	867.8
308.15	3100.00	867.8
308.15	5000.00	869.6
308.15	10000.00	873.9
308.15	15000.00	878.0
308.15	20000.00	881.9
308.15	25000.00	885.6
308.15	30000.00	890.0
308.15	35000.00	894.8
313.15	100.00	859.9
313.15	1000.00	860.8
313.15	2000.00	861.7
313.15	3000.00	862.7
313.15	3100.00	862.7
313.15	5000.00	864.6
313.15	10000.00	869.0
313.15	15000.00	873.2
313.15	20000.00	877.2
313.15	25000.00	881.0
313.15	30000.00	885.6
313.15	35000.00	890.5
318.15	100.00	854.9
318.15	1000.00	855.7
318.15	2000.00	856.7
318.15	3000.00	857.8
318.15	3100.00	857.9
318.15	5000.00	859.6
318.15	10000.00	864.2
318.15	15000.00	868.5
318.15	20000.00	872.6
318.15	25000.00	876.5
318.15	30000.00	881.3
318.15	35000.00	886.3
323.15	100.00	849.7

323.15	1000.00	851.0
323.15	2000.00	852.0
323.15	3000.00	853.0
323.15	3100.00	853.1
323.15	5000.00	854.6
323.15	10000.00	859.4
323.15	15000.00	863.9
323.15	20000.00	868.1
323.15	25000.00	872.3
323.15	30000.00	877.3
323.15	35000.00	882.4
328.15	100.00	844.6
328.15	1000.00	845.7
328.15	2000.00	846.8
328.15	3000.00	847.9
328.15	3100.00	848.0
328.15	5000.00	849.7
328.15	10000.00	854.6
328.15	15000.00	859.3
328.15	20000.00	863.6
328.15	25000.00	867.8
328.15	30000.00	872.5
328.15	35000.00	877.7
333.15	100.00	839.6
333.15	1000.00	840.7
333.15	2000.00	841.8
333.15	3000.00	842.9
333.15	3100.00	842.9
333.15	5000.00	844.9
333.15	10000.00	850.0
333.15	15000.00	854.8
333.15	20000.00	859.3
333.15	25000.00	863.6
333.15	30000.00	868.6
333.15	35000.00	873.9
338.15	100.00	834.5
338.15	1000.00	835.6
338.15	2000.00	836.7
338.15	3000.00	837.9
338.15	3100.00	838.0
338.15	5000.00	840.1
338.15	10000.00	845.5
338.15	15000.00	850.1
338.15	20000.00	855.0

338.15	25000.00	859.5
338.15	30000.00	864.6
338.15	35000.00	870.1
343.15	100.00	829.5
343.15	1000.00	830.5
343.15	2000.00	831.7
343.15	3000.00	832.9
343.15	3100.00	833.0
343.15	5000.00	835.2
343.15	10000.00	840.7
343.15	15000.00	845.7
343.15	20000.00	850.5
343.15	25000.00	855.1
343.15	30000.00	860.7
343.15	35000.00	866.3
348.15	100.00	824.4
348.15	1000.00	825.4
348.15	2000.00	826.7
348.15	3000.00	827.9
348.15	3100.00	828.0
348.15	5000.00	830.5
348.15	10000.00	836.1
348.15	15000.00	841.3
348.15	20000.00	846.2
348.15	25000.00	850.9
348.15	30000.00	856.6
348.15	35000.00	862.4
353.15	100.00	819.3
353.15	1000.00	820.4
353.15	2000.00	821.7
353.15	3000.00	822.9
353.15	3100.00	823.0
353.15	5000.00	825.5
353.15	10000.00	831.3
353.15	15000.00	836.7
353.15	20000.00	841.8
353.15	25000.00	846.7
353.15	30000.00	852.5
353.15	35000.00	858.4
358.15	100.00	811.6
358.15	1000.00	813.2
358.15	2000.00	813.9
358.15	3100.00	815.3
358.15	5000.00	817.7

358.15	10000.00	823.6
358.15	15000.00	829.1
358.15	20000.00	835.5
363.15	100.00	806.1
363.15	1000.00	807.5
363.15	2000.00	808.8
363.15	3000.00	810.1
363.15	3100.00	810.3
363.15	5000.00	812.8
363.15	10000.00	819.2
363.15	15000.00	824.9
363.15	20000.00	830.4
368.15	100.00	800.3
368.15	1000.00	802.1
368.15	2000.00	803.6
368.15	3000.00	804.8
368.15	3100.00	805.0
368.15	5000.00	807.7
368.15	10000.00	814.3
368.15	15000.00	820.3
368.15	20000.00	825.9
373.15	100.00	795.8
373.15	1000.00	797.2
373.15	2000.00	798.7
373.15	3000.00	800.2
373.15	3100.00	800.4
373.15	5000.00	803.1
373.15	10000.00	809.9
373.15	15000.00	815.9
373.15	20000.00	821.3
378.15	100.00	790.4
378.15	1000.00	791.9
378.15	2000.00	793.7
378.15	3000.00	795.2
378.15	3100.00	795.4
378.15	5000.00	798.0
378.15	10000.00	804.7
378.15	15000.00	810.8
378.15	20000.00	817.1
383.15	100.00	785.2
383.15	1000.00	786.7
383.15	2000.00	788.3
383.15	3000.00	789.9
383.15	3100.00	790.0

383.15	5000.00	792.9
383.15	10000.00	800.1
383.15	15000.00	806.7
383.15	20000.00	812.8
388.15	100.00	779.9
388.15	1000.00	781.6
388.15	2000.00	783.2
388.15	3000.00	785.2
388.15	3100.00	785.4
388.15	5000.00	788.4
388.15	10000.00	795.8
388.15	15000.00	802.4
388.15	20000.00	808.6
393.15	100.00	775.2
393.15	1000.00	776.4
393.15	2000.00	778.1
393.15	3000.00	779.5
393.15	3100.00	779.7
393.15	5000.00	782.8
393.15	10000.00	790.6
393.15	15000.00	797.7
393.15	20000.00	804.2

Reference *https://www.doi.org/10.1021/je060339m*

Sources

Liquid phase equilibria of (water + phosphoric acid + 1-butanol or butyl acetate) ternary systems at T = 303.2 K:	https://www.doi.org/10.1016/j.jct.2008.07.001
Solubility of 1-H-Tetrazole-1-acetic Acid in Different Solvents between 283 K and 323 K:	https://www.doi.org/10.1021/je700200b
Aqueous Solubility Prediction Method:	http://onschallenge.wikispaces.com/file/view/AqueousDataset002.xlsx/351826032/AqueousDa
Densities, speeds of sound, and refractive indices of the ternary mixtures (toluene + methyl acetate + butyl acetate) and (toluene + methyl acetate + methyl heptanoate) at 298.15 K:	https://www.doi.org/10.1016/j.jct.2006.07.013
Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate [illegible] SAFT Model:	https://www.doi.org/10.1021/acs.jced.8b00524
Solution thermodynamics of simvastatin in pure solvents and binary solvent mixtures:	https://www.doi.org/10.1016/j.fluid.2015.07.055
Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa:	https://www.doi.org/10.1016/j.fluid.2018.02.003
Isobaric VLE data for the system of butan-1-ol + butylethanoate + 1-butyl-3-methylimidazolium bis[(trifluoromethyl)sulfonyl]imide:	https://www.doi.org/10.1016/j.fluid.2013.05.020
Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures:	https://www.doi.org/10.1021/je0340248
Vapor liquid equilibria for the binary mixtures of 2,3-butanediol with [illegible]	https://www.doi.org/10.1016/j.fluid.2007.09.001
Studies of viscosities of dilute solutions of alkylamine in non-electrolyte solvents. II. Haloalkanes and other polar solvents:	https://www.doi.org/10.1016/j.tca.2004.08.013
Solubility of Lovastatin in Acetone, Methanol, Ethanol, Ethyl Acetate, and Butyl Acetate between 283 K and 323 K:	https://www.doi.org/10.1021/je0500781
Thermodynamic study of (alkyl esters + alpha,beta-alkyl dihalides) VI.H and V for 20 binary mixtures {xCu-1H2u-1CO2(CH2)3CH3 + (1 - x)alpha,omega-BrCH2(CH2)v-2CH2Br}, where u = 1 to 5, alpha = 1, and v = omega = 2 to 6:	https://www.doi.org/10.1016/j.jct.2009.05.006
Quaternary liquid-liquid equilibrium, solubility and critical states: Acetic acid - n-butanol - n-butyl acetate - water at 318.15 K and atmospheric pressure:	https://www.doi.org/10.1016/j.fluid.2019.04.020

Solubility of Hydroquinone in Different Solvents from 276.65 K to 345.10 K:	https://www.doi.org/10.1021/je0502748
Solubility of Penicillin Sulfoxide in Different Solvents:	https://www.doi.org/10.1021/je900326e
Density and Viscosity of Binary Mixtures of n-Butyl Acetate with Ketones at (298.15, 303.15, 308.15, and 313.15) K:	https://www.doi.org/10.1021/je300085z
Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ionic liquid – hydroxyacetone – water mixtures:	https://www.doi.org/10.1016/j.fluid.2018.01.026
Solubility Measurement and Correlation of Probenecid in 12 Pure Organic Solvents and Thermodynamic Properties of Mixing of Solutions:	https://www.doi.org/10.1021/acs.jced.8b00863
Experimental and theoretical study of surface tension of binary mixtures of (n-alkyl acetates + heptane, benzene, and toluene):	https://www.doi.org/10.1016/j.jct.2008.10.009
Surface Tension Data of Aqueous Binary Mixtures of Methyl, Ethyl, Propyl, and Butyl Acetates at 298.15 K:	https://www.doi.org/10.1021/je900962v
Solubility and thermodynamic properties of vanillyl alcohol in some pure solvents:	https://www.doi.org/10.1016/j.jct.2016.11.030
Determination and Thermodynamic Analysis of the Solubility of Limonin in Eight Organic Solvents and Ethyl Acetate + 2-Propanol Binary Solvents from 283.2 to 323.2 K:	https://www.doi.org/10.1021/acs.jced.7b00851
Solution thermodynamics of valnemulin hydrogen fumarate in different pure solvents:	https://www.doi.org/10.1016/j.jct.2015.07.023
Solubility of Lovastatin in Ethyl Acetate, Propyl Acetate, Isopropyl Acetate, Butyl Acetate, sec-Butyl Acetate, Isobutyl Acetate, tert-Butyl Acetate, and 2-Butanone between (285 and 313) K:	https://www.doi.org/10.1021/je800120p
Solubility of Chlorpheniramine Maleate in Ethanol, 1-Propanol, 1-Butanol, Benzene, Ethyl Acetate, Ethyl Formate and Butyl Acetate between 283 K and 333 K:	https://www.doi.org/10.1021/je7001682
Thermodynamic equilibrium of 4-hydroxy-2,5-dimethyl-3(2H)-furanone in different solvent systems:	https://www.doi.org/10.1016/j.jct.2015.08.035
Solubilities of Phloretin in 12 Solvents at Different Temperatures:	https://www.doi.org/10.1021/je101168w
Liquid-Liquid Equilibria for Water + Benzonitrile + Ethyl Acetate or + Butyl Acetate:	https://www.doi.org/10.1021/je050051h
Joback Method:	https://en.wikipedia.org/wiki/Joback_method
Solubility of 3-Aminopyridine in Acetone + n-Butyl Acetate from (288.15 to 323.15) K:	https://www.doi.org/10.1021/je800945e
Binary mixtures of ([C4mim][NTf2] + molecular organic solvents): Thermophysical, acoustic and transport properties at various compositions and temperatures:	https://www.doi.org/10.1016/j.jct.2015.09.022
Solubility Modeling and Mixing Properties for Benzoin in Different Monosolvents and Solvent Mixtures at the Temperature Range from 273.15 to 313.15 K:	https://www.doi.org/10.1021/acs.jced.7b00743
Liquid–Liquid Equilibria for the Ternary System n-Butyl Acetate + Pyrocatechol + Water at Different Temperatures at 101.3 kPa:	https://www.doi.org/10.1021/acs.jced.6b00280
Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K:	https://www.doi.org/10.1021/je300789a
Solubility of Losartan Potassium in Different Pure Solvents from (293.15 to 343.15) K:	https://www.doi.org/10.1021/je7007236
Solubility and Caloric Properties of Cinnarizine:	https://www.doi.org/10.1021/acs.jced.5b00075
Solid-liquid phase equilibrium and mixing properties of 2-Cyano-4'-methylbiphenyl in pure solvents:	https://www.doi.org/10.1016/j.jct.2016.07.050
Liquid-Liquid Equilibria of Water + 2,3-Butanediol + Butyl Acetate at T) 298.15 K, T) 308.15 K, and T) 318.15 K:	https://www.doi.org/10.1021/je700705d
Isobaric (vapour + liquid) equilibria of binary systems containing butyl acetate for the separation of methoxy aromatic compounds (anisole and guaiacol) from biomass fast pyrolysis oil:	https://www.doi.org/10.1016/j.jct.2015.04.003
Molecular interactions in (2,4,6-trimethyl-1,3,5-trioxane + n-alkyl acetates) at T = (298.15, 303.15, and 308.15) K:	https://www.doi.org/10.1016/j.jct.2006.03.014
Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa:	https://www.doi.org/10.1021/je700411p
Liquid-liquid equilibrium and critical states for the system acetic acid + n-butanol + n-butyl acetate + water at 308.15 K:	https://www.doi.org/10.1016/j.fluid.2014.11.004
Excess Volumes and Excess Isentropic Compressibilities of Binary Liquid Mixtures of Trichloroethylene with Esters at 303.15 K:	https://www.doi.org/10.1007/s10765-015-1927-y
Phase Equilibrium (VLE, LLE, and VLLE) Data of the Ternary System: Ionic Liquid [OMIM][PF6] + Butan-1-ol + Butyl Acetate:	https://www.doi.org/10.1021/je5000296
Ternary Liquid–Liquid Equilibrium of Azeotropes (Ester + Alcohol) with Different Ionic Liquids at T = 298.15 K:	https://www.doi.org/10.1021/acs.jced.6b00811
Liquid–Liquid Equilibria of Water + Acetoin + Butyl Acetate at several temperatures:	https://www.doi.org/10.1021/je100861u
Properties of ionic liquid HMIMPF6 with carbonates, ketones and alkyl acetates:	https://www.doi.org/10.1016/j.jct.2005.07.020
Liquid-liquid equilibrium determination and thermodynamics modeling for extraction of isopropanol from its aqueous solution:	https://www.doi.org/10.1016/j.fluid.2017.11.010
Activity Coefficients at Infinite Dilution by GLC in Alkanediamines as Stationary Phases:	https://www.doi.org/10.1021/je200628n
Measurement and correlation of solubility and solution thermodynamics of 1,3-dimethylurea in different solvents from T = (288.15 to 328.15) K:	https://www.doi.org/10.1016/j.jct.2015.12.032
Surface Tension and Surface Properties of Binary Mixtures of 1,4-Dioxane or N,N-Dimethyl Formamide with n-Alkyl Acetates:	https://www.doi.org/10.1021/je9002114
Liquid–Liquid Equilibria, Density, Viscosity, and Surface and Interfacial Tension of the System Water + n-Butyl Acetate + 1-Propanol at 323.15 K and Atmospheric Pressure:	https://www.doi.org/10.1021/je900337a
Solubilities of Betulinic Acid in Thirteen Organic Solvents at Different Temperatures:	https://www.doi.org/10.1021/je200531k
Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates:	https://www.doi.org/10.1016/j.jct.2014.01.012
Liquid-liquid equilibrium for the ternary system water + 2-methyl-1-propanol + butyl acetate and water + 2-methyl-2-propanol + butyl acetate at (298.15 and 323.15) K:	https://www.doi.org/10.1016/j.fluid.2014.08.014
Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K:	https://www.doi.org/10.1021/je800653d

KDB Vapor Pressure Data:	https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=1079
Thermodynamic study of (alkyl esters + a,x-alkyl dihalides)III. HE m and V E m for 20 binary mixtures {xCu-1H2u-1CO2C4H9 + (1 - x)a,x-ClCH2(CH2)v-2CH2Cl}, where u = 1 to 4, a = 1, and v = 2 to 6:	https://www.doi.org/10.1016/j.jct.2005.11.003
Biomass-Derived Platform Chemicals: Thermodynamic Studies on the Conversion of 5-Hydroxymethylfurfural into Bulk Intermediates and Fuels:	https://www.doi.org/10.1021/je300529j
Vapor-Liquid Equilibrium at 350 K, Excess Molar Enthalpies at 298 K, and Excess Molar Volumes at 298 K of Binary Mixtures Containing Ethyl Acetate, Butyl Acetate, and 2-Butanol:	https://www.doi.org/10.1021/je400036b
Measurement and Correlation of Solubility of Amorphous Cefmetazole Sodium in Pure and Binary Solvent Mixtures:	https://www.doi.org/10.1021/acs.jced.6b00741
Activity Coefficients at Infinite Dilution for Hydrocarbons in Fatty Alcohols Determined by Gas-Liquid Chromatography:	https://www.doi.org/10.1021/je1005517
Vapor-Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation:	https://www.doi.org/10.1021/je400885z
Study of Ether-, Alcohol-, or Cyano-Functionalized Ionic Liquids Using Inverse Gas Chromatography:	https://www.doi.org/10.1021/je900838a
Measurement and Correlation of Isobaric Vapor-Liquid Equilibrium for Binary Systems of Allyl Alcohol with Isobutyl Acetate, Butyl Acetate, and Butyl Propionate at 101.3 kPa:	https://www.doi.org/10.1021/acs.jced.7b01024
Determination and Prediction of Vapor Liquid Equilibria for a System Containing Water + Butyl Acetate + Cyclohexane + Ethanol:	https://www.doi.org/10.1021/je3005408
Thermodynamics of 4'-bromomethyl-2-cyanobiphenyl in different solvents:	https://www.doi.org/10.1016/j.jct.2014.12.002
McGowan Method:	http://link.springer.com/article/10.1007/BF02311772
Vapour-liquid equilibrium and extractive distillation for separation of azeotrope isopropyl alcohol and diisopropyl ether:	https://www.doi.org/10.1016/j.jct.2018.11.013
Solubility of Captopril in 2-Propanol, Acetone, Acetonitrile, Methyl Acetate, Ethyl Acetate, and Butyl Acetate:	https://www.doi.org/10.1021/je900401z
Studies on liquid-liquid interactions of some ternary mixtures by density, viscosity, ultrasonic speed and refractive index measurements:	https://www.doi.org/10.1016/j.tca.2009.07.011
KDB:	https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=1079
Ternary Liquid-Liquid Equilibria for Systems Containing Alcohol or Acetic Acid + Ester + 1-Ethyl-3-methylimidazolium Hydrogen Sulfate at 313.2 K Using Headspace Gas Chromatography:	https://www.doi.org/10.1021/je800547k
Measurement and Modelization of VLE for Butyl Acetate with Methanol, Ethanol, 1-Propanol, and 1-Butanol: Experimental Data at 0.15 MPa:	https://www.doi.org/10.1021/acs.jced.8b00182
Solubility of 3-Nitrophthalic Acid in Different Solvents between 278 K and 353 K:	https://www.doi.org/10.1021/je0604737
Phase equilibria of (water + butyric acid + butyl acetate) ternary systems at different temperatures:	https://www.doi.org/10.1016/j.fluid.2014.07.023
PVT Property Measurements for Some Aliphatic Esters from (298 to 393) K and up to 35 MPa:	https://www.doi.org/10.1021/je060339m
Solubility Determination and Thermodynamic Models for 2-Methylnaphthalene in Different Solvents from T = (278.15 to 303.15) K:	https://www.doi.org/10.1021/je5010627
Density and Viscosity for a Binary Mixture of cis-3-Hexenyl Formate, Butyl Acetate, trans-2-Hexenyl Acetate, and cis-3-Hexenyl Acetate with Ethanol at Several Temperatures:	https://www.doi.org/10.1021/je0500025
Vapor-Liquid Equilibria at 101.32 kPa and Excess Properties of Binary Mixtures of Butyl Esters + tert-Butyl Alcohol:	https://www.doi.org/10.1021/je0497350
Solubility of o-Phthalic Acid in Methanol + Water and Methanol + Butyl Acetate from (295.87 to 359.75) K:	https://www.doi.org/10.1021/je0600505
Excess Molar Volumes and Viscosity Deviations of Binary Liquid Mixtures of 1,3-Dioxolane and 1,4-Dioxane with Butyl Acetate, Butyric Acid, Butylamine, and 2-Butanone at 298.15 K:	https://www.doi.org/10.1021/je0504109
Vapor-Liquid Equilibrium Data for Binary Mixtures of Dimethyl Carbonate with Methyl Acetate, Ethyl Acetate, n-Propyl Acetate, Isopropyl Acetate, n-Butyl Acetate, and Isoamyl Acetate at 93.13 kPa:	https://www.doi.org/10.1021/acs.jced.7b00704
Measurement and Correlation of Solubility on Reactive Crystallization of Methyl D-(4-Hydroxy-phenyl)glycinate:	https://www.doi.org/10.1021/acs.jced.6b00415
Measurement and correlation of solubility of D-camphor-10-sulfonic acid in pure solvents:	https://www.doi.org/10.1016/j.fluid.2015.04.014
Isothermal vapor-liquid equilibria, excess molar volume and the deviation of refractive indices for binary mixtures of 1-butanol, 1-hexanol, 3-methyl-1-butanol and butyl acetate:	https://www.doi.org/10.1016/j.fluid.2016.12.025
Measurement and thermodynamic modelling of ternary liquid-liquid equilibrium for extraction of thioglycolic acid from aqueous solution with different solvents:	https://www.doi.org/10.1016/j.jct.2017.06.015
Solubility of 2-Aminopyridine in Ethanol + n-Butyl Acetate from (288.15 to 318.15) K:	https://www.doi.org/10.1021/je800841v
Liquid-liquid equilibrium data for water + formic acid + solvent (butyl acetate, ethyl acetate, and isoamyl alcohol) at T = 291.15 K:	https://www.doi.org/10.1016/j.fluid.2016.01.045
Densities, speeds of sound, isentropic compressibilities, refractive indexes, and viscosities of tetrahydrofuran with haloalkane or alkyl ethanoate at T = 303.15 K:	https://www.doi.org/10.1016/j.tca.2004.08.001
Measurement and Correlation of the Solubility of e-CL-20 in 12 Organic Solvents at Temperatures Ranging from 278.15 to 318.15 K:	https://www.doi.org/10.1021/acs.jced.6b00761
Solubility Determination of Nicotinamide and Its Application for the Cocrystallization with Benzoic Acid:	https://www.doi.org/10.1021/acs.jced.8b00560
Application of ERAS model and Prigogine-Flory-Patterson theory to excess molar volumes for ternary mixtures of (2-chlorobutane + butylacetate + isobutanol) at T = 298.15 K:	https://www.doi.org/10.1016/j.jct.2011.05.017
Liquid-Liquid Equilibrium in Systems with an Ionic Liquid: Experimental Data for an Example of the Biphasic Acid Scavenging Utilizing Ionic Liquids Process:	https://www.doi.org/10.1021/je1004966
Densities, Excess Molar Volumes, Viscosities, and Refractive Indices of Binary Mixtures of n-Butyl Acetate with 1-Chloroalkanes (C4-C8) at 298.15 K:	https://www.doi.org/10.1007/s10765-010-0902-x
Isobaric Vapor-Liquid Equilibrium for Binary Systems of Thioglycolic Acid with Water, Butyl Acetate, Butyl Formate, and Isobutyl Acetate at 101.3 kPa:	https://www.doi.org/10.1021/acs.jced.6b00686
Thermodynamic properties of (an ester + an alkane). XVI. Experimental HEm and V Em values and a new correlation method for (an alkyl ethanoate + an n-alkane) at 318.15 K:	https://www.doi.org/10.1016/j.jct.2003.11.008
Liquid-Liquid Equilibria for the Ternary Systems Acetic Acid + Water + Butyl Acetate and Acetic Acid + Water + 2-Methyl Propyl Acetate at 304.15 K, 332.15 K, and 366.15 K:	https://www.doi.org/10.1021/je6005746
Densities, Sound Speed, and IR Studies of (Methanol + 1-Acetoxybutane) and (Methanol + 1,1-Dimethylethyl Ester) at (298.15, 303.15, 308.15, and 313.15) K:	https://www.doi.org/10.1021/je900442b

Liquid-Liquid Equilibrium Measurements and Correlation for Ternary Systems (Butyl Acetate + 1-Butanol + Ethylene Glycol/1,3-Propanediol/Ethanolamine) at 298.15 K:	https://www.doi.org/10.1021/acs.jced.8b01219
Abraham model linear free energy relationships for describing the partitioning and solubility behavior of nonelectrolyte organic solutes dissolved in pyridine at 298.15 K:	https://www.doi.org/10.1016/j.fluid.2016.10.009
Solubility of lansoprazole in different solvents:	https://www.doi.org/10.1016/j.fluid.2012.06.011
Solubility and limiting activity coefficient of simvastatin in different organic solvents:	https://www.doi.org/10.1016/j.fluid.2009.03.006
Determination and Modeling of Solubility of 4-Aminobenzamide in Different Pure Solvents:	https://www.doi.org/10.1021/acs.jced.8b01144
The Yaws Handbook of Vapor Pressure:	https://www.sciencedirect.com/book/9780128029992/the-yaws-handbook-of-vapor-pressure
Measurements and Modeling of VLE Data for Butyl Acetate with 2-Propanol or 2-Butanol: Binary Systems at 0.15 and 0.6 MPa:	https://www.doi.org/10.1021/acs.jced.7b00141
NIST Webbook:	http://webbook.nist.gov/cgi/cbook.cgi?ID=C123864&Units=SI
Experimental isobaric vapour liquid liquid equilibrium data for the quaternary systems water (1) ethanol (2) acetone (3) n-butyl acetate (4) and water (1) ethanol (2) acetone (3) methyl ethyl ketone (4) and their partially miscible-constituent ternaries:	https://www.doi.org/10.1016/j.fluid.2006.11.011
Liquid liquid equilibrium of ternary mixture (propargyl alcohol + water + butyl acetate):	https://www.doi.org/10.1016/j.fluid.2009.04.010
Thermodynamics of Phase and Chemical Equilibrium in a Strongly Nonideal Esterification System:	https://www.doi.org/10.1021/je0498199
Solubility of Valsartan in Different Organic Solvents and Ethanol + Water Binary Mixtures from (278.15 to 313.15) K:	https://www.doi.org/10.1021/je8007815
Viscosities and Interfacial Properties of 1-Methyl-3-butylimidazolium Hexafluorophosphate and 1-Isobutenyl-3-methylimidazolium Tetrafluoroborate Ionic Liquids:	https://www.doi.org/10.1021/je0604277
Effect of Temperature on the Change of Refractive Index on Mixing for Butyl Acetate + Aromatic Hydrocarbons:	https://www.doi.org/10.1007/s10765-005-8096-3
Solubility of Cloxacillin Sodium in Different Binary Solvents:	https://www.doi.org/10.1021/je800730k
Temperature dependence of limiting activity coefficients, Henry's law constants, and related infinite dilution properties of C4-C6 isomeric n-alkyl ethanoates/ethyl n-alkanoates in water. Measurement, critical compilation, correlation, and recommended data:	https://www.doi.org/10.1016/j.fluid.2014.05.023
Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5):	https://www.doi.org/10.1021/acs.jced.8b01120
Isobaric Vapor-Liquid Equilibria for the Binary Systems Benzene + Methyl Ethanoate, Benzene + Butyl Ethanoate, and Benzene + Methyl Heptanoate at 101.31 kPa:	https://www.doi.org/10.1021/je800915d
Solubility of Hydrogen in Ethylbenzene, Cumene, Acetone, Acetonitrile, Ethyl Acetate, Ethyl Formate, and Butyl Acetate from (288.2 to 318.2) K:	https://www.doi.org/10.1021/je800838w
Liquid-liquid equilibria for ternary systems acetic acid + n-butyl acetate + hydrocarbons at 293.15 K:	https://www.doi.org/10.1016/j.fluid.2013.07.032
Determination and correlation of solubility and mixing properties of isonicotinamide (form II) in some pure solvents:	https://www.doi.org/10.1016/j.tca.2016.01.012
Crippen Method:	http://pubs.acs.org/doi/abs/10.1021/ci990307l
Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters:	https://www.doi.org/10.1021/je050001c
Densities, surface tensions, and derived surface thermodynamics properties of (trimethylbenzene + propyl acetate, or butyl acetate) from T = 298.15 K to 313.15 K:	https://www.doi.org/10.1016/j.jct.2006.07.025
Dortmund Data Bank Vapor-Liquid Equilibrium Data:	http://www.ddbst.com/en/EED/VLE/VLE%20Acetonitrile%3BAcetic acid butyl ester.php
Solubility of 1H-1,2,4-Triazole in Ethanol, 1-Propanol, 2-Propanol, 1,2-Propanediol, Ethyl Formate, Methyl Acetate, Ethyl Acetate, and Butyl Acetate at (283 to 363) K:	https://www.doi.org/10.1021/je060452c
Topological and thermodynamic investigations of molecular interactions in binary mixtures: Molar excess volumes and molar excess enthalpies:	https://www.doi.org/10.1016/j.fluid.2005.06.011
Vapor-Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane:	https://www.doi.org/10.1021/acs.jced.5b01058
Solubility and Thermodynamic Modeling of Dimethyl Terephthalate in Pure Solvents and the Evaluation of the Mixing Properties of the Solutions:	https://www.doi.org/10.1021/acs.jced.9b00658

Legend

af:	Acentric Factor
aigt:	Autoignition Temperature
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
fll:	Lower Flammability Limit
flu:	Upper Flammability Limit

fpc:	Flash Point (Closed Cup Method)
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
speedsl:	Speed of sound in fluid
srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tc:	Critical Temperature
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility
zra:	Rackett Parameter