

Acetic acid

Other names:	Acetasol Acetic acid, glacial Aci-jel Acide acetique Acido acetico Azijnzuur CH ₃ COOH Essigsaeure Ethanoic acid Ethanoic acid monomer Ethylic acid Glacial acetic acid Kyselina octova Methanecarboxylic acid NSC 132953 Octowy kwas Shotgun UN 2789 Vinegar acid
Inchi:	InChI=1S/C2H4O2/c1-2(3)4/h1H3,(H,3,4)
InchiKey:	QTBSBXVTEAMEQO-UHFFFAOYSA-N
Formula:	C ₂ H ₄ O ₂
SMILES:	CC(=O)O
Mol. weight [g/mol]:	60.05
CAS:	64-19-7

Physical Properties

Property code	Value	Unit	Source
af	0.4470		KDB
affp	783.70	kJ/mol	NIST Webbook
aigt	699.82	K	KDB
basg	752.80	kJ/mol	NIST Webbook
chl	-874.20 ± 0.20	kJ/mol	NIST Webbook
chl	-875.16 ± 0.34	kJ/mol	NIST Webbook
chl	-872.40	kJ/mol	NIST Webbook
chl	-874.50 ± 0.40	kJ/mol	NIST Webbook
dm	1.30	debye	KDB

fil	5.40	% in Air	KDB
flu	16.00	% in Air	KDB
fpc	317.59	K	KDB
fpo	313.15	K	KDB
gf	-376.90	kJ/mol	KDB
gyrad	2.5950		KDB
hf	-432.90 ± 1.50	kJ/mol	NIST Webbook
hf	-431.90 ± 1.50	kJ/mol	NIST Webbook
hf	-435.40 ± 4.30	kJ/mol	NIST Webbook
hf	-435.40	kJ/mol	NIST Webbook
hf	-432.50 ± 1.60	kJ/mol	NIST Webbook
hf	-432.50 ± 1.60	kJ/mol	NIST Webbook
hf	-432.90 ± 1.50	kJ/mol	NIST Webbook
hf	-431.90 ± 1.50	kJ/mol	NIST Webbook
hf	-435.10	kJ/mol	KDB
hfl	-483.52 ± 0.36	kJ/mol	NIST Webbook
hfl	-487.00	kJ/mol	NIST Webbook
hfl	-484.10 ± 0.40	kJ/mol	NIST Webbook
hfl	-484.50 ± 0.20	kJ/mol	NIST Webbook
hfus	6.62	kJ/mol	Joback Method
hvap	51.60 ± 1.50	kJ/mol	NIST Webbook
hvap	51.60 ± 1.60	kJ/mol	NIST Webbook
hvap	50.30	kJ/mol	NIST Webbook
hvap	51.60	kJ/mol	NIST Webbook
ie	10.63	eV	NIST Webbook
ie	10.35 ± 0.03	eV	NIST Webbook
ie	10.90	eV	NIST Webbook
ie	10.84	eV	NIST Webbook
ie	10.64 ± 0.00	eV	NIST Webbook
ie	10.63	eV	NIST Webbook
ie	11.50	eV	NIST Webbook
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ie	10.66 ± 0.05	eV	NIST Webbook
ie	10.66 ± 0.00	eV	NIST Webbook
ie	10.80	eV	NIST Webbook
ie	10.65	eV	NIST Webbook
ie	10.69 ± 0.03	eV	NIST Webbook
ie	10.37 ± 0.03	eV	NIST Webbook
ie	10.70	eV	NIST Webbook

log10ws	1.22		Aqueous Solubility Prediction Method
logp	0.091		Crippen Method
mcvol	46.480	ml/mol	McGowan Method
nfpaf	%!d(float64=2)		KDB
nfpah	%!d(float64=3)		KDB
nfpas	%!d(float64=1)		KDB
pc	5786.00 ± 8.00	kPa	NIST Webbook
pc	5829.01 ± 90.00	kPa	NIST Webbook
pc	5787.00 ± 101.32	kPa	NIST Webbook
pc	5786.70 ± 26.66	kPa	NIST Webbook
pc	5781.00 ± 20.00	kPa	NIST Webbook
pc	5786.00	kPa	KDB
pt	1.28	kPa	KDB
rhoc	350.58 ± 1.20	kg/m3	NIST Webbook
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ripol	1450.00	NIST Webbook
ripol	1432.00	NIST Webbook
ripol	1452.00	NIST Webbook
ripol	1418.00	NIST Webbook
ripol	1401.00	NIST Webbook
ripol	1425.00	NIST Webbook
ripol	1436.00	NIST Webbook
ripol	1451.00	NIST Webbook
ripol	1453.00	NIST Webbook
ripol	1449.00	NIST Webbook
ripol	1449.00	NIST Webbook
ripol	1449.00	NIST Webbook
ripol	1413.00	NIST Webbook
ripol	1449.00	NIST Webbook
ripol	1461.00	NIST Webbook
ripol	1447.00	NIST Webbook
ripol	1435.00	NIST Webbook
ripol	1447.00	NIST Webbook
ripol	1434.00	NIST Webbook
ripol	1446.00	NIST Webbook
ripol	1476.00	NIST Webbook
ripol	1450.00	NIST Webbook
ripol	1447.00	NIST Webbook
ripol	1468.00	NIST Webbook

ripol	1430.00		NIST Webbook
ripol	1439.00		NIST Webbook
ripol	1475.00		NIST Webbook
ripol	1425.00		NIST Webbook
ripol	1408.00		NIST Webbook
ripol	1457.00		NIST Webbook
ripol	1453.00		NIST Webbook
ripol	1463.00		NIST Webbook
ripol	1431.00		NIST Webbook
ripol	1435.00		NIST Webbook
ripol	1439.00		NIST Webbook
ripol	1428.00		NIST Webbook
ripol	1435.00		NIST Webbook
ripol	1446.00		NIST Webbook
ripol	1455.00		NIST Webbook
ripol	1449.00		NIST Webbook
sg	282.84	J/mol×K	NIST Webbook
sl	193.70	J/mol×K	NIST Webbook
sl	158.00	J/mol×K	NIST Webbook
tb	391.20 ± 0.10	K	Liquid-Liquid Equilibria of Water + Acetic Acid + Dimethyl Glutarate Ternary System
tb	391.10	K	Measurement and modelling of static dielectric constants of aqueous solutions of methanol, ethanol and acetic acid at T = 293.15 K and 91.3 kPa
tb	390.93	K	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tb	391.20	K	(Liquid + liquid) equilibria of the (water + acetic acid + dibutyl phthalate) system
tb	390.93	K	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tb	390.85	K	Quaternary Liquid-Liquid Equilibrium of Water + Acetic Acid + Propionic Acid + Solvent (Amyl Alcohol, Cyclohexyl Acetate, or Toluene) Systems
tb	391.03	K	Isobaric Vapor-Liquid Equilibria for Water + Acetic Acid + 1-Ethyl-3-methylimidazolium Diethylphosphate at 101.32 kPa

tb	391.20 ± 0.10	K	Liquid liquid equilibria of the ternary system water + acetic acid + dimethyl succinate
tb	390.95	K	Vapor liquid equilibria for the quaternary reactive system ethyl acetate + ethanol + water + acetic acid and some of the constituent binary systems at 101.3 kPa
tb	390.85	K	Liquid liquid equilibria of ternary systems (water + carboxylic acid + cumene) at 298.15K
tb	391.05 ± 0.20	K	Determination and correlation of liquid liquid equilibria for the (water + carboxylic acid + dimethyl maleate) ternary systems at T = 298.2K
tb	391.00 ± 0.10	K	Vapor liquid equilibria for water + acetic acid + (N,N-dimethylformamide or dimethyl sulfoxide) at 13.33 kPa
tb	390.20 ± 0.10	K	Phase equilibrium of (water + formic or acetic acid + ethyl heptanoate) ternary liquid systems at different temperatures
tb	391.03 ± 0.01	K	Isobaric vapor-liquid equilibrium for water + acetic acid + 1-butyl-3-methylimidazolium dibutylphosphate at 101.32 kPa
tb	391.05	K	Quaternary phase equilibrium of water-carboxylic acid mixture (formic-propionic acid or acetic-propionic acid)-solvent liquid systems at 298.15 K
tb	391.20 ± 0.10	K	(Liquid + liquid) equilibria of the (water + carboxylic acid + dibasic esters mixture (DBE-2)) ternary systems
tb	391.20 ± 0.10	K	Liquid-liquid equilibria of water + acetic acid + 2-ethyl hexyl acetate ternary system
tb	391.08 ± 0.10	K	Isobaric vapor-liquid equilibrium of the binary system sec-butyl acetate + para-xylene and the quaternary system methyl acetate + para-xylene + sec-butyl acetate + acetic acid at 101.3 kPa

tb	391.20	K	Liquid liquid equilibria of the ternary system water + acetic acid + dimethyl succinate
tb	390.95 ± 0.10	K	Ternary liquid-liquid phase equilibria of (water-carboxylic acid-1-undecanol) systems at 298.15 K
tb	391.00	K	KDB
tb	391.44 ± 0.05	K	Isobaric Vapor-Liquid Equilibria for (Acetic Acid + Cyclohexane) and (Cyclohexane + Acetylacetone) at a Pressure of 101.3 kPa and for (Acetic Acid + Acetylacetone) at a Pressure of 60.0 kPa
tb	390.91	K	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
tb	391.10 ± 0.10	K	Liquid-Liquid Equilibria of (Water + Acetic Acid + Diethyl Succinate or Diethyl Glutarate or Diethyl Adipate) Ternary Systems
tb	391.20 ± 0.10	K	Liquid Phase Equilibria of the Water + Acetic Acid + Dimethyl Carbonate Ternary System at Several Temperatures
tb	390.96 ± 0.10	K	Investigation on Isobaric Vapor Liquid Equilibrium for Water + Acetic Acid + sec-Butyl Acetate
tb	391.03	K	Isobaric Vapor-Liquid Equilibria for Water + Acetic Acid + 1-Ethyl-3-methylimidazolium Diethylphosphate at 101.32 kPa
tb	391.43	K	Geometric Structures of Associating Component Optimized toward Correlation and Prediction of Isobaric Vapor Liquid Equilibria for Binary and Ternary Mixtures of Ethanal, Ethanol, and Ethanoic Acid
tb	390.85 ± 0.10	K	Measurements of Quaternary Liquid-Liquid Equilibrium for Water + Acetic Acid + Propionic Acid + Solvent (Butyronitrile, Benzyl Acetate, or Methyl Isobutyl Ketone) at 298.15 K

tb	390.85 ± 0.10		K	Isobaric vapor liquid equilibria for water + acetic acid + (N-methyl pyrrolidone or N-methyl acetamide)
tc	592.71		K	KDB
tf	289.70 ± 0.03		K	NIST Webbook
tf	289.80 ± 0.30		K	NIST Webbook
tf	289.75 ± 0.05		K	NIST Webbook
tf	289.49 ± 0.05		K	NIST Webbook
tf	289.67 ± 0.05		K	NIST Webbook
tf	289.62 ± 0.10		K	NIST Webbook
tf	289.00 ± 1.50		K	NIST Webbook
tf	289.69 ± 0.20		K	NIST Webbook
tf	289.93		K	Aqueous Solubility Prediction Method
tf	289.95		K	Differential scanning calorimetry determination of phase diagrams and water activities of aqueous carboxylic acid solutions
tf	289.84		K	Solid liquid equilibrium in the ternary system acetic acid propanoic acid formamide
tf	289.70		K	KDB
tf	289.85		K	NIST Webbook
tt	289.80 ± 0.15		K	NIST Webbook
tt	289.69 ± 0.04		K	NIST Webbook
tt	289.80 ± 0.05		K	NIST Webbook
tt	289.69		K	KDB
vc	0.171	m ³ /kmol		KDB
zc	0.2007690			KDB
zra	0.22			KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	81.64	J/mol×K	420.52	Joback Method
cpg	88.73	J/mol×K	479.15	Joback Method
cpg	92.08	J/mol×K	508.46	Joback Method
cpg	95.29	J/mol×K	537.78	Joback Method
cpg	98.37	J/mol×K	567.09	Joback Method
cpg	77.89	J/mol×K	391.21	Joback Method
cpg	85.25	J/mol×K	449.84	Joback Method

cpl	123.10	J/mol×K	298.15	NIST Webbook
cpl	159.80	J/mol×K	298.10	NIST Webbook
cpl	120.50	J/mol×K	298.00	NIST Webbook
cpl	137.00	J/mol×K	311.00	NIST Webbook
cpl	121.30	J/mol×K	297.10	NIST Webbook
cpl	137.21 ± 0.55	J/mol×K	333.15	Heat Capacities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
cpl	135.50 ± 0.54	J/mol×K	313.15	Heat Capacities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
cpl	123.40	J/mol×K	294.70	NIST Webbook
cpl	123.50	J/mol×K	298.00	NIST Webbook
cpl	139.70	J/mol×K	332.00	NIST Webbook
dvisc	0.0011270 ± 0.0000030	Paxs	298.15	Densities, Excess Molar Volumes, Viscosity, and Refractive Indices of Binary Mixtures of Ethanoic Acid and Trichloroethylene with Dimethylbenzenes at Different Temperatures
dvisc	0.0010590 ± 0.0000030	Paxs	303.15	Densities and Viscosities of N,N-Dimethylformamide + Formic Acid, and + Acetic Acid in the Temperature Range from (303.15 to 353.15) K
dvisc	0.0006320 ± 0.0000030	Paxs	343.15	Densities and Viscosities of N,N-Dimethylformamide + Formic Acid, and + Acetic Acid in the Temperature Range from (303.15 to 353.15) K

dvisc	0.0007090 ± 0.0000030	Paxs	333.15	Densities and Viscosities of N,N-Dimethylformamide + Formic Acid, and + Acetic Acid in the Temperature Range from (303.15 to 353.15) K
dvisc	0.0008040 ± 0.0000030	Paxs	323.15	Densities and Viscosities of N,N-Dimethylformamide + Formic Acid, and + Acetic Acid in the Temperature Range from (303.15 to 353.15) K
dvisc	0.0006970 ± 0.0000050	Paxs	333.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0009200 ± 0.0000030	Paxs	313.15	Densities and Viscosities of N,N-Dimethylformamide + Formic Acid, and + Acetic Acid in the Temperature Range from (303.15 to 353.15) K
dvisc	0.0010340 ± 0.0000010	Paxs	303.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure

dvisc	0.0011150 ± 0.0000010	Paxs	298.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
dvisc	0.0005700 ± 0.0000030	Paxs	353.15	Densities and Viscosities of N,N-Dimethylformamide + Formic Acid, and + Acetic Acid in the Temperature Range from (303.15 to 353.15) K
dvisc	0.0012040 ± 0.0000050	Paxs	293.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0011140 ± 0.0000050	Paxs	298.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0010370 ± 0.0000050	Paxs	303.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0009640 ± 0.0000050	Paxs	308.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures

dvisc	0.0012110 ± 0.0000010	Paxs	293.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
dvisc	0.0008410 ± 0.0000050	Paxs	318.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0007870 ± 0.0000050	Paxs	323.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0007410 ± 0.0000050	Paxs	328.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0006970 ± 0.0000050	Paxs	333.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0006570 ± 0.0000050	Paxs	338.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures

dvisc	0.0012040 ± 0.0000050	Paxs	293.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0011140 ± 0.0000050	Paxs	298.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0010370 ± 0.0000050	Paxs	303.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0011150	Paxs	298.15	Vapor liquid equilibria for the quaternary reactive system ethyl acetate + ethanol + water + acetic acid and some of the constituent binary systems at 101.3 kPa
dvisc	0.0009020 ± 0.0000050	Paxs	313.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0008410 ± 0.0000050	Paxs	318.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures

dvisc	0.0007870 ± 0.0000050	Paxs	323.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0007410 ± 0.0000050	Paxs	328.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0009640 ± 0.0000050	Paxs	308.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
dvisc	0.0009020 ± 0.0000050	Paxs	313.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
hfust	11.72	kJ/mol	298.70	NIST Webbook
hfust	10.83	kJ/mol	289.80	NIST Webbook
hfust	11.52	kJ/mol	283.70	NIST Webbook
hfust	11.13	kJ/mol	290.06	NIST Webbook
hfust	11.72	kJ/mol	298.70	NIST Webbook
hfust	11.73	kJ/mol	289.90	NIST Webbook
hsubt	67.00 ± 1.00	kJ/mol	221.50	NIST Webbook
hsubt	70.00 ± 1.00	kJ/mol	221.50	NIST Webbook
hvapt	41.60	kJ/mol	340.50	NIST Webbook
hvapt	42.00	kJ/mol	343.00	NIST Webbook
hvapt	43.00	kJ/mol	308.00	NIST Webbook
hvapt	40.90	kJ/mol	357.50	NIST Webbook
hvapt	39.10	kJ/mol	364.00	NIST Webbook
hvapt	23.70	kJ/mol	391.10	NIST Webbook
hvapt	23.68	kJ/mol	391.30	KDB
hvapt	40.30	kJ/mol	358.00	NIST Webbook
hvapt	38.10	kJ/mol	486.00	NIST Webbook
hvapt	41.60	kJ/mol	351.00	NIST Webbook
hvapt	38.70	kJ/mol	419.00	NIST Webbook

hvapt	38.80	kJ/mol	559.00	NIST Webbook
hvapt	37.90	kJ/mol	470.50	NIST Webbook
pvap	101.32 ± 0.03	kPa	391.03	Isobaric Vapor-Liquid Equilibria for Water + Acetic Acid + 1-Ethyl-3-methylimidazolium Diethylphosphate at 101.32 kPa
pvap	49.34	kPa	368.10	Separation of Furfural from Ternary Mixtures
pvap	10.97 ± 0.10	kPa	330.65	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	96.15	kPa	388.91	Vapor Liquid Equilibrium Data for Binary Mixtures of Acetic Acid + Anisole, Acetone + Anisole, and Isopropanol + Anisole at Pressure 96.15 kPa
pvap	13.97 ± 0.10	kPa	336.23	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	20.00	kPa	345.03	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
pvap	17.98 ± 0.10	kPa	342.25	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	19.98 ± 0.10	kPa	344.81	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa

pvap	21.98 ± 0.10	kPa	347.19	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	23.98 ± 0.10	kPa	349.40	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	26.97 ± 0.10	kPa	352.43	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	11.98 ± 0.10	kPa	332.65	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	40.00	kPa	363.04	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
pvap	60.00	kPa	374.54	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
pvap	80.00	kPa	383.32	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
pvap	101.30	kPa	390.93	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems

pvap	101.32	kPa	391.03	Isobaric Vapor-Liquid Equilibria for Water + Acetic Acid + 1-Ethyl-3-methylimidazolium Diethylphosphate at 101.32 kPa
pvap	7.72 ± 0.01	kPa	323.15	Isothermal vapour liquid equilibrium with chemical reaction in the quaternary water + methanol + acetic acid + methyl acetate system, and in five binary subsystems
pvap	9.98 ± 0.10	kPa	328.56	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	29.96 ± 0.10	kPa	355.18	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	88.98	kPa	386.07	Separation of Furfural from Ternary Mixtures
pvap	7.57 ± 0.01	kPa	323.15	Vapor-Liquid Equilibria in the Propyl Acetate + Ethanoic Acid Binary System from (323.15 to 353.15) K: Measurement with a Static Method and Modeling with the NRTL, Wilson, UNIQUAC, and COSMO-SAC Approaches

pvap	12.04 ± 0.01	kPa	333.15	Vapor-Liquid Equilibria in the Propyl Acetate + Ethanoic Acid Binary System from (323.15 to 353.15) K: Measurement with a Static Method and Modeling with the NRTL, Wilson, UNIQUAC, and COSMO-SAC Approaches
pvap	18.66 ± 0.01	kPa	343.15	Vapor-Liquid Equilibria in the Propyl Acetate + Ethanoic Acid Binary System from (323.15 to 353.15) K: Measurement with a Static Method and Modeling with the NRTL, Wilson, UNIQUAC, and COSMO-SAC Approaches
pvap	28.20 ± 0.01	kPa	353.15	Vapor-Liquid Equilibria in the Propyl Acetate + Ethanoic Acid Binary System from (323.15 to 353.15) K: Measurement with a Static Method and Modeling with the NRTL, Wilson, UNIQUAC, and COSMO-SAC Approaches
pvap	32.98 ± 0.10	kPa	357.72	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	35.94 ± 0.10	kPa	360.09	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa

pvap	38.96 ± 0.10	kPa	362.26	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	42.93 ± 0.10	kPa	365.00	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	44.95 ± 0.10	kPa	366.30	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	49.94 ± 0.10	kPa	369.30	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	54.93 ± 0.10	kPa	372.09	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	59.83 ± 0.10	kPa	374.63	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	64.87 ± 0.10	kPa	377.03	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	69.84 ± 0.10	kPa	379.25	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	74.82 ± 0.10	kPa	381.39	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa

pvap	79.71 ± 0.10	kPa	383.35	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	89.81 ± 0.10	kPa	387.10	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	94.52 ± 0.10	kPa	388.77	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	101.30 ± 0.10	kPa	390.91	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
pvap	20.00 ± 0.10	kPa	345.27	Isobaric Vapor Liquid Equilibrium for Binary Systems of Toluene + Acrylic Acid, Toluene + Acetic Acid, and Cyclohexane + Acrylic Acid at 20 kPa
pvap	101.33	kPa	391.43	Geometric Structures of Associating Component Optimized toward Correlation and Prediction of Isobaric Vapor Liquid Equilibria for Binary and Ternary Mixtures of Ethanal, Ethanol, and Ethanoic Acid
pvap	15.97 ± 0.10	kPa	339.41	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa

pvap	84.52 ± 0.10	kPa	385.23	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
rfi	1.37100 ± 0.00002		293.15	Ternary liquid-liquid phase equilibria of (water-carboxylic acid-1-undecanol) systems at 298.15 K
rfi	1.37150 ± 0.00020		293.15	Isobaric Vapor-Liquid Equilibria for (Acetic Acid + Cyclohexane) and (Cyclohexane + Acetylacetone) at a Pressure of 101.3 kPa and for (Acetic Acid + Acetylacetone) at a Pressure of 60.0 kPa
rfi	1.36960 ± 0.00020		298.15	Liquid-Liquid Equilibria for the System 1-Methyl Propyl Ethanoate (1) + Acetic Acid (2) + Water (3) at (283.15 and 323.15) K
rfi	1.37200 ± 0.00010		293.15	Isobaric Vapor-Liquid Equilibria for the Binary Systems of Acetic Acid + Isopropenyl Acetate, Acetic Acid + Acetylacetone, and Water + Acetylacetone
rfi	1.36960		298.15	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
rfi	1.37201 ± 0.00005		293.15	Liquid-Liquid Equilibria of (Water + Acetic Acid + Diethyl Succinate or Diethyl Glutarate or Diethyl Adipate) Ternary Systems

rfi	1.37000	298.15	Solubilities of Benzoic Acid and Phthalic Acid in Acetic Acid + Water Solvent Mixtures
rfi	1.37130 ± 0.00001	298.20	Liquid Phase Equilibria of the Water + Acetic Acid + Dimethyl Carbonate Ternary System at Several Temperatures
rfi	1.37160	298.15	Geometric Structures of Associating Component Optimized toward Correlation and Prediction of Isobaric Vapor Liquid Equilibria for Binary and Ternary Mixtures of Ethanal, Ethanol, and Ethanoic Acid
rfi	1.37160	293.15	Solubilities of Phosphorus-Containing Compounds in Selected Solvents
rfi	1.37160	298.15	Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures of Methanol, Ethanoic Acid, and Propanoic Acid
rfi	1.37180	293.15	Solubilities of Some Phosphaspirocyclic Compounds in Selected Solvents
rfi	1.36969 ± 0.00001	298.15	Refractive Index, Surface Tension, and Density of Aqueous Mixtures of Carboxylic Acids at 298.15 K

rfi	1.37210 ± 0.00050	293.15	Measurements of Quaternary Liquid-Liquid Equilibrium for Water + Acetic Acid + Propionic Acid + Solvent (Butyronitrile, Benzyl Acetate, or Methyl Isobutyl Ketone) at 298.15 K
rfi	1.37190	293.15	Isobaric Vapor-Liquid Equilibria for Water + Acetic Acid + (n-Pentyl Acetate or Isopropyl Acetate)
rfi	1.37190 ± 0.00050	293.20	Liquid-Liquid Equilibria of Water + Acetic Acid + Dimethyl Glutarate Ternary System
rfi	1.36485 ± 0.00010	303.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.36643 ± 0.00010	303.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.36675 ± 0.00010	303.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures

rfi	1.36815 ± 0.00010	303.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.36968 ± 0.00010	303.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37261 ± 0.00010	303.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37611 ± 0.00010	303.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37917 ± 0.00010	303.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures

rfi	1.36686 ± 0.00010	298.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.36844 ± 0.00010	298.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.36876 ± 0.00010	298.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37018 ± 0.00010	298.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37174 ± 0.00010	298.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures

rfi	1.37466 ± 0.00010	298.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37816 ± 0.00010	298.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.38126 ± 0.00010	298.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.36896 ± 0.00010	293.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37055 ± 0.00010	293.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures

rfi	1.37087 ± 0.00010	293.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37230 ± 0.00010	293.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37386 ± 0.00010	293.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37681 ± 0.00010	293.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.38034 ± 0.00010	293.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures

rfi	1.38345 ± 0.00010	293.15	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.36809 ± 0.00010	94.64	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37012 ± 0.00010	94.64	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37224 ± 0.00010	94.64	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rfi	1.37160 ± 0.00040	303.15	Phase equilibria measurements of ternary mixtures (sulfolane + a carboxylic acid + pentane) at 303.15 K

rfi	1.37180 ± 0.00010	293.15	Isobaric vapor-liquid equilibrium of the binary system sec-butyl acetate + para-xylene and the quaternary system methyl acetate + para-xylene + sec-butyl acetate + acetic acid at 101.3 kPa
rfi	1.37160 ± 0.00040	303.15	Liquid liquid equilibria measurements of ternary systems (acetonitrile + a carboxylic acid + dodecane) at 303.15 K
rfi	1.37130 ± 0.00001	298.15	Liquid-liquid equilibria of water + acetic acid + 2-ethyl hexyl acetate ternary system
rfi	1.37135 ± 0.00001	298.20	(Liquid + liquid) equilibria of the (water + carboxylic acid + dibasic esters mixture (DBE-2)) ternary systems
rfi	1.36960 ± 0.00020	298.15	Study of liquid liquid equilibrium of the systems isobutyl acetate + acetic acid +water and isobutyl alcohol + acetic acid +water at different temperatures
rfi	1.37190 ± 0.00050	293.15	Determination and correlation of liquid liquid equilibria for the (water + carboxylic acid + dimethyl maleate) ternary systems at T = 298.2K
rfi	1.37210	293.15	Liquid liquid equilibria of ternary systems (water + carboxylic acid + cumene) at 298.15K

rfi	1.37130	298.20	Liquid liquid equilibria of the ternary system water + acetic acid + dimethyl succinate
rfi	1.37200	293.00	Quaternary Liquid-Liquid Equilibrium of Water + Acetic Acid + Propionic Acid + Solvent (Amyl Alcohol, Cyclohexyl Acetate, or Toluene) Systems
rfi	1.37170	293.15	Liquid-Liquid Phase Equilibria for Quinary, Quaternary, and Ternary Systems {Water + Furfural + Acetic Acid + Cyclopentyl Methyl Ether + CaCl ₂ }: Measurement, Effect of Salt, and Comparative Study
rfi	1.37170	293.15	Measurement and Modeling of Liquid Liquid Equilibrium for the Systems Vinyl Acetate + Acetic Acid/Ethanol + Water at 298.15 and 308.15 K
rfi	1.37240	96.15	Vapor Liquid Equilibrium Data for Binary Mixtures of Acetic Acid + Anisole, Acetone + Anisole, and Isopropanol + Anisole at Pressure 96.15 kPa
rfi	1.37140	298.15	Liquid Phase Equilibria of Aqueous Mixtures of Carboxylic Acids (C1-C4) with Ethylbenzene: Thermodynamic and Mathematical Modeling

rfi	1.37203	298.00	Quaternary and ternary LLE measurements for solvent (2-methyltetrahydrofuran and cyclopentyl methyl ether) + furfural + acetic acid + water between 298 and 343 K
rfi	1.37200	293.15	Measurement and modelling of static dielectric constants of aqueous solutions of methanol, ethanol and acetic acid at T = 293.15 K and 91.3 kPa
rfi	1.37130	293.15	Isobaric (vapour + liquid) equilibria data for the binary systems {1,2-dichloroethane (1) + toluene (2)} and {1,2-dichloroethane (1) + acetic acid (2)} at atmospheric pressure
rfi	1.37150	298.20	(Liquid + liquid) equilibria of the (water + acetic acid + dibutyl phthalate) system
rfi	1.36440	313.20	Liquid-liquid equilibrium data and thermophysical properties for ternary systems composed of water, acetic acid and different solvents
rfi	1.37240	293.20	Liquid-liquid equilibrium data and thermophysical properties for ternary systems composed of water, acetic acid and different solvents

rfi	1.36440	313.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
rfi	1.37240	293.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
rfi	1.37030	298.15	Liquid - liquid equilibrium for the quaternary reaction system water p sec-butyl alcohol p sec-butyl acetate p acetic acid
rfi	1.37210	293.15	Quaternary phase equilibrium of water-carboxylic acid mixture (formic-propionic acid or acetic-propionic acid)-solvent liquid systems at 298.15 K
rfi	1.37130	298.15	Liquid liquid equilibria of the ternary system water + acetic acid + dimethyl succinate
rfi	1.36980 ± 0.00020	298.15	Densities, Excess Molar Volumes, Viscosity, and Refractive Indices of Binary Mixtures of Ethanoic Acid and Trichloroethylene with Dimethylbenzenes at Different Temperatures

rfi	1.37104 ± 0.00001		298.15	Phase equilibrium of (water + formic or acetic acid + ethyl heptanoate) ternary liquid systems at different temperatures
rfi	1.36870 ± 0.00020		293.15	Volumetric Properties of Highly Nonideal Binary Mixtures Containing Ethanoic Acid and Propanoic Acid with Butan-2-ol, Methyl-2-propanol, and 2-Methyl-2-butanol at Different Temperatures
rhoL	1044.60	kg/m ³	298.15	Liquid - liquid equilibrium for the quaternary reaction system water p sec-butyl alcohol p sec-butyl acetate p acetic acid
rhoL	1049.80	kg/m ³	293.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
rhoL	1028.13	kg/m ³	313.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
rhoL	1049.80	kg/m ³	293.20	Liquid-liquid equilibrium data and thermophysical properties for ternary systems composed of water, acetic acid and different solvents

rhoI	1028.13	kg/m3	313.20	Liquid-liquid equilibrium data and thermophysical properties for ternary systems composed of water, acetic acid and different solvents
rhoI	1049.44	kg/m3	298.20	(Liquid + liquid) equilibria of the (water + acetic acid + dibutyl phthalate) system
rhoI	1049.40	kg/m3	293.15	Isobaric (vapour + liquid) equilibria data for the binary systems {1,2-dichloroethane (1) + toluene (2)} and {1,2-dichloroethane (1) + acetic acid (2)} at atmospheric pressure
rhoI	1055.00	kg/m3	293.15	Measurement and modelling of static dielectric constants of aqueous solutions of methanol, ethanol and acetic acid at T = 293.15 K and 91.3 kPa
rhoI	1055.01	kg/m3	288.20	The impact of uni-univalent electrolytes on (water + acetic acid + toluene) equilibria: Representation with electrolyte-NRTL model
rhoI	1043.67	kg/m3	298.20	The impact of uni-univalent electrolytes on (water + acetic acid + toluene) equilibria: Representation with electrolyte-NRTL model

rho1	1026.72	kg/m3	313.20	The impact of uni-univalent electrolytes on (water + acetic acid + toluene) equilibria: Representation with electrolyte-NRTL model
rho1	1053.00	kg/m3	288.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rho1	1052.00	kg/m3	293.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rho1	1042.00	kg/m3	298.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rho1	1037.00	kg/m3	303.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rho1	1025.00	kg/m3	313.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rho1	1015.00	kg/m3	323.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume

rhoI	1004.00	kg/m3	333.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhoI	993.00	kg/m3	343.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhoI	1044.12	kg/m3	298.15	Liquid Phase Equilibria of Aqueous Mixtures of Carboxylic Acids (C1-C4) with Ethylbenzene: Thermodynamic and Mathematical Modeling
rhoI	1048.93	kg/m3	293.15	Liquid-Liquid Phase Equilibria for Quinary, Quaternary, and Ternary Systems {Water + Furfural + Acetic Acid + Cyclopentyl Methyl Ether + CaCl ₂ }: Measurement, Effect of Salt, and Comparative Study
rhoI	1052.50	kg/m3	293.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid
rhoI	1046.90	kg/m3	298.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid

rhoI	1041.40	kg/m3	303.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid
rhoI	1035.80	kg/m3	308.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid
rhoI	1030.00	kg/m3	313.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid
rhoI	1049.50	kg/m3	293.00	Quaternary Liquid-Liquid Equilibrium of Water + Acetic Acid + Propionic Acid + Solvent (Amyl Alcohol, Cyclohexyl Acetate, or Toluene) Systems
rhoI	1049.42	kg/m3	293.20	Liquid liquid equilibria of the ternary system water + acetic acid + dimethyl succinate
rhoI	1043.60	kg/m3	298.15	Vapor liquid equilibria for the quaternary reactive system ethyl acetate + ethanol + water + acetic acid and some of the constituent binary systems at 101.3 kPa
rhoI	1044.30	kg/m3	298.15	Liquid liquid equilibria of ternary systems (water + carboxylic acid + cumene) at 298.15K

rho1	1044.70 ± 0.10	kg/m3	293.15	Determination and correlation of liquid liquid equilibria for the (water + carboxylic acid + dimethyl maleate) ternary systems at T = 298.2K
rho1	1043.90 ± 0.01	kg/m3	298.15	Study of liquid liquid equilibrium of the systems isobutyl acetate + acetic acid +water and isobutyl alcohol + acetic acid +water at different temperatures
rho1	1044.30 ± 0.01	kg/m3	293.15	Phase equilibrium of (water + formic or acetic acid + ethyl heptanoate) ternary liquid systems at different temperatures
rho1	1042.50 ± 0.10	kg/m3	298.15	Isobaric vapor-liquid equilibrium for water + acetic acid + 1-butyl-3-methylimidazolium dibutylphosphate at 101.32 kPa
rho1	1049.42 ± 0.01	kg/m3	298.20	(Liquid + liquid) equilibria of the (water + carboxylic acid + dibasic esters mixture (DBE-2)) ternary systems
rho1	1049.42 ± 0.01	kg/m3	298.15	Liquid-liquid equilibria of water + acetic acid + 2-ethyl hexyl acetate ternary system

rho	1043.50 ± 0.10	kg/m ³	298.15	Isobaric vapor-liquid equilibrium of the binary system sec-butyl acetate + para-xylene and the quaternary system methyl acetate + para-xylene + sec-butyl acetate + acetic acid at 101.3 kPa
rho	1049.63 ± 0.05	kg/m ³	96.64	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rho	1043.57 ± 0.05	kg/m ³	96.64	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rho	1037.64 ± 0.05	kg/m ³	96.64	Solubility, Thermodynamic Properties, and Derived Excess Properties of Benzoic Acid in (Acetic Acid + Water) and (Acetic Acid + Toluene) Binary Mixtures
rho	1049.30 ± 0.00	kg/m ³	293.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure

rho	1043.65 ± 0.00	kg/m ³	298.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
rho	1038.00 ± 0.00	kg/m ³	303.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
rho	1047.22	kg/m ³	298.20	Liquid-Liquid Equilibria of Water + Acetic Acid + Dimethyl Glutarate Ternary System
rho	1044.30 ± 0.10	kg/m ³	298.15	Measurements of Quaternary Liquid-Liquid Equilibrium for Water + Acetic Acid + Propionic Acid + Solvent (Butyronitrile, Benzyl Acetate, or Methyl Isobutyl Ketone) at 298.15 K
rho	1043.95 ± 0.10	kg/m ³	298.15	Refractive Index, Surface Tension, and Density of Aqueous Mixtures of Carboxylic Acids at 298.15 K

rho	1050.00	kg/m ³	293.15	Solubilities of Some Phosphaspirocyclic Compounds in Selected Solvents
rho	1049.42 ± 0.01	kg/m ³	298.15	Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures of Methanol, Ethanoic Acid, and Propanoic Acid
rho	1049.00	kg/m ³	293.15	Solubilities of Phosphorus-Containing Compounds in Selected Solvents
rho	1049.42	kg/m ³	298.15	Geometric Structures of Associating Component Optimized toward Correlation and Prediction of Isobaric Vapor Liquid Equilibria for Binary and Ternary Mixtures of Ethanal, Ethanol, and Ethanoic Acid
rho	1044.11 ± 0.50	kg/m ³	298.15	Investigation on Isobaric Vapor Liquid Equilibrium for Water + Acetic Acid + sec-Butyl Acetate
rho	1049.42 ± 0.01	kg/m ³	298.20	Liquid Phase Equilibria of the Water + Acetic Acid + Dimethyl Carbonate Ternary System at Several Temperatures
rho	1045.00	kg/m ³	298.15	Solubilities of Benzoic Acid and Phthalic Acid in Acetic Acid + Water Solvent Mixtures

rho	1044.30 ± 0.01	kg/m ³	293.15	Liquid-Liquid Equilibria of (Water + Acetic Acid + Diethyl Succinate or Diethyl Glutarate or Diethyl Adipate) Ternary Systems
rho	1043.90	kg/m ³	298.15	Phase Equilibrium for the Esterification Reaction of Acetic Acid + Butan-1-ol at 101.3 kPa
rho	1038.66 ± 0.05	kg/m ³	303.15	Densities and Viscosities of N,N-Dimethylformamide + Formic Acid, and + Acetic Acid in the Temperature Range from (303.15 to 353.15) K
rho	1027.37 ± 0.05	kg/m ³	313.15	Densities and Viscosities of N,N-Dimethylformamide + Formic Acid, and + Acetic Acid in the Temperature Range from (303.15 to 353.15) K
rho	1043.65 ± 0.01	kg/m ³	298.15	Volumetric Properties of Highly Nonideal Binary Mixtures Containing Ethanoic Acid and Propanoic Acid with Butan-2-ol, Methyl-2-propanol, and 2-Methyl-2-butanol at Different Temperatures
rho	1005.04 ± 0.05	kg/m ³	333.15	Densities and Viscosities of N,N-Dimethylformamide + Formic Acid, and + Acetic Acid in the Temperature Range from (303.15 to 353.15) K

rhoI	993.69 ± 0.05	kg/m ³	343.15	Densities and Viscosities of N,N-Dimethylformamide + Formic Acid, and + Acetic Acid in the Temperature Range from (303.15 to 353.15) K
rhoI	982.95 ± 0.05	kg/m ³	353.15	Densities and Viscosities of N,N-Dimethylformamide + Formic Acid, and + Acetic Acid in the Temperature Range from (303.15 to 353.15) K
rhoI	1047.40 ± 0.10	kg/m ³	298.15	Isobaric Vapor-Liquid Equilibria for the Binary Systems of Acetic Acid + Isopropenyl Acetate, Acetic Acid + Acetylacetone, and Water + Acetylacetone
rhoI	1049.42 ± 0.01	kg/m ³	293.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rhoI	1043.76 ± 0.01	kg/m ³	298.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rhoI	1038.10 ± 0.01	kg/m ³	303.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures

rho	1032.44 ± 0.01	kg/m ³	308.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho	1026.77 ± 0.01	kg/m ³	313.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho	1021.11 ± 0.01	kg/m ³	318.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho	1015.44 ± 0.01	kg/m ³	323.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho	1009.77 ± 0.01	kg/m ³	328.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho	1004.09 ± 0.01	kg/m ³	333.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho	998.38 ± 0.01	kg/m ³	338.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures

rho1	1049.42 ± 0.01	kg/m3	293.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho1	1043.76 ± 0.01	kg/m3	298.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho1	1038.10 ± 0.01	kg/m3	303.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho1	1032.44 ± 0.01	kg/m3	308.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho1	1026.77 ± 0.01	kg/m3	313.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho1	1044.50	kg/m3	298.15	Quaternary phase equilibrium of water-carboxylic acid mixture (formic-propionic acid or acetic-propionic acid)-solvent liquid systems at 298.15 K

rho1	1015.44 ± 0.01	kg/m3	323.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho1	1009.77 ± 0.01	kg/m3	328.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho1	1004.09 ± 0.01	kg/m3	333.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho1	1043.90 ± 0.01	kg/m3	298.15	Liquid-Liquid Equilibria for the System 1-Methyl Propyl Ethanoate (1) + Acetic Acid (2) + Water (3) at (283.15 and 323.15) K
rho1	1046.90 ± 0.01	kg/m3	298.15	Isobaric Vapor-Liquid Equilibria for (Acetic Acid + Cyclohexane) and (Cyclohexane + Acetylacetone) at a Pressure of 101.3 kPa and for (Acetic Acid + Acetylacetone) at a Pressure of 60.0 kPa
rho1	1049.00	kg/m3	293.00	KDB
rho1	1044.30 ± 0.05	kg/m3	293.15	Ternary liquid-liquid phase equilibria of (water-carboxylic acid-1-undecanol) systems at 298.15 K

rho	1049.42	kg/m ³	293.15	Liquid liquid equilibria of the ternary system water + acetic acid + dimethyl succinate
rho	1021.11 ± 0.01	kg/m ³	318.15	Densities and Viscosities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures
rho	1004.01 ± 0.01	kg/m ³	333.15	Volumetric Properties of Highly Nonideal Binary Mixtures Containing Ethanoic Acid and Propanoic Acid with Butan-2-ol, Methyl-2-propanol, and 2-Methyl-2-butanol at Different Temperatures
rho	1015.36 ± 0.01	kg/m ³	323.15	Volumetric Properties of Highly Nonideal Binary Mixtures Containing Ethanoic Acid and Propanoic Acid with Butan-2-ol, Methyl-2-propanol, and 2-Methyl-2-butanol at Different Temperatures
rho	1026.68 ± 0.01	kg/m ³	313.15	Volumetric Properties of Highly Nonideal Binary Mixtures Containing Ethanoic Acid and Propanoic Acid with Butan-2-ol, Methyl-2-propanol, and 2-Methyl-2-butanol at Different Temperatures

rho1	1037.99 ± 0.01	kg/m3	303.15	Volumetric Properties of Highly Nonideal Binary Mixtures Containing Ethanoic Acid and Propanoic Acid with Butan-2-ol, Methyl-2-propanol, and 2-Methyl-2-butanol at Different Temperatures
rho1	1016.08 ± 0.05	kg/m3	323.15	Densities and Viscosities of N,N-Dimethylformamide + Formic Acid, and + Acetic Acid in the Temperature Range from (303.15 to 353.15) K
rho1	1049.31 ± 0.01	kg/m3	293.15	Volumetric Properties of Highly Nonideal Binary Mixtures Containing Ethanoic Acid and Propanoic Acid with Butan-2-ol, Methyl-2-propanol, and 2-Methyl-2-butanol at Different Temperatures
rho1	1043.58 ± 0.01	kg/m3	298.15	Densities, Excess Molar Volumes, Viscosity, and Refractive Indices of Binary Mixtures of Ethanoic Acid and Trichloroethylene with Dimethylbenzenes at Different Temperatures
sfust	40.47	J/mol×K	289.90	NIST Webbook
sfust	38.36	J/mol×K	290.06	NIST Webbook

speedsl	1132.00 ± 0.10	m/s	298.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
speedsl	1149.00 ± 0.10	m/s	293.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
speedsl	1094.85	m/s	313.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid
speedsl	1109.56	m/s	308.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid
speedsl	1126.27	m/s	303.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid

speedsl	1142.78	m/s	298.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid
speedsl	1159.31	m/s	293.15	Probe of Interactions of Acetic and Propionic Acids with 2',3'-N-Epoxypropyl-N-methyl-2-oxopyrrolidinium Salicylate Ionic Liquid
speedsl	1093.09	m/s	313.20	Liquid-liquid equilibrium data and thermophysical properties for ternary systems composed of water, acetic acid and different solvents
speedsl	1115.00 ± 0.10	m/s	303.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
speedsl	1161.15	m/s	293.20	Liquid-liquid equilibrium data and thermophysical properties for ternary systems composed of water, acetic acid and different solvents
srf	0.02 ± 0.00	N/m	343.15	Surface Tension of o-Xylene + Acetic Acid and m-Xylene + Acetic Acid Binary Mixtures from 303.15 K to 343.15 K

srf	0.02 ± 0.00	N/m	333.15	Surface Tension of o-Xylene + Acetic Acid and m-Xylene + Acetic Acid Binary Mixtures from 303.15 K to 343.15 K
srf	0.02 ± 0.00	N/m	323.15	Surface Tension of o-Xylene + Acetic Acid and m-Xylene + Acetic Acid Binary Mixtures from 303.15 K to 343.15 K
srf	0.02 ± 0.00	N/m	318.15	Surface Tension of o-Xylene + Acetic Acid and m-Xylene + Acetic Acid Binary Mixtures from 303.15 K to 343.15 K
srf	0.03 ± 0.00	N/m	313.15	Surface Tension of o-Xylene + Acetic Acid and m-Xylene + Acetic Acid Binary Mixtures from 303.15 K to 343.15 K
srf	0.03 ± 0.00	N/m	308.15	Surface Tension of o-Xylene + Acetic Acid and m-Xylene + Acetic Acid Binary Mixtures from 303.15 K to 343.15 K
srf	0.03 ± 0.00	N/m	303.15	Surface Tension of o-Xylene + Acetic Acid and m-Xylene + Acetic Acid Binary Mixtures from 303.15 K to 343.15 K
srf	0.03 ± 0.00	N/m	298.15	Refractive Index, Surface Tension, and Density of Aqueous Mixtures of Carboxylic Acids at 298.15 K
srf	0.03	N/m	303.20	KDB

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbp	341.30	K	17.00	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	342.87	K	18.47	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	345.03	K	20.01	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	346.41	K	21.29	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	348.49	K	23.18	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	350.35	K	24.92	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	352.88	K	27.44	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems

tbp	355.01	K	29.78	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	357.54	K	32.78	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	359.26	K	34.97	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	363.04	K	39.99	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	368.56	K	48.99	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	372.27	K	55.76	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	374.54	K	60.04	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	376.66	K	64.44	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	379.05	K	69.39	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems

tbp	381.60	K	75.23	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	383.32	K	79.98	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	384.82	K	83.66	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	386.07	K	87.18	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems
tbp	389.58	K	97.08	Study of Vapor-Liquid Equilibria for Acetic Acid + n-Propyl Acetate + Isopropyl Acetate Systems

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logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
nfpas:	NFPA Safety Rating
pc:	Critical Pressure
pt:	Triple Point Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhoL:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sg:	Molar entropy at standard conditions
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tbp:	Boiling point at given pressure
tc:	Critical Temperature
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility
zra:	Rackett Parameter

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