Ethyl Acetate

Other names:	1-Acetoxyethane
	Acetic acid, ethyl ester
	Acetic ether
	Acetidin
	Acetoxyethane
	Aethylacetat
	CH3COOC2H5
	Essigester
	Ethyl acetic ester
	Ethyl ester of acetic acid
	Ethyl ethanoate
	Ethylacetaat
	Ethyle (acetate d')
	Ethylester kyseliny octove
	Etile (acetato di)
	NSC 70930
	Rcra waste number U112
	UN 1173
	Vinegar naphtha
	ac. acetic ethyl ester
Inchi:	InChI=1S/C4H8O2/c1-3-6-4(2)5/h3H2,1-2H3
InchiKey:	XEKOWRVHYACXOJ-UHFFFAOYSA-N
Formula:	C4H8O2
SMILES:	CCOC(C)=O
Mol. weight [g/mol]:	88.11
CAS:	141-78-6

Physical Properties

Property code	Value	Unit	Source
af	0.3620		KDB
affp	835.70	kJ/mol	NIST Webbook
aigt	699.82	K	KDB
basg	804.70	kJ/mol	NIST Webbook
basg	799.90 ± 0.20	kJ/mol	NIST Webbook
chl	-2256.00	kJ/mol	NIST Webbook
chl	-2235.40 ± 3.90	kJ/mol	NIST Webbook
chl	-2246.00	kJ/mol	NIST Webbook

chl	-2238.54 ± 0.48	kJ/mol	NIST Webbook
dm	1.90	debye	KDB
dvisc	0.0004260	Pa×s	Densities and Viscosities of Ternary Mixtures of Cyclohexane + Cyclohexanone + Some Alkyl Acetates at 298.15 K
dvisc	0.0004274	Pa×s	Densities and Viscosities of Binary Liquid Mixtures of Trichloroethylene and Tetrachloroethylene with Some Polar and Nonpolar Solvents
dvisc	0.0004370	Pa×s	A volumetric and viscosity study for the binary mixtures of 1-hexyl-3-methylimidazolium tetrafluoroborate with some molecular solvents
fll	2.20	% in Air	KDB
flu	9.00	% in Air	KDB
fpc	285.93	K	KDB
fpo	268.71	K	KDB
gf	-327.60	kJ/mol	KDB
gyrad	3.3480		KDB
hf	-446.90	kJ/mol	NIST Webbook
hf	-443.20	kJ/mol	KDB
hf	-445.43 ± 0.84	kJ/mol	NIST Webbook
hf	-443.80	kJ/mol	NIST Webbook
hf	-444.80 ± 0.40	kJ/mol	NIST Webbook
hfl	-480.57 ± 0.79	kJ/mol	NIST Webbook
hfl	-479.86 ± 0.46	kJ/mol	NIST Webbook
hfl	-478.82 ± 0.73	kJ/mol	NIST Webbook
hfl	-482.00 ± 4.00	kJ/mol	NIST Webbook
hfus	8.90	kJ/mol	Joback Method
hvap	33.65	kJ/mol	Joback Method
ie	10.24	eV	NIST Webbook
ie	9.90 ± 0.05	eV	NIST Webbook
ie	10.11 ± 0.02	eV	NIST Webbook
ie	10.00 ± 0.10	eV	NIST Webbook
ie	10.01 ± 0.05	eV	NIST Webbook
ie	10.16	eV	NIST Webbook
ie	10.09 ± 0.02	eV	NIST Webbook
ie	10.45	eV	NIST Webbook
ie	10.01 ± 0.05	eV	NIST Webbook
ie	9.90	eV	NIST Webbook
log10ws	-0.04		Estimated Solubility Method

log10ws	-0.04		Aqueous Solubility Prediction Method
logp	0.569		Crippen Method
mcvol	74.660	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
pc	4280.00 ± 405.30	kPa	NIST Webbook
pc	3830.00 ± 81.06	kPa	NIST Webbook
pc	3851.70 ± 40.00	kPa	NIST Webbook
pc	4018.00 ± 202.65	kPa	NIST Webbook
pc	3900.00	kPa	Critical Properties of the Reacting Mixture in the Esterification of Acetic Acid with Ethanol
pc	3882.00 ± 3.87	kPa	NIST Webbook
pc	3882.00	kPa	KDB
rhoc	307.66 ± 5.29	kg/m3	NIST Webbook
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tb	350.10 ± 2.00	K	NIST Webbook
tb	350.30 ± 2.00	K	NIST Webbook
tb	350.20 ± 2.00	K	NIST Webbook
tb	350.30 ± 2.00	K	NIST Webbook
tb	347.45 ± 2.00	K	NIST Webbook

tb	350.30 ± 0.50	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tb	350.16	K	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tb	350.30 ± 0.50	K	NIST Webbook
tb	349.90 ± 0.20	K	NIST Webbook
tb	347.45 ± 2.00	K	NIST Webbook
tb	350.25 ± 1.00	K	NIST Webbook
tb	350.26	K	KDB
tb	350.27	K	Vapor liquid equilibria for the quaternary reactive system ethyl acetate + ethanol +water + acetic acid and some of the constituent binary systems at 101.3 kPa
tb	350.24	K	Vapor liquid equilibria for the binary mixtures of 2,3-butanediol with n-butanol, n-butyl acetate, and ethyl acetate at 101.3 kPa
tb	350.24	K	Liquid-liquid equilibria of water + 3-hydroxy-2-butanone + ethyl ethanoate
tb	350.20	K	Solubility and tie-line data for ternary aqueous mixtures of cyclopentanol with organic solvents at T = 298.2 K: Experiments and NRTL model
tb	350.15	K	The isobaric vapor liquid equilibria of ethyl acetate p acetonitrile p bis(trifluoromethylsulfonyl)imide-based ionic liquids at 101.3 kPa
tb	350.29	K	Isobaric vapor-liquid equilibrium of a ternary system of ethyl acetate + propyl acetate + dimethyl sulfoxide and binary systems of ethyl acetate + dimethyl sulfoxide and propyl acetate + dimethyl sulfoxide at 101.3 kPa
tb	350.35	K	Isobaric Vapor - Liquid Equilibrium for Ethyl acetate + Methanol + Ionic Liquids Ternary systems at 101.3 kPa
tb	350.30 ± 0.20	K	NIST Webbook

tb	350.20	K	Isobaric Vapor Liquid Equilibrium for Three Binary Systems of Acetaldehyde + Ethanol, Ethyl Acetate, 1-Butanol at 101.3 kPa
tb	349.95	K	Effect of Ionic Liquids on the Binary Vapor-Liquid Equilibrium of Ethyl Acetate + Methanol System at 101.3 kPa
tb	350.28	K	Isobaric Vapor-Liquid Phase Equilibrium Measurements for Allyl Alcohol with Chloroform, Ethyl Acetate, and Methyl Propionate at 101.3 kPa
tb	350.25	K	Isobaric Vapor-Liquid Equilibria and Excess Quantities for Binary Mixtures of an Ethyl Ester + tert-Butanol and a New Approach to VLE Data Processing
tb	350.15	K	Vapor-Liquid Equilibrium of Binary Mixtures Containing Ethyl Acetate + 2-Methyl-1-propanol and Ethyl Acetate + 2-Methyl-1-butanol at 101.3 kPa
tb	350.21	K	Volumetric Behavior and Saturated Pressure for Carbon Dioxide + Ethyl Acetate at a Temperature of 313.15 K
tb	350.15	K	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
tb	350.19	K	Experimental Determination of Vapor Liquid Equilibria. Binary Systems of Methyl Acetate, Ethyl Acetate, and Propyl Acetate with 1-Propanol at 0.6 MPa
tb	350.13 ± 0.30	K	NIST Webbook
tb	350.20	K	NIST Webbook
tb	350.00	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	349.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tb	350.30	K	NIST Webbook

tb	350.25 ± 0.30	K	NIST Webbook
tb	350.19 ± 0.50	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tb	350.30 ± 0.30	K	NIST Webbook
tb	375.00 ± 2.00	K	NIST Webbook
tb	350.35	K	NIST Webbook
tb	350.05 ± 0.30	K	NIST Webbook
tb	350.21 ± 0.50	K	NIST Webbook
tb	350.25 ± 0.50	K	NIST Webbook
tb	350.30 ± 0.30	K	NIST Webbook
tb	350.00 ± 2.00	K	NIST Webbook
tb	350.29 ± 0.15	K	NIST Webbook
tb	350.15 ± 2.00	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 0.50	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.65 ± 2.00	K	NIST Webbook
tb	349.65 ± 2.00	K	NIST Webbook
tb	352.15 ± 2.00	K	NIST Webbook
tb	350.25 ± 1.00	K	NIST Webbook
tb	350.30 ± 1.00	K	NIST Webbook
tb	350.30 ± 1.00	K	NIST Webbook
tb	349.97 ± 2.00	K	NIST Webbook
tb	351.15 ± 2.00	K	NIST Webbook
tb	350.45 ± 1.00	K	NIST Webbook
tb	350.25 ± 1.00	K	NIST Webbook
tb	350.30 ± 0.40	K	NIST Webbook
tb	349.15 ± 2.00	K	NIST Webbook
tb	349.65 ± 2.50	K	NIST Webbook
tb	350.26 ± 0.06	K	NIST Webbook
tb	350.30 ± 0.15	K	NIST Webbook
tb	350.00 ± 2.00	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.15 ± 2.00	K	NIST Webbook
tb	349.95 ± 2.00	K	NIST Webbook
tb	350.20 ± 0.50	K	NIST Webbook
tb	350.30 ± 0.20	K	NIST Webbook
tb	350.25 ± 0.50	K	NIST Webbook
tb	350.21 ± 0.50	K	NIST Webbook
tb	349.65 ± 2.00	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook
tb	350.30 ± 0.50	K	NIST Webbook

tb	350.30 ± 0.50	K	NIST Webbook
tb	350.45 ± 0.60	K	NIST Webbook
tb	350.25 ± 0.30	K	NIST Webbook
tb	350.25 ± 1.00	K	NIST Webbook
tc	523.29	K	Development of a Predictive Equation of State for CO2 + Ethyl Ester Mixtures Based on Critical Points Measurements
tc	523.30	K	KDB
tc	513.00 ± 6.00	K	NIST Webbook
tc	522.70 ± 2.00	K	NIST Webbook
tc	523.30 ± 1.00	K	NIST Webbook
tc	523.30 ± 1.00	K	NIST Webbook
tc	523.30 ± 0.05	K	NIST Webbook
tc	523.20	K	NIST Webbook
tc	548.90 ± 20.00	K	NIST Webbook
tf	189.50	K	KDB
tf	189.25	K	Aqueous Solubility Prediction Method
tt	189.30 ± 0.20	K	NIST Webbook
tt	189.30 ± 0.05	K	NIST Webbook
vc	0.286	m3/kmol	KDB
zc	0.2551730		KDB
zra	0.25		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	125.82	J/mol×K	360.00	NIST Webbook
cpg	131.06	J/mol×K	380.00	NIST Webbook
cpg	136.22	J/mol×K	400.00	NIST Webbook
cpg	142.80	J/mol×K	425.00	NIST Webbook
cpg	149.47	J/mol×K	450.00	NIST Webbook
cpl	169.20	J/mol×K	293.60	NIST Webbook
cpl	170.59	J/mol×K	298.32	NIST Webbook
cpl	169.30	J/mol×K	298.15	NIST Webbook
cpl	168.94	J/mol×K	298.15	NIST Webbook
cpl	169.06	J/mol×K	298.15	NIST Webbook
cpl	169.60	J/mol×K	298.15	NIST Webbook
cpl	169.60	J/mol×K	298.15	NIST Webbook
cpl	167.40	J/mol×K	298.15	NIST Webbook

cpl	169.50	J/mol×K	298.10	NIST Webbook
cpl	168.82	J/mol×K	303.61	NIST Webbook
cpl	157.70	J/mol×K	290.00	NIST Webbook
dvisc	0.0003300	Pa×s	323.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003630	Pa×s	313.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003990	Pa×s	303.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004210	Pa×s	298.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004430	Pa×s	293.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004030	Pa×s	303.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure

dvisc	0.0004260	Pa×s	298.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
dvisc	0.0003870	Pa×s	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
dvisc	0.0004280	Pa×s	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
dvisc	0.0003810	Pa×s	308.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters

dvisc	0.0004260	Pa×s	298.15	Density, dynamic viscosity, and derived properties of binary mixtures of methanol or ethanol with water, ethyl acetate, and methyl acetate at T = (293.15, 298.15, and 303.15) K	
dvisc	0.0004520	Pa×s	293.15	Density, dynamic viscosity, and derived properties of binary mixtures of methanol or ethanol with water, ethyl acetate, and methyl acetate at T = (293.15, 298.15, and 303.15) K	
dvisc	0.0003460	Pa×s	318.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters	
dvisc	0.0003440	Pa×s	313.15	Volumetric and Transport Properties of Binary Liquid Mixtures of Phenylacetonitrile with Aliphatic Esters at Temperatures of (303.15 to 313.15) K	
dvisc	0.0003610	Pa×s	308.15	Volumetric and Transport Properties of Binary Liquid Mixtures of Phenylacetonitrile with Aliphatic Esters at Temperatures of (303.15 to 313.15) K	

dvisc	0.0003790	Pa×s	303.15	Volumetric and Transport Properties of Binary Liquid Mixtures of Phenylacetonitrile with Aliphatic Esters at Temperatures of (303.15 to 313.15) K	
dvisc	0.0003426	Pa×s	313.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K	
dvisc	0.0003622	Pa×s	308.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K	
dvisc	0.0003806	Pa×s	303.15	Densities, Viscosities, and Speeds of Sound of Binary Liquid Mixtures of Sulfolane with Ethyl Acetate, n-Propyl Acetate, and n-Butyl Acetate at Temperature of (303.15, 308.15, and 313.15) K	
dvisc	0.0002750	Pa×s	343.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters	
dvisc	0.0002880	Pa×s	338.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters	

dvisc	0.0004520	Pa×s	293.15	Dynamic Viscosities, Densities, and Speed of Sound and Derived Properties of the Binary Systems Acetic Acid with Water, Methanol, Ethanol, Ethyl Acetate and Methyl Acetate at T = (293.15, 298.15, and 303.15) K at Atmospheric Pressure
dvisc	0.0003010	Pa×s	333.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0003150	Pa×s	328.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0004030	Pa×s	303.15	Density, dynamic viscosity, and derived properties of binary mixtures of methanol or ethanol with water, ethyl acetate, and methyl acetate at T = (293.15, 298.15, and 303.15) K
hfust	10.48	kJ/mol	189.30	NIST Webbook
hfust	10.48	kJ/mol	189.30	NIST Webbook
hfust	10.48	kJ/mol	189.30	NIST Webbook
hvapt	33.80 ± 0.10	kJ/mol	326.00	NIST Webbook
hvapt	35.70	kJ/mol	319.50	NIST Webbook
hvapt	36.70	kJ/mol	322.00	NIST Webbook
hvapt	34.60 ± 0.10	kJ/mol	313.00	NIST Webbook
hvapt	31.40 ± 0.10	kJ/mol	343.00	NIST Webbook
hvapt	34.10	kJ/mol	345.00	NIST Webbook
hvapt	33.40 ± 0.10	kJ/mol	331.00	NIST Webbook
hvapt	31.90 ± 0.10	kJ/mol	351.00	NIST Webbook
hvapt	31.00 ± 0.10	kJ/mol	363.00	NIST Webbook
hvapt	34.00	kJ/mol	320.00	NIST Webbook
hvapt	31.90	kJ/mol	350.00	NIST Webbook
hvapt	31.94	kJ/mol	350.30	NIST Webbook

hvapt	32.22	kJ/mol	349.80	KDB
hvapt	32.40 ± 0.10	kJ/mol	344.00	NIST Webbook
pvap	139.07	kPa	360.03	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	160.53	kPa	364.81	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	163.99	kPa	365.52	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	155.58	kPa	363.72	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	150.43	kPa	362.62	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	146.37	kPa	361.73	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	167.81	kPa	366.29	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	171.33	kPa	367.00	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	174.65	kPa	367.64	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	176.37	kPa	367.98	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	180.88	kPa	368.83	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	184.43	kPa	369.49	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	

pvap	187.47	kPa	370.07	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	190.92	kPa	370.69	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	195.35	kPa	371.50	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	202.90	kPa	373.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	142.55	kPa	360.88	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	687.53	kPa	423.15	Vapor Liquid Equilibrium for Several Compounds Relevant to the Biofuels Industry Modeled with the Wilson Equation
pvap	21.72	kPa	310.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa

pvap	24.78	kPa	313.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	28.18	kPa	316.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	31.95	kPa	319.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	157.94	kPa	364.25	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	36.12	kPa	322.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	40.73	kPa	325.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	45.80	kPa	328.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa

pvap	51.36	kPa	331.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	57.46	kPa	334.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	64.13	kPa	337.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	71.40	kPa	340.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	79.32	kPa	343.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	87.93	kPa	346.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	97.26	kPa	349.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa

pvap	107.36	kPa	352.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	118.27	kPa	355.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	130.03	kPa	358.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	31.37	kPa	318.40	Vapour liquid equilibrium for the ethyl ethanoate + 1-butene, +cis-2-butene, +trans-2-butene, +2-methylpropene, +n-butane and +2-methylpropane
pvap	40.00	kPa	324.44	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	53.33	kPa	331.90	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	66.66	kPa	337.99	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components

pvap	79.99	kPa	343.18	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	93.32	kPa	347.70	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	101.30	kPa	350.15	The isobaric vapor liquid equilibria of ethyl acetate p acetonitrile p bis(trifluoromethylsulfonyl)imide-based ionic liquids at 101.3 kPa
pvap	205.70	kPa	373.00	Isothermal (vapour + liquid) equilibrium (VLE) for binary mixtures containing diethyl carbonate, phenyl acetate, diphenyl carbonate, or ethyl acetate
pvap	557.10	kPa	412.80	Isothermal (vapour + liquid) equilibrium (VLE) for binary mixtures containing diethyl carbonate, phenyl acetate, diphenyl carbonate, or ethyl acetate
pvap	1222.70	kPa	452.30	Isothermal (vapour + liquid) equilibrium (VLE) for binary mixtures containing diethyl carbonate, phenyl acetate, diphenyl carbonate, or ethyl acetate

pvap	101.30	kPa	350.29	Isobaric vapor-liquid equilibrium of a ternary system of ethyl acetate + propyl acetate + dimethyl sulfoxide and binary systems of ethyl acetate + dimethyl sulfoxide and propyl acetate + dimethyl sulfoxide at 101.3 kPa
pvap	101.30	kPa	350.35	Isobaric Vapor - Liquid Equilibrium for Ethyl acetate + Methanol + Ionic Liquids Ternary systems at 101.3 kPa
pvap	1500.00	kPa	462.75	Measurement and modeling of high pressure VLE for methyl acetate or ethyl acetate with 2-butanol. Isobaric data at 1.5 MPa
pvap	111.76	kPa	353.15	Vapor Liquid Equilibrium and Excess Enthalpy Data for Systems Containing N,N-Dimethylacetamide
pvap	45.95	kPa	328.15	Isothermal Vapor-Liquid Equilibria for Binary Mixtures of Methyl Nonafluorobutyl Ether + Acetone, Cyclopentyl Methyl Ether, Ethyl Acetate, n-Heptane, Methanol, and Toluene
pvap	101.30	kPa	349.95	Effect of Ionic Liquids on the Binary Vapor-Liquid Equilibrium of Ethyl Acetate + Methanol System at 101.3 kPa

pvap	101.30	kPa	350.28	Isobaric Vapor-Liquid Phase Equilibrium Measurements for Allyl Alcohol with Chloroform, Ethyl Acetate, and Methyl Propionate at 101.3 kPa
pvap	100.00	kPa	349.53	Isobaric Vapor Liquid Equilibria for Binary Mixtures of Isoamyl Acetate + Ethyl Acetate at 50 and 100 kPa
pvap	50.00	kPa	330.01	Isobaric Vapor Liquid Equilibria for Binary Mixtures of Isoamyl Acetate + Ethyl Acetate at 50 and 100 kPa
pvap	25.08	kPa	313.15	Total Vapor Pressure Measurements for 2-Ethoxyethanol with Methyl Acetate, Ethyl Acetate, Propyl Acetate, and Ethyl Propionate at 313.15 K and for 2-Ethoxyethanol with Methyl Formate at 308.15 K
pvap	25.30	kPa	313.15	Isothermal Vapor-Liquid Equilibria of ethyl acetate + dibromomethane, or + bromochloromethane or + 1,2-dichloroethane or +1-bromo-2-chloroethane at T = 313.15 K
pvap	11.89	kPa	297.17	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	16.04	kPa	303.35	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	18.33	kPa	306.25	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	20.64	kPa	308.86	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	22.44	kPa	310.67	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	24.34	kPa	312.53	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	27.63	kPa	315.44	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	31.33	kPa	318.46	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	34.85	kPa	321.01	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	38.43	kPa	323.47	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	40.61	kPa	324.80	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	44.98	kPa	327.41	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	49.27	kPa	329.77	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	

pvap	52.56	kPa	331.51	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	55.72	kPa	333.07	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	59.91	kPa	335.02	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	62.83	kPa	336.33	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	66.49	kPa	337.91	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	69.34	kPa	339.09	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	

pvap	72.26	kPa	340.23	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	76.02	kPa	341.69	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	79.83	kPa	343.03	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	82.56	kPa	344.11	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	86.85	kPa	345.53	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	90.81	kPa	346.86	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	

pvap	94.63	kPa	348.09	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	96.74	kPa	348.75	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	98.97	kPa	349.45	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	99.36	kPa	349.56	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	100.07	kPa	349.76	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	100.68	kPa	349.93	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	101.32	kPa	350.15	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	104.65	kPa	351.12	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	106.84	kPa	351.77	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	108.13	kPa	352.12	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	134.15	kPa	359.00	Isobaric Vapor-Liquid Equilibria for Ethyl Acetate + Ethanol + 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate at 100 kPa
pvap	114.65	kPa	353.91	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	116.46	kPa	354.43	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	118.56	kPa	354.93	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	120.68	kPa	355.50	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	122.31	kPa	355.91	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	124.00	kPa	356.37	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	
pvap	127.89	kPa	357.35	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)	

pvap	130.00	kPa	357.92	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	133.45	kPa	358.74	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	136.34	kPa	359.44	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	111.21	kPa	352.94	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
rfi	1.37010		293.15	Liquid-Liquid Equilibrium of (Water + Pentane-2,4-dione + Ethyl Ethanoate) and (Water + Pentane-2,4-dione + Cyclohexane) at (298.15 and 313.15) K
rfi	1.35368		328.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K

rfi	1.37270	298.15	Effects of the presence of ethylacetate or benzene on the densities and volumetric properties of mixture (styrene + N,N-dimethylformamide)
rfi	1.37000	298.15	Molecular interactions in (2,4,6-trimethyl-1,3,5-trioxane + n-alkyl acetates) at T=(298.15, 303.15, and 308.15) K
rfi	1.36977	298.15	Properties of ionic liquid HMIMPF6 with carbonates, ketones and alkyl acetates
rfi	1.36920	298.15	Thermodynamic study of (alkyl esters + a,x-alkyl dihalides) I: HE and V E for 25 binary mixtures {xCu-1H2u-1CO2C2H5 + (1-x)a,x-ClCH2(CH2)v-2CH2Cl}, where u = 1 to 5, a = 1 and v = x = 2 to 6
rfi	1.35970	318.15	Thermodynamic properties of (an ester + an alkane). XVI. Experimental HEm and V Em values and a new correlation method for (an alkyl ethanoate + an n-alkane) at 318.15 K
rfi	1.37240	293.15	A novel static analytical apparatus for phase equilibrium measurements
rfi	1.35940	318.20	Experimental and calculated liquid-liquid equilibrium data for water + furfural + solvents

rfi	1.36720	303.20	Experimental and calculated liquid-liquid equilibrium data for water + furfural + solvents
rfi	1.37490	288.20	Experimental and calculated liquid-liquid equilibrium data for water + furfural + solvents
rfi	1.37020	293.20	Vapor liquid equilibria for the ternary system of carbon dioxide + ethanol + ethyl acetate at elevated pressures
rfi	1.36977	298.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.37241	293.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.36977	298.15	Ternary (liquid + liquid) equilibria of the azeotrope (ethyl acetate + 2-propanol) with different ionic liquids at T = 298.15 K
rfi	1.37000	298.15	Correlation and prediction of mixing thermodynamic properties of ester-containing systems: Ester + alkane and ester + ester binary systems and the ternary dodecane + ethyl pentanoate + ethyl ethanoate

rfi	1.36720	303.15	Density, refraction index and vapor-liquid equilibria of N-methyl-2-hydroxyethylammonium butyrate plus (methyl acetate or ethyl acetate or propyl acetate) at several temperatures
rfi	1.36750	303.15	Liquid-liquid equilibrium for ternary systems of ethyl acetate/isopropyl acetate + 2,2,3,3-tetrafluoro-1-propanol + water at 298.15, 318.15 K
rfi	1.36640	303.15	Densities, speeds of sound, isentropic compressibilities, refractive indexes, and viscosities of tetrahydrofuran with haloalkane or alkyl ethanoate at T = 303.15 K
rfi	1.36980	298.15	Vapor-Liquid Equilibrium Data for Binary Mixtures of Dimethyl Carbonate with Methyl Acetate, Ethyl Acetate, n-Propyl Acetate, Isopropyl Acetate, n-Butyl Acetate, and Isoamyl Acetate at 93.13 kPa
rfi	1.37244	298.15	Isobaric Vapor-Liquid Equilibrium Data for Binary Systems of Anisole with Methyl Acetate, Ethyl Acetate, n-Propyl Acetate, and Isopropyl Acetate at 93.9 kPa

rfi	1.36981	298.15	Measurement of VLE Data by Using an Experimental Installation with Automatic Control: Modeling of Binary Systems of Methyl Acetate or Ethyl Acetate with n-Heptane or 2,2,4-Trimethylpentane at Both 0.1 and 1.5 MPa
rfi	1.36712	303.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.36980	298.15	Density, Refractive Index, and Speed of Sound at 298.15 K and Vapor-Liquid Equilibria at 101.3 kPa for Binary Mixtures of Ethyl Acetate + 1-Pentanol and Ethanol + 2-Methyl-1-propanol
rfi	1.37130	298.15	Density, Viscosity, Refractive Index, and Speed of Sound for Binary Mixtures of 1,4-Dioxane with Different Organic Liquids at (298.15, 303.15, and 308.15) K
rfi	1.36730	303.15	Density, Viscosity, Refractive Index, and Speed of Sound for Binary Mixtures of 1,4-Dioxane with Different Organic Liquids at (298.15, 303.15, and 308.15) K

rfi	1.36310	308.15	Density, Viscosity, Refractive Index, and Speed of Sound for Binary Mixtures of 1,4-Dioxane with Different Organic Liquids at (298.15, 303.15, and 308.15) K
rfi	1.36990	298.15	Densities, Viscosities, and Refractive Indices for Binary and Ternary Mixtures of N,N-Dimethylacetamide (1) + 2-Methylbutan-2-ol (2) + Ethyl Acetate (3) at 298.15 K for the Liquid Region and at Ambient Pressure
rfi	1.36978	298.15	Liquid-Liquid Equilibrium Diagrams of Ethanol + Water + (Ethyl Acetate or 1-Pentanol) at Several Temperatures
rfi	1.37190	293.15	Solubilities of Some Phosphaspirocyclic Compounds in Selected Solvents
rfi	1.37241	293.15	Thermodynamic Properties of Ionic Liquids in Organic Solvents from (293.15 to 303.15) K
rfi	1.36977	298.15	Thermodynamic Properties of Ionic Liquids in Organic Solvents from (293.15 to 303.15) K
rfi	1.36712	303.15	Thermodynamic Properties of Ionic Liquids in Organic Solvents from (293.15 to 303.15) K
rfi	1.37190	293.15	Solubilities of Phosphorus-Containing Compounds in Selected Solvents

rfi	1.37000	298.15	Vapor-Liquid Equilibria for Ethyl Acetate + Methanol at (0.1, 0.5, and 0.7) MPa. Measurements with a New Ebulliometer
rfi	1.36978	298.15	Density, Refractive Index, Speed of Sound at 298.15 K, and Vapor-Liquid Equilibria at 101.3 kPa for Binary Mixtures of Ethyl Acetate + Ethyl Lactate and Methyl Acetate + Ethyl Lactate
rfi	1.35919	318.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.36460	308.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.36994	298.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K

rfi	1.37519		288.15	Density, Speed of Sound, and Refractive Index of 1-Ethyl-3-methylimidazolium Trifluoromethanesulfonate with Acetone, Methyl Acetate, and Ethyl Acetate at Temperatures from (278.15 to 328.15) K
rfi	1.35880		293.15	Solubilities of Methyldiphenylphosphine Oxide in Selected Solvents
rfi	1.36983		298.15	Physical Properties of Binary and Ternary Mixtures of Ethyl Acetate, Ethanol, and 1-Octyl-3-methyl-imidazolium Bis(trifluoromethylsulfonyl)imide at 298.15 K
rfi	1.35880		293.15	Solubilities of Triphenylphosphine Oxide in Selected Solvents
rfi	1.37120		298.15	Determination and Correlation of Vapor Liquid Equilibrium Data for the Ethyl Acetate + Hexamethyl Disiloxane System at 101.3 kPa
rhol	900.88	kg/m3	293.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhol	900.57	kg/m3	293.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates

rhol	875.14	kg/m3	313.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhol	881.52	kg/m3	308.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhol	887.85	kg/m3	303.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhol	894.14	kg/m3	298.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhol	900.26	kg/m3	293.15	Volumetric properties of binary mixtures of N-ethylformamide with tetrahydrofuran, 2-butanone and ethylacetate from (293.15 to 313.15) K
rhol	894.47	kg/m3	298.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates

rhol	876.10	kg/m3	313.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
rhol	900.57	kg/m3	293.20	Liquid-liquid equilibrium data for ternary systems of water + acetic acid + acetate esters at 293.2 K and 303.2 K and ~ 95 kPa
rhol	875.73	kg/m3	313.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhol	881.98	kg/m3	308.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhol	888.35	kg/m3	303.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhol	882.17	kg/m3	308.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates
rhol	875.95	kg/m3	313.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates

rhol	869.68	kg/m3	318.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates	
rhol	863.36	kg/m3	323.15	Study on thermo physical and excess molar properties of binary systems of ionic liquids. I: [Cnmim][PF6] (n = 6, 8) and alkyl acetates	
rhol	894.50	kg/m3	298.15	(Liquid + liquid) equilibria for mixtures of dodecane and ethanol with alkylsulfate-based ionic liquids	
rhol	893.40	kg/m3	298.15	Solubility and solution thermodynamics of sorbic acid in eight pure organic solvents	
rhol	894.51	kg/m3	298.15	Standard partial molar volumes of some electrolytes in ethylene carbonate based mixtures	
rhol	894.40	kg/m3	298.15	Measurement and correlation of solubility and solution thermodynamics of 1,3-dimethylurea in different solvents from T = (288.15 to 328.15) K	
rhol	888.50	kg/m3	303.15	Volumetric and transport properties of ternary mixtures containing 1-propanol + ethyl ethanoate + cyclohexane or benzene at 303.15 K: Experimental data, correlation and prediction by ERAS model	

rhol	888.50	kg/m3	303.15	Volumetric and transport properties of ternary mixtures containing 1-alkanol + ethyl ethanoate + cyclohexane at 303.15 K: Experimental data, correlation and prediction by ERAS model	
rhol	894.40	kg/m3	298.15	Apparent molar volume and apparent molar isentropic compressibility for thebinary systems {methyltrioctylammoniumbis(trifluoromethylsulfonyl)imide + ethyl acetate or ethanol} at different temperatures underatmospheric pressure	
rhol	888.50	kg/m3	303.15	Apparent molar volume and apparent molar isentropic compressibility for thebinary systems {methyltrioctylammoniumbis(trifluoromethylsulfonyl)imide + ethyl acetate or ethanol} at different temperatures underatmospheric pressure	
rhol	882.70	kg/m3	308.15	Apparent molar volume and apparent molar isentropic compressibility for thebinary systems {methyltrioctylammoniumbis(trifluoromethylsulfonyl)imide + ethyl acetate or ethanol} at different temperatures underatmospheric pressure	

rhol	876.30	kg/m3	313.15	Apparent molar volume and apparent molar isentropic compressibility for thebinary systems {methyltrioctylammoniumbis(trifluoromethylsulfonyl)imide + ethyl acetate or ethanol} at different temperatures underatmospheric pressure
rhol	900.44	kg/m3	293.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	894.37	kg/m3	298.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	888.26	kg/m3	303.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K

rhol	882.09	kg/m3	308.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	875.88	kg/m3	313.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	869.62	kg/m3	318.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	888.19	kg/m3	303.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhol	894.36	kg/m3	298.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures

rhol	900.48	kg/m3	293.15	Liquid-liquid equilibria and COSMO-SAC modeling of organic solvent/ ionic liquid - hydroxyacetone - water mixtures
rhol	830.62	kg/m3	348.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	843.86	kg/m3	338.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	856.81	kg/m3	328.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	875.81	kg/m3	313.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa

rhol	894.38	kg/m3	298.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	906.55	kg/m3	288.15	Excess molar enthalpies of diethyl malonate+ (1-butanol, 2-methyl-1-propanol, 1-pentanol, n-heptane, and ethyl acetate) at T= (288.2, 298.2, 313.2, 328.2, 338.2, and 348.2 K) and p = 101.3 kPa
rhol	863.30	kg/m3	323.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rhol	894.40	kg/m3	298.15	Revision of the volumetric method for measurements of liquid liquid equilibria in binary systems
rhol	888.75	kg/m3	303.15	Excess Volumes and Excess Isentropic Compressibilities of Binary Liquid Mixtures of Trichloroethylene with Esters at 303.15 K

rhol	899.50	kg/m3	298.15	Isobaric Vapor-liquid Equilibrium for Three Binary Systems of Ethyl Acetate + Propyl Acetate, Ethyl Acetate + Propylene Carbonate, and Propyl Acetate + Propylene Carbonate at 101.3 kPa
rhol	901.00	kg/m3	293.00	KDB
rhol	894.79	kg/m3	298.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhol	888.66	kg/m3	303.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhol	882.48	kg/m3	308.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhol	876.25	kg/m3	313.15	Volumetric and FT-IR Studies of the Binary Liquid Mixtures of Tributylamine and Alkyl Ester (C1-C5)
rhol	894.40	kg/m3	298.15	Liquid-Liquid Equilibrium in Ternary Systems Containing Ethylene Glycol, Monofunctional Benzene Derivative, and Ethyl Acetate
rhol	897.72	kg/m3	298.15	Effect of Inorganic Salts on the Isobaric Vapor Liquid Equilibrium of the Ethyl Acetate Ethanol System

rhol	893.90	kg/m3	298.40	Vapor Liquid Equilibrium at 350 K, Excess Molar Enthalpies at 298 K, and Excess Molar Volumes at 298 K of Binary Mixtures Containing Ethyl Acetate, Butyl Acetate, and 2-Butanol
rhol	894.70	kg/m3	298.15	Ternary Excess Molar Volumes of {Methyltrioctylammonium Bis[(trifluoromethyl)sulfonyl]imide + Methanol + Methyl Acetate or Ethyl Acetate} Systems at (298.15, 303.15, and 313.15) K
rhol	888.50	kg/m3	303.15	Ternary Excess Molar Volumes of {Methyltrioctylammonium Bis[(trifluoromethyl)sulfonyl]imide + Methanol + Methyl Acetate or Ethyl Acetate} Systems at (298.15, 303.15, and 313.15) K
rhol	875.10	kg/m3	313.15	Ternary Excess Molar Volumes of {Methyltrioctylammonium Bis[(trifluoromethyl)sulfonyl]imide + Methanol + Methyl Acetate or Ethyl Acetate} Systems at (298.15, 303.15, and 313.15) K
rhol	894.60	kg/m3	298.15	Experimental Determination of Densities and Isobaric Vapor Liquid Equilibria of Methyl Acetate and Ethyl Acetate with Alcohols (C3 and C4) at 0.3 MPa
rhol	851.36	kg/m3	332.70	Isothermal vapor liquid equilibria for different binary mixtures involved in the alcoholic distillation

rhol	888.42	kg/m3	303.15	Studies of viscosities of dilute solutions of alkylamine in non-electrolyte solvents. II. Haloalkanes and other polar solvents
sfust	55.27	J/mol×K	189.30	NIST Webbook
speedsl	1081.00	m/s	313.15	Density and Speed of Sound of Binary Mixtures of N-Methylacetamide with Ethyl Acetate, Ethyl Chloroacetate, and Ethyl Cyanoacetate in the Temperature Interval (303.15 to 318.15) K
speedsl	1143.23	m/s	298.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K
speedsl	1119.00	m/s	303.15	Density and Speed of Sound of Binary Mixtures of N-Methylacetamide with Ethyl Acetate, Ethyl Chloroacetate, and Ethyl Cyanoacetate in the Temperature Interval (303.15 to 318.15) K
speedsl	1098.00	m/s	308.15	Density and Speed of Sound of Binary Mixtures of N-Methylacetamide with Ethyl Acetate, Ethyl Chloroacetate, and Ethyl Cyanoacetate in the Temperature Interval (303.15 to 318.15) K

speedsl	1120.80	m/s	303.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K	
speedsl	1058.00	m/s	318.15	Density and Speed of Sound of Binary Mixtures of N-Methylacetamide with Ethyl Acetate, Ethyl Chloroacetate, and Ethyl Cyanoacetate in the Temperature Interval (303.15 to 318.15) K	
speedsl	1187.92	m/s	288.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K	
speedsl	1165.80	m/s	293.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K	
speedsl	1098.43	m/s	308.15	Densities and Speeds of Sound of Binary Liquid Mixtures of Some n-Alkoxypropanols with Methyl Acetate, Ethyl Acetate, and n-Butyl Acetate at T = (288.15, 293.15, 298.15, 303.15, and 308.15) K	

srf	0.03	N/m	323.20	KDB	
srf	0.02	N/m	298.15	Concentration Dependence of Surface Tension for Very Dilute Aqueous Solutions of Organic Non-Electrolytes	
srf	0.02	N/m	298.15	Surface Tension Data of Aqueous Binary Mixtures of Methyl, Ethyl, Propyl, and Butyl Acetates at 298.15 K	
tcondl	0.15	W/m×K	290.42	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase	
tcondl	0.15	W/m×K	285.31	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase	
tcondl	0.15	W/m×K	281.34	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase	
tcondl	0.14	W/m×K	295.44	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase	
tcondl	0.15	W/m×K	268.04	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase	
tcondl	0.16	W/m×K	260.17	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase	
tcondl	0.16	W/m×K	253.89	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase	

tcondl	0.16	W/m×K	249.13	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	298.52	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	303.53	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	308.44	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.14	W/m×K	313.45	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	323.25	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	328.39	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	333.37	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	338.34	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	343.27	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase

tcondl	0.12	W/m×K	345.43	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.12	W/m×K	348.46	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.13	W/m×K	318.40	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase
tcondl	0.15	W/m×K	274.35	Measurement of the thermal conductivity of five aliphatic esters in the liquid phase

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbp	332.82	K	54.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	335.16	K	59.98	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	339.42	K	70.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	340.92	K	75.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil

tbp	343.18	K	80.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	344.93	K	84.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	346.58	K	89.91	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	348.20	K	95.01	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	351.26	K	104.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	352.67	K	109.98	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	355.36	K	119.90	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	356.62	K	124.98	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil
tbp	357.86	K	129.93	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil

tbp	359.08	K	134.95	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	360.24	K	139.96	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	362.48	K	149.95	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	363.56	K	154.97	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	364.60	K	159.96	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	365.64	K	164.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	367.61	K	174.99	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	
tbp	368.58	K	180.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil	

tbp	369.50	K	185.00	Vapor Liquid Equilibrium for Binary Mixtures of Acetates in the Direct Esterification of Fusel Oil

Correlations

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)
Coeff. A	1.47020e+01
Coeff. B	-3.08216e+03
Coeff. C	-4.45420e+01
Temperature range (K), min.	258.37
Temperature range (K), max.	372.76

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/T + C*ln(T) + D*T^2
Coeff. A	8.09498e+01
Coeff. B	-6.86243e+03
Coeff. C	-9.83731e+00
Coeff. D	7.27641e-06
Temperature range (K), min.	189.60
Temperature range (K), max.	523.30

Datasets

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
298.15	100.00	894.0
298.15	1000.00	894.7
298.15	2000.00	895.7

298.15	3000.00	896.7
298.15	3800.00	897.4
298.15	5000.00	898.8
298.15	10000.00	903.4
298.15	15000.00	907.7
298.15	20000.00	912.0
298.15	25000.00	916.1
298.15	30000.00	921.1
298.15	35000.00	926.3
303.15	100.00	887.6
303.15	1000.00	888.5
303.15	2000.00	889.5
303.15	3000.00	890.5
303.15	3800.00	891.3
303.15	5000.00	892.7
303.15	10000.00	897.5
303.15	15000.00	902.0
303.15	20000.00	906.3
303.15	25000.00	910.7
303.15	30000.00	915.9
303.15	35000.00	921.2
308.15	100.00	881.4
308.15	1000.00	882.3
308.15	2000.00	883.3
308.15	3000.00	884.4
308.15	3800.00	885.3
308.15	5000.00	886.7
308.15	10000.00	891.7
308.15	15000.00	896.4
308.15	20000.00	900.9
308.15	25000.00	905.4
308.15	30000.00	910.7
308.15	35000.00	916.2
313.15	100.00	875.2
313.15	1000.00	876.1
313.15	2000.00	877.2
313.15	3000.00	878.3
313.15	3800.00	879.2
313.15	5000.00	880.6
313.15	10000.00	885.8
313.15	15000.00	890.7
313.15	20000.00	895.4
313.15	25000.00	899.8
313.15	30000.00	905.3

313.15	35000.00	910.9
318.15	100.00	868.8
318.15	1000.00	869.8
318.15	2000.00	871.0
318.15	3000.00	872.2
318.15	3800.00	873.1
318.15	5000.00	874.5
318.15	10000.00	880.0
318.15	15000.00	885.1
318.15	20000.00	889.8
318.15	25000.00	894.5
318.15	30000.00	900.1
318.15	35000.00	905.9
323.15	100.00	862.7
323.15	1000.00	864.0
323.15	2000.00	865.1
323.15	3000.00	866.2
323.15	3800.00	867.1
323.15	5000.00	868.6
323.15	10000.00	874.2
323.15	15000.00	879.4
323.15	20000.00	884.3
323.15	25000.00	889.2
323.15	30000.00	895.0
323.15	35000.00	900.9
328.15	100.00	856.4
328.15	1000.00	857.8
328.15	2000.00	859.2
328.15	3000.00	860.5
328.15	3800.00	861.5
328.15	5000.00	862.5
328.15	10000.00	868.4
328.15	15000.00	873.9
328.15	20000.00	879.0
328.15	25000.00	884.1
328.15	30000.00	890.1
328.15	35000.00	896.2
333.15	100.00	850.4
333.15	1000.00	851.7
333.15	2000.00	853.0
333.15	3000.00	854.4
333.15	3800.00	855.4
333.15	5000.00	856.8
333.15	10000.00	862.9

333.15	15000.00	868.5
333.15	20000.00	873.8
333.15	25000.00	879.0
333.15	30000.00	885.2
333.15	35000.00	891.4
338.15	100.00	844.0
338.15	1000.00	845.4
338.15	2000.00	846.8
338.15	3000.00	848.2
338.15	3800.00	849.3
338.15	5000.00	850.8
338.15	10000.00	857.1
338.15	15000.00	863.0
338.15	20000.00	868.5
338.15	25000.00	873.9
338.15	30000.00	880.3
338.15	35000.00	886.7
343.15	100.00	837.5
343.15	1000.00	839.1
343.15	2000.00	840.6
343.15	3000.00	842.0
343.15	3800.00	843.2
343.15	5000.00	844.5
343.15	10000.00	851.2
343.15	15000.00	857.3
343.15	20000.00	863.0
343.15	25000.00	868.5
343.15	30000.00	875.1
343.15	35000.00	881.6
348.15	100.00	829.4
348.15	1000.00	830.5
348.15	2000.00	832.3
348.15	3000.00	833.8
348.15	3800.00	835.0
348.15	5000.00	836.8
348.15	10000.00	845.5
348.15	15000.00	851.8
348.15	20000.00	857.7
348.15	25000.00	863.5
348.15	30000.00	870.2
348.15	35000.00	877.0
353.15	1000.00	824.3
353.15	2000.00	826.0
353.15	3000.00	827.5

353.15	3800.00	828.8
353.15	5000.00	830.6
353.15	10000.00	837.7
353.15	15000.00	844.3
353.15	20000.00	850.4
353.15	25000.00	856.1
353.15	30000.00	862.7
353.15	35000.00	869.6
358.15	1000.00	818.4
358.15	2000.00	820.0
358.15	3000.00	821.6
358.15	3800.00	822.8
358.15	5000.00	824.7
358.15	10000.00	832.1
358.15	15000.00	838.9
358.15	20000.00	845.2
358.15	25000.00	851.0
358.15	30000.00	857.6
358.15	35000.00	864.7
363.15	1000.00	811.8
363.15	2000.00	813.5
363.15	3000.00	815.3
363.15	3800.00	816.6
363.15	5000.00	818.5
363.15	10000.00	826.3
363.15	15000.00	833.3
363.15	20000.00	839.7
363.15	25000.00	845.8
363.15	30000.00	852.9
363.15	35000.00	860.2
368.15	1000.00	804.9
368.15	2000.00	806.8
368.15	3000.00	808.6
368.15	3800.00	810.0
368.15	5000.00	812.1
368.15	10000.00	820.2
368.15	15000.00	827.5
368.15	20000.00	834.3
368.15	25000.00	840.6
368.15	30000.00	848.0
368.15	35000.00	855.5
373.15	1000.00	798.5
373.15	2000.00	800.4
373.15	3000.00	802.4

373.15	3800.00	803.8
373.15	5000.00	806.0
373.15	10000.00	814.4
373.15	15000.00	822.0
373.15	20000.00	829.0
373.15	25000.00	835.5
373.15	30000.00	843.0
373.15	35000.00	850.6
378.15	1000.00	791.8
378.15	2000.00	793.8
378.15	3000.00	795.8
378.15	3800.00	797.3
378.15	5000.00	799.6
378.15	10000.00	808.5
378.15	15000.00	816.5
378.15	20000.00	823.7
378.15	25000.00	830.5
378.15	30000.00	838.4
378.15	35000.00	846.3
383.15	1000.00	784.8
383.15	2000.00	787.1
383.15	3000.00	789.1
383.15	3800.00	790.8
383.15	5000.00	793.2
383.15	10000.00	802.4
383.15	15000.00	810.7
383.15	20000.00	818.2
383.15	25000.00	825.3
383.15	30000.00	833.5
383.15	35000.00	841.6
388.15	1000.00	778.2
388.15	2000.00	780.5
388.15	3000.00	782.7
388.15	3800.00	784.4
388.15	5000.00	786.9
388.15	10000.00	796.4
388.15	15000.00	805.1
388.15	20000.00	813.0
388.15	25000.00	820.3
388.15	30000.00	828.8
388.15	35000.00	837.2
393.15	1000.00	771.0
393.15	2000.00	773.5
393.15	3000.00	775.9

393.15	3800.00	777.7
393.15	5000.00	780.4
393.15	10000.00	790.5
393.15	15000.00	799.4
393.15	20000.00	807.6
393.15	25000.00	815.2
393.15	30000.00	823.9
393.15	35000.00	832.4

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Legend

af: Acentric Factor

affp:	Proton affinity
aigt:	Autoignition Temperature
basg:	Gas basicity
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
fll:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpc:	Flash Point (Closed Cup Method)
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sg:	Molar entropy at standard conditions
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tbp:	Boiling point at given pressure
tc:	Critical Temperature
tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature

vc:	Critical Volume
zc:	Critical Compressibility
zra:	Rackett Parameter