

Benzene, ethyl-

Other names:	.alpha.-methyltoluene Aethylbenzol EB Ethylbenzeen Ethylbenzol Etilbenzene Etylobenzen NCI-C56393 NSC 406903 UN 1175 ethylbenzene phenylethane «alpha»-Methyltoluene
Inchi:	InChI=1S/C8H10/c1-2-8-6-4-3-5-7-8/h3-7H,2H2,1H3
InchiKey:	YNQLUTRBYVCPMQ-UHFFFAOYSA-N
Formula:	C8H10
SMILES:	CCc1ccccc1
Mol. weight [g/mol]:	106.17
CAS:	100-41-4

Physical Properties

Property code	Value	Unit	Source
af	0.3020		KDB
affp	789.90	kJ/mol	NIST Webbook
affp	788.00	kJ/mol	NIST Webbook
aigt	733.15	K	KDB
basg	760.30	kJ/mol	NIST Webbook
basg	760.20	kJ/mol	NIST Webbook
chl	-4584.00	kJ/mol	NIST Webbook
chl	-4565.90	kJ/mol	NIST Webbook
chl	-4557.60	kJ/mol	NIST Webbook
chl	-4566.40	kJ/mol	NIST Webbook
chl	-4564.87 ± 0.71	kJ/mol	NIST Webbook
chl	-4562.40 ± 1.00	kJ/mol	NIST Webbook
cpl	185.44	J/mol×K	Thermodynamics of mixtures involving some (benzene derivatives + benzonitrile)

dm	0.40	debye	KDB
fil	1.00	% in Air	KDB
flu	6.70	% in Air	KDB
fpc	299.82	K	KDB
fpo	288.15	K	KDB
gf	130.70	kJ/mol	KDB
gyrad	3.8210		KDB
hcg	4564.87	kJ/mol	KDB
hcn	4344.792	kJ/mol	KDB
hf	29.81	kJ/mol	KDB
hf	69.30	kJ/mol	NIST Webbook
hf	49.00 ± 4.00	kJ/mol	NIST Webbook
hf	29.80 ± 0.84	kJ/mol	NIST Webbook
hfl	27.00	kJ/mol	NIST Webbook
hfl	6.80 ± 4.00	kJ/mol	NIST Webbook
hfl	-12.50 ± 0.84	kJ/mol	NIST Webbook
hfus	10.52	kJ/mol	Joback Method
hvap	42.26	kJ/mol	NIST Webbook
hvap	42.40 ± 0.10	kJ/mol	NIST Webbook
hvap	42.30	kJ/mol	NIST Webbook
hvap	42.20 ± 0.10	kJ/mol	NIST Webbook
hvap	42.24	kJ/mol	NIST Webbook
hvap	42.30	kJ/mol	NIST Webbook
hvap	36.00 ± 0.20	kJ/mol	NIST Webbook
ie	8.77	eV	NIST Webbook
ie	8.77 ± 0.01	eV	NIST Webbook
ie	9.38	eV	NIST Webbook
ie	8.77 ± 0.01	eV	NIST Webbook
ie	8.61	eV	NIST Webbook
ie	8.73	eV	NIST Webbook
ie	8.65 ± 0.10	eV	NIST Webbook
ie	8.76	eV	NIST Webbook
ie	8.77 ± 0.01	eV	NIST Webbook
ie	8.75 ± 0.05	eV	NIST Webbook
ie	8.77	eV	NIST Webbook
ie	8.76 ± 0.01	eV	NIST Webbook
log10ws	-2.77		Aqueous Solubility Prediction Method
log10ws	-2.77		Estimated Solubility Method
logp	2.249		Crippen Method
mvol	99.820	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=2)		KDB
pc	3649.00 ± 6.89	kPa	NIST Webbook

pc	3608.80 ± 5.00	kPa	NIST Webbook
pc	3609.00 ± 10.00	kPa	NIST Webbook
pc	3609.00	kPa	KDB
pc	3619.00 ± 41.37	kPa	NIST Webbook
pc	3609.00 ± 0.10	kPa	NIST Webbook
pc	3740.00 ± 7.84	kPa	NIST Webbook
rhoc	284.52 ± 1.06	kg/m3	NIST Webbook
rhoc	283.46 ± 4.25	kg/m3	NIST Webbook
rinpol	861.00		NIST Webbook
rinpol	866.85		NIST Webbook
rinpol	870.00		NIST Webbook
rinpol	857.00		NIST Webbook
rinpol	859.00		NIST Webbook
rinpol	857.00		NIST Webbook
rinpol	854.00		NIST Webbook
rinpol	854.00		NIST Webbook
rinpol	848.00		NIST Webbook
rinpol	845.00		NIST Webbook
rinpol	847.80		NIST Webbook
rinpol	848.20		NIST Webbook
rinpol	851.40		NIST Webbook
rinpol	859.00		NIST Webbook
rinpol	867.00		NIST Webbook
rinpol	854.00		NIST Webbook
rinpol	859.00		NIST Webbook
rinpol	864.00		NIST Webbook
rinpol	870.00		NIST Webbook
rinpol	821.00		NIST Webbook
rinpol	845.30		NIST Webbook
rinpol	847.70		NIST Webbook
rinpol	858.90		NIST Webbook
rinpol	864.20		NIST Webbook
rinpol	870.10		NIST Webbook
rinpol	846.00		NIST Webbook
rinpol	834.10		NIST Webbook
rinpol	839.50		NIST Webbook
rinpol	844.60		NIST Webbook
rinpol	844.60		NIST Webbook
rinpol	844.80		NIST Webbook
rinpol	845.30		NIST Webbook
rinpol	839.40		NIST Webbook
rinpol	840.60		NIST Webbook
rinpol	839.00		NIST Webbook
rinpol	839.20		NIST Webbook

rinpol	845.30	NIST Webbook
rinpol	847.70	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	844.00	NIST Webbook
rinpol	844.00	NIST Webbook
rinpol	855.20	NIST Webbook
rinpol	837.00	NIST Webbook
rinpol	839.00	NIST Webbook
rinpol	841.56	NIST Webbook
rinpol	864.00	NIST Webbook
rinpol	866.00	NIST Webbook
rinpol	870.00	NIST Webbook
rinpol	873.00	NIST Webbook
rinpol	868.00	NIST Webbook
rinpol	872.00	NIST Webbook
rinpol	875.00	NIST Webbook
rinpol	877.00	NIST Webbook
rinpol	880.00	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	835.00	NIST Webbook
rinpol	840.00	NIST Webbook
rinpol	849.10	NIST Webbook
rinpol	849.10	NIST Webbook
rinpol	849.10	NIST Webbook
rinpol	849.10	NIST Webbook
rinpol	849.10	NIST Webbook
rinpol	849.10	NIST Webbook
rinpol	847.70	NIST Webbook
rinpol	848.00	NIST Webbook
rinpol	843.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	852.00	NIST Webbook
rinpol	855.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	834.00	NIST Webbook
rinpol	848.00	NIST Webbook
rinpol	844.20	NIST Webbook
rinpol	851.30	NIST Webbook
rinpol	844.30	NIST Webbook
rinpol	879.00	NIST Webbook
rinpol	830.00	NIST Webbook
rinpol	836.00	NIST Webbook
rinpol	841.00	NIST Webbook

rinpol	846.00	NIST Webbook
rinpol	876.00	NIST Webbook
rinpol	884.00	NIST Webbook
rinpol	892.00	NIST Webbook
rinpol	868.00	NIST Webbook
rinpol	847.00	NIST Webbook
rinpol	853.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	843.00	NIST Webbook
rinpol	840.00	NIST Webbook
rinpol	844.00	NIST Webbook
rinpol	848.00	NIST Webbook
rinpol	864.10	NIST Webbook
rinpol	844.00	NIST Webbook
rinpol	853.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	843.00	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	851.00	NIST Webbook
rinpol	855.00	NIST Webbook
rinpol	857.00	NIST Webbook
rinpol	868.00	NIST Webbook
rinpol	855.60	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	866.00	NIST Webbook
rinpol	862.00	NIST Webbook
rinpol	879.00	NIST Webbook
rinpol	871.00	NIST Webbook
rinpol	868.00	NIST Webbook
rinpol	869.00	NIST Webbook
rinpol	854.00	NIST Webbook
rinpol	864.00	NIST Webbook
rinpol	864.00	NIST Webbook
rinpol	893.00	NIST Webbook
rinpol	850.80	NIST Webbook
rinpol	876.00	NIST Webbook
rinpol	856.30	NIST Webbook
rinpol	855.50	NIST Webbook
rinpol	853.20	NIST Webbook
rinpol	856.30	NIST Webbook
rinpol	857.20	NIST Webbook
rinpol	839.80	NIST Webbook
rinpol	868.30	NIST Webbook

rinpol	872.00	NIST Webbook
rinpol	860.00	NIST Webbook
rinpol	857.00	NIST Webbook
rinpol	865.00	NIST Webbook
rinpol	866.00	NIST Webbook
rinpol	865.00	NIST Webbook
rinpol	866.00	NIST Webbook
rinpol	856.00	NIST Webbook
rinpol	847.00	NIST Webbook
rinpol	855.00	NIST Webbook
rinpol	849.00	NIST Webbook
rinpol	834.00	NIST Webbook
rinpol	860.90	NIST Webbook
rinpol	836.10	NIST Webbook
rinpol	841.70	NIST Webbook
rinpol	846.10	NIST Webbook
rinpol	846.40	NIST Webbook
rinpol	861.50	NIST Webbook
rinpol	853.20	NIST Webbook
rinpol	856.30	NIST Webbook
rinpol	857.20	NIST Webbook
rinpol	856.30	NIST Webbook
rinpol	855.50	NIST Webbook
rinpol	844.19	NIST Webbook
rinpol	844.47	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	845.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	844.50	NIST Webbook
rinpol	844.74	NIST Webbook
rinpol	845.00	NIST Webbook
rinpol	864.00	NIST Webbook
rinpol	855.00	NIST Webbook
rinpol	848.30	NIST Webbook
rinpol	856.20	NIST Webbook
rinpol	848.30	NIST Webbook
rinpol	848.30	NIST Webbook
rinpol	856.20	NIST Webbook
rinpol	845.17	NIST Webbook
rinpol	845.49	NIST Webbook
rinpol	848.70	NIST Webbook
rinpol	844.80	NIST Webbook
rinpol	844.60	NIST Webbook
rinpol	841.26	NIST Webbook

rinpol	844.05	NIST Webbook
rinpol	845.90	NIST Webbook
rinpol	857.33	NIST Webbook
rinpol	860.40	NIST Webbook
rinpol	862.45	NIST Webbook
rinpol	843.00	NIST Webbook
rinpol	877.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	863.00	NIST Webbook
rinpol	865.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	870.79	NIST Webbook
rinpol	845.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	852.00	NIST Webbook
rinpol	855.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	864.00	NIST Webbook
rinpol	869.00	NIST Webbook
rinpol	853.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	847.00	NIST Webbook
rinpol	857.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	847.00	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	863.00	NIST Webbook
rinpol	864.00	NIST Webbook
rinpol	843.00	NIST Webbook
rinpol	843.00	NIST Webbook
rinpol	844.00	NIST Webbook
rinpol	844.00	NIST Webbook
rinpol	842.00	NIST Webbook
rinpol	842.00	NIST Webbook
rinpol	842.00	NIST Webbook
rinpol	852.00	NIST Webbook
rinpol	852.00	NIST Webbook
rinpol	852.00	NIST Webbook

rinpol	852.00	NIST Webbook
rinpol	852.00	NIST Webbook
rinpol	852.00	NIST Webbook
rinpol	853.00	NIST Webbook
rinpol	835.00	NIST Webbook
rinpol	847.00	NIST Webbook
rinpol	831.00	NIST Webbook
rinpol	838.00	NIST Webbook
rinpol	845.00	NIST Webbook
rinpol	849.00	NIST Webbook
rinpol	842.00	NIST Webbook
rinpol	856.00	NIST Webbook
rinpol	836.00	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	852.00	NIST Webbook
rinpol	857.00	NIST Webbook
rinpol	849.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	864.00	NIST Webbook
rinpol	845.00	NIST Webbook
rinpol	863.00	NIST Webbook
rinpol	851.00	NIST Webbook
rinpol	851.00	NIST Webbook
rinpol	866.00	NIST Webbook
rinpol	845.00	NIST Webbook
rinpol	861.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	863.30	NIST Webbook
rinpol	868.00	NIST Webbook
rinpol	829.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	886.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	866.00	NIST Webbook
rinpol	860.00	NIST Webbook
rinpol	865.00	NIST Webbook
rinpol	878.00	NIST Webbook
rinpol	855.00	NIST Webbook
rinpol	849.00	NIST Webbook
rinpol	847.66	NIST Webbook
rinpol	851.00	NIST Webbook
rinpol	847.00	NIST Webbook
rinpol	868.10	NIST Webbook

rinpol	843.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	852.00	NIST Webbook
rinpol	838.00	NIST Webbook
rinpol	841.00	NIST Webbook
rinpol	842.00	NIST Webbook
rinpol	856.00	NIST Webbook
rinpol	869.00	NIST Webbook
rinpol	843.00	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	848.00	NIST Webbook
rinpol	844.00	NIST Webbook
rinpol	844.00	NIST Webbook
rinpol	844.00	NIST Webbook
rinpol	868.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	835.30	NIST Webbook
rinpol	837.60	NIST Webbook
rinpol	840.80	NIST Webbook
rinpol	843.30	NIST Webbook
rinpol	845.30	NIST Webbook
rinpol	847.00	NIST Webbook
rinpol	835.00	NIST Webbook
rinpol	837.00	NIST Webbook
rinpol	840.00	NIST Webbook
rinpol	843.00	NIST Webbook
rinpol	845.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	842.00	NIST Webbook
rinpol	841.00	NIST Webbook
rinpol	845.00	NIST Webbook
rinpol	842.00	NIST Webbook
rinpol	860.00	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	864.00	NIST Webbook
rinpol	866.00	NIST Webbook
rinpol	852.00	NIST Webbook
rinpol	840.00	NIST Webbook
rinpol	867.00	NIST Webbook
rinpol	857.00	NIST Webbook
rinpol	868.00	NIST Webbook
rinpol	851.00	NIST Webbook

rinpol	870.00	NIST Webbook
rinpol	869.00	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	871.00	NIST Webbook
rinpol	855.00	NIST Webbook
rinpol	893.00	NIST Webbook
rinpol	855.00	NIST Webbook
rinpol	868.00	NIST Webbook
rinpol	868.00	NIST Webbook
rinpol	851.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	866.00	NIST Webbook
rinpol	851.00	NIST Webbook
rinpol	839.30	NIST Webbook
rinpol	869.00	NIST Webbook
rinpol	879.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	848.00	NIST Webbook
rinpol	868.00	NIST Webbook
rinpol	853.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	848.00	NIST Webbook
rinpol	854.00	NIST Webbook
rinpol	861.00	NIST Webbook
rinpol	854.00	NIST Webbook
rinpol	872.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	851.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	854.00	NIST Webbook
rinpol	854.00	NIST Webbook
rinpol	863.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	854.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	847.00	NIST Webbook
rinpol	849.00	NIST Webbook
rinpol	860.00	NIST Webbook
rinpol	859.10	NIST Webbook
rinpol	863.30	NIST Webbook
rinpol	862.80	NIST Webbook
rinpol	862.60	NIST Webbook
rinpol	847.50	NIST Webbook
rinpol	867.00	NIST Webbook

rinpol	844.00	NIST Webbook
rinpol	870.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	830.00	NIST Webbook
rinpol	840.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	848.00	NIST Webbook
rinpol	849.00	NIST Webbook
rinpol	864.00	NIST Webbook
rinpol	843.00	NIST Webbook
rinpol	118.80	NIST Webbook
rinpol	118.30	NIST Webbook
rinpol	134.54	NIST Webbook
rinpol	118.90	NIST Webbook
rinpol	129.41	NIST Webbook
rinpol	860.00	NIST Webbook
rinpol	840.00	NIST Webbook
rinpol	870.00	NIST Webbook
rinpol	893.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	879.00	NIST Webbook
rinpol	846.00	NIST Webbook
rinpol	872.00	NIST Webbook
rinpol	860.00	NIST Webbook
rinpol	833.30	NIST Webbook
rinpol	848.10	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	845.00	NIST Webbook
rinpol	852.00	NIST Webbook
rinpol	829.00	NIST Webbook
rinpol	847.66	NIST Webbook
rinpol	842.00	NIST Webbook
rinpol	848.00	NIST Webbook
rinpol	843.30	NIST Webbook
rinpol	841.00	NIST Webbook
rinpol	118.80	NIST Webbook
rinpol	850.60	NIST Webbook
rinpol	843.50	NIST Webbook
rinpol	875.40	NIST Webbook
rinpol	880.00	NIST Webbook
rinpol	847.60	NIST Webbook
rinpol	863.30	NIST Webbook
rinpol	834.60	NIST Webbook

rinpol	867.00	NIST Webbook
rinpol	821.00	NIST Webbook
rinpol	870.10	NIST Webbook
rinpol	844.60	NIST Webbook
rinpol	839.00	NIST Webbook
rinpol	844.00	NIST Webbook
rinpol	841.56	NIST Webbook
rinpol	868.00	NIST Webbook
rinpol	850.00	NIST Webbook
rinpol	849.10	NIST Webbook
rinpol	855.00	NIST Webbook
rinpol	851.30	NIST Webbook
rinpol	850.60	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	857.00	NIST Webbook
rinpol	838.50	NIST Webbook
rinpol	832.80	NIST Webbook
rinpol	860.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	840.00	NIST Webbook
rinpol	858.00	NIST Webbook
rinpol	839.80	NIST Webbook
rinpol	834.60	NIST Webbook
rinpol	849.70	NIST Webbook
rinpol	844.50	NIST Webbook
rinpol	846.80	NIST Webbook
rinpol	844.60	NIST Webbook
rinpol	857.00	NIST Webbook
rinpol	857.30	NIST Webbook
rinpol	843.40	NIST Webbook
rinpol	841.80	NIST Webbook
rinpol	843.50	NIST Webbook
rinpol	848.10	NIST Webbook
rinpol	847.00	NIST Webbook
rinpol	879.95	NIST Webbook
rinpol	847.30	NIST Webbook
rinpol	875.40	NIST Webbook
rinpol	848.34	NIST Webbook
rinpol	848.34	NIST Webbook
rinpol	859.20	NIST Webbook
rinpol	861.00	NIST Webbook
rinpol	847.00	NIST Webbook
rinpol	850.00	NIST Webbook

rinpol	848.00	NIST Webbook
rinpol	854.80	NIST Webbook
rinpol	871.10	NIST Webbook
rinpol	880.00	NIST Webbook
rinpol	847.80	NIST Webbook
rinpol	862.80	NIST Webbook
rinpol	848.10	NIST Webbook
rinpol	848.20	NIST Webbook
rinpol	847.60	NIST Webbook
rinpol	863.30	NIST Webbook
rinpol	858.40	NIST Webbook
rinpol	875.00	NIST Webbook
rinpol	849.00	NIST Webbook
rinpol	874.00	NIST Webbook
rinpol	848.00	NIST Webbook
rinpol	848.00	NIST Webbook
rinpol	848.00	NIST Webbook
rinpol	859.00	NIST Webbook
rinpol	859.00	NIST Webbook
ripol	1114.00	NIST Webbook
ripol	1146.00	NIST Webbook
ripol	1122.00	NIST Webbook
ripol	1116.00	NIST Webbook
ripol	1120.00	NIST Webbook
ripol	1135.00	NIST Webbook
ripol	1123.00	NIST Webbook
ripol	1138.00	NIST Webbook
ripol	1168.00	NIST Webbook
ripol	1115.00	NIST Webbook
ripol	1129.00	NIST Webbook
ripol	1116.00	NIST Webbook
ripol	1154.00	NIST Webbook
ripol	1158.40	NIST Webbook
ripol	1164.30	NIST Webbook
ripol	1100.00	NIST Webbook
ripol	1120.00	NIST Webbook
ripol	1117.00	NIST Webbook
ripol	1110.00	NIST Webbook
ripol	1117.00	NIST Webbook
ripol	1129.00	NIST Webbook
ripol	1132.00	NIST Webbook
ripol	1129.00	NIST Webbook
ripol	1131.00	NIST Webbook
ripol	1111.00	NIST Webbook

ripol	1129.00	NIST Webbook
ripol	1132.00	NIST Webbook
ripol	1109.00	NIST Webbook
ripol	1161.00	NIST Webbook
ripol	1138.00	NIST Webbook
ripol	1125.00	NIST Webbook
ripol	1127.00	NIST Webbook
ripol	1125.00	NIST Webbook
ripol	1121.00	NIST Webbook
ripol	1161.00	NIST Webbook
ripol	1130.00	NIST Webbook
ripol	1161.00	NIST Webbook
ripol	1119.00	NIST Webbook
ripol	1122.00	NIST Webbook
ripol	1127.00	NIST Webbook
ripol	1139.00	NIST Webbook
ripol	1134.00	NIST Webbook
ripol	1124.00	NIST Webbook
ripol	1124.00	NIST Webbook
ripol	1126.00	NIST Webbook
ripol	1128.00	NIST Webbook
ripol	1125.00	NIST Webbook
ripol	1135.00	NIST Webbook
ripol	1126.00	NIST Webbook
ripol	1116.00	NIST Webbook
ripol	1147.00	NIST Webbook
ripol	1108.00	NIST Webbook
ripol	1141.00	NIST Webbook
ripol	1118.00	NIST Webbook
ripol	1119.00	NIST Webbook
ripol	1122.00	NIST Webbook
ripol	1104.00	NIST Webbook
ripol	1161.00	NIST Webbook
ripol	1116.00	NIST Webbook
ripol	1130.00	NIST Webbook
ripol	1139.00	NIST Webbook
ripol	1142.00	NIST Webbook
ripol	1130.00	NIST Webbook
ripol	1130.00	NIST Webbook
ripol	1146.00	NIST Webbook
ripol	1111.00	NIST Webbook
ripol	1135.00	NIST Webbook
ripol	1125.00	NIST Webbook
ripol	1166.00	NIST Webbook

ripol	1157.00	NIST Webbook
ripol	1146.00	NIST Webbook
ripol	1144.00	NIST Webbook
ripol	1145.00	NIST Webbook
ripol	1126.00	NIST Webbook
ripol	1135.00	NIST Webbook
ripol	1180.00	NIST Webbook
ripol	1168.00	NIST Webbook
ripol	1157.00	NIST Webbook
ripol	1132.00	NIST Webbook
ripol	1132.00	NIST Webbook
ripol	1129.00	NIST Webbook
ripol	1122.00	NIST Webbook
ripol	1121.00	NIST Webbook
ripol	1125.00	NIST Webbook
ripol	1109.00	NIST Webbook
ripol	1125.00	NIST Webbook
ripol	1135.00	NIST Webbook
ripol	1133.00	NIST Webbook
ripol	1107.00	NIST Webbook
ripol	1132.00	NIST Webbook
ripol	1130.00	NIST Webbook
ripol	1123.00	NIST Webbook
ripol	1122.00	NIST Webbook
ripol	1128.00	NIST Webbook
ripol	1116.00	NIST Webbook
ripol	1130.00	NIST Webbook
ripol	1122.00	NIST Webbook
ripol	1098.00	NIST Webbook
ripol	1129.00	NIST Webbook
ripol	1125.00	NIST Webbook
ripol	1123.00	NIST Webbook
ripol	1125.00	NIST Webbook
ripol	1138.00	NIST Webbook
ripol	1124.00	NIST Webbook
ripol	1125.00	NIST Webbook
ripol	1125.00	NIST Webbook
ripol	1138.00	NIST Webbook
ripol	1168.00	NIST Webbook
ripol	1133.00	NIST Webbook
ripol	1118.00	NIST Webbook
ripol	1130.00	NIST Webbook
ripol	1115.00	NIST Webbook
ripol	1147.00	NIST Webbook

ripol	1138.00		NIST Webbook
ripol	1127.00		NIST Webbook
ripol	1131.00		NIST Webbook
ripol	1129.00		NIST Webbook
ripol	1129.00		NIST Webbook
ripol	1123.00		NIST Webbook
ripol	1146.10		NIST Webbook
ripol	1134.00		NIST Webbook
ripol	1125.00		NIST Webbook
ripol	1122.00		NIST Webbook
ripol	1100.00		NIST Webbook
ripol	1105.00		NIST Webbook
ripol	1138.00		NIST Webbook
ripol	1131.90		NIST Webbook
ripol	1158.90		NIST Webbook
ripol	1164.30		NIST Webbook
ripol	1169.80		NIST Webbook
ripol	1175.20		NIST Webbook
ripol	1136.00		NIST Webbook
ripol	1160.90		NIST Webbook
ripol	1158.40		NIST Webbook
ripol	1159.40		NIST Webbook
ripol	1127.10		NIST Webbook
ripol	1111.10		NIST Webbook
ripol	1178.00		NIST Webbook
ripol	1154.00		NIST Webbook
ripol	1162.00		NIST Webbook
ripol	1169.00		NIST Webbook
ripol	1115.00		NIST Webbook
sg	360.60 ± 0.50	J/mol×K	NIST Webbook
sl	256.10	J/mol×K	NIST Webbook
sl	255.01	J/mol×K	NIST Webbook
tb	409.34 ± 0.06	K	NIST Webbook
tb	136.10 ± 0.30	K	NIST Webbook
tb	409.25 ± 0.30	K	NIST Webbook
tb	409.10 ± 1.50	K	NIST Webbook
tb	407.00 ± 2.00	K	NIST Webbook
tb	412.45 ± 0.50	K	NIST Webbook
tb	408.80 ± 0.50	K	NIST Webbook
tb	409.00 ± 2.00	K	NIST Webbook
tb	409.35	K	Isobaric (vapour + liquid) equilibria for sulfolane with toluene, ethylbenzene, and isopropylbenzene at 101.33 kPa
tb	409.30 ± 0.20	K	NIST Webbook

tb	409.15 ± 2.00	K	NIST Webbook
tb	407.65 ± 2.00	K	NIST Webbook
tb	409.00 ± 2.00	K	NIST Webbook
tb	409.50 ± 0.30	K	NIST Webbook
tb	408.70 ± 1.50	K	NIST Webbook
tb	408.00 ± 4.00	K	NIST Webbook
tb	409.20 ± 0.25	K	NIST Webbook
tb	136.00 ± 0.50	K	NIST Webbook
tb	409.00 ± 2.00	K	NIST Webbook
tb	409.15 ± 2.00	K	NIST Webbook
tb	408.65 ± 2.00	K	NIST Webbook
tb	409.30 ± 0.25	K	NIST Webbook
tb	409.30 ± 0.50	K	NIST Webbook
tb	409.30 ± 0.50	K	NIST Webbook
tb	409.30 ± 0.30	K	NIST Webbook
tb	409.55 ± 0.70	K	NIST Webbook
tb	409.15 ± 1.00	K	NIST Webbook
tb	409.20 ± 0.15	K	NIST Webbook
tb	408.95 ± 1.00	K	NIST Webbook
tb	409.15 ± 1.50	K	NIST Webbook
tb	409.25 ± 0.50	K	NIST Webbook
tb	408.15 ± 1.50	K	NIST Webbook
tb	409.30 ± 0.10	K	NIST Webbook
tb	409.15 ± 2.00	K	NIST Webbook
tb	408.15 ± 1.50	K	NIST Webbook
tb	409.00 ± 4.00	K	NIST Webbook
tb	409.30 ± 0.30	K	NIST Webbook
tb	409.47 ± 0.10	K	NIST Webbook
tb	409.65 ± 0.30	K	NIST Webbook
tb	429.60	K	NIST Webbook
tb	409.15 ± 1.00	K	NIST Webbook
tb	409.30 ± 0.20	K	NIST Webbook
tb	409.55 ± 0.30	K	NIST Webbook
tb	409.10 ± 0.30	K	NIST Webbook
tb	409.35	K	Isobaric (vapour + liquid) equilibria for N-formylmorpholine with ethylbenzene, n-butylbenzene, iso-propylbenzene and 1,2,4-trimethylbenzene at 101.33 kPa

tb	409.32	K	Isobaric Vapor-Liquid Equilibrium for the Binary Systems of Methyl Formate with o-Xylene, m-Xylene, p-Xylene, and Ethylbenzene at 101.33 kPa
tb	409.25	K	Isobaric Vapor Liquid Equilibrium of Binary and Ternary Systems with 2-Ethoxyethanol + Ethylbenzene + Dimethyl Sulfoxide
tb	409.34	K	KDB
tb	409.15 ± 0.20	K	NIST Webbook
tb	409.40	K	NIST Webbook
tb	409.70 ± 0.30	K	NIST Webbook
tb	409.45 ± 0.50	K	NIST Webbook
tb	409.40 ± 0.20	K	NIST Webbook
tb	409.33 ± 0.01	K	NIST Webbook
tb	409.30 ± 0.30	K	NIST Webbook
tb	409.30 ± 0.40	K	NIST Webbook
tb	409.40 ± 0.15	K	NIST Webbook
tb	408.70 ± 0.40	K	NIST Webbook
tb	409.33 ± 0.10	K	NIST Webbook
tb	409.35 ± 0.50	K	NIST Webbook
tb	409.40 ± 0.50	K	NIST Webbook
tb	409.00 ± 2.00	K	NIST Webbook
tb	409.15 ± 1.00	K	NIST Webbook
tb	410.00 ± 2.00	K	NIST Webbook
tb	409.33 ± 0.02	K	NIST Webbook
tb	409.50 ± 0.50	K	NIST Webbook
tb	408.15 ± 2.00	K	NIST Webbook
tb	409.40 ± 0.50	K	NIST Webbook
tb	409.35 ± 0.13	K	NIST Webbook
tb	407.00 ± 3.00	K	NIST Webbook
tb	136.40 ± 0.40	K	NIST Webbook
tb	409.25 ± 0.70	K	NIST Webbook
tb	409.20 ± 0.50	K	NIST Webbook
tb	409.00 ± 4.00	K	NIST Webbook
tb	409.00 ± 4.00	K	NIST Webbook
tb	409.00 ± 4.00	K	NIST Webbook
tb	408.15 ± 1.50	K	NIST Webbook
tb	409.33 ± 0.25	K	NIST Webbook
tb	408.15 ± 2.00	K	NIST Webbook
tb	409.45 ± 0.40	K	NIST Webbook
tb	409.33 ± 0.30	K	NIST Webbook
tb	409.35 ± 0.30	K	NIST Webbook

tb	409.35 ± 0.25	K	NIST Webbook
tb	409.35 ± 0.30	K	NIST Webbook
tb	411.90 ± 2.00	K	NIST Webbook
tb	409.50 ± 0.30	K	NIST Webbook
tb	409.34 ± 0.30	K	NIST Webbook
tb	409.45 ± 0.30	K	NIST Webbook
tb	409.40 ± 0.60	K	NIST Webbook
tb	409.30 ± 0.20	K	NIST Webbook
tb	409.25 ± 0.30	K	NIST Webbook
tb	409.30 ± 0.20	K	NIST Webbook
tb	409.35 ± 0.20	K	NIST Webbook
tb	409.33 ± 0.20	K	NIST Webbook
tb	409.35	K	NIST Webbook
tb	409.33 ± 0.20	K	NIST Webbook
tb	409.00 ± 0.30	K	NIST Webbook
tb	409.35 ± 0.30	K	NIST Webbook
tb	409.30	K	NIST Webbook
tb	409.35 ± 0.10	K	NIST Webbook
tb	409.35 ± 0.10	K	NIST Webbook
tb	409.35 ± 0.30	K	NIST Webbook
tc	619.60 ± 2.00	K	NIST Webbook
tc	617.15	K	KDB
tc	617.20 ± 0.10	K	NIST Webbook
tc	617.20 ± 0.10	K	NIST Webbook
tc	617.10	K	NIST Webbook
tc	616.80 ± 0.50	K	NIST Webbook
tc	618.20 ± 0.70	K	NIST Webbook
tc	616.80 ± 0.50	K	NIST Webbook
tc	617.07 ± 0.10	K	NIST Webbook
tc	617.12 ± 0.20	K	NIST Webbook
tc	617.20 ± 0.40	K	NIST Webbook
tf	178.80 ± 0.50	K	NIST Webbook
tf	278.29	K	Phase Equilibria Study of the Binary Systems (N-Butyl-4-methylpyridinium Tosylate Ionic Liquid + Organic Solvent, or Water)
tf	178.10 ± 0.60	K	NIST Webbook
tf	181.15 ± 2.00	K	NIST Webbook
tf	171.90 ± 0.50	K	NIST Webbook
tf	178.06 ± 0.01	K	NIST Webbook
tf	179.50 ± 0.60	K	NIST Webbook
tf	178.20 ± 2.00	K	NIST Webbook
tf	178.15	K	NIST Webbook
tf	178.15 ± 0.20	K	NIST Webbook
tf	178.15 ± 0.20	K	NIST Webbook

tf	178.20	K	Aqueous Solubility Prediction Method
tf	178.20	K	KDB
tf	179.00 ± 1.00	K	NIST Webbook
tf	179.25 ± 0.40	K	NIST Webbook
tf	180.80 ± 1.00	K	NIST Webbook
tf	178.37 ± 0.06	K	NIST Webbook
tf	178.17 ± 0.03	K	NIST Webbook
tf	177.89 ± 0.15	K	NIST Webbook
tf	178.14 ± 0.15	K	NIST Webbook
tt	178.15 ± 0.02	K	NIST Webbook
tt	178.00 ± 0.30	K	NIST Webbook
tt	178.15 ± 0.02	K	NIST Webbook
tt	178.00 ± 0.30	K	NIST Webbook
vc	0.374	m3/kmol	KDB
vc	0.374	m3/kmol	NIST Webbook
zc	0.2630460		KDB
zra	0.26		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	159.24 ± 0.80	J/mol×K	373.15	NIST Webbook
cpg	164.25 ± 0.33	J/mol×K	385.65	NIST Webbook
cpg	169.25 ± 0.34	J/mol×K	398.15	NIST Webbook
cpg	178.96 ± 0.36	J/mol×K	423.15	NIST Webbook
cpg	188.28 ± 0.38	J/mol×K	448.15	NIST Webbook
cpg	197.35 ± 0.39	J/mol×K	473.15	NIST Webbook
cpg	205.94 ± 0.41	J/mol×K	498.15	NIST Webbook
cpg	214.02 ± 0.43	J/mol×K	523.15	NIST Webbook
cpl	181.60	J/mol×K	297.40	NIST Webbook
cpl	178.70	J/mol×K	302.80	NIST Webbook
cpl	185.78	J/mol×K	298.15	NIST Webbook
cpl	183.70	J/mol×K	298.50	NIST Webbook
cpl	186.60	J/mol×K	298.15	NIST Webbook
cpl	184.50	J/mol×K	298.00	NIST Webbook
cpl	178.70	J/mol×K	302.70	NIST Webbook
cpl	181.60	J/mol×K	303.00	NIST Webbook
cpl	184.80	J/mol×K	293.31	NIST Webbook
cpl	185.81	J/mol×K	298.15	NIST Webbook
cpl	186.04	J/mol×K	298.15	NIST Webbook

cpl	185.80	J/mol×K	298.00	NIST Webbook
cpl	161.00	J/mol×K	295.00	NIST Webbook
cpl	185.57	J/mol×K	298.15	NIST Webbook
cpl	185.56	J/mol×K	298.15	NIST Webbook
dvisc	0.0005060	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0003660	Pa×s	353.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure
dvisc	0.0005380	Pa×s	313.15	Thermophysical Properties of Isoamyl Acetate or Methyl Benzoate + Hydrocarbon Binary Mixtures, at (303.15 and 313.15) K
dvisc	0.0005970	Pa×s	303.15	Thermophysical Properties of Isoamyl Acetate or Methyl Benzoate + Hydrocarbon Binary Mixtures, at (303.15 and 313.15) K
dvisc	0.0004371	Pa×s	333.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K

dvisc	0.0004566	Pa×s	328.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0004805	Pa×s	323.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0005372	Pa×s	313.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0005652	Pa×s	308.15	Viscometric and Volumetric Properties of 10 Regular Binary Systems at 308.15 K and 313.15 K
dvisc	0.0005294	Pa×s	313.15	Viscometric and Volumetric Properties of 10 Regular Binary Systems at 308.15 K and 313.15 K
dvisc	0.0006793	Pa×s	293.15	Viscosities, Densities, and Ultrasonic Velocities of 3-Pentanone + Ethylbenzene and 3-Pentanone + o-Xylene at (293.15, 303.15, and 313.15) K

dvisc	0.0006006	Paxs	303.15	Viscosities, Densities, and Ultrasonic Velocities of 3-Pentanone + Ethylbenzene and 3-Pentanone + o-Xylene at (293.15, 303.15, and 313.15) K
dvisc	0.0005355	Paxs	313.15	Viscosities, Densities, and Ultrasonic Velocities of 3-Pentanone + Ethylbenzene and 3-Pentanone + o-Xylene at (293.15, 303.15, and 313.15) K
dvisc	0.0006380	Paxs	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for $C_mH_{2m+1}(OCH_2CH_2)_nOH$ (m) 1 or 2 or 4 and n) 1) + Benzene, + Toluene, + (o-, m-, and p-) Xylenes, + Ethylbenzene, and + Cyclohexane
dvisc	0.0005340	Paxs	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for $C_mH_{2m+1}(OCH_2CH_2)_nOH$ (m) 1 or 2 or 4 and n) 1) + Benzene, + Toluene, + (o-, m-, and p-) Xylenes, + Ethylbenzene, and + Cyclohexane

dvisc	0.0006299	Paxs	298.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Sulfolane with Benzene, Toluene, Ethylbenzene, p-Xylene, o-Xylene, and m-Xylene at 303.15 and 323.15 K and Atmospheric Pressure
dvisc	0.0005981	Paxs	303.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Sulfolane with Benzene, Toluene, Ethylbenzene, p-Xylene, o-Xylene, and m-Xylene at 303.15 and 323.15 K and Atmospheric Pressure
dvisc	0.0004829	Paxs	323.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Sulfolane with Benzene, Toluene, Ethylbenzene, p-Xylene, o-Xylene, and m-Xylene at 303.15 and 323.15 K and Atmospheric Pressure
dvisc	0.0005970	Paxs	303.15	Viscosity, Density, and Refractive Index of Some (Ester + Hydrocarbon) Binary Mixtures at 303.15 K and 313.15 K
dvisc	0.0005380	Paxs	313.15	Viscosity, Density, and Refractive Index of Some (Ester + Hydrocarbon) Binary Mixtures at 303.15 K and 313.15 K

dvisc	0.0005980	Pa×s	303.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure
dvisc	0.0005370	Pa×s	313.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure
dvisc	0.0004830	Pa×s	323.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure
dvisc	0.0004370	Pa×s	333.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure
dvisc	0.0003970	Pa×s	343.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure

dvisc	0.0005691	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
dvisc	0.0006280	Pa×s	298.15	Viscosities, Densities, and Ultrasonic Velocities of Binary Mixtures of Ethylbenzene with Ethanol, 1-Propanol, and 1-Butanol at (298.15 and 308.15)K
dvisc	0.0005530	Pa×s	308.15	Viscosities, Densities, and Ultrasonic Velocities of Binary Mixtures of Ethylbenzene with Ethanol, 1-Propanol, and 1-Butanol at (298.15 and 308.15)K
dvisc	0.0005986	Pa×s	303.15	Densities and Viscosities of Binary Mixtures of Vitamin K3 with Benzene, Toluene, Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene from (303.15 to 333.15) K
hfust	9.18	kJ/mol	178.15	NIST Webbook
hfust	9.16	kJ/mol	178.00	NIST Webbook
hfust	9.18	kJ/mol	178.15	NIST Webbook
hfust	9.16	kJ/mol	178.00	NIST Webbook
hfust	9.16	kJ/mol	178.20	NIST Webbook
hfust	9.16	kJ/mol	178.20	NIST Webbook
hfust	9.16	kJ/mol	178.17	NIST Webbook
hvapt	41.80	kJ/mol	359.00	NIST Webbook
hvapt	35.57	kJ/mol	409.30	NIST Webbook
hvapt	42.49	kJ/mol	294.01	NIST Webbook
hvapt	35.56	kJ/mol	409.20	KDB
hvapt	37.00	kJ/mol	434.00	NIST Webbook

hvapt	35.80	kJ/mol	505.50	NIST Webbook
hvapt	40.60	kJ/mol	360.00	NIST Webbook
hvapt	35.50	kJ/mol	583.00	NIST Webbook
hvapt	40.50 ± 0.10	kJ/mol	328.00	NIST Webbook
hvapt	39.50 ± 0.10	kJ/mol	343.00	NIST Webbook
hvapt	38.60 ± 0.10	kJ/mol	358.00	NIST Webbook
hvapt	40.00	kJ/mol	370.00	NIST Webbook
hvapt	42.49	kJ/mol	294.01	NIST Webbook
pvap	10.00	kPa	340.00	Isobaric Low-Pressure Vapor Liquid Equilibrium Data for Ethylbenzene + Styrene + Sulfolane and the Three Constituent Binary Systems
pvap	53.33	kPa	386.94	Isobaric Vapor-Liquid Equilibria of the Ternary System Toluene + Ethylbenzene + Amyl Acetate
pvap	26.66	kPa	365.86	Isobaric Vapor-Liquid Equilibria of the Ternary System Toluene + Ethylbenzene + Amyl Acetate
pvap	93.13	kPa	406.23	Refractive Index and Vapor-Liquid Equilibrium Data for the Binary Systems of Anisole with Xylene Isomers at 93.13 kPa
pvap	11.79	kPa	344.15	Vapour-liquid equilibrium for tripropylene glycol + aromatic hydrocarbons binary systems: Experimental data and regression
pvap	9.19	kPa	338.15	Vapour-liquid equilibrium for tripropylene glycol + aromatic hydrocarbons binary systems: Experimental data and regression

pvap	7.09	kPa	332.15	Vapour-liquid equilibrium for tripropylene glycol + aromatic hydrocarbons binary systems: Experimental data and regression
pvap	5.41	kPa	326.15	Vapour-liquid equilibrium for tripropylene glycol + aromatic hydrocarbons binary systems: Experimental data and regression
pvap	4.08	kPa	320.15	Vapour-liquid equilibrium for tripropylene glycol + aromatic hydrocarbons binary systems: Experimental data and regression
pvap	85.64	kPa	403.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	47.75	kPa	383.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	29.11	kPa	368.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression

pvap	20.42	kPa	358.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	13.79	kPa	348.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	11.41	kPa	343.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	9.25	kPa	338.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	7.45	kPa	333.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	5.97	kPa	328.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression

pvap	4.71	kPa	323.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	3.75	kPa	318.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	2.10	kPa	313.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	2.22	kPa	308.15	Vapor-liquid equilibrium for the binary mixtures of dipropylene glycol with aromatic hydrocarbons: Experimental and regression
pvap	95.30	kPa	406.95	Vapor-liquid equilibrium for the binary mixtures of dimethylsulfoxide with substituted benzenes
pvap	93.32	kPa	406.12	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	79.99	kPa	400.51	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components

pvap	66.66	kPa	394.14	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	53.33	kPa	386.69	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	40.00	kPa	377.54	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	79.99	kPa	400.70	Isobaric Vapor-Liquid Equilibria of the Ternary System Toluene + Ethylbenzene + Amyl Acetate
pvap	681.00	kPa	498.15	High-Temperature VLE for the Ethylbenzene + Quinoline System
pvap	1027.00	kPa	523.15	High-Temperature VLE for the Ethylbenzene + Quinoline System
pvap	1601.00	kPa	553.15	High-Temperature VLE for the Ethylbenzene + Quinoline System
pvap	2387.00	kPa	583.15	High-Temperature VLE for the Ethylbenzene + Quinoline System
pvap	3451.00	kPa	613.15	High-Temperature VLE for the Ethylbenzene + Quinoline System

pvap	5.00	kPa	324.40	Isobaric Low-Pressure Vapor Liquid Equilibrium Data for Ethylbenzene + Styrene + Sulfolane and the Three Constituent Binary Systems
pvap	7.50	kPa	333.40	Isobaric Low-Pressure Vapor Liquid Equilibrium Data for Ethylbenzene + Styrene + Sulfolane and the Three Constituent Binary Systems
pvap	12.50	kPa	345.50	Isobaric Low-Pressure Vapor Liquid Equilibrium Data for Ethylbenzene + Styrene + Sulfolane and the Three Constituent Binary Systems
pvap	15.00	kPa	350.10	Isobaric Low-Pressure Vapor Liquid Equilibrium Data for Ethylbenzene + Styrene + Sulfolane and the Three Constituent Binary Systems
pvap	17.50	kPa	354.10	Isobaric Low-Pressure Vapor Liquid Equilibrium Data for Ethylbenzene + Styrene + Sulfolane and the Three Constituent Binary Systems
pvap	20.00	kPa	357.70	Isobaric Low-Pressure Vapor Liquid Equilibrium Data for Ethylbenzene + Styrene + Sulfolane and the Three Constituent Binary Systems

pvap	22.50	kPa	360.90	Isobaric Low-Pressure Vapor Liquid Equilibrium Data for Ethylbenzene + Styrene + Sulfolane and the Three Constituent Binary Systems
pvap	25.00	kPa	363.80	Isobaric Low-Pressure Vapor Liquid Equilibrium Data for Ethylbenzene + Styrene + Sulfolane and the Three Constituent Binary Systems
pvap	250.00	kPa	447.20	Isobaric Vapor Liquid Equilibrium for Binary Systems of 2,2,4-Trimethylpentane with o-Xylene, m-Xylene, p-Xylene, and Ethylbenzene at 250 kPa
rfi	1.49304		298.15	Density, Speed of Sound, and Refractive Index of the Binary Systems Cyclohexane (1) or Methylcyclohexane (1) or Cyclo-octane (1) with Benzene (2), Toluene (2), and Ethylbenzene (2) at Two Temperatures
rfi	1.49316		298.15	Effect of Temperature on the Change of Refractive Index on Mixing for Butyl Acetate + Aromatic Hydrocarbons
rfi	1.49320		298.15	KDB

rfi	1.49304	298.15	Effect of the Chain Length on the Aromatic Ring in the Separation of Aromatic Compounds from Methylcyclohexane Using the Ionic Liquid 1-Ethyl-3-methylpyridinium Ethylsulfate
rfi	1.49304	298.15	Liquid-Liquid Equilibrium for Ternary Mixtures of Hexane + Aromatic Compounds + [EMpy][ESO4] at T = 298.15 K
rfi	1.50129	283.15	Density, Speed of Sound, and Refractive Index of the Binary Systems Cyclohexane (1) or Methylcyclohexane (1) or Cyclo-octane (1) with Benzene (2), Toluene (2), and Ethylbenzene (2) at Two Temperatures
rfi	1.50090	293.15	Solubilities of Methyl-diphenylphosphine Oxide in Selected Solvents
rfi	1.49304	298.15	Liquid-Liquid Extraction of Aromatic Compounds from Cycloalkanes Using 1-Butyl-3-methylimidazolium Methylsulfate Ionic Liquid
rfi	1.49320	298.15	Isobaric Vapor-Liquid Equilibria for the Binary Mixtures of Styrene with Ethylbenzene, o-Xylene, m-Xylene, and p-Xylene

rfi	1.49600	293.15	Activity Coefficients at Infinite Dilution of Cyclohexylamine + Octane, Toluene, Ethylbenzene, or Aniline and Excess Molar Volumes in Binary Mixtures of Cyclohexylamine + Heptane, Octane, Nonane, Decane, Undecane, Aniline, or Water
rfi	1.49020	303.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of Anisole with Benzene, Methylbenzene, Ethylbenzene, Propylbenzene, and Butylbenzene at (293.15 and 303.15) K
rfi	1.49570	293.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of Anisole with Benzene, Methylbenzene, Ethylbenzene, Propylbenzene, and Butylbenzene at (293.15 and 303.15) K
rfi	1.49550	293.15	Infinite Dilution Activity Coefficients of Hydrocarbons in Triethylene Glycol and Tetraethylene Glycol
rfi	1.49300	298.15	Experimental and correlational study of phase equilibria in aqueous mixtures of phosphoric acid with aromatic hydrocarbons at various temperatures

rfi	1.49220	293.15	Volumetric properties of binary mixtures of tributylamine with benzene derivatives and comparison with ERAS model results at temperatures from (293.15 to 333.15) K
rfi	1.49304	298.15	(Liquid + liquid) equilibrium data for the ternary systems (cycloalkane + ethylbenzene + 1-ethyl-3-methylimidazolium ethylsulfate) at T = 298.15 K and atmospheric pressure
rfi	1.49620	293.10	A study on densities and excess volumes in the (c-butyrolactone + aromatic hydrocarbon) system at various temperatures
rfi	1.49620	298.15	Densities and excess volumes of binary mixtures of N,N-dimethylformamide with aromatic hydrocarbon at different temperature
rfi	1.49620	293.10	Densities and volumetric properties of N-methyl-2-pyrrolidone with aromatic hydrocarbon at different temperature
rfi	1.54395	293.15	Bubble points of the binary mixtures formed by ethylbenzene with some chloroaliphatics and substituted benzenes at p = 94.7 kPa

rfi	1.49620	298.15	The volumetric properties of (1,2-propanediol carbonate + benzene, or toluene, or styrene) binary mixtures at temperatures from T = 293.15 K to T = 353.15 K
rfi	1.49310	298.15	Excess Molar Volumes of (propiophenone + benzene, or toluene, or ethylbenzene, or butylbenzene) at temperatures 298.15 K and 328.15 K
rfi	1.49620	293.15	A study of densities and volumetric properties of binary mixtures containing nitrobenzene at T = (293.15 to 353.15) K
rfi	1.49320	298.15	Bubble temperature measurements on seven binary mixtures formed by ethylbenzene at 94.7 kPa
rfi	1.49620	293.15	Experimental densities and excess volumes for binary mixtures of (dimethyl sulfoxide + an aromatic hydrocarbon) at temperatures from (293.15 to 353.15) K at atmospheric pressure
rfi	1.49620	293.15	Effect of temperature on the volumetric properties of (cyclohexanone + an aromatic hydrocarbon)

rhoI	862.70	kg/m3	298.15	Densities and Kinematic Viscosities of One Quinary Regular Liquid System and Its Five Quaternary Sub-Systems at Temperatures (293.15 and 298.15) K
rhoI	853.68	kg/m3	308.15	Experimental density, viscosity, interfacial tension and water solubility of ethyl benzene - a-methyl benzyl alcohol - water system
rhoI	862.37	kg/m3	298.15	Experimental Study of the Dynamic Viscosity Deviations in the Binary Systems: Hexane + Ethylbenzene, + o-Xylene, + m-Xylene, + p-Xylene at 298.15 K
rhoI	867.10	kg/m3	293.15	Densities and Kinematic Viscosities of One Quinary Regular Liquid System and Its Five Quaternary Sub-Systems at Temperatures (293.15 and 298.15) K
rhoI	862.70	kg/m3	298.15	The density, the refractive index and the adjustment of the excess thermodynamic properties by means of the multiple linear regression method for the ternary system ethylbenzene-octane-propylbenzene

rhoI	867.10	kg/m3	293.15	Densities and Kinematic Viscosities of a Quinary Regular Liquid System and Its Five Quaternary Subsystems at 293.15A K and 298.15A K
rhoI	862.70	kg/m3	298.15	Densities and Kinematic Viscosities of a Quinary Regular Liquid System and Its Five Quaternary Subsystems at 293.15A K and 298.15A K
rhoI	862.55	kg/m3	298.15	Thermodynamic study of 1,1,2,2-tetrachloroethane + hydrocarbon mixtures I. Excess and solvation enthalpies
rhoI	862.97	kg/m3	298.15	Phase behaviour of ionic liquid 1-butyl-1-methylpyrrolidinium tris(pentafluoroethyl)trifluorophosphate with alcohols, water and aromatic hydrocarbons
rhoI	862.97	kg/m3	298.15	Phase behaviour of tricyanomethanide-based ionic liquids with alcohols and hydrocarbons
rhoI	862.50	kg/m3	298.15	Bubble point measurements of binary mixtures formed by ethyl benzene with selected compounds at 95.35 kPa
rhoI	867.20	kg/m3	293.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K

rhoI	858.30	kg/m3	303.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhoI	849.30	kg/m3	313.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhoI	840.30	kg/m3	323.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhoI	831.20	kg/m3	333.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhoI	822.10	kg/m3	343.15	Densities and volumetric properties of (N-acetylmorpholine + aromatic hydrocarbon) binary mixtures from T = (293.15 to 343.15) K
rhoI	863.54	kg/m3	298.15	Separation of ethylbenzene/styrene systems using ionic liquids in ternary LLE
rhoI	862.58	kg/m3	298.15	The physicochemical properties of 1,3,5-trimethyl-1,3,5-tris(3,3,3-trifluoropropyl)cyclotrisiloxane with various aromatic hydrocarbons at T = (308.15 to 323.15) K

rhoI	840.28	kg/m3	323.15	The physicochemical properties of 1,3,5-trimethyl-1,3,5-tris(3,3,3-trifluoropropyl)cyclotrisiloxane with various aromatic hydrocarbons at T = (308.15 to 323.15) K
rhoI	844.70	kg/m3	318.15	The physicochemical properties of 1,3,5-trimethyl-1,3,5-tris(3,3,3-trifluoropropyl)cyclotrisiloxane with various aromatic hydrocarbons at T = (308.15 to 323.15) K
rhoI	849.29	kg/m3	313.15	The physicochemical properties of 1,3,5-trimethyl-1,3,5-tris(3,3,3-trifluoropropyl)cyclotrisiloxane with various aromatic hydrocarbons at T = (308.15 to 323.15) K
rhoI	853.71	kg/m3	308.15	The physicochemical properties of 1,3,5-trimethyl-1,3,5-tris(3,3,3-trifluoropropyl)cyclotrisiloxane with various aromatic hydrocarbons at T = (308.15 to 323.15) K
rhoI	835.94	kg/m3	328.15	Thermophysical properties of binary mixtures of triethoxysilane, methyltriethoxysilane, vinyltriethoxysilane and 3-mercaptopropyltriethoxysilane with ethylbenzene at various temperatures
rhoI	844.89	kg/m3	318.15	Thermophysical properties of binary mixtures of triethoxysilane, methyltriethoxysilane, vinyltriethoxysilane and 3-mercaptopropyltriethoxysilane with ethylbenzene at various temperatures

rhoI	853.77	kg/m3	308.15	Thermophysical properties of binary mixtures of triethoxysilane, methyltriethoxysilane, vinyltriethoxysilane and 3-mercaptopropyltriethoxysilane with ethylbenzene at various temperatures
rhoI	862.59	kg/m3	298.15	Thermophysical properties of binary mixtures of triethoxysilane, methyltriethoxysilane, vinyltriethoxysilane and 3-mercaptopropyltriethoxysilane with ethylbenzene at various temperatures
rhoI	871.33	kg/m3	288.15	Thermophysical properties of binary mixtures of triethoxysilane, methyltriethoxysilane, vinyltriethoxysilane and 3-mercaptopropyltriethoxysilane with ethylbenzene at various temperatures
rhoI	862.51	kg/m3	298.15	(Liquid + liquid) equilibrium at T = 298.15 K for ternary mixtures of alkane + aromatic compounds + imidazolium-based ionic liquids
rhoI	858.16	kg/m3	303.15	The density, refractive index, and thermodynamic behaviour of binary mixtures of 1,3-Diethenyl-1,1,3,3-tetramethyldisiloxane with aromatic hydrocarbons

rhoI	862.58	kg/m3	298.15	The density, refractive index, and thermodynamic behaviour of binary mixtures of 1,3-Diethenyl-1,1,3,3-tetramethyldisiloxane with aromatic hydrocarbons	
rhoI	866.90	kg/m3	293.15	The density, refractive index, and thermodynamic behaviour of binary mixtures of 1,3-Diethenyl-1,1,3,3-tetramethyldisiloxane with aromatic hydrocarbons	
rhoI	871.31	kg/m3	288.15	Effect of temperature and composition on the density, refractive index, and excess quantities of binary mixtures of 2,4,6,8-tetramethyl-2,4,6,8-tetraethenylcyclotetrasiloxane with aromatic hydrocarbons	
rhoI	867.00	kg/m3	293.00	KDB	
rhoI	862.50	kg/m3	298.15	Density, Speed of Sound, and Refractive Index for Binary Mixtures Containing Cycloalkanes and Aromatic Compounds at T = 313.15 K	
rhoI	862.55	kg/m3	298.15	Excess Enthalpies of Chloroalkylbenzene + Alkylbenzene Mixtures	
rhoI	794.20	kg/m3	373.15	Density, Viscosity, Speed of Sound, Bulk Modulus, Surface Tension, and Flash Point of Binary Mixtures of n-Hexadecane + Ethylbenzene or + Toluene at (293.15 to 373.15) K and 0.1 MPa	

rhoI	803.70	kg/m3	363.15	Density, Viscosity, Speed of Sound, Bulk Modulus, Surface Tension, and Flash Point of Binary Mixtures of n-Hexadecane + Ethylbenzene or + Toluene at (293.15 to 373.15) K and 0.1 MPa
rhoI	813.10	kg/m3	353.15	Density, Viscosity, Speed of Sound, Bulk Modulus, Surface Tension, and Flash Point of Binary Mixtures of n-Hexadecane + Ethylbenzene or + Toluene at (293.15 to 373.15) K and 0.1 MPa
rhoI	822.30	kg/m3	343.15	Density, Viscosity, Speed of Sound, Bulk Modulus, Surface Tension, and Flash Point of Binary Mixtures of n-Hexadecane + Ethylbenzene or + Toluene at (293.15 to 373.15) K and 0.1 MPa
rhoI	831.40	kg/m3	333.15	Density, Viscosity, Speed of Sound, Bulk Modulus, Surface Tension, and Flash Point of Binary Mixtures of n-Hexadecane + Ethylbenzene or + Toluene at (293.15 to 373.15) K and 0.1 MPa
rhoI	840.38	kg/m3	323.15	Density, Viscosity, Speed of Sound, Bulk Modulus, Surface Tension, and Flash Point of Binary Mixtures of n-Hexadecane + Ethylbenzene or + Toluene at (293.15 to 373.15) K and 0.1 MPa

rhoI	849.29	kg/m3	313.15	Density, Viscosity, Speed of Sound, Bulk Modulus, Surface Tension, and Flash Point of Binary Mixtures of n-Hexadecane + Ethylbenzene or + Toluene at (293.15 to 373.15) K and 0.1 MPa
rhoI	858.15	kg/m3	303.15	Density, Viscosity, Speed of Sound, Bulk Modulus, Surface Tension, and Flash Point of Binary Mixtures of n-Hexadecane + Ethylbenzene or + Toluene at (293.15 to 373.15) K and 0.1 MPa
rhoI	866.95	kg/m3	293.15	Density, Viscosity, Speed of Sound, Bulk Modulus, Surface Tension, and Flash Point of Binary Mixtures of n-Hexadecane + Ethylbenzene or + Toluene at (293.15 to 373.15) K and 0.1 MPa
rhoI	862.57	kg/m3	298.15	Vapor Liquid Equilibrium for 2-Methyl-1-butanol + Ethylbenzene + Xylene Isomers at 101.33 kPa
rhoI	866.54	kg/m3	293.15	Isobaric vapor liquid equilibrium for the binary systems of 1-butanol with o-xylene, m-xylene, p-xylene, and ethylbenzene at 101.33 kPa
rhoI	862.59	kg/m3	298.15	Liquid-Liquid Equilibria in Ternary Systems of Aromatic Hydrocarbons (Toluene or Ethylbenzene) + Phenols + Water

rhoI	867.10	kg/m3	293.10	Vapor-Liquid Equilibria Data for Binary Systems of Ethylbenzene + Xylene Isomers at 100.65 kPa
rhoI	862.50	kg/m3	298.15	Thermodynamics of Ternary Liquid Mixtures Containing Toluene, Ethylbenzene, and Chlorobenzene
rhoI	862.50	kg/m3	298.15	Excess Molar Enthalpies for Dimethyl Carbonate with o-Xylene, m-Xylene, p-Xylene, Ethylbenzene or Ethyl Benzoate at 298.15 K and 10.2 MPa
rhoI	862.50	kg/m3	298.15	Excess Molar Enthalpies of Dimethyl Carbonate with o-Xylene, m-Xylene, p-Xylene, Ethylbenzene, or Ethyl Benzoate at 298.15 K
rhoI	862.70	kg/m3	298.15	Isobaric Vapor-Liquid Equilibrium for Binary and Ternary Systems of 2-Methoxyethanol, Ethylbenzene, and Dimethyl Sulfoxide at 100.00 kPa
rhoI	862.51	kg/m3	298.15	Liquid Phase Equilibria of Aqueous Mixtures of Carboxylic Acids (C1-C4) with Ethylbenzene: Thermodynamic and Mathematical Modeling

rhoI	871.30	kg/m3	288.15	The density, refractive index, and thermodynamic behaviour of binary mixtures of 1,3-Diethenyl-1,1,3,3-tetramethyldisiloxane with aromatic hydrocarbons
rhoI	862.57	kg/m3	298.15	Isobaric Vapor Liquid Equilibrium for the Binary Systems of Diethyl Carbonate with Xylene Isomers and Ethylbenzene at 101.33 kPa
rhoI	844.80	kg/m3	318.15	The density, the refractive index and the adjustment of the excess thermodynamic properties by means of the multiple linear regression method for the ternary system ethylbenzene-octane-propylbenzene
rhoI	853.80	kg/m3	308.15	The density, the refractive index and the adjustment of the excess thermodynamic properties by means of the multiple linear regression method for the ternary system ethylbenzene-octane-propylbenzene
rhoI	875.69	kg/m3	283.15	The density, refractive index, and thermodynamic behaviour of binary mixtures of 1,3-Diethenyl-1,1,3,3-tetramethyldisiloxane with aromatic hydrocarbons

rhoI	862.51	kg/m3	298.15	Phase behavior of ternary mixtures {aliphatic hydrocarbon + aromatic hydrocarbon + ionic liquid}: Experimental LLE data and their modeling by COSMO-RS
rhoI	849.26	kg/m3	313.15	Experimental density, viscosity, interfacial tension and water solubility of ethyl benzene - a-methyl benzyl alcohol - water system
rhoI	853.75	kg/m3	308.15	Effect of temperature and composition on the density, refractive index, and excess quantities of binary mixtures of 2,4,6,8-tetramethyl-2,4,6,8-tetraethenylcyclotetrasiloxane with aromatic hydrocarbons
rhoI	858.10	kg/m3	303.15	Experimental density, viscosity, interfacial tension and water solubility of ethyl benzene - a-methyl benzyl alcohol - water system
rhoI	862.51	kg/m3	298.15	Experimental density, viscosity, interfacial tension and water solubility of ethyl benzene - a-methyl benzyl alcohol - water system

rhoI	853.61	kg/m3	308.15	Acoustic and thermodynamic properties of binary mixtures of 1-nonanol with o-xylene, m-xylene, p-xylene, ethylbenzene and mesitylene at T = (298.15 and 308.15) K
rhoI	862.43	kg/m3	298.15	Acoustic and thermodynamic properties of binary mixtures of 1-nonanol with o-xylene, m-xylene, p-xylene, ethylbenzene and mesitylene at T = (298.15 and 308.15) K
rhoI	862.55	kg/m3	298.15	Effect of temperature and composition on the density, refractive index, and excess quantities of binary mixtures of 2,4,6,8-tetramethyl-2,4,6,8-tetraethenylcyclotetrasiloxane with aromatic hydrocarbons
rhoI	835.93	kg/m3	328.15	Effect of temperature and composition on the density, refractive index, and excess quantities of binary mixtures of 2,4,6,8-tetramethyl-2,4,6,8-tetraethenylcyclotetrasiloxane with aromatic hydrocarbons

rhoI	844.87	kg/m3	318.15	Effect of temperature and composition on the density, refractive index, and excess quantities of binary mixtures of 2,4,6,8-tetramethyl-2,4,6,8-tetraethenylcyclotetrasiloxane with aromatic hydrocarbons
sfust	51.48	J/mol×K	178.00	NIST Webbook
sfust	51.54	J/mol×K	178.15	NIST Webbook
sfust	51.43	J/mol×K	178.17	NIST Webbook
sfust	51.48	J/mol×K	178.00	NIST Webbook
sfust	51.54	J/mol×K	178.15	NIST Webbook
speedsl	1246.12	m/s	315.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1236.06	m/s	318.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1360.73	m/s	288.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1349.91	m/s	290.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1339.40	m/s	293.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives

speedsl	1328.86	m/s	295.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1318.36	m/s	298.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1307.90	m/s	300.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1297.48	m/s	303.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1287.09	m/s	305.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1276.75	m/s	308.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1266.54	m/s	310.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1316.23	m/s	298.15	Temperature influence on mixing properties of {ethyl tert-butyl ether (ETBE) + gasoline additives}

speedsl	1256.29	m/s	313.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1213.59	m/s	323.15	Temperature influence on mixing properties of {ethyl tert-butyl ether (ETBE) + gasoline additives}
speedsl	1359.11	m/s	288.15	Temperature influence on mixing properties of {ethyl tert-butyl ether (ETBE) + gasoline additives}
speedsl	1226.09	m/s	320.65	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives
speedsl	1257.00	m/s	313.15	Densities, Speeds of Sound, and Isentropic Compressibilities of Binary Mixtures of {Alkan-1-ols + 1,2-Dimethylbenzene, or 1,3-Dimethylbenzene, or 1,4-Dimethylbenzene, or Ethylbenzene} at (293.15, 303.15, and 313.15) K
speedsl	1298.00	m/s	303.15	Densities, Speeds of Sound, and Isentropic Compressibilities of Binary Mixtures of {Alkan-1-ols + 1,2-Dimethylbenzene, or 1,3-Dimethylbenzene, or 1,4-Dimethylbenzene, or Ethylbenzene} at (293.15, 303.15, and 313.15) K

speedsl	1340.00	m/s	293.15	Densities, Speeds of Sound, and Isentropic Compressibilities of Binary Mixtures of {Alkan-1-ols + 1,2-Dimethylbenzene, or 1,3-Dimethylbenzene, or 1,4-Dimethylbenzene, or Ethylbenzene} at (293.15, 303.15, and 313.15) K
speedsl	1276.00	m/s	308.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene
speedsl	1319.00	m/s	298.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene
speedsl	1216.34	m/s	323.15	Influence of Temperature on Thermodynamic Properties of Methyl t-Butyl Ether (MTBE)+Gasoline Additives

srf	0.03	N/m	323.15	Thermo Physical Properties of 4-Hydroxy 4-Methyl Pentanone with Nitrobenzene or Ethyl Benzene at Temperatures of (303.15, 313.15, and 323.15) K and a Pressure of 0.1 MPa
srf	0.03	N/m	313.15	Thermo Physical Properties of 4-Hydroxy 4-Methyl Pentanone with Nitrobenzene or Ethyl Benzene at Temperatures of (303.15, 313.15, and 323.15) K and a Pressure of 0.1 MPa
srf	0.03	N/m	293.20	KDB
srf	0.03	N/m	298.15	Densities and Surface Tensions of Propyl Acetate + Xylenes or + Ethylbenzene from (298.15 to 308.15) K
srf	0.03	N/m	303.15	Densities and Surface Tensions of Propyl Acetate + Xylenes or + Ethylbenzene from (298.15 to 308.15) K
srf	0.03	N/m	308.15	Densities and Surface Tensions of Propyl Acetate + Xylenes or + Ethylbenzene from (298.15 to 308.15) K
srf	0.03	N/m	303.15	Thermo Physical Properties of 4-Hydroxy 4-Methyl Pentanone with Nitrobenzene or Ethyl Benzene at Temperatures of (303.15, 313.15, and 323.15) K and a Pressure of 0.1 MPa
svapt	144.50	J/mol×K	294.01	NIST Webbook
svapt	144.50	J/mol×K	294.01	NIST Webbook

tcondl	0.13	W/m×K	296.42	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.13	W/m×K	277.65	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	329.41	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	329.66	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	329.05	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

tcondl	0.14	W/m×K	258.50	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.13	W/m×K	277.34	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.14	W/m×K	258.00	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.13	W/m×K	277.88	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.13	W/m×K	295.86	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

tcondl	0.13	W/m×K	296.19	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.14	W/m×K	258.29	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	312.38	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	312.72	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	312.96	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbp	408.75	K	95.30	Excess enthalpies of dimethylsulfoxide with substituted benzenes at 298.15K

Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.44625e+01
Coeff. B	-3.59099e+03
Coeff. C	-4.45680e+01
Temperature range (K), min.	297.90
Temperature range (K), max.	436.98

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C*\ln(T) + D*T^2$
Coeff. A	7.97937e+01
Coeff. B	-7.63808e+03
Coeff. C	-9.55398e+00
Coeff. D	5.65318e-06
Temperature range (K), min.	178.15
Temperature range (K), max.	617.17

Datasets

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
292.25	100.00	867.0
292.25	5000.00	870.8
292.25	9900.00	874.0
292.25	19700.00	881.3
292.25	29500.00	887.1
292.25	39300.00	893.0
292.25	49100.00	898.5
292.25	58900.00	903.8
313.45	100.00	849.1
313.45	5000.00	853.1
313.45	19700.00	864.4
313.45	29500.00	871.4
313.45	39300.00	877.6
313.45	49100.00	883.6
313.45	58900.00	889.4
336.55	100.00	828.7
336.55	5000.00	833.6
336.55	9900.00	838.5
336.55	19700.00	845.8
336.55	29500.00	854.0
336.55	39300.00	860.9
336.55	49100.00	867.8
336.55	58900.00	873.6
358.81	100.00	808.4
358.81	5000.00	814.5
358.81	9900.00	820.0
358.81	19700.00	827.6
358.81	29500.00	836.8
358.81	39300.00	844.8
358.81	49100.00	852.4
358.81	58900.00	858.6
382.95	5000.00	793.0
382.95	9900.00	799.0
382.95	19700.00	808.1
382.95	29500.00	818.2
382.95	39300.00	827.1
382.95	49100.00	835.1
382.95	58900.00	842.5
408.05	5000.00	770.4

408.05	9900.00	777.3
408.05	19700.00	788.5
408.05	29500.00	799.7
408.05	39300.00	809.5
408.05	49100.00	817.9
408.05	58900.00	826.0
434.45	5000.00	746.0
434.45	9900.00	754.4
434.45	19700.00	768.1
434.45	29500.00	780.5
434.45	39300.00	791.0
434.45	49100.00	800.4
434.45	58900.00	808.6
461.85	5000.00	718.6
461.85	9900.00	728.8
461.85	19700.00	746.2
461.85	29500.00	760.0
461.85	39300.00	771.7
461.85	49100.00	782.3
461.85	58900.00	791.0
490.15	5000.00	687.0
490.15	9900.00	700.0
490.15	19700.00	720.9
490.15	29500.00	737.2
490.15	39300.00	750.7
490.15	49100.00	762.9
490.15	58900.00	773.2

Reference

<https://www.doi.org/10.1016/j.jct.2005.03.006>

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
253.23	100.00	0.0012005
253.22	1000.00	0.0012109
253.21	5000.00	0.0012585
253.22	10000.00	0.0013112
253.24	15000.00	0.0013678
253.23	20000.00	0.0014227
253.23	25000.00	0.0014793
253.24	30000.00	0.0015353

253.22	35000.00	0.0015933
263.22	100.00	0.0010207
263.22	1000.00	0.0010280
263.21	5000.00	0.0010633
263.20	10000.00	0.0011101
263.20	15000.00	0.0011601
263.21	20000.00	0.0012071
263.21	25000.00	0.0012568
263.22	30000.00	0.0013044
263.21	35000.00	0.0013502
273.21	100.00	0.0008832
273.17	1000.00	0.0008919
273.15	5000.00	0.0009249
273.18	10000.00	0.0009635
273.19	15000.00	0.0010026
273.15	20000.00	0.0010421
273.16	25000.00	0.0010818
273.15	30000.00	0.0011232
273.15	35000.00	0.0011632
283.16	100.00	0.0007737
283.13	1000.00	0.0007784
283.16	5000.00	0.0008028
283.14	10000.00	0.0008372
283.17	15000.00	0.0008678
283.15	20000.00	0.0009017
283.17	25000.00	0.0009314
283.16	30000.00	0.0009641
283.16	35000.00	0.0009964
293.26	100.00	0.0006786
293.20	1000.00	0.0006832
293.18	5000.00	0.0007056
293.24	10000.00	0.0007327
293.23	15000.00	0.0007607
293.24	20000.00	0.0007871
293.22	25000.00	0.0008173
293.24	30000.00	0.0008447
293.26	35000.00	0.0008724
303.15	100.00	0.0006033
303.17	1000.00	0.0006074
303.18	5000.00	0.0006268
303.20	10000.00	0.0006499
303.19	15000.00	0.0006744
303.17	20000.00	0.0006989
303.18	25000.00	0.0007235

303.19	30000.00	0.0007502
303.18	35000.00	0.0007739
313.12	100.00	0.0005386
313.12	1000.00	0.0005427
313.11	5000.00	0.0005596
313.10	10000.00	0.0005812
313.12	15000.00	0.0006039
313.09	20000.00	0.0006261
313.10	25000.00	0.0006490
313.08	30000.00	0.0006722
313.10	35000.00	0.0006940
322.97	100.00	0.0004865
322.98	1000.00	0.0004895
322.98	5000.00	0.0005042
322.98	10000.00	0.0005245
322.98	15000.00	0.0005440
322.97	20000.00	0.0005648
322.98	25000.00	0.0005856
322.98	30000.00	0.0006060
322.98	35000.00	0.0006259
332.91	100.00	0.0004422
332.92	1000.00	0.0004448
332.91	5000.00	0.0004595
332.92	10000.00	0.0004780
332.92	15000.00	0.0004961
332.92	20000.00	0.0005149
332.92	25000.00	0.0005331
332.92	30000.00	0.0005516
332.92	35000.00	0.0005706
342.81	100.00	0.0004022
342.80	1000.00	0.0004049
342.81	5000.00	0.0004186
342.80	10000.00	0.0004356
342.80	15000.00	0.0004524
342.80	20000.00	0.0004691
342.80	25000.00	0.0004869
342.80	30000.00	0.0005045
342.80	35000.00	0.0005223
352.73	100.00	0.0003693
352.73	1000.00	0.0003720
352.72	5000.00	0.0003851
352.73	10000.00	0.0004003
352.73	15000.00	0.0004164
352.72	20000.00	0.0004335

352.73	25000.00	0.0004495
352.73	30000.00	0.0004654
352.72	35000.00	0.0004807
362.66	100.00	0.0003390
362.66	1000.00	0.0003418
362.66	5000.00	0.0003538
362.67	10000.00	0.0003685
362.66	15000.00	0.0003838
362.66	20000.00	0.0003986
362.66	25000.00	0.0004137
362.66	30000.00	0.0004289
362.67	35000.00	0.0004429
372.61	100.00	0.0003127
372.60	1000.00	0.0003155
372.59	5000.00	0.0003272
372.59	10000.00	0.0003410
372.59	15000.00	0.0003541
372.59	20000.00	0.0003688
372.59	25000.00	0.0003822
372.59	30000.00	0.0003967
372.59	35000.00	0.0004108

Reference

<https://www.doi.org/10.1016/j.jct.2015.11.027>

Refractive index (Na D-line)

Pressure, kPa - Liquid	Temperature, K - Liquid	Refractive index (Na D-line) - Liquid
93.00	298.15	1.493

Reference

<https://www.doi.org/10.1021/acs.jced.7b00372>

Sources

Distribution of MEG and methanol in well-defined hydrocarbon and water systems: Experimental measurement and modeling using the CPA EoS: Activity Coefficients at Infinite Dilution of Organic Solutes in Experimental Densities and Excess Volumes for Binary Mixtures of 1-butyl-3-methylimidazolium perchlorate with 1,4-dioxane and aromatic hydrocarbons at infinite dilution for organic compounds and water in the gas liquid phase

- <https://www.doi.org/10.1016/j.fluid.2012.09.009>
- <http://webbook.nist.gov/cgi/cbook.cgi?ID=C100414&Units=SI>
- <https://www.doi.org/10.1021/je200050q>
- <https://www.doi.org/10.1016/j.jct.2004.07.024>
- <https://www.doi.org/10.1016/j.jct.2017.07.012>

[illegible]

<https://www.doi.org/10.1016/j.ijct.2010.05.017>

<https://www.doi.org/10.1021/je4001894>

<https://www.doi.org/10.1016/j.fluid.2010.01.025>

<https://www.doi.org/10.1016/j.jct.2017.12.012>

<https://www.doi.org/10.1016/j.jct.2017.03.004>

<https://www.doi.org/10.1016/j.fluid.2007.11.012>

<https://www.doi.org/10.1016/j.ijct.2013.11.020>

<https://www.doi.org/10.1016/j.ijct.2006.10.005>

<https://www.doi.org/10.1016/j.ijct.2016.09.003>

<https://www.doi.org/10.1016/j.fluid.2010.05.009>

<https://www.doi.org/10.1016/j.fluid.2011.11.027>

<https://www.doi.org/10.1021/je034162x>

<https://www.doi.org/10.1016/j.ijct.2013.10.038>

<https://www.doi.org/10.1016/j.ijct.2014.06.006>

<https://www.doi.org/10.1016/j.ijct.2009.06.011>

<https://www.doi.org/10.1016/j.fluid.2014.03.003>

<https://www.doi.org/10.1016/j.ijct.2016.11.019>

<https://www.doi.org/10.1016/j.fluid.2015.10.042>

<https://www.doi.org/10.1016/j.fluid.2010.08.016>

<https://www.doi.org/10.1016/j.ijct.2013.05.011>

<https://www.doi.org/10.1021/je020120h>

<https://www.doi.org/10.1031/jo100069a>

<https://www.doi.org/10.1031/jo020181f>

<https://www.doi.org/10.1031/jc800658v>

<https://www.doi.org/10.1031/jo0503554>

<https://www.doi.org/10.1016/j.ijet.2010.01.004>

<https://www.doi.org/10.1016/j.itca.2014.06.003>

<https://www.doi.org/10.1021/jc000838c>

<https://www.doi.org/10.1021/jc100724t>

<http://www.doi.org/10.1016/j.ijot.2013.05.006>

<https://www.doi.org/10.1021/jc000553v>

<https://www.doi.org/10.1021/jc000800v>

<https://www.doi.org/10.1021/acs.9b02546>

<https://www.doi.org/10.1016/j.jst.2016.10.009>

<https://www.doi.org/10.1021/acs.2012054>

DOI: 10.1016/j.jmb.2015.09.009

[illegible]

bioRxiv preprint doi: <https://doi.org/10.1101/011051>; this version posted November 11, 2014. The copyright holder for this preprint (which was not certified by peer review) is the author/funder, who has granted bioRxiv a license to display the preprint in perpetuity. It is made available under aCC-BY-NC-ND 4.0 International license.

10-1001:
00000000

[illegible]

Keywords: child sexual abuse; disclosure; social support; coping strategies

doi:10.1371/journal.pone.0136927.g002

[illegible]

<https://www.doi.org/10.1016/j.ijct.2010.12.005>

<https://www.doi.org/10.1021/je9008443>

<https://www.doi.org/10.1021/je800218a>

<https://www.doi.org/10.1021/je900277m>

<https://www.doi.org/10.1016/j.fluid.2012.05.006>

<https://www.doi.org/10.1016/j.ijct.2012.09.017>

<https://www.doi.org/10.1016/j.ijct.2016.07.017>

<https://www.doi.org/10.1016/j.ijct.2015.05.014>

<https://www.doi.org/10.1021/ie200098d>

<https://www.sciencedirect.com/book/9780128029992/the-vaws-handbook-of-vapor-pressure>

<https://www.doi.org/10.1021/je060033f>

<https://www.doi.org/10.1016/j.ijct.2018.05.003>

<https://www.doi.org/10.1021/ie900460m>

<https://www.doi.org/10.1016/j.fluid.2014.06.021>

<https://www.doi.org/10.1016/j.ijct.2015.07.020><https://www.doi.org/10.1016/j.ijct.2014.04.024>

<http://onschallenge.wikispaces.com/file/view/AqueousDataset002.xlsx/351826032/AqueousDataset002.xlsx>

<https://www.doi.org/10.1021/ie900468u>

<https://www.doi.org/10.1021/acs.iced.6b00085>

<https://www.doi.org/10.1016/j.ijct.2007.05.005>

<https://www.doi.org/10.1021/acs.jced.8b00600>

<https://www.doi.org/10.1016/j.fluid.2013.06.038>

<https://www.doi.org/10.1021/jc200627v>

<https://www.doi.org/10.1016/j.ijet.2018.03.034>

<https://www.doi.org/10.1016/j.fluid.2007.08.001>

<https://www.doi.org/10.1016/j.fluid.2019.03.032>

<https://www.doi.org/10.1021/la000686n>

<http://www.doi.org/10.1016/j.jst.2013.04.016>

<https://www.doi.org/10.1031/ja501140r>

<https://www.doi.org/10.1016/j.jst.2016.03.007>

10.1101/101015

<https://doi.org/10.1001/jama.2019.0000>

<https://doi.org/10.1016/j.jmb.2020.105377>

doi:10.1371/journal.pone.0203731.g001

doi:10.1371/journal.pone.0231037.g002

[illegible]

Downloaded from <http://ajphaphysocpharm.sagepub.com> at 10:00 11 July 2015

-based

.....

<https://doi.org/10.1002/for>

<https://doi.org/10.1016/j.jcta.2018.03.003>

<https://www.industry.gov.au/data-and-reports/industry-4.0>

<https://www.washpost.com/archive/1981-01-01/jjett-01-1981-01-01>

<https://www.washpost.com/archive/1981-05-11/j00000123X>

[illegible]

<https://www.doi.org/10.1021/acs.jced.6b00655>

<https://www.doi.org/10.1016/j.jct.2012.03.015>

<https://www.doi.org/10.1016/j.jct.2008.09.004>

<https://www.doi.org/10.1021/je0301850>

<https://www.doi.org/10.1007/s10765-009-0622-2>

<https://www.doi.org/10.1016/j.jct.2012.10.023>

<https://www.doi.org/10.1016/j.jct.2011.06.015>

<https://www.doi.org/10.1016/j.jct.2010.06.009>

<https://www.doi.org/10.1016/j.jct.2011.10.021>

<https://www.doi.org/10.1016/j.jct.2016.07.021>

<https://www.doi.org/10.1016/j.jct.2015.12.033>

<https://www.doi.org/10.1021/je049546h>

<https://www.doi.org/10.1007/s10765-005-8096-3>

<https://www.doi.org/10.1016/j.ijct.2011.02.012>

<https://www.doi.org/10.1021/ie201129v>

<https://www.doi.org/10.1021/acs.jced.7b00699>

<https://www.doi.org/10.1021/je200822w>

<https://www.doi.org/10.1016/j.ijct.2009.07.010>

<https://www.doi.org/10.1021/je401057z>

<https://www.doi.org/10.1016/j.ijct.2013.02.006>

<https://www.doi.org/10.1016/j.ijct.2018.09.003>

<https://www.doi.org/10.1016/j.ijct.2014.01.022>

<https://www.doi.org/10.1016/j.ijct.2016.01.017>

<https://www.doi.org/10.1021/ie049572f>

<https://www.doi.org/10.1016/j.ijct.2013.02.004>

<https://www.doi.org/10.1016/j.ijct.2008.12.018>

<https://www.doi.org/10.1016/j.ijct.2013.01.005>

https://en.wikipedia.org/wiki/10back_method

<https://www.doi.org/10.1021/jo034235c>

<https://www.doi.org/10.1021/jo9003179>

<https://www.doi.org/10.1021/jc7006540>

<https://www.doi.org/10.1016/j.fluid.2019.01.038>

<https://www.doi.org/10.1031/jc030151c>

<https://www.doi.org/10.1016/j.ijet.2018.01.007>

<https://www.doi.org/10.1016/j.fluid.2006.03.015>

<https://www.doi.org/10.1016/j.ijat.2006.07.022>

<https://www.doi.org/10.1016/j.ijet.2013.08.030>

<https://www.doi.org/10.1016/j.jst.2013.09.002>

<https://doi.org/10.1016/j.jst.2020.03.003>

<https://link.springer.com/article/10.1007/BF00011730>

<https://www.doi.org/10.1016/j.fluid.2006.10.010>

<https://doi.org/10.1016/j.jst.2022.05.002>

[illegible]

Effect of temperature on the volumetric properties of (cyclohexanone + an aromatic liquid):

[illegible]

1-butyl-1-methylpyrrolidinium
n-pentyl-n-methylcarbamate dilution.
of organic solutes in the ionic liquid
Volume fraction properties of binary
mixtures of tripropylamine with perfluoro-
octane and perfluorooctylphosphine oxide
Organic Solubility in Ionic Liquids
The phase behavior and thermodynamic properties of
methyldimethylammonium salt, 1,1,1-trifluoro-2-propyl-2-propanesulfonate at infinite dilution
in tetrahydrofuran at infinite
dilution of Partitioning Organic
Coefficients of Numerous Organic
Solute in Various Aqueous Phases in
Aqueous Aqueous and the Phase as
the Aqueous Phase of Organic Solutes
and Ethanol in the Aqueous Phase
for Organic Solutes and Water in the Ionic
Equilibrium of Ionic liquids + alkane +
hydrocarbon in the presence of methyl-
trimethylammonium cation in the ionic liquid
Binary Ether (MDE) Gasoline Binary
Systems based on activity coefficients
at infinite dilution in benzene and
(methanol+ ethylbenzene):
Activity coefficient at infinite dilution
measurements for organic solutes
(polar and non-polar) Equilibrium for
Benzene and Toluene Systems of acids:
2-methoxy-2-methylpropane and
Toluene, Ethylbenzene, n-octane,
Acetylene, and p-Xylene between
of cyclohexanone and Octane, Toluene,
Ethylbenzene and Benzene and Excess
Enthalpies in the Binary Systems of
Cyclohexanone and Benzene, Octane,
Ethylbenzene and Benzene, or
with characteristic enthalpies of Some
Linear and Branched Alkylbenzenes
Benzene, Octane and p-Xylene
(1-Ethyl-3-methylimidazolium
Bis(trifluoromethyl)phosphate at infinite dilution
of organic solutes and water in
Measuring the solubility of
Provisional Coefficients of Activity
for Organic Solutes and Water in the
Interaction between gas solvents:
Compounds that are vaporized and
based on chemical and thermodynamic
properties for organic solutes and
water in the ionic liquid
ethyl-dimethyl-(2-methoxyethyl)ammonium
trifluorotris(perfluoroethyl)phosphate:

<https://www.doi.org/10.1016/j.ijct.2004.07.010>

<https://www.doi.org/10.1016/j.fluid.2015.06.046>

<https://www.doi.org/10.1016/j.jct.2012.05.017>

<https://www.doi.org/10.1016/j.jct.2011.11.021>

<https://www.doi.org/10.1016/j.fluid.2018.09.024>

<https://www.doi.org/10.1021/je100652b>

<https://www.doi.org/10.1016/j.ijct.2010.02.006>

<https://www.doi.org/10.1021/ie060485s>

<https://www.doi.org/10.1016/j.ijct.2012.08.010>

<https://www.doi.org/10.1016/j.ijct.2013.10.017>

<https://www.doi.org/10.1016/j.ijct.2014.03.003>

<https://www.doi.org/10.1021/ie060198o>

<https://www.doi.org/10.1021/acs.jced.8b00080>

<https://www.doi.org/10.1016/j.fluid.2015.08.022>

<https://www.doi.org/10.1016/j.ijct.2013.03.023>

<https://www.doi.org/10.1016/j.ijct.2015.06.004>

<https://www.doi.org/10.1016/j.ijct.2008.07.009>

<https://www.doi.org/10.1016/j.fluid.2009.01.011>

<https://www.cheric.org/research/kdb/hcprop/showprop.php?cmpid=653>

<https://www.doi.org/10.1016/j.ijct.2010.12.019>

<https://www.doi.org/10.1016/j.ijct.2011.10.027>

<https://www.doi.org/10.1021/je900807v>

<https://www.doi.org/10.1016/j.ijct.2015.12.025>

opyl)cyclotrisiloxane
<https://www.doi.org/10.1016/j.ijct.2017.10.003>

<https://www.doi.org/10.1021/je050368h>

<https://www.doi.org/10.1021/ie700221w>

<https://www.doi.org/10.1016/j.ijct.2015.02.024>

<https://www.doi.org/10.1016/j.fluid.2015.08.031>

<https://www.doi.org/10.1007/s10765-007-0233-y>

<https://www.doi.org/10.1016/j.ijct.2019.05.011>

<https://www.doi.org/10.1016/j.ijct.2005.03.006>

<https://www.doi.org/10.1016/j.ijct.2013.12.009>

<https://www.doi.org/10.1021/acs.jced.8b00235>

<https://www.doi.org/10.1021/jc700289f>

<https://www.doi.org/10.1021/jc050216a>

<https://www.doi.org/10.1021/jc060280l>

<https://www.doi.org/10.1021/jc2010525>

<https://www.doi.org/10.1021/jc050272f>

<https://doi.org/10.1001/ja.790501>

<https://www.doi.org/10.1016/j.fluid.2016.09.004>

<https://www.doi.org/10.1001/ja.6005604>

<https://www.doi.org/10.1016/j.jst.2021.100227>

doi:10.1371/journal.pone.0231535.g002

[illegible]

<https://www.doi.org/10.1016/j.fluid.2009.04.007>

<https://www.doi.org/10.1021/je800754w>

<https://www.doi.org/10.1016/j.ijct.2012.03.005>

<https://www.doi.org/10.1021/je8009336>

<https://www.doi.org/10.1016/j.jct.2003.11.002>

<https://www.doi.org/10.1016/j.jct.2018.09.023>

<https://www.doi.org/10.1016/j.ijct.2013.12.025>

<https://www.doi.org/10.1021/je9002724>

<https://www.doi.org/10.1016/j.ijct.2005.12.009>

<https://www.doi.org/10.1021/acs.iced.5b00980>

<https://www.doi.org/10.1021/je0602723>

<https://www.doi.org/10.1021/je7007268>

<https://www.doi.org/10.1016/j.fluid.2012.08.004>

<https://www.doi.org/10.1021/acs.iced.6b00112>

<https://www.doi.org/10.1021/acs.iced.7b00372>

<https://www.doi.org/10.1016/j.ijct.2012.01.004>

<https://www.doi.org/10.1016/j.ijct.2005.03.019>

<https://www.doi.org/10.1021/je020186c>

<https://www.doi.org/10.1016/j.ijct.2018.05.017>

<https://www.doi.org/10.1016/j.fluid.2009.08.017>

<https://www.doi.org/10.1016/j.ijct.2009.06.020>

<https://www.doi.org/10.1021/jo034107c>

<https://www.doi.org/10.1021/jo034005v>

<https://www.doi.org/10.1021/jo200638n>

<https://www.doi.org/10.1021/jo050327f>

<https://www.doi.org/10.1021/acs.jced.8b00248>

<https://www.doi.org/10.1021/jc050544m>

<https://www.doi.org/10.1016/j.ijet.2019.10.036>

<https://www.doi.org/10.1016/j.fluid.2007.01.013>

<https://www.doi.org/10.1016/j.fluid.2013.09.044>

<https://www.doi.org/10.1016/j.jst.2011.09.028>

<https://www.doi.org/10.1016/j.jst.2018.03.014>

<https://www.doi.org/10.1016/j.jst.2024.11.015>

<https://www.doi.org/10.1021/acs.0241020>

<https://www.doi.org/10.1016/j.fluid.2017.12.020>

DOI: 10.1016/j.jmb.2019.08.003

140-13315 000150

bioRxiv preprint doi: <https://doi.org/10.1101/081976>; this version posted September 1, 2016. The copyright holder for this preprint (which was not certified by peer review) is the author/funder, who has granted bioRxiv a license to display the preprint in perpetuity. It is made available under aCC-BY-NC-ND 4.0 International license.

<https://www.ncbi.nlm.nih.gov/pmc/articles/PMC4133141/>

<https://www.industry.gov.au/publications/18-1001-00000000>

<https://www.industry.gov.au/publications/industry-2020-2021-report>

<https://doi.org/10.1016/j.jclepro.2020.122050>

<https://www.aacn.org/101-021/jc-00002p>

KDB Vapor Pressure Data:

Thermodynamics and activity

coefficients at infinite dilution for
Activity coefficients at infinite dilution
and physicochemical properties of
organic solutes and water. In the ionic
liquid 1-butyl-3-methylimidazolium
hexafluorophosphate, an investigation
of activity coefficients of organic solutes
at infinite dilution of aromatic and
aliphatic hydrocarbons, alcohols, and
acetate or methyl benzoate.
Hexafluorophosphate ionic liquids: Dilution
measurements of organic solutes and
water in the ionic liquid
1-butyl-3-methylimidazolium for
tripropylene glycol, aromatic
hydrocarbons, and alcohols in binary
mixtures. Experimental data and regression:
ethylbenzene, acetonitrile. Solubility in
Several Pure Solvents: Measurement,
Modeling, and Activity Coefficients of
Hydrocarbons in Triethylene Glycol
and Propylene Glycol Equilibrium for the
binary systems of 1-butanol with
liquid-liquid extraction of aromatics
from benzene by triethylene glycol using
1-butanol as extractant. Activity coefficients of
volatile organic compounds in two
ionic liquids composed of acetic acid
in 1-butyl-3-methylimidazolium from T =
298.15 K to 313.15 K. Thermodynamic properties of
hydrocarbons in ionic liquid and a
hydrocarbon-ionic liquid eutectic mixture:
glycerol deep eutectic solvent as
solvent for organic solutes at infinite dilution
in methylimidazolium nitrate ionic
liquid. Thermodynamic properties of
ternary and quaternary systems of representative
compounds in aqueous methanol at
ternary systems of ethylbenzene, phenol,
phenol, and 1-methyl-2-pyrrolidone. Viscosities of
Quaternary Regular Liquid Systems
and the First Quaternary Sub-Systems at
Temperatures (293.15 and 303.15 K):
Benzene, 1,2-Dichloroethane, and
Systems of Ethylbenzene, Xlenes:
Solutions at Infinite Dilution
measurements for organic solutes and
water in ionic liquid dimethylsulfoxide
with substituted benzenes at 298.15 K:
Measurement and correlation of liquid
liquid equilibria for ternary systems
for acetone + aromatic hydrocarbon +
hexafluorophosphate ionic liquid
1-butyl-3-methylimidazolium and
1-butyl-3-methylimidazolium hexafluorophosphate based on liquid
liquid equilibrium measurements.
Solutions Dissolved in Two
Phases and the Activity Coefficient of the
(N-alkylisoquinolinium thiocyanate
Determination of Activity Coefficients
at Infinite Dilution of 35 Solutes in the
Measurement of Activity Coefficient at
Infinite Dilution of Organic Solutes,
Benzene, and 1,2-Dichloroethane in
Chloroform by Gas-Liquid Chromatography:
Chloroform + Alkylbenzene
Mixtures of
1-Alkyl-3-methylimidazolium
Hexafluorophosphate in Hydrocarbons:
and physicochemical properties for
Standard and Glycerol in two and
ethylbenzene, and 1-butanol in
acetonitrile, and 1-butanol in
acetonitrile. Thermodynamic properties of
organic solutes in the ionic liquid
1-butyl-3-methylimidazolium
hexafluorophosphate. Thermodynamic
properties of binary mixtures
containing ionic liquids and coefficients
at infinite dilution of solutes in
Non-Selective Water-butanol Azeotrope
Separation on Investigation of Limiting
Activity Coefficients by Method:
IP8.8.8.8] [NTT] ionic liquid:
Thermodynamics and activity
coefficients at infinite dilution
Activity Coefficients at Infinite Dilution
of Organic Compounds in Four New
Imidazolium-Based Ionic Liquids:
tetracyanoborate:

<https://www.thermo.com/research/kdb/hcprop/showprop.php?cmpid=653>

<https://www.doi.org/10.1016/j.jct.2018.08.028>

<https://www.doi.org/10.1016/j.jct.2012.08.016>

<https://www.doi.org/10.1016/j.fluid.2018.07.028>

<https://www.doi.org/10.1016/j.jct.2008.01.004>

<https://www.doi.org/10.1021/je800325d>

<https://www.doi.org/10.1021/je1000582>

<https://www.doi.org/10.1016/j.fluid.2016.05.032>

<https://www.doi.org/10.1016/j.fluid.2007.09.021>

<https://www.doi.org/10.1021/acs.jced.9b00243>

<https://www.doi.org/10.1021/je020196d>

<https://www.doi.org/10.1021/je201053v>

<https://www.doi.org/10.1016/j.jct.2012.05.006>

<https://www.doi.org/10.1016/j.jct.2013.05.035>

<https://www.doi.org/10.1021/acs.jced.8b00139>

<https://www.doi.org/10.1016/j.jct.2006.05.006>

<https://www.doi.org/10.1016/j.fluid.2018.06.003>

<https://www.doi.org/10.1021/je100998r>

<https://www.doi.org/10.1016/j.fluid.2013.03.022>

<https://www.doi.org/10.1016/j.fluid.2012.05.010>

<https://www.doi.org/10.1007/s10765-012-1159-3>

<https://www.doi.org/10.1021/je050529h>

<https://www.doi.org/10.1021/je049701s>

<https://www.doi.org/10.1016/j.jct.2008.12.005>

<https://www.doi.org/10.1016/j.fluid.2007.10.017>

<https://www.doi.org/10.1016/j.fluid.2009.12.019>

<https://www.doi.org/10.1016/j.jct.2017.11.017>

<https://www.doi.org/10.1016/j.fluid.2014.12.003>

<https://www.doi.org/10.1021/je500050p>

<https://www.doi.org/10.1016/j.jct.2013.04.011>

<https://www.doi.org/10.1021/je100410k>

<https://www.doi.org/10.1021/je700139p>

<https://www.doi.org/10.1021/je7002447>

<https://www.doi.org/10.1021/je020145g>

<https://www.doi.org/10.1016/j.jct.2018.01.003>

<https://www.doi.org/10.1016/j.tca.2015.11.010>

<https://www.doi.org/10.1016/j.fluid.2010.10.008>

<https://www.doi.org/10.1016/j.jct.2004.12.008>

<https://www.doi.org/10.1021/acs.jced.8b00635>

<https://www.doi.org/10.1016/j.fluid.2017.06.001>

http://pubs.acs.org/doi/suppl/10.1021/ci034243x/suppl_file/ci034243xsi20040112_053635.txt

<https://www.doi.org/10.1016/j.jct.2011.06.007>

<https://www.doi.org/10.1021/je200195q>

Legend

af:	Acentric Factor
affp:	Proton affinity
aigt:	Autoignition Temperature
basg:	Gas basicity
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity

dm:	Dipole Moment
dvisc:	Dynamic viscosity
fl:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpc:	Flash Point (Closed Cup Method)
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hcg:	Heat of Combustion, Gross form
hcn:	Heat of Combustion, Net Form
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rho:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sg:	Molar entropy at standard conditions
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
svapt:	Entropy of vaporization at a given temperature
tb:	Normal Boiling Point Temperature
tbp:	Boiling point at given pressure
tc:	Critical Temperature
tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility

zra:

Rackett Parameter

Latest version available from:

<https://www.chemeo.com/cid/51-337-1/Benzene-ethyl.pdf>

Generated by Cheméo on 2026-07-21 14:46:28.130272257 +0000 UTC m=+156283.972157646.

Cheméo (<https://www.chemeo.com>) is the biggest free database of chemical and physical data for the process industry.