

# Ethyl Acetate

<b>Other names:</b>	1-Acetoxyethane Acetic acid, ethyl ester Acetic ether Acetidin Acetoxyethane Aethylacetat CH <sub>3</sub> COOC <sub>2</sub> H <sub>5</sub> Essigester Ethyl acetic ester Ethyl ester of acetic acid Ethyl ethanoate Ethylacetaat Ethyle (acetate d') Ethylester kyseliny octove Etile (acetato di) NSC 70930 Rcra waste number U112 UN 1173 Vinegar naphtha ac. acetic ethyl ester
<b>Inchi:</b>	InChI=1S/C4H8O2/c1-3-6-4(2)5/h3H2,1-2H3
<b>InchiKey:</b>	XEKOWRVHYACXOJ-UHFFFAOYSA-N
<b>Formula:</b>	C <sub>4</sub> H <sub>8</sub> O <sub>2</sub>
<b>SMILES:</b>	CCOC(C)=O
<b>Mol. weight [g/mol]:</b>	88.11
<b>CAS:</b>	141-78-6

## Physical Properties

Property code	Value	Unit	Source
af	0.3620		KDB
affp	835.70	kJ/mol	NIST Webbook
aigt	699.82	K	KDB
basg	804.70	kJ/mol	NIST Webbook
basg	799.90 ± 0.20	kJ/mol	NIST Webbook
chl	-2235.40 ± 3.90	kJ/mol	NIST Webbook
chl	-2238.54 ± 0.48	kJ/mol	NIST Webbook
chl	-2246.00	kJ/mol	NIST Webbook

chl	-2256.00	kJ/mol	NIST Webbook
dm	1.90	debye	KDB
dvisc	0.0004370	Paxs	A volumetric and viscosity study for the binary mixtures of 1-hexyl-3-methylimidazolium tetrafluoroborate with some molecular solvents
dvisc	0.0004274	Paxs	Densities and Viscosities of Binary Liquid Mixtures of Trichloroethylene and Tetrachloroethylene with Some Polar and Nonpolar Solvents
dvisc	0.0004260	Paxs	Densities and Viscosities of Ternary Mixtures of Cyclohexane + Cyclohexanone + Some Alkyl Acetates at 298.15 K
fil	2.20	% in Air	KDB
flu	9.00	% in Air	KDB
fpc	285.93	K	KDB
fpo	268.71	K	KDB
gf	-327.60	kJ/mol	KDB
gyrad	3.3480		KDB
hf	-445.43 ± 0.84	kJ/mol	NIST Webbook
hf	-443.20	kJ/mol	KDB
hf	-446.90	kJ/mol	NIST Webbook
hf	-443.80	kJ/mol	NIST Webbook
hf	-444.80 ± 0.40	kJ/mol	NIST Webbook
hfl	-479.86 ± 0.46	kJ/mol	NIST Webbook
hfl	-480.57 ± 0.79	kJ/mol	NIST Webbook
hfl	-482.00 ± 4.00	kJ/mol	NIST Webbook
hfl	-478.82 ± 0.73	kJ/mol	NIST Webbook
hfus	8.90	kJ/mol	Joback Method
hvap	33.65	kJ/mol	Joback Method
ie	10.09 ± 0.02	eV	NIST Webbook
ie	9.90 ± 0.05	eV	NIST Webbook
ie	10.01 ± 0.05	eV	NIST Webbook
ie	9.90	eV	NIST Webbook
ie	10.01 ± 0.05	eV	NIST Webbook
ie	10.00 ± 0.10	eV	NIST Webbook
ie	10.24	eV	NIST Webbook
ie	10.11 ± 0.02	eV	NIST Webbook
ie	10.45	eV	NIST Webbook
ie	10.16	eV	NIST Webbook
log10ws	-0.04		Aqueous Solubility Prediction Method

log10ws	-0.04		Estimated Solubility Method
logp	0.569		Crippen Method
mcvol	74.660	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
pc	3830.00 ± 81.06	kPa	NIST Webbook
pc	3882.00 ± 3.87	kPa	NIST Webbook
pc	3900.00	kPa	Critical Properties of the Reacting Mixture in the Esterification of Acetic Acid with Ethanol
pc	3851.70 ± 40.00	kPa	NIST Webbook
pc	4018.00 ± 202.65	kPa	NIST Webbook
pc	4280.00 ± 405.30	kPa	NIST Webbook
pc	3882.00	kPa	KDB
rhoc	307.66 ± 5.29	kg/m3	NIST Webbook
rhoc	308.10 ± 4.41	kg/m3	NIST Webbook
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tb	350.65 ± 2.00	K	NIST Webbook
tb	350.70 ± 2.00	K	NIST Webbook
tb	350.10 ± 2.00	K	NIST Webbook
tb	350.30 ± 2.00	K	NIST Webbook

tb	350.20 ± 2.00	K	NIST Webbook
tb	350.30 ± 2.00	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tb	350.16	K	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tb	347.45 ± 2.00	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.26	K	KDB
tb	350.27	K	Vapor liquid equilibria for the quaternary reactive system ethyl acetate + ethanol + water + acetic acid and some of the constituent binary systems at 101.3 kPa
tb	350.24	K	Vapor liquid equilibria for the binary mixtures of 2,3-butanediol with n-butanol, n-butyl acetate, and ethyl acetate at 101.3 kPa
tb	350.24	K	Liquid-liquid equilibria of water + 3-hydroxy-2-butanone + ethyl ethanoate
tb	350.20	K	Solubility and tie-line data for ternary aqueous mixtures of cyclopentanol with organic solvents at T = 298.2 K: Experiments and NRTL model
tb	350.15	K	The isobaric vapor liquid equilibria of ethyl acetate p acetonitrile p bis(trifluoromethylsulfonyl)imide-based ionic liquids at 101.3 kPa
tb	350.29	K	Isobaric vapor-liquid equilibrium of a ternary system of ethyl acetate + propyl acetate + dimethyl sulfoxide and binary systems of ethyl acetate + dimethyl sulfoxide and propyl acetate + dimethyl sulfoxide at 101.3 kPa
tb	350.35	K	Isobaric Vapor - Liquid Equilibrium for Ethyl acetate + Methanol + Ionic Liquids Ternary systems at 101.3 kPa
tb	349.90 ± 0.20	K	NIST Webbook

tb	350.20	K	Isobaric Vapor Liquid Equilibrium for Three Binary Systems of Acetaldehyde + Ethanol, Ethyl Acetate, 1-Butanol at 101.3 kPa
tb	350.25 ± 1.00	K	NIST Webbook
tb	350.28	K	Isobaric Vapor-Liquid Phase Equilibrium Measurements for Allyl Alcohol with Chloroform, Ethyl Acetate, and Methyl Propionate at 101.3 kPa
tb	350.25	K	Isobaric Vapor-Liquid Equilibria and Excess Quantities for Binary Mixtures of an Ethyl Ester + tert-Butanol and a New Approach to VLE Data Processing
tb	350.15	K	Vapor-Liquid Equilibrium of Binary Mixtures Containing Ethyl Acetate + 2-Methyl-1-propanol and Ethyl Acetate + 2-Methyl-1-butanol at 101.3 kPa
tb	350.21	K	Volumetric Behavior and Saturated Pressure for Carbon Dioxide + Ethyl Acetate at a Temperature of 313.15 K
tb	350.15	K	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
tb	350.19	K	Experimental Determination of Vapor Liquid Equilibria. Binary Systems of Methyl Acetate, Ethyl Acetate, and Propyl Acetate with 1-Propanol at 0.6 MPa
tb	350.13 ± 0.30	K	NIST Webbook
tb	350.20	K	NIST Webbook
tb	350.00	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	349.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tb	350.30	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.19 ± 0.50	K	NIST Webbook



tb	350.25 ± 0.30	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tb	350.30 ± 0.30	K	NIST Webbook
tb	375.00 ± 2.00	K	NIST Webbook
tb	350.35	K	NIST Webbook
tb	350.05 ± 0.30	K	NIST Webbook
tb	350.21 ± 0.50	K	NIST Webbook
tb	350.25 ± 0.50	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.30 ± 0.30	K	NIST Webbook
tb	350.29 ± 0.15	K	NIST Webbook
tb	350.15 ± 2.00	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 0.50	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.65 ± 2.00	K	NIST Webbook
tb	349.65 ± 2.00	K	NIST Webbook
tb	352.15 ± 2.00	K	NIST Webbook
tb	350.25 ± 1.00	K	NIST Webbook
tb	350.30 ± 1.00	K	NIST Webbook
tb	350.30 ± 1.00	K	NIST Webbook
tb	349.97 ± 2.00	K	NIST Webbook
tb	351.15 ± 2.00	K	NIST Webbook
tb	350.45 ± 1.00	K	NIST Webbook
tb	350.25 ± 1.00	K	NIST Webbook
tb	350.30 ± 0.40	K	NIST Webbook
tb	349.15 ± 2.00	K	NIST Webbook
tb	349.65 ± 2.50	K	NIST Webbook
tb	350.26 ± 0.06	K	NIST Webbook
tb	350.30 ± 0.15	K	NIST Webbook
tb	350.00 ± 2.00	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.15 ± 2.00	K	NIST Webbook
tb	349.95 ± 2.00	K	NIST Webbook
tb	350.20 ± 0.50	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tb	350.25 ± 0.50	K	NIST Webbook
tb	350.21 ± 0.50	K	NIST Webbook
tb	349.65 ± 2.00	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.45 ± 0.60	K	NIST Webbook

tb	350.00 ± 2.00	K	NIST Webbook
tb	350.25 ± 1.00	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tc	548.90 ± 20.00	K	NIST Webbook
tc	523.20	K	NIST Webbook
tc	523.30 ± 0.05	K	NIST Webbook
tc	522.70 ± 2.00	K	NIST Webbook
tc	513.00 ± 6.00	K	NIST Webbook
tc	523.30	K	KDB
tc	523.29	K	Development of a Predictive Equation of State for CO <sub>2</sub> + Ethyl Ester Mixtures Based on Critical Points Measurements
tc	523.30 ± 1.00	K	NIST Webbook
tc	523.30 ± 1.00	K	NIST Webbook
tf	189.25	K	Aqueous Solubility Prediction Method
tf	189.50	K	KDB
tt	189.30 ± 0.20	K	NIST Webbook
tt	189.30 ± 0.05	K	NIST Webbook
vc	0.286	m <sup>3</sup> /kmol	KDB
zc	0.2551730		KDB
zra	0.25		KDB

## Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	149.47	J/mol×K	450.00	NIST Webbook
cpg	131.06	J/mol×K	380.00	NIST Webbook
cpg	125.82	J/mol×K	360.00	NIST Webbook
cpg	142.80	J/mol×K	425.00	NIST Webbook
cpg	136.22	J/mol×K	400.00	NIST Webbook
cpl	169.60	J/mol×K	298.15	NIST Webbook
cpl	169.60	J/mol×K	298.15	NIST Webbook
cpl	169.06	J/mol×K	298.15	NIST Webbook
cpl	169.30	J/mol×K	298.15	NIST Webbook
cpl	169.50	J/mol×K	298.10	NIST Webbook
cpl	168.82	J/mol×K	303.61	NIST Webbook
cpl	157.70	J/mol×K	290.00	NIST Webbook
cpl	169.20	J/mol×K	293.60	NIST Webbook
cpl	170.59	J/mol×K	298.32	NIST Webbook

cpl	168.94	J/mol×K	298.15	NIST Webbook
cpl	167.40	J/mol×K	298.15	NIST Webbook
dvisc	0.0004520	Paxs	293.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
dvisc	0.0004280	Paxs	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
dvisc	0.0003870	Paxs	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures

dvisc	0.0004030	Paxs	303.15	Density, dynamic viscosity, and derived properties of binary mixtures of methanol or ethanol with water, ethyl acetate, and methyl acetate at T = (293.15, 298.15, and 303.15) K
dvisc	0.0004260	Paxs	298.15	Density, dynamic viscosity, and derived properties of binary mixtures of methanol or ethanol with water, ethyl acetate, and methyl acetate at T = (293.15, 298.15, and 303.15) K
dvisc	0.0004030	Paxs	303.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
dvisc	0.0004430	Paxs	293.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004210	Paxs	298.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003990	Paxs	303.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters

dvisc	0.0003810	Paxs	308.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003630	Paxs	313.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003460	Paxs	318.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003300	Paxs	323.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003150	Paxs	328.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003010	Paxs	333.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0002880	Paxs	338.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0002750	Paxs	343.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003806	Paxs	303.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K

dvisc	0.0003622	Paxs	308.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K
dvisc	0.0003426	Paxs	313.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K
dvisc	0.0003790	Paxs	303.15	Volumetric and Transport Properties of Binary Liquid Mixtures of Phenylacetonitrile with Aliphatic Esters at Temperatures of (303.15 to 313.15) K
dvisc	0.0003610	Paxs	308.15	Volumetric and Transport Properties of Binary Liquid Mixtures of Phenylacetonitrile with Aliphatic Esters at Temperatures of (303.15 to 313.15) K
dvisc	0.0003440	Paxs	313.15	Volumetric and Transport Properties of Binary Liquid Mixtures of Phenylacetonitrile with Aliphatic Esters at Temperatures of (303.15 to 313.15) K

dvisc	0.0004520	Paxs	293.15	Density, dynamic viscosity, and derived properties of binary mixtures of methanol or ethanol with water, ethyl acetate, and methyl acetate at T = (293.15, 298.15, and 303.15) K
dvisc	0.0004260	Paxs	298.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
hfust	10.48	kJ/mol	189.30	NIST Webbook
hfust	10.48	kJ/mol	189.30	NIST Webbook
hfust	10.48	kJ/mol	189.30	NIST Webbook
hvapt	32.40 ± 0.10	kJ/mol	344.00	NIST Webbook
hvapt	31.90	kJ/mol	350.00	NIST Webbook
hvapt	34.00	kJ/mol	320.00	NIST Webbook
hvapt	31.00 ± 0.10	kJ/mol	363.00	NIST Webbook
hvapt	31.90 ± 0.10	kJ/mol	351.00	NIST Webbook
hvapt	33.80 ± 0.10	kJ/mol	326.00	NIST Webbook
hvapt	33.40 ± 0.10	kJ/mol	331.00	NIST Webbook
hvapt	31.40 ± 0.10	kJ/mol	343.00	NIST Webbook
hvapt	34.60 ± 0.10	kJ/mol	313.00	NIST Webbook
hvapt	36.70	kJ/mol	322.00	NIST Webbook
hvapt	35.70	kJ/mol	319.50	NIST Webbook
hvapt	34.10	kJ/mol	345.00	NIST Webbook
hvapt	31.94	kJ/mol	350.30	NIST Webbook
hvapt	32.22	kJ/mol	349.80	KDB
pvap	136.34	kPa	359.44	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	24.78	kPa	313.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	21.72	kPa	310.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	687.53	kPa	423.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	202.90	kPa	373.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	195.35	kPa	371.50	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	190.92	kPa	370.69	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	187.47	kPa	370.07	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)



pvap	184.43	kPa	369.49	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	180.88	kPa	368.83	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	176.37	kPa	367.98	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	174.65	kPa	367.64	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	171.33	kPa	367.00	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	167.81	kPa	366.29	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	28.18	kPa	316.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	160.53	kPa	364.81	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	157.94	kPa	364.25	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	155.58	kPa	363.72	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	150.43	kPa	362.62	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	146.37	kPa	361.73	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	142.55	kPa	360.88	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	139.07	kPa	360.03	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	31.95	kPa	319.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	133.45	kPa	358.74	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	130.00	kPa	357.92	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	127.89	kPa	357.35	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	124.00	kPa	356.37	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	122.31	kPa	355.91	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	120.68	kPa	355.50	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	118.56	kPa	354.93	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	116.46	kPa	354.43	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	114.65	kPa	353.91	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	111.21	kPa	352.94	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	108.13	kPa	352.12	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	106.84	kPa	351.77	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	104.65	kPa	351.12	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	101.32	kPa	350.15	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	100.68	kPa	349.93	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	100.07	kPa	349.76	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	99.36	kPa	349.56	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	98.97	kPa	349.45	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	96.74	kPa	348.75	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	94.63	kPa	348.09	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	90.81	kPa	346.86	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	86.85	kPa	345.53	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	82.56	kPa	344.11	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	79.83	kPa	343.03	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	76.02	kPa	341.69	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	72.26	kPa	340.23	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	69.34	kPa	339.09	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	36.12	kPa	322.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	40.73	kPa	325.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	45.80	kPa	328.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	51.36	kPa	331.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	57.46	kPa	334.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	64.13	kPa	337.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	71.40	kPa	340.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa



pvap	79.32	kPa	343.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	87.93	kPa	346.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	97.26	kPa	349.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	107.36	kPa	352.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	66.49	kPa	337.91	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	62.83	kPa	336.33	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	59.91	kPa	335.02	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	55.72	kPa	333.07	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	52.56	kPa	331.51	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	49.27	kPa	329.77	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	44.98	kPa	327.41	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	40.61	kPa	324.80	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	38.43	kPa	323.47	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	34.85	kPa	321.01	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	31.33	kPa	318.46	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	27.63	kPa	315.44	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	24.34	kPa	312.53	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	22.44	kPa	310.67	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	20.64	kPa	308.86	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	18.33	kPa	306.25	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	16.04	kPa	303.35	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	11.89	kPa	297.17	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	25.30	kPa	313.15	Isothermal Vapor-Liquid Equilibria of ethyl acetate + dibromomethane, or + bromochloromethane or + 1,2-dichloroethane or +1-bromo-2-chloroethane at T = 313.15 K
pvap	25.08	kPa	313.15	Total Vapor Pressure Measurements for 2-Ethoxyethanol with Methyl Acetate, Ethyl Acetate, Propyl Acetate, and Ethyl Propionate at 313.15 K and for 2-Ethoxyethanol with Methyl Formate at 308.15 K

pvap	50.00	kPa	330.01	Isobaric Vapor Liquid Equilibria for Binary Mixtures of Isoamyl Acetate + Ethyl Acetate at 50 and 100 kPa
pvap	100.00	kPa	349.53	Isobaric Vapor Liquid Equilibria for Binary Mixtures of Isoamyl Acetate + Ethyl Acetate at 50 and 100 kPa
pvap	118.27	kPa	355.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	130.03	kPa	358.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	134.15	kPa	359.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	101.30	kPa	350.28	Isobaric Vapor-Liquid Phase Equilibrium Measurements for Allyl Alcohol with Chloroform, Ethyl Acetate, and Methyl Propionate at 101.3 kPa
pvap	101.30	kPa	349.95	Effect of Ionic Liquids on the Binary Vapor-Liquid Equilibrium of Ethyl Acetate + Methanol System at 101.3 kPa

pvap	45.95	kPa	328.15	Isothermal Vapor-Liquid Equilibria for Binary Mixtures of Methyl Nonafluorobutyl Ether + Acetone, Cyclopentyl Methyl Ether, Ethyl Acetate, n-Heptane, Methanol, and Toluene
pvap	111.76	kPa	353.15	Vapor Liquid Equilibrium and Excess Enthalpy Data for Systems Containing N,N-Dimethylacetamide
pvap	1500.00	kPa	462.75	Measurement and modeling of high pressure VLE for methyl acetate or ethyl acetate with 2-butanol. Isobaric data at 1.5 MPa
pvap	101.30	kPa	350.35	Isobaric Vapor - Liquid Equilibrium for Ethyl acetate + Methanol + Ionic Liquids Ternary systems at 101.3 kPa
pvap	31.37	kPa	318.40	Vapour liquid equilibrium for the ethyl ethanoate + 1-butene, +cis-2-butene, +trans-2-butene, +2-methylpropene, +n-butane and +2-methylpropane
pvap	101.30	kPa	350.29	Isobaric vapor-liquid equilibrium of a ternary system of ethyl acetate + propyl acetate + dimethyl sulfoxide and binary systems of ethyl acetate + dimethyl sulfoxide and propyl acetate + dimethyl sulfoxide at 101.3 kPa

pvap	1222.70	kPa	452.30	Isothermal (vapour + liquid) equilibrium (VLE) for binary mixtures containing diethyl carbonate, phenyl acetate, diphenyl carbonate, or ethyl acetate
pvap	557.10	kPa	412.80	Isothermal (vapour + liquid) equilibrium (VLE) for binary mixtures containing diethyl carbonate, phenyl acetate, diphenyl carbonate, or ethyl acetate
pvap	205.70	kPa	373.00	Isothermal (vapour + liquid) equilibrium (VLE) for binary mixtures containing diethyl carbonate, phenyl acetate, diphenyl carbonate, or ethyl acetate
pvap	101.30	kPa	350.15	The isobaric vapor liquid equilibria of ethyl acetate p acetonitrile p bis(trifluoromethylsulfonyl)imide-based ionic liquids at 101.3 kPa
pvap	93.32	kPa	347.70	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	79.99	kPa	343.18	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components

pvap	66.66	kPa	337.99	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	53.33	kPa	331.90	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	40.00	kPa	324.44	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	163.99	kPa	365.52	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
rfi	1.36920		298.15	Thermodynamic study of (alkyl esters + a,x-alkyl dihalides) I: HE and V E for 25 binary mixtures $\{x\text{C}_u-1\text{H}_{2u-1}\text{CO}_2\text{C}_2\text{H}_5 + (1-x)\text{a},x\text{-ClCH}_2(\text{CH}_2)_v-2\text{CH}_2\text{Cl}\}$ , where $u = 1$ to $5$ , $a = 1$ and $v = x = 2$ to $6$
rfi	1.37244		298.15	Isobaric Vapor-Liquid Equilibrium Data for Binary Systems of Anisole with Methyl Acetate, Ethyl Acetate, n-Propyl Acetate, and Isopropyl Acetate at 93.9 kPa



rfi	1.36981	298.15	Measurement of VLE Data by Using an Experimental Installation with Automatic Control: Modeling of Binary Systems of Methyl Acetate or Ethyl Acetate with n-Heptane or 2,2,4-Trimethylpentane at Both 0.1 and 1.5 MPa
rfi	1.36980	298.15	Density, Refractive Index, and Speed of Sound at 298.15 K and Vapor-Liquid Equilibria at 101.3 kPa for Binary Mixtures of Ethyl Acetate + 1-Pentanol and Ethanol + 2-Methyl-1-propanol
rfi	1.37130	298.15	Density, Viscosity, Refractive Index, and Speed of Sound for Binary Mixtures of 1,4-Dioxane with Different Organic Liquids at (298.15, 303.15, and 308.15) K
rfi	1.36730	303.15	Density, Viscosity, Refractive Index, and Speed of Sound for Binary Mixtures of 1,4-Dioxane with Different Organic Liquids at (298.15, 303.15, and 308.15) K
rfi	1.36310	308.15	Density, Viscosity, Refractive Index, and Speed of Sound for Binary Mixtures of 1,4-Dioxane with Different Organic Liquids at (298.15, 303.15, and 308.15) K

rfi	1.36990	298.15	Densities, Viscosities, and Refractive Indices for Binary and Ternary Mixtures of N,N-Dimethylacetamide (1) + 2-Methylbutan-2-ol (2) + Ethyl Acetate (3) at 298.15 K for the Liquid Region and at Ambient Pressure
rfi	1.36978	298.15	Density, Refractive Index, Speed of Sound at 298.15 K, and Vapor-Liquid Equilibria at 101.3 kPa for Binary Mixtures of Ethyl Acetate + Ethyl Lactate and Methyl Acetate + Ethyl Lactate
rfi	1.36978	298.15	Liquid-Liquid Equilibrium Diagrams of Ethanol + Water + (Ethyl Acetate or 1-Pentanol) at Several Temperatures
rfi	1.37190	293.15	Solubilities of Some Phosphaspirocyclic Compounds in Selected Solvents
rfi	1.37241	293.15	Thermodynamic Properties of Ionic Liquids in Organic Solvents from (293.15 to 303.15) K
rfi	1.36977	298.15	Thermodynamic Properties of Ionic Liquids in Organic Solvents from (293.15 to 303.15) K
rfi	1.36712	303.15	Thermodynamic Properties of Ionic Liquids in Organic Solvents from (293.15 to 303.15) K

rfi	1.37190	293.15	Solubilities of Phosphorus-Containing Compounds in Selected Solvents
rfi	1.37000	298.15	Vapor-Liquid Equilibria for Ethyl Acetate + Methanol at (0.1, 0.5, and 0.7) MPa. Measurements with a New Ebulliometer
rfi	1.37010	293.15	Liquid-Liquid Equilibrium of (Water + Pentane-2,4-dione + Ethyl Ethanoate) and (Water + Pentane-2,4-dione + Cyclohexane) at (298.15 and 313.15) K
rfi	1.37120	298.15	Determination and Correlation of Vapor Liquid Equilibrium Data for the Ethyl Acetate + Hexamethyl Disiloxane System at 101.3 kPa
rfi	1.35880	293.15	Solubilities of Triphenylphosphine Oxide in Selected Solvents
rfi	1.36983	298.15	Physical Properties of Binary and Ternary Mixtures of Ethyl Acetate, Ethanol, and 1-Octyl-3-methyl-imidazolium Bis(trifluoromethylsulfonyl)imide at 298.15 K
rfi	1.35880	293.15	Solubilities of Methyl-diphenylphosphine Oxide in Selected Solvents

rfi	1.37519	288.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.36994	298.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.36460	308.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.36980	298.15	Vapor-Liquid Equilibrium Data for Binary Mixtures of Dimethyl Carbonate with Methyl Acetate, Ethyl Acetate, n-Propyl Acetate, Isopropyl Acetate, n-Butyl Acetate, and Isoamyl Acetate at 93.13 kPa
rfi	1.35368	328.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K

rfi	1.36640	303.15	Densities, speeds of sound, isentropic compressibilities, refractive indexes, and viscosities of tetrahydrofuran with haloalkane or alkyl ethanoate at T = 303.15 K
rfi	1.36750	303.15	Liquid-liquid equilibrium for ternary systems of ethyl acetate/isopropyl acetate + 2,2,3,3-tetrafluoro-1-propanol + water at 298.15, 318.15 K
rfi	1.36720	303.15	Density, refraction index and vapor-liquid equilibria of N-methyl-2-hydroxyethylammonium butyrate plus (methyl acetate or ethyl acetate or propyl acetate) at several temperatures
rfi	1.37000	298.15	Correlation and prediction of mixing thermodynamic properties of ester-containing systems: Ester + alkane and ester + ester binary systems and the ternary dodecane + ethyl pentanoate + ethyl ethanoate
rfi	1.36977	298.15	Ternary (liquid + liquid) equilibria of the azeotrope (ethyl acetate + 2-propanol) with different ionic liquids at T = 298.15 K
rfi	1.36712	303.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures

rfi	1.36977	298.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.37241	293.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.37270	298.15	Effects of the presence of ethylacetate or benzene on the densities and volumetric properties of mixture (styrene + N,N-dimethylformamide)
rfi	1.37000	298.15	Molecular interactions in (2,4,6-trimethyl-1,3,5-trioxane + n-alkyl acetates) at T=(298.15, 303.15, and 308.15) K
rfi	1.36977	298.15	Properties of ionic liquid HMIMPF6 with carbonates, ketones and alkyl acetates
rfi	1.35970	318.15	Thermodynamic properties of (an ester + an alkane). XVI. Experimental HEm and V Em values and a new correlation method for (an alkyl ethanoate + an n-alkane) at 318.15 K
rfi	1.37240	293.15	A novel static analytical apparatus for phase equilibrium measurements
rfi	1.35940	318.20	Experimental and calculated liquid-liquid equilibrium data for water + furfural + solvents

rfi	1.36720		303.20	Experimental and calculated liquid-liquid equilibrium data for water + furfural + solvents
rfi	1.37490		288.20	Experimental and calculated liquid-liquid equilibrium data for water + furfural + solvents
rfi	1.37020		293.20	Vapor liquid equilibria for the ternary system of carbon dioxide + ethanol + ethyl acetate at elevated pressures
rfi	1.35919		318.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rhol	856.81	kg/m3	328.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	888.75	kg/m3	303.15	Excess Volumes and Excess Isentropic Compressibilities of Binary Liquid Mixtures of Trichloroethylene with Esters at 303.15 K
rhol	894.40	kg/m3	298.15	Revision of the volumetric method for measurements of liquid liquid equilibria in binary systems

rho1	894.60	kg/m3	298.15	Experimental Determination of Densities and Isobaric Vapor Liquid Equilibria of Methyl Acetate and Ethyl Acetate with Alcohols (C3 and C4) at 0.3 MPa
rho1	906.55	kg/m3	288.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rho1	894.38	kg/m3	298.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rho1	875.81	kg/m3	313.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rho1	901.00	kg/m3	293.00	KDB
rho1	897.72	kg/m3	298.15	Effect of Inorganic Salts on the Isobaric Vapor Liquid Equilibrium of the Ethyl Acetate Ethanol System



rho1	843.86	kg/m3	338.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rho1	830.62	kg/m3	348.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rho1	900.48	kg/m3	293.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rho1	894.36	kg/m3	298.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rho1	888.19	kg/m3	303.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rho1	881.98	kg/m3	308.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures

rho1	875.73	kg/m3	313.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rho1	900.57	kg/m3	293.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
rho1	876.10	kg/m3	313.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
rho1	894.51	kg/m3	298.15	Standard partial molar volumes of some electrolytes in ethylene carbonate based mixtures
rho1	900.26	kg/m3	293.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rho1	894.14	kg/m3	298.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rho1	875.10	kg/m3	313.15	Ternary Excess Molar Volumes of {Methyltrioctylammonium Bis[(trifluoromethyl)sulfonyl]imide + Methanol + Methyl Acetate or Ethyl Acetate} Systems at (298.15, 303.15, and 313.15) K

rho	888.50	kg/m <sup>3</sup>	303.15	Ternary Excess Molar Volumes of {Methyltrioctylammonium Bis[(trifluoromethyl)sulfonyl]imide + Methanol + Methyl Acetate or Ethyl Acetate} Systems at (298.15, 303.15, and 313.15) K
rho	894.70	kg/m <sup>3</sup>	298.15	Ternary Excess Molar Volumes of {Methyltrioctylammonium Bis[(trifluoromethyl)sulfonyl]imide + Methanol + Methyl Acetate or Ethyl Acetate} Systems at (298.15, 303.15, and 313.15) K
rho	893.90	kg/m <sup>3</sup>	298.40	Vapor Liquid Equilibrium at 350 K, Excess Molar Enthalpies at 298 K, and Excess Molar Volumes at 298 K of Binary Mixtures Containing Ethyl Acetate, Butyl Acetate, and 2-Butanol
rho	881.52	kg/m <sup>3</sup>	308.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rho	894.40	kg/m <sup>3</sup>	298.15	Liquid-Liquid Equilibrium in Ternary Systems Containing Ethylene Glycol, Monofunctional Benzene Derivative, and Ethyl Acetate
rho	876.25	kg/m <sup>3</sup>	313.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)

rhoI	882.48	kg/m <sup>3</sup>	308.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhoI	888.66	kg/m <sup>3</sup>	303.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhoI	894.79	kg/m <sup>3</sup>	298.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhoI	900.88	kg/m <sup>3</sup>	293.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhoI	899.50	kg/m <sup>3</sup>	298.15	Isobaric Vapor-liquid Equilibrium for Three Binary Systems of Ethyl Acetate + Propyl Acetate, Ethyl Acetate + Propylene Carbonate, and Propyl Acetate + Propylene Carbonate at 101.3 kPa
rhoI	863.30	kg/m <sup>3</sup>	323.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K

rhoI	869.62	kg/m3	318.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	875.88	kg/m3	313.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	882.09	kg/m3	308.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	888.26	kg/m3	303.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K

rhoI	894.37	kg/m3	298.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	900.44	kg/m3	293.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	876.30	kg/m3	313.15	Apparent molar volume and apparent molar isentropic compressibility for the binary systems {methyltrioctylammoniumbis(trifluoromethylsulfonyl)imide + ethyl acetate or ethanol} at different temperatures underatmospheric pressure
rhoI	882.70	kg/m3	308.15	Apparent molar volume and apparent molar isentropic compressibility for the binary systems {methyltrioctylammoniumbis(trifluoromethylsulfonyl)imide + ethyl acetate or ethanol} at different temperatures underatmospheric pressure

rho	887.85	kg/m <sup>3</sup>	303.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rho	894.40	kg/m <sup>3</sup>	298.15	Apparent molar volume and apparent molar isentropic compressibility for the binary systems {methyltrioctylammoniumbis(trifluoromethylsulfonyl)imide + ethyl acetate or ethanol} at different temperatures under atmospheric pressure
rho	888.50	kg/m <sup>3</sup>	303.15	Volumetric and transport properties of ternary mixtures containing 1-alkanol + ethyl ethanoate + cyclohexane at 303.15 K: Experimental data, correlation and prediction by ERAS model
rho	888.50	kg/m <sup>3</sup>	303.15	Volumetric and transport properties of ternary mixtures containing 1-propanol + ethyl ethanoate + cyclohexane or benzene at 303.15 K: Experimental data, correlation and prediction by ERAS model
rho	888.42	kg/m <sup>3</sup>	303.15	Studies of viscosities of dilute solutions of alkylamine in non-electrolyte solvents. II. Haloalkanes and other polar solvents

rho1	894.40	kg/m <sup>3</sup>	298.15	Measurement and correlation of solubility and solution thermodynamics of 1,3-dimethylurea in different solvents from T = (288.15 to 328.15) K
rho1	893.40	kg/m <sup>3</sup>	298.15	Solubility and solution thermodynamics of sorbic acid in eight pure organic solvents
rho1	894.50	kg/m <sup>3</sup>	298.15	(Liquid + liquid) equilibria for mixtures of dodecane and ethanol with alkylsulfate-based ionic liquids
rho1	863.36	kg/m <sup>3</sup>	323.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [C <sub>n</sub> mim][PF <sub>6</sub> ] (n = 6, 8) and alkyl acetates
rho1	869.68	kg/m <sup>3</sup>	318.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [C <sub>n</sub> mim][PF <sub>6</sub> ] (n = 6, 8) and alkyl acetates
rho1	875.95	kg/m <sup>3</sup>	313.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [C <sub>n</sub> mim][PF <sub>6</sub> ] (n = 6, 8) and alkyl acetates
rho1	882.17	kg/m <sup>3</sup>	308.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [C <sub>n</sub> mim][PF <sub>6</sub> ] (n = 6, 8) and alkyl acetates



rhoI	888.35	kg/m <sup>3</sup>	303.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhoI	894.47	kg/m <sup>3</sup>	298.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhoI	900.57	kg/m <sup>3</sup>	293.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhoI	875.14	kg/m <sup>3</sup>	313.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhoI	888.50	kg/m <sup>3</sup>	303.15	Apparent molar volume and apparent molar isentropic compressibility for the binary systems {methyltrioctylammonium bis(trifluoromethylsulfonyl)imide + ethyl acetate or ethanol} at different temperatures under atmospheric pressure
rhoI	851.36	kg/m <sup>3</sup>	332.70	Isothermal vapor liquid equilibria for different binary mixtures involved in the alcoholic distillation
sfust	55.27	J/mol×K	189.30	NIST Webbook

speedsl	1098.43	m/s	308.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K
speedsl	1098.00	m/s	308.15	Density and Speed of Sound of Binary Mixtures of N-Methylacetamide with Ethyl Acetate, Ethyl Chloroacetate, and Ethyl Cyanoacetate in the Temperature Interval (303.15 to 318.15) K
speedsl	1081.00	m/s	313.15	Density and Speed of Sound of Binary Mixtures of N-Methylacetamide with Ethyl Acetate, Ethyl Chloroacetate, and Ethyl Cyanoacetate in the Temperature Interval (303.15 to 318.15) K
speedsl	1058.00	m/s	318.15	Density and Speed of Sound of Binary Mixtures of N-Methylacetamide with Ethyl Acetate, Ethyl Chloroacetate, and Ethyl Cyanoacetate in the Temperature Interval (303.15 to 318.15) K
speedsl	1120.80	m/s	303.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K

speedsl	1119.00	m/s	303.15	Density and Speed of Sound of Binary Mixtures of N-Methylacetamide with Ethyl Acetate, Ethyl Chloroacetate, and Ethyl Cyanoacetate in the Temperature Interval (303.15 to 318.15) K
speedsl	1143.23	m/s	298.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K
speedsl	1187.92	m/s	288.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K
speedsl	1165.80	m/s	293.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K
srf	0.03	N/m	323.20	KDB
srf	0.02	N/m	298.15	Surface Tension Data of Aqueous Binary Mixtures of Methyl, Ethyl, Propyl, and Butyl Acetates at 298.15 K

srf	0.02	N/m	298.15	Concentration Dependence of Surface Tension for Very Dilute Aqueous Solutions of Organic Non-Electrolytes
tcondl	0.13	W/m×K	333.37	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	323.25	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	328.39	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	318.40	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	338.34	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	343.27	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.12	W/m×K	345.43	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.12	W/m×K	348.46	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	313.45	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase

tcondl	0.14	W/m×K	303.53	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	298.52	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	295.44	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.15	W/m×K	290.42	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.15	W/m×K	285.31	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.15	W/m×K	281.34	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.15	W/m×K	274.35	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.15	W/m×K	268.04	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.16	W/m×K	260.17	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.16	W/m×K	253.89	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase

tcondl	0.16	W/m×K	249.13	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	308.44	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase

## Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbp	332.82	K	54.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	335.16	K	59.98	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	339.42	K	70.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	340.92	K	75.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	343.18	K	80.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil

tbp	344.93	K	84.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	346.58	K	89.91	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	348.20	K	95.01	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	351.26	K	104.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	352.67	K	109.98	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	355.36	K	119.90	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	356.62	K	124.98	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	357.86	K	129.93	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	359.08	K	134.95	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil

tbp	360.24	K	139.96	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	362.48	K	149.95	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	363.56	K	154.97	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	364.60	K	159.96	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	365.64	K	164.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	367.61	K	174.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	368.58	K	180.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	369.50	K	185.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil



# Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.47020e+01
Coeff. B	-3.08216e+03
Coeff. C	-4.45420e+01
Temperature range (K), min.	258.37
Temperature range (K), max.	372.76

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C \cdot \ln(T) + D \cdot T^2$
Coeff. A	8.09498e+01
Coeff. B	-6.86243e+03
Coeff. C	-9.83731e+00
Coeff. D	7.27641e-06
Temperature range (K), min.	189.60
Temperature range (K), max.	523.30

# Datasets

## Mass density, kg/m<sup>3</sup>

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m <sup>3</sup> - Liquid
298.15	100.00	894.0
298.15	1000.00	894.7
298.15	2000.00	895.7
298.15	3000.00	896.7
298.15	3800.00	897.4
298.15	5000.00	898.8
298.15	10000.00	903.4
298.15	15000.00	907.7
298.15	20000.00	912.0

298.15	25000.00	916.1
298.15	30000.00	921.1
298.15	35000.00	926.3
303.15	100.00	887.6
303.15	1000.00	888.5
303.15	2000.00	889.5
303.15	3000.00	890.5
303.15	3800.00	891.3
303.15	5000.00	892.7
303.15	10000.00	897.5
303.15	15000.00	902.0
303.15	20000.00	906.3
303.15	25000.00	910.7
303.15	30000.00	915.9
303.15	35000.00	921.2
308.15	100.00	881.4
308.15	1000.00	882.3
308.15	2000.00	883.3
308.15	3000.00	884.4
308.15	3800.00	885.3
308.15	5000.00	886.7
308.15	10000.00	891.7
308.15	15000.00	896.4
308.15	20000.00	900.9
308.15	25000.00	905.4
308.15	30000.00	910.7
308.15	35000.00	916.2
313.15	100.00	875.2
313.15	1000.00	876.1
313.15	2000.00	877.2
313.15	3000.00	878.3
313.15	3800.00	879.2
313.15	5000.00	880.6
313.15	10000.00	885.8
313.15	15000.00	890.7
313.15	20000.00	895.4
313.15	25000.00	899.8
313.15	30000.00	905.3
313.15	35000.00	910.9
318.15	100.00	868.8
318.15	1000.00	869.8
318.15	2000.00	871.0
318.15	3000.00	872.2
318.15	3800.00	873.1

318.15	5000.00	874.5
318.15	10000.00	880.0
318.15	15000.00	885.1
318.15	20000.00	889.8
318.15	25000.00	894.5
318.15	30000.00	900.1
318.15	35000.00	905.9
323.15	100.00	862.7
323.15	1000.00	864.0
323.15	2000.00	865.1
323.15	3000.00	866.2
323.15	3800.00	867.1
323.15	5000.00	868.6
323.15	10000.00	874.2
323.15	15000.00	879.4
323.15	20000.00	884.3
323.15	25000.00	889.2
323.15	30000.00	895.0
323.15	35000.00	900.9
328.15	100.00	856.4
328.15	1000.00	857.8
328.15	2000.00	859.2
328.15	3000.00	860.5
328.15	3800.00	861.5
328.15	5000.00	862.5
328.15	10000.00	868.4
328.15	15000.00	873.9
328.15	20000.00	879.0
328.15	25000.00	884.1
328.15	30000.00	890.1
328.15	35000.00	896.2
333.15	100.00	850.4
333.15	1000.00	851.7
333.15	2000.00	853.0
333.15	3000.00	854.4
333.15	3800.00	855.4
333.15	5000.00	856.8
333.15	10000.00	862.9
333.15	15000.00	868.5
333.15	20000.00	873.8
333.15	25000.00	879.0
333.15	30000.00	885.2
333.15	35000.00	891.4
338.15	100.00	844.0

338.15	1000.00	845.4
338.15	2000.00	846.8
338.15	3000.00	848.2
338.15	3800.00	849.3
338.15	5000.00	850.8
338.15	10000.00	857.1
338.15	15000.00	863.0
338.15	20000.00	868.5
338.15	25000.00	873.9
338.15	30000.00	880.3
338.15	35000.00	886.7
343.15	100.00	837.5
343.15	1000.00	839.1
343.15	2000.00	840.6
343.15	3000.00	842.0
343.15	3800.00	843.2
343.15	5000.00	844.5
343.15	10000.00	851.2
343.15	15000.00	857.3
343.15	20000.00	863.0
343.15	25000.00	868.5
343.15	30000.00	875.1
343.15	35000.00	881.6
348.15	100.00	829.4
348.15	1000.00	830.5
348.15	2000.00	832.3
348.15	3000.00	833.8
348.15	3800.00	835.0
348.15	5000.00	836.8
348.15	10000.00	845.5
348.15	15000.00	851.8
348.15	20000.00	857.7
348.15	25000.00	863.5
348.15	30000.00	870.2
348.15	35000.00	877.0
353.15	1000.00	824.3
353.15	2000.00	826.0
353.15	3000.00	827.5
353.15	3800.00	828.8
353.15	5000.00	830.6
353.15	10000.00	837.7
353.15	15000.00	844.3
353.15	20000.00	850.4
353.15	25000.00	856.1

353.15	30000.00	862.7
353.15	35000.00	869.6
358.15	1000.00	818.4
358.15	2000.00	820.0
358.15	3000.00	821.6
358.15	3800.00	822.8
358.15	5000.00	824.7
358.15	10000.00	832.1
358.15	15000.00	838.9
358.15	20000.00	845.2
358.15	25000.00	851.0
358.15	30000.00	857.6
358.15	35000.00	864.7
363.15	1000.00	811.8
363.15	2000.00	813.5
363.15	3000.00	815.3
363.15	3800.00	816.6
363.15	5000.00	818.5
363.15	10000.00	826.3
363.15	15000.00	833.3
363.15	20000.00	839.7
363.15	25000.00	845.8
363.15	30000.00	852.9
363.15	35000.00	860.2
368.15	1000.00	804.9
368.15	2000.00	806.8
368.15	3000.00	808.6
368.15	3800.00	810.0
368.15	5000.00	812.1
368.15	10000.00	820.2
368.15	15000.00	827.5
368.15	20000.00	834.3
368.15	25000.00	840.6
368.15	30000.00	848.0
368.15	35000.00	855.5
373.15	1000.00	798.5
373.15	2000.00	800.4
373.15	3000.00	802.4
373.15	3800.00	803.8
373.15	5000.00	806.0
373.15	10000.00	814.4
373.15	15000.00	822.0
373.15	20000.00	829.0
373.15	25000.00	835.5

373.15	30000.00	843.0
373.15	35000.00	850.6
378.15	1000.00	791.8
378.15	2000.00	793.8
378.15	3000.00	795.8
378.15	3800.00	797.3
378.15	5000.00	799.6
378.15	10000.00	808.5
378.15	15000.00	816.5
378.15	20000.00	823.7
378.15	25000.00	830.5
378.15	30000.00	838.4
378.15	35000.00	846.3
383.15	1000.00	784.8
383.15	2000.00	787.1
383.15	3000.00	789.1
383.15	3800.00	790.8
383.15	5000.00	793.2
383.15	10000.00	802.4
383.15	15000.00	810.7
383.15	20000.00	818.2
383.15	25000.00	825.3
383.15	30000.00	833.5
383.15	35000.00	841.6
388.15	1000.00	778.2
388.15	2000.00	780.5
388.15	3000.00	782.7
388.15	3800.00	784.4
388.15	5000.00	786.9
388.15	10000.00	796.4
388.15	15000.00	805.1
388.15	20000.00	813.0
388.15	25000.00	820.3
388.15	30000.00	828.8
388.15	35000.00	837.2
393.15	1000.00	771.0
393.15	2000.00	773.5
393.15	3000.00	775.9
393.15	3800.00	777.7
393.15	5000.00	780.4
393.15	10000.00	790.5
393.15	15000.00	799.4
393.15	20000.00	807.6
393.15	25000.00	815.2

393.15

30000.00

823.9

393.15

35000.00

832.4

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**Separation of binary mixtures based on gamma infinity data using the NRTL and the thermodynamic Modeling of Solid-Liquid Phase Equilibrium for Organic Acid in the water-ethanol, methanol-propan-2-ol, acetone-methanol, ethyl acetate, and Ethyl acetate-propan-2-ol binary mixtures at the critical temperature at infinite, 15 to 323.15 K** <https://www.doi.org/10.1016/j.fluid.2015.03.036>

**Equilibrium Vapor Pressure and Apparent Molar Density of *p*-Nitrobenzoic Acid in Different Organic Solvents and Fluoromethylsulfonylimide** <https://www.doi.org/10.1016/j.jct.2017.12.012>

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**Determination and Correlation of Solubility of *p*-Nitrobenzoic Acid in Different Organic Solvents and Fluoromethylsulfonylimide** <https://www.doi.org/10.1021/acs.jced.8b00632>

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**Determination and Correlation of Solubility of *p*-Nitrobenzoic Acid in Different Organic Solvents and Fluoromethylsulfonylimide** <https://www.doi.org/10.1016/j.fluid.2018.06.003>

**Determination and Correlation of Solubility of *p*-Nitrobenzoic Acid in Different Organic Solvents and Fluoromethylsulfonylimide** <https://www.doi.org/10.1021/je200822w>

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Acetates in the Direct Esterification of Acetyl Chloride with Hydrogen Sulfate in Different Pure Solvents https://www.doi.org/10.1016/j.jct.2011.11.009





Solid Liquid Equilibrium and Phase Diagram for the Ternary

Thermodynamic Models for + Determination of the Solubility

Behavior of Plasmonic in Five

Solubility of  $\gamma$ -butyric acid in

Different Pure Solvents and

Binary or Ternary Binary

Methylacetate + Ethylacetate +

Diethylacetate and Binary

Methylacetate + Ethylacetate +

Diethylacetate Binary Mixtures:

Viscosities, Speeds of Sound, Excess

Solubility of Tripropyl Hydrogen

Fluoride in Acetone, Acetonitrile,

Methylacetate, Ethylacetate, and

Diethylacetate Binary and Ternary

Mixtures: Thermodynamic Properties

of Methylacetate + Ethylacetate +

Diethylacetate Binary Mixtures

at 298.15 K: Coumaric Acid in Nine

Pure and Mixed + Ethanol Mixed

Solvents at Temperatures from 293.15

to 333.15 K: Vapor-Liquid Behavior and

Saturated Pressure for Carbon Dioxide +

Ethylacetate Vapor-Liquid Equilibria

for K: Binary Mixtures of Isoamyl

Acetate + Benzylacetate and n-Propyl

acetate + Benzylacetate Binary

Mixtures: Vapor-Liquid Equilibria

of Vapor-Liquid Equilibria of

Binary Mixtures of Ethylacetate +

Diethylacetate + Ethylacetate +

Diethylacetate Binary Mixtures:

Thermodynamic Properties of

Binary Mixtures of Ethylacetate +

Diethylacetate Binary Mixtures:

Thermodynamic Properties of

Binary Mixtures of Ethylacetate +

Diethylacetate Binary Mixtures:

Thermodynamic Properties of

Binary Mixtures of Ethylacetate +

Diethylacetate Binary Mixtures:

Thermodynamic Properties of

Binary Mixtures of Ethylacetate +

<https://www.doi.org/10.1021/je3013588>

<https://www.doi.org/10.1021/acs.jced.5b00758>

<https://www.doi.org/10.1021/je8006088>

<https://www.doi.org/10.1021/je060452c>

<https://www.doi.org/10.1021/acs.jced.6b00721>

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<https://www.doi.org/10.1021/je900711h>

<https://www.doi.org/10.1016/j.jct.2018.05.017>

[HMMIM][BF4]:



Separation of binary mixtures based on limiting activity coefficients data using investigation of Surface Properties and Solubility of thermodynamic parameters of ester-monomer-maleide model of soil-organic-matter functional groups in 1,3-dichloropropane in pure solvents Carbon Dioxide with 2-butanol and 2-propanol or some 2-butanol and 2-propanol (water) systems and data Correlation of BSA protein in Different Monosolvents Activity Coefficients at Infinite Dilution for Hydrocarbons in Fatty Alcohols Systems and Ionic Liquid Interactions of Ternary mixtures by density, viscosity and phase Equilibrium of the Ternary System Methanol + Ethyl + 4-methylphenol and the effect of interaction between 200 and 308.15) K and the effect of methanide coefficients at infinite dilution for organic compounds and effect of the Pyridine-3-amine Solubility in Eight Binary Ionic Liquids in extraction of piperidine (283.15 to 313.15) K using activity coefficients and phase liquid equilibrium for binary systems Solubility of close-boiling 1-(6-bromohexyl)-6,7,8,9-tetrahydrophenanthro[1,2-b]furan-10,11-dione Experiment and correlation of liquid-liquid equilibrium data for water in the dilute region: activity coefficients of volatile organic compounds in two solvents composition of various Organic Solvents from (301 to 313) K: 1-methyl-2-pyrrolidone and Naringin in Different Solvents and Dissociation Constants of Naringin in Metastable Zone Width of the (1,4-Dioxan-2-one + 2-methyl-2-butanol) System: Measurement and correlation of the solubility of maleic acid in acetone-ethyl acetate binary mixture: separation on investigation of limiting activity coefficients and Thermodynamic Analysis of the Solubility of Limonin in High Organic Solvents and High pressure VLE for mixtures of solvents and organic liquids: Equilibrium of ethyl acetate + dibromomethane, or + bromodichloromethane on data for water + formic acid - solvent (butyl acetate, 2-propanol, 2-methyl-2-butanol) Experimental Data for Systems Containing Non-Difficult Water Correlation, and Solvent Effect of Liquid-Liquid Equilibria of (water-2-Propanol-solvent) at T = 298.2K: Measurement and Correlation of the Solubility of Enrofloxacin in Different Solvents from 298.15 to 318.15 K: Solubility Measurement and Phase Equilibrium Modeling of Solubility of 2-mercapto-2-phenylacetic Acid Potassium in Organic Solvents and Binary Water-2-Ethylhexanone in Binary Mixtures of Oligocymene Derivatives with Different Number of Methylene Groups and Correlation of Dissociation and Model Correlation of Dissociation and Correlation of Pure Solvents of 3,5-dimethyl-1,2,4-triazolate] Determination of Salt (CBNT) in Various Solvents and Binary Mixtures of Organic Solvents: mixtures of acetone, ethyl acetate, 2-propanol + 2-methyl-2-butanol Binary System of 2-Propanol + 2-methyl-2-butanol and Ethyl Hexanoate Thermodynamic Modeling of 2-mercapto-2-phenylacetic acid in twelve binary solvent mixtures at 298.2 (283.15-318.15) K and mixing properties of solutions:

<https://www.doi.org/10.1016/j.fluid.2017.12.029>  
<https://www.doi.org/10.1021/je500205z>  
<https://www.doi.org/10.1016/j.jct.2016.03.007>  
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<https://www.doi.org/10.1021/je300517q>  
<https://www.doi.org/10.1016/j.fluid.2018.09.024>  
<https://www.doi.org/10.1016/j.fluid.2007.01.042>  
<https://www.doi.org/10.1021/je800238y>  
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<https://www.doi.org/10.1016/j.jct.2013.05.035>  
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<https://www.doi.org/10.1021/je501004g>  
<https://www.doi.org/10.1021/je050149w>  
<https://www.doi.org/10.1021/acs.jced.9b00353>  
<https://www.doi.org/10.1021/acs.jced.9b00432>  
<https://www.doi.org/10.1016/j.tca.2012.03.023>  
<https://www.doi.org/10.1016/j.fluid.2017.06.001>  
<https://www.doi.org/10.1021/acs.jced.7b00851>  
<https://www.doi.org/10.1021/acs.jced.5b00773>  
<https://www.doi.org/10.1021/je034259j>  
<https://www.doi.org/10.1016/j.fluid.2016.01.045>  
<https://www.doi.org/10.1021/acs.jced.7b00119>  
<https://www.doi.org/10.1021/acs.jced.8b01226>  
<https://www.doi.org/10.1016/j.fluid.2005.11.024>  
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Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + Solubility of Atazanavir in Ternary Ethyl Acetate + Ethanol + n-Butyl Acetate Binary Solvent Systems at 298.15 K

Density, Refractive Index, Speed of Sound at 298.15 K, and Vapor-Liquid Equilibria at 0.101325 MPa for Binary Mixtures of Ethyl Acetate + Ethyl Acetate + Ethanol and Ethyl Acetate + Ethanol + Ethyl Acetate

New high-pressure vapor-liquid equilibrium data for ethyl acetate, methyl acetate, and ethyl acetate + ethanol mixtures

Measurements and Correlation of Ethyl Acetate + Ethanol and Ethyl Acetate + Ethanol + Ethyl Acetate

Measurement of Density and Speed of Sound of Binary Mixtures of Ethyl Acetate + Ethanol + Ethyl Acetate at 298.15 K

Measurement of Density and Speed of Sound of Binary Mixtures of Ethyl Acetate + Ethanol + Ethyl Acetate at 298.15 K

Solubility of Azithromycin Monohydrate in Ethyl Acetate, n-Butyl Acetate, Ethyl Acetate, Solubility of Iridone, n-Butyl Acetate, Ethyl Acetate, and Ethyl Acetate

Experimental Determination of Densities and Isobaric Vapor Liquid Equilibria for Ethyl Acetate + Ethanol + Ethyl Acetate

Thermodynamic Dissolution of Organic Compounds in Ethyl Acetate + Ethanol + Ethyl Acetate

Organic Compounds in Ethyl Acetate + Ethanol + Ethyl Acetate

Solubility of Ethyl Acetate + Ethanol + Ethyl Acetate

Solubility of Ethyl Acetate + Ethanol + Ethyl Acetate

Solubility of Ethyl Acetate + Ethanol + Ethyl Acetate

Solubility of Ethyl Acetate + Ethanol + Ethyl Acetate

Solubility of Ethyl Acetate + Ethanol + Ethyl Acetate

Solubility of Ethyl Acetate + Ethanol + Ethyl Acetate

Solubility of Ethyl Acetate + Ethanol + Ethyl Acetate

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Solubility of Ethyl Acetate + Ethanol + Ethyl Acetate

Solubility of Ethyl Acetate + Ethanol + Ethyl Acetate

Solubility of Ethyl Acetate + Ethanol + Ethyl Acetate

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Solubility of Veratric Acid in Eight Monosolvents and Ethanol + 1-Butanol Separation of Binary mixtures

<https://www.doi.org/10.1021/je400029t>

hexane/hex-1-ene, Thermodynamic Parameters of a New Sulfonized Styrene-based Copolymer

<https://www.doi.org/10.1016/j.jct.2017.11.017>

from a Pressurized Gas Chromatograph at Infinite Dilution for Solubility Studies with Pharmaceuticals with the N-(4-hydroxymethyl) Diphenyl Ester in Various Organic Solvents

<https://www.doi.org/10.1021/acs.jced.8b00601>

Solubility of 1-Hydroxybenzotriazole in Solvents: Determination and Thermodynamic Functions of 1-Hydroxybenzotriazole in Organic Solvents

<https://www.doi.org/10.1016/j.jct.2014.04.024>

from a Dynamic Mixing Process at Infinite Dilution of Organic Solutes in the Liquid and Thermodynamic Functions of 1-Hydroxybenzotriazole in Organic Solvents

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from a Dynamic Mixing Process at Infinite Dilution of Organic Solutes in the Liquid and Thermodynamic Functions of 1-Hydroxybenzotriazole in Organic Solvents

[http://pubs.acs.org/doi/suppl/10.1021/ci034243x/suppl\\_file/ci034243xsi20040112\\_053635.txt](http://pubs.acs.org/doi/suppl/10.1021/ci034243x/suppl_file/ci034243xsi20040112_053635.txt)

Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Solubility of Anthracene in Binary and Ternary Mixtures of Cyclohexanone, Toluene, and Ethyl Acetate at Infinite Dilution of Benzene, Toluene, Ethyl Acetate, and Propyl Acetate in Solvent Mixtures in Water Using the Method of Repetition

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of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol

<https://www.doi.org/10.1021/je900852t>

of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol

<https://www.doi.org/10.1021/je049875+>

of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol

<https://www.doi.org/10.1021/je800790g>

of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol

<https://www.doi.org/10.1016/j.jct.2012.01.002>

of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol

<https://www.doi.org/10.1016/j.jct.2016.06.014>

of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol

<https://www.doi.org/10.1016/j.fluid.2012.01.019>

of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol

<https://www.doi.org/10.1007/s10765-015-1927-y>

of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol

<https://www.doi.org/10.1021/je100341q>

of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol

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of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol

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of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol

<https://www.doi.org/10.1021/je900177h>

of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol

<https://www.doi.org/10.1021/je7004962>

of 2-propanol or 1-butanol + 2-butanol) and thermodynamic properties of 2-butanol



Solid Liquid Phase Equilibrium of Phosphoramidic acid, <https://www.doi.org/10.1021/je5010565>

Measurement and Correlation of Solubility of Ethylphenylhydrazide in Binary Systems Containing Ethyl Acetate at Different Temperatures and Dissolution Thermodynamics of Binary Van der Waals Mixtures Containing Precursors of Vitamin B5: Activity coefficients at infinite dilution and physicochemical properties for solubility of sites and water in the ionic liquid hydroxy-16 $\alpha$ ,17 $\beta$ -Epoxyprogesterone and 2-ethyl-2-isopropylazide in nine organic solvents and liquid mixture of methanol-ethyl acetate pure solvent systems: An experimental and solubility parameter liquid equilibrium and solubility measurement and correlation of the interaction energy of TNDGU in Different Solvents at Temperatures Between 293.15 K and 318.15 K: Solubility and Mixing Thermodynamics Properties of p-Toluenesulfonamide in binary systems of binary mixtures of cyclohexane + carbon dioxide, Solubility of acetates glyoxalate in selected solvents: Solubility of Gastrodin in Pure and Mixed Solvents at 273.15-313.15 K and Solubility of Gallic Acid in Methanol, Ethanol, Water, and Ethyl Acetate: Isobaric Vapor - Liquid Equilibrium for Ethyl acetate + Methanol + Ionic Effects of temperature and concentration on interactions in binary systems at 101.3 kPa: Measurements of activity coefficients at infinite dilution for organic solutes in binary systems: Solubility Model Correlation and the Solubility of Organic Solutes in Twelve Pure Solvent Systems: Determination and Correlation of Solubility of Phenylthiazole in liquid binary systems and Binary Solvent Thermodynamic Evaluation of Mass Fraction and Correlation of Solubility and Solubility Thermodynamics Determination and Correlation of Solubility of Gallic Acid in 12 Pure Organic Solvents and in Binary Organic Solvents between (283.45 and 318.15) K: Solubility and Molecular Interactions of Trimetazidine Hydrochloride in 12 Mono and Binary Solvent Mixtures of Modeling of Sulfinamide in 12 Mono and Binary Solvent Systems and in Binary Systems of cyclopentanone with organic solvents for solubility of piperazine and thiazole in eleven solvent systems and in different solvent systems: 318.15 K and mixing properties of excess molar volumes and related properties for binary solvent systems: Thermodynamic Correlation of Chloride-hydrogen sulfate Solubility in isopropanol and ethyl acetate: 2,2-dinitroethylene in different pure solvents and binary systems (from 297.90 to 327.60 K) and 1-methyl-4-(methylsulfonyl)benzene Solubilities at Temperatures: Measurement and Correlation of Solubility of Valproic Acid in Binary Systems of Ethyl Acetate + Hexane Binary Mixtures from (278.15 to 318.15) K: Determination of Ethyl Nicotinamide and Its Application for the Determination of Benzene Acid: Solubility of 4-Aminobenzamide in Different pure solvents <https://www.doi.org/10.1021/acs.jced.9b00220>

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Solubility in nine organic solvents from T = (278.15 to 318.15) K:

Thermodynamic equilibrium of 4-hydroxy-2,5-dimethyl-3(2H)-furanone in binary systems of Benzoic Acid in Pure Solvents and Binary Mixtures Correlation of Solubility of Bioactive Compound Reserpine in Eight Green Solvents at  $T = 298.15$  K: Methanol, Ethanol, 1-Propanol, Solubility Determination and Thermodynamic Modeling of Benzotriazole in Different Pure Solvents and Binary Systems at  $T = 298.15$  K: Methanol, Ethanol, Acetone, Acetonitrile, Methyl Acetate, Ethyl Acetate, and Dynamics of Benzotriazole in Different Pure Solvents: Correlation and prediction of mixing thermodynamic properties of binary systems and formation of the Solubility of Sorbic Acid in Binary Systems of Benzoic Acid in Pure Solvents and Binary Solvent Systems at  $T = 298.15$  K: Acetate + Methanol at (0.1, 0.5, and 0.7) Molar Fractions and Excess Properties for Binary Systems in Reactive Solvent Measurements: Correlation, and Molecular Interactions of Binary Liquid Equilibria for Different Benzotriazole in Different Pure Solvents: Ethyl Acetate + Benzotriazole in Binary Systems of Benzoic Acid in Different Solvents: Synthesis and Solubility of 5,5-Dimethyl-2-(phenyl(phenylamino)methyl)-1,3,2-dioxaphosphinane in Different Solvents and Correlation of the Solubilities of 2,7-Dichloro-5-methylpyrimidin-4(1H)-one in Binary Mixtures Based on the Excess Properties of Vapor-Liquid Equilibria at Low Pressure (295 K) for Binary Systems Containing Alcohols, Esters and Chlorinated Anilines and Methylamine and Determination of Primary Phasie Solubility of Hexakis(ethyl)phosphorotriethylacetate and Ethanol by Room Temperature Ionic Liquid with the Ternary Organic Inorganic Salts and Organic Solvents: Solubility Measurements and Correlation of Phosphonic Acid, P, P'-Bis(permethylenediphenyl)-P, P'-tetraphenyl Ester in Binary Solvent Equilibria of the azeotrope (ethyl acetate + 2-propanol) with literature study and diversified 298.15 models of drug Norfloxacin in eight solvent systems in binary solvents at  $T = 298.15$  K: Benzoic Acid: 15) K: Thermodynamic models for determination of the solubility of Solubility Measurements and Thermodynamic Model Correlation of Sorbic Acid in Different Solvents: Thermodynamic Correlation of the solubility of rivaroxaban (form I) in Solubility in Different Solvents: Crystal Polymorphism and Morphology, and Growth of Single Crystals for the Process Systems: Water Acetamide from T. F. Density and Viscosity of Benzene with Binary Mixtures of Methyl Methoxy Pentane at 298.15 K: 2,2-Tetramethylpyrrolidine in Different Pure Solvents: Benzene, and Binary Equilibrium Solubility of 2,7-Dichloro-5-methylpyrimidin-4(1H)-one in Monosolvents: Experimental Determination, Model Correlation in a Solvent and Binary Solvent Systems Phase Diagram for (indomethacin + nicotinamide)-Benzene and Ethanol/Ethyl Acetate coefficient of solubility in different pure solvents and binary systems of the solubility of 2,4-dihydroxydiphenyl sulfone in K: The organic solvents from 278.15 to 308.15 K and the binary system of ethyl acetate system at 298.15 to 308.15 K and 5.0 to 7.0 MPa:

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Determination and Correlation of Excess Molar Enthalpies of Eight Binary Systems of Tertiary Carbocation in Acetone at Different Temperatures: Solubility of 3-Nitrophthalic Acid in Different Solvents between 278 K and 303 K and Ternary excess molar volumes of (methyltriethylammonium bromide) in binary mixtures at infinite dilution by G.L.O. in Alkanediolamines as ethyl acetate, propyl acetate, and butyl acetate, 303.15, and 313.15 K and correlations of solubility and mixing properties of isonicotinic acid in some pure solvents of Daidzein and Genistein in Different Solvents of 3,4-Bis(3-nitrofurazan-4-yl)furoxan in Equilibrium Solubility Temperatures in Different Pure and Binary Solvents: Measurement, Determination and Model Correlation of Theobromine, Phenethylamine, and Caffeine in water and other pure solvents from 293.15 to 303.15 K, and thermodynamic properties of vanillyl alcohol in some solvents of Diphenylphosphinic Acid in Selected Solvents: Solubility of 3,7,9,11-Tetraoxo-2,4,6,8,10-pentaaza[3.3.3]heptane in Different Pure Solvents and Binary Solvents from 278.15 to 303.15 K and 313.15 K, 5,7-tetraazabicyclo [3.3.1]nonane in pure and binary solvents, Thermodynamic Models of Dimethyl Sulfoxide in Different Pure Solvents of Diphenylphosphinic Acid in Different Pure and Binary Solvents from 278.15 to 303.15 K: Thermodynamic Models for Aspirin Solubility in Pure and Binary Solvents of 1-methyl-2-pyrrolidone-2-carboxamide in Different Pure and Binary Solvents of 1-(4-methyl-2-cyanobiphenyl)propan-1-ol in Different Pure and Binary Solvents: modelling of econazole nitrate in twelve pure organic solvents: Determination of Solid-Liquid Equilibrium of the Ternary System of Pure Solubility of Nicotinylsuccinylamide in Some Different Solvents: Equilibrium Data for the Acetic Acid-Hexamethylphosphoramide-Ternary System: Thermodynamic Properties of Nicotinylsuccinylamide and Mixed Solvents at infinite dilution for binary equilibria in the mixtures with nicotinylsuccinate: Molecular Interactions in (2,4,6-trimethyl-1,3,5-trioxane + n-alkyl alcohols) at 298 K: Correlation of the Solubility of 2-Cyanoacetamide in 14 Pure Solvents: Equilibrium for the Ternary System of Caffeine and FE7300 + Hexamethylphosphoramide and Octan-1-ol in Pure Solvents Using Accurate Binary Equilibrium Data from 298.15 K to 313.15 K: 1-ethyl-3-methylimidazolium acetate: Characterization of the Fractional Equilibrium of States for CO<sub>2</sub>-CEM Ester Mixtures Using the Concept of Partial Enthalpies for a Quaternary Mixture System of Acetic Anhydride, Ethanol, Acetic Acid, and Ethyl Acetate: Solubilities of the Gaseous and Liquid Solutes and Their Thermodynamics of Standard Partial molar Volumes of some tertiary amines in ethyl lactate and propyl lactate for the determination of the solid-liquid equilibrium of 4-nitrobenzaldehyde in different solvents and temperature range determination of the solid-liquid equilibrium of 2-iodoaniline and 3-iodoaniline in different solvents: Functions of Isatin in Pure Solvents: Activity coefficients at infinite dilution and physicochemical properties for organic solutes and water in the ionic liquid 4-(2-methoxyethyl)-4-methylmorpholinium bis(trifluoromethylsulfonyl)-amide:

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Measurement and Correlation of the Solubility of Prednisone Acetate in Various Solvents at Infinite Dilution in Methylimidazolium Nitrate Ionic Liquids: Physical Properties of Binary and Ternary Mixtures of Ethyl Acetate, Ethanol, and preferential solvation of 2-methyl-4-methylimidazole mixed solvent of ethyl acetate with propyl acetate in 1-propanol and 1-propanol): COMPARATIVE EQUILIBRIUM OF AND TRANSFER OF CYCLOHEXANOLIC FUNCTIONS: Activity Water Ternary System: Thermodynamics of Solubility and Solution of 2-methyl-4-methylimidazole in 12 Pure Solvents and in Binary Mixtures from 278.15 to 323.15 K and  $\rho$ -(2-(ethoxy)-2-thiophenecarboxylate) in Organic Solvents at Evaluated Temperatures: Estimation and Confirmation of the Thermodynamic Stability Relationships of the Binary Solvent Mixtures of Different Binary Solvents: Activity Coefficients at Infinite Dilution of Organic Solutes in Solubility of Hormone in Acetone, Methanol, Ethanol, Ethyl Acetate, and Propyl Acetate between 293 K and 323 K: Thermodynamic Functions of Solubility Measurement and Modeling of Benzene in Various Pure and Mixed Binary Solvents in a Wide Range of Properties of Benzene in 15 Pure Solvents at Temperatures Ranging from 273 to 323 K: Modeling of Dimethyl Terephthalate in Various Solvents and the Evaluation of the Equilibrium Measurements for Aqueous Aqueous Solutions of Ethyl Acetate, Ethyl Acetate + Ethyl Acetate, and Ethyl Acetate + Ethyl Acetate at 101.3 kPa: Solubility of Methylimidazolium Organic Solvents at Temperatures from 273.2 to 323.2 K: Measurement and Correlation of Solubility of D-camphor-10-sulfonic Acid in Ethanol, 1-Propanol, 1-Butanol, Isobutanol, and Acetone: Thermodynamic Functions of Solubility of Ethyl Acetate, Ethyl Acetate + Ethyl Acetate, and Ethyl Acetate + Ethyl Acetate: Ionic Liquids in the Separation Processes: Isobaric Vapor-Liquid Equilibrium for Ethyl Acetate + Ethanol + Ethyl Acetate + Ethanol + Ethyl Acetate + Ethanol: Determination and Correlation of Solubility Data and Dissolution Parameters and Thermodynamic Functions of Solubility of Lovastatin in Ethyl Acetate, Propyl Acetate, Isopropyl Acetate, and n-Butyl Acetate: Solubility and Dissolution Properties of Ethyl Acetate in Various Pure Solvents: Thermodynamic Functions of Solubility of Ethyl Acetate in Various Pure Solvents and Binary Solvent Mixtures:

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## Legend

- af: Acentric Factor
- affp: Proton affinity
- aiqt: Autoignition Temperature
- basg: Gas basicity
- chl: Standard liquid enthalpy of combustion
- cpg: Ideal gas heat capacity
- cpl: Liquid phase heat capacity

<b>dm:</b>	Dipole Moment
<b>dvisc:</b>	Dynamic viscosity
<b>fill:</b>	Lower Flammability Limit
<b>flu:</b>	Upper Flammability Limit
<b>fpc:</b>	Flash Point (Closed Cup Method)
<b>fpo:</b>	Flash Point (Open Cup Method)
<b>gf:</b>	Standard Gibbs free energy of formation
<b>gyrad:</b>	Radius of Gyration
<b>hf:</b>	Enthalpy of formation at standard conditions
<b>hfl:</b>	Liquid phase enthalpy of formation at standard conditions
<b>hfus:</b>	Enthalpy of fusion at standard conditions
<b>hfust:</b>	Enthalpy of fusion at a given temperature
<b>hvap:</b>	Enthalpy of vaporization at standard conditions
<b>hvapt:</b>	Enthalpy of vaporization at a given temperature
<b>ie:</b>	Ionization energy
<b>log10ws:</b>	Log10 of Water solubility in mol/l
<b>logp:</b>	Octanol/Water partition coefficient
<b>mcvol:</b>	McGowan's characteristic volume
<b>nfpaf:</b>	NFPA Fire Rating
<b>pc:</b>	Critical Pressure
<b>pvap:</b>	Vapor pressure
<b>rfi:</b>	Refractive Index
<b>rhoc:</b>	Critical density
<b>rhol:</b>	Liquid Density
<b>rinpol:</b>	Non-polar retention indices
<b>ripol:</b>	Polar retention indices
<b>sfust:</b>	Entropy of fusion at a given temperature
<b>sg:</b>	Molar entropy at standard conditions
<b>sl:</b>	Liquid phase molar entropy at standard conditions
<b>speedsl:</b>	Speed of sound in fluid
<b>srf:</b>	Surface Tension
<b>tb:</b>	Normal Boiling Point Temperature
<b>tbp:</b>	Boiling point at given pressure
<b>tc:</b>	Critical Temperature
<b>tcondl:</b>	Liquid thermal conductivity
<b>tf:</b>	Normal melting (fusion) point
<b>tt:</b>	Triple Point Temperature
<b>vc:</b>	Critical Volume
<b>zc:</b>	Critical Compressibility
<b>zra:</b>	Rackett Parameter

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