1-Hexanol

Other names:	1-Hexyl alcohol
	1-Hydroxyhexane
	Amylcarbinol
	Caproyl alcohol
	Epal 6
	Hexan-1-ol
	Hexanol
	Hexanol-(1)
	Hexyl alcohol
	NSC 9254
	Pentylcarbinol
	n-C6H13OH
	n-Hexan-1-ol
	n-Hexanol
	n-Hexyl alcohol
Inchi:	InChI=1S/C6H14O/c1-2-3-4-5-6-7/h7H,2-6H2,1H3
InchiKey:	ZSIAUFGUXNUGDI-UHFFFAOYSA-N
Formula:	C6H14O
SMILES:	CCCCCCO
Mol. weight [g/mol]:	102.17
CAS:	111-27-3

Physical Properties

Property code	Value	Unit	Source
af	0.5600		KDB
affp	799.00	kJ/mol	NIST Webbook
aigt	577.59	K	KDB
chl	-3978.10 ± 2.00	kJ/mol	NIST Webbook
chl	-3982.60 ± 0.92	kJ/mol	NIST Webbook
chl	-3978.10	kJ/mol	NIST Webbook
chl	-3984.37 ± 0.44	kJ/mol	NIST Webbook
dm	1.80	debye	KDB

dvisc	0.0044395	Pa×s	Volumetric and Viscometric Properties of Binary Liquid Mixtures of Ethylene Glycol Monomethyl Ether + 1-Hexanol, 1-Octanol, and 1-Decanol at Temperatures of T = (293.15, 298.15, 303.15, and 308.15) K
dvisc	0.0052910	Pa×s	Studies on Transport and Thermodynamic Properties of Binary Mixtures of Hexan-1-ol with Halogenated Compounds at 293.15 K
fll	1.20	% in Air	KDB
flu	7.70	% in Air	KDB
fpc	338.15	K	KDB
fpo	335.93	K	KDB
gf	-135.70	kJ/mol	KDB
hf	-317.80	kJ/mol	KDB
hfl	-383.90 ± 2.00	kJ/mol	NIST Webbook
hfl	-387.70	kJ/mol	NIST Webbook
hfl	-377.50 ± 0.44	kJ/mol	NIST Webbook
hfl	-379.40 ± 1.00	kJ/mol	NIST Webbook
hfus	16.73	kJ/mol	Heat Capacities and Derived Thermodynamic Functions of 1-Hexanol, 1-Heptanol, 1-Octanol, and 1-Decanol between 5 K and 390 K
hvap	59.90	kJ/mol	NIST Webbook
hvap	61.61	kJ/mol	NIST Webbook
hvap	59.10	kJ/mol	NIST Webbook
hvap	61.70 ± 0.30	kJ/mol	NIST Webbook
hvap	69.20	kJ/mol	NIST Webbook
hvap	62.80 ± 1.30	kJ/mol	NIST Webbook
hvap	61.60 ± 0.20	kJ/mol	NIST Webbook
hvap	61.60 ± 0.20	kJ/mol	NIST Webbook
hvap	60.80 ± 0.20	kJ/mol	NIST Webbook
hvap	61.85 ± 0.20	kJ/mol	NIST Webbook
hvap	61.60	kJ/mol	NIST Webbook
hvap	61.50	kJ/mol	NIST Webbook
hvap	62.10 ± 0.20	kJ/mol	NIST Webbook
hvap	61.10	kJ/mol	NIST Webbook
ie	9.89	eV	NIST Webbook
ie	10.35	eV	NIST Webbook
log10ws	-1.24		Aqueous Solubility Prediction Method

log10ws	-1.24		Estimated Solubility Method
logp	1.559		Crippen Method
mcvol	101.270	ml/mol	McGowan Method
nfpaf	%!d(float64=2)		KDB
nfpah	%!d(float64=1)		KDB
pc	3420.00 ± 50.00	kPa	NIST Webbook
pc	3420.00 ± 20.00	kPa	NIST Webbook
pc	3417.00	kPa	KDB
pc	3413.00 ± 6.00	kPa	NIST Webbook
pc	3413.00 ± 20.00	kPa	NIST Webbook
rhoc	259.52 ± 6.13	kg/m3	NIST Webbook
rhoc	267.70	kg/m3	NIST Webbook
rhoc	263.61 ± 2.04	kg/m3	NIST Webbook
rhoc	267.70 ± 3.07	kg/m3	NIST Webbook
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sl	287.40	J/mol×K	NIST Webbook
tb	430.50	K	NIST Webbook
tb	430.70	K	KDB
tb	430.75	K	Excess molar volumes of ternary mixtures of 1,3-dichlorobenzene and methyl ethyl ketone with 1-alkanols at 303.15K
tb	430.50	K	Phase equilibria of (water + levunilic acid + alcohol) ternary systems
tb	430.11	K	Vapor-liquid equilibrium data of binary mixtures of 1-hexanol, 1-heptanol, 1-nonanol and 1,3-propanediol at P = 101.3 kPa using differential scanning calorimetry (DSC)
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tc	610.30	K	KDB
tf	228.50	K	KDB
tf	229.00	K	Vapour liquid equilibria, azeotropic data, excess enthalpies, activity coefficients at infinite dilution and solid liquid equilibria for binary alcohol ketone systems
tf	224.75	K	Aqueous Solubility Prediction Method
tt	225.80 ± 0.30	K	NIST Webbook
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Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	259.79	J/mol×K	589.96	Joback Method
cpg	207.67	J/mol×K	428.86	Joback Method
cpg	217.18	J/mol×K	455.71	Joback Method
cpg	226.36	J/mol×K	482.56	Joback Method
cpg	235.20	J/mol×K	509.41	Joback Method
cpg	243.71	J/mol×K	536.26	Joback Method
cpg	251.90	J/mol×K	563.11	Joback Method
cpl	232.46	J/mol×K	290.01	NIST Webbook
cpl	243.20	J/mol×K	298.15	NIST Webbook
cpl	242.50	J/mol×K	298.15	NIST Webbook
cpl	241.32	J/mol×K	298.15	NIST Webbook
cpl	237.85	J/mol×K	298.15	NIST Webbook
cpl	236.50	J/mol×K	293.15	NIST Webbook
cpl	239.68	J/mol×K	298.15	NIST Webbook
cpl	239.62	J/mol×K	298.15	NIST Webbook
cpl	249.15	J/mol×K	300.61	NIST Webbook
cpl	241.32	J/mol×K	298.15	NIST Webbook
cpl	240.65	J/mol×K	298.15	NIST Webbook
cpl	240.57	J/mol×K	298.15	NIST Webbook
cpl	236.50	J/mol×K	293.15	NIST Webbook
cpl	247.70	J/mol×K	303.74	NIST Webbook
cpl	244.80	J/mol×K	298.00	NIST Webbook
dvisc	0.0046426	Pa×s	298.15	Densities, Viscosities, and Volumetric Properties of Binary Mixtures of 1,2-Propanediol + 1-Heptanol or 1-Hexanol and 1,2-Ethanediol + 2-Butanol or 2-Propanol at T = (298.15, 303.15, and 308.15) K

dvisc	0.0054120	Pa×s	293.15	A Study on Properties Derived from Densities and Viscosities for the Ternary Systems (Methyl Pentanoate or Methyl Heptanoate) + n-Octane + 1-Hexanol and their Binary Subsystems at Various Temperatures.	
dvisc	0.0045960	Pa×s	298.15	A Study on Properties Derived from Densities and Viscosities for the Ternary Systems (Methyl Pentanoate or Methyl Heptanoate) + n-Octane + 1-Hexanol and their Binary Subsystems at Various Temperatures.	
dvisc	0.0034713	Pa×s	308.15	Densities, Viscosities, and Volumetric Properties of Binary Mixtures of 1,2-Propanediol + 1-Heptanol or 1-Hexanol and 1,2-Ethanediol + 2-Butanol or 2-Propanol at T = (298.15, 303.15, and 308.15) K	
dvisc	0.0039985	Pa×s	303.15	Densities, Viscosities, and Volumetric Properties of Binary Mixtures of 1,2-Propanediol + 1-Heptanol or 1-Hexanol and 1,2-Ethanediol + 2-Butanol or 2-Propanol at T = (298.15, 303.15, and 308.15) K	

dvisc	0.0033180	Pa×s	308.15	Density and Viscosity of the Binary Mixtures of Hexan-1-ol with Isomeric Xylenes at T = (308.15 and 318.15) K and Atmospheric Pressure	
dvisc	0.0022150	Pa×s	323.15	Thermodynamic Properties of the Binary Mixture of Hexan-1-ol with m-Xylene at T = (303.15, 313.15, and 323.15) K	
dvisc	0.0028790	Pa×s	313.15	Thermodynamic Properties of the Binary Mixture of Hexan-1-ol with m-Xylene at T = (303.15, 313.15, and 323.15) K	
dvisc	0.0038290	Pa×s	303.15	Thermodynamic Properties of the Binary Mixture of Hexan-1-ol with m-Xylene at T = (303.15, 313.15, and 323.15) K	
dvisc	0.0014110	Pa×s	343.15	Densities and Viscosities for Binary and Ternary Mixtures of 1, 4-Dioxane + 1-Hexanol + N,N-Dimethylaniline from T) (283.15 to 343.15) K	
dvisc	0.0016540	Pa×s	333.15	Densities and Viscosities for Binary and Ternary Mixtures of 1, 4-Dioxane + 1-Hexanol + N,N-Dimethylaniline from T) (283.15 to 343.15) K	
dvisc	0.0022760	Pa×s	323.15	Densities and Viscosities for Binary and Ternary Mixtures of 1, 4-Dioxane + 1-Hexanol + N,N-Dimethylaniline from T) (283.15 to 343.15) K	

dvisc	0.0021720	Pa×s	323.15	Densities and Viscosities for Binary and Ternary Mixtures of 1, 4-Dioxane + 1-Hexanol + N,N-Dimethylaniline from T) (283.15 to 343.15) K
dvisc	0.0029370	Pa×s	313.15	Densities and Viscosities for Binary and Ternary Mixtures of 1, 4-Dioxane + 1-Hexanol + N,N-Dimethylaniline from T) (283.15 to 343.15) K
dvisc	0.0039170	Pa×s	303.15	Densities and Viscosities for Binary and Ternary Mixtures of 1, 4-Dioxane + 1-Hexanol + N,N-Dimethylaniline from T) (283.15 to 343.15) K
dvisc	0.0037630	Pa×s	303.15	Densities and Viscosities for Binary and Ternary Mixtures of 1, 4-Dioxane + 1-Hexanol + N,N-Dimethylaniline from T) (283.15 to 343.15) K
dvisc	0.0053350	Pa×s	293.15	Densities and Viscosities for Binary and Ternary Mixtures of 1, 4-Dioxane + 1-Hexanol + N,N-Dimethylaniline from T) (283.15 to 343.15) K
dvisc	0.0039640	Pa×s	303.15	A Study on Properties Derived from Densities and Viscosities for the Ternary Systems (Methyl Pentanoate or Methyl Heptanoate) + n-Octane + 1-Hexanol and their Binary Subsystems at Various Temperatures.

dvisc	0.0022510	Pa×s	323.15	Densities and Viscosities of Binary Mixtures of 2,2,4-Trimethylpentane + 1-Propanol, + 1-Pentanol, + 1-Hexanol, and + 1-Heptanol from (298.15 to 323.15) K
dvisc	0.0025810	Pa×s	318.15	Densities and Viscosities of Binary Mixtures of 2,2,4-Trimethylpentane + 1-Propanol, + 1-Pentanol, + 1-Hexanol, and + 1-Heptanol from (298.15 to 323.15) K
dvisc	0.0029600	Pa×s	313.15	Densities and Viscosities of Binary Mixtures of 2,2,4-Trimethylpentane + 1-Propanol, + 1-Pentanol, + 1-Hexanol, and + 1-Heptanol from (298.15 to 323.15) K
dvisc	0.0034140	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of 2,2,4-Trimethylpentane + 1-Propanol, + 1-Pentanol, + 1-Hexanol, and + 1-Heptanol from (298.15 to 323.15) K
dvisc	0.0039440	Pa×s	303.15	Densities and Viscosities of Binary Mixtures of 2,2,4-Trimethylpentane + 1-Propanol, + 1-Pentanol, + 1-Hexanol, and + 1-Heptanol from (298.15 to 323.15) K

dvisc	0.0046050	Pa×s	298.15	Densities and Viscosities of Binary Mixtures of 2,2,4-Trimethylpentane + 1-Propanol, + 1-Pentanol, + 1-Hexanol, and + 1-Heptanol from (298.15 to 323.15) K
dvisc	0.0025180	Pa×s	318.15	Density and Viscosity of the Binary Mixtures of Hexan-1-ol with Isomeric Xylenes at T = (308.15 and 318.15) K and Atmospheric Pressure
dvisc	0.0022150	Pa×s	323.15	Volumetric and Viscometric Behavior of the Binary System: (Hexan-1-ol + p-Xylene)
dvisc	0.0028790	Pa×s	313.15	Volumetric and Viscometric Behavior of the Binary System: (Hexan-1-ol + p-Xylene)
dvisc	0.0038290	Pa×s	303.15	Volumetric and Viscometric Behavior of the Binary System: (Hexan-1-ol + p-Xylene)
dvisc	0.0029140	Pa×s	313.15	Acoustical and Excess Properties of {Chlorobenzene + 1-Hexanol, or 1-Heptanol, or 1-Octanol, or 1-Nonanol, or 1-Decanol} at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0033590	Pa×s	308.15	Acoustical and Excess Properties of {Chlorobenzene + 1-Hexanol, or 1-Heptanol, or 1-Octanol, or 1-Nonanol, or 1-Decanol} at (298.15, 303.15, 308.15, and 313.15) K

dvisc	0.0038870	Pa×s	303.15	Acoustical and Excess Properties of {Chlorobenzene + 1-Hexanol, or 1-Heptanol, or 1-Octanol, or 1-Nonanol, or 1-Decanol} at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0045940	Pa×s	298.15	Acoustical and Excess Properties of {Chlorobenzene + 1-Hexanol, or 1-Heptanol, or 1-Octanol, or 1-Nonanol, or 1-Decanol} at (298.15, 303.15, 308.15, and 313.15) K
dvisc	0.0029660	Pa×s	313.15	A Study on Properties Derived from Densities and Viscosities for the Ternary Systems (Methyl Pentanoate or Methyl Heptanoate) + n-Octane + 1-Hexanol and their Binary Subsystems at Various Temperatures.
dvisc	0.0074590	Pa×s	283.15	Densities and Viscosities for Binary and Ternary Mixtures of 1, 4-Dioxane + 1-Hexanol + N,N-Dimethylaniline from T) (283.15 to 343.15) K
hfust	15.38	kJ/mol	225.80	NIST Webbook
hfust	15.48	kJ/mol	225.80	NIST Webbook
hfust	15.48	kJ/mol	225.80	NIST Webbook
hvapt	57.70	kJ/mol	320.50	NIST Webbook
hvapt	57.90	kJ/mol	369.00	NIST Webbook
hvapt	47.90	kJ/mol	398.50	NIST Webbook
hvapt	53.80 ± 0.20	kJ/mol	368.00	NIST Webbook
hvapt	56.00	kJ/mol	357.50	NIST Webbook
hvapt	55.20 ± 0.20	kJ/mol	358.00	NIST Webbook
hvapt	57.60 ± 0.20	kJ/mol	343.00	NIST Webbook
hvapt	58.50 ± 0.20	kJ/mol	328.00	NIST Webbook

hvapt	58.50	kJ/mol	378.00	NIST Webbook
hvapt	57.90	kJ/mol	379.00	NIST Webbook
hvapt	61.20	kJ/mol	295.50	NIST Webbook
hvapt	61.90 ± 0.20	kJ/mol	300.50	NIST Webbook
hvapt	62.00	kJ/mol	296.50	NIST Webbook
hvapt	51.40	kJ/mol	393.00	NIST Webbook
hvapt	59.70	kJ/mol	364.00	NIST Webbook
hvapt	44.50	kJ/mol	430.50	NIST Webbook
hvapt	48.53	kJ/mol	430.30	KDB
kvisc	0.0000036	m2/s	313.15	Densities, Viscosities, and Ultrasonic Velocity Studies of Binary Mixtures of Chloroform with Pentan-1-ol, Hexan-1-ol, and Heptan-1-ol at (303.15 and 313.15) K
kvisc	0.0000047	m2/s	303.15	Densities, Viscosities, and Ultrasonic Velocity Studies of Binary Mixtures of Chloroform with Pentan-1-ol, Hexan-1-ol, and Heptan-1-ol at (303.15 and 313.15) K
pvap	15.12	kPa	379.75	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	16.97	kPa	382.25	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	16.71	kPa	381.89	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	16.37	kPa	381.45	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	16.15	kPa	381.15	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	15.95	kPa	380.87	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	15.61	kPa	380.41	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	15.37	kPa	380.06	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	5.84e-03	kPa	268.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	14.91	kPa	379.46	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	14.65	kPa	379.10	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	14.40	kPa	378.72	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	14.15	kPa	378.37	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	13.85	kPa	378.01	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	13.71	kPa	377.83	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	13.53	kPa	377.22	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	13.15	kPa	376.59	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	17.21	kPa	382.56	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	17.44	kPa	382.85	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	17.69	kPa	383.18	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	17.84	kPa	383.34	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	18.09	kPa	383.67	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	18.43	kPa	384.08	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	19.05	kPa	384.87	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	19.47	kPa	385.37	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	19.91	kPa	385.86	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	20.31	kPa	386.31	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	20.79	kPa	386.83	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	5.84e-03	kPa	268.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	5.84e-03	kPa	268.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	9.87e-03	kPa	273.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol

pvap	99.78	kPa	429.19	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems	
pvap	9.86e-03	kPa	273.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	0.01	kPa	273.65	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	0.01	kPa	273.65	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	0.01	kPa	273.65	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	0.02	kPa	278.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	

pvap	0.02	kPa	278.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	0.02	kPa	278.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	0.03	kPa	283.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	0.03	kPa	283.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	0.03	kPa	283.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	0.04	kPa	288.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	0.04	kPa	288.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	

pvap	0.04	kPa	288.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	0.07	kPa	293.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	0.07	kPa	293.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	0.07	kPa	293.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	12.73	kPa	375.93	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	0.10	kPa	298.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	0.10	kPa	298.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol

pvap	0.10	kPa	298.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	101.30	kPa	430.11	Vapor-liquid equilibrium data of binary mixtures of 1-hexanol, 1-heptanol, 1-nonanol and 1,3-propanediol at P = 101.3 kPa using differential scanning calorimetry (DSC)
pvap	0.15	kPa	303.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	0.15	kPa	303.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	0.15	kPa	303.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	0.22	kPa	308.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol

pvap	0.22	kPa	308.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	21.15	kPa	387.23	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	21.48	kPa	387.62	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	21.91	kPa	388.10	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	22.37	kPa	388.59	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	22.79	kPa	389.05	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	23.20	kPa	389.48	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	23.60	kPa	389.89	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	23.95	kPa	390.23	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	24.36	kPa	390.65	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	24.67	kPa	390.93	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	25.13	kPa	391.40	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	25.51	kPa	391.75	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	25.83	kPa	392.06	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	12.27	kPa	375.14	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	11.73	kPa	374.19	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	11.43	kPa	373.67	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	11.05	kPa	373.00	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	10.59	kPa	372.10	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	10.27	kPa	371.45	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	9.95	kPa	370.83	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	9.67	kPa	370.24	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	9.40	kPa	369.67	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	9.08	kPa	368.99	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	8.67	kPa	368.05	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	8.40	kPa	367.44	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	7.92	kPa	366.30	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	7.64	kPa	365.58	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	7.27	kPa	364.61	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	6.99	kPa	363.85	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	6.29	kPa	361.86	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	6.04	kPa	361.12	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	5.79	kPa	360.34	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	5.51	kPa	359.43	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	5.15	kPa	358.22	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	4.79	kPa	357.01	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	4.31	kPa	355.20	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	3.39e-03	kPa	263.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol

pvap	3.89	kPa	353.31	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	3.83	kPa	353.00	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	3.73	kPa	352.63	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	3.64	kPa	352.20	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	3.44	kPa	351.39	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	3.32	kPa	350.75	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	3.11	kPa	349.75	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	3.04	kPa	349.38	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	2.85	kPa	348.35	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	2.79	kPa	348.10	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	2.67	kPa	347.27	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	2.47	kPa	346.17	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	2.35	kPa	345.36	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	2.23	kPa	344.60	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	2.16	kPa	344.20	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	2.04	kPa	343.46	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	90.00	kPa	426.69	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	85.00	kPa	424.87	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	80.00	kPa	423.01	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	9.87e-03	kPa	273.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	75.00	kPa	421.05	Phase Equlibria for Hexyl Acetate Reactive Distillation

pvap	70.00	kPa	418.98	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	65.00	kPa	416.75	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	60.00	kPa	414.44	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	55.00	kPa	411.92	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	50.00	kPa	409.25	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	45.00	kPa	406.36	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	40.00	kPa	403.15	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	35.00	kPa	399.65	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	30.00	kPa	395.62	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	25.00	kPa	391.07	Phase Equlibria for Hexyl Acetate Reactive Distillation
pvap	82.16	kPa	423.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	69.49	kPa	418.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	58.50	kPa	413.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	49.02	kPa	408.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	40.85	kPa	403.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols

pvap	33.84	kPa	398.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	27.86	kPa	393.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	22.79	kPa	388.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	18.50	kPa	383.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	14.90	kPa	378.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	11.91	kPa	373.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	9.44	kPa	368.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	7.41	kPa	363.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	5.76	kPa	358.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	4.43	kPa	353.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	3.38	kPa	348.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	2.54	kPa	343.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	1.90	kPa	338.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	1.40	kPa	333.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols

pvap	1.01	kPa	328.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	0.73	kPa	323.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	0.52	kPa	318.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	0.36	kPa	313.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	0.25	kPa	308.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	0.17	kPa	303.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	0.12	kPa	298.15	Vapor Pressure Determination of the Aliphatic C5 to C8 1-Alcohols
pvap	7.87	kPa	363.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols
pvap	6.13	kPa	358.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols

pvap	5.79	kPa	357.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols
pvap	4.64	kPa	353.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols
pvap	3.48	kPa	348.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols
pvap	2.64	kPa	343.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols

pvap	1.98	kPa	338.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols
pvap	1.46	kPa	333.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols
pvap	1.43	kPa	333.10	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols
pvap	1.01	kPa	328.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols

pvap	1.03	kPa	328.10	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols
pvap	0.71	kPa	323.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols
pvap	0.75	kPa	323.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols
pvap	0.53	kPa	318.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols

pvap	0.53	kPa	318.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	0.37	kPa	313.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	0.36	kPa	313.10	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	0.30	kPa	310.40	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	

pvap	0.25	kPa	308.30	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	0.25	kPa	308.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	0.17	kPa	303.30	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	0.17	kPa	303.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	

pvap	0.17	kPa	303.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	0.11	kPa	298.30	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	0.12	kPa	298.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	27.00	kPa	393.14	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	0.07	kPa	293.30	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	

pvap	0.07	kPa	293.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	0.05	kPa	288.10	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	0.03	kPa	283.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	0.02	kPa	278.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	

pvap	0.01	kPa	273.40	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	6.64e-03	kPa	268.20	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	4.68e-03	kPa	265.00	Measurement and Prediction of Thermochemical Properties. Improved Benson-Type Increments for the Estimation of Enthalpies of Vaporization and Standard Enthalpies of Formation of Aliphatic Alcohols	
pvap	40.00	kPa	402.36	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems	
pvap	40.02	kPa	403.66	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems	

pvap	48.72	kPa	407.89	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems
pvap	58.84	kPa	413.31	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems
pvap	69.27	kPa	418.35	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems
pvap	77.40	kPa	421.90	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems
pvap	85.63	kPa	425.15	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems

pvap	92.07	kPa	427.54	Low-Pressure VLE Measurements and Thermodynamic Modeling, with PSRK and NRTL, of Binary 1-Alcohol + n-Alkane Systems
pvap	26.31	kPa	392.51	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	26.59	kPa	392.77	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	8.32	kPa	366.67	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1
pvap	11.06	kPa	372.64	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1
pvap	13.87	kPa	377.56	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1
pvap	16.77	kPa	381.80	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1
pvap	16.77	kPa	381.81	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1
pvap	20.26	kPa	386.17	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1
pvap	24.54	kPa	390.77	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1

pvap	24.54	kPa	390.78	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	29.35	kPa	395.23	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	29.35	kPa	395.23	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	34.77	kPa	399.57	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	40.70	kPa	403.73	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	47.57	kPa	407.98	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	60.20	kPa	414.61	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	74.69	kPa	420.99	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	93.19	kPa	427.85	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	93.26	kPa	427.90	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	98.12	kPa	429.52	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	98.16	kPa	429.54	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	

pvap	105.46	kPa	431.85	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	106.75	kPa	432.25	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	106.98	kPa	432.32	Vapor pressure of selected aliphatic alcohols by ebulliometry. Part 1	
pvap	1.43e-04	kPa	237.95	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	1.43e-04	kPa	238.00	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	1.45e-04	kPa	238.00	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	2.96e-04	kPa	243.20	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	
pvap	2.96e-04	kPa	243.20	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol	

pvap	2.93e-04	kPa	243.25	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	5.69e-04	kPa	248.20	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	5.60e-04	kPa	248.20	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	5.64e-04	kPa	248.20	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	1.06e-03	kPa	253.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	1.05e-03	kPa	253.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	1.05e-03	kPa	253.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol

pvap	1.92e-03	kPa	258.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	1.92e-03	kPa	258.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	1.92e-03	kPa	258.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	3.39e-03	kPa	263.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	3.96	kPa	353.82	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	3.38e-03	kPa	263.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol
pvap	0.22	kPa	308.15	Vapor pressures and thermophysical properties of selected hexenols and recommended vapor pressure for hexan-1-ol

rfi	1.41570	298.15	Vapor-Liquid Equilibria of Binary Mixtures Formed by Hexan-1-ol with Chloroethanes and Chloroethenes at 95.6 kPa
rfi	1.41750	293.15	Measurement and Correlation of the Solubilities of m-Phthalic Acid in Monobasic Alcohols
rfi	1.41610	298.15	Densities, Excess Molar Volumes, and Isobaric Thermal Expansibilities for 1,2-Ethanediol + 1-Butanol, or 1-Hexanol, or 1-Octanol in the Temperature Range from (293.15 to 313.15) K
rfi	1.41830	293.15	Densities, Excess Molar Volumes, and Isobaric Thermal Expansibilities for 1,2-Ethanediol + 1-Butanol, or 1-Hexanol, or 1-Octanol in the Temperature Range from (293.15 to 313.15) K
rfi	1.42070	293.20	Vapor Liquid Equilibrium Data for Binary Systems of 1-Methyl-4-(1-methylethenyl)-cyclohexene + {Ethanol, Propan-1-ol, Propan-2-ol, Butan-1-ol, Pentan-1-ol, or Hexan-1-ol} at 40 kPa
rfi	1.41580	298.15	Liquid Liquid Phase Equilibria of 1-Propanol + Water + n-Alcohol Ternary Systems at 298.15 K and Atmospheric Pressure

rfi	1.41650	298.15	Excess Molar Enthalpies of Benzyl Alcohol + Alkanols (C1-C6) and Their Correlations at 298.15 K and Ambient Pressure
rfi	1.41570	298.15	Effect of Pressure on the Static Relative Permittivities of Alkan-1-ols at 298.15 K
rfi	1.41660	298.15	Excess Molar Enthalpies of 1,2-Propanediol + Alkan-1-ols (C1-C6) and Their Correlations at 298.15 K and Ambient Pressure (81.5 kPa)
rfi	1.41590	298.15	Density, Surface Tension, and Refractive Index of Octane + 1-Alkanol Mixtures at T) 298.15 K.
rfi	1.41800	293.15	ERAS modeling of the excess molar enthalpies of binary liquid mixtures of 1-pentanol and 1-hexanol with acetonitrile at atmospheric pressure and 288, 298, 313 and 323K
rfi	1.41600	298.15	Liquid-liquid equilibrium for (water + 5-hydroxymethylfurfural + 1-pentanol/1-hexanol/1-heptanol) systems at 298.15 K
rfi	1.41550	298.15	Ternary liquid liquid equilibrium data for the (water + butyric acid + n-hexane or n-hexanol) systems at T = (298.2, 308.2, and 318.2) K

rfi	1.41800	293.10	Viscosity and surface tension of binary systems of N,N-dimethylformamide with alkan-1-ols at different temperatures
rfi	1.41550	298.20	Ternary equilibrium data of mixtures consisting of 2-butanol, water, and heavy alcohols at T = 298.2 K
rfi	1.41270	313.15	Comparative study of physico-chemical properties of binary mixtures of N,N-dimethylformamide with 1-alkanols at different temperatures
rfi	1.41410	308.15	Comparative study of physico-chemical properties of binary mixtures of N,N-dimethylformamide with 1-alkanols at different temperatures
rfi	1.41570	303.15	Comparative study of physico-chemical properties of binary mixtures of N,N-dimethylformamide with 1-alkanols at different temperatures
rfi	1.41600	298.15	Comparative study of physico-chemical properties of binary mixtures of N,N-dimethylformamide with 1-alkanols at different temperatures

rfi	1.41780	293.15	Densities and derived thermodynamic properties of binary mixtures of diethylcarbonate, acetophenone, and 1-hexanol at T = (293.15 to 323.15) K for the liquid region and at ambient pressure
rfi	1.41423	303.15	Densities, excess molar volumes, and refractive indices of 1,1,2,2-tetrabromoethane and 1-alkanols binary mixtures
rfi	1.41826	293.15	Densities, excess molar volumes, and refractive indices of 1,1,2,2-tetrabromoethane and 1-alkanols binary mixtures
rfi	1.41423	303.15	Densities, excess molar volumes, and refractive indices of 1,1,2,2-tetrachloroethane and 1-alkanols binary mixtures
rfi	1.41826	293.15	Excess molar volumes and viscosities of (1,1,2,2-tetrabromoethane + 1-alkanols) at T = (293.15 and 303.15) K
rfi	1.41738	298.15	Atmospheric densities and interfacial tensions for 1-alkanol (1-butanol to 1-octanol) + water and ether (MTBE, ETBE, DIPE, TAME and THP) + water demixed mixtures.
rfi	1.41810	293.20	Liquid-liquid equilibrium data for systems containing of formic acid, water, and primary normal alcohols at T = 298.2 K

rfi	1.41620		298.15	Phase equilibria in the ternary system isobutyl alcohol + isobutyl acetate + 1-hexanol and the binary systems isobutyl alcohol + 1-hexanol, isobutyl acetate + 1-hexanol at 101.3 kPa
rfi	1.41340		303.15	Measurements of the Properties of Binary Mixtures of Dimethylsulphoxide (DMSO) with 1-Alkanols (C4, C6, C7) at 303.15K
rfi	1.41807		293.15	Densities, excess molar volumes, and refractive indices of 1,1,2,2-tetrachloroethane and 1-alkanols binary mixtures
rfi	1.41780		293.15	Densities, Viscosities, Speeds of Sound, and Refractive Indices for Binary Mixtures of Diethylcarbonate, Acetophenone, and 1-Hexanol at (293.15, 303.15, 313.15, and 323.15) K for the Liquid Region and at Ambient Pressure
rhol	815.00	kg/m3	298.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	815.02	kg/m3	298.15	Surface Properties of Binary Mixtures of Ethylene Glycol with a Series of Aliphatic Alcohols (1-Pentanol, 1-Hexanol, and 1-Heptanol)

rhol	814.95	kg/m3	298.15	Densities and Excess Molar Volumes of N-Methylmorpholine + 1-Alkanol Systems at 298.15 K	
rhol	793.40	kg/m3	328.15	Density and Viscosity of Binary Liquid Mixtures of Ethanol + 1-Hexanol and Ethanol + 1-Heptanol from (293.15 to 328.15) K at 0.1 MPa	
rhol	797.10	kg/m3	323.15	Density and Viscosity of Binary Liquid Mixtures of Ethanol + 1-Hexanol and Ethanol + 1-Heptanol from (293.15 to 328.15) K at 0.1 MPa	
rhol	800.80	kg/m3	318.15	Density and Viscosity of Binary Liquid Mixtures of Ethanol + 1-Hexanol and Ethanol + 1-Heptanol from (293.15 to 328.15) K at 0.1 MPa	
rhol	804.50	kg/m3	313.15	Density and Viscosity of Binary Liquid Mixtures of Ethanol + 1-Hexanol and Ethanol + 1-Heptanol from (293.15 to 328.15) K at 0.1 MPa	
rhol	808.10	kg/m3	308.15	Density and Viscosity of Binary Liquid Mixtures of Ethanol + 1-Hexanol and Ethanol + 1-Heptanol from (293.15 to 328.15) K at 0.1 MPa	

rhol	811.70	kg/m3	303.15	Density and Viscosity of Binary Liquid Mixtures of Ethanol + 1-Hexanol and Ethanol + 1-Heptanol from (293.15 to 328.15) K at 0.1 MPa	
rhol	815.30	kg/m3	298.15	Density and Viscosity of Binary Liquid Mixtures of Ethanol + 1-Hexanol and Ethanol + 1-Heptanol from (293.15 to 328.15) K at 0.1 MPa	
rhol	818.90	kg/m3	293.15	Density and Viscosity of Binary Liquid Mixtures of Ethanol + 1-Hexanol and Ethanol + 1-Heptanol from (293.15 to 328.15) K at 0.1 MPa	
rhol	796.85	kg/m3	323.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols	
rhol	800.56	kg/m3	318.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols	
rhol	804.25	kg/m3	313.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols	
rhol	807.89	kg/m3	308.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols	
rhol	811.52	kg/m3	303.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols	

rhol	815.12	kg/m3	298.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols	
rhol	822.26	kg/m3	288.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols	
rhol	815.16	kg/m3	298.10	Excess Molar Enthalpies of Propyl Propanoate + 1-Hexanol + Benzene at the Temperatures of 25 :C and 35 :C	
rhol	785.90	kg/m3	338.15	Viscosities and Densities of Fatty Alcohol Mixtures from 298.15 to 338.15 K: Estimation by Kay's Rule and Prediction by the UNIFAC-VISCO and GC-UNIMOD Group Contribution Methods	
rhol	793.50	kg/m3	328.15	Viscosities and Densities of Fatty Alcohol Mixtures from 298.15 to 338.15 K: Estimation by Kay's Rule and Prediction by the UNIFAC-VISCO and GC-UNIMOD Group Contribution Methods	
rhol	801.00	kg/m3	318.15	Viscosities and Densities of Fatty Alcohol Mixtures from 298.15 to 338.15 K: Estimation by Kay's Rule and Prediction by the UNIFAC-VISCO and GC-UNIMOD Group Contribution Methods	

rhol	808.40	kg/m3	308.15	Viscosities and Densities of Fatty Alcohol Mixtures from 298.15 to 338.15 K: Estimation by Kay's Rule and Prediction by the UNIFAC-VISCO and GC-UNIMOD Group Contribution Methods	
rhol	815.50	kg/m3	298.15	Viscosities and Densities of Fatty Alcohol Mixtures from 298.15 to 338.15 K: Estimation by Kay's Rule and Prediction by the UNIFAC-VISCO and GC-UNIMOD Group Contribution Methods	
rhol	796.80	kg/m3	323.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model	
rhol	800.60	kg/m3	318.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model	
rhol	804.20	kg/m3	313.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model	
rhol	807.90	kg/m3	308.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model	

rhol	811.50	kg/m3	303.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model
rhol	815.10	kg/m3	298.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model
rhol	818.70	kg/m3	293.15	Investigation of Molecular Interactions in Binary Mixtures of n-Butyl Acetate and (C6 - C10) 1-Alkanol: PC-SAFT Model
rhol	796.80	kg/m3	323.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory
rhol	800.60	kg/m3	318.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory
rhol	804.20	kg/m3	313.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory
rhol	807.90	kg/m3	308.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory

rhol	811.50	kg/m3	303.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory
rhol	815.10	kg/m3	298.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory
rhol	818.70	kg/m3	293.15	Correlation Studies of Cyclohexanone/(C5-C10) Alkan-1-ol Binary Mixtures: PC-SAFT Model and Free Volume Theory
rhol	765.64	kg/m3	363.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	769.78	kg/m3	358.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	773.86	kg/m3	353.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa

rhol	777.86	kg/m3	348.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	781.83	kg/m3	343.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	785.72	kg/m3	338.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	789.57	kg/m3	333.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	793.37	kg/m3	328.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa

rhol	797.12	kg/m3	323.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	800.83	kg/m3	318.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	804.50	kg/m3	313.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	808.13	kg/m3	308.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	811.74	kg/m3	303.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa

rhol	815.32	kg/m3	298.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	818.88	kg/m3	293.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	822.42	kg/m3	288.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	825.94	kg/m3	283.15	Densities and Viscosities for Binary Liquid Mixtures of n-Undecane + 1-Propanol, + 1-Butanol, + 1-Pentanol, and + 1-Hexanol from 283.15 to 363.15 K at 0.1 MPa
rhol	815.70	kg/m3	298.15	Thermodynamics of 1,3-dimethylurea in eight alcohols
rhol	796.20	kg/m3	323.15	Densities, Viscosities, and Refractive Indices of Dimethyl Carbonate + 1-Hexanol/1-Octanol Binary Mixtures at Different Temperatures

rhol	800.10	kg/m3	318.15	Densities, Viscosities, and Refractive Indices of Dimethyl Carbonate + 1-Hexanol/1-Octanol Binary Mixtures at Different Temperatures
rhol	803.90	kg/m3	313.15	Densities, Viscosities, and Refractive Indices of Dimethyl Carbonate + 1-Hexanol/1-Octanol Binary Mixtures at Different Temperatures
rhol	807.60	kg/m3	308.15	Densities, Viscosities, and Refractive Indices of Dimethyl Carbonate + 1-Hexanol/1-Octanol Binary Mixtures at Different Temperatures
rhol	811.30	kg/m3	303.15	Densities, Viscosities, and Refractive Indices of Dimethyl Carbonate + 1-Hexanol/1-Octanol Binary Mixtures at Different Temperatures
rhol	814.90	kg/m3	298.15	Densities, Viscosities, and Refractive Indices of Dimethyl Carbonate + 1-Hexanol/1-Octanol Binary Mixtures at Different Temperatures
rhol	818.00	kg/m3	293.15	Densities, Viscosities, and Refractive Indices of Dimethyl Carbonate + 1-Hexanol/1-Octanol Binary Mixtures at Different Temperatures

rhol	811.39	kg/m3	303.15	Excess molar enthalpies and heat capacities of dimethyl sulfoxide + seven normal alkanols at 303.15K and atmospheric pressure
rhol	815.20	kg/m3	298.15	Excess molar enthalpies of methyl isobutyl ketone (MIBK) with alkan-1-ols (C1-C6) and their correlations at 298.15 K
rhol	815.90	kg/m3	298.15	Excess volumes and partial molar volumes of binary liquid mixtures of furfural or 2-methylfuran with alcohols at 298.15 K
rhol	796.85	kg/m3	323.15	Volumetric and transport properties of binary liquid mixtures with 1-ethyl-3-methylimidazolium ethyl sulfate as candidate solvents for regenerative flue gas desulfurization processes
rhol	800.56	kg/m3	318.15	Volumetric and transport properties of binary liquid mixtures with 1-ethyl-3-methylimidazolium ethyl sulfate as candidate solvents for regenerative flue gas desulfurization processes
rhol	804.23	kg/m3	313.15	Volumetric and transport properties of binary liquid mixtures with 1-ethyl-3-methylimidazolium ethyl sulfate as candidate solvents for regenerative flue gas desulfurization processes

rhol	807.88	kg/m3	308.15	Volumetric and transport properties of binary liquid mixtures with 1-ethyl-3-methylimidazolium ethyl sulfate as candidate solvents for regenerative flue gas desulfurization processes
rhol	811.51	kg/m3	303.15	Volumetric and transport properties of binary liquid mixtures with 1-ethyl-3-methylimidazolium ethyl sulfate as candidate solvents for regenerative flue gas desulfurization processes
rhol	815.11	kg/m3	298.15	Volumetric and transport properties of binary liquid mixtures with 1-ethyl-3-methylimidazolium ethyl sulfate as candidate solvents for regenerative flue gas desulfurization processes
rhol	818.69	kg/m3	293.15	Volumetric and transport properties of binary liquid mixtures with 1-ethyl-3-methylimidazolium ethyl sulfate as candidate solvents for regenerative flue gas desulfurization processes
rhol	822.26	kg/m3	288.15	Volumetric and transport properties of binary liquid mixtures with 1-ethyl-3-methylimidazolium ethyl sulfate as candidate solvents for regenerative flue gas desulfurization processes

rhol	783.00	kg/m3	343.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	791.00	kg/m3	333.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	798.00	kg/m3	323.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	805.00	kg/m3	313.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	812.00	kg/m3	303.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	819.00	kg/m3	293.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume
rhol	822.00	kg/m3	288.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume

rhol	815.29	kg/m3	298.15	Densities, speeds of sound and viscosities of binary mixtures of tetrahydrofuran with 1-hexanol, 1-octanol and 1-decanol at T = (298.15 to 313.15) K
rhol	808.06	kg/m3	308.15	FT-IR studies on excess thermodynamic properties of binary liquid mixtures o-chlorotoluene with 1-propanol, 1-butanol, 1-pentanol, 1-hexanol and 1-heptanol at different temperatures
rhol	811.70	kg/m3	303.15	FT-IR studies on excess thermodynamic properties of binary liquid mixtures o-chlorotoluene with 1-propanol, 1-butanol, 1-pentanol, 1-hexanol and 1-heptanol at different temperatures
rhol	815.31	kg/m3	298.15	FT-IR studies on excess thermodynamic properties of binary liquid mixtures o-chlorotoluene with 1-propanol, 1-butanol, 1-pentanol, 1-hexanol and 1-heptanol at different temperatures
rhol	815.65	kg/m3	298.15	Thermodynamic, transport and excess properties of 2-butoxy ethanol +1-alkanol (C6,C8,C10) at different temperatures

rhol	800.66	kg/m3	318.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	
rhol	804.34	kg/m3	313.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	
rhol	807.98	kg/m3	308.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	
rhol	811.60	kg/m3	303.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	
rhol	815.19	kg/m3	298.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K	

rhol	818.75	kg/m3	293.15	Volume effects for binary mixtures of propane-1,2-diol with methanol, propan-1-ol, hexan-1-ol, octan-1-ol, or nonan-1-ol at temperatures (293.15 to 318.15) K
rhol	815.26	kg/m3	298.15	Studies of thermophysical properties of binary liquid mixtures of amine and alcohols at various temperatures
rhol	785.50	kg/m3	338.15	Effect of temperature and composition on the density, viscosity, surface tension, and thermodynamic properties of binary mixtures of N-octylisoquinolinium bis{(trifluoromethyl)sulfonyl}imide with alcohols
rhol	793.20	kg/m3	328.15	Effect of temperature and composition on the density, viscosity, surface tension, and thermodynamic properties of binary mixtures of N-octylisoquinolinium bis{(trifluoromethyl)sulfonyl}imide with alcohols
rhol	800.60	kg/m3	318.15	Effect of temperature and composition on the density, viscosity, surface tension, and thermodynamic properties of binary mixtures of N-octylisoquinolinium bis{(trifluoromethyl)sulfonyl}imide with alcohols

rhol	808.00	kg/m3	308.15	Effect of temperature and composition on the density, viscosity, surface tension, and thermodynamic properties of binary mixtures of N-octylisoquinolinium bis{(trifluoromethyl)sulfonyl}imide with alcohols
rhol	815.20	kg/m3	298.15	Effect of temperature and composition on the density, viscosity, surface tension, and thermodynamic properties of binary mixtures of N-octylisoquinolinium bis{(trifluoromethyl)sulfonyl}imide with alcohols
rhol	815.21	kg/m3	298.15	Excess molar enthalpies of binary systems containing 2-octanone, hexanoic acid, or octanoic acid at T = 298.15 K
rhol	815.30	kg/m3	298.15	Bubble point measurements of binary mixtures formed by ethyl benzene with selected compounds at 95.35 kPa
rhol	804.46	kg/m3	313.15	Excess molar volumes of binary mixtures of 1,3-dimethylimidazolidin-2-one with an alkan-1-ol at the temperatures 283.15 K, 298.15 K, and 313.15 K
rhol	815.34	kg/m3	298.15	Excess molar volumes of binary mixtures of 1,3-dimethylimidazolidin-2-one with an alkan-1-ol at the temperatures 283.15 K, 298.15 K, and 313.15 K

rhol	826.03	kg/m3	283.15	Excess molar volumes of binary mixtures of 1,3-dimethylimidazolidin-2-one with an alkan-1-ol at the temperatures 283.15 K, 298.15 K, and 313.15 K
rhol	815.88	kg/m3	298.20	Isothermal vapor-liquid equilibria, excess molar volume and the deviation of refractive indices for binary mixtures of 1-butanol, 1-hexanol, 3-methyl-1-butanol and butyl acetate
rhol	814.94	kg/m3	298.15	Phase behaviour of tricyanomethanide-based ionic liquids with alcohols and hydrocarbons
rhol	815.17	kg/m3	298.20	Liquid-liquid equilibrium data for ternary systems of water + lactic acid + C4-C7 alcohols at 298.2 K and atmospheric pressure
rhol	814.94	kg/m3	298.15	Phase behaviour of ionic liquid 1-butyl-1-methylpyrrolidinium tris(pentafluoroethyl)trifluorophosphate with alcohols, water and aromatic hydrocarbons
rhol	815.30	kg/m3	298.15	Bubble point measurements of binary mixtures formed by 1-hexanol with selected nitro-compounds and substituted benzenes at 95.6 kPa

rhol	815.40	kg/m3	298.15	Excess molar enthalpy of 1-alkanol + 1-octene mixtures at 298.15K Experimental results and theoretical description by means of the ERAS and TB models	
rhol	790.80	kg/m3	333.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	794.67	kg/m3	328.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	798.49	kg/m3	323.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	802.27	kg/m3	318.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	

rhol	806.00	kg/m3	313.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhol	809.71	kg/m3	308.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhol	813.39	kg/m3	303.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhol	817.03	kg/m3	298.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine
rhol	820.65	kg/m3	293.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine

rhol	824.25	kg/m3	288.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	827.82	kg/m3	283.15	Volumetric properties of the boldine + alcohol mixtures at atmospheric pressure from 283.15 to 333.15K A new method for the determination of the density of pure boldine	
rhol	815.15	kg/m3	298.15	Speeds of Sound and Isentropic Compressibilities in Binary Mixtures of 2-Propanol with Several 1-Alkanols at 298.15K	
rhol	819.00	kg/m3	293.00	KDB	
rhol	818.70	kg/m3	293.15	Volumetric and Viscometric Study of Binary Systems of Ethyl Butyrate with Alcohols	
sfust	68.11	J/mol×K	225.80	NIST Webbook	
speedsl	1275.70	m/s	308.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K	

speedsl	1303.19	m/s	298.15	Densities, Excess Molar Volumes, Ultrasonic Speeds, and Isentropic Compressibilities of Hexan-1-ol with 1,2-Dichloroethane, 1,2-Dibromoethane, and 1,1,2,2-Tetrachloroethene at (293.15 and 298.15) K
speedsl	1312.40	m/s	298.15	Ultrasonic speeds and isentropic compressibilities of {difurylmethane + (C1 C6) n-alkanol} binary mixtures at T = 298.15 K
speedsl	1339.20	m/s	288.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K
speedsl	1321.20	m/s	293.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K
speedsl	1306.90	m/s	298.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K

speedsl	1289.50	m/s	303.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K
speedsl	1320.11	m/s	293.15	Densities, Excess Molar Volumes, Ultrasonic Speeds, and Isentropic Compressibilities of Hexan-1-ol with 1,2-Dichloroethane, 1,2-Dibromoethane, and 1,1,2,2-Tetrachloroethene at (293.15 and 298.15) K
speedsl	1256.30	m/s	313.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K
speedsl	1320.38	m/s	293.15	Thermodynamic and spectral studies of molecular interactions in binary liquid mixtures of 1-butoxy-2-propanol with 1-alcohols
speedsl	1303.54	m/s	298.15	Thermodynamic and spectral studies of molecular interactions in binary liquid mixtures of 1-butoxy-2-propanol with 1-alcohols

speedsl	1286.68	m/s	303.15	Thermodynamic and spectral studies of molecular interactions in binary liquid mixtures of 1-butoxy-2-propanol with 1-alcohols
speedsl	1270.00	m/s	308.15	Thermodynamic and spectral studies of molecular interactions in binary liquid mixtures of 1-butoxy-2-propanol with 1-alcohols
speedsl	1253.54	m/s	313.15	Thermodynamic and spectral studies of molecular interactions in binary liquid mixtures of 1-butoxy-2-propanol with 1-alcohols
speedsl	1237.50	m/s	318.15	Ultrasonic study of molecular interactions in binary mixtures of methyl acrylate with 1-alkanols (C4 to C10) at temperatures from (288.15 to 318.15) K
srf	0.02	N/m	298.15	Study of surface tension and surface properties of binary systems of DMSO with long chain alcohols at various temperatures
srf	0.03	N/m	288.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.02	N/m	328.15	Study of surface tension and surface properties of binary systems of DMSO with long chain alcohols at various temperatures

srf	0.02	N/m	318.15	Study of surface tension and surface properties of binary systems of DMSO with long chain alcohols at various temperatures
srf	0.02	N/m	308.15	Study of surface tension and surface properties of binary systems of DMSO with long chain alcohols at various temperatures
srf	0.03	N/m	293.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.03	N/m	298.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.02	N/m	308.15	Density and surface tension variation with temperature for n-nonane + 1-hexanol
srf	0.03	N/m	298.15	Density and surface tension variation with temperature for n-nonane + 1-hexanol
srf	0.03	N/m	288.15	Density and surface tension variation with temperature for n-nonane + 1-hexanol
srf	0.03	N/m	298.20	KDB
srf	0.03	N/m	303.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.02	N/m	308.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.02	N/m	313.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes

srf	0.02	N/m	318.15	The additivity of surface and volumetric properties of alpha,omega-dihalogenoalkanes
srf	0.03	N/m	298.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.03	N/m	288.15	Study of surface tension and surface properties of binary systems of DMSO with long chain alcohols at various temperatures
srf	0.02	N/m	303.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	308.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	313.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	318.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.02	N/m	323.15	Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane +1-Alkanols from 298.15 to 323.15 K
srf	0.03	N/m	288.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol

srf	0.03	N/m	293.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol
srf	0.03	N/m	298.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol
srf	0.02	N/m	303.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol
srf	0.02	N/m	308.15	Density and Surface Tension Variation with Temperature for Heptane + 1-Alkanol

Correlations

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)
Coeff. A	1.49468e+01
Coeff. B	-3.55660e+03
Coeff. C	-8.56520e+01
Temperature range (K), min.	328.27
Temperature range (K), max.	454.77

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/T + C*ln(T) + D*T^2
Coeff. A	1.08932e+02
Coeff. B	-1.08747e+04
Coeff. C	-1.31440e+01
Coeff. D	3.48998e-06
Temperature range (K), min.	228.55
Temperature range (K), max.	611.35

Datasets

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
293.15	100.00	818.6
293.15	10000.00	824.8
293.15	20000.00	830.9
293.15	30000.00	836.4
293.15	40000.00	841.6
293.15	50000.00	846.5
293.15	60000.00	851.1
293.15	70000.00	855.5
293.15	80000.00	859.8
293.15	90000.00	863.7
293.15	100000.00	867.9
293.15	110000.00	871.5
293.15	120000.00	875.2
293.15	130000.00	878.7
293.15	140000.00	882.2
303.15	100.00	811.5
303.15	10000.00	818.2
303.15	20000.00	824.1
303.15	30000.00	830.0
303.15	40000.00	835.1
303.15	50000.00	840.5
303.15	60000.00	845.3
303.15	70000.00	849.8
303.15	80000.00	854.2
303.15	90000.00	858.4
303.15	100000.00	862.4
303.15	110000.00	866.3
303.15	120000.00	870.0
303.15	130000.00	873.6
303.15	140000.00	877.1
313.15	100.00	804.2
313.15	10000.00	811.1
313.15	20000.00	817.4
313.15	30000.00	823.5
313.15	40000.00	829.0

313.15	50000.00	834.4
313.15	60000.00	839.4
313.15	70000.00	844.3
313.15	80000.00	848.7
313.15	90000.00	853.1
313.15	100000.00	857.1
313.15	110000.00	861.2
313.15	120000.00	865.1
313.15	130000.00	868.7
313.15	140000.00	872.5
323.15	100.00	797.3
323.15	10000.00	804.5
323.15	20000.00	811.2
323.15	30000.00	817.4
323.15	40000.00	823.3
323.15	50000.00	828.7
323.15	60000.00	833.8
323.15	70000.00	838.5
323.15	80000.00	843.1
323.15	90000.00	847.6
323.15	100000.00	851.8
323.15	110000.00	856.0
323.15	120000.00	860.0
323.15	130000.00	863.7
323.15	140000.00	867.3
333.15	100.00	789.7
333.15	10000.00	797.2
333.15	20000.00	804.3
333.15	30000.00	810.8
333.15	40000.00	817.0
333.15	50000.00	822.7
333.15	60000.00	828.0
333.15	70000.00	832.8
333.15	80000.00	837.6
333.15	90000.00	842.5
333.15	100000.00	846.8
333.15	110000.00	850.8
333.15	120000.00	854.4
333.15	130000.00	858.5
333.15	140000.00	862.2
343.15	100.00	781.9
343.15	10000.00	790.2
343.15	20000.00	797.6
343.15	30000.00	804.4

343.15	40000.00	810.6
343.15	50000.00	816.4
343.15	60000.00	822.1
343.15	70000.00	827.3
343.15	80000.00	832.1
343.15	90000.00	836.9
343.15	100000.00	841.4
343.15	110000.00	845.7
343.15	120000.00	849.7
343.15	130000.00	853.6
343.15	140000.00	857.5
353.15	100.00	773.8
353.15	10000.00	782.3
353.15	20000.00	790.1
353.15	30000.00	797.3
353.15	40000.00	803.8
353.15	50000.00	810.0
353.15	60000.00	815.6
353.15	70000.00	821.0
353.15	80000.00	826.2
353.15	90000.00	831.1
353.15	100000.00	835.6
353.15	110000.00	840.0
353.15	120000.00	844.3
353.15	130000.00	848.4
353.15	140000.00	852.3
363.15	100.00	765.5
363.15	10000.00	774.9
363.15	20000.00	783.1
363.15	30000.00	790.6
363.15	40000.00	797.5
363.15	50000.00	803.8
363.15	60000.00	809.7
363.15	70000.00	815.4
363.15	80000.00	820.6
363.15	90000.00	825.6
363.15	100000.00	830.3
363.15	110000.00	834.8
363.15	120000.00	839.2
363.15	130000.00	843.3
363.15	140000.00	847.2
373.15	100.00	756.9
373.15	10000.00	766.6
373.15	20000.00	775.4

373.15	30000.00	783.4
373.15	40000.00	790.4
373.15	50000.00	796.9
373.15	60000.00	803.1
373.15	70000.00	808.9
373.15	80000.00	814.2
373.15	90000.00	819.5
373.15	100000.00	824.4
373.15	110000.00	829.2
373.15	120000.00	833.3
373.15	130000.00	837.7
373.15	140000.00	841.7
383.15	100.00	748.2
383.15	10000.00	759.1
383.15	20000.00	767.8
383.15	30000.00	776.5
383.15	40000.00	783.5
383.15	50000.00	790.4
383.15	60000.00	796.8
383.15	70000.00	802.6
383.15	80000.00	808.3
383.15	90000.00	813.7
383.15	100000.00	818.7
383.15	110000.00	823.4
383.15	120000.00	828.0
383.15	130000.00	832.3
383.15	140000.00	836.5
393.15	100.00	739.4
393.15	10000.00	750.8
393.15	20000.00	760.5
393.15	30000.00	768.8
393.15	40000.00	777.0
393.15	50000.00	783.7
393.15	60000.00	790.3
393.15	70000.00	796.5
393.15	80000.00	802.5
393.15	90000.00	807.8
393.15	100000.00	813.0
393.15	110000.00	818.1
393.15	120000.00	822.6
393.15	130000.00	827.2
393.15	140000.00	831.5
403.15	100.00	730.2
403.15	10000.00	741.8

403.15	20000.00	751.9
403.15	30000.00	761.1
403.15	40000.00	769.3
403.15	50000.00	776.9
403.15	60000.00	783.7
403.15	70000.00	790.1
403.15	80000.00	796.2
403.15	90000.00	801.8
403.15	100000.00	807.2
403.15	110000.00	812.3
403.15	120000.00	817.1
403.15	130000.00	821.8
403.15	140000.00	826.5

Reference *https://www.doi.org/10.1016/j.fluid.2012.02.007*

Temperature, K	Pressure, kPa	Mass density, kg/m3
298.15	100.00	815.1

Reference *https://www.doi.org/10.1016/j.fluid.2019.02.006*

Temperature, K	Pressure, kPa	Mass density, kg/m3
278.15	100.00	828.9
278.15	1000.00	829.5
278.15	5000.00	832.0
278.15	10000.00	835.0
278.15	15000.00	838.0
278.15	20000.00	840.8
278.15	25000.00	843.6
278.15	30000.00	846.3
278.15	35000.00	848.9
278.15	40000.00	851.4
278.15	45000.00	853.9
278.15	50000.00	856.3
278.15	55000.00	858.7
278.15	60000.00	860.9
288.15	100.00	822.1
288.15	1000.00	822.7
288.15	5000.00	825.3
288.15	10000.00	828.5
288.15	15000.00	831.6
288.15	20000.00	834.6

288.15	25000.00	837.4
288.15	30000.00	840.2
288.15	35000.00	842.9
288.15	40000.00	845.5
288.15	45000.00	848.0
288.15	50000.00	850.5
288.15	55000.00	853.0
288.15	60000.00	855.4
298.15	100.00	814.9
298.15	1000.00	815.6
298.15	5000.00	818.4
298.15	10000.00	821.7
298.15	15000.00	824.9
298.15	20000.00	828.0
298.15	25000.00	830.9
298.15	30000.00	833.8
298.15	35000.00	836.6
298.15	40000.00	839.4
298.15	45000.00	842.0
298.15	50000.00	844.6
298.15	55000.00	847.1
298.15	60000.00	849.6
308.15	100.00	807.8
308.15	1000.00	808.4
308.15	5000.00	811.4
308.15	10000.00	814.8
308.15	15000.00	818.2
308.15	20000.00	821.4
308.15	25000.00	824.5
308.15	30000.00	827.5
308.15	35000.00	830.3
308.15	40000.00	833.2
308.15	45000.00	835.9
308.15	50000.00	838.5
308.15	55000.00	841.1
308.15	60000.00	843.5
318.15	100.00	800.5
318.15	1000.00	801.2
318.15	5000.00	804.3
318.15	10000.00	807.9
318.15	15000.00	811.4
318.15	20000.00	814.7
318.15	25000.00	817.9
318.15	30000.00	821.0

318.15	35000.00	824.0
318.15	40000.00	826.9
318.15	45000.00	829.7
318.15	50000.00	832.4
318.15	55000.00	835.1
318.15	60000.00	837.7
328.15	100.00	793.0
328.15	1000.00	793.7
328.15	5000.00	797.0
328.15	10000.00	800.8
328.15	15000.00	804.4
328.15	20000.00	807.9
328.15	25000.00	811.2
328.15	30000.00	814.4
328.15	35000.00	817.6
328.15	40000.00	820.6
328.15	45000.00	823.5
328.15	50000.00	826.4
328.15	55000.00	829.1
328.15	60000.00	831.6
338.15	100.00	785.4
338.15	1000.00	786.2
338.15	5000.00	789.6
338.15	10000.00	793.6
338.15	15000.00	797.4
338.15	20000.00	801.0
338.15	25000.00	804.5
338.15	30000.00	807.9
338.15	35000.00	811.1
338.15	40000.00	814.2
338.15	45000.00	817.3
338.15	50000.00	820.2
338.15	55000.00	823.1
338.15	60000.00	825.7
348.15	100.00	777.6
348.15	1000.00	778.4
348.15	5000.00	782.0
348.15	10000.00	786.2
348.15	15000.00	790.2
348.15	20000.00	794.1
348.15	25000.00	797.6
348.15	30000.00	801.2
348.15	35000.00	804.6
348.15	40000.00	807.8

348.15	45000.00	811.0
348.15	50000.00	814.0
348.15	55000.00	817.0
348.15	60000.00	819.7
358.15	100.00	769.4
358.15	1000.00	770.0
358.15	5000.00	774.2
358.15	10000.00	778.6
358.15	15000.00	782.8
358.15	20000.00	786.9
358.15	25000.00	790.7
358.15	30000.00	794.3
358.15	35000.00	797.9
358.15	40000.00	801.3
358.15	45000.00	804.6
358.15	50000.00	807.7
358.15	55000.00	810.8
358.15	60000.00	813.5

Reference *https://www.doi.org/10.1016/j.jct.2011.02.008*

Temperature, K	Pressure, kPa	Mass density, kg/m3
278.15	100.00	828.9
278.15	1000.00	829.5
278.15	5000.00	832.0
278.15	10000.00	835.0
278.15	15000.00	838.0
278.15	20000.00	840.8
278.15	25000.00	843.6
278.15	30000.00	846.3
278.15	35000.00	848.9
278.15	40000.00	851.4
278.15	45000.00	853.9
278.15	50000.00	856.3
278.15	55000.00	858.7
278.15	60000.00	860.9
288.15	100.00	822.1
288.15	1000.00	822.7
288.15	5000.00	825.3
288.15	10000.00	828.5
288.15	15000.00	831.6
288.15	20000.00	834.6
288.15	25000.00	837.4

288.15	30000.00	840.2
288.15	35000.00	842.9
288.15	40000.00	845.5
288.15	45000.00	848.0
288.15	50000.00	850.5
288.15	55000.00	853.0
288.15	60000.00	855.4
298.15	100.00	814.9
298.15	1000.00	815.6
298.15	5000.00	818.4
298.15	10000.00	821.7
298.15	15000.00	824.9
298.15	20000.00	828.0
298.15	25000.00	830.9
298.15	30000.00	833.8
298.15	35000.00	836.6
298.15	40000.00	839.4
298.15	45000.00	842.0
298.15	50000.00	844.6
298.15	55000.00	847.1
298.15	60000.00	849.6
308.15	100.00	807.8
308.15	1000.00	808.4
308.15	5000.00	811.4
308.15	10000.00	814.8
308.15	15000.00	818.2
308.15	20000.00	821.4
308.15	25000.00	824.5
308.15	30000.00	827.5
308.15	35000.00	830.3
308.15	40000.00	833.2
308.15	45000.00	835.9
308.15	50000.00	838.5
308.15	55000.00	841.1
308.15	60000.00	843.5
318.15	100.00	800.5
318.15	1000.00	801.2
318.15	5000.00	804.3
318.15	10000.00	807.9
318.15	15000.00	811.4
318.15	20000.00	814.7
318.15	25000.00	817.9
318.15	30000.00	821.0
318.15	35000.00	824.0

318.15	40000.00	826.9
318.15	45000.00	829.7
318.15	50000.00	832.4
318.15	55000.00	835.1
318.15	60000.00	837.7
328.15	100.00	793.0
328.15	1000.00	793.7
328.15	5000.00	797.0
328.15	10000.00	800.8
328.15	15000.00	804.4
328.15	20000.00	807.9
328.15	25000.00	811.2
328.15	30000.00	814.4
328.15	35000.00	817.6
328.15	40000.00	820.6
328.15	45000.00	823.5
328.15	50000.00	826.4
328.15	55000.00	829.1
328.15	60000.00	831.6
338.15	100.00	785.4
338.15	1000.00	786.2
338.15	5000.00	789.6
338.15	10000.00	793.6
338.15	15000.00	797.4
338.15	20000.00	801.0
338.15	25000.00	804.5
338.15	30000.00	807.9
338.15	35000.00	811.1
338.15	40000.00	814.2
338.15	45000.00	817.3
338.15	50000.00	820.2
338.15	55000.00	823.1
338.15	60000.00	825.7
348.15	100.00	777.6
348.15	1000.00	778.4
348.15	5000.00	782.0
348.15	10000.00	786.2
348.15	15000.00	790.2
348.15	20000.00	794.1
348.15	25000.00	797.6
348.15	30000.00	801.2
348.15	35000.00	804.6
348.15	40000.00	807.8
348.15	45000.00	811.0

348.15	50000.00	814.0
348.15	55000.00	817.0
348.15	60000.00	819.7
358.15	100.00	769.4
358.15	1000.00	770.0
358.15	5000.00	774.2
358.15	10000.00	778.6
358.15	15000.00	782.8
358.15	20000.00	786.9
358.15	25000.00	790.7
358.15	30000.00	794.3
358.15	35000.00	797.9
358.15	40000.00	801.3
358.15	45000.00	804.6
358.15	50000.00	807.7
358.15	55000.00	810.8
358.15	60000.00	813.5

Reference *https://www.doi.org/10.1016/j.jct.2011.10.023*

Temperature, K	Pressure, kPa	Mass density, kg/m3
298.15	100.00	815.1

Reference *https://www.doi.org/10.1021/acs.jced.8b01189*

Temperature, K	Pressure, kPa	Mass density, kg/m3
313.14	1034.00	804.9
313.14	2032.00	805.6
313.14	3046.00	806.3
313.14	4016.00	807.0
313.14	5013.00	807.7
313.14	6035.00	808.4
313.14	7010.00	809.1
313.14	8036.00	809.8
313.14	9015.00	810.5
313.14	10002.00	811.2
313.14	11020.00	811.8
313.14	12017.00	812.5
313.14	13002.00	813.2
313.14	14016.00	813.8
313.14	15016.00	814.5
313.14	16009.00	815.1

313.14	17010.00	815.8
313.14	18010.00	816.4
313.14	19012.00	817.1
313.14	20019.00	817.7
313.14	21006.00	818.3
313.14	22037.00	818.9
313.14	23037.00	819.6
313.14	24010.00	820.2
313.14	25023.00	820.8
323.12	1021.00	797.6
323.12	2009.00	798.4
323.12	3003.00	799.1
323.12	4014.00	799.8
323.12	5025.00	800.6
323.12	6021.00	801.3
323.12	7032.00	802.1
323.12	8016.00	802.8
323.12	9016.00	803.5
323.12	10019.00	804.2
323.12	11015.00	805.0
323.12	12012.00	805.7
323.12	13015.00	806.3
323.12	14006.00	807.0
323.12	15002.00	807.7
323.12	16013.00	808.4
323.12	17016.00	809.1
323.12	18018.00	809.7
323.12	19000.00	810.4
323.12	20003.00	811.0
323.12	21009.00	811.7
323.12	22000.00	812.3
323.12	23002.00	813.0
323.12	24021.00	813.6
323.12	25004.00	814.3
333.01	1023.00	790.2
333.01	2011.00	791.0
333.01	3042.00	791.8
333.01	4000.00	792.6
333.01	5014.00	793.3
333.01	6004.00	794.1
333.01	7021.00	794.9
333.01	8012.00	795.7
333.01	9002.00	796.4
333.01	10004.00	797.2

333.01	11026.00	797.9
333.01	12020.00	798.7
333.01	13018.00	799.4
333.01	14009.00	800.1
333.01	15019.00	800.8
333.01	16017.00	801.6
333.01	17006.00	802.3
333.01	18018.00	803.0
333.01	19013.00	803.7
333.01	20037.00	804.4
333.01	21029.00	805.0
333.01	22008.00	805.7
333.01	23026.00	806.4
333.01	24019.00	807.0
333.01	25025.00	807.7
342.96	1036.00	782.9
342.96	2011.00	783.7
342.96	3012.00	784.5
342.96	4015.00	785.4
342.96	5007.00	786.2
342.96	6013.00	787.0
342.96	7039.00	787.8
342.96	8023.00	788.6
342.96	9022.00	789.4
342.96	10035.00	790.2
342.96	11017.00	791.0
342.96	12016.00	791.7
342.96	13023.00	792.5
342.96	14003.00	793.2
342.96	15009.00	793.9
342.96	16014.00	794.7
342.96	17038.00	795.4
342.96	18023.00	796.1
342.96	19015.00	796.8
342.96	20015.00	797.5
342.96	21026.00	798.1
342.96	22003.00	798.8
342.96	23005.00	799.5
342.96	24003.00	800.1
342.96	25031.00	800.8
352.86	1020.00	775.0
352.86	2012.00	775.9
352.86	3028.00	776.9
352.86	4014.00	777.7

352.86	5010.00	778.6
352.86	6028.00	779.5
352.86	7039.00	780.4
352.86	8000.00	781.2
352.86	9030.00	782.1
352.86	10033.00	782.9
352.86	11014.00	783.7
352.86	12017.00	784.5
352.86	13014.00	785.3
352.86	14011.00	786.1
352.86	15010.00	786.9
352.86	16023.00	787.7
352.86	17018.00	788.5
352.86	18016.00	789.3
352.86	19014.00	790.0
352.86	20021.00	790.8
352.86	21017.00	791.5
352.86	22038.00	792.3
352.86	23016.00	793.0
352.86	24020.00	793.7
352.86	25048.00	794.5
362.80	1011.00	767.0
362.80	2009.00	768.0
362.80	3024.00	769.0
362.80	4006.00	769.9
362.80	5021.00	770.8
362.80	6035.00	771.8
362.80	7009.00	772.6
362.80	8023.00	773.6
362.80	9041.00	774.5
362.80	10000.00	775.3
362.80	11014.00	776.2
362.80	12026.00	777.1
362.80	13045.00	777.9
362.80	14030.00	778.8
362.80	15012.00	779.6
362.80	16031.00	780.4
362.80	17003.00	781.2
362.80	18020.00	782.0
362.80	19033.00	782.8
362.80	20004.00	783.6
362.80	21006.00	784.4
362.80	22032.00	785.2
362.80	22989.00	785.9

362.80	24055.00	786.7
362.80	25035.00	787.5

Reference *https://www.doi.org/10.1021/je060154f*

Temperature, K	Pressure, kPa	Mass density, kg/m3
278.15	100.00	829.2
278.15	5000.00	832.2
278.15	10000.00	835.1
278.15	15000.00	837.8
278.15	20000.00	840.7
283.15	100.00	825.8
283.15	5000.00	828.7
283.15	10000.00	831.6
283.15	15000.00	834.5
283.15	20000.00	837.4
288.15	100.00	822.1
288.15	5000.00	825.2
288.15	10000.00	828.2
288.15	15000.00	831.3
288.15	20000.00	834.0
293.15	100.00	818.7
293.15	5000.00	821.9
293.15	10000.00	824.9
293.15	15000.00	827.9
293.15	20000.00	830.7
298.15	100.00	815.1
298.15	5000.00	818.3
298.15	10000.00	821.5
298.15	15000.00	824.6
298.15	20000.00	827.5
303.15	100.00	811.4
303.15	5000.00	814.8
303.15	10000.00	818.0
303.15	15000.00	821.1
303.15	20000.00	824.2
308.15	100.00	808.0
308.15	5000.00	811.3
308.15	10000.00	814.6
308.15	15000.00	817.8
308.15	20000.00	820.9
313.15	100.00	804.2
313.15	5000.00	807.6

313.15	10000.00	811.0
313.15	15000.00	814.3
313.15	20000.00	817.6

Reference *https://www.doi.org/10.1021/je800024u*

Pressure, kPa	Temperature, K	Mass density, kg/m3
100.00	283.15	825.6
100.00	288.15	822.2
100.00	293.15	818.6
100.00	298.15	815.0
100.00	303.15	811.4
100.00	308.15	807.8
100.00	313.15	804.1
100.00	318.15	800.5
100.00	323.15	796.8
5000.00	283.15	828.7
5000.00	288.15	825.2
5000.00	293.15	821.7
5000.00	298.15	818.2
5000.00	303.15	814.7
5000.00	308.15	811.1
5000.00	313.15	807.6
5000.00	318.15	804.0
5000.00	323.15	800.4
10000.00	283.15	831.7
10000.00	288.15	828.2
10000.00	293.15	824.9
10000.00	298.15	821.4
10000.00	303.15	817.9
10000.00	308.15	814.5
10000.00	313.15	811.0
10000.00	318.15	807.5
10000.00	323.15	803.9
20000.00	283.15	837.3
20000.00	288.15	834.1
20000.00	293.15	830.8
20000.00	298.15	827.4
20000.00	303.15	824.1
20000.00	308.15	820.8
20000.00	313.15	817.4
20000.00	318.15	814.0
20000.00	323.15	810.7

30000.00	283.15	842.7
30000.00	288.15	839.5
30000.00	293.15	836.3
30000.00	298.15	833.1
30000.00	303.15	829.9
30000.00	308.15	826.7
30000.00	313.15	823.5
30000.00	318.15	820.1
30000.00	323.15	816.9
40000.00	283.15	847.8
40000.00	288.15	844.7
40000.00	293.15	841.6
40000.00	298.15	838.5
40000.00	303.15	835.4
40000.00	308.15	832.3
40000.00	313.15	829.1
40000.00	318.15	825.9
40000.00	323.15	822.8
50000.00	283.15	852.6
50000.00	288.15	849.6
50000.00	293.15	846.6
50000.00	298.15	843.5
50000.00	303.15	840.5
50000.00	308.15	837.5
50000.00	313.15	834.4
50000.00	318.15	831.4
50000.00	323.15	828.2
60000.00	283.15	857.2
60000.00	288.15	854.3
60000.00	293.15	851.4
60000.00	298.15	848.3
60000.00	303.15	845.4
60000.00	308.15	842.4
60000.00	313.15	839.4
60000.00	318.15	836.4
60000.00	323.15	833.4

Reference *https://www.doi.org/10.1021/je8006875*

Speed of sound, m/s

Pressure, kPa - Liquid	Temperature, K - Liquid	Speed of sound, m/s - Liquid

101.00	292.91	1320.79
30390.00	292.92	1465.73
45590.00	292.92	1525.8
60790.00	292.91	1581.37
75990.00	292.92	1633.75
91180.00	292.91	1682.67
101320.00	292.91	1713.2
101.00	308.15	1269.05
15200.00	308.15	1349.81
30390.00	308.15	1419.69
45590.00	308.15	1482.88
60790.00	308.15	1540.4
75990.00	308.15	1594.13
91180.00	308.16	1643.48
101320.00	308.16	1675.87
101.00	298.18	1302.75
15200.00	298.19	1381.46
30390.00	298.19	1449.11
45590.00	298.19	1510.11
60790.00	298.19	1566.83
75990.00	298.19	1619.35
91180.00	298.19	1668.5
101320.00	298.19	1699.28
101.00	313.13	1252.38
15200.00	313.14	1334.05
30390.00	313.14	1404.76
45590.00	313.14	1469.3
60790.00	313.14	1527.64
75990.00	313.14	1581.73
91180.00	313.14	1632.08
101320.00	313.14	1664.3
101.00	318.22	1235.52
15200.00	318.22	1318.81
30390.00	318.21	1390.85
45590.00	318.21	1456.0
60790.00	318.21	1514.43
75990.00	318.21	1569.15
91180.00	318.21	1620.49
101320.00	318.21	1653.0

Reference *https://www.doi.org/10.1016/j.jct.2012.09.027*

Sources

Determination and Correlation of Solubilities of Lauric Acid in Eight Alcohols:	https://www.doi.org/10.1021/je500222s
Activity coefficients at infinite dilution of hydrocarbons, alkylbenzenes, and alcohols in the paramagnetic ionic liquid 1-butyl-3-methylimidazolium tetrachloroferrate(III) using gas-liquid chromatography:	https://www.doi.org/10.1016/j.jct.2008.09.004
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Legend

af:	Acentric Factor
affp:	Proton affinity
aigt:	Autoignition Temperature
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
fll:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpc:	Flash Point (Closed Cup Method)
fpo:	Flash Point (Open Cup Method)

gf:	Standard Gibbs free energy of formation
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
kvisc:	Kinematic viscosity
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sg:	Molar entropy at standard conditions
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tc:	Critical Temperature
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility