

# Acetone

Other names:	(CH <sub>3</sub> ) <sub>2</sub> CO 2-PROPANONE Chevron acetone DIMETHYL KETONE Dimethylformaldehyde Dimethylketal KETONE PROPANE Ketone, dimethyl- Methyl ketone NSC 135802 Propan-2-one Propanone Pyroacetic ether Rcra waste number U002 Sasetone UN 1090 «beta»-Ketopropane Â«betaÂ»-Ketopropane
Inchi:	InChI=1S/C3H6O/c1-3(2)4/h1-2H3
InchiKey:	CSCPPACGZOOCGX-UHFFFAOYSA-N
Formula:	C <sub>3</sub> H <sub>6</sub> O
SMILES:	CC(C)=O
Mol. weight [g/mol]:	58.08
CAS:	67-64-1

## Physical Properties

Property code	Value	Unit	Source
af	0.3040		KDB
affp	814.30	kJ/mol	NIST Webbook
affp	811.50 ± 3.40	kJ/mol	NIST Webbook
affp	811.50 ± 3.40	kJ/mol	NIST Webbook
affp	815.20	kJ/mol	NIST Webbook
affp	812.00	kJ/mol	NIST Webbook
affp	812.60 ± 0.20	kJ/mol	NIST Webbook
aigt	738.15	K	KDB
basg	782.10	kJ/mol	NIST Webbook
basg	782.20	kJ/mol	NIST Webbook

basg	782.10 ± 1.50	kJ/mol	NIST Webbook
basg	784.70	kJ/mol	NIST Webbook
basg	782.10 ± 1.50	kJ/mol	NIST Webbook
basg	782.00 ± 0.20	kJ/mol	NIST Webbook
chg	-1821.40 ± 0.84	kJ/mol	NIST Webbook
chl	-1772.00	kJ/mol	NIST Webbook
chl	-1804.20	kJ/mol	NIST Webbook
dm	2.90	debye	KDB
dvisc	0.0003121	Paxs	Densities and Viscosities of Binary Liquid Mixtures of Trichloroethylene and Tetrachloroethylene with Some Polar and Nonpolar Solvents
dvisc	0.0003000	Paxs	Densities and Viscosities of 1-Butyl-3-methylimidazolium Tetrafluoroborate + Molecular Solvent Binary Mixtures
ea	0.00	eV	NIST Webbook
fl	2.60	% in Air	KDB
flu	12.80	% in Air	KDB
fpc	257.59	K	KDB
fpo	255.37	K	KDB
gf	-153.20	kJ/mol	KDB
gyrad	2.7400		KDB
hf	-217.10 ± 0.50	kJ/mol	NIST Webbook
hf	-217.70	kJ/mol	KDB
hf	-217.50 ± 0.67	kJ/mol	NIST Webbook
hf	-216.40	kJ/mol	NIST Webbook
hf	-218.50 ± 0.59	kJ/mol	NIST Webbook
hfl	-249.40 ± 0.63	kJ/mol	NIST Webbook
hfus	5.12	kJ/mol	Joback Method
hvap	31.27	kJ/mol	NIST Webbook
hvap	29.70 ± 0.00	kJ/mol	NIST Webbook
hvap	31.30	kJ/mol	NIST Webbook
ie	9.71	eV	NIST Webbook
ie	9.68	eV	NIST Webbook
ie	9.71	eV	NIST Webbook
ie	9.71 ± 0.01	eV	NIST Webbook
ie	9.71	eV	NIST Webbook
ie	9.72	eV	NIST Webbook
ie	9.74	eV	NIST Webbook
ie	9.71 ± 0.01	eV	NIST Webbook
ie	9.74 ± 0.03	eV	NIST Webbook
ie	9.68	eV	NIST Webbook

ie	9.71 ± 0.01	eV	NIST Webbook
ie	9.70 ± 0.10	eV	NIST Webbook
ie	9.68 ± 0.02	eV	NIST Webbook
ie	9.67	eV	NIST Webbook
ie	9.71 ± 0.03	eV	NIST Webbook
ie	9.71 ± 0.03	eV	NIST Webbook
ie	9.69 ± 0.01	eV	NIST Webbook
ie	9.71	eV	NIST Webbook
ie	9.80	eV	NIST Webbook
ie	9.72	eV	NIST Webbook
ie	9.71 ± 0.02	eV	NIST Webbook
ie	9.71 ± 0.01	eV	NIST Webbook
ie	9.71 ± 0.03	eV	NIST Webbook
ie	9.71 ± 0.01	eV	NIST Webbook
ie	9.71	eV	NIST Webbook
ie	9.75 ± 0.03	eV	NIST Webbook
ie	9.68	eV	NIST Webbook
ie	9.69 ± 0.01	eV	NIST Webbook
ie	9.70	eV	NIST Webbook
ie	9.70 ± 0.01	eV	NIST Webbook
ie	9.72	eV	NIST Webbook
ie	9.50	eV	NIST Webbook
ie	9.70	eV	NIST Webbook
ie	9.70 ± 0.00	eV	NIST Webbook
ie	9.71	eV	NIST Webbook
log10ws	-0.36		Crippen Method
logp	0.595		Crippen Method
mcvol	54.700	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=1)		KDB
pc	4700.00	kPa	KDB
rhoc	234.06 ± 1.51	kg/m3	NIST Webbook
rhoc	272.97 ± 1.16	kg/m3	NIST Webbook
rhoc	268.91 ± 2.90	kg/m3	NIST Webbook
rhoc	252.06 ± 1.74	kg/m3	NIST Webbook
rhoc	278.20 ± 9.87	kg/m3	NIST Webbook
rinpol	472.00		NIST Webbook
rinpol	487.00		NIST Webbook
rinpol	474.00		NIST Webbook
rinpol	474.00		NIST Webbook
rinpol	500.00		NIST Webbook
rinpol	509.00		NIST Webbook
rinpol	512.00		NIST Webbook
rinpol	459.00		NIST Webbook

rinpol	471.00	NIST Webbook
rinpol	450.00	NIST Webbook
rinpol	476.00	NIST Webbook
rinpol	501.00	NIST Webbook
rinpol	470.00	NIST Webbook
rinpol	470.00	NIST Webbook
rinpol	450.00	NIST Webbook
rinpol	497.00	NIST Webbook
rinpol	500.00	NIST Webbook
rinpol	500.00	NIST Webbook
rinpol	460.00	NIST Webbook
rinpol	473.00	NIST Webbook
rinpol	473.00	NIST Webbook
rinpol	473.00	NIST Webbook
rinpol	465.00	NIST Webbook
rinpol	460.00	NIST Webbook
rinpol	469.00	NIST Webbook
rinpol	491.00	NIST Webbook
rinpol	474.00	NIST Webbook
rinpol	484.00	NIST Webbook
rinpol	468.00	NIST Webbook
rinpol	469.00	NIST Webbook
rinpol	478.00	NIST Webbook
rinpol	468.00	NIST Webbook
rinpol	503.00	NIST Webbook
rinpol	503.00	NIST Webbook
rinpol	471.00	NIST Webbook
rinpol	470.00	NIST Webbook
rinpol	479.00	NIST Webbook
rinpol	502.00	NIST Webbook
rinpol	477.55	NIST Webbook
rinpol	470.23	NIST Webbook
rinpol	469.50	NIST Webbook
rinpol	469.00	NIST Webbook
rinpol	478.00	NIST Webbook
rinpol	475.00	NIST Webbook
rinpol	465.00	NIST Webbook
rinpol	443.00	NIST Webbook
rinpol	447.00	NIST Webbook
rinpol	476.60	NIST Webbook
rinpol	487.00	NIST Webbook
rinpol	502.00	NIST Webbook
rinpol	502.00	NIST Webbook
rinpol	472.00	NIST Webbook

rinpol	496.00	NIST Webbook
rinpol	496.00	NIST Webbook
rinpol	500.00	NIST Webbook
rinpol	479.00	NIST Webbook
rinpol	466.00	NIST Webbook
rinpol	468.00	NIST Webbook
rinpol	466.00	NIST Webbook
rinpol	470.00	NIST Webbook
rinpol	472.00	NIST Webbook
rinpol	473.00	NIST Webbook
rinpol	472.00	NIST Webbook
rinpol	480.00	NIST Webbook
rinpol	471.00	NIST Webbook
rinpol	466.00	NIST Webbook
rinpol	468.00	NIST Webbook
rinpol	474.00	NIST Webbook
rinpol	471.00	NIST Webbook
rinpol	488.60	NIST Webbook
rinpol	500.00	NIST Webbook
rinpol	481.00	NIST Webbook
rinpol	475.30	NIST Webbook
rinpol	500.00	NIST Webbook
rinpol	503.00	NIST Webbook
rinpol	470.00	NIST Webbook
rinpol	510.00	NIST Webbook
rinpol	477.55	NIST Webbook
rinpol	503.00	NIST Webbook
rinpol	439.00	NIST Webbook
rinpol	447.00	NIST Webbook
rinpol	450.00	NIST Webbook
rinpol	475.00	NIST Webbook
rinpol	450.00	NIST Webbook
rinpol	472.00	NIST Webbook
rinpol	443.00	NIST Webbook
rinpol	459.00	NIST Webbook
rinpol	439.00	NIST Webbook
rinpol	444.00	NIST Webbook
rinpol	465.00	NIST Webbook
rinpol	443.50	NIST Webbook
rinpol	450.00	NIST Webbook
rinpol	437.00	NIST Webbook
rinpol	437.00	NIST Webbook
rinpol	475.00	NIST Webbook
rinpol	497.00	NIST Webbook

rinpol	485.00	NIST Webbook
rinpol	488.20	NIST Webbook
rinpol	488.70	NIST Webbook
rinpol	478.00	NIST Webbook
rinpol	477.00	NIST Webbook
rinpol	484.00	NIST Webbook
rinpol	481.00	NIST Webbook
rinpol	469.00	NIST Webbook
rinpol	469.00	NIST Webbook
rinpol	470.00	NIST Webbook
rinpol	470.00	NIST Webbook
rinpol	469.41	NIST Webbook
rinpol	469.28	NIST Webbook
rinpol	469.50	NIST Webbook
rinpol	469.67	NIST Webbook
rinpol	470.10	NIST Webbook
rinpol	470.70	NIST Webbook
rinpol	470.90	NIST Webbook
rinpol	470.23	NIST Webbook
rinpol	481.00	NIST Webbook
rinpol	500.00	NIST Webbook
rinpol	441.00	NIST Webbook
ripol	846.00	NIST Webbook
ripol	823.00	NIST Webbook
ripol	814.00	NIST Webbook
ripol	825.00	NIST Webbook
ripol	798.00	NIST Webbook
ripol	845.00	NIST Webbook
ripol	814.00	NIST Webbook
ripol	832.00	NIST Webbook
ripol	816.00	NIST Webbook
ripol	820.00	NIST Webbook
ripol	816.00	NIST Webbook
ripol	811.00	NIST Webbook
ripol	825.00	NIST Webbook
ripol	828.00	NIST Webbook
ripol	827.00	NIST Webbook
ripol	827.00	NIST Webbook
ripol	810.00	NIST Webbook
ripol	820.00	NIST Webbook
ripol	823.00	NIST Webbook
ripol	811.00	NIST Webbook
ripol	812.00	NIST Webbook
ripol	821.00	NIST Webbook

ripol	841.00	NIST Webbook
ripol	832.00	NIST Webbook
ripol	834.00	NIST Webbook
ripol	808.00	NIST Webbook
ripol	808.00	NIST Webbook
ripol	830.00	NIST Webbook
ripol	812.00	NIST Webbook
ripol	805.00	NIST Webbook
ripol	813.00	NIST Webbook
ripol	819.00	NIST Webbook
ripol	814.00	NIST Webbook
ripol	813.00	NIST Webbook
ripol	822.00	NIST Webbook
ripol	816.00	NIST Webbook
ripol	811.00	NIST Webbook
ripol	818.00	NIST Webbook
ripol	813.00	NIST Webbook
ripol	802.00	NIST Webbook
ripol	814.00	NIST Webbook
ripol	821.30	NIST Webbook
ripol	814.00	NIST Webbook
ripol	842.00	NIST Webbook
ripol	834.00	NIST Webbook
ripol	813.00	NIST Webbook
ripol	809.00	NIST Webbook
ripol	794.00	NIST Webbook
ripol	818.00	NIST Webbook
ripol	820.00	NIST Webbook
ripol	814.00	NIST Webbook
ripol	814.00	NIST Webbook
ripol	814.00	NIST Webbook
ripol	813.00	NIST Webbook
ripol	821.00	NIST Webbook
ripol	824.00	NIST Webbook
ripol	842.00	NIST Webbook
ripol	785.00	NIST Webbook
ripol	847.00	NIST Webbook
ripol	832.00	NIST Webbook
ripol	840.80	NIST Webbook
ripol	837.50	NIST Webbook
ripol	835.00	NIST Webbook
ripol	843.50	NIST Webbook
ripol	820.00	NIST Webbook
ripol	810.00	NIST Webbook

ripol	810.00		NIST Webbook
ripol	822.00		NIST Webbook
ripol	810.00		NIST Webbook
ripol	822.00		NIST Webbook
ripol	854.00		NIST Webbook
ripol	816.00		NIST Webbook
ripol	800.00		NIST Webbook
ripol	845.00		NIST Webbook
ripol	814.00		NIST Webbook
ripol	814.00		NIST Webbook
ripol	775.00		NIST Webbook
ripol	821.00		NIST Webbook
ripol	841.00		NIST Webbook
ripol	836.00		NIST Webbook
ripol	816.00		NIST Webbook
ripol	813.00		NIST Webbook
ripol	815.00		NIST Webbook
ripol	814.00		NIST Webbook
ripol	819.00		NIST Webbook
ripol	788.00		NIST Webbook
ripol	823.00		NIST Webbook
ripol	847.00		NIST Webbook
ripol	835.00		NIST Webbook
ripol	810.00		NIST Webbook
ripol	824.00		NIST Webbook
ripol	815.00		NIST Webbook
ripol	820.00		NIST Webbook
ripol	821.00		NIST Webbook
ripol	820.00		NIST Webbook
ripol	816.00		NIST Webbook
ripol	810.00		NIST Webbook
ripol	847.00		NIST Webbook
ripol	819.00		NIST Webbook
ripol	810.00		NIST Webbook
ripol	813.00		NIST Webbook
ripol	830.00		NIST Webbook
ripol	809.00		NIST Webbook
ripol	821.30		NIST Webbook
ripol	811.00		NIST Webbook
ripol	794.00		NIST Webbook
ripol	821.00		NIST Webbook
ripol	818.00		NIST Webbook
sl	200.00	J/molxK	NIST Webbook
sl	200.40	J/molxK	NIST Webbook



sl	217.60	J/mol×K	NIST Webbook
sl	220.50	J/mol×K	NIST Webbook
tb	329.25 ± 0.20	K	NIST Webbook
tb	329.20	K	KDB
tb	329.45 ± 1.00	K	NIST Webbook
tb	329.30	K	Vapor-liquid equilibrium in the production of the ionic liquid, 1-hexyl-3-methylimidazolium bromide ([HmIm][Br]), in acetone
tb	329.45 ± 1.00	K	NIST Webbook
tb	330.85 ± 1.00	K	NIST Webbook
tb	329.50 ± 0.50	K	NIST Webbook
tb	329.50 ± 1.00	K	NIST Webbook
tb	329.26	K	Isobaric vapor-liquid equilibrium for acetone + methanol system containing different ionic liquids at 101.3 kPa
tb	328.90 ± 1.00	K	NIST Webbook
tb	329.56	K	Isobaric vapour-liquid equilibrium measurements and extractive distillation process for the azeotrope of (N,N-dimethylisopropylamine + acetone)
tb	329.33	K	Isobaric Vapor-Liquid Equilibrium Data for the Acetone + Hexamethyl Disiloxane + Ethyl Acetate Ternary System at 101.3 kPa: Determination and Correlation
tb	329.35	K	Isobaric Vapor-Liquid Equilibrium of Acetone + Methanol System in the Presence of Calcium Bromide
tb	329.27	K	Measurement of Isobaric Vapor - Liquid Equilibria of Dimethyl Carbonate with Acetone, 2-Butanone and 2-Pentanone at 101.3 kPa and Density and Speed of Sound at 298.15 K
tb	329.55 ± 1.00	K	NIST Webbook
tb	330.15 ± 1.00	K	NIST Webbook
tb	329.55 ± 1.00	K	NIST Webbook
tb	329.40 ± 1.00	K	NIST Webbook
tb	329.15 ± 1.00	K	NIST Webbook
tb	329.34 ± 0.50	K	NIST Webbook
tb	330.20 ± 1.00	K	NIST Webbook
tb	329.25 ± 0.30	K	NIST Webbook

tb	329.30 ± 1.00	K	NIST Webbook
tb	329.30 ± 0.50	K	NIST Webbook
tb	329.25 ± 0.30	K	NIST Webbook
tb	329.40 ± 1.00	K	NIST Webbook
tb	329.30 ± 0.50	K	NIST Webbook
tb	329.70 ± 1.50	K	NIST Webbook
tb	329.65 ± 1.00	K	NIST Webbook
tb	329.15 ± 1.00	K	NIST Webbook
tb	329.30 ± 0.30	K	NIST Webbook
tb	329.65 ± 1.00	K	NIST Webbook
tb	329.45 ± 0.50	K	NIST Webbook
tb	329.35 ± 1.00	K	NIST Webbook
tb	329.65 ± 1.00	K	NIST Webbook
tb	329.25 ± 1.00	K	NIST Webbook
tb	329.48 ± 1.00	K	NIST Webbook
tb	329.20 ± 0.30	K	NIST Webbook
tb	329.30 ± 1.00	K	NIST Webbook
tb	329.23 ± 0.10	K	NIST Webbook
tb	329.22 ± 0.20	K	NIST Webbook
tb	329.35 ± 1.00	K	NIST Webbook
tb	329.15 ± 1.00	K	NIST Webbook
tb	329.65 ± 1.00	K	NIST Webbook
tb	329.32 ± 0.30	K	NIST Webbook
tb	329.50 ± 0.50	K	NIST Webbook
tb	329.17 ± 0.20	K	NIST Webbook
tb	329.35 ± 0.20	K	NIST Webbook
tb	329.30 ± 0.40	K	NIST Webbook
tb	329.35 ± 0.30	K	NIST Webbook
tb	329.45 ± 1.00	K	NIST Webbook
tb	329.35 ± 0.30	K	NIST Webbook
tb	329.35 ± 0.30	K	NIST Webbook
tb	330.00 ± 1.00	K	NIST Webbook
tb	329.39 ± 0.50	K	NIST Webbook
tb	329.40 ± 0.20	K	NIST Webbook
tb	328.95 ± 1.00	K	NIST Webbook
tb	328.75 ± 1.00	K	NIST Webbook
tb	329.65 ± 0.30	K	NIST Webbook
tb	329.55 ± 1.00	K	NIST Webbook
tb	329.30 ± 1.00	K	NIST Webbook
tb	328.57 ± 1.00	K	NIST Webbook
tb	329.15 ± 2.00	K	NIST Webbook
tb	328.85 ± 1.00	K	NIST Webbook
tb	331.15 ± 3.00	K	NIST Webbook
tb	329.26 ± 0.10	K	NIST Webbook

tb	329.15 ± 1.00	K	NIST Webbook
tb	329.20 ± 1.00	K	NIST Webbook
tb	329.65 ± 1.00	K	NIST Webbook
tb	329.25 ± 1.00	K	NIST Webbook
tb	329.75 ± 0.50	K	NIST Webbook
tb	329.20 ± 0.20	K	NIST Webbook
tb	329.25 ± 1.00	K	NIST Webbook
tb	329.40 ± 1.00	K	NIST Webbook
tb	329.30 ± 0.50	K	NIST Webbook
tb	329.27 ± 0.50	K	NIST Webbook
tb	323.40 ± 0.30	K	NIST Webbook
tb	329.15 ± 1.00	K	NIST Webbook
tb	329.30 ± 0.50	K	NIST Webbook
tb	329.65 ± 1.00	K	NIST Webbook
tb	329.35 ± 0.50	K	NIST Webbook
tb	328.65 ± 1.00	K	NIST Webbook
tb	329.65 ± 0.50	K	NIST Webbook
tb	329.30 ± 0.50	K	NIST Webbook
tb	329.50 ± 0.50	K	NIST Webbook
tb	329.28 ± 0.30	K	NIST Webbook
tb	329.33 ± 0.20	K	NIST Webbook
tb	329.35 ± 0.20	K	NIST Webbook
tb	329.35 ± 0.50	K	NIST Webbook
tb	329.35 ± 0.50	K	NIST Webbook
tb	329.35 ± 0.50	K	NIST Webbook
tb	329.25 ± 0.50	K	NIST Webbook
tb	329.15 ± 1.00	K	NIST Webbook
tb	329.28 ± 0.15	K	NIST Webbook
tb	329.35 ± 1.00	K	NIST Webbook
tb	329.25 ± 0.50	K	NIST Webbook
tb	328.90 ± 0.40	K	NIST Webbook
tb	329.75 ± 1.00	K	NIST Webbook
tb	329.25 ± 1.00	K	NIST Webbook
tb	329.33 ± 0.20	K	NIST Webbook
tb	326.15 ± 1.00	K	NIST Webbook
tb	329.15 ± 1.00	K	NIST Webbook
tb	329.26 ± 0.50	K	NIST Webbook
tb	329.25 ± 0.50	K	NIST Webbook
tb	330.95 ± 1.00	K	NIST Webbook
tb	329.26 ± 0.30	K	NIST Webbook
tb	329.25 ± 0.30	K	NIST Webbook
tb	329.21 ± 0.10	K	NIST Webbook
tb	329.25 ± 0.30	K	NIST Webbook
tb	329.25 ± 0.50	K	NIST Webbook

tb	329.40 ± 0.40	K	NIST Webbook
tb	329.30 ± 0.30	K	NIST Webbook
tb	329.30 ± 0.20	K	NIST Webbook
tb	329.00 ± 1.00	K	NIST Webbook
tb	329.15 ± 0.30	K	NIST Webbook
tb	329.40 ± 0.20	K	NIST Webbook
tb	329.38 ± 0.30	K	NIST Webbook
tb	329.25 ± 0.15	K	NIST Webbook
tb	329.25	K	NIST Webbook
tb	329.30 ± 0.06	K	NIST Webbook
tb	329.30 ± 0.20	K	NIST Webbook
tb	329.00 ± 0.20	K	NIST Webbook
tb	329.26 ± 0.30	K	NIST Webbook
tb	329.25 ± 0.05	K	NIST Webbook
tb	329.23 ± 0.05	K	NIST Webbook
tb	329.47 ± 0.50	K	NIST Webbook
tb	329.25 ± 0.30	K	NIST Webbook
tb	329.40 ± 0.40	K	NIST Webbook
tb	329.45 ± 0.30	K	NIST Webbook
tb	329.30	K	NIST Webbook
tb	329.21 ± 0.04	K	NIST Webbook
tb	329.00	K	NIST Webbook
tb	329.45 ± 0.30	K	NIST Webbook
tb	329.45 ± 0.15	K	NIST Webbook
tb	329.30 ± 0.20	K	NIST Webbook
tb	330.15 ± 0.50	K	NIST Webbook
tb	329.37	K	Vapor Liquid Equilibrium for the 1,1,1-Trifluorotrichloroethane + Sulfuryl Chloride System at 101.3 kPa
tb	329.65 ± 1.00	K	NIST Webbook
tc	508.10	K	KDB
tf	178.30	K	KDB
tt	177.60 ± 0.30	K	NIST Webbook
tt	176.60 ± 0.15	K	NIST Webbook
tt	178.50 ± 0.30	K	NIST Webbook
tt	177.60 ± 0.20	K	NIST Webbook
vc	0.209	m3/kmol	KDB
zc	0.2325190		KDB
zra	0.25		KDB

# Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	80.58 ± 0.81	J/mol×K	332.60	NIST Webbook
cpg	92.93 ± 0.19	J/mol×K	405.20	NIST Webbook
cpg	80.96 ± 0.81	J/mol×K	334.00	NIST Webbook
cpg	81.50 ± 0.16	J/mol×K	338.20	NIST Webbook
cpg	83.35 ± 0.83	J/mol×K	347.80	NIST Webbook
cpg	83.39 ± 0.83	J/mol×K	348.00	NIST Webbook
cpg	87.03 ± 0.87	J/mol×K	363.00	NIST Webbook
cpg	87.19 ± 0.17	J/mol×K	371.20	NIST Webbook
cpg	87.53 ± 0.88	J/mol×K	372.30	NIST Webbook
cpg	89.24 ± 0.89	J/mol×K	378.00	NIST Webbook
cpg	91.84 ± 0.92	J/mol×K	393.00	NIST Webbook
cpg	94.18 ± 0.94	J/mol×K	408.00	NIST Webbook
cpg	93.30	J/mol×K	410.00	NIST Webbook
cpg	96.80 ± 1.90	J/mol×K	422.60	NIST Webbook
cpg	99.40 ± 2.00	J/mol×K	428.00	NIST Webbook
cpg	100.50 ± 2.00	J/mol×K	438.00	NIST Webbook
cpg	98.66 ± 0.20	J/mol×K	439.20	NIST Webbook
cpl	123.80	J/mol×K	298.15	NIST Webbook
cpl	133.90	J/mol×K	298.00	NIST Webbook
cpl	121.30	J/mol×K	283.00	NIST Webbook
cpl	125.90	J/mol×K	293.20	NIST Webbook
cpl	123.80	J/mol×K	298.40	NIST Webbook
cpl	124.30	J/mol×K	260.00	NIST Webbook
cpl	124.68	J/mol×K	296.99	NIST Webbook
cpl	124.70	J/mol×K	298.00	NIST Webbook
cpl	124.70	J/mol×K	298.00	NIST Webbook
cpl	128.40	J/mol×K	302.40	NIST Webbook
cpl	128.24	J/mol×K	298.00	NIST Webbook
cpl	125.56	J/mol×K	298.20	NIST Webbook
cpl	126.30	J/mol×K	293.00	NIST Webbook
cpl	129.70	J/mol×K	298.00	NIST Webbook
cpl	125.90	J/mol×K	298.15	NIST Webbook
cpl	123.80	J/mol×K	298.15	NIST Webbook
cpl	123.80	J/mol×K	298.15	NIST Webbook
cpl	126.60	J/mol×K	298.15	NIST Webbook
cpl	126.60	J/mol×K	298.15	NIST Webbook
cpl	124.70	J/mol×K	289.40	NIST Webbook
cpl	125.45	J/mol×K	298.15	NIST Webbook
cps	96.00	J/mol×K	173.00	NIST Webbook

dvisc	0.0003027	Paxs	298.15	Excess parameter studies on the binary mixtures of toluene with ketones at different temperatures
dvisc	0.0002939	Paxs	308.15	Density and Viscosity of (2,2-Dichloro-N,N-di-2-propenylacetamide + Acetone) and (2,2-Dichloro-N,N-di-2-propenylacetamide + Ethanol) at T = (278.15 to 313.15) K
dvisc	0.0002839	Paxs	313.15	Density and Viscosity of (2,2-Dichloro-N,N-di-2-propenylacetamide + Acetone) and (2,2-Dichloro-N,N-di-2-propenylacetamide + Ethanol) at T = (278.15 to 313.15) K
dvisc	0.0002920	Paxs	303.15	Physical properties of the binary systems methylcyclopentane with ketones (acetone, butanone and 2-pentanone) at T = (293.15, 298.15, and 303.15) K. New UNIFAC-VISCO interaction parameters
dvisc	0.0002809	Paxs	308.15	Excess parameter studies on the binary mixtures of toluene with ketones at different temperatures
dvisc	0.0003200	Paxs	293.15	Dynamic Viscosities of the Binary Systems Cyclohexane and Cyclopentane with Acetone, Butanone, or 2-Pentanone at Three Temperatures T ) (293.15, 298.15, and 303.15) K

dvisc	0.0003060	Paxs	298.15	Dynamic Viscosities of the Binary Systems Cyclohexane and Cyclopentane with Acetone, Butanone, or 2-Pentanone at Three Temperatures T ) (293.15, 298.15, and 303.15) K
dvisc	0.0003200	Paxs	293.15	Physical properties of the binary systems methylcyclopentane with ketones (acetone, butanone and 2-pentanone) at T = (293.15, 298.15, and 303.15) K. New UNIFAC-VISCO interaction parameters
dvisc	0.0003086	Paxs	303.15	Density and Viscosity of (2,2-Dichloro-N,N-di-2-propenylacetamide + Acetone) and (2,2-Dichloro-N,N-di-2-propenylacetamide + Ethanol) at T = (278.15 to 313.15) K
dvisc	0.0003212	Paxs	298.15	Density and Viscosity of (2,2-Dichloro-N,N-di-2-propenylacetamide + Acetone) and (2,2-Dichloro-N,N-di-2-propenylacetamide + Ethanol) at T = (278.15 to 313.15) K
dvisc	0.0003339	Paxs	293.15	Density and Viscosity of (2,2-Dichloro-N,N-di-2-propenylacetamide + Acetone) and (2,2-Dichloro-N,N-di-2-propenylacetamide + Ethanol) at T = (278.15 to 313.15) K
dvisc	0.0003511	Paxs	288.15	Density and Viscosity of (2,2-Dichloro-N,N-di-2-propenylacetamide + Acetone) and (2,2-Dichloro-N,N-di-2-propenylacetamide + Ethanol) at T = (278.15 to 313.15) K

dvisc	0.0003657	Paxs	283.15	Density and Viscosity of (2,2-Dichloro-N,N-di-2-propenylacetamide + Acetone) and (2,2-Dichloro-N,N-di-2-propenylacetamide + Ethanol) at T = (278.15 to 313.15) K
dvisc	0.0002920	Paxs	303.15	Dynamic Viscosities of the Binary Systems Cyclohexane and Cyclopentane with Acetone, Butanone, or 2-Pentanone at Three Temperatures T ) (293.15, 298.15, and 303.15) K
dvisc	0.0003849	Paxs	278.15	Density and Viscosity of (2,2-Dichloro-N,N-di-2-propenylacetamide + Acetone) and (2,2-Dichloro-N,N-di-2-propenylacetamide + Ethanol) at T = (278.15 to 313.15) K
dvisc	0.0002809	Paxs	308.15	Density and Viscosity of Ketones with Toluene at Different Temperatures and at Atmospheric Pressure
dvisc	0.0003060	Paxs	298.15	Physical properties of the binary systems methylcyclopentane with ketones (acetone, butanone and 2-pentanone) at T = (293.15, 298.15, and 303.15) K. New UNIFAC-VISCO interaction parameters
dvisc	0.0002918	Paxs	303.15	Density and Viscosity of Ketones with Toluene at Different Temperatures and at Atmospheric Pressure



dvisc	0.0002918	Paxs	303.15	Excess parameter studies on the binary mixtures of toluene with ketones at different temperatures
dvisc	0.0003027	Paxs	298.15	Density and Viscosity of Ketones with Toluene at Different Temperatures and at Atmospheric Pressure
hfust	5.69	kJ/mol	177.60	NIST Webbook
hfust	4.77	kJ/mol	178.50	NIST Webbook
hfust	5.72	kJ/mol	176.60	NIST Webbook
hfust	5.72	kJ/mol	176.60	NIST Webbook
hfust	5.69	kJ/mol	177.60	NIST Webbook
hfust	5.71	kJ/mol	176.62	NIST Webbook
hvapt	30.70	kJ/mol	271.50	NIST Webbook
hvapt	32.10	kJ/mol	271.50	NIST Webbook
hvapt	35.00	kJ/mol	271.50	NIST Webbook
hvapt	29.09	kJ/mol	338.00	NIST Webbook
hvapt	31.10	kJ/mol	319.50	NIST Webbook
hvapt	32.60	kJ/mol	285.50	NIST Webbook
hvapt	29.10	kJ/mol	329.30	NIST Webbook
hvapt	31.80	kJ/mol	319.00	NIST Webbook
hvapt	9.20	kJ/mol	498.00	NIST Webbook
hvapt	15.30	kJ/mol	473.00	NIST Webbook
hvapt	21.70	kJ/mol	423.00	NIST Webbook
hvapt	26.10	kJ/mol	373.00	NIST Webbook
hvapt	31.90	kJ/mol	307.00	NIST Webbook
hvapt	32.70	kJ/mol	294.50	NIST Webbook
hvapt	32.80	kJ/mol	305.00	NIST Webbook
hvapt	29.70	kJ/mol	482.50	NIST Webbook
hvapt	30.60	kJ/mol	351.00	NIST Webbook
hvapt	33.80	kJ/mol	236.00	NIST Webbook
hvapt	32.90	kJ/mol	210.50	NIST Webbook
hvapt	29.90	kJ/mol	408.50	NIST Webbook
hvapt	32.10	kJ/mol	308.00	NIST Webbook
hvapt	29.50	kJ/mol	419.00	NIST Webbook
hvapt	29.12	kJ/mol	329.40	KDB

pvap	57.96	kPa	314.00	Isobaric vapor liquid equilibria for acetone + methanol + lithium nitrate at 100 kPa
pvap	60.29	kPa	314.76	Vapor-Liquid Equilibrium for Binary Systems of Diacetyl with Methanol and Acetone
pvap	64.95	kPa	317.00	Isobaric vapor liquid equilibria for acetone + methanol + lithium nitrate at 100 kPa
pvap	72.60	kPa	320.00	Isobaric vapor liquid equilibria for acetone + methanol + lithium nitrate at 100 kPa
pvap	80.96	kPa	323.00	Isobaric vapor liquid equilibria for acetone + methanol + lithium nitrate at 100 kPa
pvap	90.08	kPa	326.00	Isobaric vapor liquid equilibria for acetone + methanol + lithium nitrate at 100 kPa
pvap	100.00	kPa	329.00	Isobaric vapor liquid equilibria for acetone + methanol + lithium nitrate at 100 kPa
pvap	110.78	kPa	332.00	Isobaric vapor liquid equilibria for acetone + methanol + lithium nitrate at 100 kPa
pvap	122.47	kPa	335.00	Isobaric vapor liquid equilibria for acetone + methanol + lithium nitrate at 100 kPa
pvap	101.33	kPa	329.30	Vapor-liquid equilibrium in the production of the ionic liquid, 1-hexyl-3-methylimidazolium bromide ([HmIm][Br]), in acetone

pvap	101.30	kPa	329.26	Isobaric vapor-liquid equilibrium for acetone + methanol system containing different ionic liquids at 101.3 kPa
pvap	115.70	kPa	333.15	Thermodynamics of binary mixtures of N-methyl-2-pyrrolidinone and ketone. Experimental results and modelling of the solid-liquid equilibrium and vapour-liquid equilibrium. The Modified UNIFAC (Do) model characterization
pvap	101.30	kPa	329.56	Isobaric vapour-liquid equilibrium measurements and extractive distillation process for the azeotrope of (N,N-dimethylisopropylamine + acetone)
pvap	96.15	kPa	327.90	Vapor Liquid Equilibrium Data for Binary Mixtures of Acetic Acid + Anisole, Acetone + Anisole, and Isopropanol + Anisole at Pressure 96.15 kPa
pvap	68.20	kPa	318.15	Isothermal Vapor-Liquid Equilibria for Binary Mixtures of Methyl Nonafluorobutyl Ether + Acetone, Cyclopentyl Methyl Ether, Ethyl Acetate, n-Heptane, Methanol, and Toluene

pvap	101.30	kPa	329.33	Isobaric Vapor-Liquid Equilibrium Data for the Acetone + Hexamethyl Disiloxane + Ethyl Acetate Ternary System at 101.3 kPa: Determination and Correlation
pvap	101.00	kPa	329.35	Isobaric Vapor-Liquid Equilibrium of Acetone + Methanol System in the Presence of Calcium Bromide
pvap	297.10	kPa	364.51	Vapor Liquid Equilibrium for Six Binary Systems of C4-Hydrocarbons + 2-Propanone
pvap	70.07	kPa	318.77	Vapor Liquid Equilibrium for Binary Systems of 2,3-Pentanedione with Diacetyl and Acetone
pvap	65.08	kPa	316.80	Vapor Liquid Equilibrium for Binary Systems of 2,3-Pentanedione with Diacetyl and Acetone
pvap	60.29	kPa	314.76	Vapor Liquid Equilibrium for Binary Systems of 2,3-Pentanedione with Diacetyl and Acetone
pvap	55.29	kPa	312.52	Vapor Liquid Equilibrium for Binary Systems of 2,3-Pentanedione with Diacetyl and Acetone
pvap	50.40	kPa	310.08	Vapor Liquid Equilibrium for Binary Systems of 2,3-Pentanedione with Diacetyl and Acetone

pvap	45.21	kPa	307.33	Vapor Liquid Equilibrium for Binary Systems of 2,3-Pentanedione with Diacetyl and Acetone	
pvap	35.22	kPa	301.25	Vapor Liquid Equilibrium for Binary Systems of 2,3-Pentanedione with Diacetyl and Acetone	
pvap	30.23	kPa	297.67	Vapor Liquid Equilibrium for Binary Systems of 2,3-Pentanedione with Diacetyl and Acetone	
pvap	101.30	kPa	329.37	Vapor Liquid Equilibrium for the 1,1,1-Trifluorotrichloroethane + Sulfuryl Chloride System at 101.3 kPa	
pvap	100.00	kPa	329.00	1-Ethyl-3-methylimidazolium Dicyanamide as a Very Efficient Entrainer for the Extractive Distillation of the Acetone + Methanol System	
pvap	100.00	kPa	329.00	Influence of Some Ionic Liquids Containing the Trifluoromethanesulfonate Anion on the Vapor Liquid Equilibria of the Acetone + Methanol System	
pvap	81.65	kPa	323.15	Vapor-Liquid Equilibrium for Binary Systems of Diacetyl with Methanol and Acetone	
pvap	70.07	kPa	318.77	Vapor-Liquid Equilibrium for Binary Systems of Diacetyl with Methanol and Acetone	

pvap	65.08	kPa	316.80	Vapor-Liquid Equilibrium for Binary Systems of Diacetyl with Methanol and Acetone	
pvap	294.30	kPa	364.51	Vapor Liquid Equilibrium for Six Binary Systems of C4-Hydrocarbons + 2-Propanone	
pvap	56.64	kPa	313.15	Vapor-Liquid Equilibrium for Binary Systems of Diacetyl with Methanol and Acetone	
pvap	55.29	kPa	312.52	Vapor-Liquid Equilibrium for Binary Systems of Diacetyl with Methanol and Acetone	
pvap	50.40	kPa	310.08	Vapor-Liquid Equilibrium for Binary Systems of Diacetyl with Methanol and Acetone	
pvap	45.21	kPa	307.33	Vapor-Liquid Equilibrium for Binary Systems of Diacetyl with Methanol and Acetone	
pvap	40.00	kPa	304.37	Vapor-Liquid Equilibrium for Binary Systems of Diacetyl with Methanol and Acetone	
pvap	38.04	kPa	303.15	Vapor-Liquid Equilibrium for Binary Systems of Diacetyl with Methanol and Acetone	
pvap	35.22	kPa	301.25	Vapor-Liquid Equilibrium for Binary Systems of Diacetyl with Methanol and Acetone	
pvap	30.23	kPa	297.66	Vapor-Liquid Equilibrium for Binary Systems of Diacetyl with Methanol and Acetone	

pvap	302.56	kPa	365.43	Vapor Liquid Equilibrium for Six Binary Systems of C4-Hydrocarbons + 2-Propanone
pvap	296.80	kPa	364.52	Vapor Liquid Equilibrium for Six Binary Systems of C4-Hydrocarbons + 2-Propanone
pvap	296.40	kPa	364.51	Vapor Liquid Equilibrium for Six Binary Systems of C4-Hydrocarbons + 2-Propanone
pvap	135.11	kPa	338.00	Isobaric vapor liquid equilibria for acetone + methanol + lithium nitrate at 100 kPa
rfi	1.35860		293.15	Isobaric Vapor Liquid Equilibrium for Nine Binary Systems of Cracking C5 Fraction at 250 kPa
rfi	1.35890		293.15	Isothermal and Isobaric Vapor-Liquid Equilibria of the Ternary System of 2,2-Dimethoxypropane + Acetone + Methanol
rfi	1.35057		308.15	Densities, Refractive indices and Viscosities for Binary and Ternary Mixtures of Acetone, Ethanol and 2,2,4-Trimethylpentane at T = (288.15, 298.15, and 308.15) K

rfi	1.35605	298.15	Densities, Refractive indices and Viscosities for Binary and Ternary Mixtures of Acetone, Ethanol and 2,2,4-Trimethylpentane at T = (288.15, 298.15, and 308.15) K
rfi	1.36152	288.15	Densities, Refractive indices and Viscosities for Binary and Ternary Mixtures of Acetone, Ethanol and 2,2,4-Trimethylpentane at T = (288.15, 298.15, and 308.15) K
rfi	1.35553	298.15	Quaternary, Ternary and Binary LLE Measurements for 2-Methoxy-2-methylbutane + Furfural + Acetic Acid + Water at Temperatures between 298 and 341 K
rfi	1.35553	298.15	Quaternary, Ternary, and Binary LLE Measurements for 2-Methoxy-2-methylpropane + Furfural + Acetic Acid + Water at Temperatures between 298 and 307 K
rfi	1.35553	298.15	Ternary and Binary LLE Measurements for Solvent (4-Methyl-2-pentanone and 2-Methyl-2-butanol) + Furfural + Water between 298 and 401 K
rfi	1.35900	293.15	Solubilities of Some Phosphaspirocyclic Compounds in Selected Solvents



rfi	1.35620	298.15	Solubility of $\alpha$ -Carotene in Binary Solvents Formed by Some Hydrocarbons with 2,5,8-Trioxanonane, 2-Propanone, and Cyclohexanone
rfi	1.35550	298.00	Quaternary and ternary LLE measurements for solvent (2-methyltetrahydrofuran and cyclopentyl methyl ether) + furfural + acetic acid + water between 298 and 343 K
rfi	1.35900	293.15	Solubilities of (2,5-Dihydroxyphenyl)diphenyl Phosphine Oxide in Selected Solvents
rfi	1.35550	298.15	Ternary and binary LLE measurements for solvent (2-methyltetrahydrofuran and cyclopentyl methyl ether) + furfural + water between 298 and 343 K
rfi	1.34491	318.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.35054	308.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K

rfi	1.35597	298.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.36146	288.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.35566	298.15	Properties of ionic liquid HMIMPF6 with carbonates, ketones and alkyl acetates
rfi	1.35880	293.15	Isothermal vapour-liquid equilibrium data for the binary systems 2-propanone + (2-butanol or propanoic acid)
rfi	1.35732	298.15	Phase equilibria and interfacial tensions in the systems methyl tert-butyl ether + acetone + cyclohexane, methyl tert-butyl ether + acetone and methyl tert-butyl ether + cyclohexane
rfi	1.35732	298.15	Vapor liquid equilibria and interfacial tensions for the ternary system acetone + 2,2-oxybis[propane] + cyclohexane and its constituent binary systems

rfi	1.35597		298.15	Isobaric vapor liquid equilibria for mixtures of acetone, ethanol, and 2,2,4-trimethylpentane at 101.3 kPa
rfi	1.35900		293.15	Solubilities of Phosphorus-Containing Compounds in Selected Solvents
rfi	1.35820		298.15	Isobaric Vapor Liquid Equilibria for Binary Systems of Acetone + Isopropenyl Acetate, 2-Butanone + Isopropenyl Acetate, and Isopropenyl Acetate + Acetylacetone at 101.3 kPa
rfi	1.35900		293.15	Solubilities of 3,9-Dimethyl-3,9-dioxide-2,4,8,10-tetraoxa-3,9-diphosphaspiro[5.5]undecane in Selected Solvents
rfi	1.35880		293.15	Solubilities of Methyl-diphenylphosphine Oxide in Selected Solvents
rfi	1.35600		298.15	Physical properties and their corresponding changes of mixing for the ternary mixture acetone + n-hexane + water at 298.15K
rfi	1.35900		293.15	Solubilities of 2-(6-Oxido-6H-dibenz[c,e][1,2]oxaphosphorin-6-yl)-1,4-dihydroxy Phenylene in the Selected Solvents
rhoI	785.00	kg/m3	298.15	Vapor Liquid Equilibrium Data for 2,3-Pentanedione + (Acetaldehyde or Acetone) at (100, 150, and 200) kPa

rhoI	790.31	kg/m3	293.15	Excess Molar Enthalpies for Binary Mixtures of Ethanol + Acetone, + Octane, + Cyclohexane and 1-Propanol + Acetone, + Octane, + Heptane at 323.15
rhoI	801.67	kg/m3	283.15	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	767.00	kg/m3	313.15	Thermophysical approach to understand the nature of molecular interactions and structural factor between methyl isobutyl ketone and organic solvents mixtures
rhoI	779.00	kg/m3	303.15	Thermophysical approach to understand the nature of molecular interactions and structural factor between methyl isobutyl ketone and organic solvents mixtures
rhoI	790.00	kg/m3	293.15	Thermophysical approach to understand the nature of molecular interactions and structural factor between methyl isobutyl ketone and organic solvents mixtures

rhoI	778.63	kg/m3	303.15	Thermodynamics of amide + ketone mixtures. 1. Volumetric, speed of sound and refractive index data for N,N-dimethylformamide + 2-alkanone systems at several temperatures
rhoI	784.43	kg/m3	298.15	Thermodynamics of amide + ketone mixtures. 1. Volumetric, speed of sound and refractive index data for N,N-dimethylformamide + 2-alkanone systems at several temperatures
rhoI	790.19	kg/m3	293.15	Thermodynamics of amide + ketone mixtures. 1. Volumetric, speed of sound and refractive index data for N,N-dimethylformamide + 2-alkanone systems at several temperatures
rhoI	785.10	kg/m3	298.15	Measurement and correlation of solubility and solution thermodynamics of 1,3-dimethylurea in different solvents from T = (288.15 to 328.15) K
rhoI	778.70	kg/m3	303.20	Ionic liquid 1-hexyl-3-methylimidazolium hexafluorophosphate, an efficient solvent for extraction of acetone from aqueous solutions

rhoI	796.04	kg/m3	288.15	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	790.36	kg/m3	293.15	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	790.66	kg/m3	293.20	Ionic liquid 1-hexyl-3-methylimidazolium hexafluorophosphate, an efficient solvent for extraction of acetone from aqueous solutions
rhoI	790.21	kg/m3	293.15	(Liquid + liquid) equilibria for (water + 1-propanol or acetone + .beta.-citronellol) at different temperatures
rhoI	783.80	kg/m3	298.15	Solubility and solution thermodynamics of sorbic acid in eight pure organic solvents
rhoI	785.32	kg/m3	298.15	Extraction desulfurization process of fuels with ionic liquids
rhoI	785.32	kg/m3	298.15	Effect of the alkyl side chain of the 1-alkylpiperidinium-based ionic liquids on desulfurization of fuels

rhoI	785.23	kg/m3	298.15	Separation of sulfur compounds from alkanes with 1-alkylcyanopyridinium-based ionic liquids
rhoI	773.07	kg/m3	308.15	Thermodynamic properties of binary mixtures of the ionic liquid [emim][BF4] with acetone and dimethylsulphoxide
rhoI	784.40	kg/m3	298.20	Ionic liquid 1-hexyl-3-methylimidazolium hexafluorophosphate, an efficient solvent for extraction of acetone from aqueous solutions
rhoI	784.40	kg/m3	298.15	Thermodynamic properties of binary mixtures of the ionic liquid [emim][BF4] with acetone and dimethylsulphoxide
rhoI	789.99	kg/m3	293.15	Thermodynamic properties of binary mixtures of the ionic liquid [emim][BF4] with acetone and dimethylsulphoxide
rhoI	784.24	kg/m3	298.15	Apparent molar volumes and compressibilities of tetrabutyl-ammonium bromide in organic solvents
rhoI	784.23	kg/m3	298.15	Density and speed of sound of lithium bromide with organic solvents: Measurement and correlation
rhoI	784.65	kg/m3	298.15	Excess molar enthalpies and volumes of binary mixtures of nonafluorobutylmethylether with ketones at T = 298.15 K
rhoI	784.50	kg/m3	293.15	(Vapour + liquid) equilibria for (2-ethoxypropene + acetone) and (2-ethoxypropene + butanone)

rhoI	761.26	kg/m3	318.15	Densities, viscosities, and refractive indices of binary and ternary mixtures of methanol, acetone, and chloroform at temperatures from (298.15-318.15) K and ambient pressure
rhoI	766.95	kg/m3	313.15	Densities, viscosities, and refractive indices of binary and ternary mixtures of methanol, acetone, and chloroform at temperatures from (298.15-318.15) K and ambient pressure
rhoI	784.64	kg/m3	298.15	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	773.07	kg/m3	308.15	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure



rhoI	773.08	kg/m3	308.15	Densities, viscosities, and refractive indices of binary and ternary mixtures of methanol, acetone, and chloroform at temperatures from (298.15-318.15) K and ambient pressure
rhoI	767.21	kg/m3	313.14	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	761.29	kg/m3	318.14	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	755.31	kg/m3	323.14	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
rhoI	784.39	kg/m3	298.15	Excess Molar Volumes and Surface Tensions of Xylene with Acetone or 2-Butanone at 298.15 K

rhoI	785.09	kg/m3	298.15	Thermodynamics of Ketone + Amine Mixtures. Part VIII. Molar Excess Enthalpies at 298.15 K for n-Alkanone + Aniline or + N-Methylaniline Systems
rhoI	784.30	kg/m3	293.15	Liquid Liquid Equilibrium for the Ternary System Acetone Oxime Methyl Ether Acetone Water
rhoI	784.30	kg/m3	298.15	Phase equilibrium study of binary and ternary mixtures of ionic liquids + acetone + methanol
rhoI	778.66	kg/m3	303.15	Densities, viscosities, and refractive indices of binary and ternary mixtures of methanol, acetone, and chloroform at temperatures from (298.15-318.15) K and ambient pressure
rhoI	785.23	kg/m3	298.15	Separation of pyridine from heptane with tricyanomethanide-based ionic liquids
rhoI	785.09	kg/m3	298.15	Thermodynamics of ketone + amine mixtures. Part X. Excess molarenthalpies at 298.15 K for N,N,N-triethylamine + 2-alkanone systems.Characterization of tertiary amine + 2-alkanone, and ofamino-ketone + n-alkane mixtures in terms of DISQUAC

rhoI	785.09	kg/m3	298.15	Thermodynamics of ketone + amine mixtures. Part IX. Excess molar enthalpies at 298.15K for dipropylamine, or dibutylamine + 2-alkanone systems and modeling of linear or aromatic amine + 2-alkanone mixtures in terms of DISQUAC and ERAS
rhoI	790.00	kg/m3	293.00	KDB
rhoI	786.77	kg/m3	298.15	Separation of ethylbenzene/styrene systems using ionic liquids in ternary LLE
rhoI	783.81	kg/m3	298.15	Partial Molar Volumes of Butyltriethylammonium Iodide in Single Nonaqueous Solvents at 298.15 K
rhoI	766.90	kg/m3	313.15	Density, Speed of Sound, and Derived Thermodynamic Properties of Ionic Liquids [EMIM]+[BETI]- or ([EMIM]+[CH <sub>3</sub> (OCH <sub>2</sub> CH <sub>2</sub> ) <sub>2</sub> OSO <sub>3</sub> ]- + Methanol or + Acetone) at T = (298.15 or 303.15 or 313.15) K
rhoI	778.40	kg/m3	303.15	Density, Speed of Sound, and Derived Thermodynamic Properties of Ionic Liquids [EMIM]+[BETI]- or ([EMIM]+[CH <sub>3</sub> (OCH <sub>2</sub> CH <sub>2</sub> ) <sub>2</sub> OSO <sub>3</sub> ]- + Methanol or + Acetone) at T = (298.15 or 303.15 or 313.15) K

rhoI	784.10	kg/m3	298.15	Density, Speed of Sound, and Derived Thermodynamic Properties of Ionic Liquids [EMIM]+[BETI]- or ([EMIM]+[CH3(OCH2CH2)2OSO3]- + Methanol or + Acetone) at T = (298.15 or 303.15 or 313.15) K
rhoI	784.41	kg/m3	298.15	Densities, viscosities, and refractive indices of binary and ternary mixtures of methanol, acetone, and chloroform at temperatures from (298.15-318.15) K and ambient pressure
rhoI	778.87	kg/m3	303.15	Thermodynamic properties of binary mixtures of the ionic liquid [emim][BF4] with acetone and dimethylsulphoxide
rhoI	778.88	kg/m3	303.14	Experimental Densities and Excess Volumes for Binary Mixtures Containing Propionic Acid, Acetone and Water from 283.15 K to 323.15 K at Atmospheric Pressure
sfust	26.70	J/molxK	178.50	NIST Webbook
sfust	32.00	J/molxK	177.60	NIST Webbook
sfust	32.36	J/molxK	176.62	NIST Webbook
sfust	32.03	J/molxK	177.60	NIST Webbook
speedsl	1162.00	m/s	298.15	Vapor liquid equilibria for systems of diethyl carbonate and ketones and determination of group interaction parameters for the UNIFAC and ASOG methods

srf	0.02	N/m	328.15	Surface Tension of the Ternary System Water + Acetone + Toluene
srf	0.02	N/m	308.15	Surface Tension of the Ternary System Water + Acetone + Toluene
srf	0.02	N/m	298.15	Surface Tension of the Ternary System Water + Acetone + Toluene
srf	0.02	N/m	288.15	Surface Tension of the Ternary System Water + Acetone + Toluene
srf	0.02	N/m	327.88	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	317.86	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	307.86	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	297.82	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	287.81	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	298.20	KDB
srf	0.02	N/m	318.15	Surface Tension of the Ternary System Water + Acetone + Toluene
srf	0.02	N/m	293.15	Investigation of Surface Properties and Solubility of 1-Vinyl-3-alkyl/Esterimidazolium Halide Ionic Liquids by Density Functional Methods

# Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbrp	329.30	K	2.70	NIST Webbook

## Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.48340e+01
Coeff. B	-3.02945e+03
Coeff. C	-3.26710e+01
Temperature range (K), min.	240.93
Temperature range (K), max.	508.10

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C*\ln(T) + D*T^2$
Coeff. A	6.69693e+01
Coeff. B	-5.78459e+03
Coeff. C	-7.85881e+00
Coeff. D	7.10496e-06
Temperature range (K), min.	178.45
Temperature range (K), max.	508.20

## Datasets

### Viscosity, Pa\*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
303.15	101.30	0.0002974

**Speed of sound, m/s**

Temperature, K - Liquid	Pressure, kPa - Liquid	Speed of sound, m/s - Liquid
265.67	102.00	1298.93
265.67	504.00	1301.09
265.67	750.00	1302.5
265.67	1003.00	1303.56
265.67	1255.00	1304.92
265.67	1501.00	1306.29
265.67	2007.00	1308.73
265.67	2506.00	1311.28
265.67	3005.00	1313.79
265.67	4004.00	1318.59
265.67	5004.00	1323.31
265.67	6005.00	1328.01
265.67	8002.00	1338.69
265.67	10001.00	1349.81
265.67	12001.00	1358.7
265.67	14003.00	1366.48
265.67	16050.00	1375.48
265.67	18001.00	1384.77
265.67	20003.00	1394.13
265.67	23001.00	1407.08
265.67	27004.00	1425.32
265.67	31003.00	1439.78
265.67	34997.00	1455.17
265.67	39999.00	1476.05
265.67	45002.00	1494.61
265.67	49999.00	1511.6
265.67	55001.00	1528.77
265.67	60002.00	1548.05
265.67	65000.00	1564.17
265.67	18001.00	1384.54
273.16	102.00	1264.48
273.16	504.00	1266.57
273.16	750.00	1267.96
273.16	1003.00	1269.39
273.16	1255.00	1270.74

273.16	1501.00	1272.23
273.16	2007.00	1275.12
273.16	2506.00	1277.93
273.16	3005.00	1281.1
273.16	4004.00	1287.23
273.16	5004.00	1291.97
273.16	6005.00	1296.6
273.16	8002.00	1306.58
273.16	10001.00	1316.19
273.16	12001.00	1325.58
273.16	14003.00	1335.9
273.16	16005.00	1346.87
273.16	18001.00	1355.99
273.16	20003.00	1363.63
273.16	23001.00	1376.52
273.16	27004.00	1394.61
273.16	31003.00	1412.24
273.16	34997.00	1428.86
273.16	39999.00	1446.67
273.16	45002.00	1467.44
273.16	49999.00	1485.84
273.16	55001.00	1504.31
273.16	60002.00	1520.08
273.16	65000.00	1538.71
273.16	3005.00	1281.19
273.16	4004.00	1286.78
273.16	5004.00	1292.02
280.74	75.00	1233.63
280.74	504.00	1234.94
280.74	750.00	1236.39
280.74	1003.00	1237.85
280.74	1255.00	1239.22
280.74	1501.00	1240.59
280.74	2007.00	1243.75
280.74	2506.00	1247.03
280.74	3005.00	1249.76
280.74	4004.00	1255.13
280.74	5004.00	1259.87
280.74	6005.00	1264.8
280.74	8002.00	1275.79
280.74	10001.00	1286.82
280.74	12001.00	1296.79
280.74	14003.00	1306.71
280.74	16005.00	1316.23



280.74	18001.00	1325.46
280.74	20003.00	1335.09
280.74	23001.00	1350.8
280.74	27004.00	1366.99
280.74	31003.00	1384.26
280.74	34997.00	1401.32
280.74	39999.00	1423.56
280.74	45002.00	1441.37
280.74	49999.00	1461.28
280.74	55001.00	1480.44
280.74	60002.00	1498.97
280.74	65000.00	1514.56
280.74	75.00	1232.04
280.74	23001.00	1350.8
280.74	39999.00	1423.74
280.74	45002.00	1441.37
280.74	60002.00	1498.91
280.74	65000.00	1514.63
288.23	109.00	1199.01
288.23	504.00	1201.24
288.23	750.00	1202.57
288.23	1003.00	1204.2
288.23	1255.00	1205.54
288.23	1501.00	1206.97
288.23	2007.00	1209.92
288.23	2506.00	1212.8
288.23	3005.00	1215.61
288.23	4004.00	1221.35
288.23	5004.00	1227.14
288.23	6005.00	1232.71
288.23	8002.00	1244.39
288.23	10001.00	1255.4
288.23	12001.00	1265.22
288.23	14003.00	1275.63
288.23	16005.00	1286.61
288.23	18001.00	1296.18
288.23	20003.00	1305.89
288.23	23001.00	1319.61
288.23	27004.00	1339.05
288.23	31003.00	1357.37
288.23	34997.00	1373.83
288.23	39999.00	1395.08
288.23	45002.00	1416.1
288.23	49999.00	1435.37

288.23	55001.00	1453.97
288.23	60002.00	1473.72
288.23	65000.00	1492.08
298.23	109.00	1153.69
298.23	504.00	1156.23
298.23	750.00	1157.82
298.23	1003.00	1159.5
298.23	1255.00	1161.14
298.23	1501.00	1162.71
298.23	2007.00	1165.65
298.23	2506.00	1168.6
298.23	3005.00	1171.49
298.23	4004.00	1177.4
298.23	5004.00	1182.9
298.23	6005.00	1189.6
298.23	8002.00	1201.45
298.23	10001.00	1212.8
298.23	12001.00	1223.83
298.23	14003.00	1234.83
298.23	16005.00	1246.18
298.23	18001.00	1256.46
298.23	20003.00	1265.92
298.23	23001.00	1281.93
298.23	27004.00	1301.17
298.23	31003.00	1319.28
298.23	34997.00	1337.9
298.23	39999.00	1359.25
298.23	45002.00	1380.44
298.23	49999.00	1400.61
298.23	55001.00	1421.32
298.23	60002.00	1439.68
298.23	65000.00	1458.59
308.22	109.00	1107.74
308.22	504.00	1110.52
308.22	750.00	1112.35
308.22	1003.00	1114.01
308.22	1255.00	1115.75
308.22	1501.00	1117.34
308.22	2007.00	1120.69
308.22	2506.00	1123.91
308.22	3005.00	1127.11
308.22	4004.00	1133.79
308.22	5004.00	1140.56
308.22	6005.00	1146.98

308.22	8002.00	1159.51
308.22	10001.00	1171.13
308.22	12001.00	1182.37
308.22	14003.00	1194.75
308.22	16005.00	1205.76
308.22	18001.00	1216.57
308.22	20003.00	1227.49
308.22	23001.00	1244.05
308.22	27004.00	1263.44
308.22	31003.00	1283.97
308.22	34997.00	1302.46
308.22	39999.00	1324.45
308.22	45002.00	1347.09
308.22	49999.00	1367.79
308.22	55001.00	1388.31
308.22	60002.00	1408.07
308.22	65000.00	1427.73
318.22	109.00	1062.32
318.22	504.00	1065.38
318.22	750.00	1067.34
318.22	1003.00	1069.21
318.22	1255.00	1071.11
318.22	1501.00	1072.72
318.22	2007.00	1076.32
318.22	2506.00	1079.71
318.22	3005.00	1083.5
318.22	4004.00	1090.38
318.22	5004.00	1096.85
318.22	6005.00	1103.61
318.22	8002.00	1116.61
318.22	10001.00	1129.13
318.22	12001.00	1142.47
318.22	14003.00	1154.62
318.22	16005.00	1166.43
318.22	18001.00	1177.61
318.22	20003.00	1189.14
318.22	23001.00	1205.63
318.22	27004.00	1226.77
318.22	31003.00	1247.41
318.22	34997.00	1266.28
318.22	39999.00	1290.76
318.22	45002.00	1313.78
318.22	49999.00	1334.83
318.22	55001.00	1356.46

318.22	60002.00	1376.77
318.22	65000.00	1395.43
328.22	129.00	1018.3
328.22	504.00	1021.14
328.22	750.00	1023.1
328.22	1003.00	1024.91
328.22	1255.00	1026.82
328.22	1501.00	1028.6
328.22	2007.00	1032.33
328.22	2506.00	1036.21
328.22	3005.00	1040.05
328.22	4004.00	1047.07
328.22	5004.00	1053.76
328.22	6005.00	1060.7
328.22	8002.00	1074.73
328.22	10001.00	1088.42
328.22	12001.00	1101.14
328.22	14003.00	1113.97
328.22	16005.00	1126.49
328.22	18001.00	1138.92
328.22	20003.00	1151.08
328.22	23001.00	1168.1
328.22	27004.00	1190.45
328.22	31003.00	1211.66
328.22	34997.00	1231.66
328.22	39999.00	1256.67
328.22	45002.00	1280.63
328.22	49999.00	1303.34
328.22	55001.00	1324.67
328.22	60002.00	1345.81
328.22	65000.00	1365.57
338.22	170.00	972.8
338.22	504.00	976.32
338.22	750.00	978.88
338.22	1003.00	981.05
338.22	1255.00	982.97
338.22	1501.00	984.75
338.22	2007.00	988.42
338.22	2506.00	992.07
338.22	3005.00	996.0
338.22	4004.00	1004.26
338.22	5004.00	1011.63
338.22	6005.00	1019.16
338.22	8002.00	1033.34

338.22	10001.00	1047.72
338.22	12001.00	1061.19
338.22	14003.00	1074.71
338.22	16005.00	1088.09
338.22	18001.00	1100.33
338.22	20003.00	1112.58
338.22	23001.00	1131.02
338.22	27004.00	1154.76
338.22	31003.00	1176.19
338.22	34997.00	1197.57
338.22	39999.00	1223.29
338.22	45002.00	1248.14
338.22	49999.00	1271.19
338.22	55001.00	1293.31
338.22	60002.00	1315.39
338.22	65000.00	1336.38

Reference

<https://www.doi.org/10.1016/j.jct.2003.12.001>

Temperature, K	Pressure, kPa	Speed of sound, m/s
248.15	100.00	1390.16
248.15	10000.00	1435.51
248.15	20000.00	1478.36
248.15	30000.00	1518.03
248.15	40000.00	1550.78
248.15	50000.00	1590.88
248.15	60000.00	1625.12
248.15	70000.00	1657.38
248.15	80000.00	1688.07
248.15	90000.00	1717.48
248.15	100000.00	1745.43
253.15	100.00	1367.16
253.15	10000.00	1413.84
253.15	20000.00	1457.41
253.15	30000.00	1497.98
253.15	40000.00	1536.44
253.15	50000.00	1572.26
253.15	60000.00	1606.9
253.15	70000.00	1639.52
253.15	80000.00	1670.88
253.15	90000.00	1700.93
253.15	100000.00	1729.65
258.15	100.00	1344.2

258.15	10000.00	1391.98
258.15	20000.00	1436.58
258.15	30000.00	1478.11
258.15	40000.00	1517.33
258.15	50000.00	1553.89
258.15	60000.00	1588.88
258.15	70000.00	1621.91
258.15	80000.00	1653.89
258.15	90000.00	1684.43
258.15	100000.00	1713.62
263.15	100.00	1320.92
263.15	10000.00	1370.35
263.15	20000.00	1415.99
263.15	30000.00	1458.25
263.15	40000.00	1498.44
263.15	50000.00	1535.81
263.15	60000.00	1570.98
263.15	70000.00	1604.54
263.15	80000.00	1637.11
263.15	90000.00	1668.1
263.15	100000.00	1697.74
268.15	100.00	1298.67
268.15	10000.00	1349.08
268.15	20000.00	1395.62
268.15	30000.00	1438.54
268.15	40000.00	1479.77
268.15	50000.00	1517.83
268.15	60000.00	1553.2
268.15	70000.00	1587.43
268.15	80000.00	1620.54
268.15	90000.00	1651.96
268.15	100000.00	1682.01
273.15	100.00	1275.4
273.15	10000.00	1327.81
273.15	20000.00	1375.45
273.15	30000.00	1418.96
273.15	40000.00	1461.31
273.15	50000.00	1499.98
273.15	60000.00	1535.77
273.15	70000.00	1570.58
273.15	80000.00	1604.15
273.15	90000.00	1636.02
273.15	100000.00	1666.45
278.15	100.00	1253.32

278.15	10000.00	1306.75
278.15	20000.00	1355.49
278.15	30000.00	1400.47
278.15	40000.00	1443.03
278.15	50000.00	1481.78
278.15	60000.00	1518.62
278.15	70000.00	1553.98
278.15	80000.00	1587.94
278.15	90000.00	1620.26
278.15	100000.00	1650.92
283.15	100.00	1231.06
283.15	10000.00	1285.85
283.15	20000.00	1335.74
283.15	30000.00	1381.4
283.15	40000.00	1424.94
283.15	50000.00	1464.43
283.15	60000.00	1502.23
283.15	70000.00	1537.63
283.15	80000.00	1571.96
283.15	90000.00	1604.68
283.15	100000.00	1635.63
288.15	100.00	1208.58
288.15	10000.00	1265.05
288.15	20000.00	1316.19
288.15	30000.00	1362.56
288.15	40000.00	1407.06
288.15	50000.00	1447.7
288.15	60000.00	1485.52
288.15	70000.00	1521.53
288.15	80000.00	1556.22
288.15	90000.00	1589.2
288.15	100000.00	1620.74
293.15	100.00	1186.09
293.15	10000.00	1244.14
293.15	20000.00	1296.86
293.15	30000.00	1344.06
293.15	40000.00	1389.16
293.15	50000.00	1430.7
293.15	60000.00	1469.0
293.15	70000.00	1505.7
293.15	80000.00	1540.77
293.15	90000.00	1574.27
293.15	100000.00	1605.01
298.15	100.00	1165.34





Solubility of Desmosterol in Five Organic Solvents:  
Solubility of  
Tetrahydroxybenzophenone (THBP) in (Solid-liquid) phase equilibria of tetraphenyl  
Solubility, Behavior and Data Modeling of 1,4-dioxane in Different Neat and Binary Solvent Systems  
Solubility and activity coefficients at infinite dilution for organic compounds in pure solvents and binary liquid mixtures  
Solubility of Anthracene in C1-C3 Alcohols from (298.2 to 333.2) K and Thermodynamic models for determination of temperature and computation of solubility and dissociation of Anthracene, Anthracene Dithiol and Anthracene Dithione in different solvents:  
Temperature dependence of 5'-Diphosphocholine Sodium in Water and Different Binary Mixtures of different pure solvents and binary  
Measurement of activity coefficients of Dimethyl Carbonate - Liquid Mixtures  
Measurement and correlation of solubility and dissolution properties of polycrystalline polymers and binary solubility of Danthron:  
Separation of binary mixtures based on gamma infinity data using solubility of 2-mercaptans in different solvents from (283.05 to 323.90) K  
Solubilities of Palmitic Acid in Pure Solvents and Its Mixtures:  
Activity Coefficients at Infinite Dilution Measurements for Organic Solutes and Determination of Activity Coefficients at infinite Dilution of Organic Solutes in the Solvent Hexanes with and without Carbon dioxide with and without azolium salts at 0.1 MPa in equilibrium  
Measurement of VLE and  $c_1$  data and prediction of their thermodynamic properties and solubility in different solvents from (278.15 to 313.15) K:  
Solid-liquid equilibrium of sulbactam in pure solvents and binary solvent  
Measurement and Correlation of the Solubility of 5-Fluorouracil in Pure and Binary Solvents  
Solubility of Some Phosphaspirocyclic Compounds in Solid State  
Solubility of pioglitazone hydrochloride in different binary solvents  
Measurement and modelling of econazole nitrate in twelve pure organic solvents and activity coefficients at infinite dilution for organic compounds and correlation of solubility of 3,4-dihydro-2-naphthol in different binary mixed organic solvents from 298.15 to 323.15 K  
Solubility of 2,9-dioxido-2,4,8,10-tetraoxa-1,3-dithiane in different solvents from (283.0 to 323.0) K  
Solubilities of 1,1'-[1,2-Ethanediylo]bis(oxy-1,2-ethanedithiol) in organic solvents and water, LLE Measurements of 1,2-Ethanedithiol, Dimethylformamide, Dimethyl Sulfoxide, Dimethylacetamide, Dimethylacetone, and Dimethylacetone in different solvents from (298.15 to 323.15) K  
Measurement of activity coefficients at infinite dilution for organic solutes in different Thermodynamic models for determination of solid liquid solubility Modeling of Benzyladenine in 4-Methylsulfonylbenzaldehyde in Nine Organic Solvents at a Evaluation of the Temperature- Coumaric Acid in Nine Pure and Water + Ethanol Mixed Solvents at Temperatures from 293.15 to 333.15 K;

<https://www.doi.org/10.1021/je8006088>  
<https://www.doi.org/10.1021/je700434b>  
<https://www.doi.org/10.1016/j.jct.2014.06.021>  
<https://www.doi.org/10.1021/acs.jced.9b00802>  
<https://www.doi.org/10.1016/j.jct.2018.08.028>  
<https://www.doi.org/10.1021/je0201323>  
<https://www.doi.org/10.1021/je1001945>  
<https://www.doi.org/10.1016/j.jct.2016.04.007>  
<https://www.doi.org/10.1021/acs.jced.8b00333>  
<https://www.doi.org/10.1021/je700069g>  
<https://www.doi.org/10.1021/je900465r>  
<https://www.doi.org/10.1016/j.tca.2012.03.007>  
<https://www.doi.org/10.1021/je0497000>  
<https://www.doi.org/10.1016/j.fluid.2015.06.026>  
<https://www.doi.org/10.1021/acs.jced.5b00192>  
<https://www.doi.org/10.1016/j.jct.2017.12.012>  
<https://www.doi.org/10.1021/je8006869>  
<https://www.doi.org/10.1021/je8005979>  
<https://www.doi.org/10.1021/je1000582>  
<https://www.doi.org/10.1021/acs.jced.8b00080>  
<https://www.doi.org/10.1021/je0499465>  
<https://www.doi.org/10.1016/j.jct.2005.04.010>  
<https://www.doi.org/10.1016/j.jct.2015.09.026>  
<https://www.doi.org/10.1016/j.jct.2011.11.009>  
<https://www.doi.org/10.1016/j.fluid.2014.09.008>  
<https://www.doi.org/10.1021/acs.jced.8b00425>  
<https://www.doi.org/10.1021/je060138i>  
<https://www.doi.org/10.1016/j.fluid.2013.05.008>  
<https://www.doi.org/10.1016/j.jct.2016.07.043>  
<https://www.doi.org/10.1016/j.jct.2013.08.030>  
<https://www.doi.org/10.1021/acs.jced.8b00578>  
<https://www.doi.org/10.1021/acs.jced.7b00238>  
<https://www.doi.org/10.1021/je9004189>  
**a-3,9-diphosphaSpiro[5.5]undecane**  
<https://www.doi.org/10.1021/je100316k>  
<https://www.doi.org/10.1021/je5004466>  
**yl)]bis-[3-methyl-1H-imidazolium-1-yl]**  
<https://www.doi.org/10.1021/acs.jced.6b00149>  
<https://www.doi.org/10.1021/je0341763>  
<https://www.doi.org/10.1016/j.jct.2013.09.032>  
<https://www.doi.org/10.1016/j.fluid.2018.01.019>  
<https://www.doi.org/10.1021/acs.jced.7b01085>  
<https://www.doi.org/10.1016/j.jct.2016.12.002>  
<https://www.doi.org/10.1021/acs.jced.5b01053>  
<https://www.doi.org/10.1021/acs.jced.6b00361>

<https://www.doi.org/10.1021/je1003934>

<https://www.doi.org/10.1016/j.ijct.2016.06.032>

<https://www.doi.org/10.1021/je800515w>

<https://www.doi.org/10.1016/j.fluid.2012.04.008>

<https://www.doi.org/10.1016/j.ijct.2012.01.019>

<https://www.doi.org/10.1016/j.ijct.2013.10.038>

<https://www.doi.org/10.1021/ie060348v>

<https://www.doi.org/10.1021/acs.jced.9b00275>

<https://www.doi.org/10.1016/j.fluid.2013.05.006>

<https://www.doi.org/10.1016/j.ijct.2013.05.030>

<https://www.doi.org/10.1021/acs.jced.5b00714>

<https://www.doi.org/10.1021/ie800049b>

<https://www.doi.org/10.1021/je501049c>

<https://www.doi.org/10.1021/ie060178m>

<https://www.doi.org/10.1021/ie050082c>

<https://www.doi.org/10.1021/acs.iced.9b00047>

**Open-1-one**  
<https://www.doi.org/10.1016/j.fluid.2009.12.009>

<https://www.doi.org/10.1016/j.fluid.2013.06.013>

<https://www.doi.org/10.1021/ie0495435>

<https://www.doi.org/10.1021/acs.iced.5b00607>

<https://www.doi.org/10.1031/jc800803o>

<https://www.doi.org/10.1031/jc060174b>

<https://www.doi.org/10.1031/acs.jced.3b00543>

<https://www.doi.org/10.1031/jc0005618>

<https://www.doi.org/10.1016/j.ijot.2016.03.017>

<https://www.doi.org/10.1016/j.jst.2014.04.005>

<https://www.doi.org/10.1031/acs.joc.3b0036>

<https://www.doi.org/10.1016/j.jst.2017.03.016>

<https://www.doi.org/10.1001/ja.2003295>

<https://www.doi.org/10.1001/jco.040835>

[illegible]

11/10/2014 10:10:01 AM

<https://doi.org/10.1001/jama.2021.10000>

[illegible]

[http://www.scribd.com/doc/10191678/0015-10-000](#)

101-111 // 1987-1988 // "1987-1988" // 700500

[illegible]

DOI: 10.1002/for

.....

<https://www.industry.gov.au/publications/industry-2020-2021>

<https://doi.org/10.1016/j.jgl.2019.05.002>

<https://www.industry.gov.au/content/industry/industry-research-and-statistics/industry-research-and-statistics-reports>

<https://www.wdaenergy.com/energy/journal/2017/01/01/2017-01-01-01>

<https://www.wdaenergy.com/energy/17/for-30-10-12>









[illegible]

<https://www.doi.org/10.1021/acs.jced.5b00033>

<https://www.doi.org/10.1021/ie0342421>

<https://www.doi.org/10.1016/j.fluid.2005.01.007>

<https://www.doi.org/10.1016/j.ijct.2015.07.023>

<https://www.doi.org/10.1016/j.fluid.2013.11.001>

<https://www.doi.org/10.1021/je800410b>

<https://www.doi.org/10.1021/je7005693>

<https://www.doi.org/10.1021/acs.iced.9b00560>

<https://www.doi.org/10.1016/j.fluid.2006.11.011>

<https://www.doi.org/10.1021/je030122h>

<https://www.doi.org/10.1021/je400714f>

<https://www.doi.org/10.1021/je034078h>

<https://www.doi.org/10.1016/j.fluid.2007.07.030>

<https://www.doi.org/10.1021/je0505265>

<https://www.doi.org/10.1016/j.fluid.2014.12.020>

<https://www.doi.org/10.1021/acs.iced.8b00023>

<https://www.doi.org/10.1016/j.fluid.2018.11.011>

<https://www.doi.org/10.1016/j.ijct.2016.07.035>

<https://www.doi.org/10.1021/je800246v>

<https://www.doi.org/10.1016/j.ijct.2015.09.032>

<https://www.doi.org/10.1016/j.ijct.2016.10.004>

<https://www.doi.org/10.1021/je700417z>

<https://www.doi.org/10.1016/j.ijct.2016.09.012>

<https://www.doi.org/10.1016/j.ijct.2013.01.005>

<https://www.doi.org/10.1016/j.ijct.2014.08.024>

<https://www.doi.org/10.1021/jo500867u>

<https://www.doi.org/10.1016/j.ijet.2013.05.017>

<https://www.doi.org/10.1021/jc0006585>

imidazolium-1-yl)  
<https://www.doi.org/10.1016/j.ijct.2015.07.010>

<https://www.doi.org/10.1021/jc501003z>

<https://www.doi.org/10.1021/jc024203n>

<https://www.doi.org/10.1021/jz030102f>

<https://www.doi.org/10.1021/jc000743n>

<https://www.doi.org/10.1001/jama.2019.10001>

<https://www.doi.org/10.1091/ess-e2015-00025>

<https://www.doi.org/10.1001/asc.jad.7b.00510>

<http://www.ncbi.nlm.nih.gov/pmc/articles/PMC111004/>

<http://www.elsevier.com/locate/journalofelectronicmaterials>

<https://doi.org/10.1002/ajce.10000>

<https://www.doi.org/10.1021/acs.jocd.3b00291>

<https://doi.org/10.1016/j.jnua.2014.06.022>

<https://doi.org/10.1021/acs.joc.3c00033>

<https://doi.org/10.1021/jc00007a033>

<https://www.doi.org/10.1016/j.jct.2015.11.001>

[illegible]

<https://www.doi.org/10.1021/je800945e>

<https://www.doi.org/10.1021/ie0604737>

<https://www.doi.org/10.1021/acs.jced.8b00192>

<https://www.doi.org/10.1021/ie049688b>

<https://www.doi.org/10.1016/j.fluid.2013.11.005>

<https://www.doi.org/10.1021/je400691f>

<https://www.doi.org/10.1021/acs.jced.7b01011>

<https://www.doi.org/10.1016/j.ijct.2017.02.017>

<https://www.doi.org/10.1021/acs.jced.8b00566>

<https://www.doi.org/10.1021/ie800893n>

<https://www.doi.org/10.1016/j.fluid.2014.04.008>

<https://www.doi.org/10.1016/j.ijct.2012.09.017>

<https://www.doi.org/10.1016/j.ijct.2019.05.011>

<https://www.doi.org/10.1021/acs.jced.9b00658>

<https://www.doi.org/10.1016/j.ijct.2016.07.013>

<https://www.doi.org/10.1016/j.fluid.2013.05.006>

<https://www.doi.org/10.1016/j.ijct.2013.08.007>

<https://www.doi.org/10.1016/j.ijct.2015.05.014>

<https://www.doi.org/10.1016/j.ijct.2013.06.009>

<https://www.doi.org/10.1016/j.ijct.2006.03.003>

<https://www.doi.org/10.1021/jc201058i>

<https://www.doi.org/10.1016/j.fluid.2006.09.007>

<https://www.doi.org/10.1016/j.ijot.2015.05.006>

<https://www.doi.org/10.1016/j.ijot.2014.05.009>

<https://www.doi.org/10.1016/j.ijat.2019.03.003>

<http://www.doi.org/10.1016/j.jst.2013.01.010>

<https://www.doi.org/10.1016/j.jst.2019.06.004>

<https://www.doi.org/10.1031/acs.joc.3b01106>

<https://www.doi.org/10.1016/j.iast.2018.03.016>

<https://www.doi.org/10.1001/ja.5040627>

11. // 10 1010" 5" 1 0015 01 000

https://doi.org/10.1001/jama.2000.0050

<https://doi.org/10.1001/jama.1991.02710031000005>

11. // 11. 1001/ 11. 171.00000

**sphoramidate**

**Keywords:** *depression; mood disorders; anxiety disorders*

doi:10.1371/journal.pone.0136412.g002

<https://www.industry.gov.au/publications/industry-2020-2021>

<https://www.ncbi.nlm.nih.gov/pmc/articles/PMC6936333/>

<https://www.washpost.com/archive/washingtonpost.com>

<https://www.wadsworth.com/9781493995551/9781493995551-10>

<https://www.wadsworth.com/college/roberts/jjcd23111011012>



[illegible]

<https://www.doi.org/10.1016/j.jct.2016.07.021>

<https://www.doi.org/10.1016/j.ijct.2018.07.024>

<https://www.doi.org/10.1021/je050110r>

<https://www.doi.org/10.1021/je200333p>

<https://www.doi.org/10.1016/j.fluid.2018.05.023>

<https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=1191>

<https://www.doi.org/10.1021/acs.jced.6b00664>

<https://www.doi.org/10.1021/acs.jced.8b00600>

<https://www.doi.org/10.1016/j.fluid.2016.02.004>

<https://www.doi.org/10.1016/j.ijct.2014.04.024>

<https://www.doi.org/10.1016/j.ijct.2018.09.003>

<https://www.doi.org/10.1021/ie900704b>

<https://www.doi.org/10.1016/j.fluid.2012.06.011>

<https://www.doi.org/10.1021/ie7000017b>

<https://www.doi.org/10.1016/j.fluid.2012.01.019>

<https://www.doi.org/10.1021/acs.jced.9b00703>

<https://www.doi.org/10.1021/ie500986b>

<https://www.doi.org/10.1021/ie060289l>

<https://www.doi.org/10.1021/ie700639s>

<https://www.doi.org/10.1016/j.ijct.2015.12.022>

<https://www.doi.org/10.1016/j.ijct.2013.09.007>

<https://www.doi.org/10.1016/j.itca.2018.04.018>

<https://www.doi.org/10.1031/jc900031a>

<https://www.doi.org/10.1016/j.fluid.2014.01.008>

<https://www.doi.org/10.1031/ie800277a>

<https://www.doi.org/10.1016/j.fluid.2013.11.030>

<https://www.doi.org/10.1016/j.fluid.2018.07.038>

<https://www.doi.org/10.1016/j.fluid.2016.10.034>

<https://www.doi.org/10.1021/jc100638a>

<https://www.doi.org/10.1021/jc5004002>

<https://www.doi.org/10.1016/j.iat.2010.05.017>

<https://www.doi.org/10.1016/j.fluid.2013.12.022>

<https://www.doi.org/10.1016/j.fluid.2015.03.027>

<https://www.doi.org/10.1001/ja.5002001>

<https://www.doi.org/10.1001/ja.1010220>

<https://www.doi.org/10.1001/ja.2000300>

[illegible][illegible]

11. "11-10-1994" 11-10-1994

[illegible]

14. "1994" 000=000

<http://www.elsevier.com/locate/jmb>

http://www.elsevier.com/locate/jmb

1-Fluoro-4-(methylsulfonyl)benzene in  
Binary Mixtures of the Solvents: Acid,  
Formic, Acetic, Propionic, and Butyric  
1-(4-Piperazinyl)-2,2,6,6-tetramethyl-  
piperidine-1-oxide (B.P. 10) tetra-  
hydrophthalazine 1,4-dioxide in  
nine pure organic solvents and liquid  
nitrofluoride (methanol + ethyl acetate)  
1-(4,7,3-trimethyl-2-oxo-1,2,3,4-tetra-  
hydrophthalazine-1-ylidene)-2,2,6,6-  
tetramethylpiperidine-1-oxide in  
solvents: water, acetone, propylene  
and diethyl ether. Solubilities of  
Extractions: Distillation: Isobaric  
Vapor-Liquid Equilibrium for Aqueous  
Organic Solutes in the Ionic Liquid  
1-butyl-3-methylimidazolium methyl  
sulfate on investigation of limiting  
activity coefficients with and  
without the effect of water in  
the separation of 2-oxo-1,2,3,4-tetra-  
hydrophthalazine 1,4-dioxide with and  
without the equilibrium of  
dicyandiamide in different solvents:  
The determination and correlation of  
the solubility of naproxen in acetone  
and water mixtures. Equilibria for (water +  
1-propanol or acetone +  
Solubility of Cellulose at different  
temperatures: 2-diyl)-bis(3-methylpyridin-  
2-ylmethyl)propane-1,3-diol in Acetone,  
Chloroform, and Toluene:  
Solubilities of Triadimefon in Acetone +  
Water from (278.15 to 333.15) K:  
Solubility and Melting Properties of  
Salicylic Acid:  
Measurement and Correlation of  
Solubility of Theobromine,  
Therapeutic and Carcinogenic Mixtures  
Containing Cyclic Amides: A Activity  
Coefficient and Infinite Dilution of  
Hydroxybenzyl Alcohol in 2,2,4,4-tetra-  
hydrofuran, 1,2-dichloroethane, and  
1,1,2,2-tetrachloroethane Solubility,  
Thermodynamic Properties, and  
Density of Methylpropylamide,  
Fluoromethylpropylamide, and  
1,1,1,2-tetrafluoro-2-methylpropane  
in different solvents: Solubility and  
Density of Different Temperatures at  
Different Temperatures Range from 273.15 to  
303.15 K Vapor Liquid Equilibria for  
Binary Systems of Acetone +  
Methylpropylamide, 2,2,4,4-tetra-  
hydrofuran, 1,2-dichloroethane +  
solubility of acetamide in supercritical  
acetone, and the effect of ammonia on  
propylamide in ten solvents from T =  
273.15 to 323.15 K: Sound of lithium  
bromide with organic solvents:  
Equilibrium and correlation: Ethyl  
Acetate, Propyl Acetate, Isopropyl  
Acetate, and Butanol in  
Thermodynamic Properties of Mixtures  
Containing Solvent Liquids: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents: A  
thermodynamic study of the  
thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate and 1-butyl-3-  
methylimidazolium hexafluorophosphate  
in different solvents: A Activity  
Coefficient and Infinite Dilution of  
Acetamide and Butanol in (285  
K) and (295 K) in different solvents:  
Thermodynamic Properties of Ionic  
Liquids: Thermodynamic Properties of  
the 1-butyl-3-methylimidazolium  
hexafluorophosphate

<https://www.doi.org/10.1021/je5000605>

### Thermodynamic Data of Cefixime Trihydrate in Seven Pure Solvents:



Thermodynamic functions of 1-methyl-4-(methylsulfonyl)benzene  
Solubility coefficients and solid-liquid  
solubility of organic solutes in the ionic liquid  
1-butyl-3-methylimidazolium hexafluorophosphate in Methanol,  
Acetone, Ethanol, Acetone and Water from  
Experimental Measurements and  
Correlation of the Solubilities of  
2,4-Dichloro-5-methoxy pyrimidine in  
Ethyl Acetate, Ethanol, Acetone, +  
1-butyl-3-methylimidazolium hexafluorophosphate  
and 1-butyl-3-methylimidazolium nitrate  
Solubility of Sulfachloropyridazine in  
Pure and Binary Solvent Mixtures and  
Solubility of Acetaminophen in Different  
Solvents from (292.90 to 327.60) K:  
Crystal Structures, Reaction Rates, and  
Selected Physical Properties of  
Halo-Borane-amine complexes (Halo =  
determination of the solubility of)  
onebiphenyl in pure and mixture of  
organic solvents from T = (278.15 to  
353.15) K. Measurement and  
Thermodynamic Model Correlation of  
4-Nitroethyl Chloride in Different  
thermodynamics of viscous flow of  
hydrocarbons and carotenes in water  
alcohols, amorphous sucrose and  
polyethylene glycol elements correlation  
solubility of sodium in six organic  
solvents and binary mixtures of solvents  
and organic solvents and polymers from  
273.15 to 323.15 K: correlation of  
measurements and thermodynamic  
modeling of methyl acetate dilution  
pure organic alcohols and ketones in  
methyl acetate: experimental data and  
atomistic dilution of organic solutes  
and water in the ionic liquid  
Equilibria of Some Gaseous Dioxides in Organic  
Solvents  
Solubility of Hexone Disodium in  
Acetone, Methanol, Ethanol,  
Methyl acetate, and water: coefficients  
of binary dilution of organic 318 K:  
Solubility of water in Hydrogen  
Sulfide from 0 to 100 °C in Different Solvents:  
Activity coefficients at infinite dilution  
and physicochemical properties for  
organic dynamic studies in water for  
Amino-4-chloro-6-methoxypyrimidine  
and 4-chloro-6-methoxypyrimidine  
in Solvents Solvent Mixtures 323.15  
Interactions of 3-Aminotetrahydro-2H-  
pyran-2-yl with a Binary System of  
2,2-Dimethoxypropane + Acetone +  
Water: formation of the solid-liquid  
equilibrium of 1,3-bis(2-methyl-2-ethyl  
ketene)urea as a catalyst for the reduction of  
methylglyoxal and benzoylformate:  
Solubility of Diethoxy in Twelve Pure  
and Binary Solvents and Solvents  
and triphenylphosphine in the different  
binary solvents.  
Measurement and correlation of the  
solubility of  
Acetone in Hexamethane and Correlation  
of Oxidation in 12 Pure Organic  
Solvents  
liquid equilibria for the system  
acetone + solketal + glycerol at 303.2,  
323.15, and 343.15 K  
Determination and Correlation of  
Solubilities of 2-Isopropylthioxanthone  
in Various Different Solvents from  
(298.15 to 327.65) K: 8,9-tetrahydrophenanthrene  
in Organic Solvents and Correlation  
of the form A of ibuprofen in organic  
solvents from 278.15 to 323.15 K:  
3,7,9,11-Tetraoxo-2,4,6,8,10-pentaaza[3.  
Properties of Propylpyridine in  
solvents and temperatures in  
pure and binary mixtures of the  
1,3-bis(2-methyl-2-ethylketene)urea  
in Solvents and binary mixtures from 278.15 K  
and 323.15 K: Correlation of  
superficial carbon dioxide and  
Mixed Solvents, 273.15-313.15 K and  
its Correlation with Different  
Thermodynamic Models:

<https://www.doi.org/10.1016/j.jct.2016.08.021>  
<https://www.doi.org/10.1016/j.jct.2010.12.005>  
<https://www.doi.org/10.1021/je900554r>  
<https://www.doi.org/10.1021/je9005689>  
<https://www.doi.org/10.1021/je501089z>  
<https://www.doi.org/10.1021/je049908l>  
<https://www.doi.org/10.1021/je100998r>  
<https://www.doi.org/10.1021/acs.jced.7b01134>  
<https://www.doi.org/10.1021/je0603630>  
<https://www.doi.org/10.1021/je3005112>  
<https://www.doi.org/10.1016/j.jct.2015.11.005>  
<https://www.doi.org/10.1021/je100255z>  
<https://www.doi.org/10.1021/acs.jced.9b00232>  
<https://www.doi.org/10.1016/j.tca.2006.01.019>  
<https://www.doi.org/10.1016/j.fluid.2018.08.014>  
<https://www.doi.org/10.1021/acs.jced.7b00638>  
<https://www.doi.org/10.1016/j.jct.2016.09.039>  
<https://www.doi.org/10.1021/acs.jced.8b01226>  
<https://www.doi.org/10.1016/j.fluid.2015.09.003>  
<https://www.doi.org/10.1016/j.jct.2012.03.005>  
<https://www.doi.org/10.1021/je0498560>  
<https://www.doi.org/10.1021/je0501989>  
<https://www.doi.org/10.1016/j.jct.2010.10.026>  
<https://www.doi.org/10.1021/je100022w>  
<https://www.doi.org/10.1016/j.jct.2015.02.024>  
<https://www.doi.org/10.1016/j.jct.2016.10.020>  
<https://www.doi.org/10.1021/acs.jced.9b00385>  
<https://www.doi.org/10.1021/je050013y>  
<https://www.doi.org/10.1016/j.jct.2017.03.015>  
<https://www.doi.org/10.1016/j.jct.2004.08.002>  
<https://www.doi.org/10.1021/acs.jced.9b00696>  
<https://www.doi.org/10.1016/j.fluid.2015.03.036>  
<https://www.doi.org/10.1016/j.fluid.2014.08.036>  
<https://www.doi.org/10.1021/acs.jced.9b00308>  
<https://www.doi.org/10.1021/je500469a>  
<https://www.doi.org/10.1021/je501011t>  
<https://www.doi.org/10.1021/je800238y>  
<https://www.doi.org/10.1016/j.jct.2016.08.034>  
<https://www.doi.org/10.1021/acs.jced.6b00349>  
<https://www.doi.org/10.1016/j.jct.2013.05.035>  
<https://www.doi.org/10.1021/je500806u>  
<https://www.doi.org/10.1021/je800700r>  
<https://www.doi.org/10.1021/acs.jced.9b00286>

[illegible]

<https://www.doi.org/10.1016/j.jct.2011.11.025>  
<https://www.doi.org/10.1016/j.jct.2003.12.001>  
<https://www.doi.org/10.1016/j.jct.2018.12.044>  
<https://www.doi.org/10.1021/acs.jced.5b00190>  
<https://www.doi.org/10.1021/je0496239>  
<https://www.doi.org/10.1016/j.fluid.2007.06.001>  
<https://www.doi.org/10.1016/j.jct.2011.04.018>  
<https://www.doi.org/10.1016/j.fluid.2015.01.001>  
<https://www.doi.org/10.1016/j.jct.2007.10.006>  
<https://www.doi.org/10.1021/je700539w>  
<https://www.doi.org/10.1021/je800218g>  
<https://www.doi.org/10.1021/je500418f>  
<https://www.doi.org/10.1016/j.jct.2016.06.033>  
<https://www.doi.org/10.1021/je900711h>  
<https://www.doi.org/10.1021/je300711r>  
<https://www.doi.org/10.1021/acs.jced.7b00301>  
<https://www.doi.org/10.1016/j.jct.2009.08.012>  
<https://www.doi.org/10.1016/j.fluid.2019.03.023>  
<https://www.doi.org/10.1021/acs.jced.8b00430>  
<https://www.doi.org/10.1021/je034160c>  
<https://www.doi.org/10.1016/j.jct.2016.10.006>  
<https://www.doi.org/10.1016/j.jct.2018.03.019>  
<https://www.doi.org/10.1016/j.fluid.2014.10.011>  
<https://www.doi.org/10.1016/j.jct.2016.10.040>  
<https://www.doi.org/10.1021/je1002016>  
<https://www.doi.org/10.1021/je050544m>  
<https://www.doi.org/10.1021/acs.jced.9b00243>  
<https://www.doi.org/10.1021/je500012b>  
<https://www.doi.org/10.1016/j.tca.2005.11.035>  
<https://www.doi.org/10.1016/j.jct.2017.03.004>  
<https://www.doi.org/10.1021/je700497h>  
<https://www.doi.org/10.1021/je100890f>  
<https://www.doi.org/10.1016/j.jct.2012.09.033>  
<https://www.doi.org/10.1016/j.fluid.2014.12.037>  
<https://www.doi.org/10.1021/je4010917>  
<https://www.doi.org/10.1021/je100344z>  
<https://www.doi.org/10.1021/je8005826>  
<https://www.doi.org/10.1021/je3001816>  
<https://www.doi.org/10.1016/j.jct.2016.10.011>  
<https://www.doi.org/10.1021/je060133l>  
<https://www.doi.org/10.1021/acs.jced.8b00292>  
<https://www.doi.org/10.1016/j.jct.2016.08.008>  
<https://www.doi.org/10.1021/acs.jced.8b00235>



[illegible]

<https://www.doi.org/10.1021/je0500781>  
<https://www.doi.org/10.1021/je700453v>  
<https://www.doi.org/10.1016/j.jct.2016.07.001>  
<https://www.doi.org/10.1021/je7007457>  
<https://www.doi.org/10.1021/acs.jced.9b00360>  
<https://www.doi.org/10.1021/je8001128>  
<https://www.doi.org/10.1016/j.jct.2011.06.007>  
<https://www.doi.org/10.1016/j.jct.2017.06.008>  
<https://www.doi.org/10.1021/je1011136>  
<https://www.doi.org/10.1021/je900535d>  
<https://www.doi.org/10.1021/je501026m>  
<https://www.doi.org/10.1021/acs.jced.9b00353>  
<https://www.doi.org/10.1016/j.jct.2016.08.035>  
<https://www.doi.org/10.1021/je900524t>  
<https://www.doi.org/10.1016/j.jct.2018.09.017>  
<https://www.doi.org/10.1021/je700312r>  
<https://www.doi.org/10.1021/acs.jced.8b00717>  
<https://www.doi.org/10.1016/j.jct.2011.01.005>  
<https://www.doi.org/10.1021/je101008y>  
<https://www.doi.org/10.1016/j.jct.2013.05.008>  
<https://www.doi.org/10.1021/je100949x>  
<https://www.doi.org/10.1021/je200822w>  
<https://www.doi.org/10.1021/je800063d>  
<https://www.doi.org/10.1021/je050406x>  
<https://www.doi.org/10.1016/j.fluid.2019.06.004>  
<https://www.doi.org/10.1016/j.fluid.2012.02.011>  
<https://www.doi.org/10.1016/j.jct.2016.11.014>  
<https://www.doi.org/10.1021/je400513s>  
<https://www.doi.org/10.1016/j.fluid.2013.09.023>  
<https://www.doi.org/10.1021/acs.jced.8b01080>  
<https://www.doi.org/10.1016/j.jct.2011.11.007>  
<https://www.doi.org/10.1021/je301243f>  
<https://www.doi.org/10.1016/j.jct.2016.03.011>  
<https://www.doi.org/10.1016/j.jct.2015.11.025>  
<https://www.doi.org/10.1016/j.fluid.2018.09.024>  
<https://www.doi.org/10.1021/je301194e>  
<https://www.doi.org/10.1021/je400259a>  
<https://www.doi.org/10.1021/acs.jced.7b00118>  
<https://www.doi.org/10.1016/j.jct.2014.03.026>  
<https://www.doi.org/10.1021/je400544h>  
<https://www.doi.org/10.1021/acs.jced.6b00700>  
<https://www.doi.org/10.1016/j.jct.2013.01.024>  
<https://www.doi.org/10.1021/je500205z>

[illegible]

<https://www.doi.org/10.1021/acs.jced.5b00738>  
<https://www.doi.org/10.1021/acs.jced.8b01256>  
<https://www.doi.org/10.1021/je900542y>  
<https://www.doi.org/10.1016/j.fluid.2011.09.027>  
<https://www.doi.org/10.1016/j.fluid.2013.01.011>  
<https://www.doi.org/10.1016/j.fluid.2010.06.021>  
<https://www.doi.org/10.1021/acs.jced.9b00350>  
<https://www.doi.org/10.1021/acs.jced.5b00783>  
<https://www.doi.org/10.1021/acs.jced.5b00306>  
<https://www.doi.org/10.1021/acs.jced.9b00341>  
<https://www.doi.org/10.1021/acs.jced.8b00863>  
<https://www.doi.org/10.1021/acs.jced.6b00145>  
<https://www.doi.org/10.1021/je800428r>  
<https://www.doi.org/10.1021/je100343v>  
<https://www.doi.org/10.1016/j.jct.2014.12.002>  
<https://www.doi.org/10.1021/acs.jced.6b00929>  
<https://www.doi.org/10.1021/je500682v>  
<https://www.doi.org/10.1016/j.fluid.2012.05.003>  
<https://www.doi.org/10.1021/je100609r>  
<https://www.doi.org/10.1021/acs.jced.9b00445>  
<https://www.doi.org/10.1016/j.jct.2016.02.016>  
<https://www.doi.org/10.1021/je700050r>  
<https://www.doi.org/10.1016/j.jct.2016.01.023>  
<https://www.doi.org/10.1007/s10765-013-1527-7>  
<https://www.doi.org/10.1021/je800768x>  
<https://www.doi.org/10.1016/j.fluid.2014.01.043>  
<https://www.doi.org/10.1016/j.jct.2016.07.023>  
<https://www.doi.org/10.1016/j.fluid.2009.08.017>  
<https://www.doi.org/10.1016/j.fluid.2013.06.037>  
<https://www.doi.org/10.1021/je901025f>  
<https://www.doi.org/10.1016/j.fluid.2005.01.002>  
<https://www.doi.org/10.1016/j.jct.2015.10.015>  
<https://www.doi.org/10.1016/j.fluid.2005.06.024>  
<https://www.doi.org/10.1016/j.fluid.2017.12.029>  
<https://www.doi.org/10.1021/je3010535>  
<https://www.doi.org/10.1016/j.tca.2013.07.002>  
<https://www.doi.org/10.1021/je1005517>  
<https://www.doi.org/10.1021/je900328c>  
<https://www.doi.org/10.1021/je060305e>  
<https://www.doi.org/10.1021/je200252c>  
<https://www.doi.org/10.1021/acs.jced.9b00411>  
<https://www.doi.org/10.1021/acs.jced.7b00846>  
<https://www.doi.org/10.1021/je800838w>



Solubility of 4-Hydroxybenzaldehyde in Supercritical Carbon Dioxide with and without Co-Solvents, Model Correlation, and Solvent Effect of Excess Parameter: A Study on the Binary Mixtures of Toluene with Ketones at Different Temperatures: Equilibrium and Dissolution Properties of Ethyl Vanillin in Ternary Systems and Activity Coefficients at Infinite Dilution for Organic Solutes in the Ionic Liquid 3-Carboxy-3-hydroxyoctanedioic Acid (Citric Acid) in 1,2-Dichloroethane, Acetone, and Other Organic Solvents between 293.05 and 313.15 K: Measurement of Activity Coefficients at Infinite Dilution for Organic Solutes and Water in Camphorquinone in Pure Solvents from (293.15 to 313.15) K: Influence of Sulfate-based Anion Ionic Liquids on the Separation Factor of the Binary 2-Ethoxy-1-Propanol + Ethanol for Non-Binary Systems of Cracking C5 Fraction at 200 K: Densities, and Isothermal Compressibility of CO<sub>2</sub> + Benzene and CO<sub>2</sub> + Acetone Systems by Using the Peng-Robinson (PR) Equation: Phase Diagrams of the Binary System of Water + Benzoinitrile + Propanone, or + Isoamyl Isopropyl liquid equilibrium for ternary mixtures of acetone + methanol + benzoinitrile in Different Single and Binary Solvent Mixtures between 284.15 and 313.15 K, Ethanol, and Acetone from (288.2 to 328.2) K: Measurement and Correlation of Solubility of L-Valine in Water + Phase Diagrams of Acetone + Ethanol, Acetone + Water, and Ethanol + Water at 298.15 K and Aqueous Ethanol + Acetone in Pure Benzoinitrile and 2-Propanol at 298.15 K: Solubility of Acetone in Methylhydrate Measurement and Correlation of Ternary Solid-Liquid Equilibrium of 2-Ethyl-1,4-naphthoquinone + Phthalic Anhydride + Acetone System: Solubility of 4-(3,4-Dichlorophenyl)-1-tetralone in Solvents of Various Types: Solubility of Hexacarbopine in Eight Solvents within the Temperature Range 293.15 to 313.15 K: Phthalic Anhydride and 4-Chlorophthalic Anhydride in Organic Solvents and Hydroxyacetic Acid in Pure and Binary Acetone + Hydroxyacetic Acid in Water from (2-Ethoxypropane + Acetone) and (2-Ethoxypropane + Butanone): 2,4-Dinitro-L-phenylalanine in Determination and Modeling of the Solubility of (Limonin in Methanol or Ethanol + Water) in CO<sub>2</sub> + Toluene, CO<sub>2</sub> + Acetone, and CO<sub>2</sub> + Ethanol at High Temperatures and Model Evaluation and Thermodynamic Analysis of Phase Equilibria in Binary Mixtures of Carbon Dioxide with Ethanol and Acetone for Binary Systems of 2,3-Pentanedione with Solubility of Protonic Hydrochloride Hemi-Hydrate in (Water + Acetone): Measurement and Correlation of Solubility of Dodecanedioic Acid in Different Solvents from (288.15 to 313.15) K: Solubility in Eleven Hydroxyacetic Acid, Ethanol, and 2-Ethoxy-1-Propanol + Acetone in Mixed Solvents from 298.15 to 323.15 K: Solubility of 2-Ethoxy-1-Propanol + Acetone and Stigmasteryl Maleate in Acetone and Ethanol: Solubility of Difloxacin in Acetone, Methanol, and Ethanol from (293.15 to 313.15) K:

<https://www.doi.org/10.1021/je401082x>

<https://www.doi.org/10.1021/acs.jced.8b01265>

<https://www.doi.org/10.1016/j.jct.2009.12.008>

<https://www.doi.org/10.1016/j.jct.2016.10.029>

<https://www.doi.org/10.1016/j.fluid.2018.06.013>

<https://www.doi.org/10.1021/je101167z>

<https://www.doi.org/10.1021/je700426k>

<https://www.doi.org/10.1016/j.jct.2011.09.028>

<https://www.doi.org/10.1016/j.jct.2013.07.004>

<https://www.doi.org/10.1021/je800801x>

<https://www.doi.org/10.1016/j.fluid.2012.12.006>

<https://www.doi.org/10.1021/acs.jced.6b00180>

<https://www.doi.org/10.1021/je034087q>

<https://www.doi.org/10.1021/je7002463>

<https://www.doi.org/10.1021/je030115t>

<https://www.doi.org/10.1016/j.fluid.2017.03.014>

<https://www.doi.org/10.1021/je100125x>

<https://www.doi.org/10.1021/je050076g>

<https://www.doi.org/10.1021/je500255d>

<https://www.doi.org/10.1016/j.jct.2012.03.026>

<https://www.doi.org/10.1021/acs.jced.8b01193>

<https://www.doi.org/10.1021/je400899e>

<https://www.doi.org/10.1016/j.fluid.2015.09.019>

<https://www.thermo.com/research/kdb/hcprop/showprop.php?cmpid=1191>

<https://www.doi.org/10.1021/je060329I>

<https://www.doi.org/10.1016/j.jct.2016.09.011>

<https://www.doi.org/10.1021/je800869g>

<https://www.doi.org/10.1016/j.jct.2017.01.004>

<https://www.doi.org/10.1016/j.jct.2005.10.001>

<https://www.doi.org/10.1021/je100352r>

<https://www.doi.org/10.1016/j.jct.2016.03.037>

<https://www.doi.org/10.1021/je060099a>

<https://www.doi.org/10.1016/j.jct.2016.09.036>

<https://www.doi.org/10.1021/je800371a>

<https://www.doi.org/10.1021/je7005924>

<https://www.doi.org/10.1016/j.jct.2004.12.006>

<https://www.doi.org/10.1016/j.jct.2013.09.012>

<https://www.doi.org/10.1016/j.jct.2016.09.015>

<https://www.doi.org/10.1016/j.tca.2013.02.007>

<https://www.doi.org/10.1016/j.jct.2016.10.037>

<https://www.doi.org/10.1021/je7000396>

<https://www.doi.org/10.1021/je7001094>

<https://www.doi.org/10.1021/je800742d>







<https://www.doi.org/10.1021/je800739y>  
<https://www.doi.org/10.1021/acs.jced.8b01105>  
<https://www.doi.org/10.1021/acs.jced.7b00316>  
<https://www.doi.org/10.1021/je900177h>  
<https://www.doi.org/10.1016/j.jct.2019.02.005>  
<https://www.doi.org/10.1021/acs.jced.8b01051>  
<https://www.doi.org/10.1016/j.jct.2016.11.029>  
<https://www.doi.org/10.1021/je0342771>  
<https://www.doi.org/10.1016/j.jct.2016.08.017>  
<https://www.doi.org/10.1016/j.jct.2016.08.013>  
<https://www.doi.org/10.1021/je800156m>  
<https://www.doi.org/10.1021/acs.jced.6b00150>  
<https://www.doi.org/10.1021/acs.jced.6b00816>  
<https://www.doi.org/10.1021/je300517q>  
<https://www.doi.org/10.1021/je200972w>  
<https://www.doi.org/10.1021/acs.jced.8b00309>  
<https://www.doi.org/10.1016/j.fluid.2018.06.003>  
<https://www.doi.org/10.1016/j.fluid.2018.06.008>  
<http://webbook.nist.gov/cgi/cbook.cgi?ID=C67641&Units=SI>  
[https://en.wikipedia.org/wiki/Joback\\_method](https://en.wikipedia.org/wiki/Joback_method)

<https://www.doi.org/10.1021/acs.jced.5b00980>  
<https://www.doi.org/10.1021/je900888e>  
<https://www.doi.org/10.1021/je100626x>  
<https://www.doi.org/10.1021/je900547w>  
<https://www.doi.org/10.1021/je800405b>  
<https://www.doi.org/10.1016/j.jct.2017.10.003>  
<https://www.doi.org/10.1016/j.jct.2017.12.015>  
<https://www.doi.org/10.1021/je8003639>  
<https://www.doi.org/10.1021/acs.jced.8b01062>  
<https://www.doi.org/10.1021/acs.jced.8b00536>  
<https://www.doi.org/10.1021/je301014d>  
<https://www.doi.org/10.1021/je800837z>  
<https://www.doi.org/10.1016/j.fluid.2008.06.006>  
<https://www.doi.org/10.1016/j.jct.2015.08.017>  
<https://www.doi.org/10.1016/j.jct.2012.04.013>  
<https://www.doi.org/10.1021/je100410k>  
<https://www.doi.org/10.1016/j.jct.2005.08.002>  
<https://www.doi.org/10.1021/je0602723>  
<https://www.doi.org/10.1016/j.jct.2015.04.025>  
<https://www.doi.org/10.1021/je034250h>  
<https://www.doi.org/10.1016/j.fluid.2012.09.027>  
<https://www.doi.org/10.1016/j.jct.2017.04.019>  
<https://www.doi.org/10.1016/j.jct.2016.06.028>



Isobaric Vapor Liquid Equilibrium for Acetone + Methanol + Phosphate Ionic Determination and Correlation of Solubility of Phenylbutazone in Measurements of Solubility of Mykrocin acetone solvate in aqueous solutions and excess properties of binary liquid mixtures of Polyamines Carbonic acid in Ethanol, 2-Propanol, Acetone, Benzene, and Tetralin and Interfacial Tension of Binary Organic Liquid Mixtures Equilibrium Solubility of Amidinothiourea in Monosolvents: Solubility of Ibuprofen from Model Different Solvents between 273 K and 323 K

<https://www.doi.org/10.1021/je5007373>  
<https://www.doi.org/10.1021/acs.jced.6b00911>  
<https://www.doi.org/10.1016/j.fluid.2008.10.016>  
<https://www.doi.org/10.1021/je034204h>  
<https://www.doi.org/10.1021/je060350m>  
<https://www.doi.org/10.1021/je034062r>  
<https://www.doi.org/10.1021/acs.jced.9b00458>  
<https://www.doi.org/10.1021/je700296x>

## Legend

<b>af:</b>	Acentric Factor
<b>affp:</b>	Proton affinity
<b>aigt:</b>	Autoignition Temperature
<b>basg:</b>	Gas basicity
<b>chg:</b>	Standard gas enthalpy of combustion
<b>chl:</b>	Standard liquid enthalpy of combustion
<b>cpg:</b>	Ideal gas heat capacity
<b>cpl:</b>	Liquid phase heat capacity
<b>cps:</b>	Solid phase heat capacity
<b>dm:</b>	Dipole Moment
<b>dvisc:</b>	Dynamic viscosity
<b>ea:</b>	Electron affinity
<b>fl:</b>	Lower Flammability Limit
<b>flu:</b>	Upper Flammability Limit
<b>fpc:</b>	Flash Point (Closed Cup Method)
<b>fpo:</b>	Flash Point (Open Cup Method)
<b>gf:</b>	Standard Gibbs free energy of formation
<b>gyrad:</b>	Radius of Gyration
<b>hf:</b>	Enthalpy of formation at standard conditions
<b>hfl:</b>	Liquid phase enthalpy of formation at standard conditions
<b>hfus:</b>	Enthalpy of fusion at standard conditions
<b>hfust:</b>	Enthalpy of fusion at a given temperature
<b>hvap:</b>	Enthalpy of vaporization at standard conditions
<b>hvapt:</b>	Enthalpy of vaporization at a given temperature
<b>ie:</b>	Ionization energy
<b>log10ws:</b>	Log10 of Water solubility in mol/l
<b>logp:</b>	Octanol/Water partition coefficient
<b>mcvol:</b>	McGowan's characteristic volume
<b>nfpaf:</b>	NFPA Fire Rating
<b>nfpah:</b>	NFPA Health Rating

<b>pc:</b>	Critical Pressure
<b>pvap:</b>	Vapor pressure
<b>rfi:</b>	Refractive Index
<b>rhoc:</b>	Critical density
<b>rho:</b>	Liquid Density
<b>rinpol:</b>	Non-polar retention indices
<b>ripol:</b>	Polar retention indices
<b>sfust:</b>	Entropy of fusion at a given temperature
<b>sl:</b>	Liquid phase molar entropy at standard conditions
<b>speedsl:</b>	Speed of sound in fluid
<b>srf:</b>	Surface Tension
<b>tb:</b>	Normal Boiling Point Temperature
<b>tbrp:</b>	Boiling point at reduced pressure
<b>tc:</b>	Critical Temperature
<b>tf:</b>	Normal melting (fusion) point
<b>tt:</b>	Triple Point Temperature
<b>vc:</b>	Critical Volume
<b>zc:</b>	Critical Compressibility
<b>zra:</b>	Rackett Parameter

Latest version available from:

<https://www.chemeo.com/cid/50-301-1/Acetone.pdf>

Generated by Cheméo on 2025-12-24 00:20:36.238447929 +0000 UTC m=+6283833.768488584.

Cheméo (<https://www.chemeo.com>) is the biggest free database of chemical and physical data for the process industry.