

Ethanol, 2,2'-oxybis-

Other names: 1,1'-oxybis[1-methoxy]methane
1,5-Dihydroxy-3-oxapentane
2,2'-Dihydroxyethyl ether
2,2'-OXYBIS ETHANOL
2,2'-Oxybis[Ethanol]
2,2'-Oxydiethanol
2,2'-Oxyethanol
2,2'-oxybis(ethan-1-ol)
2,2'-oxybis-ethanol
2,2-Di(hydroxyethyl) ether
2,4,6-trioxaheptane
2-(2-Hydroxyethoxy)ethanol
2-Hydroxyethyl ether
3-Oxa-1,5-pentanediol
3-Oxapentamethylene-1,5-diol
3-Oxapentane-1,5-diol
3-oxapentan-1,5-diol
BETA,BETA'-DIHYDROXYDIETHYL ETHER
Bis(2-hydroxyethyl) ether
Bis(«beta»-hydroxyethyl) ether
Bis(Â«betaÂ»-hydroxyethyl) ether
Brecolane NDG
Carbitol
D.E.H. 20
D.E.H. 52
DEG
Deactivator E
Deactivator H
Dicol
Diethylene glycol
Diethylenglykol
Digenos
Diglycol
Digol
Dihydroxydiethyl ether
Dissolvant APV
ETHYLENE DIGLYCOL
Ethanol, 2,2'-oxydi-
Glycol ether
Glycol hydroxyethyl ether

Her
 NSC 36391
 TL4N
 «beta»,«beta»'-Dihydroxydiethyl ether
 «beta»,«beta»'-Dihydroxyethyl ether
 Ä«betaÄ»,Ä«betaÄ»'-Dihydroxydiethyl ether
 Ä«betaÄ»,Ä«betaÄ»'-Dihydroxyethyl ether
Inchi: InChI=1S/C4H10O3/c5-1-3-7-4-2-6/h5-6H,1-4H2
InchiKey: MTHSVFCYNBDYFN-UHFFFAOYSA-N
Formula: C4H10O3
SMILES: OCCOCOC
Mol. weight [g/mol]: 106.12
CAS: 111-46-6

Physical Properties

Property code	Value	Unit	Source
chl	-2372.90	kJ/mol	NIST Webbook
chl	-2374.70 ± 2.40	kJ/mol	NIST Webbook
gf	-395.84	kJ/mol	Joback Method
hf	-571.50	kJ/mol	KDB
hfl	-628.50 ± 2.40	kJ/mol	NIST Webbook
hfus	15.48	kJ/mol	Joback Method
hvap	60.27	kJ/mol	Joback Method
log10ws	0.89		Crippen Method
logp	-1.012		Crippen Method
mcvol	84.830	ml/mol	McGowan Method
pc	4700.00	kPa	KDB
pc	4770.00 ± 50.00	kPa	NIST Webbook
rinpol	925.00		NIST Webbook
rinpol	967.00		NIST Webbook
rinpol	941.00		NIST Webbook
rinpol	927.00		NIST Webbook
ripol	1989.00		NIST Webbook
ripol	1975.00		NIST Webbook
ripol	1968.00		NIST Webbook
ripol	1975.00		NIST Webbook
ripol	1953.00		NIST Webbook
tb	519.00	K	KDB
tc	680.00 ± 20.00	K	NIST Webbook
tc	723.50 ± 50.00	K	NIST Webbook

tc	753.00 ± 4.00	K	NIST Webbook
tc	681.00	K	KDB
tc	753.00	K	Critical temperatures and pressures of ethylene glycols
tf	265.35	K	NIST Webbook
tf	265.40 ± 0.60	K	NIST Webbook
tf	263.05 ± 0.50	K	NIST Webbook
tf	262.80 ± 0.10	K	NIST Webbook
tf	265.00	K	KDB
vc	0.316	m3/kmol	Joback Method
zra	0.25		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	205.96	J/mol×K	550.58	Joback Method
cpg	228.87	J/mol×K	656.34	Joback Method
cpg	223.44	J/mol×K	629.90	Joback Method
cpg	217.81	J/mol×K	603.46	Joback Method
cpg	211.98	J/mol×K	577.02	Joback Method
cpg	193.32	J/mol×K	497.70	Joback Method
cpg	199.74	J/mol×K	524.14	Joback Method
cpl	259.20	J/mol×K	333.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	266.80	J/mol×K	353.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	243.90	J/mol×K	298.00	NIST Webbook
cpl	287.00	J/mol×K	298.00	NIST Webbook
cpl	263.80	J/mol×K	343.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	248.20	J/mol×K	303.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)

cpl	251.30	J/mol×K	313.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
cpl	255.00	J/mol×K	323.15	Heat capacities of the mixed-solvents desiccants (glycols +water + salts)
dvisc	0.0156000	Paxs	313.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0100290	Paxs	323.15	Supplementary Densities and Viscosities of Aqueous Solutions of Diethylene Glycol from (283.15 to 353.15) K
dvisc	0.0072200	Paxs	333.15	Supplementary Densities and Viscosities of Aqueous Solutions of Diethylene Glycol from (283.15 to 353.15) K
dvisc	0.0053690	Paxs	343.15	Supplementary Densities and Viscosities of Aqueous Solutions of Diethylene Glycol from (283.15 to 353.15) K
dvisc	0.0041390	Paxs	353.15	Supplementary Densities and Viscosities of Aqueous Solutions of Diethylene Glycol from (283.15 to 353.15) K

dvisc	0.0300120	Paxs	298.15	Thermophysical Properties For Diethylene Glycol + Nitrobenzene and Triethylene Glycol + (Chloro-, Bromo-, Nitro-) Benzene Systems at Different Temperatures
dvisc	0.0169720	Paxs	308.15	Thermophysical Properties For Diethylene Glycol + Nitrobenzene and Triethylene Glycol + (Chloro-, Bromo-, Nitro-) Benzene Systems at Different Temperatures
dvisc	0.0365200	Paxs	293.15	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0283600	Paxs	298.15	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0152500	Paxs	312.60	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure

dvisc	0.0084580	Paxs	329.28	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0053400	Paxs	344.99	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0048090	Paxs	349.77	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0032310	Paxs	366.77	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0014090	Paxs	413.65	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure

dvisc	0.0007890	Paxs	464.05	Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure
dvisc	0.0381100	Paxs	293.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0298200	Paxs	298.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0236400	Paxs	303.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0190200	Paxs	308.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0088530	Paxs	328.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation

dvisc	0.0126900	Paxs	318.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0106200	Paxs	323.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0145630	Paxs	313.15	Supplementary Densities and Viscosities of Aqueous Solutions of Diethylene Glycol from (283.15 to 353.15) K
dvisc	0.0073620	Paxs	333.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0062080	Paxs	338.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0053240	Paxs	343.20	Phase equilibria study on bromide-based ionic liquids with glycols and sulfolane. Experimental data and correlation
dvisc	0.0351000	Paxs	294.20	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K

dvisc	0.0151000	Paxs	313.05	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0076400	Paxs	333.05	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0044100	Paxs	353.05	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0027600	Paxs	373.60	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0019200	Paxs	393.40	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0014100	Paxs	413.25	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K

dvisc	0.0011500	Paxs	428.15	Density, Viscosity and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene Glycol Mixtures between 290 K and 450 K
dvisc	0.0300120	Paxs	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
dvisc	0.0169720	Paxs	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for Alkyl (Methyl, Ethyl, Butyl, and Isoamyl) Acetates + Glycols at Different Temperatures
dvisc	0.0221560	Paxs	303.15	Densities, Viscosities, and Surface Tensions of the System Water + Diethylene Glycol
dvisc	0.0220910	Paxs	303.15	Supplementary Densities and Viscosities of Aqueous Solutions of Diethylene Glycol from (283.15 to 353.15) K

dvisc	0.0147060	Paxs	313.15	Densities, Viscosities, and Surface Tensions of the System Water + Diethylene Glycol
dvisc	0.0121910	Paxs	318.15	Densities, Viscosities, and Surface Tensions of the System Water + Diethylene Glycol
dvisc	0.0101950	Paxs	323.15	Densities, Viscosities, and Surface Tensions of the System Water + Diethylene Glycol
dvisc	0.0364330	Paxs	293.15	Supplementary Densities and Viscosities of Aqueous Solutions of Diethylene Glycol from (283.15 to 353.15) K
dvisc	0.0179340	Paxs	308.15	Densities, Viscosities, and Surface Tensions of the System Water + Diethylene Glycol
hvapt	57.30 ± 5.90	kJ/mol	273.00	NIST Webbook
hvapt	66.80	kJ/mol	462.50	NIST Webbook
hvapt	66.57	kJ/mol	523.00	NIST Webbook
hvapt	69.20	kJ/mol	458.00	NIST Webbook
hvapt	59.80	kJ/mol	441.00	NIST Webbook
hvapt	66.50	kJ/mol	413.00	NIST Webbook
hvapt	66.90 ± 0.30	kJ/mol	474.50	NIST Webbook
hvapt	63.10 ± 0.30	kJ/mol	474.50	NIST Webbook
hvapt	59.20 ± 0.30	kJ/mol	474.50	NIST Webbook
hvapt	55.10 ± 0.50	kJ/mol	474.50	NIST Webbook
rfl	1.44724		293.15	Liquid-Liquid Equilibria of (Limonene + Linalool + Ethyleneglycol or Diethyleneglycol or Triethyleneglycol or 1,2-Propylene Glycol) Ternary Systems

rhol	1109.30	kg/m3	303.15	Densities, Ultrasonic Speeds, and Excess Properties of Binary Mixtures of Diethylene Glycol with 1-Butanol, 2-Butanol, and 1,4-Butanediol at Different Temperatures
rhol	1112.56	kg/m3	298.15	Isobaric Vapor-Liquid Equilibrium for Four Binary Systems of Ethane-1,2-diol, Butane-1,4-diol, 2-(2- Hydroxyethoxy)ethan-1-ol and 2-[2-(2- Hydroxyethoxy)ethoxy]ethanol at 10.0 kPa, 20.0 kPa and 40.0 kPa
rhol	1110.00	kg/m3	303.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
rhol	1103.00	kg/m3	313.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
rhol	1095.90	kg/m3	323.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
rhol	1116.00	kg/m3	293.00	KDB

rhol	1112.70	kg/m3	298.15	Densities, Ultrasonic Speeds, and Excess Properties of Binary Mixtures of Diethylene Glycol with 1-Butanol, 2-Butanol, and 1,4-Butanediol at Different Temperatures
rhol	1088.50	kg/m3	333.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
rhol	1105.90	kg/m3	308.15	Densities, Ultrasonic Speeds, and Excess Properties of Binary Mixtures of Diethylene Glycol with 1-Butanol, 2-Butanol, and 1,4-Butanediol at Different Temperatures
rhol	1102.50	kg/m3	313.15	Densities, Ultrasonic Speeds, and Excess Properties of Binary Mixtures of Diethylene Glycol with 1-Butanol, 2-Butanol, and 1,4-Butanediol at Different Temperatures
rhol	1113.00	kg/m3	298.15	Solubility for dilute sulfur dioxide, viscosities, excess properties, and viscous flow thermodynamics of binary system N, N-dimethylformamide + diethylene glycol

rhol	1109.20	kg/m3	303.15	Solubility for dilute sulfur dioxide, viscosities, excess properties, and viscous flow thermodynamics of binary system N, N-dimethylformamide + diethylene glycol
rhol	1106.10	kg/m3	308.15	Solubility for dilute sulfur dioxide, viscosities, excess properties, and viscous flow thermodynamics of binary system N, N-dimethylformamide + diethylene glycol
rhol	1103.00	kg/m3	313.15	Solubility for dilute sulfur dioxide, viscosities, excess properties, and viscous flow thermodynamics of binary system N, N-dimethylformamide + diethylene glycol
rhol	1099.30	kg/m3	318.15	Solubility for dilute sulfur dioxide, viscosities, excess properties, and viscous flow thermodynamics of binary system N, N-dimethylformamide + diethylene glycol

rhol	1109.16	kg/m3	298.00	Removal of aromatic hydrocarbons from hydrocarbon mixture using glycols at 303.15 K and 333.15 K and atmospheric pressure: Experimental and calculated data by NRTL and UNIQUAC models
rhol	1109.00	kg/m3	303.15	Vapour pressures and densities of the mixed-solvent desiccants (glycols + water + salts)
rhol	1103.00	kg/m3	313.15	Vapour pressures and densities of the mixed-solvent desiccants (glycols + water + salts)
rhol	1095.00	kg/m3	323.15	Vapour pressures and densities of the mixed-solvent desiccants (glycols + water + salts)
rhol	1088.00	kg/m3	333.15	Vapour pressures and densities of the mixed-solvent desiccants (glycols + water + salts)
rhol	1081.00	kg/m3	343.15	Vapour pressures and densities of the mixed-solvent desiccants (glycols + water + salts)
rhol	1120.05	kg/m3	288.15	Activity coefficients at infinite dilution of organic solutes in diethylene glycol and triethylene glycol from gas-liquid chromatography

rhol	1120.30	kg/m3	288.15	Activity coefficients at infinite dilution of hydrocarbons in glycols: Experimental data and thermodynamic modeling with the GCA-EoS
rhol	1116.50	kg/m3	293.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1113.00	kg/m3	298.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1109.40	kg/m3	303.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1105.80	kg/m3	308.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture

rhol	1102.20	kg/m3	313.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1098.60	kg/m3	318.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1095.00	kg/m3	323.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1091.40	kg/m3	328.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture
rhol	1087.70	kg/m3	333.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO2 capture

rhol	1084.00	kg/m3	338.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO ₂ capture
rhol	1080.30	kg/m3	343.15	Measurement and correlation of physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO ₂ capture
rhol	1116.73	kg/m3	293.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhol	1113.17	kg/m3	298.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhol	1109.60	kg/m3	303.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure
rhol	1106.01	kg/m3	308.15	Thermodynamics properties of binary mixtures of aqueous solutions of glycols at several temperatures and atmospheric pressure

rhol	1105.65	kg/m3	308.15	Excess molar enthalpies of binary mixtures containing ethylene glycols or poly(ethylene glycols) + ethyl alcohol at 308.15K and atmospheric pressure
rhol	1112.80	kg/m3	298.15	Density, viscosity, surface tension, and spectroscopic properties for binary system of 1,2-ethanediamine + diethylene glycol
rhol	1109.20	kg/m3	303.15	Density, viscosity, surface tension, and spectroscopic properties for binary system of 1,2-ethanediamine + diethylene glycol
rhol	1105.60	kg/m3	308.15	Density, viscosity, surface tension, and spectroscopic properties for binary system of 1,2-ethanediamine + diethylene glycol
rhol	1102.30	kg/m3	313.15	Density, viscosity, surface tension, and spectroscopic properties for binary system of 1,2-ethanediamine + diethylene glycol
rhol	1099.20	kg/m3	318.15	Density, viscosity, surface tension, and spectroscopic properties for binary system of 1,2-ethanediamine + diethylene glycol
rhol	1121.40	kg/m3	288.15	Thermophysical properties of glycols and glymes

rhol	1117.80	kg/m3	293.15	Thermophysical properties of glycols and glymes
rhol	1114.20	kg/m3	298.15	Thermophysical properties of glycols and glymes
rhol	1110.60	kg/m3	303.15	Thermophysical properties of glycols and glymes
rhol	1107.00	kg/m3	308.15	Thermophysical properties of glycols and glymes
rhol	1103.40	kg/m3	313.15	Thermophysical properties of glycols and glymes
rhol	1099.70	kg/m3	318.15	Thermophysical properties of glycols and glymes
rhol	1096.10	kg/m3	323.15	Thermophysical properties of glycols and glymes
rhol	1092.50	kg/m3	328.15	Thermophysical properties of glycols and glymes
rhol	1088.80	kg/m3	333.15	Thermophysical properties of glycols and glymes
rhol	1085.20	kg/m3	338.15	Thermophysical properties of glycols and glymes
rhol	1081.50	kg/m3	343.15	Thermophysical properties of glycols and glymes
rhol	1077.80	kg/m3	348.15	Thermophysical properties of glycols and glymes
rhol	1074.10	kg/m3	353.15	Thermophysical properties of glycols and glymes
rhol	1070.30	kg/m3	358.15	Thermophysical properties of glycols and glymes
rhol	1066.60	kg/m3	363.15	Thermophysical properties of glycols and glymes

rhol	1062.80	kg/m3	368.15	Thermophysical properties of glycols and glymes
rhol	1059.00	kg/m3	373.15	Thermophysical properties of glycols and glymes
rhol	1123.30	kg/m3	283.15	Thermophysical properties of glycols and glymes
rhol	1119.80	kg/m3	288.15	Thermophysical properties of glycols and glymes
rhol	1116.20	kg/m3	293.15	Thermophysical properties of glycols and glymes
rhol	1112.70	kg/m3	298.15	Thermophysical properties of glycols and glymes
rhol	1109.10	kg/m3	303.15	Thermophysical properties of glycols and glymes
rhol	1105.50	kg/m3	308.15	Thermophysical properties of glycols and glymes
rhol	1101.90	kg/m3	313.15	Thermophysical properties of glycols and glymes
rhol	1094.70	kg/m3	323.15	Thermophysical properties of glycols and glymes
rhol	1087.40	kg/m3	333.15	Thermophysical properties of glycols and glymes
rhol	1080.00	kg/m3	343.15	Thermophysical properties of glycols and glymes
rhol	1105.65	kg/m3	308.15	Excess Molar Enthalpies of Binary Mixtures Containing Glycols or Polyglycols + Dimethyl Sulfoxide at 308.15 K

rhol	1112.38	kg/m3	298.15	Thermodynamic Study of Binary Mixtures Containing Glycols or Polyethylene Glycols + Benzyl Alcohol at 308.15 K
rhol	1105.88	kg/m3	308.15	Thermodynamic Study of Binary Mixtures Containing Glycols or Polyethylene Glycols + Benzyl Alcohol at 308.15 K
rhol	1112.38	kg/m3	298.15	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Glycols or Poly(Ethylene Glycols) and 2-Phenylethyl Alcohol at 308.15 K and Atmospheric Pressure
rhol	1105.88	kg/m3	308.15	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Glycols or Poly(Ethylene Glycols) and 2-Phenylethyl Alcohol at 308.15 K and Atmospheric Pressure
rhol	1105.86	kg/m3	308.50	Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Ethers and Benzyl Alcohol at 308.15 K and Atmospheric Pressure

rh _{ol}	1081.10	kg/m ³	343.15	Density, Viscosities, and Excess Properties for Binary Mixtures of Sulfolane + Alcohols and Sulfolane + Glycols at Different Temperatures
tcondl	0.21	W/m×K	338.20	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.20	W/m×K	328.40	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.20	W/m×K	318.20	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.20	W/m×K	308.00	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols
tcondl	0.20	W/m×K	298.10	Application of the Multi-Current Transient Hot-Wire Technique for Absolute Measurements of the Thermal Conductivity of Glycols

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbrp	406.20	K	1.90	NIST Webbook

Correlations

Information	Value
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Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.56166e+01
Coeff. B	-4.75686e+03
Coeff. C	-8.64930e+01
Temperature range (K), min.	396.81
Temperature range (K), max.	548.09

Information	Value
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Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C*\ln(T) + D*T^2$
Coeff. A	1.08791e+02
Coeff. B	-1.28556e+04
Coeff. C	-1.28373e+01
Coeff. D	3.16995e-06
Temperature range (K), min.	262.70
Temperature range (K), max.	744.60

Datasets

Mass density, kg/m³

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m ³ - Liquid
283.15	100.00	1124.3

283.15	1000.00	1124.7
283.15	2000.00	1125.3
283.15	5000.00	1126.5
283.15	7000.00	1127.4
283.15	10000.00	1128.8
283.15	12000.00	1129.6
283.15	16000.00	1131.3
283.15	20000.00	1133.0
283.15	25000.00	1135.1
283.15	30000.00	1137.2
283.15	35000.00	1139.2
283.15	40000.00	1141.2
283.15	45000.00	1143.0
283.15	50000.00	1145.1
283.15	55000.00	1146.9
283.15	60000.00	1148.8
283.15	65000.00	1150.7
283.15	70000.00	1152.4
283.15	75000.00	1154.2
283.15	80000.00	1155.8
283.15	85000.00	1157.5
283.15	90000.00	1159.2
283.15	95000.00	1160.9
293.15	100.00	1117.1
293.15	1000.00	1117.5
293.15	2000.00	1118.0
293.15	5000.00	1119.3
293.15	7000.00	1120.2
293.15	10000.00	1121.6
293.15	12000.00	1122.5
293.15	16000.00	1124.3
293.15	20000.00	1126.0
293.15	25000.00	1128.2
293.15	30000.00	1130.3
293.15	35000.00	1132.4
293.15	40000.00	1134.3
293.15	45000.00	1136.4
293.15	50000.00	1138.4
293.15	55000.00	1140.4
293.15	60000.00	1142.2
293.15	65000.00	1144.1
293.15	70000.00	1145.8
293.15	75000.00	1147.7
293.15	80000.00	1149.4

293.15	85000.00	1151.2
293.15	90000.00	1152.9
293.15	95000.00	1154.6
303.14	100.00	1109.9
303.14	1000.00	1110.3
303.14	2000.00	1110.7
303.14	5000.00	1112.2
303.14	7000.00	1113.1
303.14	10000.00	1114.5
303.14	12000.00	1115.4
303.14	16000.00	1117.3
303.14	20000.00	1119.0
303.14	25000.00	1121.2
303.14	30000.00	1123.4
303.14	35000.00	1125.5
303.14	40000.00	1127.5
303.14	45000.00	1129.6
303.14	50000.00	1131.6
303.14	55000.00	1133.6
303.14	60000.00	1135.5
303.14	65000.00	1137.4
303.14	70000.00	1139.3
303.14	75000.00	1141.1
303.14	80000.00	1142.9
303.14	85000.00	1144.6
303.14	90000.00	1146.4
303.14	95000.00	1148.2
313.15	100.00	1102.7
313.15	1000.00	1103.2
313.15	2000.00	1103.6
313.15	5000.00	1105.2
313.15	7000.00	1106.2
313.15	10000.00	1107.7
313.15	12000.00	1108.6
313.15	16000.00	1110.4
313.15	20000.00	1112.3
313.15	25000.00	1114.5
313.15	30000.00	1116.7
313.15	35000.00	1118.9
313.15	40000.00	1121.0
313.15	45000.00	1123.1
313.15	50000.00	1125.1
313.15	55000.00	1127.1
313.15	60000.00	1129.1

313.15	65000.00	1131.1
313.15	70000.00	1132.9
313.15	75000.00	1134.8
313.15	80000.00	1136.6
313.15	85000.00	1138.4
313.15	90000.00	1140.2
313.15	95000.00	1141.9
323.20	100.00	1095.4
323.20	1000.00	1095.8
323.20	2000.00	1096.3
323.20	5000.00	1097.8
323.20	7000.00	1098.8
323.20	10000.00	1100.3
323.20	12000.00	1101.3
323.20	16000.00	1103.3
323.20	20000.00	1105.2
323.20	25000.00	1107.5
323.20	30000.00	1109.9
323.20	35000.00	1112.0
323.20	40000.00	1114.2
323.20	45000.00	1116.3
323.20	50000.00	1118.4
323.20	55000.00	1120.5
323.20	60000.00	1122.5
323.20	65000.00	1124.5
323.20	70000.00	1126.5
323.20	75000.00	1128.3
323.20	80000.00	1130.3
323.20	85000.00	1132.2
323.20	90000.00	1133.9
323.20	95000.00	1135.7
333.20	100.00	1088.1
333.20	1000.00	1088.7
333.20	2000.00	1089.2
333.20	5000.00	1090.8
333.20	7000.00	1091.8
333.20	10000.00	1093.3
333.20	12000.00	1094.4
333.20	16000.00	1096.4
333.20	20000.00	1098.3
333.20	25000.00	1100.7
333.20	30000.00	1103.0
333.20	35000.00	1105.3
333.20	40000.00	1107.6

333.20	45000.00	1109.7
333.20	50000.00	1111.9
333.20	55000.00	1113.9
333.20	60000.00	1116.0
333.20	65000.00	1118.0
333.20	70000.00	1120.1
333.20	75000.00	1121.9
333.20	80000.00	1123.8
333.20	85000.00	1125.9
333.20	90000.00	1127.7
333.20	95000.00	1129.5
343.20	100.00	1080.7
343.20	1000.00	1081.2
343.20	2000.00	1081.7
343.20	5000.00	1083.4
343.20	7000.00	1084.5
343.20	10000.00	1086.1
343.20	12000.00	1087.1
343.20	16000.00	1089.1
343.20	20000.00	1091.2
343.20	25000.00	1093.7
343.20	30000.00	1096.1
343.20	35000.00	1098.5
343.20	40000.00	1100.8
343.20	45000.00	1103.1
343.20	50000.00	1105.2
343.20	55000.00	1107.4
343.20	60000.00	1109.5
343.20	65000.00	1111.6
343.20	70000.00	1113.7
343.20	75000.00	1115.7
343.20	80000.00	1117.6
343.20	85000.00	1119.5
343.20	90000.00	1121.4
343.20	95000.00	1123.3
353.19	100.00	1073.2
353.19	1000.00	1073.8
353.19	2000.00	1074.3
353.19	5000.00	1076.0
353.19	7000.00	1077.1
353.19	10000.00	1078.7
353.19	12000.00	1079.8
353.19	16000.00	1081.9
353.19	20000.00	1084.0

353.19	25000.00	1086.6
353.19	30000.00	1089.1
353.19	35000.00	1091.6
353.19	40000.00	1093.9
353.19	45000.00	1096.3
353.19	50000.00	1098.5
353.19	55000.00	1100.8
353.19	60000.00	1102.9
353.19	65000.00	1105.0
353.19	70000.00	1107.2
353.19	75000.00	1109.2
353.19	80000.00	1111.2
353.19	85000.00	1113.2
353.19	90000.00	1115.1
353.19	95000.00	1117.0
363.17	100.00	1065.6
363.17	1000.00	1066.2
363.17	2000.00	1066.8
363.17	5000.00	1068.5
363.17	7000.00	1069.6
363.17	10000.00	1071.4
363.17	12000.00	1072.5
363.17	16000.00	1074.6
363.17	20000.00	1076.9
363.17	25000.00	1079.4
363.17	30000.00	1082.0
363.17	35000.00	1084.6
363.17	40000.00	1087.0
363.17	45000.00	1089.4
363.17	50000.00	1091.8
363.17	55000.00	1094.1
363.17	60000.00	1096.3
363.17	65000.00	1098.5
363.17	70000.00	1100.5
363.17	75000.00	1102.6
363.17	80000.00	1104.8
363.17	85000.00	1106.8
363.17	90000.00	1108.8
363.17	95000.00	1110.7

Reference

<https://www.doi.org/10.1016/j.fluid.2017.01.003>

Temperature, K

Pressure, kPa

Mass density, kg/m³

283.15	100.00	1123.1
283.15	100.00	1123.1
283.15	640.00	1123.3
283.15	1080.00	1123.5
283.15	1590.00	1123.7
283.15	2140.00	1124.0
283.15	3050.00	1124.3
283.15	5050.00	1125.2
283.15	6930.00	1126.0
283.15	9930.00	1127.2
283.15	14810.00	1129.3
283.15	19760.00	1131.3
283.15	24610.00	1133.3
283.15	29600.00	1135.2
283.15	34500.00	1137.1
283.15	39420.00	1139.0
283.15	44300.00	1140.8
283.15	49180.00	1142.6
283.15	54060.00	1144.4
283.15	59030.00	1146.1
283.15	63810.00	1147.8
283.15	68760.00	1149.5
293.15	100.00	1115.9
293.15	100.00	1115.9
293.15	570.00	1116.1
293.15	1080.00	1116.3
293.15	1530.00	1116.6
293.15	2110.00	1116.8
293.15	3080.00	1117.2
293.15	5040.00	1118.1
293.15	6990.00	1118.9
293.15	9940.00	1120.2
293.15	14840.00	1122.3
293.15	19740.00	1124.3
293.15	24680.00	1126.4
293.15	29600.00	1128.4
293.15	34530.00	1130.3
293.15	39360.00	1132.2
293.15	44320.00	1134.1
293.15	49120.00	1136.0
293.15	54090.00	1137.8
293.15	58990.00	1139.6
293.15	63820.00	1141.3
293.15	68750.00	1143.0

303.15	100.00	1108.8
303.15	100.00	1108.8
303.15	680.00	1109.0
303.15	1130.00	1109.2
303.15	1580.00	1109.4
303.15	2120.00	1109.7
303.15	3030.00	1110.1
303.15	5040.00	1111.0
303.15	6950.00	1111.9
303.15	9960.00	1113.2
303.15	14840.00	1115.4
303.15	19740.00	1117.5
303.15	24680.00	1119.6
303.15	29610.00	1121.6
303.15	34520.00	1123.6
303.15	39380.00	1125.6
303.15	44350.00	1127.5
303.15	49140.00	1129.4
303.15	54090.00	1131.3
303.15	58990.00	1133.1
303.15	63850.00	1134.9
303.15	68760.00	1136.6
313.15	100.00	1101.7
313.15	100.00	1101.6
313.15	640.00	1101.8
313.15	1140.00	1102.1
313.15	1640.00	1102.3
313.15	2100.00	1102.5
313.15	3090.00	1103.0
313.15	5130.00	1103.9
313.15	6960.00	1104.8
313.15	9960.00	1106.1
313.15	14940.00	1108.4
313.15	19750.00	1110.6
313.15	24640.00	1112.7
313.15	29640.00	1114.8
313.15	34510.00	1116.9
313.15	39340.00	1118.9
313.15	44340.00	1120.9
313.15	49190.00	1123.2
313.15	54020.00	1124.7
313.15	59030.00	1126.7
313.15	63880.00	1128.5
313.15	68820.00	1130.3

323.15	100.00	1094.3
323.15	100.00	1094.3
323.15	680.00	1094.6
323.15	1130.00	1094.8
323.15	1570.00	1095.0
323.15	2100.00	1095.2
323.15	3080.00	1095.7
323.15	5080.00	1096.7
323.15	7000.00	1097.6
323.15	9950.00	1099.0
323.15	14890.00	1101.4
323.15	19770.00	1103.6
323.15	24680.00	1105.8
323.15	29600.00	1108.0
323.15	34530.00	1110.1
323.15	39360.00	1112.2
323.15	44290.00	1114.3
323.15	49260.00	1116.3
323.15	54100.00	1118.2
323.15	59060.00	1120.2
323.15	63880.00	1122.0
323.15	68770.00	1123.8
333.15	100.00	1087.0
333.15	100.00	1087.0
333.15	660.00	1087.3
333.15	1120.00	1087.5
333.15	1630.00	1087.8
333.15	2100.00	1088.0
333.15	3070.00	1088.5
333.15	5060.00	1089.5
333.15	7050.00	1090.5
333.15	9930.00	1091.9
333.15	14780.00	1094.3
333.15	19770.00	1096.7
333.15	24660.00	1099.0
333.15	29540.00	1101.2
333.15	34500.00	1103.4
333.15	39330.00	1105.5
333.15	44230.00	1107.6
333.15	49130.00	1109.7
333.15	54060.00	1111.7
333.15	59020.00	1113.7
333.15	63840.00	1115.7
333.15	68830.00	1117.5

343.15	100.00	1079.7
343.15	100.00	1079.7
343.15	670.00	1080.0
343.15	1100.00	1080.2
343.15	1520.00	1080.4
343.15	2120.00	1080.7
343.15	3060.00	1081.2
343.15	5040.00	1082.3
343.15	6970.00	1083.3
343.15	9950.00	1084.8
343.15	14870.00	1087.3
343.15	19740.00	1089.6
343.15	24710.00	1092.1
343.15	29560.00	1094.4
343.15	34490.00	1096.6
343.15	39350.00	1098.8
343.15	44290.00	1101.0
343.15	49180.00	1103.1
343.15	54070.00	1105.2
343.15	58980.00	1107.3
343.15	63910.00	1109.3
343.15	68720.00	1111.2
353.15	100.00	1072.2
353.15	100.00	1072.2
353.15	560.00	1072.5
353.15	1090.00	1072.8
353.15	1550.00	1073.0
353.15	2080.00	1073.3
353.15	3040.00	1073.8
353.15	5060.00	1074.9
353.15	7020.00	1076.0
353.15	9970.00	1077.5
353.15	14830.00	1080.1
353.15	19740.00	1082.6
353.15	24680.00	1085.1
353.15	29560.00	1087.5
353.15	34550.00	1089.8
353.15	39420.00	1092.1
353.15	44280.00	1094.3
353.15	49230.00	1096.5
353.15	54110.00	1098.7
353.15	59020.00	1100.8
353.15	64010.00	1102.9
353.15	68770.00	1104.8

363.08	100.00	1064.5
363.08	100.00	1064.4
363.08	620.00	1064.7
363.08	1110.00	1065.0
363.08	1570.00	1065.2
363.08	2100.00	1065.5
363.08	3020.00	1066.0
363.08	5070.00	1067.2
363.08	7000.00	1068.3
363.08	9970.00	1069.9
363.08	14840.00	1072.6
363.08	19750.00	1075.1
363.08	24660.00	1077.7
363.08	29610.00	1080.2
363.08	34480.00	1082.6
363.08	39400.00	1084.9
363.08	44290.00	1087.2
363.08	49160.00	1089.5
363.08	54110.00	1091.7
363.08	58990.00	1093.9
363.08	63880.00	1096.0
363.08	68760.00	1098.0

Reference

<https://www.doi.org/10.1016/j.fluid.2018.09.026>

Temperature, K	Pressure, kPa	Mass density, kg/m3
298.15	100.00	989.2

Reference

<https://www.doi.org/10.1016/j.jct.2017.06.002>

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
293.15	98.00	0.0365200
293.15	49030.00	0.0527200
293.15	98060.00	0.0741600
293.15	147100.00	0.1026000
293.15	196130.00	0.1399000
293.15	245160.00	0.1873000
298.15	98.00	0.0283600

298.15	49030.00	0.0403600
298.15	98060.00	0.0565200
298.15	147100.00	0.0771600
298.15	196130.00	0.1038000
298.15	245160.00	0.1383000
312.60	98.00	0.0152500
312.62	49030.00	0.0210400
312.63	98060.00	0.0282000
312.67	147100.00	0.0371400
312.71	196130.00	0.0482900
312.75	245160.00	0.0620700
329.28	98.00	0.0084580
329.33	98060.00	0.0147300
329.33	196130.00	0.0238200
329.33	245160.00	0.0296100
329.38	49030.00	0.0112900
329.38	147100.00	0.0188300
344.99	98.00	0.0053400
345.20	49030.00	0.0070620
345.38	98060.00	0.0089690
345.47	147100.00	0.0112300
345.61	196130.00	0.0138100
345.78	245160.00	0.0167500
349.77	98.00	0.0048090
350.06	49030.00	0.0062500
350.13	147100.00	0.0098660
350.16	98060.00	0.0079040
350.40	196130.00	0.0120400
366.77	98.00	0.0032310
367.13	49030.00	0.0041240
367.26	147100.00	0.0063310
367.30	98060.00	0.0051450
367.37	196130.00	0.0076070
367.61	245160.00	0.0090860
413.65	98.00	0.0014090
413.80	49030.00	0.0017800
413.93	98060.00	0.0021530
414.01	147100.00	0.0025540
414.09	196130.00	0.0029870
414.29	245160.00	0.0034740
463.94	98060.00	0.0012180
463.99	49030.00	0.0010020
464.05	98.00	0.0007890
464.09	147100.00	0.0014320

464.20	196130.00	0.0016550
464.37	245160.00	0.0018790

Reference

<https://www.doi.org/10.1016/j.fluid.2011.11.022>

Pressure, kPa	Temperature, K	Viscosity, Pa*s
101.30	308.15	0.0175900
Reference		https://www.doi.org/10.1021/je020178w

Sources

Molar heat capacities of some aqueous 2-amino-2-hydroxymethyl-1,3-propanediol <https://www.doi.org/10.1016/j.jct.2012.02.022>

Solubility of Carbon Dioxide in Poly(oxymethylene) Dimethyl Ethers: <https://www.doi.org/10.1021/acs.jced.7b00718>

Heat Capacity of Several Mixed-Solvent Desiccants Containing Glycol + Water <https://www.doi.org/10.1016/j.tca.2012.02.017>

The Thermodynamic and Kinetic Studies of CO₂ Capture by Glycol and Measured by Differential Scanning Calorimetry: <https://www.doi.org/10.1021/acs.jced.8b00015>

Measure-based Deep Eutectic Systems: Models for Ternary Liquid-Liquid Molar heat capacities of several aqueous polyoxymethylene Dimethyl Ethers <https://www.doi.org/10.1021/acs.jced.8b00323>

Thermodynamic and kinetic study of CO₂ capture by glycol and measured by differential scanning calorimetry at experimental temperatures: <https://www.doi.org/10.1016/j.tca.2012.04.006>

Conductivity and pH of Glycol-Aqueous Mixtures: <https://www.doi.org/10.1016/j.jct.2018.07.006>

Glycol-Aqueous Mixtures: Experimental conductivity and pH of Glycols: <https://www.doi.org/10.1016/j.jct.2017.08.029>

Excess Molar Entropies and Hydrogen Bonding in Binary Mixtures Containing Glycols, Excess Molar Volumes, and Viscosities: Species of Solvent 1, Excess Molar Entropies and Viscosities of Aqueous mixtures of Glycols (Glycol, Ethylene Glycol, Propylene Glycol and their mixtures) and their effect on deep eutectics: Solvents from hexane aromatic mixture at different temperatures: <https://www.doi.org/10.1021/acs.jced.9b00011>

Mixtures containing Diethylene Glycol and water: Thermodynamic Interactions, Study of Some Diethylene Glycols in Aqueous Water Solvent mixtures, pure, Excess Properties for Binary Mixtures and Solvent measurements and solubility of Glycols at Different Temperatures: <https://www.doi.org/10.1021/je300827f>

Properties of Glycols and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene glycols of the Mixed solvents desiccants (glycols + water + salts): <https://www.doi.org/10.1021/acs.jced.8b00058>

Surface tension and viscosity of the mixed solvents desiccants (glycols + water + salts): <https://www.doi.org/10.1021/je500153g>

Measurement and solubility of Glycols at Different Temperatures: <https://www.doi.org/10.1016/j.fluid.2017.01.003>

Properties of Glycols and Thermal Conductivity of Aqueous Ethylene, Diethylene and Triethylene glycols of the Mixed solvents desiccants (glycols + water + salts): <https://www.doi.org/10.1021/je0256100>

Surface tension and viscosity of the mixed solvents desiccants (glycols + water + salts): <https://www.doi.org/10.1016/j.jct.2008.12.003>

Surface tension and viscosity of the mixed solvents desiccants (glycols + water + salts): <https://www.doi.org/10.1016/j.tca.2014.05.034>

System of 2,2,4-trimethyl-1-Alcohols and Ketones with Diethylene glycol: Crippen Method: <https://www.doi.org/10.1021/acs.jced.8b00126>

Salting Effect of Sodium Hydroxide and Sodium Formate on the Liquid-Liquid Equilibrium study of the influence of crown ethers and glycols on the mutual solubility of titanium Diethyleneglycol + Nitrobenzene and Thymol + Glycol binary and ternary mixtures containing Different temperatures and concentration of the glycol and diethylene/methylene) <http://pubs.acs.org/doi/abs/10.1021/ci9903071>

Thermal study on the influence of crown ethers and glycols on the mutual solubility of titanium Diethyleneglycol + Nitrobenzene and Thymol + Glycol binary and ternary mixtures containing Different temperatures and concentration of the glycol and diethylene/methylene) <https://www.doi.org/10.1021/acs.jced.9b00081>

Thermal study on the influence of crown ethers and glycols on the mutual solubility of titanium Diethyleneglycol + Nitrobenzene and Thymol + Glycol binary and ternary mixtures containing Different temperatures and concentration of the glycol and diethylene/methylene) <https://www.doi.org/10.1016/j.fluid.2018.11.036>

Thermal study on the influence of crown ethers and glycols on the mutual solubility of titanium Diethyleneglycol + Nitrobenzene and Thymol + Glycol binary and ternary mixtures containing Different temperatures and concentration of the glycol and diethylene/methylene) <https://www.doi.org/10.1007/s10765-008-0399-8>

Thermal study on the influence of crown ethers and glycols on the mutual solubility of titanium Diethyleneglycol + Nitrobenzene and Thymol + Glycol binary and ternary mixtures containing Different temperatures and concentration of the glycol and diethylene/methylene) <https://www.doi.org/10.1016/j.fluid.2016.05.017>

Thermal study on the influence of crown ethers and glycols on the mutual solubility of titanium Diethyleneglycol + Nitrobenzene and Thymol + Glycol binary and ternary mixtures containing Different temperatures and concentration of the glycol and diethylene/methylene) <https://www.doi.org/10.1021/je400064r>

Thermal study on the influence of crown ethers and glycols on the mutual solubility of titanium Diethyleneglycol + Nitrobenzene and Thymol + Glycol binary and ternary mixtures containing Different temperatures and concentration of the glycol and diethylene/methylene) <https://www.doi.org/10.1016/j.fluid.2018.10.017>

- Thermodynamic properties and spectral investigation of dilute sulfur dioxide in binary systems for the systems formed by Diethylene Glycol over the temperature range 288.15 K to 318.15 K: Excess Molar Enthalpies of Binary Mixtures Containing Glycols or Polyglycols at Dimethyl Sulfoxide at 308.15 K:**
KDB:
- <https://www.doi.org/10.1016/j.fluid.2015.01.019>
- <https://www.doi.org/10.1021/je049601m>
- <https://www.sciencedirect.com/book/9780128029992/the-yaws-handbook-of-vapor-pressure-data>
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- Measurement and Modeling of Isobaric Vapor-Liquid Equilibrium of Water + Glycols and ternary solid-liquid phase equilibrium for the systems formed by Experimental and Correlated Diethylene Glycol-Diethyl-Ether Equilibrium Data for Ternary Systems Water/quinone in Binary Mixtures of Diethylene Glycol, Diethylene Glycol and Glycerol, and Water at 293.15 K and 308.15 K and 318.15 K: Solubility of Ethane in Diethylene Glycol:**
- <https://www.doi.org/10.1021/acs.jced.7b00945>
- Solubility for dilute sulfur dioxide, viscosities, excess properties, and hydrodynamic properties of binary mixtures of glycols (with water and salts): Excess Molar Enthalpies and Hydrogen Bonding in Binary Mixtures Containing Volumetric and ultrasonic studies on K interactions of ethylene glycol, diethylene glycol and triethylene glycol Benzene/Isophorone/glycerol at temperatures 293.15 K - 343.15 K: Systems Solvent Hexane/diethylene Dimethyl Ether/ethyleneglycol/water at 293.15 K: mixtures efficiently by using ZIF-67-based Vapor-Liquid Equilibrium for Four Binary Systems of Liquid-Liquid Equilibrium of 4-Ethynone + Linoleic Acid/Ethylene Glycol and 2-[2-(2-Bromo-2-methoxyethoxy)ethoxy]Glycol/glycerol/glycerol mixtures of systems glycerol with 1-Butanol, dilution of hydrocarbons in glycerol at 293.15 K and pressure data: thermodynamic modeling with the GCA-EoS:**
- <https://www.doi.org/10.1021/acs.jced.8b00891>
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- <https://www.doi.org/10.1021/acs.jced.9b00313>
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- <https://www.doi.org/10.1021/acs.jced.6b00334>
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- <https://www.doi.org/10.1016/j.tca.2009.01.008>
- <https://www.doi.org/10.1021/je0504212>
- <https://www.doi.org/10.1016/j.jct.2018.05.016>
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- <https://www.doi.org/10.1016/j.fluid.2011.12.018>
- <https://www.doi.org/10.1016/j.jct.2017.05.020>
- Investigation on Temperature-Dependent Volumetric Properties of the Progress of molecular weight and size up the solubility of Nonionic surfactants in carbon dioxide: physicochemical properties of phosphonium-based deep eutectic solvents at several temperatures (293.15 K - 343.15 K) for CO₂ capture:**

Liquid-liquid equilibria for ternary systems polyoxymethylene dimethyl Sulfoxide + C_4 + C_6 Non-ideal Absorption System of Experimental Study of the density and viscosity of polyethylene glycols and their diffusion coefficients in binary mixtures at temperatures from 293 K to 473 K and at pressures up to 100 bar. Thermodynamic Study of Binary Mixtures Containing Glycols or Pentane in Cyclic Systems + Benzyl Alcohol Properties for Binary Mixtures of Some Cycloaliphatic Propyleneolefin Bis(Methylpropylene) Ether and α -Terpinene of the Multicomponent after Fractionation Methodology for Oxalyl Sulfoxide in Methanethiolane Thermal organic solvents + Glycols Measurement and thermodynamic Excess Enthalpies for Ternary Solutions Experimental and theoretical excess enthalpies of some working pairs of polar solvents of some working pairs experimental solutions Vapor-Liquid Equilibrium for Binary Systems Dimethyl Sulfide + Glycols + Glyceraldehyde + Glycose + Glycogenes of Aqueous Solutions of Dihydrosulfone Study 293-45 K + Acetonitrile-based Ionic Liquids with New Ion System (Methylene Glycol + Glycolic Acid) + Dimethylformamide + Methyl Chloride Based on Electrostatic Surface Tensions of the System Water + Experimental study of the density and viscosity of polyethylene glycols and their mixtures at temperatures from 293 K to 473 K and at atmospheric pressure:

<https://www.doi.org/10.1016/j.jct.2016.05.016>

<https://www.doi.org/10.1021/je401028g>

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<https://www.doi.org/10.1021/je1009976>

<https://www.doi.org/10.1016/j.jct.2011.06.013>

Legend

chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dvisc:	Dynamic viscosity
gf:	Standard Gibbs free energy of formation
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
tb:	Normal Boiling Point Temperature
tbrp:	Boiling point at reduced pressure

tc:	Critical Temperature
tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
vc:	Critical Volume
zra:	Rackett Parameter

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