1-Pentanol

Other names:	1-Pentol
	1-Pentyl alcohol
	Alcool amylique
	Amyl alcohol
	Amyl alcohol, n-
	Amyl alcohol, normal
	Amylol
	Butyl carbinol
	N-AMYL ALCOHOL
	N-PENTYL ALCOHOL
	NSC 5707
	Pentan-1-ol
	Pentanol
	Pentanol-1
	Pentasol
	Pentyl alcohol
	Primary amyl alcohol
	Primary-N-amyl alcohol
	UN 1105
	n-Amylalkohol
	n-Butylcarbinol
	n-C5H11OH
	n-Pentan-1-ol
	n-Pentanol
Inchi:	InChI=1S/C5H12O/c1-2-3-4-5-6/h6H,2-5H2,1H3
InchiKey:	AMQJEAYHLZJPGS-UHFFFAOYSA-N
Formula:	C5H12O
SMILES:	CCCCCO
Mol. weight [g/mol]:	88.15
CAS:	71-41-0

Physical Properties

Property code	Value	Unit	Source
af	0.5790		KDB
affp	795.00	kJ/mol	NIST Webbook
aigt	633.15	K	KDB

chl	-3329.96 ± 0.64	kJ/mol	NIST Webbook
chl	-3324.00	kJ/mol	NIST Webbook
chl	-3330.91 ± 0.28	kJ/mol	NIST Webbook
chl	-3324.60 ± 0.40	kJ/mol	NIST Webbook
chl	-3329.90 ± 0.67	kJ/mol	NIST Webbook
cpl	206.67	J/mol×K	THERMODYNAMICS OF MIXTURES CONTAINING AMINES. XIV. CpEm OF BENZYLAMINE WITH HEPTANE AT 293.15 K OR WITH METHANOL, 1-PROPANOL OR 1-PENTANOL AT (293.15-308.15) K
dm	1.70	debye	KDB
fll	1.10	% in Air	KDB
flu	7.50	% in Air	KDB
fpo	298.15	K	KDB
gf	-146.10	kJ/mol	KDB
hf	-300.60 ± 2.00	kJ/mol	NIST Webbook
hf	-301.00 ± 0.50	kJ/mol	NIST Webbook
hf	-295.63 ± 0.74	kJ/mol	NIST Webbook
hf	-294.70 ± 0.30	kJ/mol	NIST Webbook
hf	-294.70	kJ/mol	NIST Webbook
hf	-298.90	kJ/mol	KDB
hf	-295.70 ± 0.70	kJ/mol	NIST Webbook
hf	-301.00	kJ/mol	NIST Webbook
hfl	-357.90 ± 0.50	kJ/mol	NIST Webbook
hfl	-351.62 ± 0.28	kJ/mol	NIST Webbook
hfl	-352.60 ± 0.70	kJ/mol	NIST Webbook
hfl	-358.40 ± 1.70	kJ/mol	NIST Webbook
hfl	-352.57 ± 0.72	kJ/mol	NIST Webbook
hfus	10.51	kJ/mol	Heat Capacities and Derived Thermodynamic Functions of 1-Propanol between 10 K and 350 K and of 1-Pentanol between 85 K and 370 K
hvap	55.40	kJ/mol	NIST Webbook
hvap	57.40	kJ/mol	NIST Webbook
hvap	57.04	kJ/mol	NIST Webbook
hvap	56.94 ± 0.17	kJ/mol	NIST Webbook
hvap	55.40	kJ/mol	NIST Webbook
hvap	55.18	kJ/mol	NIST Webbook
hvap	54.23	kJ/mol	NIST Webbook
hvap	56.90	kJ/mol	NIST Webbook
hvap	56.90 ± 0.20	kJ/mol	NIST Webbook
hvap	57.80	kJ/mol	NIST Webbook
hvap	56.90 ± 0.20	kJ/mol	NIST Webbook

hvap	57.70 ± 1.10	kJ/mol	NIST Webbook
hvap	57.80	kJ/mol	NIST Webbook
hvap	57.70 ± 1.00	kJ/mol	NIST Webbook
ie	10.38	eV	NIST Webbook
ie	10.00	eV	NIST Webbook
ie	10.42 ± 0.03	eV	NIST Webbook
log10ws	-0.60		Aqueous Solubility Prediction Method
log10ws	-0.60		Estimated Solubility Method
logp	1.169		Crippen Method
mcvol	87.180	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=1)		KDB
pc	3909.00	kPa	NIST Webbook
pc	3900.00 ± 20.00	kPa	NIST Webbook
pc	3897.00	kPa	KDB
pc	3909.00	kPa	NIST Webbook
pc	3868.00 ± 20.00	kPa	NIST Webbook
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pc	3920.00 ± 40.00	kPa	NIST Webbook
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ripol	1262.00	NIST Webbook
ripol	1228.00	NIST Webbook
ripol	1216.00	NIST Webbook
ripol	1236.00	NIST Webbook
ripol	1258.00	NIST Webbook
ripol	1255.00	NIST Webbook
ripol	1251.00	NIST Webbook
ripol	1260.00	NIST Webbook
ripol	1258.00	NIST Webbook
ripol	1250.00	NIST Webbook
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ripol	1250.00	NIST Webbook
ripol	1241.00	NIST Webbook
ripol	1245.00	NIST Webbook
ripol	1294.00	NIST Webbook
ripol	1264.00	NIST Webbook
ripol	1233.00	NIST Webbook
ripol	1250.00	NIST Webbook
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ripol	1258.00	NIST Webbook
ripol	1249.00	NIST Webbook
ripol	1250.00	NIST Webbook
ripol	1239.00	NIST Webbook
ripol	1256.00	NIST Webbook
ripol	1250.00	NIST Webbook
ripol	1245.00	NIST Webbook
ripol	1251.00	NIST Webbook
ripol	1238.00	NIST Webbook
ripol	1251.00	NIST Webbook
ripol	1233.00	NIST Webbook
ripol	1274.00	NIST Webbook
ripol	1238.00	NIST Webbook
ripol	1274.00	NIST Webbook
ripol	1274.00	NIST Webbook
ripol	1274.00	NIST Webbook
ripol	1249.00	NIST Webbook
ripol	1239.00	NIST Webbook
ripol	1261.00	NIST Webbook
ripol	1232.00	NIST Webbook
ripol	1262.00	NIST Webbook
ripol	1255.00	NIST Webbook
ripol	1238.00	NIST Webbook
ripol	1220.00	NIST Webbook
ripol	1242.00	NIST Webbook
ripol	1241.00	NIST Webbook

ripol	1255.00		NIST Webbook
ripol	1252.00		NIST Webbook
ripol	1252.00		NIST Webbook
ripol	1255.00		NIST Webbook
ripol	1254.00		NIST Webbook
ripol	1260.00		NIST Webbook
ripol	1252.00		NIST Webbook
ripol	1288.00		NIST Webbook
ripol	1210.00		NIST Webbook
ripol	1241.00		NIST Webbook
ripol	1208.00		NIST Webbook
ripol	1226.00		NIST Webbook
ripol	1222.00		NIST Webbook
ripol	1255.00		NIST Webbook
ripol	1250.00		NIST Webbook
ripol	1218.00		NIST Webbook
ripol	1245.00		NIST Webbook
ripol	1258.00		NIST Webbook
ripol	1244.00		NIST Webbook
ripol	1252.00		NIST Webbook
ripol	1258.00		NIST Webbook
ripol	1245.00		NIST Webbook
ripol	1256.00		NIST Webbook
ripol	1260.00		NIST Webbook
ripol	1257.00		NIST Webbook
ripol	1230.00		NIST Webbook
ripol	1250.00		NIST Webbook
ripol	1242.00		NIST Webbook
ripol	1236.00		NIST Webbook
ripol	1220.00		NIST Webbook
ripol	1214.00		NIST Webbook
ripol	1213.00		NIST Webbook
ripol	1261.00		NIST Webbook
ripol	1271.00		NIST Webbook
ripol	1230.00		NIST Webbook
ripol	1256.00		NIST Webbook
ripol	1255.00		NIST Webbook
ripol	1217.00		NIST Webbook
ripol	1232.00		NIST Webbook
ripol	1237.00		NIST Webbook
sg	401.30	J/mol×K	NIST Webbook
sl	258.90	J/mol×K	NIST Webbook
sl	254.80	J/mol×K	NIST Webbook
tb	411.40 ± 0.10	K	NIST Webbook

tb	409.65 ± 1.00	K	NIST Webbook
tb	402.90 ± 1.00	K	NIST Webbook
tb	411.00 ± 1.00	K	NIST Webbook
tb	404.75 ± 3.00	K	NIST Webbook
tb	410.00 ± 3.00	K	NIST Webbook
tb	404.15 ± 4.00	K	NIST Webbook
tb	404.15 ± 3.00	K	NIST Webbook
tb	404.25 ± 3.00	K	NIST Webbook
tb	411.10 ± 0.10	K	NIST Webbook
tb	411.10 ± 0.20	K	NIST Webbook
tb	411.15 ± 1.00	K	NIST Webbook
tb	410.65 ± 1.00	K	NIST Webbook
tb	411.00 ± 0.50	K	NIST Webbook
tb	411.20 ± 0.20	K	NIST Webbook
tb	409.15 ± 2.00	K	NIST Webbook
tb	410.40 ± 0.30	K	NIST Webbook
tb	411.15 ± 0.07	K	NIST Webbook
tb	410.95 ± 0.50	K	NIST Webbook
tb	411.13	K	KDB
tb	410.95 ± 0.30	K	NIST Webbook
tb	410.95	K	Liquid-liquid equilibrium data for ternary aqueous mixtures containing 1-pentanol and 2-methyl-1-propanol at (298.15, 323.15, and 348.15) K
tb	411.11	K	Isobaric Phase Equilibria of Diethyl Carbonate with Five Alcohols at 101.3 kPa
tb	410.78	K	Vapor-Liquid Equilibria of the Binary System 1-Pentanol + Anisole and the Quaternary System Benzene+Cyclohexane+1-Pentanol+Anisc at 101.32 kPa
tb	410.85	K	Vapor-Liquid Equilibria at 101.3 kPa for Binary Mixtures Containing 2-Methyl-1-propanol + 2-Methyl-1-butanol, 2-Methyl-1-propanol + 3-Methyl-1-butanol, and 2-Methyl-1-propanol + 1-Pentanol
tb	411.10	K	Isobaric Vapor-Liquid Equilibria of Heptane + 1-Butanol and Heptane + 1-Pentanol Systems at (53.3 and 91.3) kPa
tb	684.20 ± 0.40	K	NIST Webbook
tb	410.90 ± 0.30	K	NIST Webbook
tb	410.20	K	NIST Webbook

tb	410.15 ± 0.40	K	NIST Webbook
tb	411.20	K	NIST Webbook
tb	392.40	K	NIST Webbook
tb	411.00 ± 0.30	K	NIST Webbook
tb	411.10 ± 0.08	K	NIST Webbook
tb	411.00 ± 0.50	K	NIST Webbook
tb	273.28 ± 0.10	K	NIST Webbook
tb	410.80 ± 0.40	K	NIST Webbook
tb	411.20 ± 0.50	K	NIST Webbook
tb	411.20 ± 0.40	K	NIST Webbook
tb	411.15	K	NIST Webbook
tb	409.15 ± 3.00	K	NIST Webbook
tb	411.65 ± 0.50	K	NIST Webbook
tb	410.65 ± 3.00	K	NIST Webbook
tb	410.65 ± 0.50	K	NIST Webbook
tb	411.15 ± 0.50	K	NIST Webbook
tb	411.00 ± 0.50	K	NIST Webbook
tb	410.15 ± 0.70	K	NIST Webbook
tb	408.65 ± 2.00	K	NIST Webbook
tb	411.07 ± 0.20	K	NIST Webbook
tb	408.90 ± 1.50	K	NIST Webbook
tb	406.65 ± 3.00	K	NIST Webbook
tb	410.65 ± 0.50	K	NIST Webbook
tb	411.15 ± 0.50	K	NIST Webbook
tb	411.35 ± 0.50	K	NIST Webbook
tb	411.05 ± 1.00	K	NIST Webbook
tb	411.15 ± 0.50	K	NIST Webbook
tb	410.15 ± 1.00	K	NIST Webbook
tb	410.15 ± 1.00	K	NIST Webbook
tb	411.40 ± 0.50	K	NIST Webbook
tb	411.35 ± 0.50	K	NIST Webbook
tb	411.15 ± 0.50	K	NIST Webbook
tb	409.15 ± 3.00	K	NIST Webbook
tb	410.90 ± 0.50	K	NIST Webbook
tb	411.15 ± 1.00	K	NIST Webbook
tb	410.95 ± 0.50	K	NIST Webbook
tb	411.10 ± 0.50	K	NIST Webbook
tb	407.15 ± 3.00	K	NIST Webbook
tb	411.21 ± 0.05	K	NIST Webbook
tb	410.80 ± 0.20	K	NIST Webbook
tb	411.10 ± 0.10	K	NIST Webbook
tb	409.85 ± 0.50	K	NIST Webbook
tb	410.95 ± 0.30	K	NIST Webbook

tb	411.15	K	Excess molar volumes of ternary mixtures of 1,3-dichlorobenzene and methyl ethyl ketone with 1-alkanols at 303.15K
tb	402.20 ± 0.50	K	NIST Webbook
tc	588.10 ± 0.50	K	NIST Webbook
tc	588.20 ± 0.50	K	NIST Webbook
tc	551.60	K	NIST Webbook
tc	588.20	K	NIST Webbook
tc	587.70 ± 0.20	K	NIST Webbook
tc	588.00	K	NIST Webbook
tc	588.50 ± 0.60	K	NIST Webbook
tc	588.11	K	NIST Webbook
tc	588.00 ± 0.40	K	NIST Webbook
tc	588.50 ± 0.60	K	NIST Webbook
tc	588.10	K	KDB
tf	194.65 ± 0.50	K	NIST Webbook
tf	194.20	K	KDB
tf	194.68	K	Aqueous Solubility Prediction Method
tf	194.95	K	NIST Webbook
tf	194.35 ± 0.30	K	NIST Webbook
tf	194.65 ± 0.50	K	NIST Webbook
tt	194.20 ± 0.20	K	NIST Webbook
tt	195.56	K	KDB
tt	195.56 ± 0.02	K	NIST Webbook
vc	0.326	m3/kmol	NIST Webbook
vc	0.326	m3/kmol	KDB
zc	0.2598130		KDB
zra	0.26		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	167.91	J/mol×K	403.49	NIST Webbook
cpg	177.70 ± 1.40	J/mol×K	418.95	NIST Webbook
cpg	178.20 ± 1.40	J/mol×K	420.75	NIST Webbook
cpg	174.58	J/mol×K	423.32	NIST Webbook
cpg	179.70 ± 1.40	J/mol×K	426.15	NIST Webbook
cpg	181.70 ± 1.40	J/mol×K	433.45	NIST Webbook
cpg	179.33	J/mol×K	438.26	NIST Webbook
cpg	184.40 ± 1.40	J/mol×K	442.85	NIST Webbook

cpg	184.80 ± 1.40	J/mol×K	444.35	NIST Webbook
cpg	184.35	J/mol×K	453.45	NIST Webbook
cpg	192.90 ± 1.40	J/mol×K	472.85	NIST Webbook
cpg	190.44	J/mol×K	473.19	NIST Webbook
cpg	195.50 ± 1.40	J/mol×K	482.25	NIST Webbook
cpg	209.30 ± 1.40	J/mol×K	531.25	NIST Webbook
cpg	215.80 ± 1.40	J/mol×K	554.15	NIST Webbook
cpg	221.40 ± 1.40	J/mol×K	573.95	NIST Webbook
cpl	207.45	J/mol×K	298.15	NIST Webbook
cpl	205.60	J/mol×K	293.15	NIST Webbook
cpl	212.30	J/mol×K	301.26	NIST Webbook
cpl	208.40	J/mol×K	298.15	NIST Webbook
cpl	208.30	J/mol×K	298.15	NIST Webbook
cpl	201.70	J/mol×K	302.40	NIST Webbook
cpl	209.12	J/mol×K	298.00	NIST Webbook
cpl	183.30	J/mol×K	298.00	NIST Webbook
cpl	208.19	J/mol×K	298.15	NIST Webbook
cpl	208.98	J/mol×K	298.15	NIST Webbook
cpl	240.60	J/mol×K	313.20	NIST Webbook
cpl	207.45	J/mol×K	298.15	NIST Webbook
cpl	207.40	J/mol×K	298.15	NIST Webbook
dvisc	0.0023320	Pa×s	313.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0018220	Pa×s	323.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method

dvisc	0.0014400	Pa×s	333.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0011460	Pa×s	343.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0009310	Pa×s	353.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0030600	Pa×s	303.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0046820	Pa×s	288.15	Densities and Viscosities of Four Binary Diethyl Carbonate + 1-Alcohol Systems from (288.15 to 313.15) K

dvisc	0.0035560	Pa×s	298.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method	
dvisc	0.0034970	Pa×s	298.15	Densities and Viscosities of Four Binary Diethyl Carbonate + 1-Alcohol Systems from (288.15 to 313.15) K	
dvisc	0.0041170	Pa×s	293.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method	
dvisc	0.0023120	Pa×s	313.15	Densities and Viscosities of Four Binary Diethyl Carbonate + 1-Alcohol Systems from (288.15 to 313.15) K	
dvisc	0.0054170	Pa×s	283.15	Density and Viscosity of the Binary Systems Ethanol + Butan-1-ol, + Pentan-1-ol, + Heptan-1-ol, + Octan-1-ol, Nonan-1-ol, + Decan-1-ol at 0.1 MPa and Temperatures from 283.15 K to 313.15 K	

dvisc	0.0039740	Pa×s	293.15	Density and Viscosity of the Binary Systems Ethanol + Butan-1-ol, + Pentan-1-ol, + Heptan-1-ol, + Octan-1-ol, Nonan-1-ol, + Decan-1-ol at 0.1 MPa and Temperatures from 283.15 K to 313.15 K
dvisc	0.0034410	Pa×s	298.15	Density and Viscosity of the Binary Systems Ethanol + Butan-1-ol, + Pentan-1-ol, + Heptan-1-ol, + Octan-1-ol, Nonan-1-ol, + Decan-1-ol at 0.1 MPa and Temperatures from 283.15 K to 313.15 K
dvisc	0.0029900	Pa×s	303.15	Density and Viscosity of the Binary Systems Ethanol + Butan-1-ol, + Pentan-1-ol, + Heptan-1-ol, + Octan-1-ol, Nonan-1-ol, + Decan-1-ol at 0.1 MPa and Temperatures from 283.15 K to 313.15 K
dvisc	0.0022630	Pa×s	313.15	Density and Viscosity of the Binary Systems Ethanol + Butan-1-ol, + Pentan-1-ol, + Heptan-1-ol, + Octan-1-ol, Nonan-1-ol, + Decan-1-ol at 0.1 MPa and Temperatures from 283.15 K to 313.15 K

dvisc	0.0034580	Pa×s	298.15	Densities and Viscosities of Binary Mixtures of 2,2,4-Trimethylpentane + 1-Propanol, + 1-Pentanol, + 1-Hexanol, and + 1-Heptanol from (298.15 to 323.15) K
dvisc	0.0030070	Pa×s	303.15	Densities and Viscosities of Binary Mixtures of 2,2,4-Trimethylpentane + 1-Propanol, + 1-Pentanol, + 1-Hexanol, and + 1-Heptanol from (298.15 to 323.15) K
dvisc	0.0026250	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of 2,2,4-Trimethylpentane + 1-Propanol, + 1-Pentanol, + 1-Hexanol, and + 1-Heptanol from (298.15 to 323.15) K
dvisc	0.0023170	Pa×s	313.15	Densities and Viscosities of Binary Mixtures of 2,2,4-Trimethylpentane + 1-Propanol, + 1-Pentanol, + 1-Hexanol, and + 1-Heptanol from (298.15 to 323.15) K
dvisc	0.0020290	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of 2,2,4-Trimethylpentane + 1-Propanol, + 1-Pentanol, + 1-Hexanol, and + 1-Heptanol from (298.15 to 323.15) K
dvisc	0.0030220	Pa×s	303.15	Densities and Viscosities of Four Binary Diethyl Carbonate + 1-Alcohol Systems from (288.15 to 313.15) K

dvisc	0.0040290	Pa×s	293.15	Densities and Kinematic Viscosities of Ten Binary 1-Alkanol Liquid Systems at Temperatures of (293.15 and 298.15) K
dvisc	0.0034940	Pa×s	298.15	Densities and Kinematic Viscosities of Ten Binary 1-Alkanol Liquid Systems at Temperatures of (293.15 and 298.15) K
dvisc	0.0040601	Pa×s	293.15	Densities and Viscosities of exo-Tetrahydrodicyclopentadiene + n-Butanol and exo-Tetrahydrodicyclopentadiene + n-Pentanol at Temperatures of (293.15 to 313.15) K
dvisc	0.0006470	Pa×s	373.15	Density, viscosity, vapour liquid equilibrium, excess molar enthalpy, and their correlations of the binary system [1-pentanol + R-(+)-limonene] over the complete concentration range, at different temperatures
dvisc	0.0030582	Pa×s	303.15	Densities and Viscosities of exo-Tetrahydrodicyclopentadiene + n-Butanol and exo-Tetrahydrodicyclopentadiene + n-Pentanol at Temperatures of (293.15 to 313.15) K
dvisc	0.0022995	Pa×s	313.15	Densities and Viscosities of exo-Tetrahydrodicyclopentadiene + n-Butanol and exo-Tetrahydrodicyclopentadiene + n-Pentanol at Temperatures of (293.15 to 313.15) K

dvisc	0.0007720	Pa×s	363.15	Density, viscosity, vapour liquid equilibrium, excess molar enthalpy, and their correlations of the binary system [1-pentanol + R-(+)-limonene] over the complete concentration range, at different temperatures	
dvisc	0.0009350	Pa×s	353.15	Density, viscosity, vapour liquid equilibrium, excess molar enthalpy, and their correlations of the binary system [1-pentanol + R-(+)-limonene] over the complete concentration range, at different temperatures	
dvisc	0.0011460	Pa×s	343.15	Density, viscosity, vapour liquid equilibrium, excess molar enthalpy, and their correlations of the binary system [1-pentanol + R-(+)-limonene] over the complete concentration range, at different temperatures	
dvisc	0.0014250	Pa×s	333.15	Density, viscosity, vapour liquid equilibrium, excess molar enthalpy, and their correlations of the binary system [1-pentanol + R-(+)-limonene] over the complete concentration range, at different temperatures	

dvisc	0.0018010	Pa×s	323.15	Density, viscosity, vapour liquid equilibrium, excess molar enthalpy, and their correlations of the binary system [1-pentanol + R-(+)-limonene] over the complete concentration range, at different temperatures
dvisc	0.0017950	Pa×s	323.15	Densities and Viscosities of Binary Mixtures of 2,2,4-Trimethylpentane + 1-Propanol, + 1-Pentanol, + 1-Hexanol, and + 1-Heptanol from (298.15 to 323.15) K
dvisc	0.0023150	Pa×s	313.15	Density, viscosity, vapour liquid equilibrium, excess molar enthalpy, and their correlations of the binary system [1-pentanol + R-(+)-limonene] over the complete concentration range, at different temperatures
dvisc	0.0030200	Pa×s	303.15	Density, viscosity, vapour liquid equilibrium, excess molar enthalpy, and their correlations of the binary system [1-pentanol + R-(+)-limonene] over the complete concentration range, at different temperatures

dvisc	0.0034800	Pa×s	298.15	Density, viscosity, vapour liquid equilibrium, excess molar enthalpy, and their correlations of the binary system [1-pentanol + R-(+)-limonene] over the complete concentration range, at different temperatures
dvisc	0.0040300	Pa×s	293.15	Density, viscosity, vapour liquid equilibrium, excess molar enthalpy, and their correlations of the binary system [1-pentanol + R-(+)-limonene] over the complete concentration range, at different temperatures
dvisc	0.0007670	Pa×s	363.15	Density and Viscosity of Binary Mixtures of Diethyl Carbonate with Alcohols at (293.15 to 363.15) K and Predictive Results by UNIFAC-VISCO Group Contribution Method
dvisc	0.0035344	Pa×s	298.15	Densities and Viscosities of exo-Tetrahydrodicyclopentadiene + n-Butanol and exo-Tetrahydrodicyclopentadiene + n-Pentanol at Temperatures of (293.15 to 313.15) K
dvisc	0.0040250	Pa×s	293.15	Densities and Viscosities of Four Binary Diethyl Carbonate + 1-Alcohol Systems from (288.15 to 313.15) K
hfust	10.50	kJ/mol	195.60	NIST Webbook
hfust	10.50	kJ/mol	195.56	NIST Webbook

hfust	10.51	kJ/mol	195.60	NIST Webbook
hfust	10.50	kJ/mol	195.60	NIST Webbook
hfust	9.83	kJ/mol	194.20	NIST Webbook
hvapt	31.70	kJ/mol	498.00	NIST Webbook
hvapt	51.60	kJ/mol	388.00	NIST Webbook
hvapt	54.30	kJ/mol	368.50	NIST Webbook
hvapt	47.20	kJ/mol	404.00	NIST Webbook
hvapt	51.50	kJ/mol	372.50	NIST Webbook
hvapt	7.10	kJ/mol	586.00	NIST Webbook
hvapt	14.10	kJ/mol	573.00	NIST Webbook
hvapt	22.00	kJ/mol	548.00	NIST Webbook
hvapt	26.40	kJ/mol	523.00	NIST Webbook
hvapt	44.40	kJ/mol	411.00	NIST Webbook
hvapt	36.10	kJ/mol	473.00	NIST Webbook
hvapt	40.10	kJ/mol	448.00	NIST Webbook
hvapt	47.00 ± 0.10	kJ/mol	392.00	NIST Webbook
hvapt	41.40	kJ/mol	392.40	NIST Webbook
hvapt	44.36	kJ/mol	411.20	NIST Webbook
hvapt	44.35	kJ/mol	410.90	KDB
hvapt	54.40 ± 0.20	kJ/mol	328.00	NIST Webbook
hvapt	53.00 ± 0.20	kJ/mol	343.00	NIST Webbook
hvapt	44.40 ± 0.10	kJ/mol	411.00	NIST Webbook
hvapt	51.20 ± 0.20	kJ/mol	358.00	NIST Webbook
hvapt	55.00	kJ/mol	360.50	NIST Webbook
hvapt	56.20	kJ/mol	359.00	NIST Webbook
hvapt	50.50 ± 0.10	kJ/mol	362.00	NIST Webbook
hvapt	45.40	kJ/mol	424.50	NIST Webbook
hvapt	49.20 ± 0.10	kJ/mol	374.00	NIST Webbook
hvapt	55.70 ± 0.20	kJ/mol	313.00	NIST Webbook
kvisc	0.0000044	m2/s	295.15	Densities, Viscosities, and Speeds of Sound of the Nitromethane + 1-Pentanol System near the Critical Demixing Temperature: Effect of Deuterium Substitution

kvisc	0.0000037	m2/s	303.15	Densities, Viscosities, and Ultrasonic Velocity Studies of Binary Mixtures of Chloroform with Pentan-1-ol, Hexan-1-ol, and Heptan-1-ol at (303.15 and 313.15) K	
kvisc	0.0000031	m2/s	308.15	Densities, Viscosities, and Speeds of Sound of the Nitromethane + 1-Pentanol System near the Critical Demixing Temperature: Effect of Deuterium Substitution	
kvisc	0.0000035	m2/s	305.15	Densities, Viscosities, and Speeds of Sound of the Nitromethane + 1-Pentanol System near the Critical Demixing Temperature: Effect of Deuterium Substitution	
kvisc	0.0000036	m2/s	303.15	Densities, Viscosities, and Speeds of Sound of the Nitromethane + 1-Pentanol System near the Critical Demixing Temperature: Effect of Deuterium Substitution	
kvisc	0.0000039	m2/s	300.15	Densities, Viscosities, and Speeds of Sound of the Nitromethane + 1-Pentanol System near the Critical Demixing Temperature: Effect of Deuterium Substitution	

kvisc	0.0000042	m2/s	298.15	Densities, Viscosities, and Speeds of Sound of the Nitromethane + 1-Pentanol System near the Critical Demixing Temperature: Effect of Deuterium Substitution	
kvisc	0.0000050	m2/s	293.15	Densities, Viscosities, and Speeds of Sound of the Nitromethane + 1-Pentanol System near the Critical Demixing Temperature: Effect of Deuterium Substitution	
kvisc	0.0000029	m2/s	313.15	Densities, Viscosities, and Ultrasonic Velocity Studies of Binary Mixtures of Chloroform with Pentan-1-ol, Hexan-1-ol, and Heptan-1-ol at (303.15 and 313.15) K	
pvap	113.30	kPa	414.65	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa	
pvap	2.53	kPa	328.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols	
pvap	1.87	kPa	323.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols	
pvap	1.36	kPa	318.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols	
pvap	0.97	kPa	313.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols	

pvap	0.69	kPa	308.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	0.49	kPa	303.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	0.34	kPa	298.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	40.00	kPa	384.45	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems
pvap	40.01	kPa	384.85	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems
pvap	54.41	kPa	392.76	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems
pvap	66.15	kPa	398.11	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems

pvap	72.93	kPa	400.95	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems
pvap	82.75	kPa	404.59	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems
pvap	90.21	kPa	407.17	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems
pvap	101.20	kPa	410.73	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems
pvap	3.38	kPa	333.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	101.90	kPa	411.35	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	94.50	kPa	409.00	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa

pvap	81.30	kPa	404.60	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	37.36	kPa	383.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	56.90	kPa	394.70	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	45.45	kPa	388.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	54.88	kPa	393.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	65.84	kPa	398.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	78.45	kPa	403.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	4.47	kPa	338.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	5.87	kPa	343.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	0.90	kPa	313.15	Vapour-liquid equilibria of the ternary mixture (1-pentanol + 2,2,4-trimethylpentane + heptane) and the binary mixture (2,2,4-trimethylpentane + heptane) at T = 313.15 K for the characterization of second generation biofuels.

pvap	7.63	kPa	348.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	9.83	kPa	353.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	12.52	kPa	358.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	15.81	kPa	363.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	19.86	kPa	368.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	24.68	kPa	373.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	49.20	kPa	390.75	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	40.00	kPa	385.65	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	35.30	kPa	382.40	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa
pvap	31.30	kPa	379.35	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa

pvap	0.91	kPa	313.15	Characterizing second generation biofuels: Excess enthalpies and vapour-liquid equilibria of the binary mixtures containing 1-pentanol or 2-pentanol and n-hexane	
pvap	30.47	kPa	378.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols	
pvap	69.30	kPa	400.05	Isobaric (vapour + liquid) equilibria for the (1-pentanol + propionic acid) binary mixture at (53.3 and 91.3) kPa	
rfi	1.40970		293.20	Vapor Liquid Equilibrium Data for Binary Systems of 1-Methyl-4-(1-methylethenyl)-cyclohexene + {Ethanol, Propan-1-ol, Propan-2-ol, Butan-1-ol, Pentan-1-ol, or Hexan-1-ol} at 40 kPa	
rfi	1.40995		293.15	Excess molar volumes and viscosities of (1,1,2,2-tetrabromoethane + 1-alkanols) at T = (293.15 and 303.15) K	
rfi	1.40780		298.15	Excess molar volumes and partial molar volumes for (propionitrile + an alkanol) at T = 298.15 K and p = 0.1 MPa	
rfi	1.40976		293.15	Densities, excess molar volumes, and refractive indices of 1,1,2,2-tetrachloroethane and 1-alkanols binary mixtures	

rfi	1.40592	303.15	Densities, excess molar volumes, and refractive indices of 1,1,2,2-tetrachloroethane and 1-alkanols binary mixtures
rfi	1.40730	298.15	Thermodynamic properties of (tetradecane + benzene, + toluene, + chlorobenzene, + bromobenzene, + anisole) binary mixtures at T = (298.15, 303.15, and 308.15) K
rfi	1.40500	303.15	Thermodynamic properties of (tetradecane + benzene, + toluene, + chlorobenzene, + bromobenzene, + anisole) binary mixtures at T = (298.15, 303.15, and 308.15) K
rfi	1.40320	308.15	Thermodynamic properties of (tetradecane + benzene, + toluene, + chlorobenzene, + bromobenzene, + anisole) binary mixtures at T = (298.15, 303.15, and 308.15) K
rfi	1.40995	293.15	Densities, excess molar volumes, and refractive indices of 1,1,2,2-tetrabromoethane and 1-alkanols binary mixtures
rfi	1.40592	303.15	Densities, excess molar volumes, and refractive indices of 1,1,2,2-tetrabromoethane and 1-alkanols binary mixtures

rfi	1.40730	298.15	Thermodynamic interactions in binary mixtures of anisole with ethanol, propan-1-ol, propan-2-ol, butan-1-ol, pentan-1-ol, and 3-methylbutan-1-ol at T = (298.15, 303.15, and 308.15) K
rfi	1.40500	303.15	Thermodynamic interactions in binary mixtures of anisole with ethanol, propan-1-ol, propan-2-ol, butan-1-ol, pentan-1-ol, and 3-methylbutan-1-ol at T = (298.15, 303.15, and 308.15) K
rfi	1.40320	308.15	Thermodynamic interactions in binary mixtures of anisole with ethanol, propan-1-ol, propan-2-ol, butan-1-ol, pentan-1-ol, and 3-methylbutan-1-ol at T = (298.15, 303.15, and 308.15) K
rfi	1.40941	298.15	Atmospheric densities and interfacial tensions for 1-alkanol (1-butanol to 1-octanol) + water and ether (MTBE, ETBE, DIPE, TAME and THP) + water demixed mixtures.
rfi	1.40030	318.15	Mixing thermodynamic properties of 1-butyl-4-methylpyridinium tetrafluoroborate [b4mpy][BF4] with water and with an alkan-1ol (methanol to pentanol)

rfi	1.40784	298.15	Thermophysical properties of the binary mixtures (1,8-cineole + 1-alkanol) at T = (298.15 and 313.15) K and at atmospheric pressure
rfi	1.40178	313.15	Thermophysical properties of the binary mixtures (1,8-cineole + 1-alkanol) at T = (298.15 and 313.15) K and at atmospheric pressure
rfi	1.40850	298.15	Comparative study of physico-chemical properties of binary mixtures of N,N-dimethylformamide with 1-alkanols at different temperatures
rfi	1.40690	303.15	Comparative study of physico-chemical properties of binary mixtures of N,N-dimethylformamide with 1-alkanols at different temperatures
rfi	1.40590	308.15	Comparative study of physico-chemical properties of binary mixtures of N,N-dimethylformamide with 1-alkanols at different temperatures
rfi	1.40390	313.15	Comparative study of physico-chemical properties of binary mixtures of N,N-dimethylformamide with 1-alkanols at different temperatures

rfi	1.40900	293.10	Viscosity and surface tension of binary systems of N,N-dimethylformamide with alkan-1-ols at different temperatures
rfi	1.40730	298.20	Tie line data for the (water + butyric acid + n-butyl alcohol or amyl alcohol) at T = (298.2, 308.2, and 318.2) K and (water + butyric acid + isoamyl alcohol) at T = 298.2 K
rfi	1.40774	298.15	Effect of the temperature on the physical properties of the pure ionic liquid 1-ethyl-3-methylimidazolium methylsulfate and characterization of its binary mixtures with alcohols
rfi	1.40980	293.15	Experimental solubility for betulin and estrone in various solvents within the temperature range T = (293.2 to 328.2) K
rfi	1.40710	298.15	Liquid-liquid equilibrium for (water + 5-hydroxymethylfurfural + 1-pentanol/1-hexanol/1-heptanol) systems at 298.15 K
rfi	1.40980	293.15	ERAS modeling of the excess molar enthalpies of binary liquid mixtures of 1-pentanol and 1-hexanol with acetonitrile at atmospheric pressure and 288, 298, 313 and 323K

rfi	1.41192	288.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.40994	293.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.40796	298.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.40595	303.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.40388	308.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K

rfi	1.40189	313.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.39987	318.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.39776	323.15	Experimental Determination and Modeling of Densities and Refractive Indices of the Binary Systems Alcohol + Dicyclohexylamine at T = (288.15 to 323.15) K
rfi	1.41000	293.15	Isothermal Vapor-Liquid Equilibrium Measurements of Butan-2-one + 2-Methyl-propan-1-ol/Pentan-1-ol
rfi	1.40764	298.20	Vapor-Liquid Equilibrium Measurements of Ether Alcohol Blends for Investigation on Reformulated Gas
rfi	1.40770	298.15	Density, Refractive Index, and Speed of Sound at 298.15 K and Vapor-Liquid Equilibria at 101.3 kPa for Binary Mixtures of Ethyl Acetate + 1-Pentanol and Ethanol + 2-Methyl-1-propanol

rfi	1.40800	298.15	Density, Surface Tension, and Refractive Index of Octane + 1-Alkanol Mixtures at T) 298.15 K.
rfi	1.41040	293.00	Quaternary Liquid-Liquid Equilibrium of Water + Acetic Acid + Propionic Acid + Solvent (Amyl Alcohol, Cyclohexyl Acetate, or Toluene) Systems
rfi	1.40980	293.15	Isobaric Vapor-Liquid Equilibria of the Ternary System Methylbutyl Ketone + 1-Pentanol + Nonane
rfi	1.40770	298.15	Liquid-Liquid Equilibrium Diagrams of Ethanol + Water + (Ethyl Acetate or 1-Pentanol) at Several Temperatures
rfi	1.40890	298.15	Excess Molar Enthalpies of 1,2-Propanediol + Alkan-1-ols (C1-C6) and Their Correlations at 298.15 K and Ambient Pressure (81.5 kPa)
rfi	1.40980	293.15	Isobaric Vapor-Liquid Equilibria of the Ternary System Dibutyl Ether + 1-Pentanol + Nonane
rfi	1.40780	298.15	Effect of Pressure on the Static Relative Permittivities of Alkan-1-ols at 298.15 K

rfi	1.40880	298.15	Excess Molar Enthalpies of Benzyl Alcohol + Alkanols (C1-C6) and Their Correlations at 298.15 K and Ambient Pressure
rfi	1.40860	298.15	Excess Molar Enthalpies of 2-Methyl-2-butanol (1) + 1-Alkanols (C1-C5) (2) at 298.15 K
rfi	1.40980	293.13	Isobaric Vapor-Liquid Equilibria of the Ternary System Pentan-1-ol + Pentyl Acetate + Nonane
rfi	1.40770	298.15	Isobaric Vapor Liquid Equilibrium of 3-Methyl-1-butanol + Ethyl Lactate and 1-Pentanol + Ethyl Lactate at (13.0 and 101.3) kPa
rfi	1.40703	298.15	Liquid Liquid Phase Equilibria of 1-Propanol + Water + n-Alcohol Ternary Systems at 298.15 K and Atmospheric Pressure
rfi	1.40850	298.15	Bubble temperature measurements on seven binary mixtures formed by ethylbenzene at 94.7 kPa
rfi	1.40970	293.20	Vapor Liquid Equilibrium Data for Binary Systems of 1H-Pyrrole with Butan-1-ol, Propan-1-ol, or Pentan-1-ol
rfi	1.40797	298.15	Experimental Liquid-Liquid Equilibria of 1-Alkyl-3-methylimidazolium Hexafluorophosphate with 1-Alcohols

rfi	1.40980	293.15	Isobaric Vapor Liquid Equilibria of the Ternary System 1-Pentanol + Nonane Anisole
rfi	1.40920	293.15	Measurement and Correlation of the Solubilities of m-Phthalic Acid in Monobasic Alcohols
rfi	1.40980	293.13	Isobaric Vapor-Liquid Equilibria of the Ternary System Methylbutyl Ketone + 1-Pentanol + Anisole
rfi	1.40770	298.15	Isobaric Vapor-Liquid Equilibrium for Binary Mixtures of 3-Methyl-1-butanol + 3-Methyl-1-butyl Ethanoate and 1-Pentanol + Pentyl Ethanoate at 101.3 kPa
rfi	1.40680	298.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of Methyl Ethyl Ketone + Pentanol Isomers at Different Temperatures
rfi	1.40310	308.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of Methyl Ethyl Ketone + Pentanol Isomers at Different Temperatures
rfi	1.39960	318.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of Methyl Ethyl Ketone + Pentanol Isomers at Different Temperatures

rfi	1.41000		293.20	Liquid-liquid equilibrium data for systems containing of formic acid, water, and primary normal alcohols at T = 298.2 K
rfi	1.40970		298.15	Investigation on vapor liquid equilibrium for 2-propanol + 1-butanol + 1-pentanol at 101.3 kPa
rfi	1.40780		298.15	Excess molar volumes, excess molar enthalpies and refractive index deviations for binary mixtures of propan-1-ol, butan-1-ol and pentan-1-ol with 2,2,4-trimethylpentane at 298.15 K
rfi	1.40800		298.15	Vapor liquid equilibria in the ternary system dipropyl ether + 1-propanol + 1-pentanol and the binary systems dipropyl ether + 1-pentanol, 1-propanol + 1-pentanol at 101.3 kPa
rfi	1.40780		298.15	Mixing thermodynamic properties of 1-butyl-4-methylpyridinium tetrafluoroborate [b4mpy][BF4] with water and with an alkan-1ol (methanol to pentanol)
rhol	810.80	kg/m3	298.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory

rhol	811.10	kg/m3	298.15	Surface Properties of Binary Mixtures of Ethylene Glycol with a Series of Aliphatic Alcohols (1-Pentanol, 1-Hexanol, and 1-Heptanol)
rhol	810.83	kg/m3	298.15	Densities and Excess Molar Volumes of N-Methylmorpholine + 1-Alkanol Systems at 298.15 K
rhol	810.12	kg/m3	298.15	Isobaric Vapor Liquid Equilibria of Binary Systems (Propyl Acetate + n-Pentanol), (Propyl Acetate + 1-Methyl-1-butanol), and (Propyl Acetate + 3-Methyl-1-butanol) at 101.3 kPa
rhol	792.23	kg/m3	323.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure
rhol	796.03	kg/m3	318.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure

rhol	799.79	kg/m3	313.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure	
rhol	803.53	kg/m3	308.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure	
rhol	807.24	kg/m3	303.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure	
rhol	810.93	kg/m3	298.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure	
rhol	814.59	kg/m3	293.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure	

rhol	799.90	kg/m3	313.15	Densities and Viscosities of Three Binary Monoglyme + 1-Alcohol Systems from (283.15 to 313.15) K	
rhol	807.25	kg/m3	303.15	Densities and Viscosities of Three Binary Monoglyme + 1-Alcohol Systems from (283.15 to 313.15) K	
rhol	810.93	kg/m3	298.15	Densities and Viscosities of Three Binary Monoglyme + 1-Alcohol Systems from (283.15 to 313.15) K	
rhol	814.60	kg/m3	293.15	Densities and Viscosities of Three Binary Monoglyme + 1-Alcohol Systems from (283.15 to 313.15) K	
rhol	821.95	kg/m3	283.15	Densities and Viscosities of Three Binary Monoglyme + 1-Alcohol Systems from (283.15 to 313.15) K	
rhol	788.74	kg/m3	328.15	Excess Molar Volumes of 1,3-Diethyl Propanedioate with Methanol, Ethanol, Propan-1-ol, Propan-2-ol, Butan-2-ol, 2-Methyl-propan-1-ol, and Pentan-1-ol at T = (288.15, 298.15, 313.15, and 328.15) K	

rhol	800.26	kg/m3	313.15	Excess Molar Volumes of 1,3-Diethyl Propanedioate with Methanol, Ethanol, Propan-1-ol, Propan-2-ol, Butan-2-ol, 2-Methyl-propan-1-ol, and Pentan-1-ol at T = (288.15, 298.15, 313.15, and 328.15) K
rhol	811.47	kg/m3	298.15	Excess Molar Volumes of 1,3-Diethyl Propanedioate with Methanol, Ethanol, Propan-1-ol, Propan-2-ol, Butan-2-ol, 2-Methyl-propan-1-ol, and Pentan-1-ol at T = (288.15, 298.15, 313.15, and 328.15) K
rhol	818.80	kg/m3	288.15	Excess Molar Volumes of 1,3-Diethyl Propanedioate with Methanol, Ethanol, Propan-1-ol, Propan-2-ol, Butan-2-ol, 2-Methyl-propan-1-ol, and Pentan-1-ol at T = (288.15, 298.15, 313.15, and 328.15) K
rhol	807.30	kg/m3	303.00	Fluid-Phase Behavior of {1-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl) Imide, [C6mim][NTf2], + C2-C8 n-Alcohol} Mixtures: Liquid-Liquid Equilibrium and Excess Volumes
rhol	810.90	kg/m3	298.00	Fluid-Phase Behavior of {1-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl) Imide, [C6mim][NTf2], + C2-C8 n-Alcohol} Mixtures: Liquid-Liquid Equilibrium and Excess Volumes

rhol	814.60	kg/m3	293.00	Fluid-Phase Behavior of {1-Hexyl-3-methylimidazolium Bis(trifluoromethylsulfonyl) Imide, [C6mim][NTf2], + C2-C8 n-Alcohol} Mixtures: Liquid-Liquid Equilibrium and Excess Volumes	
rhol	810.90	kg/m3	298.15	Dynamic Viscosities of Diethyl Carbonate with Linear and Secondary Alcohols at Several Temperatures	
rhol	788.61	kg/m3	328.15	Densities and Viscosities for Binary Liquid Mixtures of Pentanol Isomers from (288.15 to 328.15) K at 0.1 MPa	
rhol	792.48	kg/m3	323.15	Densities and Viscosities for Binary Liquid Mixtures of Pentanol Isomers from (288.15 to 328.15) K at 0.1 MPa	
rhol	796.32	kg/m3	318.15	Densities and Viscosities for Binary Liquid Mixtures of Pentanol Isomers from (288.15 to 328.15) K at 0.1 MPa	
rhol	800.11	kg/m3	313.15	Densities and Viscosities for Binary Liquid Mixtures of Pentanol Isomers from (288.15 to 328.15) K at 0.1 MPa	
rhol	803.86	kg/m3	308.15	Densities and Viscosities for Binary Liquid Mixtures of Pentanol Isomers from (288.15 to 328.15) K at 0.1 MPa	

rhol	807.57	kg/m3	303.15	Densities and Viscosities for Binary Liquid Mixtures of Pentanol Isomers from (288.15 to 328.15) K at 0.1 MPa
rhol	811.26	kg/m3	298.15	Densities and Viscosities for Binary Liquid Mixtures of Pentanol Isomers from (288.15 to 328.15) K at 0.1 MPa
rhol	814.92	kg/m3	293.15	Densities and Viscosities for Binary Liquid Mixtures of Pentanol Isomers from (288.15 to 328.15) K at 0.1 MPa
rhol	818.56	kg/m3	288.15	Densities and Viscosities for Binary Liquid Mixtures of Pentanol Isomers from (288.15 to 328.15) K at 0.1 MPa
rhol	792.00	kg/m3	323.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory
rhol	795.80	kg/m3	318.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory
rhol	799.60	kg/m3	313.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory

rhol	803.30	kg/m3	308.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory
rhol	807.10	kg/m3	303.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory
rhol	811.04	kg/m3	298.15	Densities and Excess Molar Volumes of Cyclopentane (1) + 1-Alkanol (2) Systems at (298.15 and 308.15) K
rhol	814.50	kg/m3	293.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory
rhol	780.70	kg/m3	338.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Pentanol, 2-Pentanol, or 2-Methyl-1-Butanol from (288.15 to 338.15) K at 0.1 MPa
rhol	784.66	kg/m3	333.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Pentanol, 2-Pentanol, or 2-Methyl-1-Butanol from (288.15 to 338.15) K at 0.1 MPa

rhol	788.56	kg/m3	328.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Pentanol, 2-Pentanol, or 2-Methyl-1-Butanol from (288.15 to 338.15) K at 0.1 MPa	
rhol	822.42	kg/m3	283.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	792.46	kg/m3	323.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Pentanol, 2-Pentanol, or 2-Methyl-1-Butanol from (288.15 to 338.15) K at 0.1 MPa	
rhol	796.29	kg/m3	318.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Pentanol, 2-Pentanol, or 2-Methyl-1-Butanol from (288.15 to 338.15) K at 0.1 MPa	
rhol	800.08	kg/m3	313.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Pentanol, 2-Pentanol, or 2-Methyl-1-Butanol from (288.15 to 338.15) K at 0.1 MPa	

rhol	803.83	kg/m3	308.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Pentanol, 2-Pentanol, or 2-Methyl-1-Butanol from (288.15 to 338.15) K at 0.1 MPa
rhol	807.55	kg/m3	303.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Pentanol, 2-Pentanol, or 2-Methyl-1-Butanol from (288.15 to 338.15) K at 0.1 MPa
rhol	811.23	kg/m3	298.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Pentanol, 2-Pentanol, or 2-Methyl-1-Butanol from (288.15 to 338.15) K at 0.1 MPa
rhol	814.89	kg/m3	293.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Pentanol, 2-Pentanol, or 2-Methyl-1-Butanol from (288.15 to 338.15) K at 0.1 MPa
rhol	818.59	kg/m3	288.15	Densities and Viscosities for Binary Liquid Mixtures of Biodiesel + 1-Pentanol, 2-Pentanol, or 2-Methyl-1-Butanol from (288.15 to 338.15) K at 0.1 MPa
rhol	795.98	kg/m3	318.15	Physical Properties of the Pure Deep Eutectic Solvent, [ChCl]:[Lev] (1:2) DES, and Its Binary Mixtures with Alcohols

rhol	803.50	kg/m3	308.15	Physical Properties of the Pure Deep Eutectic Solvent, [ChCl]:[Lev] (1:2) DES, and Its Binary Mixtures with Alcohols
rhol	810.88	kg/m3	298.15	Physical Properties of the Pure Deep Eutectic Solvent, [ChCl]:[Lev] (1:2) DES, and Its Binary Mixtures with Alcohols
rhol	759.77	kg/m3	363.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	803.68	kg/m3	308.15	Densities and Excess Molar Volumes of Cyclopentane (1) + 1-Alkanol (2) Systems at (298.15 and 308.15) K
rhol	764.08	kg/m3	358.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	768.33	kg/m3	353.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa

rhol	772.49	kg/m3	348.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	776.58	kg/m3	343.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	780.62	kg/m3	338.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	784.59	kg/m3	333.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	788.50	kg/m3	328.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa

rhol	792.36	kg/m3	323.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	796.17	kg/m3	318.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	799.94	kg/m3	313.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	803.67	kg/m3	308.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	807.37	kg/m3	303.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa

rhol	811.03	kg/m3	298.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	814.68	kg/m3	293.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	818.30	kg/m3	288.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	821.90	kg/m3	283.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	811.40	kg/m3	298.15	Thermodynamics of 1,3-dimethylurea in eight alcohols
rhol	799.40	kg/m3	313.15	Excess molar volumes of Diisopropylamine + (C1-C5) Alkan-1-ols: application of the ERAS model and cubic EOS
rhol	807.07	kg/m3	303.15	Excess molar volumes of Diisopropylamine + (C1-C5) Alkan-1-ols: application of the ERAS model and cubic EOS

rhol	810.82	kg/m3	298.15	Excess molar volumes of Diisopropylamine + (C1-C5) Alkan-1-ols: application of the ERAS model and cubic EOS	
rhol	815.00	kg/m3	293.00	KDB	
rhol	807.11	kg/m3	303.15	Volumetric and transport properties of ternary mixtures containing 1-alkanol + ethyl ethanoate + cyclohexane at 303.15 K: Experimental data, correlation and prediction by ERAS model	
rhol	818.79	kg/m3	288.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	815.13	kg/m3	293.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	811.45	kg/m3	298.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	

rhol	807.74	kg/m3	303.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	804.01	kg/m3	308.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	800.24	kg/m3	313.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	796.43	kg/m3	318.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	792.57	kg/m3	323.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	

rhol	788.67	kg/m3	328.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	784.72	kg/m3	333.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	818.28	kg/m3	288.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules	
rhol	814.63	kg/m3	293.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules	
rhol	810.97	kg/m3	298.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules	

rhol	807.28	kg/m3	303.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules	
rhol	803.56	kg/m3	308.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules	
rhol	799.82	kg/m3	313.15	Influence of chain length and degree of branching of alcohol + chlorobenzene mixtures on determination and modelling of VE by CEOS and CEOS/GE mixing rules	
rhol	818.34	kg/m3	288.15	Thermodynamic properties of mixtures containing alkoxypropanol and n-alkanol	
rhol	811.00	kg/m3	298.15	Thermodynamic properties of mixtures containing alkoxypropanol and n-alkanol	
rhol	803.30	kg/m3	308.15	Thermodynamic properties of mixtures containing alkoxypropanol and n-alkanol	

rhol	819.15	kg/m3	288.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	811.80	kg/m3	298.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	800.57	kg/m3	313.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	789.01	kg/m3	328.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	781.05	kg/m3	338.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa

rhol	772.87	kg/m3	348.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	811.29	kg/m3	298.20	Liquid-liquid equilibrium data for ternary systems of water + lactic acid + C4-C7 alcohols at 298.2 K and atmospheric pressure
rhol	811.04	kg/m3	298.15	Vapor-liquid equilibria of binary systems composed of polyoxyethylene 4-octylphenyl ether and alcohols: Experimental measurements and correlation
rhol	818.30	kg/m3	288.15	Temperature dependence of the volumetric properties of some alkoxypropanols + n-alkanol mixtures
rhol	811.10	kg/m3	298.15	Temperature dependence of the volumetric properties of some alkoxypropanols + n-alkanol mixtures
rhol	804.10	kg/m3	308.15	Temperature dependence of the volumetric properties of some alkoxypropanols + n-alkanol mixtures

rhol	821.81	kg/m3	283.15	Excess molar volumes of binary mixtures of 1,3-dimethylimidazolidin-2-one with an alkan-1-ol at the temperatures 283.15 K, 298.15 K, and 313.15 K
rhol	810.88	kg/m3	298.15	Excess molar volumes of binary mixtures of 1,3-dimethylimidazolidin-2-one with an alkan-1-ol at the temperatures 283.15 K, 298.15 K, and 313.15 K
rhol	799.71	kg/m3	313.15	Excess molar volumes of binary mixtures of 1,3-dimethylimidazolidin-2-one with an alkan-1-ol at the temperatures 283.15 K, 298.15 K, and 313.15 K
rhol	811.00	kg/m3	298.15	Volumetric, acoustic, and viscometric studies of molecular interactions in binary mixtures of dipropylene glycol dimethyl ether with 1-alkanols at 298.15 K
rhol	814.80	kg/m3	293.15	Excess molar volumes of Diisopropylamine + (C1-C5) Alkan-1-ols: application of the ERAS model and cubic EOS
rhol	803.52	kg/m3	308.15	Osmotic and apparent molar properties of binary mixtures alcohol + 1-butyl-3-methylimidazolium trifluoromethanesulfonate ionic liquid
rhol	792.15	kg/m3	323.15	Osmotic and apparent molar properties of binary mixtures alcohol + 1-butyl-3-methylimidazolium trifluoromethanesulfonate ionic liquid

rhol	810.82	kg/m3	298.15	FT-IR studies on excess thermodynamic properties of binary liquid mixtures o-chlorotoluene with 1-propanol, 1-butanol, 1-pentanol, 1-hexanol and 1-heptanol at different temperatures	
rhol	807.10	kg/m3	303.15	FT-IR studies on excess thermodynamic properties of binary liquid mixtures o-chlorotoluene with 1-propanol, 1-butanol, 1-pentanol, 1-hexanol and 1-heptanol at different temperatures	
rhol	803.38	kg/m3	308.15	FT-IR studies on excess thermodynamic properties of binary liquid mixtures o-chlorotoluene with 1-propanol, 1-butanol, 1-pentanol, 1-hexanol and 1-heptanol at different temperatures	
rhol	810.00	kg/m3	303.15	Study of molecular interactions in the mixtures of some primary alcohols with equimolar mixture of 1-propanol and alkylbenzoates at T = 303.15 K	
rhol	792.14	kg/m3	323.15	Osmotic coefficients and apparent molar volumes of 1-hexyl-3-methylimidazolium trifluoromethanesulfonate ionic liquid in alcohols	

rhol	810.89	kg/m3	298.15	Excess molar enthalpies of the binary systems: (Dibutyl ether + isomers of pentanol) at T = (298.15 and 308.15) K
rhol	803.70	kg/m3	308.15	Excess molar enthalpies of the binary systems: (Dibutyl ether + isomers of pentanol) at T = (298.15 and 308.15) K
rhol	811.10	kg/m3	298.15	The study of molecular interactions in 1-ethyl-3-methylimidazolium trifluoromethanesulfonate + 1-pentanol from density, speed of sound and refractive index measurements
rhol	803.70	kg/m3	308.15	The study of molecular interactions in 1-ethyl-3-methylimidazolium trifluoromethanesulfonate + 1-pentanol from density, speed of sound and refractive index measurements
rhol	796.10	kg/m3	318.15	The study of molecular interactions in 1-ethyl-3-methylimidazolium trifluoromethanesulfonate + 1-pentanol from density, speed of sound and refractive index measurements
rhol	788.40	kg/m3	328.15	The study of molecular interactions in 1-ethyl-3-methylimidazolium trifluoromethanesulfonate + 1-pentanol from density, speed of sound and refractive index measurements

rhol	814.81	kg/m3	293.15	Thermodynamic and spectroscopic properties of binary mixtures of n-butylammonium butanoate ionic liquid with alcohols at T = (293.15-313.15) K	
rhol	811.14	kg/m3	298.15	Thermodynamic and spectroscopic properties of binary mixtures of n-butylammonium butanoate ionic liquid with alcohols at T = (293.15-313.15) K	
rhol	807.46	kg/m3	303.15	Thermodynamic and spectroscopic properties of binary mixtures of n-butylammonium butanoate ionic liquid with alcohols at T = (293.15-313.15) K	
rhol	803.74	kg/m3	308.15	Thermodynamic and spectroscopic properties of binary mixtures of n-butylammonium butanoate ionic liquid with alcohols at T = (293.15-313.15) K	
rhol	799.99	kg/m3	313.15	Thermodynamic and spectroscopic properties of binary mixtures of n-butylammonium butanoate ionic liquid with alcohols at T = (293.15-313.15) K	

rhol	811.00	kg/m3	298.00	Comparative study of physical properties of binary mixtures of halogen free ionic liquids with alcohols
rhol	807.00	kg/m3	303.00	Comparative study of physical properties of binary mixtures of halogen free ionic liquids with alcohols
rhol	803.00	kg/m3	308.00	Comparative study of physical properties of binary mixtures of halogen free ionic liquids with alcohols
rhol	800.00	kg/m3	313.00	Comparative study of physical properties of binary mixtures of halogen free ionic liquids with alcohols
rhol	821.79	kg/m3	283.15	Excess molar enthalpies of R-fenchone + butan-1-ol or + pentan-1-ol. Modeling with COSMO-RS and UNIFAC
rhol	810.90	kg/m3	298.15	Excess molar enthalpies of R-fenchone + butan-1-ol or + pentan-1-ol. Modeling with COSMO-RS and UNIFAC
rhol	799.80	kg/m3	313.15	Excess molar enthalpies of R-fenchone + butan-1-ol or + pentan-1-ol. Modeling with COSMO-RS and UNIFAC
rhol	788.82	kg/m3	328.15	Excess molar enthalpies of R-fenchone + butan-1-ol or + pentan-1-ol. Modeling with COSMO-RS and UNIFAC

rhol	810.90	kg/m3	298.15	Excess volumes and partial molar volumes of binary liquid mixtures of furfural or 2-methylfuran with alcohols at 298.15 K
rhol	810.88	kg/m3	298.15	Excess molar enthalpies of methyl isobutyl ketone (MIBK) with alkan-1-ols (C1-C6) and their correlations at 298.15 K
rhol	814.53	kg/m3	293.15	Osmotic and apparent molar properties of binary mixtures alcohol + 1-butyl-3-methylimidazolium trifluoromethanesulfonate ionic liquid
rhol	810.84	kg/m3	298.15	Study of the Effects of Temperature and Pressure on the Thermodynamic and Acoustic Properties of Pentan-1-ol, 2-Methyl-2-butanol, and Cyclopentanol in the Pressure Range from (0.1 to 100) MPa and Temperature from (293 to 318) K
sdco	0.00	m2/s	323.10	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	364.73	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	364.59	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	364.52	Viscous Calibration Liquids for Self-diffusion Measurements

sdco	0.00	m2/s	352.55	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	352.36	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	352.35	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	347.25	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	298.27	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	347.21	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	337.74	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	337.71	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	327.86	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	327.86	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	323.15	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	253.13	Viscous Calibration Liquids for Self-diffusion Measurements

sdco	0.00	m2/s	253.19	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	323.15	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	258.47	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	263.25	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	263.28	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	268.65	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	268.66	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	278.40	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	278.43	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	288.31	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	288.33	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	298.16	Viscous Calibration Liquids for Self-diffusion Measurements

sdco	0.00	m2/s	298.17	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	298.19	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	298.21	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	298.21	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	298.27	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	308.09	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	308.11	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	318.08	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	318.09	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	323.10	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	258.42	Viscous Calibration Liquids for Self-diffusion Measurements
sfust	50.61	J/mol×K	194.20	NIST Webbook
sfust	53.70	J/mol×K	195.56	NIST Webbook

speedsl	1192.80	m/s	323.15	Acoustic, volumetric and osmotic properties of binary mixtures containing the ionic liquid 1-butyl-3-methylimidazolim dicyanamide mixed with primary and secondary alcohols
speedsl	1274.00	m/s	298.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene
speedsl	1225.50	m/s	313.15	Excess Molar Enthalpy, Density, and Speed of Sound for the Mixtures a-Pinene + 1- or 2-Pentanol at (283.15, 298.15, and 313.15) K
speedsl	1274.10	m/s	298.15	Excess Molar Enthalpy, Density, and Speed of Sound for the Mixtures a-Pinene + 1- or 2-Pentanol at (283.15, 298.15, and 313.15) K
speedsl	1325.90	m/s	283.15	Excess Molar Enthalpy, Density, and Speed of Sound for the Mixtures a-Pinene + 1- or 2-Pentanol at (283.15, 298.15, and 313.15) K

speedsl	1242.40	m/s	308.15	Acoustic, volumetric and osmotic properties of binary mixtures containing the ionic liquid 1-butyl-3-methylimidazolim dicyanamide mixed with primary and secondary alcohols
speedsl	1292.50	m/s	293.15	Acoustic, volumetric and osmotic properties of binary mixtures containing the ionic liquid 1-butyl-3-methylimidazolim dicyanamide mixed with primary and secondary alcohols
speedsl	1281.20	m/s	298.15	Ultrasonic speeds and isentropic compressibilities of {difurylmethane + (C1 C6) n-alkanol} binary mixtures at T = 298.15 K
speedsl	1243.67	m/s	308.15	Densities, excess molar volumes, speeds of sound and isothermal compressibilities for {2-(2-hexyloxyethoxy)ethanol + n-alkanol} systems at temperatures between (288.15 and 308.15) K
speedsl	1258.25	m/s	303.15	Densities, excess molar volumes, speeds of sound and isothermal compressibilities for {2-(2-hexyloxyethoxy)ethanol + n-alkanol} systems at temperatures between (288.15 and 308.15) K

speedsl	1276.01	m/s	298.15	Densities, excess molar volumes, speeds of sound and isothermal compressibilities for {2-(2-hexyloxyethoxy)ethanol + n-alkanol} systems at temperatures between (288.15 and 308.15) K
speedsl	1293.45	m/s	293.15	Densities, excess molar volumes, speeds of sound and isothermal compressibilities for {2-(2-hexyloxyethoxy)ethanol + n-alkanol} systems at temperatures between (288.15 and 308.15) K
speedsl	1240.00	m/s	308.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene
speedsl	1274.32	m/s	298.15	Densities, Speeds of Sound, and Isentropic Compressibilities for Binary Mixtures of 2-Ethyl-1-hexanol with 1-Pentanol, 1-Heptanol, or 1-Nonanol at the Temperature 298.15 K

speedsl	1312.50	m/s	288.15	Densities, excess molar volumes, speeds of sound and isothermal compressibilities for {2-(2-hexyloxyethoxy)ethanol + n-alkanol} systems at temperatures between (288.15 and 308.15) K
srf	0.02	N/m	313.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.02	N/m	308.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.02	N/m	303.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.02	N/m	318.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.03	N/m	298.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	303.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	308.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	313.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K

srf	0.02	N/m	318.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	323.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.03	N/m	293.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol
srf	0.02	N/m	298.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.02	N/m	303.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol
srf	0.02	N/m	308.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol
srf	0.02	N/m	313.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol
srf	0.02	N/m	318.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol
srf	0.02	N/m	323.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol
srf	0.03	N/m	293.15	Density and Surface Tension of Binary Mixtures of Acetonitrile + 1-Alkanol at 293.15 K
srf	0.03	N/m	293.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes

srf	0.03	N/m	293.20	KDB
srf	0.03	N/m	298.15	Surface Tension of Dilute Solutions of Linear Alcohols in Benzyl Alcohol

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbrp	323.20	K	1.70	NIST Webbook

Correlations

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)
Coeff. A	1.45991e+01
Coeff. B	-3.07041e+03
Coeff. C	-1.03369e+02
Temperature range (K), min.	317.91
Temperature range (K), max.	433.96

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/T + C*ln(T) + D*T^2
Coeff. A	1.49346e+02
Coeff. B	-1.21964e+04
Coeff. C	-1.93819e+01
Coeff. D	9.39571e-06
Temperature range (K), min.	195.56
Temperature range (K), max.	588.00

Datasets

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
293.15	100.00	814.7
293.15	10000.00	821.1
293.15	20000.00	827.3
293.15	30000.00	833.2
293.15	40000.00	838.6
293.15	50000.00	843.6
293.15	60000.00	848.5
293.15	70000.00	853.1
293.15	80000.00	857.4
293.15	90000.00	861.7
293.15	100000.00	865.8
293.15	110000.00	869.6
293.15	120000.00	873.2
293.15	130000.00	876.9
293.15	140000.00	880.3
303.15	100.00	807.3
303.15	10000.00	814.4
303.15	20000.00	820.7
303.15	30000.00	826.7
303.15	40000.00	832.2
303.15	50000.00	837.5
303.15	60000.00	842.4
303.15	70000.00	847.0
303.15	80000.00	851.6
303.15	90000.00	855.8
303.15	100000.00	860.1
303.15	110000.00	864.1
303.15	120000.00	868.0
303.15	130000.00	871.7
303.15	140000.00	875.2
313.15	100.00	799.8
313.15	10000.00	807.4
313.15	20000.00	814.1
313.15	30000.00	820.2
313.15	40000.00	826.0
313.15	50000.00	831.5
313.15	60000.00	836.6
313.15	70000.00	841.4
313.15	80000.00	846.1

313.15	90000.00	850.5
313.15	100000.00	854.8
313.15	110000.00	858.9
313.15	120000.00	862.8
313.15	130000.00	866.6
313.15	140000.00	870.2
323.15	100.00	792.5
323.15	10000.00	800.3
323.15	20000.00	807.3
323.15	30000.00	813.7
323.15	40000.00	819.8
323.15	50000.00	825.4
323.15	60000.00	830.7
323.15	70000.00	835.7
323.15	80000.00	840.4
323.15	90000.00	845.0
323.15	100000.00	849.3
323.15	110000.00	853.6
323.15	120000.00	857.6
323.15	130000.00	861.5
323.15	140000.00	865.3
333.15	100.00	784.4
333.15	10000.00	792.7
333.15	20000.00	800.1
333.15	30000.00	806.8
333.15	40000.00	813.1
333.15	50000.00	818.9
333.15	60000.00	824.4
333.15	70000.00	829.7
333.15	80000.00	834.6
333.15	90000.00	839.2
333.15	100000.00	843.7
333.15	110000.00	848.0
333.15	120000.00	852.1
333.15	130000.00	856.0
333.15	140000.00	860.0
343.15	100.00	776.5
343.15	10000.00	785.2
343.15	20000.00	792.9
343.15	30000.00	799.9
343.15	40000.00	806.6
343.15	50000.00	812.6
343.15	60000.00	818.3
343.15	70000.00	823.7

343.15	80000.00	828.7
343.15	90000.00	833.5
343.15	100000.00	838.2
343.15	110000.00	842.5
343.15	120000.00	846.8
343.15	130000.00	850.9
343.15	140000.00	854.8
353.15	100.00	768.1
353.15	10000.00	777.3
353.15	20000.00	785.6
353.15	30000.00	792.9
353.15	40000.00	799.8
353.15	50000.00	806.1
353.15	60000.00	812.0
353.15	70000.00	817.6
353.15	80000.00	822.8
353.15	90000.00	827.8
353.15	100000.00	832.6
353.15	110000.00	837.2
353.15	120000.00	841.6
353.15	130000.00	845.8
353.15	140000.00	849.7
363.15	100.00	759.4
363.15	10000.00	769.2
363.15	20000.00	777.7
363.15	30000.00	785.6
363.15	40000.00	792.6
363.15	50000.00	799.2
363.15	60000.00	805.5
363.15	70000.00	811.3
363.15	80000.00	816.7
363.15	90000.00	821.8
363.15	100000.00	826.8
363.15	110000.00	831.3
363.15	120000.00	835.8
363.15	130000.00	840.1
363.15	140000.00	844.2
373.15	100.00	750.7
373.15	10000.00	761.2
373.15	20000.00	770.3
373.15	30000.00	778.2
373.15	40000.00	785.7
373.15	50000.00	792.5
373.15	60000.00	798.9

373.15	70000.00	804.9
373.15	80000.00	810.5
373.15	90000.00	815.8
373.15	100000.00	820.9
373.15	110000.00	825.7
373.15	120000.00	830.3
373.15	130000.00	834.7
373.15	140000.00	839.0
383.15	100.00	741.5
383.15	10000.00	752.3
383.15	20000.00	761.9
383.15	30000.00	770.7
383.15	40000.00	778.5
383.15	50000.00	785.7
383.15	60000.00	792.3
383.15	70000.00	798.5
383.15	80000.00	804.3
383.15	90000.00	809.7
383.15	100000.00	815.0
383.15	110000.00	819.9
383.15	120000.00	824.7
383.15	130000.00	829.2
383.15	140000.00	833.5
393.15	100.00	731.7
393.15	10000.00	743.4
393.15	20000.00	753.7
393.15	30000.00	762.8
393.15	40000.00	771.0
393.15	50000.00	778.6
393.15	60000.00	785.6
393.15	70000.00	792.0
393.15	80000.00	798.1
393.15	90000.00	803.7
393.15	100000.00	809.1
393.15	110000.00	814.2
393.15	120000.00	819.1
393.15	130000.00	823.7
393.15	140000.00	828.1
403.15	100.00	721.7
403.15	10000.00	734.4
403.15	20000.00	745.3
403.15	30000.00	754.9
403.15	40000.00	763.4
403.15	50000.00	771.3

403.15	60000.00	778.4
403.15	70000.00	785.1
403.15	80000.00	791.3
403.15	90000.00	797.2
403.15	100000.00	802.8
403.15	110000.00	808.0
403.15	120000.00	813.0
403.15	130000.00	817.8
403.15	140000.00	822.3

Reference *https://www.doi.org/10.1016/j.fluid.2008.06.007*

Temperature, K	Pressure, kPa	Mass density, kg/m3
298.15	100.00	810.8

Reference *https://www.doi.org/10.1016/j.fluid.2019.02.006*

Temperature, K	Pressure, kPa	Mass density, kg/m3
312.96	512.00	799.65
312.96	1022.00	800.04
312.96	1998.00	800.77
312.96	3005.00	801.53
312.96	4003.00	802.28
312.96	5002.00	803.02
312.96	6018.00	803.76
312.96	6994.00	804.49
312.96	8008.00	805.21
312.96	9005.00	805.93
312.96	10008.00	806.66
312.96	11008.00	807.37
312.96	12000.00	808.07
312.96	13024.00	808.78
312.96	13987.00	809.45
312.96	15014.00	810.14
312.96	15991.00	810.8
312.96	17019.00	811.48
312.96	17991.00	812.12
312.96	19007.00	812.79
312.96	19992.00	813.44
312.96	21031.00	814.1
312.96	22041.00	814.76
312.96	23014.00	815.41

312.96	24003.00	816.04
312.96	25037.00	816.73
322.89	520.00	792.06
322.89	1010.00	792.47
322.89	2005.00	793.27
322.89	3007.00	794.07
322.89	4005.00	794.86
322.89	5018.00	795.63
322.89	6001.00	796.42
322.89	7016.00	797.2
322.89	8020.00	797.97
322.89	8997.00	798.71
322.89	10001.00	799.47
322.89	11005.00	800.21
322.89	11996.00	800.95
322.89	13002.00	801.68
322.89	14013.00	802.4
322.89	15005.00	803.11
322.89	16014.00	803.82
322.89	17001.00	804.51
322.89	18016.00	805.21
322.89	19012.00	805.89
322.89	19992.00	806.56
322.89	21036.00	807.26
322.89	22003.00	807.92
322.89	23024.00	808.61
322.89	23994.00	809.26
322.89	25023.00	810.0
332.79	493.00	784.29
332.79	1014.00	784.76
332.79	2006.00	785.61
332.79	3025.00	786.48
332.79	4011.00	787.28
332.79	5020.00	788.11
332.79	6003.00	788.91
332.79	6997.00	789.73
332.79	8009.00	790.54
332.79	8995.00	791.31
332.79	9996.00	792.12
332.79	11018.00	792.9
332.79	11995.00	793.66
332.79	13023.00	794.45
332.79	13999.00	795.19
332.79	15010.00	795.95

332.79	16028.00	796.68
332.79	17003.00	797.41
332.79	18040.00	798.14
332.79	19004.00	798.84
332.79	20035.00	799.59
332.79	21024.00	800.29
332.79	21993.00	800.97
332.79	23039.00	801.71
332.79	24015.00	802.4
332.79	25022.00	803.12
342.76	505.00	776.31
342.76	997.00	776.77
342.76	1995.00	777.69
342.76	3011.00	778.59
342.76	4012.00	779.47
342.76	5011.00	780.34
342.76	6011.00	781.22
342.76	7003.00	782.03
342.76	8015.00	782.91
342.76	9000.00	783.73
342.76	10019.00	784.58
342.76	11020.00	785.4
342.76	12002.00	786.2
342.76	13016.00	787.02
342.76	14024.00	787.81
342.76	15002.00	788.59
342.76	16007.00	789.36
342.76	17037.00	790.15
342.76	17988.00	790.87
342.76	19037.00	791.66
342.76	20003.00	792.38
342.76	21015.00	793.14
342.76	22019.00	793.88
342.76	23039.00	794.62
342.76	24027.00	795.36
342.76	25028.00	796.1
352.71	508.00	768.15
352.71	1011.00	768.66
352.71	1995.00	769.61
352.71	3014.00	770.57
352.71	3998.00	771.49
352.71	5022.00	772.45
352.71	6012.00	773.35
352.71	7006.00	774.26

352.71	8024.00	775.17
352.71	9005.00	776.05
352.71	10016.00	776.94
352.71	11026.00	777.81
352.71	12001.00	778.65
352.71	13002.00	779.5
352.71	14026.00	780.35
352.71	15000.00	781.18
352.71	16005.00	781.98
352.71	17023.00	782.81
352.71	18003.00	783.59
352.71	19049.00	784.43
352.71	20035.00	785.2
352.71	21002.00	785.96
352.71	21995.00	786.73
352.71	23020.00	787.52
352.71	24045.00	788.32
352.71	25009.00	789.05
362.59	517.00	759.7
362.59	1023.00	760.25
362.59	2005.00	761.26
362.59	3010.00	762.29
362.59	3998.00	763.28
362.59	5006.00	764.25
362.59	6013.00	765.23
362.59	7014.00	766.21
362.59	8007.00	767.16
362.59	9020.00	768.1
362.59	10006.00	769.02
362.59	10991.00	769.93
362.59	12025.00	770.87
362.59	13008.00	771.76
362.59	13998.00	772.62
362.59	15017.00	773.51
362.59	16000.00	774.37
362.59	17013.00	775.24
362.59	18032.00	776.11
362.59	19003.00	776.9
362.59	20030.00	777.77
362.59	20987.00	778.55
362.59	22033.00	779.4
362.59	23000.00	780.2
362.59	24031.00	781.02
362.59	25026.00	781.82

Temperature, K	Pressure, kPa	Mass density, kg/m3
278.15	100.00	825.2
278.15	1000.00	825.8
278.15	5000.00	828.5
278.15	10000.00	831.6
278.15	15000.00	834.7
278.15	20000.00	837.6
278.15	25000.00	840.4
278.15	30000.00	843.2
278.15	35000.00	845.9
278.15	40000.00	848.6
278.15	45000.00	851.1
278.15	50000.00	853.6
278.15	55000.00	856.1
278.15	60000.00	858.4
288.15	100.00	818.0
288.15	1000.00	818.7
288.15	5000.00	821.5
288.15	10000.00	824.8
288.15	15000.00	828.0
288.15	20000.00	831.1
288.15	25000.00	834.0
288.15	30000.00	836.9
288.15	35000.00	839.7
288.15	40000.00	842.4
288.15	45000.00	845.0
288.15	50000.00	847.6
288.15	55000.00	850.1
288.15	60000.00	852.5
298.15	100.00	810.7
298.15	1000.00	811.3
298.15	5000.00	814.2
298.15	10000.00	817.7
298.15	15000.00	821.0
298.15	20000.00	824.3
298.15	25000.00	827.3
298.15	30000.00	830.3
298.15	35000.00	833.2
298.15	40000.00	836.0
298.15	45000.00	838.7

298.15	50000.00	841.4
298.15	55000.00	844.0
298.15	60000.00	846.4
308.15	100.00	803.3
308.15	1000.00	804.0
308.15	5000.00	807.0
308.15	10000.00	810.7
308.15	15000.00	814.0
308.15	20000.00	817.5
308.15	25000.00	820.7
308.15	30000.00	823.8
308.15	35000.00	826.8
308.15	40000.00	829.7
308.15	45000.00	832.5
308.15	50000.00	835.3
308.15	55000.00	838.0
308.15	60000.00	840.4
318.15	100.00	795.8
318.15	1000.00	796.6
318.15	5000.00	799.8
318.15	10000.00	803.6
318.15	15000.00	807.2
318.15	20000.00	810.7
318.15	25000.00	814.0
318.15	30000.00	817.3
318.15	35000.00	820.4
318.15	40000.00	823.4
318.15	45000.00	826.3
318.15	50000.00	829.1
318.15	55000.00	831.9
318.15	60000.00	834.6
328.15	100.00	788.2
328.15	1000.00	789.0
328.15	5000.00	792.3
328.15	10000.00	796.3
328.15	15000.00	800.1
328.15	20000.00	803.8
328.15	25000.00	807.2
328.15	30000.00	810.6
328.15	35000.00	813.8
328.15	40000.00	817.0
328.15	45000.00	820.0
328.15	50000.00	822.9
328.15	55000.00	825.8

328.15	60000.00	828.4
338.15	100.00	780.3
338.15	1000.00	781.2
338.15	5000.00	784.8
338.15	10000.00	788.9
338.15	15000.00	792.9
338.15	20000.00	796.7
338.15	25000.00	800.3
338.15	30000.00	803.8
338.15	35000.00	807.2
338.15	40000.00	810.5
338.15	45000.00	813.6
338.15	50000.00	816.6
338.15	55000.00	819.6
338.15	60000.00	822.5
348.15	100.00	772.3
348.15	1000.00	773.1
348.15	5000.00	776.9
348.15	10000.00	781.2
348.15	15000.00	785.5
348.15	20000.00	789.5
348.15	25000.00	793.3
348.15	30000.00	796.9
348.15	35000.00	800.4
348.15	40000.00	803.8
348.15	45000.00	807.1
348.15	50000.00	810.3
348.15	55000.00	813.3
348.15	60000.00	816.2
358.15	100.00	763.8
358.15	1000.00	764.8
358.15	5000.00	768.8
358.15	10000.00	773.5
358.15	15000.00	777.9
358.15	20000.00	782.1
358.15	25000.00	786.1
358.15	30000.00	789.9
358.15	35000.00	793.6
358.15	40000.00	797.1
358.15	45000.00	800.5
358.15	50000.00	803.8
358.15	55000.00	807.0
358.15	60000.00	810.0

Reference *https://www.doi.org/10.1016/j.jct.2011.10.023*

Temperature, K	Pressure, kPa	Mass density, kg/m3
298.15	2003.00	811.93
298.15	3999.00	813.3
298.15	6003.00	814.64
298.15	8005.00	815.96
298.15	10001.00	817.26
298.15	13000.00	819.15
298.15	16004.00	821.0
298.15	19006.00	822.8
298.15	22000.00	824.56
298.15	24998.00	826.27
323.15	1999.00	794.19
323.15	4001.00	795.77
323.15	6001.00	797.32
323.15	8000.00	798.83
323.15	9998.00	800.31
323.15	12999.00	802.47
323.15	16001.00	804.56
323.15	19002.00	806.59
323.15	22001.00	808.56
323.15	25002.00	810.48

Reference *https://www.doi.org/10.1021/acs.jced.5b00152*

Temperature, K	Pressure, kPa	Mass density, kg/m3
298.15	2000.00	813.0
298.15	4000.00	814.4
298.15	6000.00	815.8
298.15	8010.00	817.1
298.15	10000.00	818.5
298.15	13000.00	820.4
298.15	16000.00	822.3
298.15	19010.00	824.1
298.15	22000.00	825.9
298.15	25000.00	827.6
298.15	27990.00	829.4
298.15	29980.00	830.4
303.16	1980.00	808.8
303.16	3980.00	810.2

303.16	6010.00	811.7
303.16	8020.00	813.0
303.16	10030.00	814.4
303.16	12990.00	816.4
303.16	15980.00	818.4
303.15	19000.00	820.3
303.16	22010.00	822.1
303.16	25000.00	823.9
303.15	27980.00	825.6
303.16	29990.00	826.7
313.15	1990.00	800.6
313.15	4000.00	802.2
313.15	5980.00	803.7
313.15	7980.00	805.1
313.15	10020.00	806.6
313.15	13010.00	808.7
313.16	15980.00	810.8
313.15	19020.00	812.8
313.15	21980.00	814.7
313.16	24990.00	816.6
313.16	28000.00	818.4
313.15	30020.00	819.6
323.15	2000.00	793.5
323.15	4000.00	795.0
323.15	6000.00	796.7
323.15	8000.00	798.2
323.15	10000.00	799.6
323.15	13000.00	801.9
323.15	16000.00	804.0
323.15	19000.00	806.1
323.15	22000.00	808.2
323.15	25000.00	810.2
323.15	27990.00	812.1
323.15	29990.00	813.4

Reference *https://www.doi.org/10.1021/acs.jced.8b00812*

Temperature, K	Pressure, kPa	Mass density, kg/m3
293.15	100.00	815.25
293.15	5000.00	818.83
293.15	10000.00	822.19
293.15	15000.00	825.37
293.15	20000.00	828.41

293.15	25000.00	831.36
293.15	30000.00	834.24
293.15	35000.00	837.11
303.15	100.00	808.05
303.15	5000.00	811.93
303.15	10000.00	815.5
303.15	15000.00	818.82
303.15	20000.00	821.92
303.15	25000.00	824.88
303.15	30000.00	827.74
303.15	35000.00	830.55
313.15	100.00	800.67
313.15	5000.00	804.61
313.15	10000.00	808.28
313.15	15000.00	811.75
313.15	20000.00	815.06
313.15	25000.00	818.26
313.15	30000.00	821.41
313.15	35000.00	824.56

Reference *https://www.doi.org/10.1021/acs.jced.8b00975*

Temperature, K	Pressure, kPa	Mass density, kg/m3
298.15	100.00	810.8

Reference *https://www.doi.org/10.1021/acs.jced.8b01189*

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Legend

af: Acentric Factor

affp:	Proton affinity
aigt:	Autoignition Temperature
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
fll:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
kvisc:	Kinematic viscosity
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sdco:	Self diffusion coefficient
sfust:	Entropy of fusion at a given temperature
sg:	Molar entropy at standard conditions
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tbrp:	Boiling point at reduced pressure
tc:	Critical Temperature
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume

zc:	Critical Compressibility
zra:	Rackett Parameter