

# Ethyl Acetate

Other names:	1-Acetoxyethane
	Acetic acid, ethyl ester
	Acetic ether
	Acetidin
	Acetoxyethane
	Aethylacetat
	CH3COOC2H5
	Essigester
	Ethyl acetic ester
	Ethyl ester of acetic acid
	Ethyl ethanoate
	Ethylacetaat
	Ethyle (acetate d')
	Ethylester kyseliny octove
	Etile (acetato di)
	NSC 70930
	Rcra waste number U112
	UN 1173
	Vinegar naphtha
	ac. acetic ethyl ester
Inchi:	InChI=1S/C4H8O2/c1-3-6-4(2)5/h3H2,1-2H3
InchiKey:	XEKOWRVHYACXOJ-UHFFFAOYSA-N
Formula:	C4H8O2
SMILES:	CCOC(C)=O
Mol. weight [g/mol]:	88.11
CAS:	141-78-6

## Physical Properties

Property code	Value	Unit	Source
af	0.3620		KDB
affp	835.70	kJ/mol	NIST Webbook
aigt	699.82	K	KDB
basg	804.70	kJ/mol	NIST Webbook
basg	799.90 ± 0.20	kJ/mol	NIST Webbook
chl	-2246.00	kJ/mol	NIST Webbook
chl	-2238.54 ± 0.48	kJ/mol	NIST Webbook
chl	-2235.40 ± 3.90	kJ/mol	NIST Webbook

chl	-2256.00	kJ/mol	NIST Webbook
dm	1.90	debye	KDB
dvisc	0.0004274	Paxs	Densities and Viscosities of Binary Liquid Mixtures of Trichloroethylene and Tetrachloroethylene with Some Polar and Nonpolar Solvents
dvisc	0.0004260	Paxs	Densities and Viscosities of Ternary Mixtures of Cyclohexane + Cyclohexanone + Some Alkyl Acetates at 298.15 K
dvisc	0.0004370	Paxs	A volumetric and viscosity study for the binary mixtures of 1-hexyl-3-methylimidazolium tetrafluoroborate with some molecular solvents
fll	2.20	% in Air	KDB
flu	9.00	% in Air	KDB
fpc	285.93	K	KDB
fpo	268.71	K	KDB
gf	-327.60	kJ/mol	KDB
gyrad	3.3480		KDB
hf	-444.80 ± 0.40	kJ/mol	NIST Webbook
hf	-443.20	kJ/mol	KDB
hf	-443.80	kJ/mol	NIST Webbook
hf	-445.43 ± 0.84	kJ/mol	NIST Webbook
hf	-446.90	kJ/mol	NIST Webbook
hfl	-482.00 ± 4.00	kJ/mol	NIST Webbook
hfl	-478.82 ± 0.73	kJ/mol	NIST Webbook
hfl	-479.86 ± 0.46	kJ/mol	NIST Webbook
hfl	-480.57 ± 0.79	kJ/mol	NIST Webbook
hfus	8.90	kJ/mol	Joback Method
hvap	33.65	kJ/mol	Joback Method
ie	10.24	eV	NIST Webbook
ie	10.01 ± 0.05	eV	NIST Webbook
ie	10.01 ± 0.05	eV	NIST Webbook
ie	10.00 ± 0.10	eV	NIST Webbook
ie	10.09 ± 0.02	eV	NIST Webbook
ie	10.16	eV	NIST Webbook
ie	9.90	eV	NIST Webbook
ie	9.90 ± 0.05	eV	NIST Webbook
ie	10.45	eV	NIST Webbook
ie	10.11 ± 0.02	eV	NIST Webbook
log10ws	-0.04		Aqueous Solubility Prediction Method

log10ws	-0.04		Estimated Solubility Method
logp	0.569		Crippen Method
mcvol	74.660	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
pc	4280.00 ± 405.30	kPa	NIST Webbook
pc	4018.00 ± 202.65	kPa	NIST Webbook
pc	3851.70 ± 40.00	kPa	NIST Webbook
pc	3882.00 ± 3.87	kPa	NIST Webbook
pc	3900.00	kPa	Critical Properties of the Reacting Mixture in the Esterification of Acetic Acid with Ethanol
pc	3882.00	kPa	KDB
pc	3830.00 ± 81.06	kPa	NIST Webbook
rhoc	308.10 ± 4.41	kg/m3	NIST Webbook
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sl	259.40	J/molxK	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tb	350.27	K	Vapor liquid equilibria for the quaternary reactive system ethyl acetate + ethanol +water + acetic acid and some of the constituent binary systems at 101.3 kPa

tb	350.24	K	Vapor liquid equilibria for the binary mixtures of 2,3-butanediol with n-butanol, n-butyl acetate, and ethyl acetate at 101.3 kPa
tb	350.24	K	Liquid-liquid equilibria of water + 3-hydroxy-2-butanone + ethyl ethanoate
tb	350.20	K	Solubility and tie-line data for ternary aqueous mixtures of cyclopentanol with organic solvents at T = 298.2 K: Experiments and NRTL model
tb	350.15	K	The isobaric vapor liquid equilibria of ethyl acetate p acetonitrile p bis(trifluoromethylsulfonyl)imide-based ionic liquids at 101.3 kPa
tb	350.29	K	Isobaric vapor-liquid equilibrium of a ternary system of ethyl acetate + propyl acetate + dimethyl sulfoxide and binary systems of ethyl acetate + dimethyl sulfoxide and propyl acetate + dimethyl sulfoxide at 101.3 kPa
tb	350.35	K	Isobaric Vapor - Liquid Equilibrium for Ethyl acetate + Methanol + Ionic Liquids Ternary systems at 101.3 kPa
tb	350.16	K	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tb	350.20	K	Isobaric Vapor Liquid Equilibrium for Three Binary Systems of Acetaldehyde + Ethanol, Ethyl Acetate, 1-Butanol at 101.3 kPa
tb	349.95	K	Effect of Ionic Liquids on the Binary Vapor-Liquid Equilibrium of Ethyl Acetate + Methanol System at 101.3 kPa
tb	350.28	K	Isobaric Vapor-Liquid Phase Equilibrium Measurements for Allyl Alcohol with Chloroform, Ethyl Acetate, and Methyl Propionate at 101.3 kPa

tb	350.25	K	Isobaric Vapor-Liquid Equilibria and Excess Quantities for Binary Mixtures of an Ethyl Ester + tert-Butanol and a New Approach to VLE Data Processing
tb	350.15	K	Vapor-Liquid Equilibrium of Binary Mixtures Containing Ethyl Acetate + 2-Methyl-1-propanol and Ethyl Acetate + 2-Methyl-1-butanol at 101.3 kPa
tb	350.21	K	Volumetric Behavior and Saturated Pressure for Carbon Dioxide + Ethyl Acetate at a Temperature of 313.15 K
tb	350.15	K	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
tb	350.19	K	Experimental Determination of Vapor Liquid Equilibria. Binary Systems of Methyl Acetate, Ethyl Acetate, and Propyl Acetate with 1-Propanol at 0.6 MPa
tb	350.13 ± 0.30	K	NIST Webbook
tb	350.20	K	NIST Webbook
tb	350.00	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	349.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.26	K	KDB
tb	350.30	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.19 ± 0.50	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tb	350.30 ± 0.30	K	NIST Webbook
tb	375.00 ± 2.00	K	NIST Webbook
tb	350.35	K	NIST Webbook
tb	350.05 ± 0.30	K	NIST Webbook
tb	350.21 ± 0.50	K	NIST Webbook
tb	350.25 ± 0.50	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook



tb	350.00 ± 2.00	K	NIST Webbook
tb	350.29 ± 0.15	K	NIST Webbook
tb	350.15 ± 2.00	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 0.50	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.65 ± 2.00	K	NIST Webbook
tb	349.65 ± 2.00	K	NIST Webbook
tb	352.15 ± 2.00	K	NIST Webbook
tb	350.25 ± 1.00	K	NIST Webbook
tb	350.30 ± 1.00	K	NIST Webbook
tb	350.30 ± 1.00	K	NIST Webbook
tb	349.97 ± 2.00	K	NIST Webbook
tb	346.65 ± 3.00	K	NIST Webbook
tb	350.45 ± 1.00	K	NIST Webbook
tb	350.25 ± 1.00	K	NIST Webbook
tb	350.30 ± 0.40	K	NIST Webbook
tb	349.15 ± 2.00	K	NIST Webbook
tb	349.65 ± 2.50	K	NIST Webbook
tb	350.26 ± 0.06	K	NIST Webbook
tb	350.30 ± 0.15	K	NIST Webbook
tb	350.00 ± 2.00	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.15 ± 2.00	K	NIST Webbook
tb	349.95 ± 2.00	K	NIST Webbook
tb	350.20 ± 0.50	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tb	350.25 ± 0.50	K	NIST Webbook
tb	350.21 ± 0.50	K	NIST Webbook
tb	349.65 ± 2.00	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.45 ± 0.60	K	NIST Webbook
tb	350.30 ± 0.30	K	NIST Webbook
tb	350.25 ± 1.00	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tb	350.25 ± 1.00	K	NIST Webbook
tb	349.90 ± 0.20	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	347.45 ± 2.00	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.30 ± 2.00	K	NIST Webbook

tb	350.20 ± 2.00	K	NIST Webbook
tb	350.30 ± 2.00	K	NIST Webbook
tb	350.10 ± 2.00	K	NIST Webbook
tb	350.70 ± 2.00	K	NIST Webbook
tb	350.65 ± 2.00	K	NIST Webbook
tb	351.15 ± 2.00	K	NIST Webbook
tb	347.45 ± 2.00	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tc	522.70 ± 2.00	K	NIST Webbook
tc	523.30	K	KDB
tc	513.00 ± 6.00	K	NIST Webbook
tc	523.20	K	NIST Webbook
tc	523.30 ± 0.05	K	NIST Webbook
tc	523.30 ± 1.00	K	NIST Webbook
tc	523.30 ± 1.00	K	NIST Webbook
tc	548.90 ± 20.00	K	NIST Webbook
tc	523.29	K	Development of a Predictive Equation of State for CO2 + Ethyl Ester Mixtures Based on Critical Points Measurements
tf	189.25	K	Aqueous Solubility Prediction Method
tf	189.50	K	KDB
tt	189.30 ± 0.20	K	NIST Webbook
tt	189.30 ± 0.05	K	NIST Webbook
vc	0.286	m3/kmol	KDB
zc	0.2551730		KDB
zra	0.25		KDB

## Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	142.80	J/molxK	425.00	NIST Webbook
cpg	149.47	J/molxK	450.00	NIST Webbook
cpg	125.82	J/molxK	360.00	NIST Webbook
cpg	131.06	J/molxK	380.00	NIST Webbook
cpg	136.22	J/molxK	400.00	NIST Webbook
cpl	169.60	J/molxK	298.15	NIST Webbook
cpl	169.20	J/molxK	293.60	NIST Webbook
cpl	169.50	J/molxK	298.10	NIST Webbook
cpl	169.30	J/molxK	298.15	NIST Webbook

cpl	170.59	J/molxK	298.32	NIST Webbook
cpl	168.94	J/molxK	298.15	NIST Webbook
cpl	157.70	J/molxK	290.00	NIST Webbook
cpl	168.82	J/molxK	303.61	NIST Webbook
cpl	169.06	J/molxK	298.15	NIST Webbook
cpl	167.40	J/molxK	298.15	NIST Webbook
cpl	169.60	J/molxK	298.15	NIST Webbook
dvisc	0.0004210	Paxs	298.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003990	Paxs	303.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003810	Paxs	308.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004430	Paxs	293.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003460	Paxs	318.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003300	Paxs	323.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004260	Paxs	298.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure

dvisc	0.0003010	Paxs	333.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0002880	Paxs	338.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004520	Paxs	293.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
dvisc	0.0002750	Paxs	343.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003806	Paxs	303.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K
dvisc	0.0003622	Paxs	308.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K

dvisc	0.0003870	Paxs	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
dvisc	0.0003790	Paxs	303.15	Volumetric and Transport Properties of Binary Liquid Mixtures of Phenylacetonitrile with Aliphatic Esters at Temperatures of (303.15 to 313.15) K
dvisc	0.0003610	Paxs	308.15	Volumetric and Transport Properties of Binary Liquid Mixtures of Phenylacetonitrile with Aliphatic Esters at Temperatures of (303.15 to 313.15) K
dvisc	0.0003440	Paxs	313.15	Volumetric and Transport Properties of Binary Liquid Mixtures of Phenylacetonitrile with Aliphatic Esters at Temperatures of (303.15 to 313.15) K

dvisc	0.0004280	Paxs	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
dvisc	0.0004030	Paxs	303.15	Density, dynamic viscosity, and derived properties of binary mixtures of methanol or ethanol with water, ethyl acetate, and methyl acetate at T = (293.15, 298.15, and 303.15) K
dvisc	0.0004260	Paxs	298.15	Density, dynamic viscosity, and derived properties of binary mixtures of methanol or ethanol with water, ethyl acetate, and methyl acetate at T = (293.15, 298.15, and 303.15) K
dvisc	0.0003426	Paxs	313.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K

dvisc	0.0004520	Paxs	293.15	Density, dynamic viscosity, and derived properties of binary mixtures of methanol or ethanol with water, ethyl acetate, and methyl acetate at T = (293.15, 298.15, and 303.15) K
dvisc	0.0003630	Paxs	313.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003150	Paxs	328.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004030	Paxs	303.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
hfust	10.48	kJ/mol	189.30	NIST Webbook
hfust	10.48	kJ/mol	189.30	NIST Webbook
hfust	10.48	kJ/mol	189.30	NIST Webbook
hvapt	32.40 ± 0.10	kJ/mol	344.00	NIST Webbook
hvapt	34.60 ± 0.10	kJ/mol	313.00	NIST Webbook
hvapt	31.40 ± 0.10	kJ/mol	343.00	NIST Webbook
hvapt	33.80 ± 0.10	kJ/mol	326.00	NIST Webbook
hvapt	33.40 ± 0.10	kJ/mol	331.00	NIST Webbook
hvapt	36.70	kJ/mol	322.00	NIST Webbook
hvapt	32.22	kJ/mol	349.80	KDB
hvapt	31.90 ± 0.10	kJ/mol	351.00	NIST Webbook
hvapt	31.90	kJ/mol	350.00	NIST Webbook
hvapt	31.00 ± 0.10	kJ/mol	363.00	NIST Webbook
hvapt	34.00	kJ/mol	320.00	NIST Webbook
hvapt	34.10	kJ/mol	345.00	NIST Webbook

hvapt	35.70	kJ/mol	319.50	NIST Webbook
hvapt	31.94	kJ/mol	350.30	NIST Webbook
pvap	59.91	kPa	335.02	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	101.30	kPa	349.95	Effect of Ionic Liquids on the Binary Vapor-Liquid Equilibrium of Ethyl Acetate + Methanol System at 101.3 kPa
pvap	101.30	kPa	350.28	Isobaric Vapor-Liquid Phase Equilibrium Measurements for Allyl Alcohol with Chloroform, Ethyl Acetate, and Methyl Propionate at 101.3 kPa
pvap	100.00	kPa	349.53	Isobaric Vapor Liquid Equilibria for Binary Mixtures of Isoamyl Acetate + Ethyl Acetate at 50 and 100 kPa
pvap	50.00	kPa	330.01	Isobaric Vapor Liquid Equilibria for Binary Mixtures of Isoamyl Acetate + Ethyl Acetate at 50 and 100 kPa
pvap	25.08	kPa	313.15	Total Vapor Pressure Measurements for 2-Ethoxyethanol with Methyl Acetate, Ethyl Acetate, Propyl Acetate, and Ethyl Propionate at 313.15 K and for 2-Ethoxyethanol with Methyl Formate at 308.15 K



pvap	25.30	kPa	313.15	Isothermal Vapor-Liquid Equilibria of ethyl acetate + dibromomethane, or + bromochloromethane or + 1,2-dichloroethane or +1-bromo-2-chloroethane at T = 313.15 K
pvap	11.89	kPa	297.17	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	16.04	kPa	303.35	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	18.33	kPa	306.25	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	20.64	kPa	308.86	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	22.44	kPa	310.67	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	24.34	kPa	312.53	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	27.63	kPa	315.44	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	31.33	kPa	318.46	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	34.85	kPa	321.01	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	45.95	kPa	328.15	Isothermal Vapor-Liquid Equilibria for Binary Mixtures of Methyl Nonafluorobutyl Ether + Acetone, Cyclopentyl Methyl Ether, Ethyl Acetate, n-Heptane, Methanol, and Toluene
pvap	40.61	kPa	324.80	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	44.98	kPa	327.41	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	49.27	kPa	329.77	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	52.56	kPa	331.51	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	55.72	kPa	333.07	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	111.76	kPa	353.15	Vapor Liquid Equilibrium and Excess Enthalpy Data for Systems Containing N,N-Dimethylacetamide
pvap	62.83	kPa	336.33	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	66.49	kPa	337.91	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	69.34	kPa	339.09	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	72.26	kPa	340.23	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	76.02	kPa	341.69	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	79.83	kPa	343.03	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	82.56	kPa	344.11	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	86.85	kPa	345.53	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	90.81	kPa	346.86	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	94.63	kPa	348.09	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	96.74	kPa	348.75	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	98.97	kPa	349.45	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	99.36	kPa	349.56	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	100.07	kPa	349.76	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	100.68	kPa	349.93	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	101.32	kPa	350.15	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	104.65	kPa	351.12	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	106.84	kPa	351.77	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	108.13	kPa	352.12	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	111.21	kPa	352.94	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	114.65	kPa	353.91	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	1500.00	kPa	462.75	Measurement and modeling of high pressure VLE for methyl acetate or ethyl acetate with 2-butanol. Isobaric data at 1.5 MPa
pvap	118.56	kPa	354.93	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	120.68	kPa	355.50	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	122.31	kPa	355.91	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	124.00	kPa	356.37	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	127.89	kPa	357.35	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	130.00	kPa	357.92	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	133.45	kPa	358.74	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	136.34	kPa	359.44	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	139.07	kPa	360.03	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)



pvap	142.55	kPa	360.88	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	146.37	kPa	361.73	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	150.43	kPa	362.62	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	155.58	kPa	363.72	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	157.94	kPa	364.25	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	160.53	kPa	364.81	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	163.99	kPa	365.52	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	167.81	kPa	366.29	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	171.33	kPa	367.00	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	174.65	kPa	367.64	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	176.37	kPa	367.98	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	180.88	kPa	368.83	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	184.43	kPa	369.49	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	187.47	kPa	370.07	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	190.92	kPa	370.69	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	195.35	kPa	371.50	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	202.90	kPa	373.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	687.53	kPa	423.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	21.72	kPa	310.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa

pvap	24.78	kPa	313.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	28.18	kPa	316.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	31.95	kPa	319.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	36.12	kPa	322.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	40.73	kPa	325.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	45.80	kPa	328.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	51.36	kPa	331.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa

pvap	57.46	kPa	334.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	101.30	kPa	350.35	Isobaric Vapor - Liquid Equilibrium for Ethyl acetate + Methanol + Ionic Liquids Ternary systems at 101.3 kPa
pvap	71.40	kPa	340.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	79.32	kPa	343.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	87.93	kPa	346.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	97.26	kPa	349.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	107.36	kPa	352.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa

pvap	118.27	kPa	355.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa	
pvap	130.03	kPa	358.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa	
pvap	134.15	kPa	359.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa	
pvap	101.30	kPa	350.29	Isobaric vapor-liquid equilibrium of a ternary system of ethyl acetate + propyl acetate + dimethyl sulfoxide and binary systems of ethyl acetate + dimethyl sulfoxide and propyl acetate + dimethyl sulfoxide at 101.3 kPa	
pvap	1222.70	kPa	452.30	Isothermal (vapour + liquid) equilibrium (VLE) for binary mixtures containing diethyl carbonate, phenyl acetate, diphenyl carbonate, or ethyl acetate	
pvap	557.10	kPa	412.80	Isothermal (vapour + liquid) equilibrium (VLE) for binary mixtures containing diethyl carbonate, phenyl acetate, diphenyl carbonate, or ethyl acetate	

pvap	205.70	kPa	373.00	Isothermal (vapour + liquid) equilibrium (VLE) for binary mixtures containing diethyl carbonate, phenyl acetate, diphenyl carbonate, or ethyl acetate
pvap	93.32	kPa	347.70	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	79.99	kPa	343.18	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	66.66	kPa	337.99	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	53.33	kPa	331.90	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	40.00	kPa	324.44	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	31.37	kPa	318.40	Vapour liquid equilibrium for the ethyl ethanoate + 1-butene, +cis-2-butene, +trans-2-butene, +2-methylpropene, +n-butane and +2-methylpropane

pvap	38.43	kPa	323.47	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	64.13	kPa	337.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	116.46	kPa	354.43	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	101.30	kPa	350.15	The isobaric vapor liquid equilibria of ethyl acetate p acetonitrile p bis(trifluoromethylsulfonyl)imide-based ionic liquids at 101.3 kPa
rfi	1.36990		298.15	Densities, Viscosities, and Refractive Indices for Binary and Ternary Mixtures of N,N-Dimethylacetamide (1) + 2-Methylbutan-2-ol (2) + Ethyl Acetate (3) at 298.15 K for the Liquid Region and at Ambient Pressure
rfi	1.35368		328.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K



rfi	1.35919	318.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.36460	308.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.36994	298.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.37519	288.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.35880	293.15	Solubilities of Methyl diphenylphosphine Oxide in Selected Solvents
rfi	1.35880	293.15	Solubilities of Triphenylphosphine Oxide in Selected Solvents

rfi	1.37120	298.15	Determination and Correlation of Vapor Liquid Equilibrium Data for the Ethyl Acetate + Hexamethyl Disiloxane System at 101.3 kPa
rfi	1.37010	293.15	Liquid-Liquid Equilibrium of (Water + Pentane-2,4-dione + Ethyl Ethanoate) and (Water + Pentane-2,4-dione + Cyclohexane) at (298.15 and 313.15) K
rfi	1.37000	298.15	Vapor-Liquid Equilibria for Ethyl Acetate + Methanol at (0.1, 0.5, and 0.7) MPa. Measurements with a New Ebulliometer
rfi	1.37190	293.15	Solubilities of Phosphorus-Containing Compounds in Selected Solvents
rfi	1.36712	303.15	Thermodynamic Properties of Ionic Liquids in Organic Solvents from (293.15 to 303.15) K
rfi	1.36977	298.15	Thermodynamic Properties of Ionic Liquids in Organic Solvents from (293.15 to 303.15) K
rfi	1.37241	293.15	Thermodynamic Properties of Ionic Liquids in Organic Solvents from (293.15 to 303.15) K
rfi	1.37190	293.15	Solubilities of Some Phosphaspirocyclic Compounds in Selected Solvents

rfi	1.36978	298.15	Liquid-Liquid Equilibrium Diagrams of Ethanol + Water + (Ethyl Acetate or 1-Pentanol) at Several Temperatures
rfi	1.36978	298.15	Density, Refractive Index, Speed of Sound at 298.15 K, and Vapor-Liquid Equilibria at 101.3 kPa for Binary Mixtures of Ethyl Acetate + Ethyl Lactate and Methyl Acetate + Ethyl Lactate
rfi	1.36310	308.15	Density, Viscosity, Refractive Index, and Speed of Sound for Binary Mixtures of 1,4-Dioxane with Different Organic Liquids at (298.15, 303.15, and 308.15) K
rfi	1.36730	303.15	Density, Viscosity, Refractive Index, and Speed of Sound for Binary Mixtures of 1,4-Dioxane with Different Organic Liquids at (298.15, 303.15, and 308.15) K
rfi	1.37130	298.15	Density, Viscosity, Refractive Index, and Speed of Sound for Binary Mixtures of 1,4-Dioxane with Different Organic Liquids at (298.15, 303.15, and 308.15) K

rfi	1.36980	298.15	Density, Refractive Index, and Speed of Sound at 298.15 K and Vapor-Liquid Equilibria at 101.3 kPa for Binary Mixtures of Ethyl Acetate + 1-Pentanol and Ethanol + 2-Methyl-1-propanol
rfi	1.36981	298.15	Measurement of VLE Data by Using an Experimental Installation with Automatic Control: Modeling of Binary Systems of Methyl Acetate or Ethyl Acetate with n-Heptane or 2,2,4-Trimethylpentane at Both 0.1 and 1.5 MPa
rfi	1.37244	298.15	Isobaric Vapor-Liquid Equilibrium Data for Binary Systems of Anisole with Methyl Acetate, Ethyl Acetate, n-Propyl Acetate, and Isopropyl Acetate at 93.9 kPa
rfi	1.36980	298.15	Vapor-Liquid Equilibrium Data for Binary Mixtures of Dimethyl Carbonate with Methyl Acetate, Ethyl Acetate, n-Propyl Acetate, Isopropyl Acetate, n-Butyl Acetate, and Isoamyl Acetate at 93.13 kPa

rfi	1.36640	303.15	Densities, speeds of sound, isentropic compressibilities, refractive indexes, and viscosities of tetrahydrofuran with haloalkane or alkyl ethanoate at T = 303.15 K
rfi	1.36750	303.15	Liquid-liquid equilibrium for ternary systems of ethyl acetate/isopropyl acetate + 2,2,3,3-tetrafluoro-1-propanol + water at 298.15, 318.15 K
rfi	1.36720	303.15	Density, refraction index and vapor-liquid equilibria of N-methyl-2-hydroxyethylammonium butyrate plus (methyl acetate or ethyl acetate or propyl acetate) at several temperatures
rfi	1.37000	298.15	Correlation and prediction of mixing thermodynamic properties of ester-containing systems: Ester + alkane and ester + ester binary systems and the ternary dodecane + ethyl pentanoate + ethyl ethanoate
rfi	1.36977	298.15	Ternary (liquid + liquid) equilibria of the azeotrope (ethyl acetate + 2-propanol) with different ionic liquids at T = 298.15 K
rfi	1.36712	303.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures

rfi	1.36977	298.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.37241	293.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.37270	298.15	Effects of the presence of ethylacetate or benzene on the densities and volumetric properties of mixture (styrene + N,N-dimethylformamide)
rfi	1.37000	298.15	Molecular interactions in (2,4,6-trimethyl-1,3,5-trioxane + n-alkyl acetates) at T=(298.15, 303.15, and 308.15) K
rfi	1.36977	298.15	Properties of ionic liquid HMIMPF <sub>6</sub> with carbonates, ketones and alkyl acetates
rfi	1.36920	298.15	Thermodynamic study of (alkyl esters + $\alpha,\alpha$ -alkyl dihalides) I: HE and V E for 25 binary mixtures {xCu-1H <sub>2</sub> u-1CO <sub>2</sub> C <sub>2</sub> H <sub>5</sub> + (1-x) $\alpha,\alpha$ -ClCH <sub>2</sub> (CH <sub>2</sub> ) <sub>v</sub> -2CH <sub>2</sub> Cl}, where u = 1 to 5, $\alpha$ = 1 and v = x = 2 to 6
rfi	1.35970	318.15	Thermodynamic properties of (an ester + an alkane). XVI. Experimental HEm and V Em values and a new correlation method for (an alkyl ethanoate + an n-alkane) at 318.15 K

rfi	1.37240		293.15	A novel static analytical apparatus for phase equilibrium measurements
rfi	1.35940		318.20	Experimental and calculated liquid-liquid equilibrium data for water + furfural + solvents
rfi	1.36720		303.20	Experimental and calculated liquid-liquid equilibrium data for water + furfural + solvents
rfi	1.37490		288.20	Experimental and calculated liquid-liquid equilibrium data for water + furfural + solvents
rfi	1.37020		293.20	Vapor liquid equilibria for the ternary system of carbon dioxide + ethanol + ethyl acetate at elevated pressures
rfi	1.36983		298.15	Physical Properties of Binary and Ternary Mixtures of Ethyl Acetate, Ethanol, and 1-Octyl-3-methyl-imidazolium Bis(trifluoromethylsulfonyl)imide at 298.15 K
rhoI	888.42	kg/m3	303.15	Studies of viscosities of dilute solutions of alkylamine in non-electrolyte solvents. II. Haloalkanes and other polar solvents
rhoI	875.10	kg/m3	313.15	Ternary Excess Molar Volumes of {Methyltrioctylammonium Bis[(trifluoromethyl)sulfonyl]imide + Methanol + Methyl Acetate or Ethyl Acetate} Systems at (298.15, 303.15, and 313.15) K

rhoI	894.70	kg/m3	298.15	Ternary Excess Molar Volumes of {Methyltrioctylammonium Bis[(trifluoromethyl)sulfonyl]imide + Methanol + Methyl Acetate or Ethyl Acetate} Systems at (298.15, 303.15, and 313.15) K
rhoI	893.90	kg/m3	298.40	Vapor Liquid Equilibrium at 350 K, Excess Molar Enthalpies at 298 K, and Excess Molar Volumes at 298 K of Binary Mixtures Containing Ethyl Acetate, Butyl Acetate, and 2-Butanol
rhoI	897.72	kg/m3	298.15	Effect of Inorganic Salts on the Isobaric Vapor Liquid Equilibrium of the Ethyl Acetate Ethanol System
rhoI	894.40	kg/m3	298.15	Liquid-Liquid Equilibrium in Ternary Systems Containing Ethylene Glycol, Monofunctional Benzene Derivative, and Ethyl Acetate
rhoI	876.25	kg/m3	313.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhoI	882.48	kg/m3	308.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhoI	888.66	kg/m3	303.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)



rhoI	894.79	kg/m3	298.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhoI	901.00	kg/m3	293.00	KDB
rhoI	888.50	kg/m3	303.15	Ternary Excess Molar Volumes of {Methyltrioctylammonium Bis[(trifluoromethyl)sulfonyl]imide + Methanol + Methyl Acetate or Ethyl Acetate} Systems at (298.15, 303.15, and 313.15) K
rhoI	894.60	kg/m3	298.15	Experimental Determination of Densities and Isobaric Vapor Liquid Equilibria of Methyl Acetate and Ethyl Acetate with Alcohols (C3 and C4) at 0.3 MPa
rhoI	894.40	kg/m3	298.15	Revision of the volumetric method for measurements of liquid liquid equilibria in binary systems
rhoI	851.36	kg/m3	332.70	Isothermal vapor liquid equilibria for different binary mixtures involved in the alcoholic distillation
rhoI	906.55	kg/m3	288.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa

rhoI	894.38	kg/m3	298.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhoI	875.81	kg/m3	313.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhoI	856.81	kg/m3	328.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhoI	843.86	kg/m3	338.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhoI	830.62	kg/m3	348.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa

rhoI	900.48	kg/m3	293.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhoI	894.36	kg/m3	298.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhoI	888.19	kg/m3	303.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhoI	881.98	kg/m3	308.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhoI	875.73	kg/m3	313.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhoI	900.57	kg/m3	293.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
rhoI	876.10	kg/m3	313.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa

rhoI	894.51	kg/m3	298.15	Standard partial molar volumes of some electrolytes in ethylene carbonate based mixtures
rhoI	900.26	kg/m3	293.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhoI	894.14	kg/m3	298.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhoI	887.85	kg/m3	303.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhoI	881.52	kg/m3	308.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhoI	875.14	kg/m3	313.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K

rhoI	900.57	kg/m3	293.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhoI	894.47	kg/m3	298.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhoI	869.62	kg/m3	318.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	888.35	kg/m3	303.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhoI	882.17	kg/m3	308.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhoI	875.95	kg/m3	313.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates

rhoI	869.68	kg/m3	318.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhoI	863.36	kg/m3	323.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhoI	894.50	kg/m3	298.15	(Liquid + liquid) equilibria for mixtures of dodecane and ethanol with alkylsulfate-based ionic liquids
rhoI	893.40	kg/m3	298.15	Solubility and solution thermodynamics of sorbic acid in eight pure organic solvents
rhoI	900.88	kg/m3	293.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhoI	899.50	kg/m3	298.15	Isobaric Vapor-liquid Equilibrium for Three Binary Systems of Ethyl Acetate + Propyl Acetate, Ethyl Acetate + Propylene Carbonate, and Propyl Acetate + Propylene Carbonate at 101.3 kPa

rhoI	863.30	kg/m3	323.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	888.50	kg/m3	303.15	Volumetric and transport properties of ternary mixtures containing 1-propanol + ethyl ethanoate + cyclohexane or benzene at 303.15 K: Experimental data, correlation and prediction by ERAS model
rhoI	875.88	kg/m3	313.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	882.09	kg/m3	308.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K

rhoI	888.26	kg/m3	303.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	894.37	kg/m3	298.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	900.44	kg/m3	293.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhoI	876.30	kg/m3	313.15	Apparent molar volume and apparent molar isentropic compressibility for the binary systems {methyltriethylammoniumbis(trifluoromethylsulfonyl)imide + ethyl acetate or ethanol} at different temperatures under atmospheric pressure



rhoI	882.70	kg/m3	308.15	Apparent molar volume and apparent molar isentropic compressibility for thebinary systems {methyltrioctylammoniumbis(trifluoromethylsulfonyl)imide + ethyl acetate or ethanol} at different temperatures underatmospheric pressure
rhoI	888.50	kg/m3	303.15	Apparent molar volume and apparent molar isentropic compressibility for thebinary systems {methyltrioctylammoniumbis(trifluoromethylsulfonyl)imide + ethyl acetate or ethanol} at different temperatures underatmospheric pressure
rhoI	894.40	kg/m3	298.15	Apparent molar volume and apparent molar isentropic compressibility for thebinary systems {methyltrioctylammoniumbis(trifluoromethylsulfonyl)imide + ethyl acetate or ethanol} at different temperatures underatmospheric pressure
rhoI	888.50	kg/m3	303.15	Volumetric and transport properties of ternary mixtures containing 1-alkanol + ethyl ethanoate + cyclohexane at 303.15 K: Experimental data, correlation and prediction by ERAS model

rhoI	894.40	kg/m <sup>3</sup>	298.15	Measurement and correlation of solubility and solution thermodynamics of 1,3-dimethylurea in different solvents from T = (288.15 to 328.15) K
rhoI	888.75	kg/m <sup>3</sup>	303.15	Excess Volumes and Excess Isentropic Compressibilities of Binary Liquid Mixtures of Trichloroethylene with Esters at 303.15 K
sfust	55.27	J/mol×K	189.30	NIST Webbook
speedsl	1098.00	m/s	308.15	Density and Speed of Sound of Binary Mixtures of N-Methylacetamide with Ethyl Acetate, Ethyl Chloroacetate, and Ethyl Cyanoacetate in the Temperature Interval (303.15 to 318.15) K
speedsl	1081.00	m/s	313.15	Density and Speed of Sound of Binary Mixtures of N-Methylacetamide with Ethyl Acetate, Ethyl Chloroacetate, and Ethyl Cyanoacetate in the Temperature Interval (303.15 to 318.15) K
speedsl	1058.00	m/s	318.15	Density and Speed of Sound of Binary Mixtures of N-Methylacetamide with Ethyl Acetate, Ethyl Chloroacetate, and Ethyl Cyanoacetate in the Temperature Interval (303.15 to 318.15) K

speedsl	1187.92	m/s	288.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K
speedsl	1165.80	m/s	293.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K
speedsl	1143.23	m/s	298.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K
speedsl	1120.80	m/s	303.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K
speedsl	1098.43	m/s	308.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K

speedsl	1119.00	m/s	303.15	Density and Speed of Sound of Binary Mixtures of N-Methylacetamide with Ethyl Acetate, Ethyl Chloroacetate, and Ethyl Cyanoacetate in the Temperature Interval (303.15 to 318.15) K
srf	0.03	N/m	323.20	KDB
srf	0.02	N/m	298.15	Concentration Dependence of Surface Tension for Very Dilute Aqueous Solutions of Organic Non-Electrolytes
srf	0.02	N/m	298.15	Surface Tension Data of Aqueous Binary Mixtures of Methyl, Ethyl, Propyl, and Butyl Acetates at 298.15 K
tcondl	0.15	W/m×K	268.04	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.15	W/m×K	285.31	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.15	W/m×K	281.34	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.15	W/m×K	274.35	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.15	W/m×K	290.42	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase

tcondl	0.16	W/m×K	260.17	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.16	W/m×K	253.89	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.16	W/m×K	249.13	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	295.44	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	298.52	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	303.53	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	308.44	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	313.45	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	323.25	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	328.39	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase

tcondl	0.13	W/m×K	333.37	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	338.34	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	343.27	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.12	W/m×K	345.43	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.12	W/m×K	348.46	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	318.40	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase

## Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbp	332.82	K	54.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	335.16	K	59.98	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil

tbp	339.42	K	70.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	340.92	K	75.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	343.18	K	80.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	344.93	K	84.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	346.58	K	89.91	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	348.20	K	95.01	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	351.26	K	104.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	352.67	K	109.98	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	355.36	K	119.90	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil

tbp	356.62	K	124.98	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	357.86	K	129.93	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	359.08	K	134.95	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	360.24	K	139.96	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	362.48	K	149.95	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	363.56	K	154.97	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	364.60	K	159.96	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	365.64	K	164.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil



tdp	367.61	K	174.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tdp	368.58	K	180.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tdp	369.50	K	185.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil

## Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.47020e+01
Coeff. B	-3.08216e+03
Coeff. C	-4.45420e+01
Temperature range (K), min.	258.37
Temperature range (K), max.	372.76

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C \cdot \ln(T) + D \cdot T^2$
Coeff. A	8.09498e+01
Coeff. B	-6.86243e+03
Coeff. C	-9.83731e+00
Coeff. D	7.27641e-06
Temperature range (K), min.	189.60
Temperature range (K), max.	523.30

# Datasets

## Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
298.15	100.00	894.0
298.15	1000.00	894.7
298.15	2000.00	895.7
298.15	3000.00	896.7
298.15	3800.00	897.4
298.15	5000.00	898.8
298.15	10000.00	903.4
298.15	15000.00	907.7
298.15	20000.00	912.0
298.15	25000.00	916.1
298.15	30000.00	921.1
298.15	35000.00	926.3
303.15	100.00	887.6
303.15	1000.00	888.5
303.15	2000.00	889.5
303.15	3000.00	890.5
303.15	3800.00	891.3
303.15	5000.00	892.7
303.15	10000.00	897.5
303.15	15000.00	902.0
303.15	20000.00	906.3
303.15	25000.00	910.7
303.15	30000.00	915.9
303.15	35000.00	921.2
308.15	100.00	881.4
308.15	1000.00	882.3
308.15	2000.00	883.3
308.15	3000.00	884.4
308.15	3800.00	885.3
308.15	5000.00	886.7
308.15	10000.00	891.7
308.15	15000.00	896.4
308.15	20000.00	900.9
308.15	25000.00	905.4
308.15	30000.00	910.7

308.15	35000.00	916.2
313.15	100.00	875.2
313.15	1000.00	876.1
313.15	2000.00	877.2
313.15	3000.00	878.3
313.15	3800.00	879.2
313.15	5000.00	880.6
313.15	10000.00	885.8
313.15	15000.00	890.7
313.15	20000.00	895.4
313.15	25000.00	899.8
313.15	30000.00	905.3
313.15	35000.00	910.9
318.15	100.00	868.8
318.15	1000.00	869.8
318.15	2000.00	871.0
318.15	3000.00	872.2
318.15	3800.00	873.1
318.15	5000.00	874.5
318.15	10000.00	880.0
318.15	15000.00	885.1
318.15	20000.00	889.8
318.15	25000.00	894.5
318.15	30000.00	900.1
318.15	35000.00	905.9
323.15	100.00	862.7
323.15	1000.00	864.0
323.15	2000.00	865.1
323.15	3000.00	866.2
323.15	3800.00	867.1
323.15	5000.00	868.6
323.15	10000.00	874.2
323.15	15000.00	879.4
323.15	20000.00	884.3
323.15	25000.00	889.2
323.15	30000.00	895.0
323.15	35000.00	900.9
328.15	100.00	856.4
328.15	1000.00	857.8
328.15	2000.00	859.2
328.15	3000.00	860.5
328.15	3800.00	861.5
328.15	5000.00	862.5
328.15	10000.00	868.4

328.15	15000.00	873.9
328.15	20000.00	879.0
328.15	25000.00	884.1
328.15	30000.00	890.1
328.15	35000.00	896.2
333.15	100.00	850.4
333.15	1000.00	851.7
333.15	2000.00	853.0
333.15	3000.00	854.4
333.15	3800.00	855.4
333.15	5000.00	856.8
333.15	10000.00	862.9
333.15	15000.00	868.5
333.15	20000.00	873.8
333.15	25000.00	879.0
333.15	30000.00	885.2
333.15	35000.00	891.4
338.15	100.00	844.0
338.15	1000.00	845.4
338.15	2000.00	846.8
338.15	3000.00	848.2
338.15	3800.00	849.3
338.15	5000.00	850.8
338.15	10000.00	857.1
338.15	15000.00	863.0
338.15	20000.00	868.5
338.15	25000.00	873.9
338.15	30000.00	880.3
338.15	35000.00	886.7
343.15	100.00	837.5
343.15	1000.00	839.1
343.15	2000.00	840.6
343.15	3000.00	842.0
343.15	3800.00	843.2
343.15	5000.00	844.5
343.15	10000.00	851.2
343.15	15000.00	857.3
343.15	20000.00	863.0
343.15	25000.00	868.5
343.15	30000.00	875.1
343.15	35000.00	881.6
348.15	100.00	829.4
348.15	1000.00	830.5
348.15	2000.00	832.3

348.15	3000.00	833.8
348.15	3800.00	835.0
348.15	5000.00	836.8
348.15	10000.00	845.5
348.15	15000.00	851.8
348.15	20000.00	857.7
348.15	25000.00	863.5
348.15	30000.00	870.2
348.15	35000.00	877.0
353.15	1000.00	824.3
353.15	2000.00	826.0
353.15	3000.00	827.5
353.15	3800.00	828.8
353.15	5000.00	830.6
353.15	10000.00	837.7
353.15	15000.00	844.3
353.15	20000.00	850.4
353.15	25000.00	856.1
353.15	30000.00	862.7
353.15	35000.00	869.6
358.15	1000.00	818.4
358.15	2000.00	820.0
358.15	3000.00	821.6
358.15	3800.00	822.8
358.15	5000.00	824.7
358.15	10000.00	832.1
358.15	15000.00	838.9
358.15	20000.00	845.2
358.15	25000.00	851.0
358.15	30000.00	857.6
358.15	35000.00	864.7
363.15	1000.00	811.8
363.15	2000.00	813.5
363.15	3000.00	815.3
363.15	3800.00	816.6
363.15	5000.00	818.5
363.15	10000.00	826.3
363.15	15000.00	833.3
363.15	20000.00	839.7
363.15	25000.00	845.8
363.15	30000.00	852.9
363.15	35000.00	860.2
368.15	1000.00	804.9
368.15	2000.00	806.8

368.15	3000.00	808.6
368.15	3800.00	810.0
368.15	5000.00	812.1
368.15	10000.00	820.2
368.15	15000.00	827.5
368.15	20000.00	834.3
368.15	25000.00	840.6
368.15	30000.00	848.0
368.15	35000.00	855.5
373.15	1000.00	798.5
373.15	2000.00	800.4
373.15	3000.00	802.4
373.15	3800.00	803.8
373.15	5000.00	806.0
373.15	10000.00	814.4
373.15	15000.00	822.0
373.15	20000.00	829.0
373.15	25000.00	835.5
373.15	30000.00	843.0
373.15	35000.00	850.6
378.15	1000.00	791.8
378.15	2000.00	793.8
378.15	3000.00	795.8
378.15	3800.00	797.3
378.15	5000.00	799.6
378.15	10000.00	808.5
378.15	15000.00	816.5
378.15	20000.00	823.7
378.15	25000.00	830.5
378.15	30000.00	838.4
378.15	35000.00	846.3
383.15	1000.00	784.8
383.15	2000.00	787.1
383.15	3000.00	789.1
383.15	3800.00	790.8
383.15	5000.00	793.2
383.15	10000.00	802.4
383.15	15000.00	810.7
383.15	20000.00	818.2
383.15	25000.00	825.3
383.15	30000.00	833.5
383.15	35000.00	841.6
388.15	1000.00	778.2
388.15	2000.00	780.5







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The potential of head-space gas chromatography for VLE measurements and correlation of solubility and solution thermodynamics

Specific Heat Measurements and the Correlation of 1-Naphthaleneacetic Acid in Pure and Methyl Propyl Ketone Binary Liquid Mixtures of (278.25 to 320.55) K: Solubility with Aliphatic Esters of  $\alpha$ -Naphthalene and Ethanol to 3 Butanol: Solubility Measurements and modelling of 1,8-dinitronaphthalene in nine binary and quaternary mixtures for 273.15 to 303.15 K and Ethyl Acetate + Butyl Alcohol: Properties of Binary and Ternary Mixtures of Ethyl Acetate, Ethanol and dynamic models for determination of the solubility of 1,8-dinitronaphthalene in binary and ternary mixtures at different temperatures and pressures at different solvents from  $T = (278.15 \text{ to } 320.15) \text{ K}$  and Thermodynamic Behavior of Veramoss in Different Pure Solvents and {Ethanol + Water} Mixtures from  $T = (278.15 \text{ to } 320.15) \text{ K}$  in Different Solvents and Temperatures from 273.15 to 320.15 K and Dissolution of 1,8-dinitronaphthalene in the Solubility of 1,8-dinitronaphthalene in Pure and Water-Ethanol Mixture Solvents: Solubility temperatures from 293.15 to 353.15 K Liquid Equilibria of the trans-1,2-Cyclohexanediol + Ethyl Acetate and trans-1,2-Cyclohexanediol + Ethyl Methanol, Ethanol, Acetone, and Ethyl Acetate: Solubility in Methanol K:

**Activity Coefficients at Infinite Dilution for Hydrocarbons in Fatty Alcohols Determined by Equilibrium at 350 K, Excess Molar Enthalpies at 298 K, and Excess Molar Volume Mixtures Based on Binary Mixing Coefficients Entailing Solvents and Organic Substances and a Selfing System of Ethyl Acetate and Propyl Acetate, Ethyl Acetate, Propanamide, and their Derivatives in Organic Solvents and Mixing Property of 2,5-Dinitro-2-methylbenzoic Acid in 1,3-Difluorobenzene from 276.15 to 333.15 K: Thermodynamic Properties of Benzophenone, Diethyl Ether, Methanol, Propanone, Fluoromethane, and Nitrate, and Thermochemical Properties of Isomeric Compounds in Water and Other Neat or Aqueous Solutions from 276.15 to 311.15 K; and Water-Miscible Binary Solvents as a Function of Infinite Dilution at 18.15 °C: Amide Compounds in the Ionic Liquid Thermal Acid Indifferentium chloride: Solubilities from 276.15 K to Different Organic Solvents at Several Temperatures from 211.5 to Hexane, Ethyl Acetate, Diethyl Ether, and Ethanol from 293.15 to 323.15 K: Different Solvents between 278 K and Solubility of Lovastatin in Ethyl Acetate, Propyl Acetate, Isopropyl Alcohol, Butylacetate, and Butyl Thermodynamic Model Correlation of Pure and Binary Mixtures of Binary Mixtures of Methyl, Ethyl, Propyl and Isopropyl Acetate and Binary Mixtures of N-Methylacetamide with Measurement of Activity Coefficients of Solutes at Infinite Dilution Temperature Dependence of the Free Energy of Solution of Urea and Guanidinium in 1,4-Dioxane from 25 to 40 °C: Temperature Dependence of Solubility in the absence and presence of co-solvent organic compounds with the ionic liquids Determination and Correlation of the Solubility of Male Ketone in Pure and Binary Systems from 273.15 to 313.15 K: Solubility of Gracitidine in Different Pure Solvents and Binary Mixtures:**



Activity coefficient at infinite dilution measurements for organic solutes

Effects of temperature and concentration on interactions in the critical states for the quaternary systems of the quaternary ammonium salts and the organic solvents

2-dioxaphosphorinane-5,5-dimethyl-2-one in ethyl acetate and in several pure solvents: Measurement, correlation, and solvent effect

Hydrazine carbonylation and thermodynamic modeling of 38.15 K: 1,3-dimethyl-2-oxo-1,2,3,4-tetrahydro-2H-pyridine-4-one in ethyl acetate and in several pure solvents from (287 to 323) K: Isobaric Vapor-Liquid Equilibrium for Ethyl Acetate + Ethanol + Solubility measurements and correlation of the form of rutin in organic solvents from 273.15 to 323.15 K in Pure and Binary Solvent Mixtures and Thermodynamic and Molecular Parameters at infinite dilution for organic compounds in ethyl acetate + Ethyl Acetate + Oleic Acid mixtures at high pressure

2-Chloro-4,6-dinitroresorcinol in Ethanol: Thermodynamic Data for Binary Mixtures of Dimethyl Carbonate with Methanol, Ethyl Acetate, 4-Amino-2-methylphenol, and Six Monofluorinated Phenols at 298.15 K: Solubility of five aliphatic esters in the liquid and thermodynamic functions of tebuconazole in nine solvents from T = (278.15 to 323.15) K: 17- $\alpha$ -Epoxyprogesterone in different solvents: Correlation, and Solute-Solvent Molecular Interactions of Phenylglyoxime methyl ether in methanol, water and in organic and inorganic liquids in extraction of boron from water phase using organic solvents

Thermodynamic functions of separation processes based on binary organic solvents at temperatures from (248.2 to 323.15) K: Coefficients at infinite dilution of organic solutes in various solvents

Equilibrium for Several Compounds in the Vapor Phase: Industry Related with the Wilson Equation: Solubility of 3-chloro-N-phenylphthalimide in ten solvents from T = (288.15 to 323.15) K: Thermodynamic and thermodynamic properties of (methanol and methylamine) mixtures from T = (273.15 to 323.15) K: Determination and correlation of the thermodynamic properties of solid liquid and liquid liquid mixtures of Surface active agents: Thermodynamic properties of organic non-electrolytes: Solubility of mifepristone in Eight Pure and Water of methanol mixed solvents at temperatures from 273.15 to 318.15 K: Solubility and limiting activity coefficient of simvastatin in different organic solvents and theoretical study of interaction between organic solid liquid and liquid

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**Thermodynamics and activity coefficients at infinite dilution for organic acids in water-organic liquid mixtures**

(Model for binary mixtures containing ethyl acetate and propyl acetate, methyl acetate and ethyl acetate, and ethyl acetate and propyl acetate)

Solvent: Organic liquids: Hydroxyacetone - Water and Binary Solvent Mixtures

Temperature: (298.15 and 313.15) K and solubility parameters:

Nitrobenzene-methylamine-Pure Solvents from (293.15 to 343.15) K:

Solubility of tridecanedioic acid in pure solvent systems: An experimental and computational study

Activity Coefficients at Infinite Dilution by GLC in Alkanediamines as Solubility Parameters and modelling of 4-nitro-1,2-phenylenediamine in Measurment and Correlation of the Distribution Equilibrium of o-Iodoaniline and p-Toluenedinitrobenzene in solutions: solubility of ciclosoxide in seven pure solubilities of phosphoramidic Acid, N-(phenylmethyl)-, Diphenyl Ester in Binary Equilibrium Solubility of Amidinothiourea in Monosolvents: Experimental measurements and Model thermodynamic properties effect

Methylpropylacetate in Green Solvent and Solvated of hydrogen chloride ions in twelve Pure Organic Solutes in 1-ethyl-3-(3-dimethylammonium) carbodiimide + (propanol) and diethyl carbonate at PCP 298.15 Modified Supercritical Carbon Dioxide A (306.76-320.00) K

Pyridinium-based ionic liquid in the separation processes: Interactions of volatile organic compounds with the ionic liquid Part II: Coefficients of Organic Compounds in New Imidazolium and Tetrahydropyran Derivatives Properties of Salts Using Inverse Gas Chromatography and Solubility of Bioactive Compound Reserpine in Eight Green Solvents Refractive Index Spectra of Sound at 298.15 K, and Vapor-Liquid Thermodynamic Properties of Asymmetric and symmetric binary organic solvents: Liquid-liquid equilibria of water + Ethyl Lactate and Methyl Acetate + Ethyl 2-hydroxy-2-butanone + ethyl acetate coefficients at Infinite Dilution of Organic Solutes in Measurement and correlation of the partition coefficient between hexan-2-one and n-octane for binary mixtures of organic esters with gamma-butyrolactone

Methylcyclopentadiene and Thermodynamic Models for Miscibility of Ether at 298.15 K and Water

Excess Gibbs Energies of Ethylacrylate + Diethylphosphorothioate in Different Pure Solvents from (293.15 to 313.15) K

Supercritical Behavior and Saturated Pressure for Carbon Dioxide + Ethyl Acetate at Temperatures up to 313.15 K: thermodynamic properties of Measurement and Correlation of Solvents: Solubility of Amorphous Cefmetazole Solid in Lipid Phase Equilibrium Binary Solubility of Dibenzofuran and Sulfolane-modelling Solubility Solvents: thermodynamics and preferential Solvent for chloroform in soft fat phases of ethyl acetate + (methanol, dimethylacetone and dimethylsiloxane) pure components Data for the Ethyl Acetate Hexamethylenes in octyl Systems in Butyric Acid, Ethyl Acetate, Dimethylpyrrolidine, and

Solid-liquid phase equilibrium for tetrahydrofuran-gamma-butyrolactone + Ethyl acetate-Ethyl Acetate and (298.2 to 313.15) K temperature and thermodynamic modeling of n-pentylazobenzene in organic solvents from T = (278.15 to 318.15) K and mixing properties of solutions:

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Activity coefficients at infinite dilution for organic solutes and water in Determination and Thermodynamic Analysis of the Solubility of Limonin in Binary and Ternary Systems in Pure Organic Solvents and Mixtures of Ethyl Acetate + Ethanol + Water; Thermodynamic Properties of Limonin in Different Solvents and Dissociation Equilibrium of Limonin in Ethyl acetate + ethanol mixtures at several temperatures and correlation with the McGowan's model; tetrahydrophenanthrene organic solvents from 283.2 to 309.6 K of Theobromine, Theophylline, and Caffeine solubility and thermodynamic properties in binary systems and correlation of (278.15 to 313.15) K of benzenediacetic acid in different solvents and correlation of the solubility of d-Pantolactone in Four Pure Solvents Solubility in Binary and Ternary Solvents: Effect of Molecular Interaction and Analysis of Crystallized Products; Study on thermo physical and excess molar properties of binary systems of Measurment and Correlation ( $\alpha = 6, 8$ ) Solubility and Dissolution Prediction and Problems, P.P. (1-2)-Piperazine dihydrochloride in pure and binary solvent systems for Some Aliphatic Esters from (298 to 393) K and thermodynamic properties of (an ester + an alkane). XVI. Experimental HEM and Thermodynamic Modeling of the Diffusion Coefficient of Sulfuric Acid in Methanol-Ethyl Alcohol Mixture and Modeling of Methanol and Ethanol in Ethyl Alcohol Mixture (Methanol-Ethanol) in Pure and Binary Solvent Systems; Thermodynamic Properties of the System Ethyl Acetate + Ethanol + 2-Amino-4-chloro-6-methoxypyrimidine in Various Organic Solvents; Gallic Acid Using Thermodynamic Data in Different Classes of Organic Acid and Oleonic Acid in Four Solvents from Measurement and Correlation of the Solubility of 5-Fluorouracil in Pure and Binary Systems; correlations for describing the thermodynamic measurement and correlation of pentyl acetylacetone measured in 11 ethanolic and acetic acid solutions; 2, 3-pyridine dicarboxylic acid + water + acetic acid - acetate esters at equilibrium of 0.32 K 4-hydroxy-2,5-dimethyl-3(2H)-furanone Measurement and correlation for solubility of levofloxacin in six solvents; Solubility parameters of solid compounds predicting the type of solubility profile and application of thermodynamic thermodynamic model correlation of partitioning of surface and solubility Properties of N-Vinylimidazolium Tetrafluoroborate in Organic Media; Correlation of the Functional Groups of Cinnamic Acid Esters in Organic Solvents; Densities and Speeds of Sound of Binary Liquid Mixtures of Some Solubility of Proxime Hydrochloride Hemisalts between 286.0 and 363 K: Isobaric Vapor Pressure of Ethyl Acetate + Ethanol + Ethylmethylimidazolium Acetic Acid TriFluoromethanesulfonate at 100 kPa: 273.15 to 323.15 K and thermodynamic properties in a binary mixture of methanol and 1,5-Naphthalenediamine and 1,8-Naphthalenediamine in Different Solvents and Mixing Properties of Solutions;

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**Equilibrium Solubility of Biapenem in Different Neat and Binary Solvents:** Effect of temperature, salinity on the solubility of biapenem in neat and binary solvents.

**Vapor-Liquid Equilibrium of the Ethyl Methyl Ether Mixtures in**

(2,4,6-trimethyl-1,3,5-trioxane + n-alkyl alcohols at T=298.15, 303.15, and 307.2 K) by cosolvent and its determination in the solubility Acree and Danner equation and entropy of activation of different mixtures as function of dilution affect physicochemical properties for organic solvents and water in the hydroxyacetic acid in pure and binary solutions of dimethyl-1-methylpyrrolidinium 2,4-dinitrophenylalanine imide; Monosolvents at (298.15 to 308.15 K) of binary hydrocarbons mixtures based on solubility data and measurement of clopidogrel hydrogen sulfate monomer and copolymer solubility and mixing properties of L-malic acid in partially miscible organic solvents; Thermodynamic Data of Mefenamic Acid in Pure and Different Classes of Mixed Solvents at 273.15-313.15 K and Its Behavior in Solution

**Thermodynamic Models:**

Born-Haber cycle approach to liquid equilibrium data and desorption from 278.15 to 303.15 K of carbon dioxide + ethyl acetate systems of ethyl acetate and carbon dioxide for the binary mixtures of 2,3-butenediol with urethane diisocyanates and acrylonitrile and methyl methacrylate with phenol S-bis (5-isopropyl-1,3,5-triazin-2-yl)-phosphoranyl-ene ligands at infinite dilution of polymer blends in the solid liquid coexisting regions from 283.15 to 293.15 K; Volumetric and transport properties of ternary mixtures containing 1-alkanol + bisurethane derivatives solution of bicyclic and Displacement of the Effect of Temperature and Correlation of the Solubility of maleic anhydride in different organic solvents

**Solubility of e-CL-20 in 12 Organic Experiments Temperature Ranging Solubility and Dissolution Properties for Ethylphenylacetamide and Modeling p-Toluene in Pure Solvents;**

Monofluorobenzene vapor phase modeling current covers title in Binary Solvent Systems of 2,3-Dichloropropane of Benzene and Nitrogen (Ethyl acetate and Carbon dioxide) Several temperatures Carbon Dioxide + Ethyl Propanoate and Carbon Isocyanide Vapor Liquid Phase

**Equilibrium Measurements for 1MPa, 1MPa and 1MPa Pressure ENH 595 with dimethyl Sulfoxide at 101.3 kPa:**

Thermodynamic study of (alkyl esters + α,x-alkyl dihalides) I: HE and V E for 25 dissociation constants and 1020 J/mol of Danderson Consistency in Different Solubility and thermodynamic properties of vanillyl alcohol in some organic solvents.Mixing Thermodynamics Properties of p-Toluenesulfonamide liquid-liquid equilibrium data Seven Monosolvents (propylene acetonitrile) tetrahydrofuran and 2-propanone, and Solubility of Phenylbutazone in Monosolvents and Binary Solventary Mixtures-Containing Ethylene Glycol, Methoxybenzene and Benzene Diolative, Solubility of acetate :

Measurement of enthalpy of fusion of the solubility Solvents:

297.45 K and 303.15 K Enthalpy for Ethyl Acetate Acetonitrile + Butylacetate and propylalcohol from 2,5-Dimethyl-2-(phenyl)(phenylamino)maleic anhydride solvent mixtures between 270 K and 310 K Hydrogen chloride in 12 Monosolvents and Solvent Mixtures of Methanol + (Ethanol, N,N-Dimethylformamide or Ethyl Acetate);

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**l-phosphabicyclo[2.2.2]octane**  
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Solubilities of Organic Semiconductors and Nonsteroidal Anti-inflammatory Drugs in pure and mixed solvents at 298.15 K: Measurement and Modeling <https://www.doi.org/10.1021/acs.jced.8b00536>

Solubilities of alkyamines in organic solvents at 298.15 K: Measurement and Modeling <https://www.doi.org/10.1016/j.fluid.2007.07.030>

Self-Association of 2-Chloronicotinic Acid and Analysis of Hydrophobic Solubility Parameter: Determination and correlation of solubility and solution thermodynamics <https://www.doi.org/10.1021/acs.jced.9b00661>

Studies of viscosity of dilute solutions of alkylamine in non-aqueous solvents <https://www.doi.org/10.1016/j.jct.2019.03.029>

Equilibrium Data for Vapor-Liquid Equilibria and other polar solvents: <https://www.doi.org/10.1016/j.tca.2004.08.013>

Equilibrium Data for Vapor-Liquid Equilibria and other polar solvents: [http://www.ddbst.com/en/EED/VLE/VLE%20Acetonitrile%3BEthyl acetate.php](http://www.ddbst.com/en/EED/VLE/VLE%20Acetonitrile%3BEthyl+acetate.php)

## Legend

<b>af:</b>	Acentric Factor
<b>affp:</b>	Proton affinity
<b>aigt:</b>	Autoignition Temperature
<b>basg:</b>	Gas basicity
<b>chl:</b>	Standard liquid enthalpy of combustion
<b>cpg:</b>	Ideal gas heat capacity
<b>cpl:</b>	Liquid phase heat capacity
<b>dm:</b>	Dipole Moment
<b>dvisc:</b>	Dynamic viscosity
<b>fl:</b>	Lower Flammability Limit
<b>flu:</b>	Upper Flammability Limit
<b>fpc:</b>	Flash Point (Closed Cup Method)
<b>fpo:</b>	Flash Point (Open Cup Method)
<b>gf:</b>	Standard Gibbs free energy of formation
<b>gyrad:</b>	Radius of Gyration
<b>hf:</b>	Enthalpy of formation at standard conditions
<b>hfl:</b>	Liquid phase enthalpy of formation at standard conditions
<b>hfus:</b>	Enthalpy of fusion at standard conditions
<b>hfust:</b>	Enthalpy of fusion at a given temperature
<b>hvap:</b>	Enthalpy of vaporization at standard conditions
<b>hvapt:</b>	Enthalpy of vaporization at a given temperature
<b>ie:</b>	Ionization energy
<b>log10ws:</b>	Log10 of Water solubility in mol/l
<b>logp:</b>	Octanol/Water partition coefficient
<b>mcvol:</b>	McGowan's characteristic volume
<b>nfpaf:</b>	NFPA Fire Rating
<b>pc:</b>	Critical Pressure
<b>pvap:</b>	Vapor pressure
<b>rfi:</b>	Refractive Index
<b>rhoc:</b>	Critical density
<b>rhof:</b>	Liquid Density
<b>rinpol:</b>	Non-polar retention indices

<b>ripol:</b>	Polar retention indices
<b>sfust:</b>	Entropy of fusion at a given temperature
<b>sg:</b>	Molar entropy at standard conditions
<b>sl:</b>	Liquid phase molar entropy at standard conditions
<b>speedsl:</b>	Speed of sound in fluid
<b>srf:</b>	Surface Tension
<b>tb:</b>	Normal Boiling Point Temperature
<b>tbp:</b>	Boiling point at given pressure
<b>tc:</b>	Critical Temperature
<b>tcondl:</b>	Liquid thermal conductivity
<b>tf:</b>	Normal melting (fusion) point
<b>tt:</b>	Triple Point Temperature
<b>vc:</b>	Critical Volume
<b>zc:</b>	Critical Compressibility
<b>zra:</b>	Rackett Parameter

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