

Triethylene glycol

Other names:	1,2-BIS(2-HYDROXYETHOXY)ETHANE
	1,2-di(.beta.-hydroxyethoxy)ethane
	2,2'-(1,2-EthanediyIbis(oxy))bisethanol
	2,2'-(ethane-1,2-diylbis(oxy))bis(ethan-1-ol)
	2,2'-(ethylenedioxy)diethanol
	2,2'-Ethylenedioxybis(ethanol)
	2,2'-Ethylenedioxydiethanol
	2,2'-Ethylenedioxyethanol
	2-(2-(2-hydroxyethoxy)ethoxy)ethanol
	3,6-Dioxaoctane-1,8-diol
	3,6-dioxa-1,8-octanediol
	Di-«beta»-hydroxyethoxyethane
	Di-Â«betaÂ»-hydroxyethoxyethane
	Ethanol, 2,2'-(ethylenedioxy)di-
	Ethanol, 2,2'-[1,2-ethanediyIbis(oxy)]bis-
	Ethylene glycol dihydroxydiethyl ether
	Ethylene glycol-bis-(2-hydroxyethyl ether)
	Glycol bis(hydroxyethyl) ether
	NSC 60758
	TEG
	TRIGEN
	Triethylenglykol
	Trigenos
	Triglycol
	Trigol
	ethylene glycol bis(2-hydroxyethyl) ether
Inchi:	InChI=1S/C6H14O4/c7-1-3-9-5-6-10-4-2-8/h7-8H,1-6H2
InchiKey:	ZIBGPFATKBEMQZ-UHFFFAOYSA-N
Formula:	C6H14O4
SMILES:	OCCOCCOCCO
Mol. weight [g/mol]:	150.17
CAS:	112-27-6

Physical Properties

Property code	Value	Unit	Source
chl	-3557.60 ± 3.60	kJ/mol	NIST Webbook

gf	-484.00	kJ/mol	Joback Method
hf	-736.07	kJ/mol	Joback Method
hfl	-804.20 ± 3.60	kJ/mol	NIST Webbook
hfus	21.85	kJ/mol	Joback Method
hvap	60.50	kJ/mol	NIST Webbook
log10ws	0.96		Crippen Method
logp	-0.996		Crippen Method
mcvol	118.880	ml/mol	McGowan Method
nfpaf	%!d(float64=1)		KDB
nfpah	%!d(float64=1)		KDB
pc	3300.00 ± 60.00	kPa	NIST Webbook
rinpol	206.80		NIST Webbook
rinpol	1177.00		NIST Webbook
rinpol	1143.00		NIST Webbook
rinpol	206.80		NIST Webbook
tb	549.00 ± 3.00	K	NIST Webbook
tb	551.50	K	NIST Webbook
tb	549.00 ± 2.00	K	NIST Webbook
tb	439.00 ± 5.00	K	NIST Webbook
tb	571.60 ± 1.00	K	NIST Webbook
tb	561.15	K	NIST Webbook
tb	558.20	K	NIST Webbook
tc	797.00 ± 10.00	K	NIST Webbook
tc	788.00	K	Critical temperatures and pressures of ethylene glycols
tc	713.00 ± 20.00	K	NIST Webbook
tf	268.85	K	NIST Webbook
tf	263.75 ± 0.50	K	NIST Webbook
vc	0.446	m3/kmol	Joback Method

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	299.99	J/mol×K	565.88	Joback Method
cpg	308.46	J/mol×K	592.21	Joback Method
cpg	316.66	J/mol×K	618.55	Joback Method
cpg	324.59	J/mol×K	644.88	Joback Method
cpg	332.24	J/mol×K	671.22	Joback Method
cpg	339.62	J/mol×K	697.55	Joback Method
cpg	346.71	J/mol×K	723.89	Joback Method

cpl	336.30	J/mol×K	303.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	339.50	J/mol×K	313.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	343.10	J/mol×K	323.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	347.90	J/mol×K	333.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	353.70	J/mol×K	343.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	359.30	J/mol×K	353.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	333.70	J/mol×K	298.00	NIST Webbook
cpl	327.60	J/mol×K	298.00	NIST Webbook
dvisc	0.0189600	Pa×s	313.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)
dvisc	0.0169720	Pa×s	308.15	Thermophysical Properties For Diethylene Glycol + Nitrobenzene and Triethylene Glycol + (Chloro-, Bromo-, Nitro-) Benzene Systems at Different Temperatures

dvisc	0.0292700	Pa×s	303.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)
dvisc	0.0300120	Pa×s	298.15	Thermophysical Properties For Diethylene Glycol + Nitrobenzene and Triethylene Glycol + (Chloro-, Bromo-, Nitro-) Benzene Systems at Different Temperatures
dvisc	0.0129600	Pa×s	323.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)
dvisc	0.0092880	Pa×s	333.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)
dvisc	0.0069060	Pa×s	343.15	Vapour pressures, densities, and viscosities of the aqueous solutions containing (triethylene glycol or propylene glycol) and (LiCl or LiBr)

dvisc	0.0368200	Paxs	298.15	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0190300	Paxs	312.96	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0343980	Paxs	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
dvisc	0.0059450	Paxs	349.25	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0041310	Paxs	364.44	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure

dvisc	0.0016790	Pa×s	413.73	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure	
dvisc	0.0009970	Pa×s	462.25	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure	
dvisc	0.0483200	Pa×s	293.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation	
dvisc	0.0090020	Pa×s	334.96	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure	
dvisc	0.0292700	Pa×s	303.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation	
dvisc	0.0237400	Pa×s	308.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation	

dvisc	0.0192600	Pa×s	313.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0164100	Pa×s	318.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0135100	Pa×s	323.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0113500	Pa×s	328.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0096020	Pa×s	333.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0082780	Pa×s	338.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0073510	Pa×s	343.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation

dvisc	0.0351000	Pa×s	299.65	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0195000	Pa×s	313.05	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0096600	Pa×s	333.10	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0055500	Pa×s	353.05	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0034100	Pa×s	373.50	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0023600	Pa×s	393.30	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K

dvisc	0.0017100	Pa×s	413.25	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0013900	Pa×s	428.10	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0371600	Pa×s	298.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0213060	Pa×s	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
hvapt	72.20 ± 0.30	kJ/mol	502.00	NIST Webbook
hvapt	68.50 ± 0.30	kJ/mol	502.00	NIST Webbook
hvapt	60.80 ± 0.50	kJ/mol	502.00	NIST Webbook
hvapt	67.70	kJ/mol	295.50	NIST Webbook
hvapt	71.50	kJ/mol	469.50	NIST Webbook
hvapt	77.00	kJ/mol	300.50	NIST Webbook
hvapt	79.20 ± 7.90	kJ/mol	273.00	NIST Webbook
hvapt	64.60 ± 0.30	kJ/mol	502.00	NIST Webbook

rfi	1.45314		293.15	Liquid-Liquid Equilibria of (Limonene + Linalool + Ethylene Glycol or Diethylene Glycol or Triethylene Glycol or 1,2-Propylene Glycol) Ternary Systems
rfi	1.45560		293.15	Infinite Dilution Activity Coefficients of Hydrocarbons in Triethylene Glycol and Tetraethylene Glycol
rhoI	1096.30	kg/m3	328.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhoI	1127.37	kg/m3	288.15	Activity coefficients at infinite dilution of organic solutes in diethylene glycol and triethylene glycol from gas-liquid chromatography
rhoI	1124.70	kg/m3	293.15	Density and vapour pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water)
rhoI	1117.00	kg/m3	303.15	Density and vapour pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water)

rhoI	1109.20	kg/m3	313.15	Density and vapour pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water)
rhoI	1101.50	kg/m3	323.15	Density and vapour pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water)
rhoI	1093.70	kg/m3	333.15	Density and vapour pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water)
rhoI	1085.90	kg/m3	343.15	Density and vapour pressure of mixed-solvent desiccant systems (propylene glycol or dipropylene glycol or tripropylene glycol + magnesium chloride + water)
rhoI	1135.14	kg/m3	278.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhoI	1131.29	kg/m3	283.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range

rhoI	1127.43	kg/m3	288.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhoI	1123.56	kg/m3	293.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhoI	1119.69	kg/m3	298.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhoI	1115.81	kg/m3	303.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhoI	1111.92	kg/m3	308.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhoI	1108.03	kg/m3	313.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhoI	1104.13	kg/m3	318.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range

rhoI	1100.22	kg/m3	323.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhoI	1116.05	kg/m3	298.00	Removal of aromatic hydrocarbons from hydrocarbon mixture using glycols at 303.15 K and 333.15 K and atmospheric pressure: Experimental and calculated data by NRTL and UNIQUAC models
rhoI	1092.38	kg/m3	333.15	Acoustic and volumetric studies on (triethylene glycol + water) mixtures in a wide temperature range
rhoI	1124.60	kg/m3	293.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhoI	1120.80	kg/m3	298.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture

rhoI	1116.90	kg/m3	303.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhoI	1113.00	kg/m3	308.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhoI	1109.10	kg/m3	313.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhoI	1105.20	kg/m3	318.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhoI	1101.30	kg/m3	323.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture

rhoI	1097.40	kg/m3	328.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhoI	1093.50	kg/m3	333.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhoI	1089.60	kg/m3	338.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhoI	1085.60	kg/m3	343.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhoI	1123.48	kg/m3	293.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure

rhoI	1119.59	kg/m3	298.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhoI	1115.70	kg/m3	303.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhoI	1111.81	kg/m3	308.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhoI	1112.09	kg/m3	308.15	Excess molar enthalpies of binary mixtures containing ethylene glycols or poly(ethylene glycols) + ethyl alcohol at 308.15K and atmospheric pressure
rhoI	1124.60	kg/m3	293.15	Experimental and prediction of volumetric properties of aqueous solution of (allyltriphenylPhosphonium bromide - Triethylene glycol) deep eutectic solvents
rhoI	1120.80	kg/m3	298.15	Experimental and prediction of volumetric properties of aqueous solution of (allyltriphenylPhosphonium bromide - Triethylene glycol) deep eutectic solvents

rhoI	1113.00	kg/m3	308.15	Experimental and prediction of volumetric properties of aqueous solution of (allyltriphenylPhosphonium bromide - Triethylene glycol) deep eutectic solvents
rhoI	1105.20	kg/m3	318.15	Experimental and prediction of volumetric properties of aqueous solution of (allyltriphenylPhosphonium bromide - Triethylene glycol) deep eutectic solvents
rhoI	1097.40	kg/m3	328.15	Experimental and prediction of volumetric properties of aqueous solution of (allyltriphenylPhosphonium bromide - Triethylene glycol) deep eutectic solvents
rhoI	1085.60	kg/m3	343.15	Experimental and prediction of volumetric properties of aqueous solution of (allyltriphenylPhosphonium bromide - Triethylene glycol) deep eutectic solvents
rhoI	1128.60	kg/m3	288.15	Thermophysical properties of glycols and glymes
rhoI	1124.60	kg/m3	293.15	Thermophysical properties of glycols and glymes
rhoI	1120.70	kg/m3	298.15	Thermophysical properties of glycols and glymes
rhoI	1116.80	kg/m3	303.15	Thermophysical properties of glycols and glymes

rhoI	1112.90	kg/m3	308.15	Thermophysical properties of glycols and glymes	
rhoI	1109.00	kg/m3	313.15	Thermophysical properties of glycols and glymes	
rhoI	1105.10	kg/m3	318.15	Thermophysical properties of glycols and glymes	
rhoI	1101.20	kg/m3	323.15	Thermophysical properties of glycols and glymes	
rhoI	1097.30	kg/m3	328.15	Thermophysical properties of glycols and glymes	
rhoI	1093.40	kg/m3	333.15	Thermophysical properties of glycols and glymes	
rhoI	1089.50	kg/m3	338.15	Thermophysical properties of glycols and glymes	
rhoI	1085.60	kg/m3	343.15	Thermophysical properties of glycols and glymes	
rhoI	1081.70	kg/m3	348.15	Thermophysical properties of glycols and glymes	
rhoI	1077.80	kg/m3	353.15	Thermophysical properties of glycols and glymes	
rhoI	1073.80	kg/m3	358.15	Thermophysical properties of glycols and glymes	
rhoI	1069.80	kg/m3	363.15	Thermophysical properties of glycols and glymes	
rhoI	1124.50	kg/m3	293.15	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K	

rhoI	1061.90	kg/m3	373.15	Thermophysical properties of glycols and glymes	
rhoI	1131.30	kg/m3	283.15	Thermophysical properties of glycols and glymes	
rhoI	1127.40	kg/m3	288.15	Thermophysical properties of glycols and glymes	
rhoI	1123.50	kg/m3	293.15	Thermophysical properties of glycols and glymes	
rhoI	1119.70	kg/m3	298.15	Thermophysical properties of glycols and glymes	
rhoI	1115.80	kg/m3	303.15	Thermophysical properties of glycols and glymes	
rhoI	1111.90	kg/m3	308.15	Thermophysical properties of glycols and glymes	
rhoI	1108.00	kg/m3	313.15	Thermophysical properties of glycols and glymes	
rhoI	1100.20	kg/m3	323.15	Thermophysical properties of glycols and glymes	
rhoI	1092.40	kg/m3	333.15	Thermophysical properties of glycols and glymes	
rhoI	1084.50	kg/m3	343.15	Thermophysical properties of glycols and glymes	
rhoI	1112.10	kg/m3	308.15	Excess Molar Enthalpies of Binary Mixtures Containing Glycols or Polyglycols + Dimethyl Sulfoxide at 308.15 K	

rhoI	1119.78	kg/m3	298.15	Thermodynamic Study of Binary Mixtures Containing Glycols or Polyethylene Glycols + Benzyl Alcohol at 308.15 K
rhoI	1112.61	kg/m3	308.15	Thermodynamic Study of Binary Mixtures Containing Glycols or Polyethylene Glycols + Benzyl Alcohol at 308.15 K
rhoI	1119.78	kg/m3	298.15	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Glycols or Poly(Ethylene Glycols) and 2-Phenylethyl Alcohol at 308.15 K and Atmospheric Pressure
rhoI	1112.61	kg/m3	308.15	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Glycols or Poly(Ethylene Glycols) and 2-Phenylethyl Alcohol at 308.15 K and Atmospheric Pressure
rhoI	1112.59	kg/m3	308.50	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Ethers and Benzyl Alcohol at 308.15 K and Atmospheric Pressure

rhoI	1120.70	kg/m3	298.15	Isobaric Vapor-Liquid Equilibrium for Four Binary Systems of Ethane-1,2-diol, Butane-1,4-diol, 2-(2-Hydroxyethoxy)ethan-1-ol and 2-[2-(2-Hydroxyethoxy)ethoxy]ethanol at 10.0 kPa, 20.0 kPa and 40.0 kPa
rhoI	1116.50	kg/m3	303.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
rhoI	1108.90	kg/m3	313.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
rhoI	1101.10	kg/m3	323.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
rhoI	1093.40	kg/m3	333.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures

rhoI	1085.50	kg/m3	343.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
rhoI	1116.60	kg/m3	302.85	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhoI	1111.90	kg/m3	307.75	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhoI	1108.40	kg/m3	312.65	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhoI	1104.70	kg/m3	317.45	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhoI	1101.00	kg/m3	322.25	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K

rhoI	1097.90	kg/m3	327.05	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhoI	1093.50	kg/m3	332.15	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhoI	1086.10	kg/m3	341.45	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhoI	1123.20	kg/m3	293.35	Measurement and Correlation of Densities and Viscosities of Thiourea in Triglycol + Water at Temperatures from (302.85 to 341.45) K
rhoI	1065.90	kg/m3	368.15	Thermophysical properties of glycols and glymes
tcondI	0.19	W/m×K	298.10	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondI	0.19	W/m×K	308.20	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols

tcondl	0.19	W/m×K	318.40	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.19	W/m×K	328.40	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.19	W/m×K	338.40	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.94699e+01
Coeff. B	-8.61684e+03
Coeff. C	2.20480e+01
Temperature range (K), min.	427.16
Temperature range (K), max.	586.55

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C*\ln(T) + D*T^2$
Coeff. A	2.93684e+01
Coeff. B	-8.89710e+03
Coeff. C	-1.46752e+00
Coeff. D	2.12637e-06

Temperature range (K), min.	265.79
Temperature range (K), max.	700.00

Datasets

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
283.08	100.00	1131.7
283.08	1000.00	1132.4
283.08	2000.00	1132.8
283.08	5000.00	1134.1
283.08	7000.00	1134.9
283.08	10000.00	1136.2
283.08	12000.00	1137.1
283.08	16000.00	1138.8
283.08	20000.00	1140.5
283.08	25000.00	1142.5
283.08	30000.00	1144.5
283.08	35000.00	1146.5
283.08	40000.00	1148.4
283.08	45000.00	1150.2
283.08	50000.00	1152.1
283.08	55000.00	1154.0
283.08	60000.00	1155.8
283.08	65000.00	1157.6
283.08	70000.00	1159.4
283.08	75000.00	1161.0
283.08	80000.00	1162.8
283.08	85000.00	1164.5
283.08	90000.00	1166.1
283.08	95000.00	1167.7
293.14	100.00	1124.1
293.14	1000.00	1124.5
293.14	2000.00	1124.9
293.14	5000.00	1126.3
293.14	7000.00	1127.3
293.14	10000.00	1128.6
293.14	12000.00	1129.4

293.14	16000.00	1131.3
293.14	20000.00	1132.9
293.14	25000.00	1135.0
293.14	30000.00	1137.1
293.14	35000.00	1139.2
293.14	40000.00	1141.1
293.14	45000.00	1143.0
293.14	50000.00	1145.0
293.14	55000.00	1146.9
293.14	60000.00	1148.7
293.14	65000.00	1150.5
293.14	70000.00	1152.4
293.14	75000.00	1154.2
293.14	80000.00	1155.9
293.14	85000.00	1157.6
293.14	90000.00	1159.2
293.14	95000.00	1160.9
303.12	100.00	1116.2
303.12	1000.00	1116.6
303.12	2000.00	1117.1
303.12	5000.00	1118.5
303.12	7000.00	1119.5
303.12	10000.00	1120.9
303.12	12000.00	1121.8
303.12	16000.00	1123.6
303.12	20000.00	1125.4
303.12	25000.00	1127.6
303.12	30000.00	1129.7
303.12	35000.00	1131.8
303.12	40000.00	1133.9
303.12	45000.00	1135.9
303.12	50000.00	1137.9
303.12	55000.00	1139.9
303.12	60000.00	1141.8
303.12	65000.00	1143.7
303.12	70000.00	1145.5
303.12	75000.00	1147.3
303.12	80000.00	1149.1
303.12	85000.00	1150.8
303.12	90000.00	1152.6
303.12	95000.00	1154.2
313.18	100.00	1108.3
313.18	1000.00	1108.7
313.18	2000.00	1109.2

313.18	5000.00	1110.7
313.18	7000.00	1111.7
313.18	10000.00	1113.1
313.18	12000.00	1114.1
313.18	16000.00	1115.9
313.18	20000.00	1117.8
313.18	25000.00	1120.0
313.18	30000.00	1122.3
313.18	35000.00	1124.4
313.18	40000.00	1126.6
313.18	45000.00	1128.7
313.18	50000.00	1130.6
313.18	55000.00	1132.6
313.18	60000.00	1134.6
313.18	65000.00	1136.6
313.18	70000.00	1138.5
313.18	75000.00	1140.3
313.18	80000.00	1142.1
313.18	85000.00	1143.9
313.18	90000.00	1145.6
313.18	95000.00	1147.4
323.14	100.00	1100.5
323.14	1000.00	1101.0
323.14	2000.00	1101.5
323.14	5000.00	1103.0
323.14	7000.00	1104.1
323.14	10000.00	1105.5
323.14	12000.00	1106.5
323.14	16000.00	1108.4
323.14	20000.00	1110.3
323.14	25000.00	1112.6
323.14	30000.00	1114.9
323.14	35000.00	1117.1
323.14	40000.00	1119.4
323.14	45000.00	1121.5
323.14	50000.00	1123.7
323.14	55000.00	1125.7
323.14	60000.00	1127.7
323.14	65000.00	1129.7
323.14	70000.00	1131.7
323.14	75000.00	1133.5
323.14	80000.00	1135.4
323.14	85000.00	1137.3
323.14	90000.00	1139.0

323.14	95000.00	1140.8
333.10	100.00	1092.7
333.10	1000.00	1093.2
333.10	2000.00	1093.8
333.10	5000.00	1095.4
333.10	7000.00	1096.4
333.10	10000.00	1098.0
333.10	12000.00	1098.9
333.10	16000.00	1100.9
333.10	20000.00	1102.9
333.10	25000.00	1105.3
333.10	30000.00	1107.7
333.10	35000.00	1110.1
333.10	40000.00	1112.3
333.10	45000.00	1114.5
333.10	50000.00	1116.6
333.10	55000.00	1118.9
333.10	60000.00	1120.8
333.10	65000.00	1122.9
333.10	70000.00	1124.9
333.10	75000.00	1126.9
333.10	80000.00	1128.8
333.10	85000.00	1130.7
333.10	90000.00	1132.5
333.10	95000.00	1134.4
343.14	100.00	1084.7
343.14	1000.00	1085.3
343.14	2000.00	1086.0
343.14	5000.00	1087.6
343.14	7000.00	1088.6
343.14	10000.00	1090.2
343.14	12000.00	1091.3
343.14	16000.00	1093.4
343.14	20000.00	1095.4
343.14	25000.00	1097.9
343.14	30000.00	1100.4
343.14	35000.00	1102.8
343.14	40000.00	1105.1
343.14	45000.00	1107.4
343.14	50000.00	1109.6
343.14	55000.00	1111.9
343.14	60000.00	1114.0
343.14	65000.00	1116.1
343.14	70000.00	1118.1

343.14	75000.00	1120.1
343.14	80000.00	1122.1
343.14	85000.00	1124.1
343.14	90000.00	1126.0
343.14	95000.00	1128.0
353.10	100.00	1077.0
353.10	1000.00	1076.9
353.10	2000.00	1078.0
353.10	5000.00	1079.8
353.10	7000.00	1080.9
353.10	10000.00	1082.6
353.10	12000.00	1083.6
353.10	16000.00	1085.7
353.10	20000.00	1088.0
353.10	25000.00	1090.5
353.10	30000.00	1093.2
353.10	35000.00	1095.5
353.10	40000.00	1098.0
353.10	45000.00	1100.3
353.10	50000.00	1102.6
353.10	55000.00	1104.9
353.10	60000.00	1107.3
353.10	65000.00	1109.1
353.10	70000.00	1111.5
353.10	75000.00	1113.3
353.10	80000.00	1115.6
353.10	85000.00	1117.4
353.10	90000.00	1119.5
353.10	95000.00	1121.3
363.16	100.00	1068.9
363.16	1000.00	1069.4
363.16	2000.00	1070.1
363.16	5000.00	1071.8
363.16	7000.00	1073.0
363.16	10000.00	1074.6
363.16	12000.00	1075.8
363.16	16000.00	1078.2
363.16	20000.00	1080.3
363.16	25000.00	1082.9
363.16	30000.00	1085.6
363.16	35000.00	1088.1
363.16	40000.00	1090.6
363.16	45000.00	1093.0
363.16	50000.00	1095.4

363.16	55000.00	1097.8
363.16	60000.00	1100.1
363.16	65000.00	1102.3
363.16	70000.00	1104.5
363.16	75000.00	1106.6
363.16	80000.00	1108.7
363.16	85000.00	1110.7
363.16	90000.00	1112.8
363.16	95000.00	1114.8

Reference

<https://www.doi.org/10.1016/j.fluid.2017.01.003>

Temperature, K	Pressure, kPa	Mass density, kg/m3
283.15	100.00	1130.8
283.15	100.00	1130.8
283.15	660.00	1131.0
283.15	1150.00	1131.2
283.15	1570.00	1131.4
283.15	2090.00	1131.6
283.15	3090.00	1132.0
283.15	5060.00	1132.9
283.15	6940.00	1133.6
283.15	10020.00	1134.9
283.15	14850.00	1136.9
283.15	19830.00	1138.9
283.15	24700.00	1140.8
283.15	29600.00	1142.7
283.15	34510.00	1144.6
283.15	39360.00	1146.4
283.15	44290.00	1148.2
283.15	49180.00	1150.0
283.15	54110.00	1151.7
283.15	58970.00	1153.4
283.15	63860.00	1155.1
283.15	68790.00	1156.8
293.15	100.00	1122.9
293.15	100.00	1122.9
293.15	640.00	1123.1
293.15	1090.00	1123.4
293.15	1600.00	1123.6
293.15	2140.00	1123.8
293.15	3080.00	1124.2
293.15	5030.00	1125.1

293.15	7010.00	1125.9
293.15	9950.00	1127.2
293.15	14850.00	1129.3
293.15	19770.00	1131.3
293.15	24660.00	1133.3
293.15	29510.00	1135.2
293.15	34610.00	1137.2
293.15	39370.00	1139.1
293.15	44320.00	1141.0
293.15	49130.00	1142.8
293.15	54050.00	1144.6
293.15	59060.00	1146.4
293.15	63780.00	1148.0
303.15	100.00	1115.2
303.15	100.00	1115.1
303.15	630.00	1115.4
303.15	1130.00	1115.6
303.15	1620.00	1115.9
303.15	2140.00	1116.1
303.15	3070.00	1116.5
303.15	5080.00	1117.4
303.15	6960.00	1118.3
303.15	9960.00	1119.6
303.15	14840.00	1121.7
303.15	19750.00	1123.8
303.15	24670.00	1125.9
303.15	29570.00	1127.9
303.15	34500.00	1129.9
303.15	39360.00	1131.9
303.15	44300.00	1133.8
303.15	49190.00	1135.7
303.15	54090.00	1137.6
303.15	58850.00	1139.3
303.15	63890.00	1141.2
303.15	68750.00	1142.9
313.15	100.00	1107.4
313.15	100.00	1107.4
313.15	670.00	1107.6
313.15	1130.00	1107.9
313.15	1600.00	1108.1
313.15	2080.00	1108.3
313.15	3100.00	1108.8
313.15	5030.00	1109.7
313.15	7010.00	1110.6

313.15	10010.00	1112.0
313.15	14880.00	1114.2
313.15	19750.00	1116.4
313.15	24680.00	1118.6
313.15	29560.00	1120.6
313.15	34510.00	1122.7
313.15	39330.00	1124.7
313.15	44290.00	1126.7
313.15	49180.00	1128.6
313.15	54160.00	1130.6
313.15	59000.00	1132.4
313.15	63910.00	1134.3
313.15	68840.00	1136.0
323.15	100.00	1099.6
323.15	100.00	1099.5
323.15	590.00	1099.8
323.15	1140.00	1100.0
323.15	1600.00	1100.3
323.15	2080.00	1100.5
323.15	3020.00	1101.0
323.15	5050.00	1101.9
323.15	7000.00	1102.9
323.15	9970.00	1104.3
323.15	14870.00	1106.7
323.15	19780.00	1108.9
323.15	24700.00	1111.2
323.15	29650.00	1113.3
323.15	34470.00	1115.4
323.15	39340.00	1117.5
323.15	44250.00	1119.6
323.15	49170.00	1121.6
323.15	54080.00	1123.5
323.15	58970.00	1125.5
323.15	63800.00	1127.3
323.15	68780.00	1129.2
333.15	100.00	1091.7
333.15	100.00	1091.7
333.15	660.00	1092.0
333.15	1110.00	1092.2
333.15	1600.00	1092.5
333.15	2100.00	1092.7
333.15	3070.00	1093.2
333.15	5060.00	1094.2
333.15	6980.00	1095.2

333.15	9970.00	1096.6
333.15	14840.00	1099.0
333.15	19660.00	1101.3
333.15	24670.00	1103.7
333.15	29610.00	1106.0
333.15	34530.00	1108.2
333.15	39400.00	1110.3
333.15	44280.00	1112.5
333.15	49110.00	1114.5
333.15	54040.00	1116.5
333.15	59060.00	1118.6
333.15	63830.00	1120.5
333.15	68770.00	1122.4
343.15	100.00	1083.9
343.15	100.00	1083.9
343.15	640.00	1084.2
343.15	1120.00	1084.4
343.15	1600.00	1084.7
343.15	2110.00	1084.9
343.15	3040.00	1085.5
343.15	5040.00	1086.6
343.15	6960.00	1087.5
343.15	9920.00	1089.0
343.15	14810.00	1091.6
343.15	19680.00	1093.9
343.15	24620.00	1096.4
343.15	29580.00	1098.7
343.15	34460.00	1101.0
343.15	39370.00	1103.3
343.15	44240.00	1105.4
343.15	49160.00	1107.6
343.15	54020.00	1109.7
343.15	58940.00	1111.7
343.15	63890.00	1113.8
343.15	68680.00	1115.7
353.15	100.00	1076.0
353.15	100.00	1076.0
353.15	650.00	1076.3
353.15	1100.00	1076.5
353.15	1550.00	1076.7
353.15	2100.00	1077.1
353.15	3050.00	1077.6
353.15	5040.00	1078.6
353.15	7010.00	1079.8

353.15	9960.00	1081.3
353.15	14810.00	1084.0
353.15	19780.00	1086.5
353.15	24610.00	1089.0
353.15	29560.00	1091.9
353.15	34450.00	1093.8
353.15	39370.00	1096.1
353.15	44270.00	1098.4
353.15	49200.00	1100.6
353.15	54090.00	1102.8
353.15	59010.00	1104.9
353.15	63820.00	1107.0
353.15	68800.00	1109.0
363.15	100.00	1068.1
363.15	100.00	1068.0
363.15	660.00	1068.4
363.15	1120.00	1068.7
363.15	1560.00	1068.9
363.15	2130.00	1069.2
363.15	3050.00	1069.8
363.15	5090.00	1070.9
363.15	6990.00	1072.0
363.15	9980.00	1073.7
363.15	14880.00	1076.4
363.15	19680.00	1079.0
363.15	24720.00	1081.7
363.15	29630.00	1084.2
363.15	34490.00	1086.6
363.15	39430.00	1089.0
363.15	44200.00	1091.4
363.15	49240.00	1093.7
363.15	54100.00	1095.9
363.15	59010.00	1098.1
363.15	63880.00	1100.2
363.15	68830.00	1102.3

Reference

<https://www.doi.org/10.1016/j.fluid.2018.09.026>

Viscosity, Pa*s

Temperature, K - Liquid

Pressure, kPa - Liquid

Viscosity, Pa*s - Liquid

298.15	98.00	0.0368200
298.15	49030.00	0.0552300
298.15	98060.00	0.0802900
298.15	147100.00	0.1144000
298.15	196130.00	0.1606000
298.15	245160.00	0.2218000
312.96	98.00	0.0190300
313.05	49030.00	0.0274200
313.10	98060.00	0.0382800
313.18	147100.00	0.0525000
313.25	196130.00	0.0706800
313.26	245160.00	0.0939900
334.96	98.00	0.0090020
335.11	49030.00	0.0124500
335.14	98060.00	0.0167000
335.20	147100.00	0.0220300
335.25	196130.00	0.0284800
335.26	245160.00	0.0363700
349.25	98.00	0.0059450
349.94	196130.00	0.0175300
349.98	49030.00	0.0080610
349.98	98060.00	0.0106600
349.99	245160.00	0.0218400
350.03	147100.00	0.0137500
364.44	98.00	0.0041310
364.44	49030.00	0.0055370
364.72	98060.00	0.0071490
365.03	147100.00	0.0090210
365.07	196130.00	0.0112400
365.20	245160.00	0.0138000
413.73	98.00	0.0016790
414.00	49030.00	0.0021790
414.15	98060.00	0.0028360
414.27	147100.00	0.0033200
414.30	196130.00	0.0039950
414.43	245160.00	0.0044850
462.25	98.00	0.0009970
462.26	49030.00	0.0013030
462.32	98060.00	0.0016140
462.41	147100.00	0.0019410
462.45	196130.00	0.0023000
462.58	245160.00	0.0026780

Pressure, kPa	Temperature, K	Viscosity, Pa*s
101.30	308.15	0.0238400
Reference		https://www.doi.org/10.1021/je020178w

Joule-Thomson coefficient, K/kPa

Temperature, K - Liquid	Pressure, kPa - Liquid	Joule-Thomson coefficient, K/kPa - Liquid
293.10	7000.00	-0.0004
Reference		https://www.doi.org/10.1016/j.fluid.2011.03.011

Sources

Molar heat capacities of some aqueous
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Excess enthalpy and excess entropy
The MD dynamic interactions Study of
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Amino-ionic Paddings for
Diethylene Glycol + Nitrogen and
Triethylene Glycol + Nitrogen
Nonhydrocarbon Systems Ethylene
Glycol + Water
Mixture between 290 K and 450 K:
Vapor-Liquid Equilibria of Water +
Triethylene Glycol (TEG) and Water +
Triethylene Glycol (TEG) and Water +
Experimental and predicted refractive
index properties in ternary mixtures of
Resorcinol and aromatic hydrocarbons
from hydrocarbon mixture using
glycols at 303.15 K and 308.15 K and
properties for binary mixtures of same
and water at 303.15 K and 308.15 K
UNMOL database at 308.15 K:

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tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
vc:	Critical Volume

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