

Triethylene glycol

Other names:	1,2-BIS(2-HYDROXYETHOXY)ETHANE 1,2-di(.beta.-hydroxyethoxy)ethane 2,2'-(1,2-Ethanediylbis(oxy))bisethanol 2,2'-(ethane-1,2-diylbis(oxy))bis(ethan-1-ol) 2,2'-(ethylenedioxy)diethanol 2,2'-Ethylenedioxybis(ethanol) 2,2'-Ethylenedioxydiethanol 2,2'-Ethylenedioxyethanol 2-(2-(2-hydroxyethoxy)ethoxy)ethanol 3,6-Dioxaoctane-1,8-diol 3,6-dioxa-1,8-octanediol Di-«beta»-hydroxyethoxyethane Di-Â«betaÂ»-hydroxyethoxyethane Ethanol, 2,2'-(ethylenedioxy)di- Ethanol, 2,2'-[1,2-ethanediylbis(oxy)]bis- Ethylene glycol dihydroxydiethyl ether Ethylene glycol-bis-(2-hydroxyethyl ether) Glycol bis(hydroxyethyl) ether NSC 60758 TEG TRIGEN Triethylenglykol Trigenos Triglycol Trigol ethylene glycol bis(2-hydroxyethyl) ether
Inchi:	InChI=1S/C6H14O4/c7-1-3-9-5-6-10-4-2-8/h7-8H,1-6H2
InchiKey:	ZIBGPFATKBEMQZ-UHFFFAOYSA-N
Formula:	C6H14O4
SMILES:	OCCOCCOC
Mol. weight [g/mol]:	150.17
CAS:	112-27-6

Physical Properties

Property code	Value	Unit	Source
chl	-3557.60 ± 3.60	kJ/mol	NIST Webbook

gf	-484.00	kJ/mol	Joback Method
hf	-736.07	kJ/mol	Joback Method
hfl	-804.20 ± 3.60	kJ/mol	NIST Webbook
hfus	21.85	kJ/mol	Joback Method
hvap	60.50	kJ/mol	NIST Webbook
log10ws	0.96		Crippen Method
logp	-0.996		Crippen Method
mcvol	118.880	ml/mol	McGowan Method
nfpaf	%!d(float64=1)		KDB
nfpah	%!d(float64=1)		KDB
pc	3300.00 ± 60.00	kPa	NIST Webbook
rinpol	206.80		NIST Webbook
rinpol	1143.00		NIST Webbook
rinpol	1177.00		NIST Webbook
rinpol	206.80		NIST Webbook
tb	558.20	K	NIST Webbook
tb	551.50	K	NIST Webbook
tb	549.00 ± 2.00	K	NIST Webbook
tb	439.00 ± 5.00	K	NIST Webbook
tb	571.60 ± 1.00	K	NIST Webbook
tb	561.15	K	NIST Webbook
tb	549.00 ± 3.00	K	NIST Webbook
tc	713.00 ± 20.00	K	NIST Webbook
tc	788.00	K	Critical temperatures and pressures of ethylene glycols
tc	797.00 ± 10.00	K	NIST Webbook
tf	268.85	K	NIST Webbook
tf	263.75 ± 0.50	K	NIST Webbook
vc	0.446	m3/kmol	Joback Method

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	332.24	J/mol×K	671.22	Joback Method
cpg	339.62	J/mol×K	697.55	Joback Method
cpg	316.66	J/mol×K	618.55	Joback Method
cpg	308.46	J/mol×K	592.21	Joback Method
cpg	299.99	J/mol×K	565.88	Joback Method
cpg	346.71	J/mol×K	723.89	Joback Method
cpg	324.59	J/mol×K	644.88	Joback Method

cpl	347.90	J/mol×K	333.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	353.70	J/mol×K	343.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	359.30	J/mol×K	353.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	327.60	J/mol×K	298.00	NIST Webbook
cpl	336.30	J/mol×K	303.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	333.70	J/mol×K	298.00	NIST Webbook
cpl	339.50	J/mol×K	313.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	343.10	J/mol×K	323.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
dvisc	0.0371600	Paxs	298.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0292700	Paxs	303.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation

dvisc	0.0237400	Paxs	308.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0483200	Paxs	293.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0164100	Paxs	318.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0135100	Paxs	323.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0113500	Paxs	328.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0096020	Paxs	333.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0082780	Paxs	338.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation

dvisc	0.0009970	Paxs	462.25	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0351000	Paxs	299.65	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0195000	Paxs	313.05	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0096600	Paxs	333.10	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0055500	Paxs	353.05	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0034100	Paxs	373.50	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K

dvisc	0.0073510	Paxs	343.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0017100	Paxs	413.25	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0013900	Paxs	428.10	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0343980	Paxs	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
dvisc	0.0213060	Paxs	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures

dvisc	0.0016790	Paxs	413.73	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0041310	Paxs	364.44	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0059450	Paxs	349.25	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0090020	Paxs	334.96	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0190300	Paxs	312.96	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure

dvisc	0.0368200	Paxs	298.15	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0092880	Paxs	333.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)
dvisc	0.0129600	Paxs	323.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)
dvisc	0.0189600	Paxs	313.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)
dvisc	0.0292700	Paxs	303.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)

dvisc	0.0300120	Paxs	298.15	Thermophysical Properties For Diethylene Glycol + Nitrobenzene and Triethylene Glycol + (Chloro-, Bromo-, Nitro-) Benzene Systems at Different Temperatures
dvisc	0.0169720	Paxs	308.15	Thermophysical Properties For Diethylene Glycol + Nitrobenzene and Triethylene Glycol + (Chloro-, Bromo-, Nitro-) Benzene Systems at Different Temperatures
dvisc	0.0069060	Paxs	343.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)
dvisc	0.0023600	Paxs	393.30	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0192600	Paxs	313.20	Phase equilibria study on bromide-based ionic liquids with glycals and sulfolane. Experimental data and correlation
hvapt	64.60 ± 0.30	kJ/mol	502.00	NIST Webbook
hvapt	79.20 ± 7.90	kJ/mol	273.00	NIST Webbook
hvapt	77.00	kJ/mol	300.50	NIST Webbook
hvapt	71.50	kJ/mol	469.50	NIST Webbook
hvapt	67.70	kJ/mol	295.50	NIST Webbook
hvapt	60.80 ± 0.50	kJ/mol	502.00	NIST Webbook
hvapt	68.50 ± 0.30	kJ/mol	502.00	NIST Webbook
hvapt	72.20 ± 0.30	kJ/mol	502.00	NIST Webbook

rfi	1.45560		293.15	Infinite Dilution Activity Coefficients of Hydrocarbons in Triethylene Glycol and Tetraethylene Glycol
rfi	1.45314		293.15	Liquid-Liquid Equilibria of (Limonene + Linalool + Ethylene Glycol or Diethylene Glycol or Triethylene Glycol or 1,2-Propylene Glycol) Ternary Systems
rhol	1085.60	kg/m3	343.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1104.13	kg/m3	318.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhol	1100.22	kg/m3	323.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhol	1096.30	kg/m3	328.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhol	1092.38	kg/m3	333.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range

rhol	1124.60	kg/m3	293.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1120.80	kg/m3	298.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1116.90	kg/m3	303.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1113.00	kg/m3	308.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1109.10	kg/m3	313.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture

rhol	1105.20	kg/m3	318.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1101.30	kg/m3	323.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1097.40	kg/m3	328.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1093.50	kg/m3	333.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1089.60	kg/m3	338.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture

rhol	1108.03	kg/m3	313.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhol	1123.48	kg/m3	293.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhol	1119.59	kg/m3	298.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhol	1111.92	kg/m3	308.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhol	1111.81	kg/m3	308.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhol	1112.09	kg/m3	308.15	Excess molar enthalpies of binary mixtures containing ethylene glycols or poly(ethylene glycols) + ethyl alcohol at 308.15K and atmospheric pressure

rhol	1124.60	kg/m3	293.15	Experimental and prediction of volumetric properties of aqueous solution of (allyltriphenylPhosphonium bromide - Triethylene glycol) deep eutectic solvents
rhol	1120.80	kg/m3	298.15	Experimental and prediction of volumetric properties of aqueous solution of (allyltriphenylPhosphonium bromide - Triethylene glycol) deep eutectic solvents
rhol	1113.00	kg/m3	308.15	Experimental and prediction of volumetric properties of aqueous solution of (allyltriphenylPhosphonium bromide - Triethylene glycol) deep eutectic solvents
rhol	1105.20	kg/m3	318.15	Experimental and prediction of volumetric properties of aqueous solution of (allyltriphenylPhosphonium bromide - Triethylene glycol) deep eutectic solvents
rhol	1097.40	kg/m3	328.15	Experimental and prediction of volumetric properties of aqueous solution of (allyltriphenylPhosphonium bromide - Triethylene glycol) deep eutectic solvents

rhol	1085.60	kg/m3	343.15	Experimental and prediction of volumetric properties of aqueous solution of (allyltriphenylPhosphonium bromide - Triethylene glycol) deep eutectic solvents
rhol	1128.60	kg/m3	288.15	Thermophysical properties of glycols and glymes
rhol	1124.60	kg/m3	293.15	Thermophysical properties of glycols and glymes
rhol	1120.70	kg/m3	298.15	Thermophysical properties of glycols and glymes
rhol	1116.80	kg/m3	303.15	Thermophysical properties of glycols and glymes
rhol	1112.90	kg/m3	308.15	Thermophysical properties of glycols and glymes
rhol	1109.00	kg/m3	313.15	Thermophysical properties of glycols and glymes
rhol	1105.10	kg/m3	318.15	Thermophysical properties of glycols and glymes
rhol	1101.20	kg/m3	323.15	Thermophysical properties of glycols and glymes
rhol	1097.30	kg/m3	328.15	Thermophysical properties of glycols and glymes
rhol	1093.40	kg/m3	333.15	Thermophysical properties of glycols and glymes
rhol	1089.50	kg/m3	338.15	Thermophysical properties of glycols and glymes
rhol	1085.60	kg/m3	343.15	Thermophysical properties of glycols and glymes

rhol	1081.70	kg/m3	348.15	Thermophysical properties of glycols and glymes
rhol	1077.80	kg/m3	353.15	Thermophysical properties of glycols and glymes
rhol	1073.80	kg/m3	358.15	Thermophysical properties of glycols and glymes
rhol	1069.80	kg/m3	363.15	Thermophysical properties of glycols and glymes
rhol	1065.90	kg/m3	368.15	Thermophysical properties of glycols and glymes
rhol	1061.90	kg/m3	373.15	Thermophysical properties of glycols and glymes
rhol	1131.30	kg/m3	283.15	Thermophysical properties of glycols and glymes
rhol	1127.40	kg/m3	288.15	Thermophysical properties of glycols and glymes
rhol	1123.50	kg/m3	293.15	Thermophysical properties of glycols and glymes
rhol	1119.70	kg/m3	298.15	Thermophysical properties of glycols and glymes
rhol	1115.80	kg/m3	303.15	Thermophysical properties of glycols and glymes
rhol	1111.90	kg/m3	308.15	Thermophysical properties of glycols and glymes
rhol	1108.00	kg/m3	313.15	Thermophysical properties of glycols and glymes
rhol	1100.20	kg/m3	323.15	Thermophysical properties of glycols and glymes
rhol	1092.40	kg/m3	333.15	Thermophysical properties of glycols and glymes

rhol	1084.50	kg/m3	343.15	Thermophysical properties of glycols and glymes
rhol	1112.10	kg/m3	308.15	Excess Molar Enthalpies of Binary Mixtures Containing Glycols or Polyglycols + Dimethyl Sulfoxide at 308.15 K
rhol	1119.78	kg/m3	298.15	Thermodynamic Study of Binary Mixtures Containing Glycols or Polyethylene Glycols + Benzyl Alcohol at 308.15 K
rhol	1112.61	kg/m3	308.15	Thermodynamic Study of Binary Mixtures Containing Glycols or Polyethylene Glycols + Benzyl Alcohol at 308.15 K
rhol	1115.81	kg/m3	303.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhol	1112.61	kg/m3	308.15	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Glycols or Poly(Ethylene Glycols) and 2-Phenylethyl Alcohol at 308.15 K and Atmospheric Pressure

rhol	1112.59	kg/m3	308.50	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Ethers and Benzyl Alcohol at 308.15 K and Atmospheric Pressure
rhol	1120.70	kg/m3	298.15	Isobaric Vapor-Liquid Equilibrium for Four Binary Systems of Ethane-1,2-diol, Butane-1,4-diol, 2-(2-Hydroxyethoxy)ethanol and 2-[2-(2-Hydroxyethoxy)ethoxy]ethanol at 10.0 kPa, 20.0 kPa and 40.0 kPa
rhol	1116.50	kg/m3	303.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
rhol	1108.90	kg/m3	313.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
rhol	1101.10	kg/m3	323.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures

rhol	1093.40	kg/m3	333.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
rhol	1085.50	kg/m3	343.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
rhol	1116.60	kg/m3	302.85	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhol	1111.90	kg/m3	307.75	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhol	1108.40	kg/m3	312.65	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhol	1104.70	kg/m3	317.45	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K

rhol	1119.69	kg/m3	298.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhol	1097.90	kg/m3	327.05	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhol	1093.50	kg/m3	332.15	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhol	1086.10	kg/m3	341.45	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhol	1123.20	kg/m3	293.35	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhol	1124.50	kg/m3	293.15	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhol	1123.56	kg/m3	293.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range

rhol	1127.43	kg/m3	288.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhol	1131.29	kg/m3	283.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhol	1135.14	kg/m3	278.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhol	1085.90	kg/m3	343.15	Density and vapour pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water)
rhol	1093.70	kg/m3	333.15	Density and vapour pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water)
rhol	1101.50	kg/m3	323.15	Density and vapour pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water)

rhol	1109.20	kg/m3	313.15	Density and vapour pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water)
rhol	1117.00	kg/m3	303.15	Density and vapour pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water)
rhol	1124.70	kg/m3	293.15	Density and vapour pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water)
rhol	1127.37	kg/m3	288.15	Activity coefficients at infinite dilution of organic solutes in diethylene glycol and triethylene glycol from gas-liquid chromatography
rhol	1116.05	kg/m3	298.00	Removal of aromatic hydrocarbons from hydrocarbon mixture using glycols at 303.15 K and 333.15 K and atmospheric pressure: Experimental and calculated data by NRTL and UNIQUAC models

rhol	1101.00	kg/m3	322.25	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhol	1115.70	kg/m3	303.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhol	1119.78	kg/m3	298.15	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Glycols or Poly(Ethylene Glycols) and 2-Phenylethyl Alcohol at 308.15 K and Atmospheric Pressure
tcondl	0.19	W/mxK	328.40	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.19	W/mxK	318.40	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.19	W/mxK	308.20	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols

tcondl	0.19	W/mxK	298.10	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.19	W/mxK	338.40	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.94699e+01
Coeff. B	-8.61684e+03
Coeff. C	2.20480e+01
Temperature range (K), min.	427.16
Temperature range (K), max.	586.55

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C*\ln(T) + D*T^2$
Coeff. A	2.93684e+01
Coeff. B	-8.89710e+03
Coeff. C	-1.46752e+00
Coeff. D	2.12637e-06
Temperature range (K), min.	265.79
Temperature range (K), max.	700.00

Datasets

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
283.08	100.00	1131.7
283.08	1000.00	1132.4
283.08	2000.00	1132.8
283.08	5000.00	1134.1
283.08	7000.00	1134.9
283.08	10000.00	1136.2
283.08	12000.00	1137.1
283.08	16000.00	1138.8
283.08	20000.00	1140.5
283.08	25000.00	1142.5
283.08	30000.00	1144.5
283.08	35000.00	1146.5
283.08	40000.00	1148.4
283.08	45000.00	1150.2
283.08	50000.00	1152.1
283.08	55000.00	1154.0
283.08	60000.00	1155.8
283.08	65000.00	1157.6
283.08	70000.00	1159.4
283.08	75000.00	1161.0
283.08	80000.00	1162.8
283.08	85000.00	1164.5
283.08	90000.00	1166.1
283.08	95000.00	1167.7
293.14	100.00	1124.1
293.14	1000.00	1124.5
293.14	2000.00	1124.9
293.14	5000.00	1126.3
293.14	7000.00	1127.3
293.14	10000.00	1128.6
293.14	12000.00	1129.4
293.14	16000.00	1131.3
293.14	20000.00	1132.9
293.14	25000.00	1135.0
293.14	30000.00	1137.1

293.14	35000.00	1139.2
293.14	40000.00	1141.1
293.14	45000.00	1143.0
293.14	50000.00	1145.0
293.14	55000.00	1146.9
293.14	60000.00	1148.7
293.14	65000.00	1150.5
293.14	70000.00	1152.4
293.14	75000.00	1154.2
293.14	80000.00	1155.9
293.14	85000.00	1157.6
293.14	90000.00	1159.2
293.14	95000.00	1160.9
303.12	100.00	1116.2
303.12	1000.00	1116.6
303.12	2000.00	1117.1
303.12	5000.00	1118.5
303.12	7000.00	1119.5
303.12	10000.00	1120.9
303.12	12000.00	1121.8
303.12	16000.00	1123.6
303.12	20000.00	1125.4
303.12	25000.00	1127.6
303.12	30000.00	1129.7
303.12	35000.00	1131.8
303.12	40000.00	1133.9
303.12	45000.00	1135.9
303.12	50000.00	1137.9
303.12	55000.00	1139.9
303.12	60000.00	1141.8
303.12	65000.00	1143.7
303.12	70000.00	1145.5
303.12	75000.00	1147.3
303.12	80000.00	1149.1
303.12	85000.00	1150.8
303.12	90000.00	1152.6
303.12	95000.00	1154.2
313.18	100.00	1108.3
313.18	1000.00	1108.7
313.18	2000.00	1109.2
313.18	5000.00	1110.7
313.18	7000.00	1111.7
313.18	10000.00	1113.1
313.18	12000.00	1114.1

313.18	16000.00	1115.9
313.18	20000.00	1117.8
313.18	25000.00	1120.0
313.18	30000.00	1122.3
313.18	35000.00	1124.4
313.18	40000.00	1126.6
313.18	45000.00	1128.7
313.18	50000.00	1130.6
313.18	55000.00	1132.6
313.18	60000.00	1134.6
313.18	65000.00	1136.6
313.18	70000.00	1138.5
313.18	75000.00	1140.3
313.18	80000.00	1142.1
313.18	85000.00	1143.9
313.18	90000.00	1145.6
313.18	95000.00	1147.4
323.14	100.00	1100.5
323.14	1000.00	1101.0
323.14	2000.00	1101.5
323.14	5000.00	1103.0
323.14	7000.00	1104.1
323.14	10000.00	1105.5
323.14	12000.00	1106.5
323.14	16000.00	1108.4
323.14	20000.00	1110.3
323.14	25000.00	1112.6
323.14	30000.00	1114.9
323.14	35000.00	1117.1
323.14	40000.00	1119.4
323.14	45000.00	1121.5
323.14	50000.00	1123.7
323.14	55000.00	1125.7
323.14	60000.00	1127.7
323.14	65000.00	1129.7
323.14	70000.00	1131.7
323.14	75000.00	1133.5
323.14	80000.00	1135.4
323.14	85000.00	1137.3
323.14	90000.00	1139.0
323.14	95000.00	1140.8
333.10	100.00	1092.7
333.10	1000.00	1093.2
333.10	2000.00	1093.8

333.10	5000.00	1095.4
333.10	7000.00	1096.4
333.10	10000.00	1098.0
333.10	12000.00	1098.9
333.10	16000.00	1100.9
333.10	20000.00	1102.9
333.10	25000.00	1105.3
333.10	30000.00	1107.7
333.10	35000.00	1110.1
333.10	40000.00	1112.3
333.10	45000.00	1114.5
333.10	50000.00	1116.6
333.10	55000.00	1118.9
333.10	60000.00	1120.8
333.10	65000.00	1122.9
333.10	70000.00	1124.9
333.10	75000.00	1126.9
333.10	80000.00	1128.8
333.10	85000.00	1130.7
333.10	90000.00	1132.5
333.10	95000.00	1134.4
343.14	100.00	1084.7
343.14	1000.00	1085.3
343.14	2000.00	1086.0
343.14	5000.00	1087.6
343.14	7000.00	1088.6
343.14	10000.00	1090.2
343.14	12000.00	1091.3
343.14	16000.00	1093.4
343.14	20000.00	1095.4
343.14	25000.00	1097.9
343.14	30000.00	1100.4
343.14	35000.00	1102.8
343.14	40000.00	1105.1
343.14	45000.00	1107.4
343.14	50000.00	1109.6
343.14	55000.00	1111.9
343.14	60000.00	1114.0
343.14	65000.00	1116.1
343.14	70000.00	1118.1
343.14	75000.00	1120.1
343.14	80000.00	1122.1
343.14	85000.00	1124.1
343.14	90000.00	1126.0

343.14	95000.00	1128.0
353.10	100.00	1077.0
353.10	1000.00	1076.9
353.10	2000.00	1078.0
353.10	5000.00	1079.8
353.10	7000.00	1080.9
353.10	10000.00	1082.6
353.10	12000.00	1083.6
353.10	16000.00	1085.7
353.10	20000.00	1088.0
353.10	25000.00	1090.5
353.10	30000.00	1093.2
353.10	35000.00	1095.5
353.10	40000.00	1098.0
353.10	45000.00	1100.3
353.10	50000.00	1102.6
353.10	55000.00	1104.9
353.10	60000.00	1107.3
353.10	65000.00	1109.1
353.10	70000.00	1111.5
353.10	75000.00	1113.3
353.10	80000.00	1115.6
353.10	85000.00	1117.4
353.10	90000.00	1119.5
353.10	95000.00	1121.3
363.16	100.00	1068.9
363.16	1000.00	1069.4
363.16	2000.00	1070.1
363.16	5000.00	1071.8
363.16	7000.00	1073.0
363.16	10000.00	1074.6
363.16	12000.00	1075.8
363.16	16000.00	1078.2
363.16	20000.00	1080.3
363.16	25000.00	1082.9
363.16	30000.00	1085.6
363.16	35000.00	1088.1
363.16	40000.00	1090.6
363.16	45000.00	1093.0
363.16	50000.00	1095.4
363.16	55000.00	1097.8
363.16	60000.00	1100.1
363.16	65000.00	1102.3
363.16	70000.00	1104.5

363.16	75000.00	1106.6
363.16	80000.00	1108.7
363.16	85000.00	1110.7
363.16	90000.00	1112.8
363.16	95000.00	1114.8

Reference

<https://www.doi.org/10.1016/j.fluid.2017.01.003>

Temperature, K	Pressure, kPa	Mass density, kg/m3
283.15	100.00	1130.8
283.15	100.00	1130.8
283.15	660.00	1131.0
283.15	1150.00	1131.2
283.15	1570.00	1131.4
283.15	2090.00	1131.6
283.15	3090.00	1132.0
283.15	5060.00	1132.9
283.15	6940.00	1133.6
283.15	10020.00	1134.9
283.15	14850.00	1136.9
283.15	19830.00	1138.9
283.15	24700.00	1140.8
283.15	29600.00	1142.7
283.15	34510.00	1144.6
283.15	39360.00	1146.4
283.15	44290.00	1148.2
283.15	49180.00	1150.0
283.15	54110.00	1151.7
283.15	58970.00	1153.4
283.15	63860.00	1155.1
283.15	68790.00	1156.8
293.15	100.00	1122.9
293.15	100.00	1122.9
293.15	640.00	1123.1
293.15	1090.00	1123.4
293.15	1600.00	1123.6
293.15	2140.00	1123.8
293.15	3080.00	1124.2
293.15	5030.00	1125.1
293.15	7010.00	1125.9
293.15	9950.00	1127.2
293.15	14850.00	1129.3
293.15	19770.00	1131.3

293.15	24660.00	1133.3
293.15	29510.00	1135.2
293.15	34610.00	1137.2
293.15	39370.00	1139.1
293.15	44320.00	1141.0
293.15	49130.00	1142.8
293.15	54050.00	1144.6
293.15	59060.00	1146.4
293.15	63780.00	1148.0
303.15	100.00	1115.2
303.15	100.00	1115.1
303.15	630.00	1115.4
303.15	1130.00	1115.6
303.15	1620.00	1115.9
303.15	2140.00	1116.1
303.15	3070.00	1116.5
303.15	5080.00	1117.4
303.15	6960.00	1118.3
303.15	9960.00	1119.6
303.15	14840.00	1121.7
303.15	19750.00	1123.8
303.15	24670.00	1125.9
303.15	29570.00	1127.9
303.15	34500.00	1129.9
303.15	39360.00	1131.9
303.15	44300.00	1133.8
303.15	49190.00	1135.7
303.15	54090.00	1137.6
303.15	58850.00	1139.3
303.15	63890.00	1141.2
303.15	68750.00	1142.9
313.15	100.00	1107.4
313.15	100.00	1107.4
313.15	670.00	1107.6
313.15	1130.00	1107.9
313.15	1600.00	1108.1
313.15	2080.00	1108.3
313.15	3100.00	1108.8
313.15	5030.00	1109.7
313.15	7010.00	1110.6
313.15	10010.00	1112.0
313.15	14880.00	1114.2
313.15	19750.00	1116.4
313.15	24680.00	1118.6

313.15	29560.00	1120.6
313.15	34510.00	1122.7
313.15	39330.00	1124.7
313.15	44290.00	1126.7
313.15	49180.00	1128.6
313.15	54160.00	1130.6
313.15	59000.00	1132.4
313.15	63910.00	1134.3
313.15	68840.00	1136.0
323.15	100.00	1099.6
323.15	100.00	1099.5
323.15	590.00	1099.8
323.15	1140.00	1100.0
323.15	1600.00	1100.3
323.15	2080.00	1100.5
323.15	3020.00	1101.0
323.15	5050.00	1101.9
323.15	7000.00	1102.9
323.15	9970.00	1104.3
323.15	14870.00	1106.7
323.15	19780.00	1108.9
323.15	24700.00	1111.2
323.15	29650.00	1113.3
323.15	34470.00	1115.4
323.15	39340.00	1117.5
323.15	44250.00	1119.6
323.15	49170.00	1121.6
323.15	54080.00	1123.5
323.15	58970.00	1125.5
323.15	63800.00	1127.3
323.15	68780.00	1129.2
333.15	100.00	1091.7
333.15	100.00	1091.7
333.15	660.00	1092.0
333.15	1110.00	1092.2
333.15	1600.00	1092.5
333.15	2100.00	1092.7
333.15	3070.00	1093.2
333.15	5060.00	1094.2
333.15	6980.00	1095.2
333.15	9970.00	1096.6
333.15	14840.00	1099.0
333.15	19660.00	1101.3
333.15	24670.00	1103.7

333.15	29610.00	1106.0
333.15	34530.00	1108.2
333.15	39400.00	1110.3
333.15	44280.00	1112.5
333.15	49110.00	1114.5
333.15	54040.00	1116.5
333.15	59060.00	1118.6
333.15	63830.00	1120.5
333.15	68770.00	1122.4
343.15	100.00	1083.9
343.15	100.00	1083.9
343.15	640.00	1084.2
343.15	1120.00	1084.4
343.15	1600.00	1084.7
343.15	2110.00	1084.9
343.15	3040.00	1085.5
343.15	5040.00	1086.6
343.15	6960.00	1087.5
343.15	9920.00	1089.0
343.15	14810.00	1091.6
343.15	19680.00	1093.9
343.15	24620.00	1096.4
343.15	29580.00	1098.7
343.15	34460.00	1101.0
343.15	39370.00	1103.3
343.15	44240.00	1105.4
343.15	49160.00	1107.6
343.15	54020.00	1109.7
343.15	58940.00	1111.7
343.15	63890.00	1113.8
343.15	68680.00	1115.7
353.15	100.00	1076.0
353.15	100.00	1076.0
353.15	650.00	1076.3
353.15	1100.00	1076.5
353.15	1550.00	1076.7
353.15	2100.00	1077.1
353.15	3050.00	1077.6
353.15	5040.00	1078.6
353.15	7010.00	1079.8
353.15	9960.00	1081.3
353.15	14810.00	1084.0
353.15	19780.00	1086.5
353.15	24610.00	1089.0

353.15	29560.00	1091.9
353.15	34450.00	1093.8
353.15	39370.00	1096.1
353.15	44270.00	1098.4
353.15	49200.00	1100.6
353.15	54090.00	1102.8
353.15	59010.00	1104.9
353.15	63820.00	1107.0
353.15	68800.00	1109.0
363.15	100.00	1068.1
363.15	100.00	1068.0
363.15	660.00	1068.4
363.15	1120.00	1068.7
363.15	1560.00	1068.9
363.15	2130.00	1069.2
363.15	3050.00	1069.8
363.15	5090.00	1070.9
363.15	6990.00	1072.0
363.15	9980.00	1073.7
363.15	14880.00	1076.4
363.15	19680.00	1079.0
363.15	24720.00	1081.7
363.15	29630.00	1084.2
363.15	34490.00	1086.6
363.15	39430.00	1089.0
363.15	44200.00	1091.4
363.15	49240.00	1093.7
363.15	54100.00	1095.9
363.15	59010.00	1098.1
363.15	63880.00	1100.2
363.15	68830.00	1102.3

Reference

<https://www.doi.org/10.1016/j.fluid.2018.09.026>

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
298.15	98.00	0.0368200
298.15	49030.00	0.0552300
298.15	98060.00	0.0802900
298.15	147100.00	0.1144000

298.15	196130.00	0.1606000
298.15	245160.00	0.2218000
312.96	98.00	0.0190300
313.05	49030.00	0.0274200
313.10	98060.00	0.0382800
313.18	147100.00	0.0525000
313.25	196130.00	0.0706800
313.26	245160.00	0.0939900
334.96	98.00	0.0090020
335.11	49030.00	0.0124500
335.14	98060.00	0.0167000
335.20	147100.00	0.0220300
335.25	196130.00	0.0284800
335.26	245160.00	0.0363700
349.25	98.00	0.0059450
349.94	196130.00	0.0175300
349.98	49030.00	0.0080610
349.98	98060.00	0.0106600
349.99	245160.00	0.0218400
350.03	147100.00	0.0137500
364.44	98.00	0.0041310
364.44	49030.00	0.0055370
364.72	98060.00	0.0071490
365.03	147100.00	0.0090210
365.07	196130.00	0.0112400
365.20	245160.00	0.0138000
413.73	98.00	0.0016790
414.00	49030.00	0.0021790
414.15	98060.00	0.0028360
414.27	147100.00	0.0033200
414.30	196130.00	0.0039950
414.43	245160.00	0.0044850
462.25	98.00	0.0009970
462.26	49030.00	0.0013030
462.32	98060.00	0.0016140
462.41	147100.00	0.0019410
462.45	196130.00	0.0023000
462.58	245160.00	0.0026780

Reference

<https://www.doi.org/10.1016/j.fluid.2011.11.022>

Pressure, kPa	Temperature, K	Viscosity, Pa*s
101.30	308.15	0.0238400

Joule-Thomson coefficient, K/kPa

Temperature, K - Liquid	Pressure, kPa - Liquid	Joule-Thomson coefficient, K/kPa - Liquid
293.10	7000.00	-0.0004

Reference <https://www.doi.org/10.1016/j.fluid.2011.03.011>

Sources

Solubilities and thermodynamic properties of CO₂ in choline-chloride Based Deep Eutectic Solvents.
Density, Viscosities, and Excess Properties for Binary Mixtures of Solubility of CO₂ in Non-Aqueous + Aqueous System at temperatures: 293.15K, densities, Joule-Thomson, Benzyl Viscosities, Speeds of Sound, Excess Thermal Stability analysis, experimental Isentropic Compressibilities, and densities and pressures for Alkyl (Methyl, Ethyl) Chloride and 1,4-Pentanediol + Glycolic Acid binary mixtures. A new empirical equation of state with a new departure for binary Mixtures of Some Glycolic Acid and Choline Chloride Based Ionic Liquids. Analysis of their Physical Properties:

KDB:

Investigation on Temperature-Dependent Volumetric Thermophysical Properties of characterization of ternary system Experimental determination of refractive index (nD₂₀) and density (ρ) of binary mixtures of aqueous solutions of glycols at several temperatures and densities of deep eutectic solvents using atomic simulation theory of Binary Mixtures Containing Glycols or binary liquid crystals in binary alcohol systems (ethylene glycol + salts + water) at different temperatures; ethanol and aqueous solutions: Densities and vapor pressures of mixed-solvent desiccant systems. Critical temperature and pressures of ethylene glycol + Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Density and vapor pressures of glycols and aqueous glycols) and properties of eutectic heat capacity of binary and ternary systems of ethylene glycol + typical organic chloride liquid desorption and extraction efficiency: Some Ethylene Glycols in Aqueous Molten Salt Ionic by Different Type III <https://www.doi.org/10.1021/acs.jced.5b00989>
Deep Eutectic Solvents: Statistical and Volumetric Approach:

- <https://www.doi.org/10.1016/j.jct.2014.04.012>
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- <https://www.doi.org/10.1021/acs.jced.7b00501>
- <https://www.doi.org/10.1016/j.jct.2012.12.011>
- <https://www.doi.org/10.1016/j.jct.2011.05.034>
- <https://www.doi.org/10.1016/j.jct.2018.02.022>
- <https://www.doi.org/10.1016/j.fluid.2013.06.050>
- <https://www.doi.org/10.1021/je0342062>
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- <https://www.doi.org/10.1016/j.fluid.2016.03.007>
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- <https://www.doi.org/10.1021/je049943s>
- <https://www.doi.org/10.1016/j.jct.2014.08.005>
- <https://www.doi.org/10.1016/j.jct.2013.10.028>
- <https://www.doi.org/10.1021/acs.jced.8b00058>

Thermophysical Properties For Diethylene Glycol + Nitrobenzene and Ternary Solvent Exchange (TASE) Binary, expansion of excess molar enthalpies at temperatures for later gas mixtures containing Glycols or Polyglycols + Dimethyl Sulfoxide at 308.15 K: Experimental and predicted excess molar enthalpies of some working pairs for the Dilution Activity Coefficients of Hydrocarbons in Triethylene Glycol (TEG) Vapor Pressure Data:

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<https://www.doi.org/10.1016/j.fluid.2011.03.011>
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Liquid-Liquid Equilibria for Benzene/Thiophene + N,N-Diethoxyhexadecane + Deep Eutectic Solvents: Data and Correlation of Liquid Equilibria for Binary and Ternary Systems Containing Glycols, Isopropyl Alcohol, and Water for Equilibrium Systems of Phenols and Model Compounds (Methyl 4-tert-butyl-2-(2-hydroxyethyl)benzoate, 2-(2-hydroxyethyl)benzoic acid, glycols and their mixtures) at Temperature from 293 K Preparation and separation from its decomposition products up to 200 MPa Solves of 1,2-OH-bis(Chloromethyl) Ether, Phosphorus Solvent, Bis(2-Ethoxyethoxy) Ethylene + Dimethyl Ether or Ethylene Glycol or Dimethyl Ether or Triethylene Glycol or 1,2-Propylene Glycol Ternary Molar heat capacities of some aqueous 2-amino-2-hydroxymethyl-1,3-propanediol Vapour pressures, densities, and viscosities of the aqueous solutions containing triethylene glycol or propylene glycol and model butyl glycol. Logistic liquid-phase equilibrium of organic solutes in diethylene glycol and properties of supercritical CO₂ in binary system of Tri-ethylene Glycol + Dimethyl Sulfoxide at 298.15 K from binary sub 15 K mixed using 23.15 MPa at 303.15 K and 330.15 K and densities and viscosities of thiourea in the Yaws Handbook of Vapor Pressure and Solubility Data by Temperatures from 200 to 1000 K: Measurement and correlation of physicochemical properties of aqueous and organic solvents in triethylene glycol/water mixtures in 293 K pressure of reverse Mixed-Solvent Desiccants Containing Glycol + Water Molar heat capacity of several aqueous solutions of NaOH, NaClO, NaOH and NaClO₄, high pressure thermodynamic + glycol: Measurement of triethylene glycol solubility in supercritical methane at pressures up to 100 MPa Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Dioxane in Heavy Mixtures Containing Diethylene and Triethylene Glycol Vapour-Liquid Equilibrium of Water + Glycerol Measurement and Correlation for Solubility of Thiourea in Triglycol + Water at temperatures of 293.15 K and 298.15 K: Joback Method:

Vapor-Liquid Equilibria of Water + Triethylene Glycol (TEG) and Water + Viscosity of liquid triethylene, triethylene and tetraethylene glycols at Moderate and High Pressure studies on interaction of triethylene glycol, Diethylene glycol and tert-butyltriethylene glycol Properties (Capillary) of glycerol at temperatures 17 – 293.15 K (308.15) K: influence of crown ethers and glycols Experimental study and phase equilibrium modeling of systems containing acid gas and glycol :

Mutual diffusion coefficients of aqueous solutions of some glycols: Effect of Ethylene, Diethylene, and Triethylene Glycols and Glycerol on the Free enthalpies of binary phase mixtures containing ethylene glycols or glycerol or acetyl glycol.
Effect of benzyl alcohol on the viscosity of some glycols and their analogues: Acoustic and thermodynamic study of DEP-anthanol in aqueous solutions of glycols at different temperatures of poly(ethylene glycol) and aromatic hydrocarbons.
Experimental study of the density and viscosity of polyethylene glycols and their analogues at temperatures from 293 degrees Celsius down to -100 degrees Celsius (down to atmospheric pressure).
Efficient extraction of benzene and thiophene by novel deep eutectic solvents based on chitosan and organic acids.
Experimental and calculation of volumetric properties at temperatures around 298 K for a series of poly(ethylene glycols) at infinite dilution in water at temperatures T = (278 to 343) K and atmospheric pressure.

Legend

chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dvisc:	Dynamic viscosity
gf:	Standard Gibbs free energy of formation
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
mujt:	Joule-Thomson coefficient
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhol:	Liquid Density
rinpolt:	Non-polar retention indices
tb:	Normal Boiling Point Temperature
tc:	Critical Temperature
tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
vc:	Critical Volume

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