Heptane

Other names:	Dipropylmethane
	Eptani
	Gettysolve-C
	Heptan
	Heptanen
	Heptyl hydride
	NSC 62784
	Skellysolve C
	n-C7H16
	n-Heptane
Inchi:	InChI=1S/C7H16/c1-3-5-7-6-4-2/h3-7H2,1-2H3
InchiKey:	IMNFDUFMRHMDMM-UHFFFAOYSA-N
Formula:	C7H16
SMILES:	CCCCCCC
Mol. weight [g/mol]:	100.20
CAS:	142-82-5

Physical Properties

Property code	Value	Unit	Source
af	0.3490		KDB
aigt	495.93	K	KDB
ap	342.850	K	KDB
chl	-4817.16 ± 0.88	kJ/mol	NIST Webbook
chl	-4817.00 ± 1.50	kJ/mol	NIST Webbook
chl	-4810.30	kJ/mol	NIST Webbook
chl	-4818.70	kJ/mol	NIST Webbook
chl	-4816.91 ± 0.63	kJ/mol	NIST Webbook
chl	-4830.00 ± 120.00	kJ/mol	NIST Webbook
chl	-4815.00 ± 1.00	kJ/mol	NIST Webbook
cpl	223.91	J/mol×K	THERMODYNAMICS OF MIXTURES CONTAINING AMINES. XIV. CpEm OF BENZYLAMINE WITH HEPTANE AT 293.15 K OR WITH METHANOL, 1-PROPANOL OR 1-PENTANOL AT (293.15-308.15) K
dm	0.00	debye	KDB

fll	1.00	% in Air	KDB
flu	7.00	% in Air	KDB
fpo	269.26	K	KDB
gf	8.00	kJ/mol	KDB
gyrad	4.2670		KDB
hcg	4816.91	kJ/mol	KDB
hcn	4464.788	kJ/mol	KDB
hf	-189.30	kJ/mol	NIST Webbook
hf	-187.80 ± 0.79	kJ/mol	NIST Webbook
hf	-187.90	kJ/mol	KDB
hfl	-225.90 ± 1.30	kJ/mol	NIST Webbook
hfl	-224.40 ± 0.79	kJ/mol	NIST Webbook
hfus	14.06	kJ/mol	Measurement of Heat Capacity by Adiabatic Calorimetry and Calculation of Thermodynamic Functions of Standard Substances: Copper, Benzoic Acid, and Heptane (For Calibration of an Adiabatic Calorimeter)
hvap	32.00 ± 0.20	kJ/mol	NIST Webbook
hvap	36.54	kJ/mol	NIST Webbook
hvap	36.55	kJ/mol	NIST Webbook
hvap	36.60 ± 0.10	kJ/mol	NIST Webbook
hvap	36.90	kJ/mol	NIST Webbook
hvap	36.60	kJ/mol	NIST Webbook
hvap	36.66	kJ/mol	NIST Webbook
ie	10.16	eV	NIST Webbook
ie	9.90 ± 0.05	eV	NIST Webbook
ie	9.91	eV	NIST Webbook
ie	9.83 ± 0.15	eV	NIST Webbook
ie	9.93 ± 0.10	eV	NIST Webbook
ie	10.15	eV	NIST Webbook
ie	10.08	eV	NIST Webbook
ie	9.93 ± 0.10	eV	NIST Webbook
log10ws	-4.53		Aqueous Solubility Prediction Method
log10ws	-4.53		Estimated Solubility Method
logp	2.977		Crippen Method
mcvol	109.490	ml/mol	McGowan Method
pc	2760.00 ± 50.66	kPa	NIST Webbook
pc	2730.00 ± 103.42	kPa	NIST Webbook
pc	2730.31 ± 20.68	kPa	NIST Webbook
pc	2750.00 ± 34.50	kPa	NIST Webbook
pc	2770.00 ± 50.66	kPa	NIST Webbook

pc	2736.00 ± 40.53	kPa	NIST Webbook
pc	2736.52 ± 17.23	kPa	NIST Webbook
pc	2735.77 ± 4.05	kPa	NIST Webbook
pc	2775.00 ± 5.00	kPa	NIST Webbook
pc	2734.00 ± 5.00	kPa	NIST Webbook
pc	2735.77 ± 5.06	kPa	NIST Webbook
pc	2734.00 ± 20.00	kPa	NIST Webbook
pc	2801.64 ± 20.26	kPa	NIST Webbook
pc	2730.00 ± 10.00	kPa	NIST Webbook
pc	2740.00 ± 30.00	kPa	NIST Webbook
pc	2730.00 ± 30.00	kPa	NIST Webbook
pc	2723.80 ± 26.70	kPa	NIST Webbook
pc	2736.00	kPa	NIST Webbook
pc	2740.00	kPa	KDB
pc	2730.00 ± 40.00	kPa	NIST Webbook
rhoc	234.71 ± 1.60	kg/m3	NIST Webbook
rhoc	234.07 ± 3.01	kg/m3	NIST Webbook
rhoc	241.49 ± 5.01	kg/m3	NIST Webbook
rhoc	234.47 ± 3.01	kg/m3	NIST Webbook
rhoc	232.47 ± 10.02	kg/m3	NIST Webbook
rhoc	233.47 ± 6.01	kg/m3	NIST Webbook
rhoc	241.49 ± 2.00	kg/m3	NIST Webbook
rhoc	234.47 ± 5.01	kg/m3	NIST Webbook
rhoc	232.47 ± 5.01	kg/m3	NIST Webbook
rhoc	241.49 ± 15.03	kg/m3	NIST Webbook
rhoc	234.67 ± 1.60	kg/m3	NIST Webbook
rhoc	232.47	kg/m3	NIST Webbook
sl	328.86	J/mol×K	NIST Webbook
sl	330.10	J/mol×K	NIST Webbook
sl	326.40	J/mol×K	NIST Webbook
sl	327.98	J/mol×K	NIST Webbook
sl	328.57	J/mol×K	NIST Webbook
tb	371.65 ± 1.50	K	NIST Webbook
tb	371.58 ± 0.05	K	NIST Webbook
tb	371.55 ± 0.50	K	NIST Webbook
tb	371.60 ± 0.50	K	NIST Webbook
tb	371.60 ± 0.20	K	NIST Webbook
tb	371.55 ± 0.30	K	NIST Webbook
tb	371.60 ± 0.50	K	NIST Webbook
tb	371.60 ± 0.20	K	NIST Webbook
tb	371.71 ± 0.20	K	NIST Webbook
tb	371.35 ± 0.50	K	NIST Webbook
tb	371.90 ± 1.50	K	NIST Webbook
tb	371.46 ± 0.25	K	NIST Webbook

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tb	371.49 ± 0.30	K	NIST Webbook
tb	371.30 ± 0.80	K	NIST Webbook
tb	371.30 ± 1.00	K	NIST Webbook
tb	371.45 ± 1.50	K	NIST Webbook
tb	371.15 ± 1.00	K	NIST Webbook
tb	371.15 ± 2.00	K	NIST Webbook
tb	371.90 ± 1.50	K	NIST Webbook
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tb	371.55 ± 0.20	K	NIST Webbook
tb	371.15 ± 2.00	K	NIST Webbook
tb	371.60	K	KDB
tb	371.47	K	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
tb	371.35	K	Measurements and correlation of vapour liquid equilibria of 2-butanone and hydrocarbons binary systems at two different pressures
tb	371.64	K	Isobaric vapor-liquid equilibrium for four binary systems of thiophene
tb	371.64	K	Isobaric vapor-liquid equilibrium for four binary systems of 3-methylthiophene
tb	371.40	K	Isobaric vapor-liquid equilibrium for binary systemsof toluene + o-xylene, benzene + o-xylene, nonane + benzene and nonane + heptane at 101.3 kPa

tb	371.64	K	Isobaric vapor-liquid equilibrium for systems containing sulfur compounds
tb	371.56	K	Solutions of alkyl methanoates and alkanes: Simultaneous modeling of phase equilibria and mixing properties. Estimation of behavior by UNIFAC with recalculation of parameters
tb	371.50	K	Excess molar volumes of the ternary system {methylcyclohexane (1) + cyclohexane (2) + n-alkanes (3)} at T = 298.15 K
tb	371.53	K	Isobaric vapor-liquid equilibrium of three binary systems containing dimethyl succinate, dimethyl glutarate and dimethyl adipate at 2, 5.2 and 8.3 kPa
tb	371.35	K	Excess volumes, densities, speeds of sound and viscosities for the binary systems of diisopropyl ether with hydrocarbons at 303.15K
tb	371.28	K	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
tb	370.97	K	A New Test System for Distillation Efficiency Experiments at Elevated Liquid Viscosities: Vapor-Liquid Equilibrium and Liquid Viscosity Data for Cyclopentanol + Cyclohexanol
tb	371.35	K	Isobaric Vapor-Liquid Equilibria and Excess Properties for the Binary Systems of Methyl Esters + Heptane
tb	371.18	K	Densities and Excess Molar Properties of Dimethyl Carbonate with Alkanes (C6 to C10) and VLE of Dimethyl Carbonate with Alkanes (C9 to C10) at 101.3 kPa
tb	371.56	K	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

tb	371.50	K	Vapor-Liquid Equilibrium in the Binary Systems 2-Butanol + tert-Amyl Methyl Ether, 2-Butanol + Heptane, and Heptane + tert-Amyl Methyl Ether
tb	371.65	K	Isobaric Vapor-Liquid Equilibria of Heptane + 1-Butanol and Heptane + 1-Pentanol Systems at (53.3 and 91.3) kPa
tb	371.50 ± 0.20	K	NIST Webbook
tb	371.46 ± 0.10	K	NIST Webbook
tb	371.55 ± 0.10	K	NIST Webbook
tb	371.80 ± 0.30	K	NIST Webbook
tb	371.35 ± 0.40	K	NIST Webbook
tb	371.55 ± 0.30	K	NIST Webbook
tb	371.46 ± 0.10	K	NIST Webbook
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tb	370.65 ± 1.50	K	NIST Webbook

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tb	371.54 ± 0.10	K	NIST Webbook
tb	371.55 ± 0.50	K	NIST Webbook
tb	371.57 ± 0.01	K	NIST Webbook
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tb	371.20 ± 0.70	K	NIST Webbook
tb	371.54 ± 0.15	K	NIST Webbook
tb	372.00 ± 1.50	K	NIST Webbook
tb	371.55 ± 0.50	K	NIST Webbook
tb	371.55 ± 0.20	K	NIST Webbook
tc	540.16 ± 0.06	K	NIST Webbook
tc	540.20	K	KDB
tc	540.10	K	Measurement of critical properties for binary and ternary mixtures containing potential gasoline additive diethyl carbonate (DEC)
tc	540.00	K	Measurement of critical temperatures and critical pressures for binary mixtures of methyl tert-butyl ether (MTBE) + alcohol and MTBE + alkane
tc	540.00	K	Measurement and correlation of critical properties for binary mixtures and ternary mixtures containing gasoline additives
tc	540.16 ± 0.05	K	NIST Webbook
tc	540.50 ± 0.55	K	NIST Webbook
tc	540.53 ± 0.27	K	NIST Webbook
tc	540.30 ± 0.33	K	NIST Webbook
tc	540.28 ± 0.20	K	NIST Webbook

tc	540.60 ± 0.40	K	NIST Webbook
tc	540.00 ± 1.00	K	NIST Webbook
tc	540.00 ± 0.40	K	NIST Webbook
tc	540.00 ± 0.30	K	NIST Webbook
tc	541.00 ± 0.50	K	NIST Webbook
tc	542.70 ± 0.70	K	NIST Webbook
tc	539.90 ± 0.30	K	NIST Webbook
tc	539.86 ± 0.07	K	NIST Webbook
tc	540.20 ± 0.30	K	NIST Webbook
tc	540.68 ± 0.08	K	NIST Webbook
tc	540.20	K	NIST Webbook
tc	540.17 ± 0.10	K	NIST Webbook
tc	540.10	K	NIST Webbook
tc	540.30	K	NIST Webbook
tc	539.80 ± 0.30	K	NIST Webbook
tc	540.40 ± 0.40	K	NIST Webbook
tc	540.00 ± 1.00	K	NIST Webbook
tc	536.70 ± 4.00	K	NIST Webbook
tc	542.65 ± 0.50	K	NIST Webbook
tc	536.80 ± 2.00	K	NIST Webbook
tc	540.20 ± 0.30	K	NIST Webbook
tc	540.14	K	Determination of the Critical Properties of C6 C10 n-Alkanes and Their Binary Systems Using a Flow Apparatus
tc	540.10	K	Measurement of Critical Properties for Binary and Ternary Mixtures Containing n-Butanol and n-Alkane
tc	540.60	K	The Critical Temperatures of a Number of (i) (Chloroalkane (C3 C4) + Hydrocarbon (C6 C7)) Binary Mixtures and (ii) (Aromatic Halocarbon (Chlorobenzene, Fluorobenzene, 1,2-Dichlorobenzene, or 1,3-Dichlorobenzene) + Alkane (C8)) Binary Mixtures
tc	540.14	K	Experimental determination of critical data of multi-component mixtures containing potential gasoline additives 2-butanol by a flow-type apparatus
tf	182.54 ± 0.02	K	NIST Webbook
tf	182.53 ± 0.02	K	NIST Webbook
tf	182.45 ± 0.20	K	NIST Webbook

tf	182.49 ± 0.08	K	NIST Webbook
tf	182.54 ± 0.03	K	NIST Webbook
tf	182.50 ± 0.06	K	NIST Webbook
tf	182.54 ± 0.03	K	NIST Webbook
tf	182.54 ± 0.05	K	NIST Webbook
tf	182.65 ± 0.40	K	NIST Webbook
tf	182.54 ± 0.01	K	NIST Webbook
tf	182.54 ± 0.03	K	NIST Webbook
tf	182.12 ± 0.20	K	NIST Webbook
tf	183.15 ± 2.00	K	NIST Webbook
tf	182.56 ± 0.05	K	NIST Webbook
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tf	182.57 ± 0.10	K	NIST Webbook
tf	182.55 ± 0.20	K	NIST Webbook
tf	182.55 ± 0.20	K	NIST Webbook
tf	182.55 ± 0.20	K	NIST Webbook
tf	182.55 ± 0.20	K	NIST Webbook
tf	182.50	K	KDB
tf	182.31	K	Aqueous Solubility Prediction Method
tf	182.45 ± 0.15	K	NIST Webbook
tf	182.45 ± 0.30	K	NIST Webbook
tf	182.50 ± 0.15	K	NIST Webbook
tf	182.55 ± 0.20	K	NIST Webbook
tf	182.54 ± 0.01	K	NIST Webbook
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tf	182.49 ± 0.15	K	NIST Webbook
tf	182.51 ± 0.20	K	NIST Webbook
tf	182.55 ± 0.20	K	NIST Webbook
tf	183.15 ± 1.50	K	NIST Webbook
tf	182.47 ± 0.20	K	NIST Webbook
tf	182.55 ± 0.07	K	NIST Webbook
tf	182.35 ± 0.30	K	NIST Webbook
tf	182.57 ± 0.08	K	NIST Webbook
tf	182.35 ± 0.40	K	NIST Webbook
tf	183.15 ± 2.00	K	NIST Webbook
tf	183.15 ± 1.50	K	NIST Webbook
tf	182.34 ± 0.30	K	NIST Webbook
tf	182.53 ± 0.15	K	NIST Webbook
tf	182.49 ± 0.20	K	NIST Webbook
tf	182.53 ± 0.10	K	NIST Webbook
tf	181.95 ± 1.00	K	NIST Webbook
tf	182.45 ± 0.50	K	NIST Webbook

tf	182.50 ± 0.08	K	NIST Webbook
tf	182.65 ± 0.50	K	NIST Webbook
tf	182.65 ± 0.50	K	NIST Webbook
tf	182.65 ± 0.40	K	NIST Webbook
tf	183.15 ± 0.30	K	NIST Webbook
tf	176.05 ± 1.00	K	NIST Webbook
tf	182.55 ± 0.40	K	NIST Webbook
tf	182.54 ± 0.02	K	NIST Webbook
tt	182.55	K	KDB
tt	182.60 ± 0.20	K	NIST Webbook
tt	183.20 ± 0.10	K	NIST Webbook
tt	182.57 ± 0.05	K	NIST Webbook
tt	182.59 ± 0.06	K	NIST Webbook
tt	182.59 ± 0.02	K	NIST Webbook
tt	182.70 ± 0.20	K	NIST Webbook
tt	182.56 ± 0.05	K	NIST Webbook
tt	182.55 ± 0.03	K	NIST Webbook
tt	182.55 ± 0.05	K	NIST Webbook
tt	182.55 ± 0.03	K	NIST Webbook
tt	182.56 ± 0.04	K	NIST Webbook
tt	182.56 ± 0.04	K	NIST Webbook
tt	182.55 ± 0.04	K	NIST Webbook
tt	182.55 ± 0.02	K	NIST Webbook
tt	182.55 ± 0.01	K	NIST Webbook
tt	182.53 ± 0.04	K	NIST Webbook
tt	182.53 ± 0.02	K	NIST Webbook
tt	182.56 ± 0.00	K	NIST Webbook
tt	187.57 ± 0.03	K	NIST Webbook
tt	182.56 ± 0.01	K	NIST Webbook
tt	182.55 ± 0.02	K	NIST Webbook
tt	182.56 ± 0.02	K	NIST Webbook
tt	182.55 ± 0.04	K	NIST Webbook
tt	182.55 ± 0.02	K	NIST Webbook
tt	182.56 ± 0.20	K	NIST Webbook
tt	182.56 ± 0.05	K	NIST Webbook
tt	182.56 ± 0.03	K	NIST Webbook
tt	183.56 ± 0.06	K	NIST Webbook
tt	182.56 ± 0.01	K	NIST Webbook
tt	182.20 ± 0.20	K	NIST Webbook
tt	182.56 ± 0.20	K	NIST Webbook
vc	0.428	m3/kmol	KDB
vc	0.428	m3/kmol	NIST Webbook
vc	0.425 ± 0.001	m3/kmol	NIST Webbook

volm	1.47e-04	m3/mol	Thermodynamic Study of Heptane + Silicone Mixtures. Excess Volumes and Enthalpies at 298.15 K
volm	1.47e-04	m3/mol	Thermodynamic study of (heptane + amine) mixtures. II. Excess and partial molar volumes at 298.15 K
zc	0.2610980		KDB
zra	0.26		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	191.50 ± 0.19	J/mol×K	357.10	NIST Webbook
cpg	198.78 ± 0.20	J/mol×K	373.15	NIST Webbook
cpg	210.75 ± 0.21	J/mol×K	400.40	NIST Webbook
cpg	225.31 ± 0.23	J/mol×K	434.35	NIST Webbook
cpg	238.49 ± 0.24	J/mol×K	466.10	NIST Webbook
cpl	224.60	J/mol×K	298.15	NIST Webbook
cpl	224.71	J/mol×K	298.15	NIST Webbook
cpl	255.00	J/mol×K	298.15	NIST Webbook
cpl	226.50	J/mol×K	333.15	NIST Webbook
cpl	220.00	J/mol×K	285.00	NIST Webbook
cpl	223.40	J/mol×K	298.00	NIST Webbook
cpl	225.60	J/mol×K	300.00	NIST Webbook
cpl	224.66	J/mol×K	298.15	NIST Webbook
cpl	224.62	J/mol×K	297.86	NIST Webbook
cpl	224.69	J/mol×K	298.15	NIST Webbook
cpl	224.00	J/mol×K	298.00	NIST Webbook
cpl	224.80	J/mol×K	298.15	NIST Webbook
cpl	225.33	J/mol×K	300.00	NIST Webbook
cpl	224.76	J/mol×K	298.15	NIST Webbook
cpl	224.78	J/mol×K	298.15	NIST Webbook
cpl	224.71	J/mol×K	298.15	NIST Webbook
cpl	224.73	J/mol×K	298.15	NIST Webbook
cpl	224.78	J/mol×K	298.15	NIST Webbook
cpl	224.78	J/mol×K	298.15	NIST Webbook
cpl	224.71	J/mol×K	298.15	NIST Webbook
cpl	225.14	J/mol×K	300.00	NIST Webbook
cpl	224.72	J/mol×K	298.15	NIST Webbook
cpl	222.88	J/mol×K	293.15	NIST Webbook

cpl	224.73	J/mol×K	298.15	NIST Webbook	
cpl	224.72	J/mol×K	298.15	NIST Webbook	
cpl	240.03	J/mol×K	333.15	Heat Capacities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures	
cpl	230.37	J/mol×K	313.15	Heat Capacities of Binary Mixtures of Acetic Acid with Acetic Anhydride and Methenamine at Different Temperatures	
cpl	230.87	J/mol×K	313.15	Isobaric Heat Capacity Measurements of Liquid Methane, Ethane, and Propane by Differential Scanning Calorimetry at High Pressures and Low Temperatures	
cpl	229.16	J/mol×K	313.15	Isobaric Heat Capacity Measurements of Liquid Methane, Ethane, and Propane by Differential Scanning Calorimetry at High Pressures and Low Temperatures	
cpl	225.25	J/mol×K	303.15	Isobaric Heat Capacity Measurements of Liquid Methane, Ethane, and Propane by Differential Scanning Calorimetry at High Pressures and Low Temperatures	

cpl	225.96	J/mol×K	303.15	Isobaric Heat Capacity Measurements of Liquid Methane, Ethane, and Propane by Differential Scanning Calorimetry at High Pressures and Low Temperatures	
cpl	205.11	J/mol×K	238.15	Isobaric Heat Capacity Measurements of Liquid Methane, Ethane, and Propane by Differential Scanning Calorimetry at High Pressures and Low Temperatures	
cpl	206.22	J/mol×K	238.15	Isobaric Heat Capacity Measurements of Liquid Methane, Ethane, and Propane by Differential Scanning Calorimetry at High Pressures and Low Temperatures	
cpl	217.00	J/mol×K	303.00	NIST Webbook	
cpl	222.20	J/mol×K	299.20	NIST Webbook	
cpl	224.30	J/mol×K	298.10	NIST Webbook	
cpl	223.00	J/mol×K	298.00	NIST Webbook	
cpl	210.90	J/mol×K	300.80	NIST Webbook	
cpl	211.30	J/mol×K	298.00	NIST Webbook	
cpl	224.60	J/mol×K	296.50	NIST Webbook	
cpl	224.85	J/mol×K	298.15	NIST Webbook	
cpl	224.74	J/mol×K	298.15	NIST Webbook	
cpl	224.74	J/mol×K	298.15	NIST Webbook	
cpl	233.13	J/mol×K	299.80	NIST Webbook	
cpl	247.30	J/mol×K	332.00	NIST Webbook	
cpl	224.93	J/mol×K	298.15	NIST Webbook	
cpl	224.93	J/mol×K	298.15	NIST Webbook	
cpl	328.61	J/mol×K	298.15	NIST Webbook	
cpl	209.60	J/mol×K	250.00	NIST Webbook	
cpl	226.53	J/mol×K	298.15	NIST Webbook	
cpl	225.30	J/mol×K	298.15	NIST Webbook	

cpl	201.51	J/mol×K	228.15	Isobaric Heat Capacity Measurements of Liquid Methane, Ethane, and Propane by Differential Scanning Calorimetry at High Pressures and Low Temperatures
cpl	202.31	J/mol×K	228.15	Isobaric Heat Capacity Measurements of Liquid Methane, Ethane, and Propane by Differential Scanning Calorimetry at High Pressures and Low Temperatures
cpl	230.51	J/mol×K	313.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	230.11	J/mol×K	312.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	229.71	J/mol×K	311.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	229.30	J/mol×K	310.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K

cpl	228.95	J/mol×K	309.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	228.54	J/mol×K	308.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	228.14	J/mol×K	307.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	227.75	J/mol×K	306.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	227.40	J/mol×K	305.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	227.00	J/mol×K	304.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K

cpl	226.61	J/mol×K	303.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	226.22	J/mol×K	302.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	225.87	J/mol×K	301.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	225.47	J/mol×K	300.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	225.10	J/mol×K	299.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	224.72	J/mol×K	298.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K

cpl	224.35	J/mol×K	297.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	223.97	J/mol×K	296.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	223.60	J/mol×K	295.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	223.23	J/mol×K	294.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	222.87	J/mol×K	293.15	Heat Capacity, Speed of Ultrasound, and Density for 1,5-Dibromopentane + Heptane within the Temperature Range from 293.15 K to 313.15 K
cpl	224.64	J/mol×K	298.15	NIST Webbook
cpl	226.53	J/mol×K	303.15	NIST Webbook
cpl	224.19	J/mol×K	298.15	NIST Webbook
dvisc	0.0003920	Pa×s	298.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K

dvisc	0.0003329	Pa×s	313.15	Viscometric and Volumetric Properties of 10 Regular Binary Systems at 308.15 K and 313.15 K	
dvisc	0.0003848	Pa×s	303.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0002834	Pa×s	333.10	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0002562	Pa×s	343.30	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0002382	Pa×s	353.30	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0002207	Pa×s	363.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	

dvisc	0.0002027	Pa×s	373.30	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0001853	Pa×s	383.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0001717	Pa×s	393.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0001590	Pa×s	403.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0001488	Pa×s	413.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0003422	Pa×s	313.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	

dvisc	0.0001392	Pa×s	423.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0001308	Pa×s	433.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0001193	Pa×s	443.40	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0001135	Pa×s	453.10	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0001047	Pa×s	463.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	
dvisc	0.0000978	Pa×s	473.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer	

dvisc	0.0000896	Pa×s	483.10	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0000817	Pa×s	493.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0000745	Pa×s	503.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0004009	Pa×s	298.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0003750	Pa×s	303.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0003373	Pa×s	313.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures

dvisc	0.0003074	Pa×s	323.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0003097	Pa×s	323.00	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0002793	Pa×s	333.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0002541	Pa×s	343.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0004038	Pa×s	293.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Dimethyl Carbonate with Chlorobenzene, Hexane, and Heptane from (293.15 to 353.15) K and at Atmospheric Pressure

dvisc	0.0003831	Pa×s	298.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Dimethyl Carbonate with Chlorobenzene, Hexane, and Heptane from (293.15 to 353.15) K and at Atmospheric Pressure
dvisc	0.0003629	Pa×s	303.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Dimethyl Carbonate with Chlorobenzene, Hexane, and Heptane from (293.15 to 353.15) K and at Atmospheric Pressure
dvisc	0.0003274	Pa×s	313.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Dimethyl Carbonate with Chlorobenzene, Hexane, and Heptane from (293.15 to 353.15) K and at Atmospheric Pressure
dvisc	0.0002980	Pa×s	323.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Dimethyl Carbonate with Chlorobenzene, Hexane, and Heptane from (293.15 to 353.15) K and at Atmospheric Pressure
dvisc	0.0002704	Pa×s	333.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Dimethyl Carbonate with Chlorobenzene, Hexane, and Heptane from (293.15 to 353.15) K and at Atmospheric Pressure

dvisc	0.0003360	Pa×s	313.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K	
dvisc	0.0002487	Pa×s	343.15	Excess Molar Volumes and Viscosities of Binary Mixtures of Dimethyl Carbonate with Chlorobenzene, Hexane, and Heptane from (293.15 to 353.15) K and at Atmospheric Pressure	
dvisc	0.0005260	Pa×s	273.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K	
dvisc	0.0003960	Pa×s	298.15	Densities and Viscosities of Binary Mixtures of Tri-n-butyl Phosphate + Cyclohexane, + n-Heptane at T) (288.15, 293.15, 298.15, 303.15, and 308.15) K	
dvisc	0.0004950	Pa×s	278.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K	
dvisc	0.0004650	Pa×s	283.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K	
dvisc	0.0004150	Pa×s	293.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K	

dvisc	0.0003420	Pa×s	313.15	Volumetric and Viscous Properties at Several Temperatures for Binary Mixtures of N-Methylpiperazine with Methylcyclohexane or n-Heptane	
dvisc	0.0003830	Pa×s	303.15	Volumetric and Viscous Properties at Several Temperatures for Binary Mixtures of N-Methylpiperazine with Methylcyclohexane or n-Heptane	
dvisc	0.0004040	Pa×s	298.15	Volumetric and Viscous Properties at Several Temperatures for Binary Mixtures of N-Methylpiperazine with Methylcyclohexane or n-Heptane	
dvisc	0.0003250	Pa×s	313.15	Density, Viscosity, and Speed of Sound of (Methyl Benzoate + Cyclohexane), (Methyl Benzoate + n-Hexane), (Methyl Benzoate + Heptane), and (Methyl Benzoate + Octane) at Temperatures of (303.15, 308.15, and 313.15) K	
dvisc	0.0003500	Pa×s	308.15	Density, Viscosity, and Speed of Sound of (Methyl Benzoate + Cyclohexane), (Methyl Benzoate + n-Hexane), (Methyl Benzoate + Heptane), and (Methyl Benzoate + Octane) at Temperatures of (303.15, 308.15, and 313.15) K	

dvisc	0.0003750	Pa×s	303.15	Density, Viscosity, and Speed of Sound of (Methyl Benzoate + Cyclohexane), (Methyl Benzoate + n-Hexane), (Methyl Benzoate + Heptane), and (Methyl Benzoate + Octane) at Temperatures of (303.15, 308.15, and 313.15) K	
dvisc	0.0003560	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of Tri-n-butyl Phosphate + Cyclohexane, + n-Heptane at T) (288.15, 293.15, 298.15, 303.15, and 308.15) K	
dvisc	0.0003750	Pa×s	303.15	Densities and Viscosities of Binary Mixtures of Tri-n-butyl Phosphate + Cyclohexane, + n-Heptane at T) (288.15, 293.15, 298.15, 303.15, and 308.15) K	
dvisc	0.0004380	Pa×s	288.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K	
dvisc	0.0004170	Pa×s	293.15	Densities and Viscosities of Binary Mixtures of Tri-n-butyl Phosphate + Cyclohexane, + n-Heptane at T) (288.15, 293.15, 298.15, 303.15, and 308.15) K	
dvisc	0.0004410	Pa×s	288.15	Densities and Viscosities of Binary Mixtures of Tri-n-butyl Phosphate + Cyclohexane, + n-Heptane at T) (288.15, 293.15, 298.15, 303.15, and 308.15) K	

dvisc	0.0003374	Pa×s	313.15	Densities and Viscosities of Ternary Mixtures of Heptane, Octane, Nonane, and Hexyl Benzene from 293.15 K to 313.15 K	
dvisc	0.0003541	Pa×s	308.15	Densities and Viscosities of Ternary Mixtures of Heptane, Octane, Nonane, and Hexyl Benzene from 293.15 K to 313.15 K	
dvisc	0.0003728	Pa×s	303.15	Densities and Viscosities of Ternary Mixtures of Heptane, Octane, Nonane, and Hexyl Benzene from 293.15 K to 313.15 K	
dvisc	0.0003928	Pa×s	298.15	Densities and Viscosities of Ternary Mixtures of Heptane, Octane, Nonane, and Hexyl Benzene from 293.15 K to 313.15 K	
dvisc	0.0004142	Pa×s	293.15	Densities and Viscosities of Ternary Mixtures of Heptane, Octane, Nonane, and Hexyl Benzene from 293.15 K to 313.15 K	
dvisc	0.0003540	Pa×s	308.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K	
dvisc	0.0003720	Pa×s	303.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K	

dvisc	0.0003497	Pa×s	308.15	Viscometric and Volumetric Properties of 10 Regular Binary Systems at 308.15 K and 313.15 K
hfust	14.06	kJ/mol	182.56	NIST Webbook
hfust	14.16	kJ/mol	182.20	NIST Webbook
hfust	14.16	kJ/mol	182.20	NIST Webbook
hfust	14.04	kJ/mol	182.60	NIST Webbook
hfust	14.04	kJ/mol	182.60	NIST Webbook
hfust	14.03	kJ/mol	182.56	NIST Webbook
hfust	14.04	kJ/mol	182.52	NIST Webbook
hfust	14.02	kJ/mol	182.56	NIST Webbook
hfust	14.02	kJ/mol	182.56	NIST Webbook
hfust	14.04	kJ/mol	182.55	NIST Webbook
hfust	14.05	kJ/mol	182.59	NIST Webbook
hfust	13.99	kJ/mol	182.57	NIST Webbook
hfust	14.04	kJ/mol	182.55	NIST Webbook
hfust	14.06	kJ/mol	182.70	NIST Webbook
hsubt	57.90	kJ/mol	183.00	NIST Webbook
hvapt	35.60 ± 0.10	kJ/mol	313.00	NIST Webbook
hvapt	36.10	kJ/mol	330.50	NIST Webbook
hvapt	36.40	kJ/mol	318.00	NIST Webbook
hvapt	34.50 ± 0.10	kJ/mol	331.00	NIST Webbook
hvapt	36.10	kJ/mol	318.00	NIST Webbook
hvapt	35.40	kJ/mol	355.50	NIST Webbook
hvapt	36.00	kJ/mol	335.50	NIST Webbook
hvapt	32.00	kJ/mol	371.00	NIST Webbook
hvapt	35.50	kJ/mol	353.50	NIST Webbook
hvapt	34.40 ± 0.10	kJ/mol	333.00	NIST Webbook
hvapt	36.10	kJ/mol	336.00	NIST Webbook
hvapt	35.20	kJ/mol	360.50	NIST Webbook
hvapt	34.70	kJ/mol	350.50	NIST Webbook
hvapt	31.77	kJ/mol	371.60	NIST Webbook
hvapt	36.72	kJ/mol	298.00	Enthalpies of Vaporization and Vapor Pressures of Some Deuterated Hydrocarbons. Liquid-Vapor Pressure Isotope Effects
hvapt	31.70	kJ/mol	371.60	KDB
hvapt	33.10 ± 0.10	kJ/mol	353.00	NIST Webbook
hvapt	33.20 ± 0.10	kJ/mol	350.00	NIST Webbook

kvisc	0.0000005	m2/s	313.15	Experimental and Predicted Kinematic Viscosities for Alkane + Chloroalkane Mixtures
kvisc	0.0000006	m2/s	298.15	Experimental and Predicted Kinematic Viscosities for Alkane + Chloroalkane Mixtures
kvisc	0.0000005	m2/s	313.15	Kinematic Viscosities for Ether + Alkane Mixtures: Experimental Results and UNIFAC-VISCO Parameters
kvisc	0.0000006	m2/s	298.15	Kinematic Viscosities for Ether + Alkane Mixtures: Experimental Results and UNIFAC-VISCO Parameters
kvisc	0.0000007	m2/s	283.15	Experimental and Predicted Kinematic Viscosities for Alkane + Chloroalkane Mixtures
kvisc	0.0000007	m2/s	283.15	Kinematic Viscosities for Ether + Alkane Mixtures: Experimental Results and UNIFAC-VISCO Parameters
pvap	20.00	kPa	324.56	Measurements and correlation of vapour liquid equilibria of 2-butanone and hydrocarbons binary systems at two different pressures
pvap	1604.13	kPa	503.59	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry

pvap	1699.51	kPa	507.39	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	1793.01	kPa	510.95	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	1911.60	kPa	515.27	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	2019.09	kPa	518.99	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	2116.11	kPa	522.22	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	2219.70	kPa	525.53	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	2309.81	kPa	528.30	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	2416.50	kPa	531.47	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	2525.68	kPa	534.57	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	2621.76	kPa	537.20	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry

pvap	1.53	kPa	273.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	2.76	kPa	283.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	4.74	kPa	293.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	6.10	kPa	298.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	7.79	kPa	303.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)

pvap	12.32	kPa	313.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	18.85	kPa	323.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	27.99	kPa	333.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	40.43	kPa	343.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	80.00	kPa	363.74	Isobaric vapor liquid equilibria for the n-hexane + 2-isopropoxyethanol and n-heptane + 2-isopropoxyethanol systems

pvap	1518.18	kPa	500.01	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	8.32	kPa	305.26	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	10.55	kPa	310.22	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	13.09	kPa	314.93	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	14.07	kPa	316.50	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	16.19	kPa	319.71	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	19.10	kPa	323.62	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	21.45	kPa	326.44	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	23.79	kPa	329.04	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	26.14	kPa	331.48	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	27.97	kPa	333.21	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	30.51	kPa	335.50	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	

pvap	32.84	kPa	337.48	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	35.53	kPa	339.56	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	37.87	kPa	341.35	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	40.12	kPa	342.96	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	42.35	kPa	344.47	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	44.75	kPa	346.04	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	46.71	kPa	347.28	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	49.09	kPa	348.72	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	51.49	kPa	350.12	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	53.41	kPa	351.21	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	55.76	kPa	352.49	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	57.88	kPa	353.62	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	60.18	kPa	354.79	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	63.11	kPa	356.25	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	66.42	kPa	357.84	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	68.27	kPa	358.68	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	71.15	kPa	359.98	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	74.25	kPa	361.33	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	76.55	kPa	362.30	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	79.00	kPa	363.32	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	81.28	kPa	364.24	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	84.05	kPa	365.32	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	86.30	kPa	366.20	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	88.10	kPa	366.87	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	

pvap	91.09	kPa	367.97	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	93.46	kPa	368.83	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	96.33	kPa	369.84	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	98.98	kPa	370.85	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	78.59	kPa	363.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)	
pvap	100.68	kPa	371.35	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	

pvap	101.32	kPa	371.56	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	103.92	kPa	372.42	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	106.48	kPa	373.25	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	108.71	kPa	373.98	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	111.77	kPa	374.93	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	113.35	kPa	375.41	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	116.21	kPa	376.29	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	119.14	kPa	377.17	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	120.32	kPa	377.51	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	123.70	kPa	378.49	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	126.80	kPa	379.37	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	130.00	kPa	380.26	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	

pvap	132.04	kPa	380.83	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	182.39	kPa	392.89	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	186.60	kPa	393.79	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	189.67	kPa	394.43	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	192.97	kPa	395.10	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	196.04	kPa	395.73	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	197.85	kPa	396.09	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	199.97	kPa	396.50	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	1.54	kPa	273.15	Excess Properties and Vapor Pressure of 2-Diethylaminoethylamine + n-Heptane
pvap	4.76	kPa	293.15	Excess Properties and Vapor Pressure of 2-Diethylaminoethylamine + n-Heptane
pvap	6.14	kPa	298.15	Excess Properties and Vapor Pressure of 2-Diethylaminoethylamine + n-Heptane
pvap	7.83	kPa	303.15	Excess Properties and Vapor Pressure of 2-Diethylaminoethylamine + n-Heptane
pvap	12.39	kPa	313.15	Excess Properties and Vapor Pressure of 2-Diethylaminoethylamine + n-Heptane
pvap	18.96	kPa	323.15	Excess Properties and Vapor Pressure of 2-Diethylaminoethylamine + n-Heptane
pvap	28.14	kPa	333.15	Excess Properties and Vapor Pressure of 2-Diethylaminoethylamine + n-Heptane

pvap	40.64	kPa	343.15	Excess Properties and Vapor Pressure of 2-Diethylaminoethylamine + n-Heptane
pvap	57.27	kPa	353.15	Excess Properties and Vapor Pressure of 2-Diethylaminoethylamine + n-Heptane
pvap	78.94	kPa	363.15	Excess Properties and Vapor Pressure of 2-Diethylaminoethylamine + n-Heptane
pvap	12.33	kPa	313.15	Vapor-Liquid Equilibria of Binary Mixtures Containing 1-Butanol and Hydrocarbons at 313.15 K
pvap	12.33	kPa	313.15	Vapor Liquid Equilibria of Binary Mixtures Containing 2-Butanol and Hydrocarbons at 313.15 K
pvap	477.00	kPa	433.15	In Situ Determination of Phase Equilibria of Methyl Benzoate + Alkane Mixtures Using an Infrared Absorption Method. Comparison with Polar GC-SAFT Predictions
pvap	587.00	kPa	443.15	In Situ Determination of Phase Equilibria of Methyl Benzoate + Alkane Mixtures Using an Infrared Absorption Method. Comparison with Polar GC-SAFT Predictions

pvap	703.00	kPa	453.15	In Situ Determination of Phase Equilibria of Methyl Benzoate + Alkane Mixtures Using an Infrared Absorption Method. Comparison with Polar GC-SAFT Predictions
pvap	1443.40	kPa	496.77	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	1384.19	kPa	494.11	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	1313.39	kPa	490.81	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	100.00	kPa	371.11	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	60.00	kPa	354.72	Isobaric vapor liquid equilibria for the n-hexane + 2-isopropoxyethanol and n-heptane + 2-isopropoxyethanol systems
pvap	1242.28	kPa	487.36	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	1169.38	kPa	483.67	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	1092.41	kPa	479.57	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry

pvap	1030.55	kPa	476.11	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	983.90	kPa	473.39	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	925.23	kPa	469.84	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	850.62	kPa	465.07	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	773.29	kPa	459.78	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	726.16	kPa	456.35	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	666.97	kPa	451.80	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	619.76	kPa	447.95	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	568.27	kPa	443.50	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	518.27	kPa	438.86	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	467.65	kPa	433.81	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	420.15	kPa	428.69	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry

pvap	378.80	kPa	423.85	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	341.76	kPa	419.17	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	302.76	kPa	413.80	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	275.09	kPa	409.66	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	248.92	kPa	405.44	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	224.89	kPa	401.26	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	200.79	kPa	396.70	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	185.50	kPa	393.58	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	166.41	kPa	389.41	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	145.56	kPa	384.39	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	120.89	kPa	377.68	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	110.39	kPa	374.50	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry

pvap	102.90	kPa	372.08	Vapor Pressures of n-Heptane Determined by Comparative Ebulliometry
pvap	101.30	kPa	370.97	A New Test System for Distillation Efficiency Experiments at Elevated Liquid Viscosities: Vapor-Liquid Equilibrium and Liquid Viscosity Data for Cyclopentanol + Cyclohexanol
pvap	57.10	kPa	353.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
pvap	40.60	kPa	343.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
pvap	28.20	kPa	333.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K

pvap	19.00	kPa	323.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
pvap	12.40	kPa	313.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
pvap	7.90	kPa	303.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
pvap	100.00	kPa	371.58	Isobaric Vapor-Liquid Equilibrium for Two Binary Systems of n-Heptane + sec-Butyl Acetate and Methylcyclohexane + sec-Butyl Acetate under Atmosphere
pvap	85.00	kPa	365.65	Experimental Vapor-Liquid Equilibria and Thermodynamic Modeling of the Methanol + n-Heptane and 1-Butanol + Aniline Binary Systems

pvap	23.04	kPa	328.15	Isothermal Vapor-Liquid Equilibria for Binary Mixtures of Methyl Nonafluorobutyl Ether + Acetone, Cyclopentyl Methyl Ether, Ethyl Acetate, n-Heptane, Methanol, and Toluene
pvap	18.90	kPa	323.15	Measurement and Correlation of Isothermal Binary Vapor Liquid Equilibrium for Diethyl Carbonate + Isooctane/n-Heptane/Toluene Systems
pvap	56.99	kPa	353.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	15.33	kPa	318.15	Measurement and Correlation of Isothermal Binary Vapor Liquid Equilibrium for Diethyl Carbonate + Isooctane/n-Heptane/Toluene Systems
pvap	12.34	kPa	313.15	Measurement and Correlation of Isothermal Binary Vapor Liquid Equilibrium for Diethyl Carbonate + Isooctane/n-Heptane/Toluene Systems

pvap	9.85	kPa	308.15	Measurement and Correlation of Isothermal Binary Vapor Liquid Equilibrium for Diethyl Carbonate + Isooctane/n-Heptane/Toluene Systems
pvap	7.79	kPa	303.15	Measurement and Correlation of Isothermal Binary Vapor Liquid Equilibrium for Diethyl Carbonate + Isooctane/n-Heptane/Toluene Systems
pvap	57.09	kPa	353.15	Vapor Liquid Equilibrium and Excess Enthalpy Data for Systems Containing N,N-Dimethylacetamide
pvap	60.00	kPa	354.63	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
pvap	26.15	kPa	331.39	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
pvap	30.59	kPa	335.45	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
pvap	38.89	kPa	341.94	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
pvap	46.80	kPa	347.16	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane

pvap	50.97	kPa	349.68	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
pvap	56.20	kPa	352.58	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
pvap	64.60	kPa	356.78	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
pvap	70.24	kPa	359.38	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
pvap	76.47	kPa	362.11	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
pvap	83.45	kPa	364.95	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
pvap	88.40	kPa	366.87	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
pvap	101.30	kPa	371.28	Vapor Liquid Equilibria Measurements for Di-n-Propyl Ether and Butyl Ethyl Ether with n-Heptane
pvap	94.00	kPa	368.85	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane

pvap	6.10	kPa	298.15	Thermophysical Study of the n-Hexane or n-Heptane with 1-Chloropropane Systems	
pvap	101.30	kPa	371.53	Isobaric vapor-liquid equilibrium of three binary systems containing dimethyl succinate, dimethyl glutarate and dimethyl adipate at 2, 5.2 and 8.3 kPa	
pvap	18.91	kPa	323.15	Measurement and correlation of (vapor + liquid) equilibria for the {2-propoxyethanol (C3E1) + n-hexane} and the {2-propoxyethanol (C3E1) + n-heptane} systems	
pvap	93.32	kPa	368.70	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components	
pvap	79.99	kPa	363.64	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components	
pvap	66.66	kPa	357.85	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components	
pvap	53.33	kPa	351.08	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components	

pvap	40.00	kPa	342.77	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components	
pvap	101.46	kPa	371.66	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa	
pvap	101.30	kPa	371.47	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa	
pvap	86.56	kPa	366.23	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa	
pvap	81.76	kPa	364.36	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa	
pvap	80.00	kPa	363.67	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa	
pvap	79.55	kPa	363.44	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa	

pvap	75.87	kPa	362.03	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	67.99	kPa	358.49	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	63.98	kPa	356.61	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	58.57	kPa	353.90	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	53.30	kPa	351.14	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	50.62	kPa	349.53	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa

pvap	12.24	kPa	313.15	Measurement and correlation of (vapor + liquid) equilibria for the {2-propoxyethanol (C3E1) + n-hexane} and the {2-propoxyethanol (C3E1) + n-heptane} systems	
pvap	42.88	kPa	344.76	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa	
pvap	35.66	kPa	339.70	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa	
pvap	32.24	kPa	336.95	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa	
pvap	29.69	kPa	334.81	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa	
pvap	26.49	kPa	331.82	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa	

pvap	7.92	kPa	303.15	Measurement and correlation of (vapor + liquid) equilibria for the {2-propoxyethanol (C3E1) + n-hexane} and the {2-propoxyethanol (C3E1) + n-heptane} systems
pvap	18.95	kPa	323.15	Phase equilibria for mixtures containing nonionic surfactant systems: Modeling and experiments
pvap	12.33	kPa	313.15	Phase equilibria for mixtures containing nonionic surfactant systems: Modeling and experiments
pvap	7.87	kPa	303.15	Phase equilibria for mixtures containing nonionic surfactant systems: Modeling and experiments
pvap	40.43	kPa	343.15	Excess properties and vapour pressure of (3-diethylaminopropylamine + n-alkanes)
pvap	27.98	kPa	333.15	Excess properties and vapour pressure of (3-diethylaminopropylamine + n-alkanes)
pvap	18.85	kPa	323.15	Excess properties and vapour pressure of (3-diethylaminopropylamine + n-alkanes)
pvap	12.32	kPa	313.15	Excess properties and vapour pressure of (3-diethylaminopropylamine + n-alkanes)

pvap	7.79	kPa	303.15	Excess properties and vapour pressure of (3-diethylaminopropylamine + n-alkanes)	
pvap	9.87	kPa	308.15	Experimental and predicted vapour-liquid equilibrium of the binary mixtures n-heptane + chlorobutane isomers	
pvap	6.09	kPa	298.15	Experimental and predicted vapour-liquid equilibrium of the binary mixtures n-heptane + chlorobutane isomers	
pvap	3.63	kPa	288.15	Experimental and predicted vapour-liquid equilibrium of the binary mixtures n-heptane + chlorobutane isomers	
pvap	57.56	kPa	353.01	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	40.62	kPa	343.04	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	28.13	kPa	333.07	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	

pvap	18.98	kPa	323.10	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	12.41	kPa	313.12	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	7.81	kPa	303.15	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	4.77	kPa	293.25	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	2.77	kPa	283.21	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	1.55	kPa	273.27	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	

pvap	0.82	kPa	263.45	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions
pvap	100.00	kPa	371.20	Isobaric vapor liquid equilibria for the n-hexane + 2-isopropoxyethanol and n-heptane + 2-isopropoxyethanol systems
pvap	2190.00	kPa	523.20	A novel continuous flow apparatus with a video camera system for high pressure phase equilibrium measurements
pvap	2180.00	kPa	523.20	A novel continuous flow apparatus with a video camera system for high pressure phase equilibrium measurements
pvap	2170.00	kPa	523.20	A novel continuous flow apparatus with a video camera system for high pressure phase equilibrium measurements
pvap	1470.00	kPa	498.20	A novel continuous flow apparatus with a video camera system for high pressure phase equilibrium measurements
pvap	1460.00	kPa	498.20	A novel continuous flow apparatus with a video camera system for high pressure phase equilibrium measurements

pvap	1490.00	kPa	498.20	A novel continuous flow apparatus with a video camera system for high pressure phase equilibrium measurements	
pvap	980.00	kPa	473.20	A novel continuous flow apparatus with a video camera system for high pressure phase equilibrium measurements	
pvap	980.00	kPa	473.10	A novel continuous flow apparatus with a video camera system for high pressure phase equilibrium measurements	
pvap	960.00	kPa	473.30	A novel continuous flow apparatus with a video camera system for high pressure phase equilibrium measurements	
pvap	12.34	kPa	313.15	Phase equilibrium properties of the ternary mixture dibutyl ether + toluene + heptane at 313.15 K	
pvap	101.30	kPa	371.35	Measurements and correlation of vapour liquid equilibria of 2-butanone and hydrocarbons binary systems at two different pressures	
pvap	47.80	kPa	347.85	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa	

pvap	12.31	kPa	313.15	Thermodynamic behaviour of second generation biofuels: Vapour liquid equilibria and excess enthalpies of the binary mixtures 2-pentanol and n-heptane or 2,2,4-trimethylpentane
rfi	1.38511		298.15	KDB
rfi	1.38850		298.10	Excess Enthalpies and Thermal Conductivity Coefficients for Binary Mixtures of Carbon Tetrachloride and Four Alkanes (C5 to C8) at a Temperature of 298.15 K
rfi	1.38530		298.15	Improvements in the Experimentation and the Representation of Thermodynamic Properties (iso-p VLE and yE) of Alkyl Propanoate + Alkane Binaries
rfi	1.38770		293.15	Vapor Liquid Equilibrium Data for the Morpholine-4-carbaldehyde + n-Hexane or n-Heptane Binary Systems Using a Static-Synthetic Apparatus
rfi	1.37480		318.15	Multiproperty Correlation of Experimental Data of the Binaries Propyl Ethanoate + Alkanes (Pentane to Decane). New Experimental Information for Vapor Liquid Equilibrium and Mixing Properties

rfi	1.38520	298.15	Multiproperty Correlation of Experimental Data of the Binaries Propyl Ethanoate + Alkanes (Pentane to Decane). New Experimental Information for Vapor Liquid Equilibrium and Mixing Properties
rfi	1.38530	298.15	Measurements and Correlations of the Isobaric Vapor Liquid Equilibria of Binary Mixtures and Excess Properties for Mixtures Containing an Alkyl (Methyl, Ethyl) Butanoate with an Alkane (Heptane, Nonane) at 101.3 kPa
rfi	1.38515	298.15	Extraction of Benzene from Aliphatic Compounds Using Commercial Ionic Liquids as Solvents: Study of the Liquid Liquid Equilibrium at T = 298.15 K
rfi	1.37197	323.15	Experimental Determination of Densities and Refractive Indices of the Ternary Mixture 2-Methyl-2-propanol + Cyclohexylamine + n-Heptane at T = (303.15 to 323.15) K

rfi	1.37463	318.15	Experimental Determination of Densities and Refractive Indices of the Ternary Mixture 2-Methyl-2-propanol + Cyclohexylamine + n-Heptane at T = (303.15 to 323.15) K
rfi	1.37731	313.15	Experimental Determination of Densities and Refractive Indices of the Ternary Mixture 2-Methyl-2-propanol + Cyclohexylamine + n-Heptane at T = (303.15 to 323.15) K
rfi	1.37995	308.15	Experimental Determination of Densities and Refractive Indices of the Ternary Mixture 2-Methyl-2-propanol + Cyclohexylamine + n-Heptane at T = (303.15 to 323.15) K
rfi	1.38259	303.15	Experimental Determination of Densities and Refractive Indices of the Ternary Mixture 2-Methyl-2-propanol + Cyclohexylamine + n-Heptane at T = (303.15 to 323.15) K
rfi	1.38515	298.15	Separation of Benzene from Linear Alkanes (C6-C9) Using 1-Ethyl-3-Methylimidazolium Ethylsulfate at T = 298.15 K
rfi	1.38530	298.15	Vapor-Liquid Equilibrium for Binary System of Diethyl Sulfide + n-Heptane and Diethyl Sulfide + 2,2,4-Trimethylpentane at (363.15 and 353.15) K

rfi	1.38530	298.15	Liquid-Liquid(-Liquid) Equilibria in Ternary Systems of Water + Cyclohexylamine + Aromatic Hydrocarbon (Toluene or Propylbenzene) or Aliphatic Hydrocarbon (Heptane or Octane)
rfi	1.38500	298.20	Liquid-Liquid Equilibria for Ternary Mixtures (an Ionic Liquid + Benzene +Heptane or Hexadecane) at T) 298.2 K and Atmospheric Pressure
rfi	1.38530	298.15	Activity Coefficients at Infinite Dilution of Cylcohexylamine + Octane, Toluene, Ethylbenzene, or Aniline and Excess Molar Volumes in Binary Mixtures of Cyclohexylamine + Heptane, Octane, Nonane, Decane, Undecane, Aniline, or Water
rfi	1.38540	298.15	Solubilities of Bis (2,2,6,6-Tetramethyl-4-Piperidinyl) Maleate in Hexane, Heptane, Octane, m-Xylene and Tetrahydrofuran from (253.15 to 310.15) K
rfi	1.38760	293.15	Limiting Activity Coefficients by Comparative Tensimetry: 1-Propanol and 1-Butanol in Heptane and in Octane

rfi	1.38510	298.15	Bubble-Temperature Measurements on Some Binary Mixtures Formed by Tetrahydrofuran or Amyl Alcohol with Hydrocarbons, Chlorohydrocarbons, or Butanols at (94.6 or 95.8) kPa
rfi	1.38510	298.15	Bubble Temperature Measurements on the Binary Mixtures of n-Heptane or Nitrobenzene or Chlorobenzene with Some Chloroethanes and Chloroethylenes at (94.6 to 95.8) kPa
rfi	1.38780	293.15	Infinite Dilution Activity Coefficients of Hydrocarbons in Triethylene Glycol and Tetraethylene Glycol
rfi	1.38527	298.15	Measurement of VLE Data by Using an Experimental Installation with Automatic Control: Modeling of Binary Systems of Methyl Acetate or Ethyl Acetate with n-Heptane or 2,2,4-Trimethylpentane at Both 0.1 and 1.5 MPa
rfi	1.38520	298.15	Isothermal vapour-liquid equilibrium data for the binary systems of (CHF3 or C2F6) and n-heptane

rfi	1.38780	293.15	Isothermal vapour-liquid equilibrium data for the binary systems of (CHF3 or C2F6) and n-heptane
rfi	1.38440	303.15	(Liquid + liquid) equilibria measurements for ternary systems (sulfolane + a carboxylic acid + n-heptane) at T = 303.15 K and at 0.1 MPa
rfi	1.38510	298.20	(Liquid + liquid) equilibria of aqueous solutions of butyric acid with n-heptane and toluene at T = (298.2, 308.2, and 318.2) K
rfi	1.38529	298.15	1-Alkyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide ionic liquids as solvents in the separation of azeotropic mixtures
rfi	1.38529	298.15	Application of [HMim][NTf2], [HMim][TfO] and [BMim][TfO] ionic liquids on the extraction of toluene from alkanes: Effect of the anion and the alkyl chain length of the cation on the LLE
rfi	1.38515	298.15	Extraction of toluene from aliphatic compounds using an ionic liquid as solvent: Influence of the alkane on the (liquid + liquid) equilibrium
rfi	1.38520	298.15	Molar heat capacities for (2-methyl-2-butanol + heptane) mixtures and cyclopentanol at temperatures from (284 to 353) K

rfi	1.38530	298.15	Thermodynamic and acoustic properties of (heptane + dodecane) mixtures under elevated pressures
rfi	1.50240	293.10	(Liquid + liquid) equilibria of {heptane + xylene + N-formylmorpholine} ternary system
rfi	1.38258	303.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.38517	298.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.38776	293.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.38820	293.10	(Liquid + liquid) equilibria of three ternary systems: (heptane + benzene + N-formylmorpholine), (heptane + toluene + N-formylmorpholine), (heptane + xylene + N-formylmorpholine) from T = (298.15 to 353.15) K
rfi	1.38100	308.15	Excess properties of the binary mixtures of methylcyclohexane + alkanes (C6 to C12) at T = 298.15 K to T = 308.15 K

rfi	1.38360	303.15	Excess properties of the binary mixtures of methylcyclohexane + alkanes (C6 to C12) at T = 298.15 K to T = 308.15 K
rfi	1.38600	298.15	Excess properties of the binary mixtures of methylcyclohexane + alkanes (C6 to C12) at T = 298.15 K to T = 308.15 K
rfi	1.38270	303.15	Physical properties of {anisole + n-alkanes} at temperatures between (293.15 and 303.15) K
rfi	1.38550	298.15	Physical properties of {anisole + n-alkanes} at temperatures between (293.15 and 303.15) K
rfi	1.38720	293.15	Physical properties of {anisole + n-alkanes} at temperatures between (293.15 and 303.15) K
rfi	1.37480	318.15	Thermodynamic properties of (an ester + an alkane). XVI. Experimental HEm and V Em values and a new correlation method for (an alkyl ethanoate + an n-alkane) at 318.15 K
rfi	1.38780	293.15	A novel static analytical apparatus for phase equilibrium measurements
rfi	1.38730	293.20	Liquid phase equilibria for mixtures of (an aliphatic hydrocarbon + toluene + gamma-butyrolactone)

rfi	1.38517		298.15	Thiophene separation from aliphatic hydrocarbons using the 1-ethyl-3-methylimidazolium ethylsulfate ionic liquid
rfi	1.38517		298.15	A study on the liquid liquid equilibria of 1-alkyl-3-methylimidazolium hexafluorophosphate with ethanol and alkanes
rfi	1.38517		298.15	Phase behaviour of 1-methyl-3-octylimidazolium bis[trifluoromethylsulfonyl]imide with thiophene and aliphatic hydrocarbons: The influence of n-alkane chain length
rfi	1.38760		293.15	Bubble points of some binary mixtures formed by o-cresol at 95.75 kPa
rfi	1.53800		298.15	Thermodynamic and Acoustic Properties of Mixtures of Dibromomethane + Heptane
rhol	651.92	kg/m3	329.04	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	679.63	kg/m3	298.15	Thermodynamics of Mixtures Containing a Strongly Polar Compound. 9. Liquid-Liquid Equilibria for epsilon-Caprolactam + Selected Alkanes
rhol	657.90	kg/m3	323.15	Densities and Excess Molar Volumes of 2-Butanol + Cyclohexanamine + Heptane and 2-Butanol + n-Heptane at Temperatures between (288.15 and 323.15) K

rhol	662.27	kg/m3	318.15	Densities and Excess Molar Volumes of 2-Butanol + Cyclohexanamine + Heptane and 2-Butanol + n-Heptane at Temperatures between (288.15 and 323.15) K
rhol	666.62	kg/m3	313.15	Densities and Excess Molar Volumes of 2-Butanol + Cyclohexanamine + Heptane and 2-Butanol + n-Heptane at Temperatures between (288.15 and 323.15) K
rhol	670.94	kg/m3	308.15	Densities and Excess Molar Volumes of 2-Butanol + Cyclohexanamine + Heptane and 2-Butanol + n-Heptane at Temperatures between (288.15 and 323.15) K
rhol	675.23	kg/m3	303.15	Densities and Excess Molar Volumes of 2-Butanol + Cyclohexanamine + Heptane and 2-Butanol + n-Heptane at Temperatures between (288.15 and 323.15) K
rhol	679.49	kg/m3	298.15	Densities and Excess Molar Volumes of 2-Butanol + Cyclohexanamine + Heptane and 2-Butanol + n-Heptane at Temperatures between (288.15 and 323.15) K

rhol	683.73	kg/m3	293.15	Densities and Excess Molar Volumes of 2-Butanol + Cyclohexanamine + Heptane and 2-Butanol + n-Heptane at Temperatures between (288.15 and 323.15) K
rhol	687.95	kg/m3	288.15	Densities and Excess Molar Volumes of 2-Butanol + Cyclohexanamine + Heptane and 2-Butanol + n-Heptane at Temperatures between (288.15 and 323.15) K
rhol	680.00	kg/m3	298.15	Effect of Temperature on Phase Equilibrium of the Mixed-Solvent System of (2,2,2-Trifluoroethanol + Methanol + Cyclohexane)
rhol	680.00	kg/m3	298.15	Liquid-Liquid Equilibrium of (Cyclohexane + 2,2,2-Trifluoroethanol) and (Cyclohexane + Methanol) from (278.15 to 318.15) K
rhol	680.02	kg/m3	298.15	Binary Liquid Liquid Equilibria of ?-Valerolactone with Some Hydrocarbons
rhol	644.60	kg/m3	338.15	Density, Viscosity, Speed of Sound, Bulk Modulus, and Surface Tension of Binary Mixtures of n-Heptane + 2,2,4-Trimethylpentane at (293.15 to 338.15) K and 0.1 MPa

rhol	649.11	kg/m3	333.15	Density, Viscosity, Speed of Sound, Bulk Modulus, and Surface Tension of Binary Mixtures of n-Heptane + 2,2,4-Trimethylpentane at (293.15 to 338.15) K and 0.1 MPa
rhol	653.57	kg/m3	328.15	Density, Viscosity, Speed of Sound, Bulk Modulus, and Surface Tension of Binary Mixtures of n-Heptane + 2,2,4-Trimethylpentane at (293.15 to 338.15) K and 0.1 MPa
rhol	657.99	kg/m3	323.15	Density, Viscosity, Speed of Sound, Bulk Modulus, and Surface Tension of Binary Mixtures of n-Heptane + 2,2,4-Trimethylpentane at (293.15 to 338.15) K and 0.1 MPa
rhol	666.73	kg/m3	313.15	Density, Viscosity, Speed of Sound, Bulk Modulus, and Surface Tension of Binary Mixtures of n-Heptane + 2,2,4-Trimethylpentane at (293.15 to 338.15) K and 0.1 MPa
rhol	671.05	kg/m3	308.15	Density, Viscosity, Speed of Sound, Bulk Modulus, and Surface Tension of Binary Mixtures of n-Heptane + 2,2,4-Trimethylpentane at (293.15 to 338.15) K and 0.1 MPa

rhol	675.35	kg/m3	303.15	Density, Viscosity, Speed of Sound, Bulk Modulus, and Surface Tension of Binary Mixtures of n-Heptane + 2,2,4-Trimethylpentane at (293.15 to 338.15) K and 0.1 MPa
rhol	679.61	kg/m3	298.15	Density, Viscosity, Speed of Sound, Bulk Modulus, and Surface Tension of Binary Mixtures of n-Heptane + 2,2,4-Trimethylpentane at (293.15 to 338.15) K and 0.1 MPa
rhol	683.85	kg/m3	293.15	Density, Viscosity, Speed of Sound, Bulk Modulus, and Surface Tension of Binary Mixtures of n-Heptane + 2,2,4-Trimethylpentane at (293.15 to 338.15) K and 0.1 MPa
rhol	666.92	kg/m3	313.15	Excess Molar Volumes and Viscosities of Binary Systems of Butylcyclohexane with n-Alkanes (C7 to C14) at T = 293.15 K to 313.15 K
rhol	671.12	kg/m3	308.15	Excess Molar Volumes and Viscosities of Binary Systems of Butylcyclohexane with n-Alkanes (C7 to C14) at T = 293.15 K to 313.15 K

rhol	675.41	kg/m3	303.15	Excess Molar Volumes and Viscosities of Binary Systems of Butylcyclohexane with n-Alkanes (C7 to C14) at T = 293.15 K to 313.15 K
rhol	679.74	kg/m3	298.15	Excess Molar Volumes and Viscosities of Binary Systems of Butylcyclohexane with n-Alkanes (C7 to C14) at T = 293.15 K to 313.15 K
rhol	683.99	kg/m3	293.15	Excess Molar Volumes and Viscosities of Binary Systems of Butylcyclohexane with n-Alkanes (C7 to C14) at T = 293.15 K to 313.15 K
rhol	679.54	kg/m3	298.15	Excess Enthalpy and Excess Volume for Pyridine + Methyldiethanolamine and Pyridine + Ethanolamine Mixtures
rhol	675.53	kg/m3	303.15	Thermodynamics of Mixtures Containing Amines. XII. Volumetric and Speed of Sound Data at (293.15, 298.15, and 303.15) K for N-Methylaniline + Hydrocarbon Systems
rhol	679.60	kg/m3	298.15	Thermodynamics of Mixtures Containing Amines. XII. Volumetric and Speed of Sound Data at (293.15, 298.15, and 303.15) K for N-Methylaniline + Hydrocarbon Systems

rhol	683.85	kg/m3	293.15	Thermodynamics of Mixtures Containing Amines. XII. Volumetric and Speed of Sound Data at (293.15, 298.15, and 303.15) K for N-Methylaniline + Hydrocarbon Systems
rhol	679.71	kg/m3	298.15	Thermodynamics of Mixtures Containing Aromatic Alcohols. 1. Liquid Liquid Equilibria for (Phenylmethanol + Alkane) Systems
rhol	679.86	kg/m3	298.20	Apparent and Partial Molar Volumes at Infinite Dilution and Solid Liquid Equilibria of Dibenzothiophene + Alkane Systems
rhol	679.43	kg/m3	298.15	Liquid-Liquid(-Liquid) Equilibria in Ternary Systems of Aliphatic Hydrocarbons (Heptane or Octane) + Phenols + Water
rhol	666.68	kg/m3	313.15	Thermophysical and Acoustical Properties of the Binary Mixtures 1,2-Dibromoethane + Heptane within the Temperature Range from 293.15 K to 313.15 K
rhol	671.02	kg/m3	308.15	Thermophysical and Acoustical Properties of the Binary Mixtures 1,2-Dibromoethane + Heptane within the Temperature Range from 293.15 K to 313.15 K

rhol	675.31	kg/m3	303.15	Thermophysical and Acoustical Properties of the Binary Mixtures 1,2-Dibromoethane + Heptane within the Temperature Range from 293.15 K to 313.15 K
rhol	679.59	kg/m3	298.15	Thermophysical and Acoustical Properties of the Binary Mixtures 1,2-Dibromoethane + Heptane within the Temperature Range from 293.15 K to 313.15 K
rhol	683.82	kg/m3	293.15	Thermophysical and Acoustical Properties of the Binary Mixtures 1,2-Dibromoethane + Heptane within the Temperature Range from 293.15 K to 313.15 K
rhol	679.63	kg/m3	298.15	Thermodynamics of Mixtures Containing a Strongly Polar Compound. 8. Liquid-Liquid Equilibria for N,N-Dialkylamide + Selected N-Alkanes
rhol	679.50	kg/m3	298.15	Vapor-Liquid Equilibria for the Ternary Systems of Methyl tert-Butyl Ether + Methanol + Methylcyclohexane and Methyl tert-Butyl Ether + Methanol + n-Heptane and Constituent Binary Systems at 313.15 K

rhol	679.54	kg/m3	298.15	Thermodynamics of Mixtures Containing Ethers. Part III. Liquid-Liquid Equilibria for 2,5,8,11-Tetraoxadodecane or 2,5,8,11,14-Pentaoxapentadecane + Selected N-Alkanes
rhol	679.50	kg/m3	298.15	Vapor-Liquid Equilibrium Data for the Binary Decafluoropentane (HFC-43-10meec) + Heptane, Decafluoropentane + Butyl Ethyl Ether, Octafluorobutane (HFC-338pcc) + Butyl Ethyl Ether, and Heptafluoro Propyl Methyl Ether (HFE-347mcc) + HFC-338pcc Systems at 101.3 kPa
rhol	680.17	kg/m3	298.15	Excess Enthalpies of Binary Mixtures of 1-Hexene with Some n-Alkanes at 298.15 K
rhol	682.30	kg/m3	298.20	Ternary Liquid-Liquid Equilibria for Mixtures of 1-Methyl-3-octylimidazolium Chloride + an Alkanol + an Alkane at 298.2 K and 1 bar
rhol	683.91	kg/m3	293.15	Excess Molar Enthalpies for Binary Mixtures of Ethanol + Acetone, + Octane, + Cyclohexane and 1-Propanol + Acetone, + Octane, + Heptane at 323.15

rhol	679.40	kg/m3	298.15	Viscosities of Dimethyl Carbonate or Diethyl Carbonate with Alkanes at Four Temperatures. New UNIFAC-VISCO Parameters	
rhol	679.00	kg/m3	298.15	Liquid-Liquid Equilibrium Data for Ternary Systems Containing Alkanes (n-Pentane, n-Hexane, n-Heptane, and n-Octane) + Alcohol (Methanol and Ethanol) + Protic Ionic Liquid (2-HEAF)	
rhol	627.85	kg/m3	356.84	Density of Working Liquids for Diffusion Vacuum Pumps	
rhol	635.91	kg/m3	347.53	Density of Working Liquids for Diffusion Vacuum Pumps	
rhol	644.32	kg/m3	338.26	Density of Working Liquids for Diffusion Vacuum Pumps	
rhol	684.00	kg/m3	293.00	KDB	
rhol	684.00	kg/m3	293.15	Densities and Kinematic Viscosities of a Quinary Regular Liquid System and Its Five Quaternary Subsystems at 293.15A K and 298.15A K	
rhol	679.70	kg/m3	298.15	Densities and Kinematic Viscosities of a Quinary Regular Liquid System and Its Five Quaternary Subsystems at 293.15A K and 298.15A K	

rhol	683.53	kg/m3	293.20	Isobaric vapour liquid equilibria for binary mixtures of n-heptane with bromobenzene, chlorobenzene and fluorobenzene at atmospheric pressure
rhol	679.54	kg/m3	298.15	Thermodynamic study of 1,1,2,2-tetrachloroethane + hydrocarbon mixtures I. Excess and solvation enthalpies
rhol	679.63	kg/m3	298.15	Thermodynamics of mixtures containing amines VI. Liquid liquid equilibria for mixtures of o-toluidine + selected alkanes
rhol	688.25	kg/m3	288.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	679.79	kg/m3	298.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa

rhol	666.89	kg/m3	313.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	653.72	kg/m3	328.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	644.77	kg/m3	338.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	635.63	kg/m3	348.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	679.57	kg/m3	298.15	Capacity of two 1-butyl-1-methylpyrrolidinium-based ionic liquidsfor the extraction of ethanol from its mixtures with heptane and hexane

rhol	683.80	kg/m3	298.15	Liquid-liquid equilibria for multicomponent mixtures of 2,2-dimethyl-1,3-dioxolane with n-heptane, toluene, ethanol and water
rhol	679.55	kg/m3	298.15	Phase behaviour of tricyanomethanide-based ionic liquids with alcohols and hydrocarbons
rhol	679.60	kg/m3	298.15	Vapour liquid equilibrium at T = 308.15 K for binary systems: Dibromomethane + n-heptane, bromotrichloromethane + n-heptane, bromotrichloromethane + dibromomethane, bromotrichloromethane + bromochloromethane and dibromomethane + bromochloromethane. Experimental data and modelling
rhol	679.48	kg/m3	298.15	Separation of pyridine from heptane with tricyanomethanide-based ionic liquids
rhol	683.80	kg/m3	298.15	Liquid-liquid equilibria for ternary mixtures of 2,2-dimethyl-1,3-dioxolane-4-methanol with n-heptane, toluene, ethanol and water
rhol	675.40	kg/m3	303.15	Effect of polarity and temperature on the binary interaction between D2EHPA extractant and organic solvents (kerosene, n-heptane, chlorobenzene and 1-octanol): Experimental and thermodynamics

rhol	666.80	kg/m3	313.15	Effect of polarity and temperature on the binary interaction between D2EHPA extractant and organic solvents (kerosene, n-heptane, chlorobenzene and 1-octanol): Experimental and thermodynamics
rhol	657.70	kg/m3	323.15	Effect of polarity and temperature on the binary interaction between D2EHPA extractant and organic solvents (kerosene, n-heptane, chlorobenzene and 1-octanol): Experimental and thermodynamics
rhol	648.40	kg/m3	333.15	Effect of polarity and temperature on the binary interaction between D2EHPA extractant and organic solvents (kerosene, n-heptane, chlorobenzene and 1-octanol): Experimental and thermodynamics
rhol	681.48	kg/m3	298.15	Quaternary isothermal vapor-liquid equilibrium of the model biofuel 2-butanone + n-heptane + tetrahydrofuran + cyclohexane using Raman spectroscopic characterization
rhol	690.60	kg/m3	298.15	Ternary (liquid + liquid) equilibria for mixtures of 1-hexyl-3-methylimidazolium (tetrafluoroborate or hexafluorophosphate) + benzene + an alkane at T = 298.2 K and p = 0.1 MPa

rhol	679.66	kg/m3	298.15	Thermodynamic and acoustic properties of binary mixtures of alcohols and alkanes. I. Speed of sound in (ethanol + n-heptane) under elevated pressures	
rhol	683.82	kg/m3	293.22	Thermodynamic and acoustic properties of binary mixtures of alcohols and alkanes. II. Density and heat capacity of (ethanol + n-heptane) under elevated pressures	
rhol	679.75	kg/m3	298.16	Thermodynamic and acoustic properties of binary mixtures of alcohols and alkanes. II. Density and heat capacity of (ethanol + n-heptane) under elevated pressures	
rhol	675.51	kg/m3	303.17	Thermodynamic and acoustic properties of binary mixtures of alcohols and alkanes. II. Density and heat capacity of (ethanol + n-heptane) under elevated pressures	
rhol	671.21	kg/m3	308.17	Thermodynamic and acoustic properties of binary mixtures of alcohols and alkanes. II. Density and heat capacity of (ethanol + n-heptane) under elevated pressures	

rhol	666.97	kg/m3	313.17	Thermodynamic and acoustic properties of binary mixtures of alcohols and alkanes. II. Density and heat capacity of (ethanol + n-heptane) under elevated pressures	
rhol	662.67	kg/m3	318.18	Thermodynamic and acoustic properties of binary mixtures of alcohols and alkanes. II. Density and heat capacity of (ethanol + n-heptane) under elevated pressures	
rhol	700.67	kg/m3	273.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	696.57	kg/m3	278.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	692.40	kg/m3	283.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	688.20	kg/m3	288.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	683.99	kg/m3	293.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	679.75	kg/m3	298.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	

rhol	675.49	kg/m3	303.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	671.19	kg/m3	308.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	666.87	kg/m3	313.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	662.52	kg/m3	318.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	658.13	kg/m3	323.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	653.71	kg/m3	328.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	649.24	kg/m3	333.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	644.74	kg/m3	338.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	640.19	kg/m3	343.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	635.60	kg/m3	348.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	

rhol	630.95	kg/m3	353.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	626.26	kg/m3	358.15	Experimental measurements and prediction of liquid densities for n-alkane mixtures	
rhol	679.47	kg/m3	298.15	Solvent extraction of thiophene from n-alkanes (C7, C12, and C16) using the ionic liquid [C8mim][BF4]	
rhol	679.54	kg/m3	298.15	Experimental and theoretical study of surface tension of binary mixtures of (n-alkyl acetates + heptane, benzene, and toluene)	
rhol	680.00	kg/m3	298.15	Phase diagrams of (hexane + methanol + 2,2,2-trifluoroethanol) at three temperatures: Measurement and correlation	
rhol	679.71	kg/m3	298.15	Thermodynamics of mixtures containing amines. XI. Liquid + liquid equilibria and molar excess enthalpies at 298.15 K for N-methylaniline + hydrocarbon systems. Characterization in terms of DISQUAC and ERAS models	
rhol	679.91	kg/m3	298.15	Volumetric and acoustic properties of binary mixtures of tri-n-butyl phosphate with n-hexane, cyclohexane, and n-heptane from T = (298.15 to 323.15) K	

rhol	675.63	kg/m3	303.15	Volumetric and acoustic properties of binary mixtures of tri-n-butyl phosphate with n-hexane, cyclohexane, and n-heptane from T = (298.15 to 323.15) K	
rhol	671.33	kg/m3	308.15	Volumetric and acoustic properties of binary mixtures of tri-n-butyl phosphate with n-hexane, cyclohexane, and n-heptane from T = (298.15 to 323.15) K	
rhol	667.01	kg/m3	313.15	Volumetric and acoustic properties of binary mixtures of tri-n-butyl phosphate with n-hexane, cyclohexane, and n-heptane from T = (298.15 to 323.15) K	
rhol	662.65	kg/m3	318.15	Volumetric and acoustic properties of binary mixtures of tri-n-butyl phosphate with n-hexane, cyclohexane, and n-heptane from T = (298.15 to 323.15) K	
rhol	658.26	kg/m3	323.15	Volumetric and acoustic properties of binary mixtures of tri-n-butyl phosphate with n-hexane, cyclohexane, and n-heptane from T = (298.15 to 323.15) K	
rhol	679.57	kg/m3	298.15	Application of 1-alkyl-3-methylpyridinium bis(trifluoromethylsulfonyl)imide ionic liquids for the ethanol removal from its mixtures with alkanes	

rhol	679.60	kg/m3	298.15	Cation effect of ammonium imide based ionic liquids in alcohols extraction from alcohol-alkane azeotropic mixtures	
rhol	692.44	kg/m3	283.15	Density, viscosity and excess molar volume of binary mixtures of tri-n-octylamine + diluents (n-heptane, n-octane, n-nonane, and n-decane) at various temperatures	
rhol	684.05	kg/m3	293.15	Density, viscosity and excess molar volume of binary mixtures of tri-n-octylamine + diluents (n-heptane, n-octane, n-nonane, and n-decane) at various temperatures	
rhol	675.54	kg/m3	303.15	Density, viscosity and excess molar volume of binary mixtures of tri-n-octylamine + diluents (n-heptane, n-octane, n-nonane, and n-decane) at various temperatures	
rhol	679.78	kg/m3	298.15	Density, viscosity and excess molar volume of binary mixtures of tri-n-octylamine + diluents (n-heptane, n-octane, n-nonane, and n-decane) at various temperatures	
rhol	679.48	kg/m3	298.15	Separation of sulfur compounds from alkanes with 1-alkylcyanopyridinium-based ionic liquids	

rhol	679.54	kg/m3	298.15	Effect of the alkyl side chain of the 1-alkylpiperidinium-based ionic liquids on desulfurization of fuels
rhol	679.57	kg/m3	298.15	Quaternary (liquid + liquid) equilibrium data for the extraction of toluene from alkanes using the ionic liquid [EMim][MSO4]
rhol	679.54	kg/m3	298.15	Extraction desulfurization process of fuels with ionic liquids
rhol	679.57	kg/m3	298.15	(Liquid + liquid) equilibrium of ternary and quaternary systems containing heptane, cyclohexane, toluene and the ionic liquid [EMim][N(CN)2]. Experimental data and correlation
rhol	679.50	kg/m3	298.15	Fully automatized apparatus for determining speed of sound for liquids in the temperature and pressure interval (283.15-343.15) K and (0.1-95) MPa
rhol	683.78	kg/m3	293.15	Surface tension and density of mixtures of m-xylene + n-alkane at 293.15 K: Analysis under the extended Langmuir and Shereshefsky models
rhol	679.46	kg/m3	298.15	Conformational analysis of branched alkanes using limiting partial molar volumes

rhol	689.00	kg/m3	288.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	685.00	kg/m3	293.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	680.00	kg/m3	298.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	676.00	kg/m3	303.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	668.00	kg/m3	313.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	660.00	kg/m3	323.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	651.00	kg/m3	333.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume

rhol	642.00	kg/m3	343.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume	
rhol	679.71	kg/m3	298.15	Liquid-liquid equilibria for (2-hydroxy benzaldehyde + n-alkane) mixtures. Intermolecular and proximity effects in systems containing hydroxyl and aldehyde groups	
rhol	679.49	kg/m3	298.15	Topological and thermodynamic investigations of binary mixtures: Molar excess volumes, molar excess enthalpies and isentropic compressibility changes of mixing	
rhol	687.95	kg/m3	288.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K	
rhol	683.73	kg/m3	293.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K	

rhol	679.49	kg/m3	298.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K
rhol	675.23	kg/m3	303.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K
rhol	670.94	kg/m3	308.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K
rhol	666.62	kg/m3	313.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K

rhol	662.27	kg/m3	318.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K	
rhol	657.90	kg/m3	323.15	Experimental determination and modelling of densities and excess molar volumes of ternary system (1-butanol + cyclohexylamine + n-heptane) and corresponding binaries from 288.15 to 323.15K	
rhol	679.49	kg/m3	298.15	Excess molar volumes and isentropic compressibilities changes of mixing of tetrahydropyran + benzene + cyclo or n-alkanes ternary mixtures at 308.15 K	
rhol	688.59	kg/m3	288.15	Excess molar volumes of (1-chlorobutane +heptane + 2-butanone or 2-pentanone) at 288.15 , 303.15 and 313.15 K . Measurements and correlations.	
rhol	675.84	kg/m3	303.15	Excess molar volumes of (1-chlorobutane +heptane + 2-butanone or 2-pentanone) at 288.15 , 303.15 and 313.15 K . Measurements and correlations.	

rhol	665.84	kg/m3	313.15	Excess molar volumes of (1-chlorobutane +heptane + 2-butanone or 2-pentanone) at 288.15 , 303.15 and 313.15 K . Measurements and correlations.
rhol	683.89	kg/m3	293.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	679.64	kg/m3	298.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	675.37	kg/m3	303.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K

rhol	671.07	kg/m3	308.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	666.74	kg/m3	313.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	662.38	kg/m3	318.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	657.98	kg/m3	323.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	688.13	kg/m3	288.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa

rhol	683.93	kg/m3	293.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rhol	679.71	kg/m3	298.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rhol	675.47	kg/m3	303.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rhol	671.20	kg/m3	308.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rhol	666.89	kg/m3	313.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rhol	662.55	kg/m3	318.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rhol	658.19	kg/m3	323.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rhol	653.79	kg/m3	328.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rhol	649.33	kg/m3	333.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa

rhol	644.84	kg/m3	338.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rhol	640.29	kg/m3	343.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rhol	683.67	kg/m3	293.15	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	675.75	kg/m3	301.62	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	667.37	kg/m3	310.71	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	659.85	kg/m3	319.85	Density of Working Liquids for Diffusion Vacuum Pumps
rhol	662.38	kg/m3	318.15	Density, Viscosity, Speed of Sound, Bulk Modulus, and Surface Tension of Binary Mixtures of n-Heptane + 2,2,4-Trimethylpentane at (293.15 to 338.15) K and 0.1 MPa
sfust	77.73	J/mol×K	182.20	NIST Webbook
sfust	76.96	J/mol×K	182.59	NIST Webbook
sfust	76.89	J/mol×K	182.55	NIST Webbook
sfust	76.89	J/mol×K	182.55	NIST Webbook
sfust	78.81	J/mol×K	182.56	NIST Webbook
sfust	76.81	J/mol×K	182.56	NIST Webbook
sfust	76.93	J/mol×K	182.52	NIST Webbook
sfust	77.00	J/mol×K	182.70	NIST Webbook
sfust	77.02	J/mol×K	182.56	NIST Webbook
sfust	76.81	J/mol×K	182.56	NIST Webbook
sfust	77.73	J/mol×K	182.20	NIST Webbook

speedsl	1108.78	m/s	303.10	Excess molar heat capacities for (decan-1-ol + n-heptane) at temperatures from (290 to 318) K. Experimental results and theoretical description using the ERAS model
speedsl	742.30	m/s	393.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	683.10	m/s	408.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	643.50	m/s	418.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	603.90	m/s	428.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa

speedsl	1109.60	m/s	303.15	Excess Molar Volumes and Speed of Sound in Bromotrichloromethane + n-Heptane, Dibromomethane + n-Heptane, Bromotrichloromethane + Dibromomethane, and Bromotrichloromethane + Bromochloromethane at Temperatures from (293.15 to 313.15) K
speedsl	523.90	m/s	448.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	801.60	m/s	378.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	861.20	m/s	363.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	921.10	m/s	348.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	981.50	m/s	333.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa

speedsl	1042.00	m/s	318.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	1108.00	m/s	302.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	1066.90	m/s	313.15	Excess Molar Volumes and Speed of Sound in Bromotrichloromethane + n-Heptane, Dibromomethane + n-Heptane, Bromotrichloromethane + Dibromomethane, and Bromotrichloromethane + Bromochloromethane at Temperatures from (293.15 to 313.15) K
speedsl	1067.10	m/s	313.15	Excess Molar Volumes and Speed of Sound in Bromotrichloromethane + n-Heptane, Dibromomethane + n-Heptane, Bromotrichloromethane + Dibromomethane, and Bromotrichloromethane + Bromochloromethane at Temperatures from (293.15 to 313.15) K

speedsl	1088.10	m/s	308.15	Excess Molar Volumes and Speed of Sound in Bromotrichloromethane + n-Heptane, Dibromomethane + n-Heptane, Bromotrichloromethane + Dibromomethane, and Bromotrichloromethane + Bromochloromethane at Temperatures from (293.15 to 313.15) K
speedsl	1088.20	m/s	308.15	Excess Molar Volumes and Speed of Sound in Bromotrichloromethane + n-Heptane, Dibromomethane + n-Heptane, Bromotrichloromethane + Dibromomethane, and Bromotrichloromethane + Bromochloromethane at Temperatures from (293.15 to 313.15) K
speedsl	1109.10	m/s	303.15	Excess Molar Volumes and Speed of Sound in Bromotrichloromethane + n-Heptane, Dibromomethane + n-Heptane, Bromotrichloromethane + Dibromomethane, and Bromotrichloromethane + Bromochloromethane at Temperatures from (293.15 to 313.15) K
speedsl	131.90	m/s	533.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa

speedsl	162.70	m/s	528.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	190.90	m/s	523.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	217.30	m/s	518.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	242.40	m/s	513.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	1130.90	m/s	298.15	Excess Molar Volumes and Speed of Sound in Bromotrichloromethane + n-Heptane, Dibromomethane + n-Heptane, Bromotrichloromethane + Dibromomethane, and Bromotrichloromethane + Bromochloromethane at Temperatures from (293.15 to 313.15) K
speedsl	266.60	m/s	508.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa

speedsl	290.10	m/s	503.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	313.00	m/s	498.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	335.40	m/s	493.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	357.40	m/s	488.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	379.00	m/s	483.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	400.30	m/s	478.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	421.30	m/s	473.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa

speedsl	442.20	m/s	468.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	462.80	m/s	463.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	483.30	m/s	458.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	503.60	m/s	453.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	111.10	m/s	536.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	1151.92	m/s	293.13	Excess molar heat capacities for (decan-1-ol + n-heptane) at temperatures from (290 to 318) K. Experimental results and theoretical description using the ERAS model

speedsl	564.00	m/s	438.15	Measurement of the Speed of Sound in Hexane and Heptane at Temperatures from (303.15 to 536.15) K and Pressures from (1.0 to 8.5) MPa
speedsl	1130.26	m/s	298.12	Excess molar heat capacities for (decan-1-ol + n-heptane) at temperatures from (290 to 318) K. Experimental results and theoretical description using the ERAS model
speedsl	1131.00	m/s	298.15	Excess Molar Volumes and Speed of Sound in Bromotrichloromethane + n-Heptane, Dibromomethane + n-Heptane, Bromotrichloromethane + Dibromomethane, and Bromotrichloromethane + Bromochloromethane at Temperatures from (293.15 to 313.15) K
speedsl	1152.20	m/s	293.15	Excess Molar Volumes and Speed of Sound in Bromotrichloromethane + n-Heptane, Dibromomethane + n-Heptane, Bromotrichloromethane + Dibromomethane, and Bromotrichloromethane + Bromochloromethane at Temperatures from (293.15 to 313.15) K

speedsl	1152.60	m/s	293.15	Excess Molar Volumes and Speed of Sound in Bromotrichloromethane + n-Heptane, Dibromomethane + n-Heptane, Bromotrichloromethane + Dibromomethane, and Bromotrichloromethane + Bromochloromethane at Temperatures from (293.15 to 313.15) K
speedsl	1064.29	m/s	313.45	Thermodynamic and Acoustic Properties of Mixtures of 1,6-Dichlorohexane with Heptane from (293 to 313) K
speedsl	1087.42	m/s	308.06	Thermodynamic and Acoustic Properties of Mixtures of 1,6-Dichlorohexane with Heptane from (293 to 313) K
speedsl	1109.45	m/s	302.98	Thermodynamic and Acoustic Properties of Mixtures of 1,6-Dichlorohexane with Heptane from (293 to 313) K
speedsl	1131.06	m/s	298.00	Thermodynamic and Acoustic Properties of Mixtures of 1,6-Dichlorohexane with Heptane from (293 to 313) K
speedsl	1154.11	m/s	292.70	Thermodynamic and Acoustic Properties of Mixtures of 1,6-Dichlorohexane with Heptane from (293 to 313) K

speedsl	1043.90	m/s	318.33	Excess molar heat capacities for (decan-1-ol + n-heptane) at temperatures from (290 to 318) K. Experimental results and theoretical description using the ERAS model
speedsl	1066.28	m/s	313.03	Excess molar heat capacities for (decan-1-ol + n-heptane) at temperatures from (290 to 318) K. Experimental results and theoretical description using the ERAS model
speedsl	1087.47	m/s	308.07	Excess molar heat capacities for (decan-1-ol + n-heptane) at temperatures from (290 to 318) K. Experimental results and theoretical description using the ERAS model
srf	0.02	N/m	308.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol
srf	0.02	N/m	298.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol
srf	0.02	N/m	303.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol
srf	0.02	N/m	293.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol
srf	0.02	N/m	288.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol

srf	0.02	N/m	323.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	318.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	313.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	308.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	303.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	298.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	293.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	288.15	Interfacial Tensions of Imidazolium-Based Ionic Liquids with N-Alkanes and Cyclohexane
srf	0.02	N/m	337.88	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	332.91	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	327.88	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	322.86	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	317.86	Surface Tension of Pure Liquids and Binary Liquid Mixtures

srf	0.02	N/m	312.86	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	307.86	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	302.83	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	297.82	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	292.81	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	287.81	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	282.83	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	277.93	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	318.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	313.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	308.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	303.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K

srf	0.02	N/m	298.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	293.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	323.15	Experimental and theoretical study of surface tension of n-pentane, n-heptane, and some of their mixtures at different temperatures
srf	0.02	N/m	313.15	Experimental and theoretical study of surface tension of n-pentane, n-heptane, and some of their mixtures at different temperatures
srf	0.02	N/m	303.15	Experimental and theoretical study of surface tension of n-pentane, n-heptane, and some of their mixtures at different temperatures
srf	0.02	N/m	293.15	Experimental and theoretical study of surface tension of n-pentane, n-heptane, and some of their mixtures at different temperatures
srf	0.02	N/m	283.15	Experimental and theoretical study of surface tension of n-pentane, n-heptane, and some of their mixtures at different temperatures

srf	0.02	N/m	293.20	KDB	
srf	0.02	N/m	298.15	Interfacial Tensions of Imidazolium-Based Ionic Liquids with N-Alkanes and Cyclohexane	
srf	0.02	N/m	308.15	Interfacial Tensions of Imidazolium-Based Ionic Liquids with N-Alkanes and Cyclohexane	
srf	0.02	N/m	318.15	Interfacial Tensions of Imidazolium-Based Ionic Liquids with N-Alkanes and Cyclohexane	
srf	0.02	N/m	328.15	Interfacial Tensions of Imidazolium-Based Ionic Liquids with N-Alkanes and Cyclohexane	
srf	0.02	N/m	293.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures	
srf	0.02	N/m	298.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures	
srf	0.02	N/m	303.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures	
srf	0.02	N/m	308.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures	
srf	0.02	N/m	313.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures	

srf	0.02	N/m	318.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures
srf	0.02	N/m	323.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures
srf	0.02	N/m	303.49	Surface Tension of 2,2-Dimethylbutane from (233 to 378) K
srf	0.02	N/m	313.13	Surface Tension of 2,2-Dimethylbutane from (233 to 378) K
srf	0.02	N/m	318.49	Surface Tension of 2,2-Dimethylbutane from (233 to 378) K
srf	0.02	N/m	323.15	Surface Tension of 2,2-Dimethylbutane from (233 to 378) K
srf	0.02	N/m	328.12	Surface Tension of 2,2-Dimethylbutane from (233 to 378) K
srf	0.02	N/m	333.13	Surface Tension of 2,2-Dimethylbutane from (233 to 378) K
srf	0.02	N/m	338.14	Surface Tension of 2,2-Dimethylbutane from (233 to 378) K
srf	0.02	N/m	343.12	Surface Tension of 2,2-Dimethylbutane from (233 to 378) K
srf	0.01	N/m	348.13	Surface Tension of 2,2-Dimethylbutane from (233 to 378) K

srf	0.01	N/m	358.12	Surface Tension of 2,2-Dimethylbutane from (233 to 378) K
srf	0.02	N/m	298.13	Surface Tension of Diethyl Ether, Diisopropyl Ether, and Dibutyl Ether
srf	0.02	N/m	303.18	Surface Tension of Diethyl Ether, Diisopropyl Ether, and Dibutyl Ether
srf	0.02	N/m	308.12	Surface Tension of Diethyl Ether, Diisopropyl Ether, and Dibutyl Ether
srf	0.02	N/m	313.18	Surface Tension of Diethyl Ether, Diisopropyl Ether, and Dibutyl Ether
srf	0.02	N/m	318.17	Surface Tension of Diethyl Ether, Diisopropyl Ether, and Dibutyl Ether
srf	0.02	N/m	323.20	Surface Tension of Diethyl Ether, Diisopropyl Ether, and Dibutyl Ether
srf	0.02	N/m	328.15	Surface Tension of Diethyl Ether, Diisopropyl Ether, and Dibutyl Ether
srf	0.02	N/m	342.92	Surface Tension of Pure Liquids and Binary Liquid Mixtures

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source

tbp	308.91	K	10.23	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	320.43	K	16.91	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	328.58	K	23.50	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	339.42	K	35.39	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	352.66	K	56.16	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	358.24	K	67.57	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	361.37	K	74.44	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures

tbp	363.45	K	79.37	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	366.31	K	86.51	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	371.21	K	100.11	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures

Correlations

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)
Coeff. A	1.42106e+01
Coeff. B	-3.08981e+03
Coeff. C	-4.94170e+01
Temperature range (K), min.	271.34
Temperature range (K), max.	396.62

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/T + C*ln(T) + D*T^2
Coeff. A	1.08146e+02
Coeff. B	-8.03007e+03
Coeff. C	-1.41239e+01
Coeff. D	1.20486e-05
Temperature range (K), min.	182.56
Temperature range (K), max.	540.26

Datasets

Speed of sound, m/s

Temperature, K - Fluid (supercritical or subcritical phases)	Pressure, kPa - Fluid (supercritical or subcritical phases)	Speed of sound, m/s - Fluid (supercritical or subcritical phases)
513.92	2500.00	266.66
525.23	2500.00	196.31
528.93	2500.00	167.01
534.12	2500.00	121.38
538.13	2500.00	101.28
544.09	2500.00	100.71
547.02	2500.00	107.6
552.59	2500.00	118.66
559.91	2500.00	129.19
564.02	2500.00	135.46
572.57	2500.00	144.47
584.19	2500.00	156.26
590.48	2500.00	161.58
601.60	2500.00	170.4
612.58	2500.00	179.23
620.87	2500.00	183.77
632.18	2500.00	189.44
640.72	2500.00	192.85
650.07	2500.00	195.77
513.59	3000.00	293.56
523.83	3000.00	242.56
528.41	3000.00	218.56
532.76	3000.00	193.81
538.36	3000.00	152.7
544.95	3000.00	115.6
549.04	3000.00	105.27
553.93	3000.00	110.64
574.87	5000.00	160.49
577.04	5000.00	154.18
582.31	5000.00	142.67
588.17	5000.00	139.88
592.28	5000.00	136.41

597.48	5000.00	135.43
602.30	5000.00	135.26
607.65	5000.00	136.72
615.11	5000.00	142.58
623.25	5000.00	150.58
632.29	5000.00	156.55
643.51	5000.00	165.41
513.58	6000.00	394.15
524.62	6000.00	357.73
529.10	6000.00	344.17
533.77	6000.00	331.99
539.09	6000.00	316.72
543.60	6000.00	300.59
548.98	6000.00	283.97
553.05	6000.00	270.32
557.86	6000.00	255.8
563.84	6000.00	236.54
574.85	6000.00	211.93
583.18	6000.00	191.45
592.57	6000.00	176.14
604.10	6000.00	161.83
613.73	6000.00	158.49
559.74	3000.00	116.03
563.09	3000.00	119.84
574.33	3000.00	134.46
582.39	3000.00	142.99
591.77	3000.00	152.87
602.84	3000.00	161.38
612.37	3000.00	167.57
623.42	3000.00	174.58
632.04	3000.00	179.96
641.53	3000.00	186.21
650.90	3000.00	189.41
513.65	4000.00	333.84
524.25	4000.00	291.43
528.90	4000.00	269.01
533.55	4000.00	252.16
537.58	4000.00	231.06
541.47	4000.00	208.26
549.16	4000.00	178.39
553.43	4000.00	160.12
560.41	4000.00	132.63
563.94	4000.00	124.51
575.28	4000.00	113.58

584.60	4000.00	122.55
591.62	4000.00	127.84
603.68	4000.00	143.88
612.08	4000.00	149.82
621.22	4000.00	157.32
631.85	4000.00	163.15
641.95	4000.00	173.32
622.48	6000.00	158.77
632.41	6000.00	159.42
643.04	6000.00	164.74
513.40	8000.00	451.65
524.62	8000.00	417.84
528.95	8000.00	403.55
533.57	8000.00	391.25
538.84	8000.00	376.34
542.55	8000.00	364.39
548.66	8000.00	346.4
553.19	8000.00	335.76
557.81	8000.00	325.48
563.58	8000.00	312.82
574.41	8000.00	287.41
583.10	8000.00	270.69
593.19	8000.00	249.19
604.67	8000.00	226.0
613.93	8000.00	218.01
620.20	8000.00	211.6
632.86	8000.00	201.03
642.59	8000.00	195.65
515.30	10000.00	481.16
523.19	10000.00	459.31
533.40	10000.00	437.12
543.16	10000.00	413.25
553.20	10000.00	388.87
563.03	10000.00	363.89
573.39	10000.00	345.21
579.18	10000.00	331.94
515.23	5000.00	363.89
521.41	5000.00	337.01
534.45	5000.00	293.97
543.50	5000.00	262.34
553.42	5000.00	225.17
565.65	5000.00	187.87
582.86	10000.00	325.02
587.85	10000.00	315.79

592.71	10000.00	307.49
603.51	10000.00	291.2
614.03	10000.00	272.94
623.13	10000.00	260.67

Reference *https://www.doi.org/10.1021/acs.jced.8b00212*

Pressure, kPa	Temperature, K	Speed of sound, m/s
100.00	293.15	1151.69
100.00	298.16	1129.87
100.00	303.06	1108.88
100.00	308.08	1087.42
100.00	313.10	1066.12
100.00	318.18	1044.54
15200.00	293.20	1256.33
15200.00	303.17	1218.64
15200.00	308.08	1200.43
15200.00	313.10	1182.05
15200.00	318.18	1163.39
30400.00	293.18	1341.5
30400.00	303.13	1306.98
30400.00	308.07	1290.28
30400.00	313.12	1273.35
30400.00	318.18	1256.47
45590.00	293.19	1416.6
45590.00	298.18	1400.09
45590.00	303.07	1384.42
45590.00	308.07	1368.71
45590.00	313.12	1352.98
45590.00	318.17	1337.39
60790.00	293.20	1484.48
60790.00	298.19	1468.69
60790.00	303.18	1453.68
60790.00	308.12	1438.95
60790.00	313.12	1424.3
60790.00	318.17	1409.63
75990.00	293.20	1546.46
75990.00	298.11	1531.64
75990.00	303.17	1517.17
75990.00	308.12	1503.23
75990.00	313.10	1489.21
75990.00	318.09	1475.54
91190.00	293.20	1603.69

91190.00	298.15	1589.43
91190.00	303.18	1575.68
91190.00	308.11	1562.39
91190.00	313.13	1549.03
91190.00	318.15	1535.72
101320.00	293.20	1639.7
101320.00	298.16	1625.72
101320.00	303.10	1612.63
101320.00	308.24	1599.12
101320.00	313.21	1586.17
101320.00	318.18	1573.59
111450.00	293.10	1674.29
111450.00	298.13	1660.46
111450.00	298.16	1660.43
111450.00	303.15	1647.6
111450.00	308.21	1634.64
111450.00	313.20	1622.05
111450.00	318.18	1609.77
121580.00	293.16	1707.09
121580.00	298.14	1692.38
121580.00	303.10	1681.25
121580.00	308.17	1668.58
121580.00	313.13	1656.4
121580.00	318.17	1644.27

Reference *https://www.doi.org/10.1021/je030136n*

Molar heat capacity at constant pressure, J/K/mol

Temperature, K - Liquid	Pressure, kPa - Liquid	Molar heat capacity at constant pressure, J/K/mol - Liquid
273.15	100.00	216.20
273.15	5000.00	213.10
273.15	10000.00	210.90
273.15	15000.00	208.10
273.15	20000.00	207.20
293.15	100.00	224.10
293.15	5000.00	223.00
293.15	10000.00	218.20
293.15	15000.00	216.80
293.15	20000.00	214.40
313.15	100.00	233.80

313.15	5000.00	230.30
313.15	10000.00	226.20
313.15	15000.00	223.10
313.15	20000.00	221.60
333.15	100.00	241.90
333.15	5000.00	238.70
333.15	10000.00	235.00
333.15	15000.00	232.00
333.15	20000.00	229.30

Reference *https://www.doi.org/10.1016/j.jct.2011.06.019*

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
298.15	98.00	0.0003960
298.15	24510.00	0.0004923
298.15	49030.00	0.0006020
298.15	98060.00	0.0008489
298.15	147100.00	0.0011368
298.15	196130.00	0.0014932
298.15	245160.00	0.0019099
303.15	98.00	0.0003730
303.15	24510.00	0.0004737
303.15	49030.00	0.0005696
303.15	98060.00	0.0008037
303.15	147100.00	0.0010712
303.15	196130.00	0.0013890
303.15	245160.00	0.0017442
323.11	49030.00	0.0004816
323.13	24510.00	0.0003966
323.20	98060.00	0.0006613
323.20	147100.00	0.0008700
323.21	196130.00	0.0011121
323.25	98.00	0.0003107
323.25	245160.00	0.0013779
362.80	147100.00	0.0006488
362.83	98060.00	0.0004956
362.85	49030.00	0.0003626
362.87	196130.00	0.0008089
362.92	98.00	0.0002146

362.98	245160.00	0.0009926
363.07	24510.00	0.0002937
391.93	147100.00	0.0005310
392.00	196130.00	0.0006621
392.00	245160.00	0.0008047
392.04	98060.00	0.0004119
393.01	24510.00	0.0002366
393.14	49030.00	0.0002965
422.17	196130.00	0.0005591
422.24	98060.00	0.0003479
422.26	147100.00	0.0004464
422.58	24510.00	0.0001951
422.60	49030.00	0.0002476
423.04	245160.00	0.0006699
452.91	245160.00	0.0005770
453.04	196130.00	0.0004784
453.10	147100.00	0.0003883
453.16	98060.00	0.0003007
453.24	49030.00	0.0002134
453.40	24510.00	0.0001668
470.10	49030.00	0.0002021
470.19	24510.00	0.0001568
470.19	98060.00	0.0002858
470.19	147100.00	0.0003672
470.57	196130.00	0.0004549
470.61	245160.00	0.0005475

Reference *https://www.doi.org/10.1007/s10765-012-1373-z*

Temperature, K	Pressure, kPa	Viscosity, Pa*s
293.15	20000.00	0.0005090
293.15	40000.00	0.0006040
293.15	60000.00	0.0007060
293.15	80000.00	0.0008170
293.15	100000.00	0.0009370
313.15	20000.00	0.0004080
313.15	40000.00	0.0004870
313.15	60000.00	0.0005700
313.15	80000.00	0.0006580
313.15	100000.00	0.0007510
333.15	20000.00	0.0003360
333.15	40000.00	0.0004020
333.15	60000.00	0.0004720

333.15	80000.00	0.0005460
333.15	100000.00	0.0006230
353.15	20000.00	0.0002890
353.15	40000.00	0.0003460
353.15	60000.00	0.0004010
353.15	80000.00	0.0004580
353.15	100000.00	0.0005210

Reference *https://www.doi.org/10.1016/j.fluid.2006.01.030*

Temperature, K	Pressure, kPa	Viscosity, Pa*s
303.15	101.33	0.0003773

Reference *https://www.doi.org/10.1016/j.fluid.2010.10.009*

Temperature, K	Pressure, kPa	Viscosity, Pa*s
298.24	100.00	0.0003880
306.79	5000.00	0.0003779
306.79	10000.00	0.0004013
323.93	100.00	0.0002979
337.54	5000.00	0.0002800
337.54	10000.00	0.0002978
348.64	100.00	0.0002354
369.35	5000.00	0.0002116
369.35	10000.00	0.0002259
407.85	5000.00	0.0001595
407.85	10000.00	0.0001718
449.64	5000.00	0.0001220
449.64	10000.00	0.0001338
473.54	5000.00	0.0001012
473.54	10000.00	0.0001130

Reference *https://www.doi.org/10.1016/j.jct.2006.01.012*

Temperature, K	Pressure, kPa	Viscosity, Pa*s
293.15	5000.00	0.0004359
293.15	10000.00	0.0004603
293.15	20000.00	0.0005074
293.15	30000.00	0.0005517
293.15	40000.00	0.0005949
293.15	60000.00	0.0006912

293.15	80000.00	0.0007864
293.15	100000.00	0.0009027
293.15	120000.00	0.0010307
313.15	5000.00	0.0003564
313.15	10000.00	0.0003756
313.15	20000.00	0.0004131
313.15	30000.00	0.0004518
313.15	40000.00	0.0004899
313.15	60000.00	0.0005683
313.15	80000.00	0.0006498
313.15	100000.00	0.0007309
313.15	120000.00	0.0008186

Reference *https://www.doi.org/10.1016/j.jct.2015.12.021*

Temperature, K	Pressure, kPa	Viscosity, Pa*s
303.15	100.00	0.0003680
303.15	1000.00	0.0003710
303.15	5000.00	0.0003870
303.15	10000.00	0.0004080
303.15	15000.00	0.0004290
303.15	20000.00	0.0004500
303.15	25000.00	0.0004710
303.15	30000.00	0.0004920
303.15	35000.00	0.0005140
303.15	40000.00	0.0005350
303.15	45000.00	0.0005560
303.15	50000.00	0.0005780
303.15	55000.00	0.0006000
303.15	60000.00	0.0006220
313.15	100.00	0.0003300
313.15	1000.00	0.0003340
313.15	5000.00	0.0003480
313.15	10000.00	0.0003680
313.15	15000.00	0.0003880
313.15	20000.00	0.0004070
313.15	25000.00	0.0004270
313.15	30000.00	0.0004460
313.15	35000.00	0.0004650
313.15	40000.00	0.0004840
313.15	45000.00	0.0005030
313.15	50000.00	0.0005220
313.15	55000.00	0.0005420

313.15	60000.00	0.0005620
323.15	100.00	0.0003030
323.15	1000.00	0.0003060
323.15	5000.00	0.0003190
323.15	10000.00	0.0003360
323.15	15000.00	0.0003540
323.15	20000.00	0.0003710
323.15	25000.00	0.0003890
323.15	30000.00	0.0004060
323.15	35000.00	0.0004240
323.15	40000.00	0.0004420
323.15	45000.00	0.0004610
323.15	50000.00	0.0004790
323.15	55000.00	0.0004980
323.15	60000.00	0.0005170
333.15	100.00	0.0002730
333.15	1000.00	0.0002760
333.15	5000.00	0.0002890
333.15	10000.00	0.0003060
333.15	15000.00	0.0003230
333.15	20000.00	0.0003400
333.15	25000.00	0.0003570
333.15	30000.00	0.0003740
333.15	35000.00	0.0003900
333.15	40000.00	0.0004070
333.15	45000.00	0.0004230
333.15	50000.00	0.0004390
333.15	55000.00	0.0004560
333.15	60000.00	0.0004720
343.15	100.00	0.0002450
343.15	1000.00	0.0002470
343.15	5000.00	0.0002600
343.15	10000.00	0.0002770
343.15	15000.00	0.0002940
343.15	20000.00	0.0003100
343.15	25000.00	0.0003260
343.15	30000.00	0.0003410
343.15	35000.00	0.0003570
343.15	40000.00	0.0003720
343.15	45000.00	0.0003870
343.15	50000.00	0.0004020
343.15	55000.00	0.0004160
343.15	60000.00	0.0004310
353.15	100.00	0.0002310

353.15	1000.00	0.0002330
353.15	5000.00	0.0002460
353.15	10000.00	0.0002620
353.15	15000.00	0.0002780
353.15	20000.00	0.0002930
353.15	25000.00	0.0003070
353.15	30000.00	0.0003220
353.15	35000.00	0.0003360
353.15	40000.00	0.0003490
353.15	45000.00	0.0003610
353.15	50000.00	0.0003740
353.15	55000.00	0.0003860
353.15	60000.00	0.0003970

Reference *https://www.doi.org/10.1021/je049662k*

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
293.00	2100.00	687.2
293.00	3000.00	688.1
293.00	4000.00	688.9
293.00	5000.00	689.8
293.00	10000.00	694.0
293.00	20000.00	701.8
293.00	30000.00	708.7
293.00	40000.00	714.8
293.00	49900.00	720.8
293.00	59900.00	726.4
293.00	69900.00	731.6
293.00	79900.00	736.8
293.00	89900.00	741.5
293.00	99900.00	746.1
293.00	109900.00	750.6
293.00	119900.00	754.9
293.00	129900.00	759.2
293.00	134900.00	761.2
293.00	137400.00	762.2
313.00	2100.00	671.9
313.00	3000.00	672.9
313.00	4000.00	673.9

313.00	5000.00	674.8
313.00	10000.00	679.4
313.00	20000.00	688.0
313.00	30000.00	695.4
313.00	40000.00	702.2
313.00	49900.00	708.5
313.00	59900.00	714.3
313.00	69900.00	720.0
313.00	79900.00	725.2
313.00	89900.00	730.3
313.00	99900.00	735.1
313.00	109900.00	739.9
313.00	119900.00	744.3
313.00	129900.00	748.7
313.00	134900.00	751.0
313.00	137400.00	751.9
333.00	2100.00	654.8
333.00	3000.00	656.0
333.00	4000.00	657.7
333.00	5000.00	658.4
333.00	10000.00	663.9
333.00	20000.00	673.8
333.00	30000.00	682.3
333.00	40000.00	689.5
333.00	49900.00	696.5
333.00	59900.00	703.1
333.00	69900.00	708.9
333.00	79900.00	714.5
333.00	89900.00	720.0
333.00	99900.00	725.2
333.00	109900.00	729.8
333.00	119900.00	734.7
333.00	129900.00	739.3
333.00	134900.00	741.4
333.00	137400.00	742.6
353.00	2100.00	636.1
353.00	3000.00	637.6
353.00	4000.00	639.1
353.00	5000.00	640.4
353.00	10000.00	647.1
353.00	20000.00	658.5
353.00	30000.00	668.0
353.00	40000.00	676.7
353.00	49900.00	684.5

353.00	59900.00	691.3
353.00	69900.00	697.9
353.00	79900.00	703.8
353.00	89900.00	709.7
353.00	99900.00	715.0
353.00	109900.00	720.3
353.00	119900.00	725.3
353.00	129900.00	730.1
353.00	134900.00	732.4
353.00	137400.00	733.5
373.00	2100.00	616.9
373.00	3000.00	618.6
373.00	4000.00	620.3
373.00	5000.00	622.0
373.00	10000.00	629.9
373.00	20000.00	643.2
373.00	30000.00	654.1
373.00	40000.00	663.6
373.00	49900.00	672.0
373.00	59900.00	679.6
373.00	69900.00	686.7
373.00	79900.00	693.3
373.00	89900.00	699.4
373.00	99900.00	705.2
373.00	109900.00	710.7
373.00	119900.00	716.0
373.00	129900.00	720.9
373.00	134900.00	723.3
373.00	137400.00	724.5
393.00	2100.00	596.5
393.00	3000.00	598.7
393.00	4000.00	600.8
393.00	5000.00	602.8
393.00	10000.00	612.2
393.00	20000.00	627.8
393.00	30000.00	640.2
393.00	40000.00	650.8
393.00	49900.00	659.9
393.00	59900.00	668.3
393.00	69900.00	675.9
393.00	79900.00	682.9
393.00	89900.00	689.5
393.00	99900.00	695.7
393.00	109900.00	701.4

393.00	119900.00	706.8
393.00	129900.00	712.1
393.00	134900.00	714.7
393.00	137400.00	715.8
413.00	2100.00	574.1
413.00	3000.00	577.0
413.00	4000.00	579.6
413.00	5000.00	582.1
413.00	10000.00	593.6
413.00	20000.00	611.9
413.00	30000.00	626.0
413.00	40000.00	637.6
413.00	49900.00	647.8
413.00	59900.00	656.9
413.00	69900.00	664.7
413.00	79900.00	672.4
413.00	89900.00	679.3
413.00	99900.00	685.8
413.00	109900.00	692.2
413.00	119900.00	698.0
413.00	129900.00	703.6
413.00	134900.00	706.2
413.00	137400.00	707.4
433.00	2100.00	550.1
433.00	3000.00	553.9
433.00	4000.00	557.5
433.00	5000.00	560.7
433.00	10000.00	574.6
433.00	20000.00	595.4
433.00	30000.00	611.5
433.00	40000.00	624.3
433.00	49900.00	635.2
433.00	59900.00	644.7
433.00	69900.00	653.5
433.00	79900.00	661.6
433.00	89900.00	669.0
433.00	99900.00	676.0
433.00	109900.00	682.3
433.00	119900.00	688.5
433.00	129900.00	694.3
433.00	134900.00	697.2
433.00	137400.00	698.6
448.00	2100.00	531.1
448.00	3000.00	535.6

448.00	4000.00	539.8
448.00	5000.00	543.6
448.00	10000.00	560.0
448.00	20000.00	583.0
448.00	30000.00	600.3
448.00	40000.00	614.4
448.00	49900.00	626.2
448.00	59900.00	636.6
448.00	69900.00	646.2
448.00	79900.00	654.4
448.00	89900.00	661.8
448.00	99900.00	669.2
448.00	109900.00	675.8
448.00	119900.00	682.3
448.00	129900.00	688.4
448.00	134900.00	691.4
448.00	137400.00	692.6
468.00	2100.00	501.1
468.00	3000.00	507.8
468.00	4000.00	513.4
468.00	5000.00	518.6
468.00	10000.00	539.1
468.00	20000.00	566.5
468.00	30000.00	586.2
468.00	40000.00	601.3
468.00	49900.00	614.2
468.00	59900.00	625.3
468.00	69900.00	635.2
468.00	79900.00	644.1
468.00	89900.00	652.3
468.00	99900.00	659.9
468.00	109900.00	667.2
468.00	119900.00	673.9
468.00	129900.00	679.9
468.00	134900.00	682.8
468.00	137400.00	684.3

Reference *https://www.doi.org/10.1016/j.fluid.2016.09.021*

Temperature, K	Pressure, kPa	Mass density, kg/m3
233.15	101.68	733.289
233.15	1104.14	733.918
233.15	2003.32	734.481

233.15	4006.02	735.714
233.15	6004.84	736.928
233.15	8009.54	738.125
233.15	9956.83	739.277
233.15	11864.20	740.377
233.15	13984.20	741.588
233.15	15994.70	742.722
233.15	17888.30	743.774
233.15	20074.10	744.977
233.15	22023.80	746.029
233.15	24017.60	747.094
233.15	25954.00	748.113
233.15	27944.50	749.147
233.15	29979.30	750.192
253.15	98.99	717.086
253.15	1101.50	717.807
253.15	2000.52	718.446
253.15	4006.34	719.85
253.15	6005.44	721.223
253.15	8147.76	722.669
253.15	10096.20	723.959
253.15	11827.30	725.088
253.15	13955.10	726.459
253.15	16060.20	727.785
253.15	18039.50	729.014
253.15	20020.00	730.22
253.15	22093.30	731.465
253.15	23827.70	732.495
253.15	25891.20	733.701
253.15	27738.70	734.762
253.15	29899.80	735.987
273.15	102.15	700.687
273.15	1101.26	701.507
273.15	2006.30	702.244
273.15	4005.43	703.841
273.15	6005.46	705.403
273.15	8197.47	707.077
273.15	10109.30	708.507
273.15	12113.70	709.976
273.15	14092.30	711.403
273.15	16115.70	712.831
273.15	18076.00	714.19
273.15	20096.30	715.565
273.15	22068.90	716.883

273.15	24101.50	718.226
273.15	25917.60	719.397
273.15	27991.30	720.718
273.15	29444.50	721.633
293.15	98.89	683.986
293.15	1104.28	684.937
293.15	2003.35	685.779
293.15	4003.02	687.611
293.15	6003.71	689.394
293.15	8007.44	691.14
293.15	10027.90	692.854
293.15	12138.70	694.603
293.15	14007.80	696.118
293.15	16160.30	697.827
293.15	18149.30	699.368
293.15	19992.10	700.756
293.15	22123.00	702.362
293.15	24036.20	703.766
293.15	25999.00	705.175
293.15	27982.80	706.576
293.15	29985.70	707.965
313.15	101.45	666.898
313.15	1102.20	667.995
313.15	2005.49	668.973
313.15	4004.53	671.086
313.15	6106.94	673.238
313.15	7941.18	675.062
313.15	9944.39	676.997
313.15	11841.20	678.793
313.15	13782.40	680.575
313.15	16032.40	682.588
313.15	17876.00	684.2
313.15	19748.40	685.804
313.15	21802.90	687.518
313.15	23828.70	689.172
313.15	25813.90	690.765
313.15	27801.40	692.324
313.15	29818.40	693.872
333.15	103.00	649.298
333.15	1105.97	650.588
333.15	2004.12	651.723
333.15	4003.59	654.18
333.15	6004.59	656.549
333.15	8005.55	658.837

333.15	9901.48	660.933
333.15	12083.40	663.274
333.15	14040.10	665.309
333.15	16005.20	667.293
333.15	17854.30	669.109
333.15	19984.70	671.149
333.15	21966.60	672.997
333.15	23925.50	674.778
333.15	25823.40	676.467
333.15	27822.80	678.205
333.15	30009.20	680.058
353.15	99.37	631.037
353.15	1182.85	632.68
353.15	2156.26	634.131
353.15	4140.73	636.982
353.15	6175.55	639.78
353.15	8138.91	642.37
353.15	10095.00	644.851
353.15	12083.30	647.284
353.15	14039.80	649.596
353.15	16039.20	651.883
353.15	18008.20	654.064
353.15	19996.30	656.201
353.15	21955.50	658.247
353.15	23925.40	660.247
353.15	25887.20	662.188
353.15	27855.00	664.084
353.15	29976.00	666.077
373.15	1164.33	613.877
373.15	2149.21	615.631
373.15	4123.49	618.999
373.15	5987.02	622.014
373.15	8094.82	625.262
373.15	10059.80	628.151
373.15	12066.30	630.972
373.15	14017.80	633.61
373.15	16044.40	636.241
373.15	18058.00	638.765
373.15	19975.60	641.085
373.15	21959.60	643.408
373.15	23948.00	645.665
373.15	25804.80	647.712
373.15	27898.40	649.952
373.15	29818.70	651.952

393.15	1101.93	593.952
393.15	2001.51	595.905
393.15	4002.83	600.027
393.15	6004.29	603.884
393.15	8005.48	607.511
393.15	10007.10	610.942
393.15	12110.90	614.361
393.15	14116.50	617.466
393.15	16097.20	620.399
393.15	18029.00	623.142
393.15	20054.00	625.904
393.15	22015.90	628.483
393.15	24005.50	631.008
393.15	25986.10	633.434
393.15	27951.60	635.769
393.15	29842.80	638.037

Reference *https://www.doi.org/10.1016/j.jct.2008.02.020*

Temperature, K	Pressure, kPa	Mass density, kg/m3
313.18	1000.00	668.09
313.18	2000.00	669.03
313.18	3000.00	669.97
313.18	4000.00	670.93
313.18	5010.00	671.9
313.18	6000.00	672.87
313.18	7000.00	673.86
313.18	8000.00	674.87
313.18	9000.00	675.87
313.18	10000.00	676.86
313.18	11000.00	677.85
313.18	12000.00	678.83
313.18	13000.00	679.81
313.18	14000.00	680.76
313.18	15000.00	681.7
313.18	16000.00	682.62
313.18	17000.00	683.53
313.18	18000.00	684.41
313.18	19000.00	685.26
313.18	20000.00	686.11
313.18	21000.00	686.92
313.18	22000.00	687.67
313.18	23000.00	688.42

313.18	23910.00	689.07
313.18	25000.00	689.85
333.04	1000.00	650.66
333.04	2000.00	651.8
333.04	3000.00	652.94
333.04	4000.00	654.08
333.04	5000.00	655.23
333.04	6000.00	656.38
333.04	7000.00	657.54
333.04	8000.00	658.65
333.04	9000.00	659.81
333.04	10000.00	660.92
333.04	11000.00	662.03
333.04	12000.00	663.1
333.04	13000.00	664.2
333.04	14000.00	665.25
333.04	15000.00	666.31
333.04	16000.00	667.33
333.04	17000.00	668.33
333.04	18030.00	669.34
333.04	19000.00	670.26
333.04	20000.00	671.2
333.04	22000.00	673.01
333.04	23000.00	673.86
333.04	24000.00	674.7
333.04	25000.00	675.52
333.04	23000.00	673.86
353.06	1010.00	632.6
353.06	2000.00	634.02
353.06	3000.00	635.41
353.06	4000.00	636.78
353.06	5000.00	638.15
353.06	6000.00	639.47
353.06	7000.00	640.8
353.06	8000.00	642.1
353.06	9010.00	643.4
353.06	10000.00	644.66
353.06	11000.00	645.92
353.06	12000.00	647.13
353.06	13000.00	648.37
353.06	14000.00	649.56
353.06	15000.00	650.72
353.06	16000.00	651.88
353.06	17000.00	653.0

353.06	18030.00	654.12
353.06	19000.00	655.16
353.06	20000.00	656.22
353.06	21000.00	657.27
353.06	22000.00	658.25
353.06	23000.00	659.24
353.06	24000.00	660.2
353.06	25000.00	661.14

Reference *https://www.doi.org/10.1016/j.jct.2011.08.016*

Temperature, K	Pressure, kPa	Mass density, kg/m3
298.15	100.00	679.5
298.15	1000.00	680.4
298.15	5000.00	684.2
298.15	10000.00	688.6
298.15	15000.00	692.8
298.15	20000.00	696.7
298.15	25000.00	700.4
298.15	30000.00	704.0
298.15	35000.00	707.4
298.15	40000.00	710.7
298.15	45000.00	713.8
298.15	50000.00	716.8
298.15	55000.00	719.7
298.15	60000.00	722.5
298.15	65000.00	725.2
298.15	70000.00	727.9
298.15	80000.00	732.9
298.15	90000.00	737.7
298.15	100000.00	742.3
298.15	110000.00	746.6
298.15	120000.00	750.7
298.15	130000.00	754.6
298.15	140000.00	758.4
313.15	100.00	666.6
313.15	1000.00	667.6
313.15	5000.00	671.8
313.15	10000.00	676.7
313.15	15000.00	681.3
313.15	20000.00	685.6
313.15	25000.00	689.5
313.15	30000.00	693.5

313.15	35000.00	697.1
313.15	40000.00	700.5
313.15	45000.00	703.9
313.15	50000.00	707.2
313.15	55000.00	710.3
313.15	60000.00	713.3
313.15	65000.00	716.1
313.15	70000.00	718.9
313.15	80000.00	724.2
313.15	90000.00	729.3
313.15	100000.00	734.0
313.15	110000.00	738.6
313.15	120000.00	742.8
313.15	130000.00	747.0
313.15	140000.00	751.1
333.15	100.00	648.9
333.15	1000.00	650.0
333.15	5000.00	655.0
333.15	10000.00	660.6
333.15	15000.00	665.8
333.15	20000.00	670.6
333.15	25000.00	675.1
333.15	30000.00	679.4
333.15	35000.00	683.4
333.15	40000.00	687.3
333.15	45000.00	690.9
333.15	50000.00	694.4
333.15	55000.00	697.7
333.15	60000.00	701.0
333.15	65000.00	704.1
333.15	70000.00	707.1
333.15	80000.00	712.8
333.15	90000.00	718.2
333.15	100000.00	723.2
333.15	110000.00	728.1
333.15	120000.00	732.6
333.15	130000.00	737.0
333.15	140000.00	741.1
353.15	100.00	631.2
353.15	1000.00	632.1
353.15	5000.00	637.8
353.15	10000.00	644.3
353.15	15000.00	650.3
353.15	20000.00	655.7

353.15	25000.00	660.8
353.15	30000.00	665.5
353.15	35000.00	670.0
353.15	40000.00	674.1
353.15	45000.00	678.1
353.15	50000.00	682.0
353.15	55000.00	685.5
353.15	60000.00	689.1
353.15	65000.00	692.4
353.15	70000.00	695.7
353.15	80000.00	701.7
353.15	90000.00	707.5
353.15	100000.00	712.8
353.15	110000.00	717.9
353.15	120000.00	722.7
353.15	130000.00	727.3
353.15	140000.00	731.6
373.15	1000.00	613.3
373.15	5000.00	620.1
373.15	10000.00	627.7
373.15	15000.00	634.5
373.15	20000.00	640.7
373.15	25000.00	646.3
373.15	30000.00	651.6
373.15	35000.00	656.5
373.15	40000.00	661.1
373.15	45000.00	665.5
373.15	50000.00	669.6
373.15	55000.00	673.5
373.15	60000.00	677.3
373.15	65000.00	680.8
373.15	70000.00	684.3
373.15	80000.00	690.8
373.15	90000.00	696.9
373.15	100000.00	702.6
373.15	110000.00	708.0
373.15	120000.00	713.0
373.15	130000.00	717.9
373.15	140000.00	722.3
393.15	1000.00	593.5
393.15	5000.00	601.7
393.15	10000.00	610.6
393.15	15000.00	618.4
393.15	20000.00	625.4

393.15	25000.00	631.7
393.15	30000.00	637.5
393.15	35000.00	643.0
393.15	40000.00	648.0
393.15	45000.00	652.8
393.15	50000.00	657.2
393.15	55000.00	661.5
393.15	60000.00	665.5
393.15	65000.00	669.3
393.15	70000.00	673.1
393.15	80000.00	680.1
393.15	90000.00	686.5
393.15	100000.00	692.5
393.15	110000.00	698.2
393.15	120000.00	703.4
393.15	130000.00	708.5
393.15	140000.00	713.4

Reference *https://www.doi.org/10.1016/j.jct.2013.05.051*

Temperature, K	Pressure, kPa	Mass density, kg/m3
288.15	101.00	688.33
293.15	101.00	684.11
298.15	101.00	679.87
303.15	101.00	675.6
308.15	101.00	671.31
313.15	101.00	667.0
288.15	100.00	688.4
288.15	1000.00	689.2
288.15	5000.00	692.5
288.15	10000.00	696.5
288.15	15000.00	700.4
288.15	20000.00	704.1
288.15	25000.00	707.7
288.15	30000.00	711.1
288.15	35000.00	714.3
288.15	40000.00	717.4
288.15	45000.00	720.3
288.15	50000.00	723.1
288.15	55000.00	725.8
288.15	60000.00	728.2
293.15	100.00	684.2
293.15	1000.00	685.0

293.15	5000.00	688.4
293.15	10000.00	692.6
293.15	15000.00	696.5
293.15	20000.00	700.4
293.15	25000.00	704.0
293.15	30000.00	707.5
293.15	35000.00	710.9
293.15	40000.00	714.0
293.15	45000.00	717.0
293.15	50000.00	719.9
293.15	55000.00	722.5
293.15	60000.00	725.1
298.15	100.00	679.9
298.15	1000.00	680.7
298.15	5000.00	684.3
298.15	10000.00	688.6
298.15	15000.00	692.7
298.15	20000.00	696.6
298.15	25000.00	700.4
298.15	30000.00	704.0
298.15	35000.00	707.4
298.15	40000.00	710.7
298.15	45000.00	713.8
298.15	50000.00	716.7
298.15	55000.00	719.4
298.15	60000.00	721.9
303.15	100.00	675.7
303.15	1000.00	676.5
303.15	5000.00	680.2
303.15	10000.00	684.6
303.15	15000.00	688.9
303.15	20000.00	693.0
303.15	25000.00	696.8
303.15	30000.00	700.5
303.15	35000.00	704.0
303.15	40000.00	707.4
303.15	45000.00	710.5
303.15	50000.00	713.5
303.15	55000.00	716.2
303.15	60000.00	718.8
308.15	100.00	671.4
308.15	1000.00	672.2
308.15	5000.00	676.0
308.15	10000.00	680.6

308.15	15000.00	685.0
308.15	20000.00	689.2
308.15	25000.00	693.2
308.15	30000.00	697.0
308.15	35000.00	700.6
308.15	40000.00	704.0
308.15	45000.00	707.2
308.15	50000.00	710.3
308.15	55000.00	713.1
308.15	60000.00	715.7
313.15	100.00	667.1
313.15	1000.00	668.0
313.15	5000.00	672.0
313.15	10000.00	676.7
313.15	15000.00	681.2
313.15	20000.00	685.5
313.15	25000.00	689.6
313.15	30000.00	693.5
313.15	35000.00	697.2
313.15	40000.00	700.7
313.15	45000.00	704.0
313.15	50000.00	707.1
313.15	55000.00	709.9
313.15	60000.00	712.6
318.15	100.00	662.7
318.15	1000.00	663.6
318.15	5000.00	667.7
318.15	10000.00	672.6
318.15	15000.00	677.3
318.15	20000.00	681.8
318.15	25000.00	686.0
318.15	30000.00	690.0
318.15	35000.00	693.8
318.15	40000.00	697.4
318.15	45000.00	700.7
318.15	50000.00	703.9
318.15	55000.00	706.8
318.15	60000.00	709.5
323.15	100.00	658.3
323.15	1000.00	659.3
323.15	5000.00	663.5
323.15	10000.00	668.6
323.15	15000.00	673.4
323.15	20000.00	678.0

323.15	25000.00	682.4
323.15	30000.00	686.5
323.15	35000.00	690.4
323.15	40000.00	694.1
323.15	45000.00	697.5
323.15	50000.00	700.7
323.15	55000.00	703.7
323.15	60000.00	706.4
328.15	100.00	653.9
328.15	1000.00	654.9
328.15	5000.00	659.3
328.15	10000.00	664.5
328.15	15000.00	669.5
328.15	20000.00	674.3
328.15	25000.00	678.8
328.15	30000.00	683.0
328.15	35000.00	687.0
328.15	40000.00	690.8
328.15	45000.00	694.3
328.15	50000.00	697.6
328.15	55000.00	700.6
328.15	60000.00	703.3
333.15	100.00	649.5
333.15	1000.00	650.6
333.15	5000.00	655.1
333.15	10000.00	660.5
333.15	15000.00	665.7
333.15	20000.00	670.6
333.15	25000.00	675.2
333.15	30000.00	679.6
333.15	35000.00	683.7
333.15	40000.00	687.5
333.15	45000.00	691.1
333.15	50000.00	694.4
333.15	55000.00	697.4
333.15	60000.00	700.2
343.15	100.00	640.5
343.15	1000.00	641.6
343.15	5000.00	646.5
343.15	10000.00	652.3
343.15	15000.00	657.8
343.15	20000.00	663.1
343.15	25000.00	668.0
343.15	30000.00	672.6

343.15	35000.00	676.9
343.15	40000.00	681.0
343.15	45000.00	684.7
343.15	50000.00	688.1
343.15	55000.00	691.3
343.15	60000.00	694.1
353.15	100.00	631.3
353.15	1000.00	632.5
353.15	5000.00	637.8
353.15	10000.00	644.0
353.15	15000.00	649.9
353.15	20000.00	655.5
353.15	25000.00	660.7
353.15	30000.00	665.6
353.15	35000.00	670.2
353.15	40000.00	674.4
353.15	45000.00	678.3
353.15	50000.00	681.9
353.15	55000.00	685.1
353.15	60000.00	688.0
363.15	100.00	621.9
363.15	1000.00	623.2
363.15	5000.00	628.9
363.15	10000.00	635.6
363.15	15000.00	641.9
363.15	20000.00	647.9
363.15	25000.00	653.4
363.15	30000.00	658.6
363.15	35000.00	663.5
363.15	40000.00	667.9
363.15	45000.00	672.0
363.15	50000.00	675.7
363.15	55000.00	679.0
363.15	60000.00	681.9
373.15	1000.00	614.2
373.15	5000.00	620.2
373.15	10000.00	627.4
373.15	15000.00	634.1
373.15	20000.00	640.4
373.15	25000.00	646.3
373.15	30000.00	651.8
373.15	35000.00	656.9
373.15	40000.00	661.5
373.15	45000.00	665.8

373.15	50000.00	669.6
373.15	55000.00	673.1
373.15	60000.00	676.1
393.15	1000.00	594.6
393.15	5000.00	601.7
393.15	10000.00	610.0
393.15	15000.00	617.8
393.15	20000.00	625.0
393.15	25000.00	631.7
393.15	30000.00	637.9
393.15	35000.00	643.6
393.15	40000.00	648.7
393.15	45000.00	653.3
393.15	50000.00	657.4
393.15	55000.00	660.9
393.15	60000.00	663.9
413.15	1000.00	574.1
413.15	5000.00	582.3
413.15	10000.00	592.0
413.15	15000.00	600.9
413.15	20000.00	609.2
413.15	25000.00	616.9
413.15	30000.00	623.9
413.15	35000.00	630.2
413.15	40000.00	635.9
413.15	45000.00	640.9
413.15	50000.00	645.2
413.15	55000.00	648.9
413.15	60000.00	651.9

Reference *https://www.doi.org/10.1016/j.jct.2016.04.014*

Pressure, kPa	Temperature, K	Mass density, kg/m3
100.00	298.15	679.71

Reference *https://www.doi.org/10.1016/j.jct.2017.09.027*

Temperature, K	Pressure, kPa	Mass density, kg/m3
283.15	100.00	692.57
288.15	100.00	688.55
293.15	100.00	684.19
298.15	100.00	679.95

303.15	100.00	675.68
308.15	100.00	671.39
313.15	100.00	667.06
318.15	100.00	662.54
323.15	100.00	658.32
328.15	100.00	653.81
283.15	2000.00	694.49
288.15	2000.00	690.28
293.15	2000.00	686.15
298.15	2000.00	682.02
303.15	2000.00	677.75
308.15	2000.00	673.45
313.15	2000.00	669.26
318.15	2000.00	664.87
323.15	2000.00	660.53
328.15	2000.00	656.27
283.15	5000.00	697.06
288.15	5000.00	693.01
293.15	5000.00	688.99
298.15	5000.00	684.8
303.15	5000.00	680.76
308.15	5000.00	676.49
313.15	5000.00	672.35
318.15	5000.00	668.35
323.15	5000.00	664.05
328.15	5000.00	659.84
283.15	7000.00	698.8
288.15	7000.00	694.77
293.15	7000.00	690.74
298.15	7000.00	686.68
303.15	7000.00	682.65
308.15	7000.00	678.48
313.15	7000.00	674.51
318.15	7000.00	670.32
323.15	7000.00	666.33
328.15	7000.00	661.99
283.15	10000.00	701.2
288.15	10000.00	697.23
293.15	10000.00	693.41
298.15	10000.00	689.23
303.15	10000.00	685.52
308.15	10000.00	681.37
313.15	10000.00	677.42
318.15	10000.00	673.52

323.15	10000.00	669.41
328.15	10000.00	665.25
283.15	20000.00	709.08
288.15	20000.00	705.18
293.15	20000.00	701.57
298.15	20000.00	697.65
303.15	20000.00	694.07
308.15	20000.00	690.12
313.15	20000.00	686.53
318.15	20000.00	682.85
323.15	20000.00	679.17
328.15	20000.00	675.25
283.15	30000.00	716.12
288.15	30000.00	712.38
293.15	30000.00	708.99
298.15	30000.00	705.17
303.15	30000.00	701.86
308.15	30000.00	698.22
313.15	30000.00	694.65
318.15	30000.00	691.31
323.15	30000.00	687.64
328.15	30000.00	684.02
283.15	40000.00	722.63
288.15	40000.00	719.01
293.15	40000.00	715.7
298.15	40000.00	712.11
303.15	40000.00	708.87
308.15	40000.00	705.32
313.15	40000.00	702.08
318.15	40000.00	698.89
323.15	40000.00	695.38
328.15	40000.00	691.84
283.15	50000.00	728.63
288.15	50000.00	725.2
293.15	50000.00	722.03
298.15	50000.00	718.54
303.15	50000.00	715.5
308.15	50000.00	712.12
313.15	50000.00	708.98
318.15	50000.00	705.82
323.15	50000.00	702.5
328.15	50000.00	699.13
283.15	60000.00	734.33
288.15	60000.00	731.01

293.15	60000.00	728.02
298.15	60000.00	724.73
303.15	60000.00	721.67
308.15	60000.00	718.41
313.15	60000.00	715.39
318.15	60000.00	712.36
323.15	60000.00	709.15
328.15	60000.00	706.05
283.15	65000.00	736.99
288.15	65000.00	733.73
293.15	65000.00	730.72
298.15	65000.00	727.65
303.15	65000.00	724.56
308.15	65000.00	721.43
313.15	65000.00	718.32
318.15	65000.00	715.32
323.15	65000.00	712.32
328.15	65000.00	709.3

Reference *https://www.doi.org/10.1016/j.tca.2015.06.017*

Temperature, K	Pressure, kPa	Mass density, kg/m3
298.15	100.00	680.0
298.15	3000.00	683.0
298.15	6000.00	686.0
298.15	9000.00	689.0
298.15	12000.00	691.0
298.15	15000.00	694.0
308.15	100.00	670.0
308.15	3000.00	674.0
308.15	6000.00	677.0
308.15	9000.00	680.0
308.15	12000.00	683.0
308.15	15000.00	685.0
318.15	100.00	662.0
318.15	3000.00	666.0
318.15	6000.00	669.0
318.15	9000.00	672.0
318.15	12000.00	675.0
318.15	15000.00	678.0

Reference *https://www.doi.org/10.1016/j.tca.2018.10.018*

Temperature, K	Pressure, kPa	Mass density, kg/m3
293.25	2103.00	685.58
293.25	3666.00	687.27
293.25	6195.00	689.52
293.25	10385.00	693.22
293.25	14421.00	696.48
293.25	17447.00	698.88
293.25	20472.00	701.01
293.25	23543.00	703.3
293.25	26611.00	705.5
313.08	2050.00	669.15
313.08	4083.00	671.15
313.08	6733.00	673.77
313.07	11204.00	678.28
313.08	14195.00	681.03
313.07	17225.00	683.61
313.07	20247.00	686.13
313.08	23266.00	688.54
313.08	26286.00	691.26
313.07	29805.00	693.98
332.78	2084.00	652.25
332.77	4091.00	654.57
332.78	7031.00	658.26
332.78	11151.00	662.67
332.78	14177.00	665.56
332.78	17172.00	668.79
332.78	20193.00	671.47
332.78	23214.00	674.57
332.78	26231.00	677.28
352.39	2184.00	635.33
352.39	4102.00	637.96
352.40	7146.00	641.83
352.39	11159.00	646.85
352.39	14169.00	650.4
352.39	17199.00	653.84
352.40	20204.00	657.05
352.40	23212.00	660.04
352.40	26228.00	663.06
352.39	29758.00	666.6

Reference *https://www.doi.org/10.1021/acs.jced.5b00152*

Pressure, kPa	Temperature, K	Mass density, kg/m3

100.00	278.15	696.3
100.00	283.15	692.1
100.00	293.15	683.7
100.00	303.15	675.3
100.00	313.15	666.6
100.00	323.15	657.6
100.00	333.15	648.9
100.00	343.15	639.8
100.00	353.15	630.6
1000.00	278.15	697.0
1000.00	283.15	692.9
1000.00	293.15	684.6
1000.00	303.15	676.2
1000.00	313.15	667.6
1000.00	323.15	658.7
1000.00	333.15	650.0
1000.00	343.15	641.1
1000.00	353.15	632.0
2500.00	278.15	698.3
2500.00	283.15	694.2
2500.00	293.15	685.9
2500.00	303.15	677.7
2500.00	313.15	669.1
2500.00	323.15	660.4
2500.00	333.15	651.8
2500.00	343.15	643.1
2500.00	353.15	634.2
5000.00	278.15	700.3
5000.00	283.15	696.3
5000.00	293.15	688.2
5000.00	303.15	680.1
5000.00	313.15	671.7
5000.00	323.15	663.1
5000.00	333.15	654.8
5000.00	343.15	646.3
5000.00	353.15	637.8
7500.00	278.15	702.3
7500.00	283.15	698.3
7500.00	293.15	690.4
7500.00	303.15	682.4
7500.00	313.15	674.2
7500.00	323.15	665.8
7500.00	333.15	657.6
7500.00	343.15	649.4

7500.00	353.15	641.1
10000.00	278.15	704.2
10000.00	283.15	700.2
10000.00	293.15	692.5
10000.00	303.15	684.7
10000.00	313.15	676.6
10000.00	323.15	668.4
10000.00	333.15	660.4
10000.00	343.15	652.4
10000.00	353.15	644.3
15000.00	278.15	707.9
15000.00	283.15	704.0
15000.00	293.15	696.6
15000.00	303.15	689.0
15000.00	313.15	681.2
15000.00	323.15	673.3
15000.00	333.15	665.6
15000.00	343.15	658.0
15000.00	353.15	650.3
20000.00	278.15	711.4
20000.00	283.15	707.6
20000.00	293.15	700.4
20000.00	303.15	693.0
20000.00	313.15	685.5
20000.00	323.15	677.9
20000.00	333.15	670.4
20000.00	343.15	663.1
20000.00	353.15	655.7
25000.00	278.15	714.7
25000.00	283.15	711.1
25000.00	293.15	703.9
25000.00	303.15	696.9
25000.00	313.15	689.5
25000.00	323.15	682.1
25000.00	333.15	674.9
25000.00	343.15	667.9
25000.00	353.15	660.8

Reference *https://www.doi.org/10.1021/je034056v*

Temperature, K	Pressure, kPa	Mass density, kg/m3
278.15	100.00	696.36
278.15	1000.00	697.01

278.15	5000.00	700.47
278.15	10000.00	704.35
278.15	15000.00	708.03
278.15	20000.00	711.54
278.15	25000.00	714.88
278.15	30000.00	718.17
278.15	35000.00	721.23
278.15	40000.00	724.19
278.15	45000.00	727.05
283.15	100.00	692.23
283.15	1000.00	693.01
283.15	5000.00	696.39
283.15	10000.00	700.44
283.15	15000.00	704.24
283.15	20000.00	707.85
283.15	25000.00	711.27
283.15	30000.00	714.56
283.15	35000.00	717.81
283.15	40000.00	720.8
283.15	45000.00	723.72
293.15	100.00	683.79
293.15	1000.00	684.6
293.15	5000.00	688.22
293.15	10000.00	692.49
293.15	15000.00	696.52
293.15	20000.00	700.34
293.15	25000.00	703.98
293.15	30000.00	707.62
293.15	35000.00	710.9
293.15	40000.00	714.1
293.15	45000.00	717.14
303.15	100.00	675.35
303.15	1000.00	676.16
303.15	5000.00	680.06
303.15	10000.00	684.63
303.15	15000.00	688.92
303.15	20000.00	692.96
303.15	25000.00	696.8
303.15	30000.00	700.52
303.15	35000.00	704.0
303.15	40000.00	707.3
303.15	45000.00	710.51
313.15	100.00	666.86
313.15	1000.00	667.7

313.15	5000.00	671.91
313.15	10000.00	676.8
313.15	15000.00	681.35
313.15	20000.00	685.63
313.15	25000.00	689.69
313.15	30000.00	693.53
313.15	35000.00	697.19
313.15	40000.00	700.67
313.15	45000.00	704.02
323.15	100.00	657.9
323.15	1000.00	658.85
323.15	5000.00	663.24
323.15	10000.00	668.53
323.15	15000.00	673.44
323.15	20000.00	677.94
323.15	25000.00	682.25
323.15	30000.00	686.3
323.15	35000.00	690.15
323.15	40000.00	693.83
323.15	45000.00	697.33
333.15	100.00	648.77
333.15	1000.00	649.92
333.15	5000.00	654.8
333.15	10000.00	660.46
333.15	15000.00	665.66
333.15	20000.00	670.49
333.15	25000.00	675.03
333.15	30000.00	679.3
333.15	35000.00	683.35
333.15	40000.00	687.19
333.15	45000.00	690.85
343.15	100.00	639.69
343.15	1000.00	640.93
343.15	5000.00	646.23
343.15	10000.00	652.33
343.15	15000.00	657.9
343.15	20000.00	663.04
343.15	25000.00	667.86
343.15	30000.00	672.37
343.15	35000.00	676.61
343.15	40000.00	680.63
343.15	45000.00	684.47
353.15	100.00	630.49
353.15	1000.00	631.83

353.15	5000.00	637.6
353.15	10000.00	644.13
353.15	15000.00	650.11
353.15	20000.00	655.53
353.15	25000.00	660.64
353.15	30000.00	665.38
353.15	35000.00	669.83
353.15	40000.00	674.08
353.15	45000.00	678.04

Reference *https://www.doi.org/10.1021/je049580w*

Temperature, K	Pressure, kPa	Mass density, kg/m3
313.15	340.00	667.1
313.15	690.00	667.5
313.15	1030.00	667.8
313.15	1380.00	668.2
313.15	1720.00	668.64
313.15	2070.00	669.0
313.15	2410.00	669.3
313.15	2760.00	669.8
313.15	3100.00	670.1
313.15	3450.00	670.4
313.15	3800.00	670.8
313.15	4140.00	671.2
313.15	4480.00	671.6
313.15	4830.00	671.9
313.15	5170.00	672.2
313.15	5510.00	672.6
313.15	5860.00	672.9
313.15	6200.00	673.3
313.15	6550.00	673.6
313.15	6890.00	674.0
313.15	7240.00	674.3
333.15	340.00	649.7
333.15	690.00	650.2
333.15	1030.00	650.6
333.15	1380.00	651.0
333.15	1720.00	651.4
333.15	2070.00	651.9
333.15	2410.00	652.3
333.15	2760.00	652.7
333.15	3100.00	653.2

333.15	3450.00	653.6
333.15	3800.00	654.0
333.15	4140.00	654.4
333.15	4480.00	654.8
333.15	4830.00	655.2
333.15	5170.00	655.6
333.15	5510.00	656.0
333.15	5860.00	656.4
333.15	6200.00	656.8
333.15	6550.00	657.2
333.15	6890.00	657.6
333.15	7240.00	658.0
333.15	7580.00	658.4
333.15	7930.00	658.8
333.15	8270.00	659.2
353.15	340.00	631.8
353.15	690.00	632.3
353.15	1030.00	632.8
353.15	1380.00	633.3
353.15	1720.00	633.9
353.15	2070.00	634.4
353.15	2410.00	634.9
353.15	2760.00	635.3
353.15	3100.00	635.8
353.15	3450.00	636.3
353.15	3800.00	636.8
353.15	4140.00	637.3
353.15	4480.00	637.7
353.15	4830.00	638.2
353.15	5170.00	638.7
353.15	5510.00	639.2
353.15	5860.00	639.6
353.15	6200.00	640.1
353.15	6550.00	640.6
353.15	6890.00	641.0
353.15	7240.00	641.5
353.15	7580.00	641.9
353.15	7930.00	642.3
353.15	8270.00	642.8
353.15	8620.00	643.2
353.15	8960.00	643.9
353.15	9310.00	644.1
353.15	9650.00	644.5
373.15	340.00	613.1

373.15	690.00	613.7
373.15	1030.00	614.3
373.15	1380.00	614.9
373.15	1720.00	615.5
373.15	2070.00	616.1
373.15	2410.00	616.7
373.15	2760.00	617.3
373.15	3100.00	618.2
373.15	3450.00	618.5
373.15	3800.00	619.0
373.15	4140.00	619.6
373.15	4480.00	620.2
373.15	4830.00	620.7
373.15	5170.00	621.2
373.15	5510.00	621.8
373.15	5860.00	622.3
373.15	6200.00	622.9
373.15	6550.00	623.4
373.15	6890.00	623.9
373.15	7240.00	624.4
373.15	7580.00	625.0
373.15	7930.00	625.5
373.15	8270.00	626.0
373.15	8620.00	626.5
373.15	8960.00	627.0
373.15	9310.00	627.5
373.15	9650.00	628.0
393.15	340.00	593.4
393.15	690.00	594.1
393.15	1030.00	594.9
393.15	1380.00	595.6
393.15	1720.00	596.3
393.15	2070.00	597.0
393.15	2410.00	597.8
393.15	2760.00	598.5
393.15	3100.00	599.2
393.15	3450.00	599.9
393.15	3800.00	600.5
393.15	4140.00	601.2
393.15	4480.00	601.9
393.15	4830.00	602.5
393.15	5170.00	603.2
393.15	5510.00	603.8
393.15	5860.00	604.4

393.15	6200.00	605.1
393.15	6550.00	605.7
393.15	6890.00	606.3
393.15	7240.00	606.9
393.15	7580.00	607.5
393.15	7930.00	608.1
393.15	8270.00	608.7
393.15	8620.00	609.3
393.15	8960.00	609.9
393.15	9310.00	610.8
393.15	9650.00	611.1

Reference *https://www.doi.org/10.1021/je301283e*

Temperature, K	Pressure, kPa	Mass density, kg/m3
283.15	101.00	692.398
283.15	267.60	692.646
283.15	550.80	692.799
283.15	878.60	693.177
283.15	991.30	693.192
283.15	2020.20	694.161
283.15	2914.80	694.997
283.15	4946.50	696.597
283.15	7034.80	698.638
283.15	9021.60	700.052
283.15	9991.90	700.869
283.15	11958.70	702.48
283.15	15011.20	704.783
283.15	18047.40	706.965
283.15	20045.40	708.637
283.15	22056.50	709.841
283.15	25044.10	712.0
283.15	28046.30	714.05
283.15	30051.70	715.435
283.15	32054.80	716.688
283.15	32971.30	717.342
283.15	32999.60	717.432
283.15	34016.50	718.012
283.15	34959.50	718.734
283.15	37943.00	720.455
283.15	40004.00	721.755
283.15	42057.90	723.102
283.15	44939.90	724.839

283.15	48022.40	726.526
283.15	49996.40	727.851
283.15	51981.80	728.904
283.15	54965.00	730.736
283.15	57949.30	732.407
283.15	59996.40	733.467
283.15	62025.40	734.345
283.15	64997.50	735.98
283.16	65971.00	736.499
288.15	102.00	688.224
288.15	391.30	688.682
288.15	554.40	688.232
288.15	882.70	689.214
288.15	989.10	688.618
288.15	2057.50	689.559
288.15	2917.80	690.931
288.15	5041.40	692.738
288.15	7088.80	693.96
288.15	9018.60	695.614
288.15	10039.90	696.278
288.15	12071.60	698.584
288.15	15001.40	700.836
288.15	17968.20	703.23
288.15	20067.60	704.758
288.15	22019.60	705.649
288.15	25001.50	707.645
288.15	28025.70	709.735
288.15	30034.70	711.006
288.15	32084.00	712.959
288.15	33050.00	713.818
288.15	33096.20	713.93
288.15	34035.60	714.067
288.15	35077.00	714.575
288.15	37992.90	716.378
288.15	40040.80	717.608
288.15	42022.80	718.735
288.15	44979.30	720.398
288.15	48045.10	723.18
288.15	50067.60	724.245
288.15	52032.00	724.841
288.15	55076.90	726.211
288.15	58004.00	729.214
288.15	59987.50	729.723
288.15	61973.60	731.101

288.15	64941.60	731.745
288.15	66025.40	732.751
293.15	100.50	683.714
293.16	305.20	684.504
293.16	476.40	684.708
293.15	825.10	684.796
293.16	1045.20	685.167
293.15	1971.70	685.978
293.15	3060.60	686.787
293.15	5011.00	688.859
293.16	7096.80	690.796
293.15	9042.10	692.394
293.15	10035.70	693.252
293.15	11946.50	694.459
293.15	14940.60	697.266
293.16	17888.60	698.789
293.16	19991.60	701.345
293.15	21987.10	701.769
293.16	24983.20	704.2
293.15	27986.00	706.659
293.16	29975.80	708.599
293.16	32232.40	710.098
293.15	33150.80	710.425
293.15	33149.70	710.401
293.15	34098.90	710.557
293.15	34999.60	711.53
293.16	38026.50	712.948
293.15	40081.00	714.898
293.15	42099.20	716.347
293.15	45068.20	718.234
293.16	48021.50	720.258
293.16	50084.50	721.322
293.16	52032.40	722.789
293.15	54965.50	724.479
293.15	58071.90	726.215
293.16	60018.30	727.31
293.16	61962.20	728.261
293.16	64991.00	729.973
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298.16	1012.60	680.891

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298.15	22004.20	699.062
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298.16	28040.20	703.578
298.16	30089.10	704.725
298.16	32033.90	706.093
298.15	33112.80	707.026
298.16	33092.70	706.936
298.15	33924.30	706.971
298.16	35216.60	707.884
298.15	38096.90	709.948
298.15	40161.30	711.975
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298.15	45020.90	715.087
298.15	48106.60	717.001
298.15	50068.10	718.317
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298.15	57930.90	723.027
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298.15	62036.30	725.393
298.15	65017.50	726.954
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308.15	40011.40	704.309
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318.15	57972.30	710.506

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333.15	35075.40	684.235
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343.15	35030.10	677.808

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343.15	50058.90	689.668
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348.15	30148.90	670.002
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348.15	33958.60	673.504
348.15	35044.60	674.428
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348.15	40025.60	678.502
348.16	42065.80	680.23
348.15	45050.60	682.511
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353.15	34945.40	670.985
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353.15	57980.30	689.013
353.15	60098.40	690.731
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353.15	65062.70	694.154
353.16	66024.30	694.802
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358.15	508.40	627.316
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363.15	31961.10	660.63
363.15	33053.30	661.633
363.15	33032.60	661.606
363.15	33999.50	663.017
363.15	35028.30	664.03
363.15	37919.20	666.495
363.15	39916.00	668.059
363.15	42015.50	669.917
363.16	44986.80	672.551
363.15	47947.20	675.063
363.15	50050.30	676.807
363.15	52022.60	678.457
363.15	54940.40	680.815
363.15	57916.50	682.78
363.15	59980.00	684.625
363.15	62042.90	686.168
363.15	64924.10	688.267
363.15	66088.40	689.169

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Sources

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Legend

af:	Acentric Factor
aigt:	Autoignition Temperature
ap:	Aniline Point
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
fll:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hcg:	Heat of Combustion, Gross form
hcn:	Heat of Combustion, Net Form
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hsubt:	Enthalpy of sublimation at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
kvisc:	Kinematic viscosity
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
pc:	Critical Pressure

pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhol:	Liquid Density
sfust:	Entropy of fusion at a given temperature
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tbp:	Boiling point at given pressure
tc:	Critical Temperature
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
volm:	Molar Volume
zc:	Critical Compressibility
zra:	Rackett Parameter