Cyclohexane, methyl-

Other names:	CYCLOHEXYLMETHANE HEXAHYDROTOLUENE Hexahydroxytoluene METHYLCYCLOHEXANE Metylocykloheksan NSC 9391 SEXTONE B Toluene hexahydride Toluene, hexahydro- UN 2296
Inchi:	InChI=1S/C7H14/c1-7-5-3-2-4-6-7/h7H,2-6H2,1H3
InchiKey:	UAEPNZWRGJTJPN-UHFFFAOYSA-N
Formula:	C7H14
SMILES:	CC1CCCCC1
Mol. weight [g/mol]:	98.19
CAS:	108-87-2

Physical Properties

Property code	Value	Unit	Source
af	0.2360		KDB
ap	314.150	K	KDB
chl	-4565.29 ± 0.96	kJ/mol	NIST Webbook
chl	-4564.30 ± 1.90	kJ/mol	NIST Webbook
chl	-4604.90	kJ/mol	NIST Webbook
dm	0.00	debye	KDB
dvisc	0.0006830	Pa×s	Speeds of sound, isentropic compressibilities, viscosities and excess molar volumes of binary mixtures of methylcyclohexane + 2-alkanols or ethanol at T = 298.15 K
gf	27.30	kJ/mol	KDB
gyrad	3.7470		KDB
hcg	4565.29	kJ/mol	KDB
hcn	4257.136	kJ/mol	KDB
hf	-154.80 ± 1.00	kJ/mol	NIST Webbook

hf	-159.90	kJ/mol	NIST Webbook
hf	-154.90	kJ/mol	KDB
hfl	-190.20 ± 1.00	kJ/mol	NIST Webbook
hfl	-195.30 ± 1.90	kJ/mol	NIST Webbook
hfus	5.72	kJ/mol	Joback Method
hvap	31.61	kJ/mol	Joback Method
ie	9.64 ± 0.10	eV	NIST Webbook
ie	9.76 ± 0.03	eV	NIST Webbook
ie	9.85 ± 0.03	eV	NIST Webbook
ie	9.62 ± 0.05	eV	NIST Webbook
ie	9.64	eV	NIST Webbook
ie	9.69 ± 0.15	eV	NIST Webbook
ie	9.64 ± 0.10	eV	NIST Webbook
log10ws	-3.85		Estimated Solubility Method
log10ws	-3.85		Aqueous Solubility Prediction Method
logp	2.587		Crippen Method
mcvol	98.630	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=2)		KDB
pc	3480.00 ± 20.00	kPa	NIST Webbook
pc	3471.00 ± 30.40	kPa	NIST Webbook
pc	3470.00	kPa	Critical Point Measurements for Five n-Alkylcyclohexanes (C6 to C10) by the Pulse-Heating Method
pc	3480.00	kPa	KDB
pc	3477.68 ± 5.06	kPa	NIST Webbook
rhoc	266.08 ± 1.96	kg/m3	NIST Webbook
rhoc	266.97 ± 2.95	kg/m3	NIST Webbook
rhoc	266.58 ± 2.95	kg/m3	NIST Webbook
rhoc	266.08 ± 1.96	kg/m3	NIST Webbook
rinpol	735.00		NIST Webbook
rinpol	719.00		NIST Webbook
rinpol	750.00		NIST Webbook
rinpol	714.00		NIST Webbook
rinpol	727.00		NIST Webbook
rinpol	717.00		NIST Webbook
rinpol	718.00		NIST Webbook
rinpol	715.75		NIST Webbook
rinpol	735.00		NIST Webbook
rinpol	717.10		NIST Webbook
rinpol	722.20		NIST Webbook
rinpol	758.30		NIST Webbook

rinpol	737.00	NIST Webbook
rinpol	754.00	NIST Webbook
rinpol	726.00	NIST Webbook
rinpol	709.00	NIST Webbook
rinpol	715.00	NIST Webbook
rinpol	733.10	NIST Webbook
rinpol	750.40	NIST Webbook
rinpol	759.70	NIST Webbook
rinpol	720.00	NIST Webbook
rinpol	724.00	NIST Webbook
rinpol	724.10	NIST Webbook
rinpol	724.20	NIST Webbook
rinpol	724.40	NIST Webbook
rinpol	723.20	NIST Webbook
rinpol	757.20	NIST Webbook
rinpol	715.00	NIST Webbook
rinpol	724.00	NIST Webbook
rinpol	726.00	NIST Webbook
rinpol	718.00	NIST Webbook
rinpol	726.00	NIST Webbook
rinpol	735.00	NIST Webbook
rinpol	740.00	NIST Webbook
rinpol	726.10	NIST Webbook
rinpol	730.20	NIST Webbook
rinpol	715.00	NIST Webbook
rinpol	725.00	NIST Webbook
rinpol	726.00	NIST Webbook
rinpol	728.00	NIST Webbook
rinpol	719.00	NIST Webbook
rinpol	721.40	NIST Webbook
rinpol	723.80	NIST Webbook
rinpol	726.20	NIST Webbook
rinpol	734.60	NIST Webbook
rinpol	714.00	NIST Webbook
rinpol	718.00	NIST Webbook
rinpol	722.00	NIST Webbook
rinpol	726.00	NIST Webbook
rinpol	731.00	NIST Webbook
rinpol	735.00	NIST Webbook
rinpol	723.10	NIST Webbook
rinpol	725.40	NIST Webbook
rinpol	727.90	NIST Webbook
rinpol	730.60	NIST Webbook
rinpol	733.30	NIST Webbook

rinpol	736.30	NIST Webbook
rinpol	724.00	NIST Webbook
rinpol	724.40	NIST Webbook
rinpol	736.00	NIST Webbook
rinpol	744.00	NIST Webbook
rinpol	730.00	NIST Webbook
rinpol	721.00	NIST Webbook
rinpol	721.00	NIST Webbook
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rinpol	720.00	NIST Webbook
rinpol	730.90	NIST Webbook
rinpol	731.90	NIST Webbook
rinpol	754.00	NIST Webbook
rinpol	737.00	NIST Webbook
rinpol	725.80	NIST Webbook
rinpol	731.50	NIST Webbook
rinpol	725.80	NIST Webbook
rinpol	730.00	NIST Webbook
rinpol	735.40	NIST Webbook
rinpol	735.70	NIST Webbook
rinpol	730.10	NIST Webbook
rinpol	730.90	NIST Webbook
rinpol	738.00	NIST Webbook
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rinpol	736.00	NIST Webbook
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rinpol	731.00	NIST Webbook
rinpol	732.00	NIST Webbook
rinpol	725.00	NIST Webbook
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rinpol	751.00	NIST Webbook
rinpol	723.00	NIST Webbook
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rinpol	760.00	NIST Webbook
rinpol	738.00	NIST Webbook
rinpol	713.00	NIST Webbook
rinpol	716.00	NIST Webbook
rinpol	739.00	NIST Webbook
rinpol	717.70	NIST Webbook
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rinpol	720.20	NIST Webbook
rinpol	715.27	NIST Webbook
rinpol	715.65	NIST Webbook
rinpol	718.30	NIST Webbook
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rinpol	721.90	NIST Webbook

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rinpol	724.00	NIST Webbook
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rinpol	719.00	NIST Webbook

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rinpol	725.00	NIST Webbook
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rinpol	736.00	NIST Webbook
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rinpol	735.00	NIST Webbook
rinpol	750.00	NIST Webbook
ripol	778.00	NIST Webbook
ripol	790.00	NIST Webbook
ripol	794.00	NIST Webbook
ripol	799.00	NIST Webbook
ripol	804.00	NIST Webbook
ripol	814.00	NIST Webbook
ripol	760.00	NIST Webbook
ripol	781.00	NIST Webbook
ripol	780.00	NIST Webbook
ripol	784.00	NIST Webbook
ripol	760.00	NIST Webbook
ripol	800.00	NIST Webbook
ripol	814.00	NIST Webbook

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ripol	759.00		NIST Webbook
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ripol	759.00		NIST Webbook
ripol	780.00		NIST Webbook
ripol	766.00		NIST Webbook
ripol	756.00		NIST Webbook
ripol	778.00		NIST Webbook
ripol	785.00		NIST Webbook
ripol	814.00		NIST Webbook
sg	343.30	J/mol×K	NIST Webbook
sl	248.10	J/mol×K	NIST Webbook
sl	247.90	J/mol×K	NIST Webbook
tb	373.35	K	Isobaric Vapor-Liquid Equilibrium for Two Binary Systems of 3,3-Dimethyloxetane + Methyl Cyclohexane and 3-Chloro-2,2-dimethyl-1-propanol + Methyl Cyclohexane at 101.3 kPa
tb	374.08	K	Isobaric Vapor-Liquid Equilibrium for Two Binary Systems of n-Heptane + sec-Butyl Acetate and Methylcyclohexane + sec-Butyl Acetate under Atmosphere
tb	373.90	K	Excess molar volumes of the ternary system {methylcyclohexane (1) + cyclohexane (2) + n-alkanes (3)} at T = 298.15 K
tb	374.07	K	VLE of the binary systems (dimethyl carbonate with 2-propanol or 2-butanol) and (diethyl carbonate with methylcyclohexane) at 101.3 kPa
tb	373.88	K	Isobaric vapor-liquid equilibrium data for methylcyclohexane + 2-methoxyethanol and methylcyclohexane + 2-ethoxyethanol at 50.00 and 101.33 kPa

tb	373.96	K	Isobaric vapor liquid equilibrium for ternary mixtures of ethanol and methylcyclohexane with 3-methylpentane and tert-butyl alcohol at 101.3 kPa
tb	373.96	K	Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures of Ethanol, Methylcyclohexane and p-Xylene
tb	374.08	K	KDB
tb	372.13	K	Measurement on vapor pressure, density and viscosity for binary mixtures of JP-10 and methylcyclohexane
tc	572.10	K	KDB
tf	146.50	K	Aqueous Solubility Prediction Method
tf	147.85	K	Density, Viscosity, and Freezing Point for Four Binary Systems of n-Dodecane or Methylcyclohexane Mixed with 1-Heptanol or Cyclohexylmethanol
tf	146.50	K	KDB
tt	146.57 ± 0.08	K	NIST Webbook
tt	146.58 ± 0.05	K	NIST Webbook
vc	0.369	m3/kmol	KDB
vc	0.369	m3/kmol	NIST Webbook
zc	0.2699580		KDB
zra	0.27		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	180.75	J/mol×K	390.00	NIST Webbook
cpg	184.60 ± 1.70	J/mol×K	398.00	NIST Webbook
cpg	189.12	J/mol×K	410.00	NIST Webbook
cpg	203.40 ± 2.10	J/mol×K	439.00	NIST Webbook
cpg	222.80 ± 2.10	J/mol×K	480.00	NIST Webbook
cpg	241.90 ± 2.50	J/mol×K	527.00	NIST Webbook
cpl	184.80	J/mol×K	298.15	NIST Webbook
cpl	184.96	J/mol×K	298.15	NIST Webbook
cpl	185.29	J/mol×K	298.15	NIST Webbook

cpl	185.27	J/mol×K	298.06	NIST Webbook
cpl	184.38	J/mol×K	298.15	NIST Webbook
cpl	182.00	J/mol×K	294.20	NIST Webbook
cpl	184.84	J/mol×K	298.15	NIST Webbook
cpl	184.51	J/mol×K	298.15	NIST Webbook
dvisc	0.0006385	Pa×s	303.15	Densities and Viscosities of Binary and Ternary Mixtures of (Nitrobenzene + 1-Bromobutane), (1-Bromobutane + Methylcyclohexane), (Nitrobenzene + Methylcyclohexane), and (Methylcyclohexane + Nitrobenzene + 1-Bromobutane) from (293.15 to 308.15) K
dvisc	0.0005268	Pa×s	323.66	Shear Viscosities of Methycyclohexane, Perfluoromethylcyclohexane, and Their Mixtures in the Vicinity of the Upper Critical Mixing Temperature. 1. Critical Isopleth and Coexistence Curve
dvisc	0.0005669	Pa×s	317.71	Shear Viscosities of Methycyclohexane, Perfluoromethylcyclohexane, and Their Mixtures in the Vicinity of the Upper Critical Mixing Temperature. 1. Critical Isopleth and Coexistence Curve
dvisc	0.0004690	Pa×s	333.69	Shear Viscosities of Methycyclohexane, Perfluoromethylcyclohexane, and Their Mixtures in the Vicinity of the Upper Critical Mixing Temperature. 1. Critical Isopleth and Coexistence Curve

dvisc	0.0007293	Pa×s	293.15	Densities and Viscosities of Binary and Ternary Mixtures of (Nitrobenzene + 1-Bromobutane), (1-Bromobutane + Methylcyclohexane), (Nitrobenzene + Methylcyclohexane), and (Methylcyclohexane + Nitrobenzene + 1-Bromobutane) from (293.15 to 308.15) K
dvisc	0.0006827	Pa×s	298.15	Densities and Viscosities of Binary and Ternary Mixtures of (Nitrobenzene + 1-Bromobutane), (1-Bromobutane + Methylcyclohexane), (Nitrobenzene + Methylcyclohexane), and (Methylcyclohexane + Nitrobenzene + 1-Bromobutane) from (293.15 to 308.15) K
dvisc	0.0006360	Pa×s	308.95	Shear Viscosities of Methycyclohexane, Perfluoromethylcyclohexane, and Their Mixtures in the Vicinity of the Upper Critical Mixing Temperature. 1. Critical Isopleth and Coexistence Curve

dvisc	0.0005997	Pa×s	308.15	Densities and Viscosities of Binary and Ternary Mixtures of (Nitrobenzene + 1-Bromobutane), (1-Bromobutane + Methylcyclohexane), (Nitrobenzene + Methylcyclohexane), and (Methylcyclohexane + Nitrobenzene + 1-Bromobutane) from (293.15 to 308.15) K
dvisc	0.0007190	Pa×s	298.15	Volumetric and Viscous Properties at Several Temperatures for Binary Mixtures of N-Methylpiperazine with Methylcyclohexane or n-Heptane
dvisc	0.0006844	Pa×s	303.63	Shear Viscosities of Methycyclohexane, Perfluoromethylcyclohexane, and Their Mixtures in the Vicinity of the Upper Critical Mixing Temperature. 1. Critical Isopleth and Coexistence Curve
dvisc	0.0005730	Pa×s	313.15	Volumetric and Viscous Properties at Several Temperatures for Binary Mixtures of N-Methylpiperazine with Methylcyclohexane or n-Heptane

dvisc	0.0007341	Pa×s	298.61	Shear Viscosities of Methycyclohexane, Perfluoromethylcyclohexane, and Their Mixtures in the Vicinity of the Upper Critical Mixing Temperature. 1. Critical Isopleth and Coexistence Curve
dvisc	0.0005620	Pa×s	313.15	Density, Viscosity, and Speed of Sound of Dialkyl Carbonates with Cyclopentane and Methyl Cyclohexane at Several Temperatures
dvisc	0.0005980	Pa×s	308.15	Density, Viscosity, and Speed of Sound of Dialkyl Carbonates with Cyclopentane and Methyl Cyclohexane at Several Temperatures
dvisc	0.0006370	Pa×s	303.15	Density, Viscosity, and Speed of Sound of Dialkyl Carbonates with Cyclopentane and Methyl Cyclohexane at Several Temperatures
dvisc	0.0006810	Pa×s	298.15	Density, Viscosity, and Speed of Sound of Dialkyl Carbonates with Cyclopentane and Methyl Cyclohexane at Several Temperatures

dvisc	0.0004964	Pa×s	328.77	Shear Viscosities of Methycyclohexane, Perfluoromethylcyclohexane, and Their Mixtures in the Vicinity of the Upper Critical Mixing Temperature. 1. Critical Isopleth and Coexistence Curve
dvisc	0.0006550	Pa×s	303.15	Volumetric and Viscous Properties at Several Temperatures for Binary Mixtures of N-Methylpiperazine with Methylcyclohexane or n-Heptane
dvisc	0.0007290	Pa×s	293.15	Density, Viscosity, and Speed of Sound of Dialkyl Carbonates with Cyclopentane and Methyl Cyclohexane at Several Temperatures
hfust	6.67	kJ/mol	146.20	NIST Webbook
hfust	6.69	kJ/mol	146.60	NIST Webbook
hfust	6.75	kJ/mol	146.58	NIST Webbook
hfust	6.75	kJ/mol	146.60	NIST Webbook
hvapt	31.13	kJ/mol	374.10	KDB
hvapt	34.90	kJ/mol	337.00	NIST Webbook
hvapt	31.80	kJ/mol	374.00	NIST Webbook
hvapt	32.50 ± 0.10	kJ/mol	353.00	NIST Webbook
hvapt	33.50 ± 0.10	kJ/mol	333.00	NIST Webbook
hvapt	34.60	kJ/mol	338.00	NIST Webbook
hvapt	31.27	kJ/mol	374.10	NIST Webbook
hvapt	33.80	kJ/mol	349.50	NIST Webbook
hvapt	36.20	kJ/mol	314.00	NIST Webbook
hvapt	32.30	kJ/mol	442.00	NIST Webbook
hvapt	31.20	kJ/mol	537.00	NIST Webbook
hvapt	23.40	kJ/mol	473.00	NIST Webbook
hvapt	32.20	kJ/mol	353.00	NIST Webbook
hvapt	29.90	kJ/mol	393.00	NIST Webbook
hvapt	26.90	kJ/mol	433.00	NIST Webbook
hvapt	36.10	kJ/mol	310.50	NIST Webbook
hvapt	34.60 ± 0.10	kJ/mol	313.00	NIST Webbook

pvap	101.30	kPa	373.35	Isobaric Vapor-Liquid Equilibrium for Two Binary Systems of 3,3-Dimethyloxetane + Methyl Cyclohexane and 3-Chloro-2,2-dimethyl-1-propanol + Methyl Cyclohexane at 101.3 kPa
pvap	73.30	kPa	363.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
pvap	53.80	kPa	353.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
pvap	38.70	kPa	343.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
pvap	27.10	kPa	333.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K

pvap	12.30	kPa	313.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K	
pvap	7.90	kPa	303.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K	
pvap	93.32	kPa	371.15	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components	
pvap	79.99	kPa	365.87	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components	
pvap	66.66	kPa	359.85	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components	
pvap	53.33	kPa	352.80	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components	
pvap	40.00	kPa	344.18	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components	

pvap	101.30	kPa	374.08	Isobaric Vapor-Liquid Equilibrium for Two Binary Systems of n-Heptane + sec-Butyl Acetate and Methylcyclohexane + sec-Butyl Acetate under Atmosphere
pvap	18.50	kPa	323.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
rfi	1.41630		308.15	Physico-chemical and excess properties of the binary mixtures of methylcyclohexane + ethanol, + propan-1-ol, + propan-2-ol, + butan-1-ol, + 2-methyl-1-propanol, or 3-methyl-1-butanol at T = (298.15, 303.15, and 308.15) K
rfi	1.41920		303.15	Physico-chemical and excess properties of the binary mixtures of methylcyclohexane + ethanol, + propan-1-ol, + propan-2-ol, + butan-1-ol, + 2-methyl-1-propanol, or 3-methyl-1-butanol at T = (298.15, 303.15, and 308.15) K

rfi	1.41920	303.15	Excess and deviation properties for the binary mixtures of methylcyclohexane with benzene, toluene, p-xylene, mesitylene, and anisole at T = (298.15, 303.15, and 308.15) K
rfi	1.41630	308.15	Excess and deviation properties for the binary mixtures of methylcyclohexane with benzene, toluene, p-xylene, mesitylene, and anisole at T = (298.15, 303.15, and 308.15) K
rfi	1.42062	298.15	Separation of toluene from cyclic hydrocarbons using 1-butyl-3-methylimidazolium methylsulfate ionic liquid at T = 298.15 K and atmospheric pressure
rfi	1.42062	298.15	(Liquid + liquid) equilibrium data for the ternary systems (cycloalkane + ethylbenzene + 1-ethyl-3-methylimidazolium ethylsulfate) at T = 298.15 K and atmospheric pressure
rfi	1.42578	288.15	Densities and Viscosities for Binary and Ternary Mixtures of Diisopropyl Ether, Ethanol, and Methylcyclohexane
rfi	1.42053	298.15	Densities and Viscosities for Binary and Ternary Mixtures of Diisopropyl Ether, Ethanol, and Methylcyclohexane

rfi	1.41537	308.15	Densities and Viscosities for Binary and Ternary Mixtures of Diisopropyl Ether, Ethanol, and Methylcyclohexane
rfi	1.42062	298.15	Liquid Extraction of Benzene from Its Mixtures Using 1-Ethyl-3-methylimidazolium Ethylsulfate as a Solvent
rfi	1.42062	298.15	Extraction of Benzene from Aliphatic Compounds Using Commercial Ionic Liquids as Solvents: Study of the Liquid Liquid Equilibrium at T = 298.15 K
rfi	1.42062	298.15	Liquid Liquid Extraction of Aromatic Compounds from Cycloalkanes Using 1-Butyl-3-methylimidazolium Methylsulfate Ionic Liquid
rfi	1.41750	293.15	Density, Viscosity, Refractive Index, and Freezing Point for Binary Mixtures of 1,1'-Bicyclohexyl with Alkylcyclohexane
rfi	1.42300	293.10	Measurement and Correlation of Liquid-Liquid Equilibria of Methylcyclohexane + Toluene + N-Formylmorpholine at (293, 303, 313, and 323) K
rfi	1.42048	298.15	Measurement and Correlation of Liquid-Liquid Equilibria of Two Imidazolium Ionic Liquids with Thiophene and Methylcyclohexane

rfi	1.42833	283.15	Density, Speed of Sound, and Refractive Index of the Binary Systems Cyclohexane (1) or Methylcyclohexane (1) or Cyclo-octane (1) with Benzene (2), Toluene (2), and Ethylbenzene (2) at Two Temperatures
rfi	1.42170	298.15	Physico-chemical and excess properties of the binary mixtures of methylcyclohexane + ethanol, + propan-1-ol, + propan-2-ol, + butan-1-ol, + 2-methyl-1-propanol, or 3-methyl-1-butanol at T = (298.15, 303.15, and 308.15) K
rfi	1.42062	298.15	Effect of the Chain Length on the Aromatic Ring in the Separation of Aromatic Compounds from Methylcyclohexane Using the Ionic Liquid 1-Ethyl-3-methylpyridinium Ethylsulfate
rfi	1.42062	298.15	Density, Speed of Sound, and Refractive Index for Binary Mixtures Containing Cycloalkanes with o-Xylene, m-Xylene, p-Xylene, and Mesitylene at T = (298.15 and 313.15) K

rfi	1.41274	313.15	Density, Speed of Sound, and Refractive Index for Binary Mixtures Containing Cycloalkanes with o-Xylene, m-Xylene, p-Xylene, and Mesitylene at T = (298.15 and 313.15) K
rfi	1.41274	313.15	Density, Speed of Sound, and Refractive Index for Binary Mixtures Containing Cycloalkanes with o-Xylene, m-Xylene, p-Xylene, and Mesitylene at T = (298.15 and 313.15) K
rfi	1.41630	308.15	Excess properties of the binary mixtures of methylcyclohexane + alkanes (C6 to C12) at T = 298.15 K to T = 308.15 K
rfi	1.41920	303.15	Excess properties of the binary mixtures of methylcyclohexane + alkanes (C6 to C12) at T = 298.15 K to T = 308.15 K
rfi	1.42170	298.15	Excess properties of the binary mixtures of methylcyclohexane + alkanes (C6 to C12) at T = 298.15 K to T = 308.15 K
rfi	1.42062	298.15	Experimental data, correlation and prediction of the extraction of benzene from cyclic hydrocarbons using [Epy][ESO4] ionic liquid

rfi	1.40250		298.15	Phase equilibria of binary systems of 3-methylthiophene with four different hydrocarbons
rfi	1.42300		293.10	Liquid liquid equilibria of methylcyclohexane benzene N-formylmorpholine at several temperatures
rfi	1.42058		298.15	KDB
rfi	1.42062		298.15	Density, Speed of Sound, and Refractive Index of the Binary Systems Cyclohexane (1) or Methylcyclohexane (1) or Cyclo-octane (1) with Benzene (2), Toluene (2), and Ethylbenzene (2) at Two Temperatures
rfi	1.42170		298.15	Excess and deviation properties for the binary mixtures of methylcyclohexane with benzene, toluene, p-xylene, mesitylene, and anisole at T = (298.15, 303.15, and 308.15) K
rhol	747.58	kg/m3	318.15	Densities, Viscosities, Refractive Indices, and Surface Tensions of Binary Mixtures of 2,2,4-Trimethylpentane with Several Alkylated Cyclohexanes from (293.15 to 343.15) K
rhol	747.60	kg/m3	318.15	Excess Molar Volume along with Viscosity and Refractive Index for Binary Systems of Tricyclo[5.2.1.0(2.6)]decane with Five Cycloalkanes

rhol	751.99	kg/m3	313.15	Excess Molar Volume along with Viscosity and Refractive Index for Binary Systems of Tricyclo[5.2.1.0(2.6)]decane with Five Cycloalkanes
rhol	774.00	kg/m3	289.00	KDB
rhol	764.96	kg/m3	298.15	Revision of the volumetric method for measurements of liquid liquid equilibria in binary systems
rhol	764.96	kg/m3	298.15	Liquid liquid equilibrium in ternary systems N,N-dimethylformamide + 2-methylpentane + methanol and N,N-dimethylformamide + methylcyclohexane + methanol
rhol	764.99	kg/m3	298.15	Excess molar volumes, viscosities, and speeds of sound of the ternary mixture {1-heptanol (1) + trichloroethylene (2) + methylcyclohexane (3)} at T = 298.15 K
rhol	765.97	kg/m3	298.15	Separation of ethylbenzene/styrene systems using ionic liquids in ternary LLE
rhol	769.38	kg/m3	293.15	Measurement and correlation of density and viscosity of binary mixtures of fatty acid (methyl esters + methylcyclohexane)
rhol	765.06	kg/m3	298.15	Measurement and correlation of density and viscosity of binary mixtures of fatty acid (methyl esters + methylcyclohexane)

rhol	760.71	kg/m3	303.15	Measurement and correlation of density and viscosity of binary mixtures of fatty acid (methyl esters + methylcyclohexane)
rhol	756.35	kg/m3	308.15	Measurement and correlation of density and viscosity of binary mixtures of fatty acid (methyl esters + methylcyclohexane)
rhol	751.98	kg/m3	313.15	Measurement and correlation of density and viscosity of binary mixtures of fatty acid (methyl esters + methylcyclohexane)
rhol	747.59	kg/m3	318.15	Measurement and correlation of density and viscosity of binary mixtures of fatty acid (methyl esters + methylcyclohexane)
rhol	743.19	kg/m3	323.15	Measurement and correlation of density and viscosity of binary mixtures of fatty acid (methyl esters + methylcyclohexane)
rhol	769.35	kg/m3	293.15	Densities, Viscosities, Refractive Indices, and Surface Tensions of Binary Mixtures of 2,2,4-Trimethylpentane with Several Alkylated Cyclohexanes from (293.15 to 343.15) K

rhol	765.05	kg/m3	298.15	Densities, Viscosities, Refractive Indices, and Surface Tensions of Binary Mixtures of 2,2,4-Trimethylpentane with Several Alkylated Cyclohexanes from (293.15 to 343.15) K
rhol	760.71	kg/m3	303.15	Densities, Viscosities, Refractive Indices, and Surface Tensions of Binary Mixtures of 2,2,4-Trimethylpentane with Several Alkylated Cyclohexanes from (293.15 to 343.15) K
rhol	756.37	kg/m3	308.15	Densities, Viscosities, Refractive Indices, and Surface Tensions of Binary Mixtures of 2,2,4-Trimethylpentane with Several Alkylated Cyclohexanes from (293.15 to 343.15) K
rhol	752.00	kg/m3	313.15	Densities, Viscosities, Refractive Indices, and Surface Tensions of Binary Mixtures of 2,2,4-Trimethylpentane with Several Alkylated Cyclohexanes from (293.15 to 343.15) K
rhol	756.36	kg/m3	308.15	Excess Molar Volume along with Viscosity and Refractive Index for Binary Systems of Tricyclo[5.2.1.0(2.6)]decane with Five Cycloalkanes

rhol	743.17	kg/m3	323.15	Densities, Viscosities, Refractive Indices, and Surface Tensions of Binary Mixtures of 2,2,4-Trimethylpentane with Several Alkylated Cyclohexanes from (293.15 to 343.15) K
rhol	734.29	kg/m3	333.15	Densities, Viscosities, Refractive Indices, and Surface Tensions of Binary Mixtures of 2,2,4-Trimethylpentane with Several Alkylated Cyclohexanes from (293.15 to 343.15) K
rhol	725.31	kg/m3	343.15	Densities, Viscosities, Refractive Indices, and Surface Tensions of Binary Mixtures of 2,2,4-Trimethylpentane with Several Alkylated Cyclohexanes from (293.15 to 343.15) K
rhol	769.72	kg/m3	293.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	769.91	kg/m3	293.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	770.07	kg/m3	293.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers

rhol	761.08	kg/m3	303.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	761.27	kg/m3	303.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	761.42	kg/m3	303.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	752.63	kg/m3	313.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	752.82	kg/m3	313.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	752.97	kg/m3	313.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	744.37	kg/m3	323.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	744.55	kg/m3	323.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	744.71	kg/m3	323.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers

rhol	736.29	kg/m3	333.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers	
rhol	736.47	kg/m3	333.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers	
rhol	736.62	kg/m3	333.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers	
rhol	728.38	kg/m3	343.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers	
rhol	728.56	kg/m3	343.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers	
rhol	728.71	kg/m3	343.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers	
rhol	720.64	kg/m3	353.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers	
rhol	720.82	kg/m3	353.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers	

rhol	720.97	kg/m3	353.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	713.07	kg/m3	363.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	713.24	kg/m3	363.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	713.39	kg/m3	363.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	705.65	kg/m3	373.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	705.82	kg/m3	373.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers
rhol	705.96	kg/m3	373.20	Measurement of Hydrogen Solubility in Potential Liquid Organic Hydrogen Carriers

rhol	764.95	kg/m3	298.15	Liquid Liquid Equilibria, Equilibrium Phase Densities, and Refractive Indices for the Quaternary Mixtures Containing 2-Propanol or 2-Methyl-2-Propanol of Fuel Oxygenate at T = 298.15 and 318.15 K
rhol	769.30	kg/m3	293.15	Densities, Viscosities, Speeds of Sound, Bulk Moduli, Surface Tensions, and Flash Points of Binary Mixtures of Ethylcyclohexane or Methylcyclohexane with n-Dodecane or n-Hexadecane at 0.1 MPa
rhol	764.99	kg/m3	298.15	Densities, Viscosities, Speeds of Sound, Bulk Moduli, Surface Tensions, and Flash Points of Binary Mixtures of Ethylcyclohexane or Methylcyclohexane with n-Dodecane or n-Hexadecane at 0.1 MPa
rhol	760.64	kg/m3	303.15	Densities, Viscosities, Speeds of Sound, Bulk Moduli, Surface Tensions, and Flash Points of Binary Mixtures of Ethylcyclohexane or Methylcyclohexane with n-Dodecane or n-Hexadecane at 0.1 MPa

rhol	751.92	kg/m3	313.15	Densities, Viscosities, Speeds of Sound, Bulk Moduli, Surface Tensions, and Flash Points of Binary Mixtures of Ethylcyclohexane or Methylcyclohexane with n-Dodecane or n-Hexadecane at 0.1 MPa
rhol	743.13	kg/m3	323.15	Densities, Viscosities, Speeds of Sound, Bulk Moduli, Surface Tensions, and Flash Points of Binary Mixtures of Ethylcyclohexane or Methylcyclohexane with n-Dodecane or n-Hexadecane at 0.1 MPa
rhol	734.25	kg/m3	333.15	Densities, Viscosities, Speeds of Sound, Bulk Moduli, Surface Tensions, and Flash Points of Binary Mixtures of Ethylcyclohexane or Methylcyclohexane with n-Dodecane or n-Hexadecane at 0.1 MPa
rhol	768.85	kg/m3	293.20	Isothermal Vapor-Liquid Equilibrium Data for Binary Systems of CHF3 or C2F6 with Methylcyclohexane or Toluene
rhol	767.19	kg/m3	295.20	Isothermal Vapor-Liquid Equilibrium Data for Binary Systems of CHF3 or C2F6 with Methylcyclohexane or Toluene

rhol	765.90	kg/m3	296.70	Isothermal Vapor-Liquid Equilibrium Data for Binary Systems of CHF3 or C2F6 with Methylcyclohexane or Toluene
rhol	765.61	kg/m3	297.00	Isothermal Vapor-Liquid Equilibrium Data for Binary Systems of CHF3 or C2F6 with Methylcyclohexane or Toluene
rhol	765.51	kg/m3	297.20	Isothermal Vapor-Liquid Equilibrium Data for Binary Systems of CHF3 or C2F6 with Methylcyclohexane or Toluene
rhol	764.67	kg/m3	298.20	Isothermal Vapor-Liquid Equilibrium Data for Binary Systems of CHF3 or C2F6 with Methylcyclohexane or Toluene
rhol	769.35	kg/m3	293.15	Densities and Viscosities for the Ternary System of Decalin + Methylcyclohexane + Cyclopentanol and Corresponding Binaries at T = 293.15 to 343.15 K
rhol	765.00	kg/m3	298.15	Densities and Viscosities for the Ternary System of Decalin + Methylcyclohexane + Cyclopentanol and Corresponding Binaries at T = 293.15 to 343.15 K

rhol	760.65	kg/m3	303.15	Densities and Viscosities for the Ternary System of Decalin + Methylcyclohexane + Cyclopentanol and Corresponding Binaries at T = 293.15 to 343.15 K
rhol	756.30	kg/m3	308.15	Densities and Viscosities for the Ternary System of Decalin + Methylcyclohexane + Cyclopentanol and Corresponding Binaries at T = 293.15 to 343.15 K
rhol	751.93	kg/m3	313.15	Densities and Viscosities for the Ternary System of Decalin + Methylcyclohexane + Cyclopentanol and Corresponding Binaries at T = 293.15 to 343.15 K
rhol	747.56	kg/m3	318.15	Densities and Viscosities for the Ternary System of Decalin + Methylcyclohexane + Cyclopentanol and Corresponding Binaries at T = 293.15 to 343.15 K
rhol	743.16	kg/m3	323.15	Densities and Viscosities for the Ternary System of Decalin + Methylcyclohexane + Cyclopentanol and Corresponding Binaries at T = 293.15 to 343.15 K

rhol	738.74	kg/m3	328.15	Densities and Viscosities for the Ternary System of Decalin + Methylcyclohexane + Cyclopentanol and Corresponding Binaries at T = 293.15 to 343.15 K
rhol	734.29	kg/m3	333.15	Densities and Viscosities for the Ternary System of Decalin + Methylcyclohexane + Cyclopentanol and Corresponding Binaries at T = 293.15 to 343.15 K
rhol	729.82	kg/m3	338.15	Densities and Viscosities for the Ternary System of Decalin + Methylcyclohexane + Cyclopentanol and Corresponding Binaries at T = 293.15 to 343.15 K
rhol	725.32	kg/m3	343.15	Densities and Viscosities for the Ternary System of Decalin + Methylcyclohexane + Cyclopentanol and Corresponding Binaries at T = 293.15 to 343.15 K
rhol	769.00	kg/m3	293.15	Isothermal Vapor-Liquid Equilibrium Data for the Binary Systems Consisting of 1,1,2,3,3,3-Hexafluoro-1-propene and Either Methylcyclohexane, Cyclohexane, n-Hexane, 2-Methyltetrahydrofuran, or 2,2,3,3,4,4,4-Heptafluoro-1-butanol

rhol	764.96	kg/m3	298.15	Liquid-Liquid Equilibrium and Excess Enthalpies in Binary Systems Methylcyclohexane + Methanol and Methylcyclohexane + N,N-Dimethylformamide
rhol	765.20	kg/m3	298.15	Vapor-Liquid Equilibria for the Ternary Systems of Methyl tert-Butyl Ether + Methanol + Methylcyclohexane and Methyl tert-Butyl Ether + Methanol + n-Heptane and Constituent Binary Systems at 313.15 K
rhol	764.86	kg/m3	298.15	Thermodynamics of Mixtures Containing a Very Strongly Polar Compound. 10. Liquid Liquid Equilibria for N,N-Dimethylacetamide + Selected Alkanes
rhol	769.35	kg/m3	293.15	Excess Molar Volume along with Viscosity and Refractive Index for Binary Systems of Tricyclo[5.2.1.0(2.6)]decane with Five Cycloalkanes
rhol	765.04	kg/m3	298.15	Excess Molar Volume along with Viscosity and Refractive Index for Binary Systems of Tricyclo[5.2.1.0(2.6)]decane with Five Cycloalkanes
rhol	760.71	kg/m3	303.15	Excess Molar Volume along with Viscosity and Refractive Index for Binary Systems of Tricyclo[5.2.1.0(2.6)]decane with Five Cycloalkanes

rhol	764.90	kg/m3	298.15	Density, Speed of Sound, and Refractive Index for Binary Mixtures Containing Cycloalkanes and Aromatic Compounds at T = 313.15 K
sfust	46.05	J/mol×K	146.58	NIST Webbook
sfust	45.14	J/mol×K	146.20	NIST Webbook
srf	0.02	N/m	293.20	KDB

Correlations

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)
Coeff. A	1.41079e+01
Coeff. B	-3.16636e+03
Coeff. C	-4.03310e+01
Temperature range (K), min.	269.44
Temperature range (K), max.	400.29

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/T + C*ln(T) + D*T^2
Coeff. A	8.72968e+01
Coeff. B	-7.12610e+03
Coeff. C	-1.09404e+01
Coeff. D	8.50410e-06
Temperature range (K), min.	146.58
Temperature range (K), max.	572.19

Datasets

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
410.00	200000.00	812.647
410.00	180000.00	804.482
410.00	160000.00	795.899
410.00	140000.00	786.383
410.00	120000.00	776.018
410.00	100000.00	764.111
410.00	90000.00	757.777
410.00	80000.00	750.846
410.00	70000.00	743.853
410.00	60000.00	736.124
410.00	50000.00	727.698
410.00	40000.00	717.821
410.00	30000.00	707.272
410.00	20000.00	695.044
450.00	200000.00	798.897
450.00	180000.00	790.183
450.00	160000.00	780.708
450.00	140000.00	770.433
450.00	120000.00	759.037
450.00	100000.00	746.296
450.00	90000.00	739.304
450.00	80000.00	731.598
450.00	70000.00	723.281
450.00	60000.00	714.464
450.00	50000.00	704.34
450.00	40000.00	693.215
450.00	30000.00	680.595
450.00	20000.00	664.914
500.00	200000.00	779.786
500.00	180000.00	770.353
500.00	160000.00	759.878
500.00	140000.00	748.645
500.00	120000.00	735.845
500.00	100000.00	721.454
500.00	90000.00	713.602
500.00	80000.00	704.872
500.00	70000.00	695.54
500.00	60000.00	684.828
500.00	50000.00	672.946

500.00	40000.00	659.481
500.00	30000.00	643.213
500.00	20000.00	623.145
550.00	200000.00	760.464
550.00	180000.00	750.159
550.00	160000.00	739.33
550.00	140000.00	726.911
550.00	120000.00	713.086
550.00	100000.00	697.29
550.00	90000.00	688.637
550.00	80000.00	678.738
550.00	70000.00	668.08
550.00	60000.00	656.179
550.00	50000.00	642.447
550.00	40000.00	626.206
550.00	30000.00	605.816
550.00	20000.00	579.029
600.00	200000.00	741.384
600.00	180000.00	730.911
600.00	160000.00	718.93
600.00	140000.00	705.698
600.00	120000.00	690.895
600.00	100000.00	673.632
600.00	90000.00	664.012
600.00	80000.00	653.239
600.00	70000.00	641.114
600.00	60000.00	627.511
600.00	50000.00	611.576
600.00	40000.00	592.364
600.00	30000.00	567.711
600.00	20000.00	532.582
600.00	12000.00	485.331
410.00	10000.00	680.503
450.00	10000.00	645.737
500.00	10000.00	595.224
550.00	10000.00	537.032

Reference *https://www.doi.org/10.1007/s10765-017-2241-7*

Temperature, K	Pressure, kPa	Mass density, kg/m3
283.15	100.00	777.6
283.15	5000.00	781.4
283.15	10000.00	785.2

283.15	15000.00	788.7
283.15	20000.00	792.1
283.15	25000.00	795.3
283.15	30000.00	798.5
283.15	35000.00	801.5
283.15	40000.00	804.4
283.15	45000.00	807.3
293.15	100.00	769.0
293.15	5000.00	773.0
293.15	10000.00	777.0
293.15	15000.00	780.7
293.15	20000.00	784.3
293.15	25000.00	787.8
293.15	30000.00	791.1
293.15	35000.00	794.2
293.15	40000.00	797.3
293.15	45000.00	800.2
303.15	100.00	760.4
303.15	5000.00	764.7
303.15	10000.00	768.9
303.15	15000.00	772.8
303.15	20000.00	776.6
303.15	25000.00	780.2
303.15	30000.00	783.7
303.15	35000.00	787.0
303.15	40000.00	790.2
303.15	45000.00	793.3
313.15	100.00	751.7
313.15	5000.00	756.2
313.15	10000.00	760.7
313.15	15000.00	764.8
313.15	20000.00	768.8
313.15	25000.00	772.7
313.15	30000.00	776.3
313.15	35000.00	779.8
313.15	40000.00	783.1
313.15	45000.00	786.4
323.15	100.00	742.9
323.15	5000.00	747.7
323.15	10000.00	752.5
323.15	15000.00	756.9
323.15	20000.00	761.1
323.15	25000.00	765.1
323.15	30000.00	769.0

323.15	35000.00	772.6
323.15	40000.00	776.1
323.15	45000.00	779.5
333.15	100.00	733.9
333.15	5000.00	739.0
333.15	10000.00	744.1
333.15	15000.00	748.8
333.15	20000.00	753.3
333.15	25000.00	757.5
333.15	30000.00	761.5
333.15	35000.00	765.4
333.15	40000.00	769.0
333.15	45000.00	772.5
343.15	100.00	724.8
343.15	5000.00	730.4
343.15	10000.00	735.8
343.15	15000.00	740.8
343.15	20000.00	745.6
343.15	25000.00	750.0
343.15	30000.00	754.2
343.15	35000.00	758.2
343.15	40000.00	762.1
343.15	45000.00	765.7
353.15	100.00	715.7
353.15	5000.00	721.7
353.15	10000.00	727.4
353.15	15000.00	732.8
353.15	20000.00	737.8
353.15	25000.00	742.5
353.15	30000.00	747.0
353.15	35000.00	751.2
353.15	40000.00	755.2
353.15	45000.00	759.0

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Thermal conductivity, W/m/K

Pressure, kPa - Liquid	Temperature, K - Liquid	Thermal conductivity, W/m/K - Liquid
96.00	302.00	0.1056
96.00	302.48	0.1054

96.00	303.02	0.1052
97.00	301.17	0.1058
97.00	301.56	0.1057
125.00	321.59	0.1008
128.00	321.98	0.1007
129.00	322.42	0.1005
132.00	322.90	0.1004
134.00	323.43	0.1003
140.00	381.25	0.0877
144.00	381.66	0.0876
148.00	382.09	0.0875
151.00	382.58	0.0874
157.00	383.11	0.0873
159.00	340.09	0.0964
179.00	340.50	0.0964
199.00	340.97	0.0963
213.00	360.16	0.0921
216.00	341.47	0.0961
229.00	342.02	0.0960
229.00	360.59	0.0920
246.00	361.06	0.0918
262.00	361.56	0.0917
319.00	360.24	0.0921
338.00	360.65	0.0920
354.00	361.12	0.0919
371.00	361.62	0.0918
389.00	362.14	0.0917
4974.00	301.55	0.1075
4975.00	301.16	0.1076
4981.00	301.98	0.1074
4988.00	302.46	0.1071
4995.00	302.99	0.1071
5052.00	323.39	0.1023
5053.00	322.87	0.1024
5058.00	322.40	0.1026
5065.00	321.59	0.1028
5066.00	321.97	0.1027
5170.00	340.29	0.0986
5183.00	340.70	0.0985
5196.00	341.15	0.0985
5209.00	341.64	0.0983
5221.00	342.17	0.0981
5232.00	381.28	0.0903
5239.00	381.67	0.0902

5242.00	382.15	0.0901
5246.00	382.61	0.0900
5250.00	383.12	0.0899
5318.00	360.52	0.0944
5334.00	360.93	0.0944
5344.00	361.38	0.0942
5355.00	361.86	0.0941
5370.00	362.40	0.0939
10060.00	323.35	0.1043
10073.00	322.84	0.1044
10074.00	321.58	0.1048
10075.00	321.96	0.1047
10077.00	322.37	0.1046
10174.00	381.41	0.0926
10175.00	360.80	0.0966
10177.00	381.79	0.0925
10181.00	382.20	0.0925
10185.00	382.65	0.0924
10187.00	361.19	0.0965
10191.00	383.16	0.0922
10202.00	361.63	0.0963
10214.00	362.05	0.0962
10220.00	362.58	0.0961
10264.00	301.15	0.1095
10268.00	301.53	0.1094
10276.00	301.96	0.1093
10282.00	302.42	0.1091
10285.00	302.94	0.1091
10297.00	340.62	0.1007
10311.00	341.02	0.1006
10324.00	341.36	0.1005
10336.00	341.88	0.1004
10348.00	342.41	0.1002
15046.00	322.36	0.1064
15047.00	322.81	0.1063
15051.00	321.94	0.1065
15052.00	323.31	0.1062
15067.00	321.56	0.1066
15359.00	301.13	0.1112
15364.00	301.51	0.1112
15367.00	301.93	0.1111
15369.00	302.39	0.1109
15369.00	302.91	0.1108
20077.00	381.47	0.0970

20079.00	381.83	0.0969
20080.00	382.23	0.0969
20083.00	382.66	0.0967
20089.00	383.14	0.0966
20101.00	301.49	0.1128
20103.00	301.91	0.1127
20105.00	302.37	0.1126
20106.00	301.12	0.1129
20111.00	302.87	0.1124
20118.00	323.27	0.1080
20122.00	322.77	0.1081
20134.00	322.33	0.1083
20137.00	321.55	0.1084
20140.00	321.92	0.1084
20146.00	360.98	0.1007
20163.00	361.36	0.1005
20175.00	361.78	0.1004
20185.00	362.23	0.1003
20191.00	362.73	0.1002
20284.00	340.69	0.1046
20295.00	341.08	0.1045
20305.00	341.50	0.1044
20315.00	341.96	0.1043
20326.00	342.45	0.1041
20779.00	401.40	0.0939
20781.00	402.98	0.0937
20783.00	401.69	0.0940
20786.00	402.08	0.0940
20788.00	402.50	0.0939
25201.00	321.53	0.1102
25206.00	321.90	0.1101
25213.00	322.30	0.1100
25216.00	322.74	0.1099
25218.00	323.23	0.1098
25356.00	301.48	0.1146
25356.00	301.89	0.1144
25357.00	301.11	0.1146
25365.00	302.34	0.1143
25376.00	302.83	0.1141
30060.00	401.62	0.0977
30061.00	401.28	0.0978
30061.00	402.00	0.0978
30062.00	402.40	0.0976
30065.00	402.86	0.0976

30157.00	301.10	0.1161
30163.00	301.45	0.1161
30166.00	381.53	0.1009
30168.00	381.88	0.1009
30170.00	382.26	0.1008
30172.00	382.68	0.1008
30173.00	301.86	0.1160
30175.00	383.14	0.1006
30178.00	302.31	0.1158
30182.00	302.80	0.1157
30197.00	361.13	0.1044
30204.00	361.49	0.1046
30214.00	361.94	0.1042
30229.00	362.37	0.1041
30238.00	321.51	0.1120
30240.00	362.86	0.1040
30245.00	321.87	0.1119
30247.00	322.27	0.1118
30248.00	322.70	0.1117
30250.00	323.18	0.1115
30916.00	340.82	0.1084
30924.00	341.19	0.1083
30924.00	342.03	0.1080
30929.00	341.58	0.1082
30930.00	342.52	0.1080
35184.00	321.89	0.1136
35184.00	322.28	0.1134
35187.00	322.71	0.1132
35189.00	321.54	0.1135
35194.00	323.19	0.1131
35410.00	302.81	0.1173
35412.00	301.12	0.1177
35412.00	302.32	0.1173
35414.00	301.88	0.1176
35415.00	301.48	0.1177
39278.00	302.78	0.1184
39375.00	302.30	0.1186
39484.00	301.86	0.1188
39611.00	301.45	0.1189
39719.00	301.10	0.1190
40156.00	361.31	0.1079
40156.00	361.66	0.1078
40164.00	362.05	0.1078
40170.00	362.47	0.1076

40176.00	362.93	0.1076
40251.00	340.96	0.1114
40255.00	382.26	0.1045
40256.00	381.56	0.1047
40257.00	382.67	0.1044
40259.00	381.89	0.1046
40259.00	383.12	0.1044
40260.00	341.32	0.1114
40269.00	341.72	0.1114
40272.00	342.62	0.1111
40276.00	342.14	0.1113
40385.00	323.14	0.1148
40395.00	321.51	0.1153
40397.00	322.25	0.1150
40398.00	321.86	0.1151
40399.00	322.67	0.1149
40492.00	401.21	0.1018
40492.00	401.53	0.1017
40496.00	401.89	0.1017
40498.00	402.28	0.1017
40498.00	402.71	0.1015

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[illegible]	https://www.doi.org/10.1021/je400487e
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Legend

af:	Acentric Factor
ap:	Aniline Point
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hcg:	Heat of Combustion, Gross form
hcn:	Heat of Combustion, Net Form
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sfust:	Entropy of fusion at a given temperature
sg:	Molar entropy at standard conditions
sl:	Liquid phase molar entropy at standard conditions
srf:	Surface Tension
tb:	Normal Boiling Point Temperature

tc:	Critical Temperature
tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility
zra:	Rackett Parameter