Cyclohexane

Other names:	Benzene, hexahydro-
	Cicloesano
	Cykloheksan
	Hexahydrobenzene
	Hexamethylene
	Hexanaphthene
	NSC 406835
	Rcra waste number U056
	UN 1145
Inchi:	InChI=1S/C6H12/c1-2-4-6-5-3-1/h1-6H2
InchiKey:	XDTMQSROBMDMFD-UHFFFAOYSA-N
Formula:	C6H12
SMILES:	C1CCCCC1
Mol. weight [g/mol]:	84.16
CAS:	110-82-7

Physical Properties

Property code	Value	Unit	Source
af	0.2120		KDB
affp	686.90	kJ/mol	NIST Webbook
aigt	543.15	K	KDB
ap	304.150	K	KDB
basg	666.90	kJ/mol	NIST Webbook
chl	-3918.00 ± 0.75	kJ/mol	NIST Webbook
chl	-3918.40 ± 1.00	kJ/mol	NIST Webbook
chl	-3919.60 ± 1.30	kJ/mol	NIST Webbook
chl	-3935.30	kJ/mol	NIST Webbook
chl	-3918.60 ± 0.70	kJ/mol	NIST Webbook
chl	-3947.00	kJ/mol	NIST Webbook
chl	-3919.90 ± 0.71	kJ/mol	NIST Webbook
dm	0.30	debye	KDB
dvisc	0.0008920	Pa×s	Densities and Viscosities of Ternary Mixtures of Cyclohexane + Cyclohexanone + Some Alkyl Acetates at 298.15 K
fll	1.33	% in Air	KDB
flu	8.35	% in Air	KDB

fpo	253.15	K	KDB
gf	31.78	kJ/mol	KDB
gyrad	3.2610		KDB
hcg	3919.82	kJ/mol	KDB
hcn	3655.770	kJ/mol	KDB
hf	-123.20	kJ/mol	KDB
hf	-124.60	kJ/mol	NIST Webbook
hf	-123.30	kJ/mol	NIST Webbook
hf	-123.10 ± 0.79	kJ/mol	NIST Webbook
hfl	-156.20 ± 0.79	kJ/mol	NIST Webbook
hfl	-157.70 ± 1.80	kJ/mol	NIST Webbook
hfl	-156.40 ± 1.30	kJ/mol	NIST Webbook
hfus	2.06	kJ/mol	Joback Method
hvap	33.12	kJ/mol	NIST Webbook
hvap	33.00	kJ/mol	NIST Webbook
hvap	33.00 ± 0.10	kJ/mol	NIST Webbook
hvap	32.90 ± 0.30	kJ/mol	NIST Webbook
hvap	32.79 ± 0.14	kJ/mol	NIST Webbook
hvap	32.90	kJ/mol	NIST Webbook
hvap	33.00 ± 0.02	kJ/mol	NIST Webbook
hvap	33.00 ± 0.10	kJ/mol	NIST Webbook
hvap	33.00 ± 0.10	kJ/mol	NIST Webbook
hvap	33.04	kJ/mol	NIST Webbook
hvap	33.50	kJ/mol	NIST Webbook
hvap	33.00	kJ/mol	NIST Webbook
hvap	33.03	kJ/mol	NIST Webbook
hvap	33.10	kJ/mol	NIST Webbook
hvap	33.30 ± 0.10	kJ/mol	NIST Webbook
hvap	33.50	kJ/mol	NIST Webbook
hvap	33.10	kJ/mol	NIST Webbook
hvap	30.20 ± 0.30	kJ/mol	NIST Webbook
hvap	30.10	kJ/mol	NIST Webbook
hvap	33.00	kJ/mol	NIST Webbook
hvap	33.00	kJ/mol	NIST Webbook
ie	9.89 ± 0.01	eV	NIST Webbook
ie	9.88	eV	NIST Webbook
ie	9.83 ± 0.05	eV	NIST Webbook
ie	9.88 ± 0.02	eV	NIST Webbook
ie	9.81	eV	NIST Webbook
ie	9.88	eV	NIST Webbook
ie	9.88 ± 0.10	eV	NIST Webbook
ie	10.00 ± 0.03	eV	NIST Webbook
ie	9.84	eV	NIST Webbook
ie	9.80 ± 0.05	eV	NIST Webbook

ie	9.88 ± 0.01	eV	NIST Webbook
ie	9.88 ± 0.03	eV	NIST Webbook
ie	9.89	eV	NIST Webbook
ie	9.88 ± 0.01	eV	NIST Webbook
ie	10.30	eV	NIST Webbook
ie	10.30 ± 0.10	eV	NIST Webbook
ie	10.32	eV	NIST Webbook
ie	11.00 ± 0.20	eV	NIST Webbook
ie	9.88 ± 0.02	eV	NIST Webbook
ie	9.79	eV	NIST Webbook
ie	9.87	eV	NIST Webbook
ie	9.82	eV	NIST Webbook
log10ws	-3.10		Aqueous Solubility Prediction Method
log10ws	-3.10		Estimated Solubility Method
logp	2.341		Crippen Method
mcvol	84.540	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
nfpah	%!d(float64=1)		KDB
pc	4071.00 ± 20.00	kPa	NIST Webbook
pc	4200.00	kPa	Critical Properties of the Reacting Mixture in the Selective Oxidation of Cyclohexane by Oxygen in the Presence of Carbon Dioxide
pc	4080.00 ± 30.00	kPa	NIST Webbook
pc	4060.00	kPa	Critical Point Measurements for Five n-Alkylcyclohexanes (C6 to C10) by the Pulse-Heating Method
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pc	4110.76 ± 101.32	kPa	NIST Webbook
pc	4036.00 ± 60.00	kPa	NIST Webbook
pc	4097.00 ± 10.34	kPa	NIST Webbook
pc	4075.00 ± 2.00	kPa	NIST Webbook
pc	4036.70 ± 39.99	kPa	NIST Webbook
pt	5.40	kPa	KDB
rhoc	273.27 ± 5.05	kg/m3	NIST Webbook
rhoc	273.52 ± 1.68	kg/m3	NIST Webbook
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sl	203.89	J/mol×K	NIST Webbook
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tb	354.55 ± 0.30	K	NIST Webbook
tb	354.00 ± 1.00	K	NIST Webbook
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tb	353.73	K	Isobaric Vapor-Liquid Equilibria for Binary and Ternary Mixtures with Cyclohexane, Cyclohexene, and 2-Methoxyethanol at 100 kPa
tb	353.90	K	Isobaric Vapor-Liquid Equilibria for (Acetic Acid + Cyclohexane) and (Cyclohexane + Acetylacetone) at a Pressure of 101.3 kPa and for (Acetic Acid + Acetylacetone) at a Pressure of 60.0 kPa

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tb	353.70 ± 2.00	K	NIST Webbook
tb	353.90 ± 0.30	K	NIST Webbook
tb	353.90 ± 0.50	K	NIST Webbook
tb	353.90 ± 0.50	K	NIST Webbook
tb	353.72 ± 0.30	K	NIST Webbook
tb	354.08 ± 0.20	K	NIST Webbook
tb	354.15 ± 0.40	K	NIST Webbook
tb	353.95 ± 0.25	K	NIST Webbook
tb	353.90 ± 0.50	K	NIST Webbook
tb	354.00 ± 0.30	K	NIST Webbook
tb	353.00 ± 3.00	K	NIST Webbook
tb	353.89 ± 0.15	K	NIST Webbook
tb	353.80 ± 0.50	K	NIST Webbook
tb	353.15 ± 1.00	K	NIST Webbook
tb	353.95 ± 0.30	K	NIST Webbook
tb	353.81 ± 0.20	K	NIST Webbook
tb	352.35 ± 1.50	K	NIST Webbook
tb	353.80 ± 0.50	K	NIST Webbook
tb	353.80 ± 0.30	K	NIST Webbook
tb	353.87 ± 0.15	K	NIST Webbook
tb	354.00 ± 0.30	K	NIST Webbook
tb	354.00 ± 0.50	K	NIST Webbook
tb	353.95 ± 0.30	K	NIST Webbook
tb	353.90 ± 0.30	K	NIST Webbook
tb	353.80 ± 0.50	K	NIST Webbook
tb	353.88 ± 0.01	K	NIST Webbook
tb	353.90 ± 1.00	K	NIST Webbook
tb	353.70 ± 1.00	K	NIST Webbook
tb	354.10 ± 0.40	K	NIST Webbook
tb	353.15 ± 0.50	K	NIST Webbook
tb	353.89 ± 0.05	K	NIST Webbook
tb	353.95 ± 0.30	K	NIST Webbook
tb	353.89 ± 0.10	K	NIST Webbook
tb	353.75 ± 0.40	K	NIST Webbook
tb	353.96 ± 0.10	K	NIST Webbook
tb	353.95 ± 0.20	K	NIST Webbook

tb	354.10 ± 0.60	K	NIST Webbook
tb	354.05 ± 0.40	K	NIST Webbook
tb	353.95 ± 0.20	K	NIST Webbook
tb	354.40 ± 1.00	K	NIST Webbook
tb	353.88 ± 0.10	K	NIST Webbook
tb	342.10 ± 0.20	K	NIST Webbook
tc	553.64 ± 0.03	K	NIST Webbook
tc	553.00 ± 2.00	K	NIST Webbook
tc	553.80	K	KDB
tc	553.60	K	Measurement of critical properties for binary and ternary mixtures containing potential gasoline additive diethyl carbonate (DEC)
tc	554.10	K	Measurement of critical temperatures and critical pressures for binary mixtures of methyl tert-butyl ether (MTBE) + alcohol and MTBE + alkane
tc	553.61	K	Experimental determination of critical data of multi-component mixtures containing potential gasoline additives 2-butanol by a flow-type apparatus
tc	553.60	K	Gas-Liquid Critical Temperatures of Some Alkenes, Amines, and Cyclic Hydrocarbons
tc	553.80 ± 0.20	K	NIST Webbook
tc	553.90 ± 0.40	K	NIST Webbook
tc	553.70 ± 0.60	K	NIST Webbook
tc	553.40	K	NIST Webbook
tc	553.20 ± 0.60	K	NIST Webbook
tc	553.00 ± 0.30	K	NIST Webbook
tc	555.10 ± 0.50	K	NIST Webbook
tc	553.40 ± 0.60	K	NIST Webbook
tc	554.20 ± 1.00	K	NIST Webbook
tc	553.35 ± 0.10	K	NIST Webbook
tc	553.40 ± 0.60	K	NIST Webbook
tc	553.45 ± 0.15	K	NIST Webbook
tc	554.15 ± 1.50	K	NIST Webbook
tc	553.40 ± 0.60	K	NIST Webbook
tc	553.90 ± 0.20	K	NIST Webbook
tc	552.97 ± 0.10	K	NIST Webbook
tf	279.62 ± 0.20	K	NIST Webbook
tf	279.55 ± 0.20	K	NIST Webbook

tf	279.55 ± 0.40	K	NIST Webbook
tf	277.70 ± 1.00	K	NIST Webbook
tf	279.55 ± 0.20	K	NIST Webbook
tf	279.40 ± 0.60	K	NIST Webbook
tf	278.65 ± 0.20	K	NIST Webbook
tf	279.35 ± 0.50	K	NIST Webbook
tf	279.15 ± 0.50	K	NIST Webbook
tf	279.40 ± 1.00	K	NIST Webbook
tf	279.00 ± 1.50	K	NIST Webbook
tf	279.55 ± 0.10	K	NIST Webbook
tf	277.15 ± 1.00	K	NIST Webbook
tf	266.75 ± 1.50	K	NIST Webbook
tf	279.55 ± 0.20	K	NIST Webbook
tf	279.55 ± 0.20	K	NIST Webbook
tf	279.65 ± 0.10	K	NIST Webbook
tf	279.51 ± 0.06	K	NIST Webbook
tf	279.30 ± 0.80	K	NIST Webbook
tf	279.69 ± 0.01	K	NIST Webbook
tf	279.50 ± 0.07	K	NIST Webbook
tf	279.57 ± 0.06	K	NIST Webbook
tf	279.55 ± 0.20	K	NIST Webbook
tf	279.65 ± 0.50	K	NIST Webbook
tf	279.65 ± 0.30	K	NIST Webbook
tf	279.65 ± 0.10	K	NIST Webbook
tf	279.70 ± 0.30	K	NIST Webbook
tf	279.70 ± 0.20	K	NIST Webbook
tf	279.22 ± 0.10	K	NIST Webbook
tf	279.69 ± 0.10	K	NIST Webbook
tf	279.55 ± 0.50	K	NIST Webbook
tf	279.75 ± 0.30	K	NIST Webbook
tf	279.58 ± 0.10	K	NIST Webbook
tf	279.70 ± 0.03	K	NIST Webbook
tf	279.72 ± 0.04	K	NIST Webbook
tf	279.96	K	Aqueous Solubility Prediction Method
tf	279.70	K	KDB
tf	280.10	K	Phase diagrams of binary systems containing n-alkanes, or cyclohexane, or 1-alkanols and 2,3-pentanedione at atmospheric and high pressure
tf	279.73 ± 0.15	K	NIST Webbook
tf	280.69 ± 0.05	K	NIST Webbook
tf	279.70 ± 0.05	K	NIST Webbook
tf	279.60 ± 2.00	K	NIST Webbook

tf	278.70 ± 2.77	K	NIST Webbook
tf	277.90 ± 0.60	K	NIST Webbook
tf	279.87 ± 0.01	K	NIST Webbook
tf	279.73 ± 0.01	K	NIST Webbook
tf	279.74 ± 0.08	K	NIST Webbook
tf	279.66 ± 0.10	K	NIST Webbook
tf	280.00	K	Determination of thermophysical properties of cyclopentane hydrate using a stirred calorimetric cell
tf	280.15 ± 1.00	K	NIST Webbook
tf	279.96	K	Solid-Liquid Equilibria for Binary Organic Systems Containing 1-Methoxy-2-propanol and 2-Butoxy Ethanol
tf	279.95	K	Liquid-Liquid-Solid Equilibria in the Ternary System Water-Phosphoric Acid-Cyclohexane at 25 and 35 deg.C: Stability Domain of Hemihydrate and Anhydrous Phosphoric Acid
tf	279.74 ± 0.02	K	NIST Webbook
tt	279.90 ± 3.00	K	NIST Webbook
tt	279.30 ± 0.20	K	NIST Webbook
tt	279.78 ± 0.06	K	NIST Webbook
tt	279.40 ± 0.20	K	NIST Webbook
tt	279.82 ± 0.05	K	NIST Webbook
tt	279.83	K	KDB
tt	279.84 ± 0.02	K	NIST Webbook
tt	279.70 ± 0.10	K	NIST Webbook
tt	279.83 ± 0.02	K	NIST Webbook
tt	186.18	K	Development of a certified reference material for calibration of DSC and DTA below room temperature: NMIJ CRM 5401-a, Cyclohexane for Thermal Analysis
vc	0.308	m3/kmol	KDB
vc	0.309 ± 0.003	m3/kmol	NIST Webbook
vc	0.308	m3/kmol	NIST Webbook
volm	1.09e-04	m3/mol	Excess Gibbs energies and volumes of the ternary system chloroform + tetrahydrofuran + cyclohexane at 298.15 K
volm	1.09e-04	m3/mol	Thermodynamic study of (perfluoroalkane + alkane) mixtures: Excess and solvation enthalpies

volm	1.09e-04	m3/mol	Excess Gibbs Energies of the Ternary System 2-Methoxyethanol + Tetrahydrofuran + Cyclohexane and Other Relevant Binaries at 298.15 K
zc	0.2729110		KDB
zra	0.27		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	206.30 ± 2.10	J/mol×K	544.00	NIST Webbook
cpg	196.70 ± 2.10	J/mol×K	521.00	NIST Webbook
cpg	189.50 ± 2.10	J/mol×K	495.00	NIST Webbook
cpg	174.50 ± 1.70	J/mol×K	460.00	NIST Webbook
cpg	161.80 ± 1.70	J/mol×K	428.00	NIST Webbook
cpg	153.97	J/mol×K	410.00	NIST Webbook
cpg	146.44	J/mol×K	390.00	NIST Webbook
cpg	143.10 ± 1.30	J/mol×K	384.00	NIST Webbook
cpg	138.07	J/mol×K	370.00	NIST Webbook
cpl	157.06	J/mol×K	298.15	NIST Webbook
cpl	156.00	J/mol×K	298.15	NIST Webbook
cpl	156.70	J/mol×K	298.00	NIST Webbook
cpl	156.40	J/mol×K	298.15	NIST Webbook
cpl	154.81	J/mol×K	293.15	NIST Webbook
cpl	155.96	J/mol×K	298.15	NIST Webbook
cpl	156.50	J/mol×K	298.15	NIST Webbook
cpl	155.85	J/mol×K	298.15	NIST Webbook
cpl	156.12	J/mol×K	298.15	NIST Webbook
cpl	155.13	J/mol×K	293.15	NIST Webbook
cpl	154.32	J/mol×K	298.15	NIST Webbook
cpl	155.96	J/mol×K	298.15	NIST Webbook
cpl	143.90	J/mol×K	326.50	NIST Webbook
cpl	156.90	J/mol×K	298.15	NIST Webbook
cpl	156.00	J/mol×K	298.15	NIST Webbook
cpl	158.95	J/mol×K	303.15	Excess Heat Capacities of Binary and Ternary Mixtures Containing 1-Ethyl-3-methylimidazolium Tetrafluoroborate and Anilines

cpl	156.20	J/mol×K	298.15	Excess Heat Capacities of Binary and Ternary Mixtures Containing 1-Ethyl-3-methylimidazolium Tetrafluoroborate and Anilines
cpl	153.75	J/mol×K	293.15	Excess Heat Capacities of Binary and Ternary Mixtures Containing 1-Ethyl-3-methylimidazolium Tetrafluoroborate and Anilines
cpl	156.07	J/mol×K	298.15	NIST Webbook
cpl	156.07	J/mol×K	298.15	NIST Webbook
cpl	156.20	J/mol×K	298.15	NIST Webbook
cpl	159.60	J/mol×K	298.15	NIST Webbook
cpl	155.20	J/mol×K	298.15	NIST Webbook
cpl	155.50	J/mol×K	298.00	NIST Webbook
cpl	152.93	J/mol×K	298.00	NIST Webbook
cpl	155.31	J/mol×K	298.00	NIST Webbook
cpl	143.90	J/mol×K	298.90	NIST Webbook
cpl	155.20	J/mol×K	311.00	NIST Webbook
cpl	154.20	J/mol×K	300.00	NIST Webbook
cpl	155.85	J/mol×K	295.00	NIST Webbook
cpl	156.31	J/mol×K	298.15	NIST Webbook
cpl	100.40	J/mol×K	304.20	NIST Webbook
cpl	176.10	J/mol×K	298.00	NIST Webbook
cpl	156.15	J/mol×K	298.15	NIST Webbook
cpl	156.12	J/mol×K	298.15	NIST Webbook
cpl	156.40	J/mol×K	298.15	NIST Webbook
cpl	154.80	J/mol×K	293.15	NIST Webbook
cpl	156.35	J/mol×K	298.15	NIST Webbook
dvisc	0.0009027	Pa×s	298.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures

dvisc	0.0005980	Pa×s	323.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure
dvisc	0.0005200	Pa×s	333.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure
dvisc	0.0006960	Pa×s	313.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure
dvisc	0.0008210	Pa×s	303.15	Thermodynamic properties of binary mixtures of N-methyl-2-pyrrolidinone with cyclohexane, benzene, toluene at (303.15 to 353.15) K and atmospheric pressure
dvisc	0.0008870	Pa×s	298.15	Dynamic viscosities of binary mixtures of cycloalkanes with primary alcohols at T = (293.15, 298.15, and 303.15) K: New UNIFAC-VISCO interaction parameters

dvisc	0.0008160	Pa×s	303.15	Dynamic viscosities of binary mixtures of cycloalkanes with primary alcohols at T = (293.15, 298.15, and 303.15) K: New UNIFAC-VISCO interaction parameters
dvisc	0.0009040	Pa×s	298.15	Densities, viscosities, and excess properties of (N-methylmorpholine + cyclohexane, + benzene, and + toluene) at T = (298.15, 303.15, 313.15, 323.15) K
dvisc	0.0008090	Pa×s	303.15	Densities, viscosities, and excess properties of (N-methylmorpholine + cyclohexane, + benzene, and + toluene) at T = (298.15, 303.15, 313.15, 323.15) K
dvisc	0.0006980	Pa×s	313.15	Densities, viscosities, and excess properties of (N-methylmorpholine + cyclohexane, + benzene, and + toluene) at T = (298.15, 303.15, 313.15, 323.15) K
dvisc	0.0009680	Pa×s	293.15	Dynamic viscosities of binary mixtures of cycloalkanes with primary alcohols at T = (293.15, 298.15, and 303.15) K: New UNIFAC-VISCO interaction parameters

dvisc	0.0006040	Pa×s	323.15	Densities, viscosities, and excess properties of (N-methylmorpholine + cyclohexane, + benzene, and + toluene) at T = (298.15, 303.15, 313.15, 323.15) K
dvisc	0.0008980	Pa×s	298.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for CmH2m+1(OCH2CH2)nOH (m) 1 or 2 or 4 andn) 1) + Benzene, + Toluene, + (o-, m-, and p-) Xylenes, + Ethylbenzene, and + Cyclohexane
dvisc	0.0007490	Pa×s	308.15	Densities, Excess Molar Volumes, Viscosities, Speeds of Sound, Excess Isentropic Compressibilities, and Relative Permittivities for CmH2m+1(OCH2CH2)nOH (m) 1 or 2 or 4 andn) 1) + Benzene, + Toluene, + (o-, m-, and p-) Xylenes, + Ethylbenzene, and + Cyclohexane
dvisc	0.0008945	Pa×s	298.15	Thermophysical Properties of Binary Mixtures of Cyclohexane + Nitrobenzene, Cyclohexanone + Nitrobenzene, and Cyclohexane + Cyclohexanone at (298.15, 303.15, and 308.15) K

dvisc	0.0007637	Pa×s	308.15	Thermophysical Properties of Binary Mixtures of Cyclohexane + Nitrobenzene, Cyclohexanone + Nitrobenzene, and Cyclohexane + Cyclohexanone at (298.15, 303.15, and 308.15) K
dvisc	0.0008205	Pa×s	303.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0006963	Pa×s	313.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0008284	Pa×s	303.15	Thermophysical Properties of Binary Mixtures of Cyclohexane + Nitrobenzene, Cyclohexanone + Nitrobenzene, and Cyclohexane + Cyclohexanone at (298.15, 303.15, and 308.15) K
dvisc	0.0005984	Pa×s	323.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0005195	Pa×s	333.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures

dvisc	0.0009680	Pa×s	293.15	Dynamic Viscosities of the Binary Systems Cyclohexane and Cyclopentane with Acetone, Butanone, or 2-Pentanone at Three Temperatures T) (293.15, 298.15, and 303.15) K
dvisc	0.0008870	Pa×s	298.15	Dynamic Viscosities of the Binary Systems Cyclohexane and Cyclopentane with Acetone, Butanone, or 2-Pentanone at Three Temperatures T) (293.15, 298.15, and 303.15) K
dvisc	0.0008160	Pa×s	303.15	Dynamic Viscosities of the Binary Systems Cyclohexane and Cyclopentane with Acetone, Butanone, or 2-Pentanone at Three Temperatures T) (293.15, 298.15, and 303.15) K
dvisc	0.0009680	Pa×s	293.15	Viscosities, Densities, and Speed of Sound of the Cycloalkanes with Secondary Alcohols at T = (293.15, 298.15, and 303.15) K: New UNIFAC-VISCO Interaction Parameters
dvisc	0.0008870	Pa×s	298.15	Viscosities, Densities, and Speed of Sound of the Cycloalkanes with Secondary Alcohols at T = (293.15, 298.15, and 303.15) K: New UNIFAC-VISCO Interaction Parameters

dvisc	0.0008160	Pa×s	303.15	Viscosities, Densities, and Speed of Sound of the Cycloalkanes with Secondary Alcohols at T = (293.15, 298.15, and 303.15) K: New UNIFAC-VISCO Interaction Parameters	
dvisc	0.0010770	Pa×s	288.15	Densities and Viscosities of Binary Mixtures of Tri-n-butyl Phosphate + Cyclohexane, + n-Heptane at T) (288.15, 293.15, 298.15, 303.15, and 308.15) K	
dvisc	0.0009840	Pa×s	293.15	Densities and Viscosities of Binary Mixtures of Tri-n-butyl Phosphate + Cyclohexane, + n-Heptane at T) (288.15, 293.15, 298.15, 303.15, and 308.15) K	
dvisc	0.0009030	Pa×s	298.15	Densities and Viscosities of Binary Mixtures of Tri-n-butyl Phosphate + Cyclohexane, + n-Heptane at T) (288.15, 293.15, 298.15, 303.15, and 308.15) K	
dvisc	0.0008300	Pa×s	303.15	Densities and Viscosities of Binary Mixtures of Tri-n-butyl Phosphate + Cyclohexane, + n-Heptane at T) (288.15, 293.15, 298.15, 303.15, and 308.15) K	
dvisc	0.0007640	Pa×s	308.15	Densities and Viscosities of Binary Mixtures of Tri-n-butyl Phosphate + Cyclohexane, + n-Heptane at T) (288.15, 293.15, 298.15, 303.15, and 308.15) K	

dvisc	0.0009840	Pa×s	293.15	Densities and Viscosities of Binary Mixtures of Tris(2-ethylhexyl) Phosphate + Cyclohexane or n-Hexane at T) (293.15, 298.15, and 303.15) K and p) 0.1 MPa	
dvisc	0.0009030	Pa×s	298.15	Densities and Viscosities of Binary Mixtures of Tris(2-ethylhexyl) Phosphate + Cyclohexane or n-Hexane at T) (293.15, 298.15, and 303.15) K and p) 0.1 MPa	
dvisc	0.0008300	Pa×s	303.15	Densities and Viscosities of Binary Mixtures of Tris(2-ethylhexyl) Phosphate + Cyclohexane or n-Hexane at T) (293.15, 298.15, and 303.15) K and p) 0.1 MPa	
dvisc	0.0011802	Pa×s	283.15	Density and Viscosity of Decalin, Cyclohexane, and Toluene Binary Mixtures at (283.15, 293.15, 303.15, 313.15, and 323.15) K	
dvisc	0.0009847	Pa×s	293.15	Density and Viscosity of Decalin, Cyclohexane, and Toluene Binary Mixtures at (283.15, 293.15, 303.15, 313.15, and 323.15) K	
dvisc	0.0008295	Pa×s	303.15	Density and Viscosity of Decalin, Cyclohexane, and Toluene Binary Mixtures at (283.15, 293.15, 303.15, 313.15, and 323.15) K	

dvisc	0.0007061	Pa×s	313.15	Density and Viscosity of Decalin, Cyclohexane, and Toluene Binary Mixtures at (283.15, 293.15, 303.15, 313.15, and 323.15) K	
dvisc	0.0005978	Pa×s	323.15	Density and Viscosity of Decalin, Cyclohexane, and Toluene Binary Mixtures at (283.15, 293.15, 303.15, 313.15, and 323.15) K	
dvisc	0.0007720	Pa×s	308.15	Density, Viscosity, and Speed of Sound of (Methyl Benzoate + Cyclohexane), (Methyl Benzoate + n-Hexane), (Methyl Benzoate + Heptane), and (Methyl Benzoate + Octane) at Temperatures of (303.15, 308.15, and 313.15) K	
dvisc	0.0006850	Pa×s	313.15	Density, Viscosity, and Speed of Sound of (Methyl Benzoate + Cyclohexane), (Methyl Benzoate + n-Hexane), (Methyl Benzoate + Heptane), and (Methyl Benzoate + Octane) at Temperatures of (303.15, 308.15, and 313.15) K	
dvisc	0.0008230	Pa×s	303.15	Density, Viscosity, and Speed of Sound of (Methyl Benzoate + Cyclohexane), (Methyl Benzoate + n-Hexane), (Methyl Benzoate + Heptane), and (Methyl Benzoate + Octane) at Temperatures of (303.15, 308.15, and 313.15) K	

hfust	2.68	kJ/mol	279.80	NIST Webbook
hfust	6.74	kJ/mol	186.10	NIST Webbook
hfust	2.68	kJ/mol	279.80	NIST Webbook
hsubt	46.60	kJ/mol	186.00	NIST Webbook
hsubt	36.50	kJ/mol	274.00	NIST Webbook
hsubt	37.70	kJ/mol	248.00	NIST Webbook
hsubt	27.60	kJ/mol	251.50	NIST Webbook
hsubt	37.20	kJ/mol	273.00	NIST Webbook
hvapt	30.30	kJ/mol	345.00	NIST Webbook
hvapt	32.90	kJ/mol	323.00	NIST Webbook
hvapt	31.40 ± 0.10	kJ/mol	324.00	NIST Webbook
hvapt	29.96	kJ/mol	353.90	KDB
hvapt	32.83	kJ/mol	298.00	Enthalpies of Vaporization and Vapor Pressures of Some Deuterated Hydrocarbons. Liquid-Vapor Pressure Isotope Effects
hvapt	29.97	kJ/mol	353.90	NIST Webbook
hvapt	33.33	kJ/mol	298.15	NIST Webbook
hvapt	33.10	kJ/mol	324.50	NIST Webbook
hvapt	32.70	kJ/mol	322.50	NIST Webbook
hvapt	31.90	kJ/mol	324.50	NIST Webbook
hvapt	32.20	kJ/mol	415.00	NIST Webbook
hvapt	32.30	kJ/mol	314.00	NIST Webbook
hvapt	31.10	kJ/mol	332.00	NIST Webbook
hvapt	30.40 ± 0.10	kJ/mol	346.00	NIST Webbook
hvapt	30.00	kJ/mol	355.00	NIST Webbook
hvapt	30.90	kJ/mol	383.50	NIST Webbook
hvapt	29.60	kJ/mol	451.50	NIST Webbook
hvapt	29.60	kJ/mol	521.00	NIST Webbook
hvapt	32.30 ± 0.10	kJ/mol	313.00	NIST Webbook
hvapt	32.80	kJ/mol	335.00	NIST Webbook
hvapt	31.20 ± 0.10	kJ/mol	333.00	NIST Webbook
hvapt	31.00 ± 0.10	kJ/mol	338.00	NIST Webbook
hvapt	30.40 ± 0.10	kJ/mol	348.00	NIST Webbook
hvapt	30.10 ± 0.10	kJ/mol	353.00	NIST Webbook
hvapt	32.20 ± 0.10	kJ/mol	313.00	NIST Webbook
hvapt	31.90 ± 0.10	kJ/mol	323.00	NIST Webbook
hvapt	31.10 ± 0.10	kJ/mol	333.00	NIST Webbook
hvapt	30.60 ± 0.10	kJ/mol	343.00	NIST Webbook
hvapt	30.10 ± 0.10	kJ/mol	354.00	NIST Webbook
hvapt	32.50	kJ/mol	323.00	NIST Webbook
hvapt	30.10	kJ/mol	354.00	NIST Webbook

hvapt	32.90	kJ/mol	324.00	NIST Webbook
pvap	12.15	kPa	297.08	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	101.33	kPa	353.85	Vapor Liquid Equilibrium Data for Binary Systems of N,N-Dimethylacetamide with Cyclohexene, Cyclohexane, and Benzene Separately at Atmospheric Pressure
pvap	16.40	kPa	303.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
pvap	24.70	kPa	313.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
pvap	36.40	kPa	323.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K

pvap	52.00	kPa	333.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
pvap	72.50	kPa	343.15	Bubble Pressure Measurement and Prediction for n-Hexadecane and n-Eicosane + Cyclohexane, Methylcyclohexane, and Ethylcyclohexane Binary Mixtures from 303.15 to 393.15 K
pvap	101.30	kPa	353.82	A New Test System for Distillation Efficiency Experiments at Elevated Liquid Viscosities: Vapor-Liquid Equilibrium and Liquid Viscosity Data for Cyclopentanol + Cyclohexanol
pvap	16.06	kPa	302.92	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	16.95	kPa	304.19	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	19.05	kPa	306.91	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	20.16	kPa	308.27	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	21.56	kPa	309.90	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water

pvap	24.61	kPa	313.16	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	30.03	kPa	318.19	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	36.23	kPa	323.14	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	43.51	kPa	328.16	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	49.68	kPa	331.90	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	51.90	kPa	333.16	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	51.90	kPa	333.17	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	61.56	kPa	338.16	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	72.53	kPa	343.16	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
pvap	101.30	kPa	353.82	A new analysis method for improving collection of vapor-liquid equilibrium (VLE) data of binary mixtures using differential scanning calorimetry (DSC)
pvap	84.73	kPa	348.05	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water

pvap	19.80	kPa	308.15	VLE and LLE Data for the System Cyclohexane + Cyclohexene + Water + Cyclohexanol
pvap	29.70	kPa	318.30	VLE and LLE Data for the System Cyclohexane + Cyclohexene + Water + Cyclohexanol
pvap	39.70	kPa	325.95	VLE and LLE Data for the System Cyclohexane + Cyclohexene + Water + Cyclohexanol
pvap	49.70	kPa	332.10	VLE and LLE Data for the System Cyclohexane + Cyclohexene + Water + Cyclohexanol
pvap	59.70	kPa	337.45	VLE and LLE Data for the System Cyclohexane + Cyclohexene + Water + Cyclohexanol
pvap	69.80	kPa	342.05	VLE and LLE Data for the System Cyclohexane + Cyclohexene + Water + Cyclohexanol
pvap	79.90	kPa	346.25	VLE and LLE Data for the System Cyclohexane + Cyclohexene + Water + Cyclohexanol
pvap	90.05	kPa	350.00	VLE and LLE Data for the System Cyclohexane + Cyclohexene + Water + Cyclohexanol

pvap	101.75	kPa	354.05	VLE and LLE Data for the System Cyclohexane + Cyclohexene + Water + Cyclohexanol
pvap	2.08	kPa	263.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	3.73	kPa	273.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	6.36	kPa	283.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	10.37	kPa	293.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)

pvap	13.04	kPa	298.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	16.26	kPa	303.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	24.65	kPa	313.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	36.24	kPa	323.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)
pvap	51.85	kPa	333.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)

pvap	72.39	kPa	343.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)	
pvap	98.85	kPa	353.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)	
pvap	132.33	kPa	363.15	Isothermal Vapor-Liquid Equilibria and Excess Enthalpies of (Propyl Ethanoate + Heptane), (Propyl Ethanoate + Cyclohexane), and (Propyl Ethanoate + 1-Hexene)	
pvap	362.80	kPa	403.15	Isothermal Vapor-Liquid Equilibrium for Methanol and 2,3-Dimethyl-1-butene at 343.06 K, 353.27 K, 363.19 K, and 372.90 K	
pvap	20.00	kPa	308.07	Isobaric Vapor Liquid Equilibrium for Binary Systems of Toluene + Acrylic Acid, Toluene + Acetic Acid, and Cyclohexane + Acrylic Acid at 20 kPa	

pvap	24.63	kPa	313.15	Vapor-Liquid Equilibria of Binary Mixtures Containing 1-Butanol and Hydrocarbons at 313.15 K	
pvap	24.62	kPa	313.15	Vapor Liquid Equilibria of Binary Mixtures Containing 2-Butanol and Hydrocarbons at 313.15 K	
pvap	29.77	kPa	317.95	Determination and Prediction of Vapor Liquid Equilibria for a System Containing Water + Butyl Acetate + Cyclohexane + Ethanol	
pvap	58.85	kPa	336.85	Determination and Prediction of Vapor Liquid Equilibria for a System Containing Water + Butyl Acetate + Cyclohexane + Ethanol	
pvap	87.65	kPa	349.15	Determination and Prediction of Vapor Liquid Equilibria for a System Containing Water + Butyl Acetate + Cyclohexane + Ethanol	
pvap	11.15	kPa	295.42	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	11.16	kPa	295.45	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	11.17	kPa	295.46	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	

pvap	11.33	kPa	295.72	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	11.35	kPa	295.75	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	11.63	kPa	296.22	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	101.30	kPa	353.94	Isobaric vapor-liquid equilibrium of three binary systems containing dimethyl succinate, dimethyl glutarate and dimethyl adipate at 2, 5.2 and 8.3 kPa
pvap	12.16	kPa	297.13	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	12.17	kPa	297.13	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	12.61	kPa	297.86	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	12.71	kPa	297.99	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	13.23	kPa	298.83	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	13.80	kPa	299.75	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	13.81	kPa	299.77	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	14.52	kPa	300.85	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	15.71	kPa	302.63	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	16.03	kPa	303.02	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	16.11	kPa	303.15	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	17.04	kPa	304.38	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	17.05	kPa	304.40	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	17.07	kPa	304.42	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	18.33	kPa	306.05	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	18.60	kPa	306.40	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	19.40	kPa	307.45	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	19.91	kPa	308.06	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	21.12	kPa	309.50	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	22.47	kPa	310.98	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	23.89	kPa	312.48	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	24.56	kPa	313.15	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	25.25	kPa	313.84	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	26.47	kPa	315.01	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	26.67	kPa	315.26	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	27.88	kPa	316.32	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	29.23	kPa	317.51	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	30.09	kPa	318.31	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	30.56	kPa	318.67	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	31.93	kPa	319.81	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	33.27	kPa	320.87	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	34.59	kPa	321.91	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	34.69	kPa	321.99	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	35.95	kPa	322.94	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	36.27	kPa	323.15	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	

pvap	36.59	kPa	323.44	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	37.23	kPa	323.88	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	37.33	kPa	323.95	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	38.56	kPa	324.83	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	132.35	kPa	363.15	Excess properties and vapour pressure of 2-diethylaminoethylamine + cyclohexane
pvap	41.25	kPa	326.68	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	42.68	kPa	327.61	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	43.97	kPa	328.43	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	45.40	kPa	329.32	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	45.43	kPa	329.35	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	46.59	kPa	330.05	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	48.07	kPa	330.94	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	49.32	kPa	331.68	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	49.89	kPa	332.02	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	50.60	kPa	332.41	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	51.87	kPa	333.11	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	51.92	kPa	333.15	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	53.15	kPa	333.83	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	53.19	kPa	333.86	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	54.47	kPa	334.53	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	55.85	kPa	335.26	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	56.56	kPa	335.64	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	57.19	kPa	335.95	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	58.63	kPa	336.70	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	59.96	kPa	337.36	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	61.39	kPa	338.06	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	61.40	kPa	338.06	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	62.63	kPa	338.65	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	62.64	kPa	338.67	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	63.95	kPa	339.29	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	65.29	kPa	339.92	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	66.63	kPa	340.54	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	67.95	kPa	341.12	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	69.29	kPa	341.72	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	70.65	kPa	342.32	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	71.93	kPa	342.88	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	72.60	kPa	343.15	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	73.25	kPa	343.43	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	74.73	kPa	344.05	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	75.96	kPa	344.55	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	77.27	kPa	345.08	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	78.76	kPa	345.69	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	80.00	kPa	346.18	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	81.25	kPa	346.67	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	82.56	kPa	347.18	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	82.57	kPa	347.18	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	83.89	kPa	347.69	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	85.23	kPa	348.19	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	86.49	kPa	348.65	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	87.93	kPa	349.19	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	89.43	kPa	349.72	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	90.64	kPa	350.18	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	90.87	kPa	350.25	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	92.07	kPa	350.67	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	93.27	kPa	351.10	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	94.63	kPa	351.57	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	95.92	kPa	352.01	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	97.23	kPa	352.45	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	98.57	kPa	352.90	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	99.31	kPa	353.15	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols

pvap	99.95	kPa	353.36	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols
pvap	98.87	kPa	353.15	Excess properties and vapour pressure of 2-diethylaminoethylamine + cyclohexane
pvap	72.39	kPa	343.15	Excess properties and vapour pressure of 2-diethylaminoethylamine + cyclohexane
pvap	51.85	kPa	333.15	Excess properties and vapour pressure of 2-diethylaminoethylamine + cyclohexane
pvap	36.24	kPa	323.15	Excess properties and vapour pressure of 2-diethylaminoethylamine + cyclohexane
pvap	24.65	kPa	313.15	Excess properties and vapour pressure of 2-diethylaminoethylamine + cyclohexane
pvap	16.26	kPa	303.15	Excess properties and vapour pressure of 2-diethylaminoethylamine + cyclohexane
pvap	13.04	kPa	298.15	Excess properties and vapour pressure of 2-diethylaminoethylamine + cyclohexane
pvap	10.36	kPa	293.15	Excess properties and vapour pressure of 2-diethylaminoethylamine + cyclohexane
pvap	6.35	kPa	283.15	Excess properties and vapour pressure of 2-diethylaminoethylamine + cyclohexane

pvap	3.73	kPa	273.15	Excess properties and vapour pressure of 2-diethylaminoethylamine + cyclohexane
pvap	132.35	kPa	363.15	Excess properties and vapour pressure of {3-diethylaminopropylamine + cyclohexane}
pvap	98.87	kPa	353.15	Excess properties and vapour pressure of {3-diethylaminopropylamine + cyclohexane}
pvap	72.40	kPa	343.15	Excess properties and vapour pressure of {3-diethylaminopropylamine + cyclohexane}
pvap	51.85	kPa	333.15	Excess properties and vapour pressure of {3-diethylaminopropylamine + cyclohexane}
pvap	36.24	kPa	323.15	Excess properties and vapour pressure of {3-diethylaminopropylamine + cyclohexane}
pvap	24.65	kPa	313.15	Excess properties and vapour pressure of {3-diethylaminopropylamine + cyclohexane}
pvap	16.26	kPa	303.15	Excess properties and vapour pressure of {3-diethylaminopropylamine + cyclohexane}
pvap	10.36	kPa	293.15	Excess properties and vapour pressure of {3-diethylaminopropylamine + cyclohexane}
pvap	6.35	kPa	283.15	Excess properties and vapour pressure of {3-diethylaminopropylamine + cyclohexane}

pvap	40.45	kPa	326.12	Vapor-Liquid Equilibria in Binary Systems Formed by Cyclohexane with Alcohols	
pvap	3.73	kPa	273.15	Excess properties and vapour pressure of {3-diethylaminopropylamine + cyclohexane}	
pvap	99.11	kPa	353.14	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	72.98	kPa	343.18	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	52.48	kPa	333.21	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	36.72	kPa	323.21	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	24.97	kPa	313.24	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	

pvap	16.45	kPa	303.27	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	13.17	kPa	298.25	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	10.42	kPa	293.27	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	8.20	kPa	288.28	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	6.39	kPa	283.32	Isothermal vapor-liquid equilibria and excess molar enthalpy of 2-methylpyrazine (2MP) containing binary mixtures. Comparison with DISQUAC predictions	
pvap	99.11	kPa	353.14	Isothermal vapour pressures and thermodynamic excess properties of 3,5- and 2,6-dimethylpyridine with cyclohexane. Measurements and prediction	

pvap	72.98	kPa	343.18	Isothermal vapour pressures and thermodynamic excess properties of 3,5- and 2,6-dimethylpyridine with cyclohexane. Measurements and prediction
pvap	52.48	kPa	333.21	Isothermal vapour pressures and thermodynamic excess properties of 3,5- and 2,6-dimethylpyridine with cyclohexane. Measurements and prediction
pvap	36.72	kPa	323.21	Isothermal vapour pressures and thermodynamic excess properties of 3,5- and 2,6-dimethylpyridine with cyclohexane. Measurements and prediction
pvap	24.97	kPa	313.24	Isothermal vapour pressures and thermodynamic excess properties of 3,5- and 2,6-dimethylpyridine with cyclohexane. Measurements and prediction
pvap	16.45	kPa	303.27	Isothermal vapour pressures and thermodynamic excess properties of 3,5- and 2,6-dimethylpyridine with cyclohexane. Measurements and prediction

pvap	13.17	kPa	298.25	Isothermal vapour pressures and thermodynamic excess properties of 3,5- and 2,6-dimethylpyridine with cyclohexane. Measurements and prediction
pvap	10.42	kPa	293.27	Isothermal vapour pressures and thermodynamic excess properties of 3,5- and 2,6-dimethylpyridine with cyclohexane. Measurements and prediction
pvap	8.20	kPa	288.28	Isothermal vapour pressures and thermodynamic excess properties of 3,5- and 2,6-dimethylpyridine with cyclohexane. Measurements and prediction
pvap	6.39	kPa	283.32	Isothermal vapour pressures and thermodynamic excess properties of 3,5- and 2,6-dimethylpyridine with cyclohexane. Measurements and prediction
pvap	84.70	kPa	348.15	Phase equilibria and excess molar enthalpies study of the binary systems (pyrrole + hydrocarbon, or an alcohol) and modeling
pvap	61.50	kPa	338.15	Phase equilibria and excess molar enthalpies study of the binary systems (pyrrole + hydrocarbon, or an alcohol) and modeling

pvap	101.30	kPa	353.70	Isobaric vapor-liquid equilibrium for the binary mixtures of nonane with cyclohexane, toluene, m-xylene, or p-xylene at 101.3 kPa
pvap	101.33	kPa	353.73	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	94.84	kPa	351.55	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	92.48	kPa	350.73	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	89.99	kPa	349.84	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	87.27	kPa	348.86	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa

pvap	85.03	kPa	348.01	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	82.52	kPa	347.06	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	79.92	kPa	346.07	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	77.54	kPa	345.11	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	75.07	kPa	344.09	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	74.96	kPa	344.05	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa

pvap	72.45	kPa	342.99	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	69.94	kPa	341.92	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	67.47	kPa	340.81	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	64.86	kPa	339.65	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	62.44	kPa	338.50	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	59.98	kPa	337.31	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa

pvap	57.44	kPa	335.99	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	54.76	kPa	334.60	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	52.43	kPa	333.33	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	49.92	kPa	331.94	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	47.45	kPa	330.44	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	44.91	kPa	328.90	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa

pvap	42.42	kPa	327.32	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	39.94	kPa	325.66	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	37.43	kPa	323.92	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	34.90	kPa	322.06	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	32.46	kPa	320.11	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	29.95	kPa	318.05	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa

pvap	27.43	kPa	315.76	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	24.95	kPa	313.40	Isobaric vapor liquid equilibrium for binary mixtures of 1-hexene + n-hexane and cyclohexane + cyclohexene at 30, 60 and 101.3 kPa
pvap	93.32	kPa	351.12	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	79.99	kPa	346.11	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	66.66	kPa	340.43	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	53.33	kPa	333.77	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components
pvap	40.00	kPa	325.65	Determination and correlation of vapor liquid equilibrium for binary systems consisting of close-boiling components

pvap	102.34	kPa	354.11	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	95.17	kPa	351.72	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	81.20	kPa	346.58	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	80.00	kPa	346.13	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	74.01	kPa	343.68	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	69.95	kPa	341.96	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	60.49	kPa	337.59	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa

pvap	53.30	kPa	333.96	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	50.00	kPa	332.08	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	38.28	kPa	324.73	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	38.19	kPa	324.72	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	101.30	kPa	353.73	Isobaric vapor liquid equilibria for binary systems of butyl chlorides with heptane, toluene and cyclohexane at 101.3, 80.0 and 53.3 kPa
pvap	77.94	kPa	345.42	Vapor-Liquid Equilibrium in a Ternary System Cyclohexane + Ethanol + Water
rfi	1.41516		313.15	Density, Speed of Sound, and Refractive Index for Binary Mixtures Containing Cycloalkanes with o-Xylene, m-Xylene, p-Xylene, and Mesitylene at T = (298.15 and 313.15) K

rfi	1.42350	298.15	Densities, Viscosities, and Refractive Indices of Mixtures of Hexane with Cyclohexane, Decane, Hexadecane, and Squalane at 298.15K
rfi	1.42050	308.15	Topological and thermodynamic investigations of molecular interactions in binary mixtures: Molar excess volumes and molar excess enthalpies
rfi	1.42350	298.15	Activity coefficients in binary mixtures formed by cyclohexanone with a variety of compounds at 94.7 kPa
rfi	1.42650	293.15	Vapour liquid equilibrium of carboxylic acid systems: Propionic acid + valeric acid and isobutyric acid + valeric acid
rfi	1.42350	298.15	Vapor liquid equilibrium for binary system of diethyl sulfide + cyclohexane at 353.15 and 343.15 K and diethyl sulfide + 2-ethoxy-2-methylpropane at 343.15 and 333.15 K
rfi	1.42378	298.15	Liquid liquid equilibria of lactam containing binary systems
rfi	1.42508	298.15	Vapor liquid equilibria and interfacial tensions for the ternary system acetone + 2,2 -oxybis[propane] + cyclohexane and its constituent binary systems

rfi	1.42508	298.15	Phase equilibria and interfacial tensions in the systems methyl tert-butyl ether + acetone + cyclohexane, methyl tert-butyl ether + acetone and methyl tert-butyl ether + cyclohexane
rfi	1.42350	298.15	Phase equilibria on four binary systems containing 3-methylthiophene
rfi	1.42630	293.20	Liquid phase equilibria for mixtures of (an aliphatic hydrocarbon + toluene + gamma-butyrolactone)
rfi	1.42360	298.15	Experimental data, correlation and prediction of the extraction of benzene from cyclic hydrocarbons using [Epy][ESO4] ionic liquid
rfi	1.42320	298.15	Azeotropic behaviour of (benzene + cyclohexane + chlorobenzene) ternary mixture using chlorobenzene as entrainer at 101.3 kPa
rfi	1.42633	293.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.42354	298.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures

rfi	1.42073	303.15	Mixing properties of binary mixtures presenting azeotropes at several temperatures
rfi	1.42403	298.15	(Liquid + liquid) equilibria of [C8mim][NTf2] ionic liquid with a sulfur-component and hydrocarbons
rfi	1.42360	298.15	Separation of toluene from cyclic hydrocarbons using 1-butyl-3-methylimidazolium methylsulfate ionic liquid at T = 298.15 K and atmospheric pressure
rfi	1.42360	298.15	(Liquid + liquid) equilibrium data for the ternary systems (cycloalkane + ethylbenzene + 1-ethyl-3-methylimidazolium ethylsulfate) at T = 298.15 K and atmospheric pressure
rfi	1.42356	298.15	Application of [HMim][NTf2], [HMim][TfO] and [BMim][TfO] ionic liquids on the extraction of toluene from alkanes: Effect of the anion and the alkyl chain length of the cation on the LLE
rfi	1.42350	293.15	Solubility Data for Roflumilast and Maraviroc in Various Solvents between T = (278.2-323.2) K
rfi	1.42350	298.15	Bubble Temperature Measurements on Binary Mixtures Formed by Cyclohexane at 94.7 kPa

rfi	1.42350	298.15	Bubble-Temperature Measurements on Some Binary Mixtures Formed by Tetrahydrofuran or Amyl Alcohol with Hydrocarbons, Chlorohydrocarbons, or Butanols at (94.6 or 95.8) kPa
rfi	1.42360	298.15	Solubility of -Carotene in Binary Solvents Formed by Some Hydrocarbons with Dibutyl Ether and 1,2-Dimethoxyethane
rfi	1.42360	298.15	Solubility of a-Carotene in Binary Solvents Formed by Some Hydrocarbons with tert-Butyl Methyl Ether and with tert-Amyl Methyl Ether
rfi	1.42690	293.20	Phase Equilibria for the Ternary Liquid Systems of (Water + Tetrahydrofurfuryl Alcohol + Cyclic Solvent) at 298.2 K
rfi	1.42360	298.15	Solubility of a-Carotene in Binary Solvents Formed by Some Hydrocarbons with 2,5,8-Trioxanonane, 2-Propanone, and Cyclohexanone
rfi	1.42660	293.15	Solubilities of Phosphorus-Containing Compounds in Selected Solvents
rfi	1.42354	298.15	KDB
rfi	1.42360	298.15	Liquid Extraction of Benzene from Its Mixtures Using 1-Ethyl-3-methylimidazolium Ethylsulfate as a Solvent

rfi	1.42590	293.15	Liquid-Liquid Equilibrium of (Water + Pentane-2,4-dione + Ethyl Ethanoate) and (Water + Pentane-2,4-dione + Cyclohexane) at (298.15 and 313.15) K
rfi	1.42360	298.15	Liquid Liquid Extraction of Aromatic Compounds from Cycloalkanes Using 1-Butyl-3-methylimidazolium Methylsulfate Ionic Liquid
rfi	1.42650	298.15	Vapor Liquid Equilibrium for Ternary and Binary Mixtures of Tetrahydrofuran, Cyclohexane, and 1,2-Propanediol at 101.3 kPa
rfi	1.42403	298.15	Liquid-Liquid Equilibria for Systems Composed by 1-Methyl-3-octylimidazolium Tetrafluoroborate Ionic Liquid, Thiophene, and n-Hexane or Cyclohexane
rfi	1.43193	283.15	Density, Speed of Sound, and Refractive Index of the Binary Systems Cyclohexane (1) or Methylcyclohexane (1) or Cyclo-octane (1) with Benzene (2), Toluene (2), and Ethylbenzene (2) at Two Temperatures

rfi	1.42360		298.15	Density, Speed of Sound, and Refractive Index of the Binary Systems Cyclohexane (1) or Methylcyclohexane (1) or Cyclo-octane (1) with Benzene (2), Toluene (2), and Ethylbenzene (2) at Two Temperatures
rfi	1.42360		298.15	Density, Speed of Sound, and Refractive Index for Binary Mixtures Containing Cycloalkanes with o-Xylene, m-Xylene, p-Xylene, and Mesitylene at T = (298.15 and 313.15) K
rhol	769.00	kg/m3	303.15	Thermophysical approach to understand the nature of molecular interactions and structural factor between methyl isobutyl ketone and organic solvents mixtures
rhol	774.00	kg/m3	298.15	Liquid-Liquid Equilibrium for 2,2,2-Trifluoroethanol + Ethanol + Cyclohexane from (288.15 to 308.15) K
rhol	773.80	kg/m3	298.15	Density, Speed of Sound, and Refractive Index for Binary Mixtures Containing Cycloalkanes and Aromatic Compounds at T = 313.15 K

rhol	748.70	kg/m3	323.15	Volumetric Behavior of the Binary Mixtures of Methyl Ethyl Ketone with n-Hexane, Cyclohexane, and Benzene at T) (303.15, 313.15, and 323.15) K
rhol	759.20	kg/m3	313.15	Volumetric Behavior of the Binary Mixtures of Methyl Ethyl Ketone with n-Hexane, Cyclohexane, and Benzene at T) (303.15, 313.15, and 323.15) K
rhol	768.90	kg/m3	303.15	Volumetric Behavior of the Binary Mixtures of Methyl Ethyl Ketone with n-Hexane, Cyclohexane, and Benzene at T) (303.15, 313.15, and 323.15) K
rhol	779.00	kg/m3	293.00	KDB
rhol	778.70	kg/m3	293.15	Densities and Kinematic Viscosities of One Quinary Regular Liquid System and Its Five Quaternary Sub-Systems at Temperatures (293.15 and 298.15) K
rhol	773.90	kg/m3	298.15	Densities and Kinematic Viscosities of One Quinary Regular Liquid System and Its Five Quaternary Sub-Systems at Temperatures (293.15 and 298.15) K

rhol	778.70	kg/m3	293.15	Densities and Kinematic Viscosities of a Quinary Regular Liquid System and Its Five Quaternary Subsystems at 293.15A K and 298.15A K
rhol	773.90	kg/m3	298.15	Densities and Kinematic Viscosities of a Quinary Regular Liquid System and Its Five Quaternary Subsystems at 293.15A K and 298.15A K
rhol	773.70	kg/m3	298.15	Fluid Phase Topology of Benzene + Cyclohexane + 1-Propanol at 101.3 kPa
rhol	773.65	kg/m3	298.15	Experimental and predicted vapour liquid equilibrium of 1,4-dioxane with cycloalkanes and benzene
rhol	773.88	kg/m3	298.10	Excess enthalpies of binary mixtures of 2-ethoxyethanol with four hydrocarbons at 298.15, 308.15, and 318.15K An experimental and theoretical study
rhol	773.86	kg/m3	298.15	Thermodynamic study of 1,1,2,2-tetrachloroethane + hydrocarbon mixtures I. Excess and solvation enthalpies
rhol	778.54	kg/m3	293.00	Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures 293.15-323.15K

rhol	769.13	kg/m3	303.00	Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures 293.15-323.15K
rhol	759.60	kg/m3	313.00	Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures 293.15-323.15K
rhol	749.94	kg/m3	323.00	Volumetric behavior of the binary systems benzene + cyclohexane and benzene + 2,2,4-trimethyl-pentane at temperatures 293.15-323.15K
rhol	774.00	kg/m3	298.15	Effect of Temperature on Phase Equilibrium of the Mixed-Solvent System of (2,2,2-Trifluoroethanol + Methanol + Cyclohexane)
rhol	759.41	kg/m3	313.15	Thermodynamic properties of cyclohexane methanol liquid mixture from shear viscosity measurements
rhol	754.60	kg/m3	318.15	Thermodynamic properties of cyclohexane methanol liquid mixture from shear viscosity measurements
rhol	749.76	kg/m3	323.15	Thermodynamic properties of cyclohexane methanol liquid mixture from shear viscosity measurements

rhol	776.11	kg/m3	298.15	Quaternary isothermal vapor-liquid equilibrium of the model biofuel 2-butanone + n-heptane + tetrahydrofuran + cyclohexane using Raman spectroscopic characterization
rhol	778.50	kg/m3	293.15	Partial molar volume of paracetamol in water, 0.1 M HCl and 0.154 M NaCl at T = (298.15, 303.15, 308.15 and 310.65) K and at 101.325 kPa
rhol	773.96	kg/m3	298.15	Thermodynamics of mixtures containing amines. XI. Liquid + liquid equilibria and molar excess enthalpies at 298.15 K for N-methylaniline + hydrocarbon systems. Characterization in terms of DISQUAC and ERAS models
rhol	773.86	kg/m3	298.15	Volumetric and acoustic properties of binary mixtures of tri-n-butyl phosphate with n-hexane, cyclohexane, and n-heptane from T = (298.15 to 323.15) K
rhol	769.12	kg/m3	303.15	Volumetric and acoustic properties of binary mixtures of tri-n-butyl phosphate with n-hexane, cyclohexane, and n-heptane from T = (298.15 to 323.15) K

rhol	764.35	kg/m3	308.15	Volumetric and acoustic properties of binary mixtures of tri-n-butyl phosphate with n-hexane, cyclohexane, and n-heptane from T = (298.15 to 323.15) K	
rhol	759.56	kg/m3	313.15	Volumetric and acoustic properties of binary mixtures of tri-n-butyl phosphate with n-hexane, cyclohexane, and n-heptane from T = (298.15 to 323.15) K	
rhol	754.74	kg/m3	318.15	Volumetric and acoustic properties of binary mixtures of tri-n-butyl phosphate with n-hexane, cyclohexane, and n-heptane from T = (298.15 to 323.15) K	
rhol	749.88	kg/m3	323.15	Volumetric and acoustic properties of binary mixtures of tri-n-butyl phosphate with n-hexane, cyclohexane, and n-heptane from T = (298.15 to 323.15) K	
rhol	778.41	kg/m3	293.15	Isothermal (vapour + liquid) equilibria for binary mixtures of diisopropyl ether with (methanol, or ethanol, or 1-butanol): Experimental data, correlations, and predictions	

rhol	773.88	kg/m3	298.15	Quaternary (liquid + liquid) equilibrium data for the extraction of toluene from alkanes using the ionic liquid [EMim][MSO4]
rhol	773.94	kg/m3	298.15	Excess molar volumes and excess isentropic compressibilities of binary and ternary mixtures of o-chlorotoluene with cyclic ether and amides or cyclohexane at different temperatures
rhol	769.21	kg/m3	303.15	Excess molar volumes and excess isentropic compressibilities of binary and ternary mixtures of o-chlorotoluene with cyclic ether and amides or cyclohexane at different temperatures
rhol	764.45	kg/m3	308.15	Excess molar volumes and excess isentropic compressibilities of binary and ternary mixtures of o-chlorotoluene with cyclic ether and amides or cyclohexane at different temperatures
rhol	773.50	kg/m3	298.15	Measurements and modeling of LLE and HE for (methanol + 2,4,4-trimethyl-1-pentene), and LLE for (water + methanol + 2,4,4-trimethyl-1-pentene)

rhol	773.87	kg/m3	298.15	Volumetric, acoustic, and refractometric properties of (thiophene + hexane/cyclohexane) solutions in the presence of some imidazolium based ionic liquids at T = 298.15 K
rhol	773.88	kg/m3	298.15	(Liquid + liquid) equilibrium of ternary and quaternary systems containing heptane, cyclohexane, toluene and the ionic liquid [EMim][N(CN)2]. Experimental data and correlation
rhol	779.00	kg/m3	293.15	Thermophysical approach to understand the nature of molecular interactions and structural factor between methyl isobutyl ketone and organic solvents mixtures
rhol	773.81	kg/m3	298.15	Volumetric investigation of the ternary system ethanol + dimethylformamide + cyclohexane at 298.15 K
rhol	760.00	kg/m3	313.15	Thermophysical approach to understand the nature of molecular interactions and structural factor between methyl isobutyl ketone and organic solvents mixtures

rhol	778.00	kg/m3	293.15	Thermophysical approach to understand the nature of molecular interactions and structural factor between methyl isobutyl ketone and organic solvents mixtures	
rhol	759.00	kg/m3	313.15	Thermophysical approach to understand the nature of molecular interactions and structural factor between methyl isobutyl ketone and organic solvents mixtures	
rhol	783.00	kg/m3	288.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume	
rhol	779.00	kg/m3	293.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume	
rhol	774.00	kg/m3	298.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume	
rhol	769.00	kg/m3	303.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume	

rhol	760.00	kg/m3	313.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume	
rhol	751.00	kg/m3	323.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume	
rhol	741.00	kg/m3	333.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume	
rhol	731.00	kg/m3	343.15	Effect of temperature on intermolecular interactions between the organic solvents: Insights from density and excess volume	
rhol	773.78	kg/m3	298.15	Densities, isobaric thermal compressibilities and derived thermodynamic properties of the binary systems of cyclohexane with allyl methacrylate, butyl methacrylate, methacrylic acid, and vinyl acetate at t = (298.15 and 308.15)K	

rhol	764.30	kg/m3	308.15	Densities, isobaric thermal compressibilities and derived thermodynamic properties of the binary systems of cyclohexane with allyl methacrylate, butyl methacrylate, methacrylic acid, and vinyl acetate at t = (298.15 and 308.15)K	
rhol	769.10	kg/m3	303.15	Studies of partial molar volumes of alkylamine in non-electrolyte solvents I. Alkylamines in hydrocarbons at 303.15 and 313.15K	
rhol	759.52	kg/m3	313.15	Studies of partial molar volumes of alkylamine in non-electrolyte solvents I. Alkylamines in hydrocarbons at 303.15 and 313.15K	
rhol	773.94	kg/m3	298.15	Topological and thermodynamic investigations of binary mixtures: Molar excess volumes, molar excess enthalpies and isentropic compressibility changes of mixing	
rhol	769.12	kg/m3	303.15	Volumetric and transport properties of ternary mixtures containing 1-propanol + ethyl ethanoate + cyclohexane or benzene at 303.15 K: Experimental data, correlation and prediction by ERAS model	

rhol	769.12	kg/m3	303.15	Volumetric and transport properties of ternary mixtures containing 1-alkanol + ethyl ethanoate + cyclohexane at 303.15 K: Experimental data, correlation and prediction by ERAS model	
rhol	773.94	kg/m3	298.15	Excess molar volumes and isentropic compressibilities changes of mixing of tetrahydropyran + benzene + cyclo or n-alkanes ternary mixtures at 308.15 K	
rhol	759.80	kg/m3	313.15	Excess Molar Volumes for Three and Four Component Mixtures Simulating the Binary Mixture (Cyclohexane+ Hexadecane)	
rhol	779.00	kg/m3	298.15	Liquid Liquid Equilibrium data for the ternary systems of Water, Isopropyl alcohol, and selected entrainers	
rhol	768.80	kg/m3	303.15	Densities and Dynamic Viscosities of Alicyclic Cyclohexane with Toluene, o-Xylene, and Mesitylene at T = (303.15 to 323.15) K and Atmospheric Pressure	

rhol	764.00	kg/m3	308.15	Densities and Dynamic Viscosities of Alicyclic Cyclohexane with Toluene, o-Xylene, and Mesitylene at T = (303.15 to 323.15) K and Atmospheric Pressure	
rhol	759.30	kg/m3	313.15	Densities and Dynamic Viscosities of Alicyclic Cyclohexane with Toluene, o-Xylene, and Mesitylene at T = (303.15 to 323.15) K and Atmospheric Pressure	
rhol	754.40	kg/m3	318.15	Densities and Dynamic Viscosities of Alicyclic Cyclohexane with Toluene, o-Xylene, and Mesitylene at T = (303.15 to 323.15) K and Atmospheric Pressure	
rhol	749.50	kg/m3	323.15	Densities and Dynamic Viscosities of Alicyclic Cyclohexane with Toluene, o-Xylene, and Mesitylene at T = (303.15 to 323.15) K and Atmospheric Pressure	
rhol	765.00	kg/m3	308.15	Total Pressure Phase Equilibrium Measurements for the Binary Systems of n-Pentane + Cyclohexane and 1-Hexene + 2-Propanol	

rhol	775.00	kg/m3	298.15	Isothermal Vapor-Liquid Equilibrium Data for the Binary Systems Consisting of 1,1,2,3,3,3-Hexafluoro-1-propene and Either Methylcyclohexane, Cyclohexane, n-Hexane, 2-Methyltetrahydrofuran, or 2,2,3,3,4,4,4-Heptafluoro-1-butanol
rhol	773.80	kg/m3	298.15	Viscosities of Dimethyl Carbonate or Diethyl Carbonate with Alkanes at Four Temperatures. New UNIFAC-VISCO Parameters
rhol	778.56	kg/m3	293.15	Excess Molar Enthalpies for Binary Mixtures of Ethanol + Acetone, + Octane, + Cyclohexane and 1-Propanol + Acetone, + Octane, + Heptane at 323.15
rhol	773.92	kg/m3	298.15	Excess Enthalpies of the Ternary Mixtures: Tetrahydrofuran + (Hexane or Cyclohexane) + Decane at 298.15K
rhol	773.98	kg/m3	298.15	Vapor-Liquid Equilibria and Excess Enthalpies for Binary Systems of Dimethoxymethane with Hydrocarbons
rhol	773.93	kg/m3	298.15	Viscosities and Excess Molar Volumes of the Ternary System Toluene (1) + Cyclohexane (2) + Pentane (3) at 298.15 K

rhol	778.20	kg/m3	293.10	Vapor-Liquid Equilibrium for Binary Systems of Cyclohexane + Cyclohexanone and + Cyclohexanol at Temperatures from (414.0 to 433.7) K
rhol	778.80	kg/m3	293.15	Densities, Excess Molar Volumes, Isothermal Compressibilities, and Isobaric Expansivities of Dimethyl Carbonate + Cyclohexane Systems at Temperatures from (293.15 to 313.15) K and Pressures from (0.1 to 40) MPa
rhol	773.90	kg/m3	298.15	Densities, Excess Molar Volumes, Isothermal Compressibilities, and Isobaric Expansivities of Dimethyl Carbonate + Cyclohexane Systems at Temperatures from (293.15 to 313.15) K and Pressures from (0.1 to 40) MPa
rhol	769.30	kg/m3	303.15	Densities, Excess Molar Volumes, Isothermal Compressibilities, and Isobaric Expansivities of Dimethyl Carbonate + Cyclohexane Systems at Temperatures from (293.15 to 313.15) K and Pressures from (0.1 to 40) MPa

rhol	764.50	kg/m3	308.15	Densities, Excess Molar Volumes, Isothermal Compressibilities, and Isobaric Expansivities of Dimethyl Carbonate + Cyclohexane Systems at Temperatures from (293.15 to 313.15) K and Pressures from (0.1 to 40) MPa
rhol	759.70	kg/m3	313.15	Densities, Excess Molar Volumes, Isothermal Compressibilities, and Isobaric Expansivities of Dimethyl Carbonate + Cyclohexane Systems at Temperatures from (293.15 to 313.15) K and Pressures from (0.1 to 40) MPa
rhol	773.85	kg/m3	298.20	Apparent and Partial Molar Volumes at Infinite Dilution and Solid Liquid Equilibria of Dibenzothiophene + Alkane Systems
rhol	778.71	kg/m3	293.15	Thermodynamics of Mixtures Containing Amines. XII. Volumetric and Speed of Sound Data at (293.15, 298.15, and 303.15) K for N-Methylaniline + Hydrocarbon Systems
rhol	774.02	kg/m3	298.15	Thermodynamics of Mixtures Containing Amines. XII. Volumetric and Speed of Sound Data at (293.15, 298.15, and 303.15) K for N-Methylaniline + Hydrocarbon Systems

rhol	769.30	kg/m3	303.15	Thermodynamics of Mixtures Containing Amines. XII. Volumetric and Speed of Sound Data at (293.15, 298.15, and 303.15) K for N-Methylaniline + Hydrocarbon Systems
rhol	778.51	kg/m3	293.15	Excess Molar Volume along with Viscosity and Refractive Index for Binary Systems of Tricyclo[5.2.1.0(2.6)]decane with Five Cycloalkanes
rhol	773.84	kg/m3	298.15	Excess Molar Volume along with Viscosity and Refractive Index for Binary Systems of Tricyclo[5.2.1.0(2.6)]decane with Five Cycloalkanes
rhol	769.11	kg/m3	303.15	Excess Molar Volume along with Viscosity and Refractive Index for Binary Systems of Tricyclo[5.2.1.0(2.6)]decane with Five Cycloalkanes
rhol	764.36	kg/m3	308.15	Excess Molar Volume along with Viscosity and Refractive Index for Binary Systems of Tricyclo[5.2.1.0(2.6)]decane with Five Cycloalkanes
rhol	759.57	kg/m3	313.15	Excess Molar Volume along with Viscosity and Refractive Index for Binary Systems of Tricyclo[5.2.1.0(2.6)]decane with Five Cycloalkanes

rhol	788.30	kg/m3	287.00	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	
rhol	763.70	kg/m3	305.90	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	
rhol	752.10	kg/m3	324.90	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	
rhol	731.80	kg/m3	351.00	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	
rhol	704.30	kg/m3	375.00	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	
rhol	686.70	kg/m3	394.80	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	
rhol	666.50	kg/m3	416.60	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	

rhol	646.20	kg/m3	431.90	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
rhol	620.20	kg/m3	452.40	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
rhol	595.50	kg/m3	475.10	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
rhol	573.50	kg/m3	488.40	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
rhol	546.30	kg/m3	504.40	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
rhol	527.50	kg/m3	513.90	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
rhol	510.30	kg/m3	522.60	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure

rhol	487.00	kg/m3	531.90	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	
rhol	454.50	kg/m3	543.00	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	
rhol	426.20	kg/m3	553.20	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	
rhol	365.60	kg/m3	561.70	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	
rhol	259.50	kg/m3	572.10	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	
rhol	187.00	kg/m3	584.20	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	
rhol	167.00	kg/m3	592.50	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure	

rhol	149.30	kg/m3	603.60	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
rhol	133.00	kg/m3	618.80	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
rhol	118.30	kg/m3	635.00	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
rhol	109.80	kg/m3	654.20	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
rhol	96.50	kg/m3	672.30	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
rhol	92.00	kg/m3	687.50	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
rhol	774.00	kg/m3	298.15	Liquid-Liquid Equilibrium of (Cyclohexane + 2,2,2-Trifluoroethanol) and (Cyclohexane + Methanol) from (278.15 to 318.15) K
rhol	773.92	kg/m3	298.15	Binary Liquid Liquid Equilibria of ?-Valerolactone with Some Hydrocarbons

rhol	89.90	kg/m3	698.50	Design of a Gamma Densitometer for Hydrocarbon Fuel at High Temperature and Supercritical Pressure
sdco	0.00	m2/s	328.13	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	328.15	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	308.16	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	308.17	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	318.22	Viscous Calibration Liquids for Self-diffusion Measurements
sdco	0.00	m2/s	318.25	Viscous Calibration Liquids for Self-diffusion Measurements
sfust	9.57	J/mol×K	279.80	NIST Webbook
sfust	36.20	J/mol×K	186.10	NIST Webbook
speedsl	1255.00	m/s	298.15	Thermodynamic and topological investigations of molecular interactions in binary and ternary mixtures containing 1-methyl pyrrolidin-2-one at T = 308.15 K
speedsl	1181.00	m/s	313.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K

speedsl	1253.90	m/s	298.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K	
speedsl	1133.70	m/s	323.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K	
speedsl	1229.30	m/s	303.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K	
speedsl	1205.10	m/s	308.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K	
speedsl	1254.40	m/s	298.15	Speeds of Sound and Isentropic Compressibilities for Binary Mixtures of a Cyclic Diether with a Cyclic Compound at Three Temperatures	

speedsl	1212.00	m/s	308.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene
speedsl	1254.00	m/s	298.15	Densities, Speeds of Sound, Excess Molar Volumes, and Excess Isentropic Compressibilities at T = (298.15 and 308.15) K for Methyl Methacrylate + 1-Alkanols (1-Butanol, 1-Pentanol, and 1-Heptanol) + Cyclohexane, + Benzene, + Toluene, + p-Xylene, and + Ethylbenzene
speedsl	1157.30	m/s	318.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K
speedsl	1327.80	m/s	283.15	Speeds of Sound and Isentropic Compressibilities for Binary Mixtures of a Cyclic Diether with a Cyclic Compound at Three Temperatures

speedsl	1181.10	m/s	313.15	Speeds of Sound and Isentropic Compressibilities for Binary Mixtures of a Cyclic Diether with a Cyclic Compound at Three Temperatures
speedsl	1279.00	m/s	293.15	Acoustic and Thermophysical Properties of Binary Liquid Mixtures of Primary Butanols with Hexane and Cyclohexane at 293.15 K
speedsl	1278.60	m/s	293.15	Temperature dependence of densities, speeds of sound, and derived properties of cyclohexylamine + cyclohexane or benzene in the range (293.15 to 323.15) K
speedsl	1133.73	m/s	323.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K
speedsl	1157.29	m/s	318.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K
speedsl	1181.03	m/s	313.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K

speedsl	1205.05	m/s	308.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K
speedsl	1229.34	m/s	303.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K
speedsl	1253.86	m/s	298.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K
speedsl	1278.55	m/s	293.15	Volumetric and Acoustic Properties of Binary Mixtures of Cyclohexane + Benzene and + Benzaldehyde at (293.15 to 323.15) K
speedsl	1212.00	m/s	308.15	Thermodynamic and topological investigations of molecular interactions in binary and ternary mixtures containing 1-methyl pyrrolidin-2-one at T = 308.15 K
srf	0.02	N/m	318.15	Interfacial Tensions of Imidazolium-Based Ionic Liquids with N-Alkanes and Cyclohexane
srf	0.02	N/m	318.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures

srf	0.02	N/m	323.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures
srf	0.03	N/m	293.20	KDB
srf	0.02	N/m	337.93	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.03	N/m	283.15	Thermophysical study of 1,4-dioxane with cycloalkane mixtures
srf	0.02	N/m	298.15	Thermophysical study of 1,4-dioxane with cycloalkane mixtures
srf	0.02	N/m	303.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures
srf	0.03	N/m	279.33	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.03	N/m	282.82	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.03	N/m	287.81	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	297.82	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	307.86	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	317.86	Surface Tension of Pure Liquids and Binary Liquid Mixtures
srf	0.02	N/m	327.88	Surface Tension of Pure Liquids and Binary Liquid Mixtures

srf	0.03	N/m	293.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	298.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	303.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	308.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	313.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	318.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.02	N/m	323.15	Surface Properties of Dilute Solutions of Alkanes in Benzyl Alcohol
srf	0.03	N/m	288.15	Interfacial Tensions of Imidazolium-Based Ionic Liquids with N-Alkanes and Cyclohexane
srf	0.02	N/m	298.15	Interfacial Tensions of Imidazolium-Based Ionic Liquids with N-Alkanes and Cyclohexane
srf	0.02	N/m	308.15	Interfacial Tensions of Imidazolium-Based Ionic Liquids with N-Alkanes and Cyclohexane
srf	0.02	N/m	313.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures

srf	0.02	N/m	328.15	Interfacial Tensions of Imidazolium-Based Ionic Liquids with N-Alkanes and Cyclohexane
srf	0.03	N/m	293.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures
srf	0.02	N/m	298.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures
srf	0.02	N/m	313.15	Thermophysical study of 1,4-dioxane with cycloalkane mixtures
srf	0.02	N/m	308.15	Surface Tension of Dilute Solutions of Alkanes in Cyclohexanol at Different Temperatures
svapt	111.80	J/mol×K	298.15	NIST Webbook
tcondl	0.12	W/m×K	300.84	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.11	W/m×K	318.82	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

tcondl	0.11	W/m×K	318.66	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.12	W/m×K	301.14	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.12	W/m×K	301.00	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.11	W/m×K	318.95	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	
tcondl	0.12	W/m×K	295.83	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons	

tcondl	0.12	W/m×K	295.70	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	295.53	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	281.15	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	281.00	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons
tcondl	0.12	W/m×K	280.83	Thermal Conductivity and Thermal Diffusivity of Twenty-Nine Liquids: Alkenes, Cyclic (Alkanes, Alkenes, Alkadienes, Aromatics), and Deuterated Hydrocarbons

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbp	312.78	K	24.08	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	318.96	K	30.70	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	325.07	K	38.72	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	330.32	K	46.85	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	335.01	K	55.20	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	338.21	K	61.52	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures

tbp	341.67	K	69.06	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	345.37	K	77.87	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	348.28	K	85.44	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	350.53	K	91.68	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures

Correlations

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/(T + C)
Coeff. A	1.38484e+01
Coeff. B	-2.76500e+03
Coeff. C	-5.43350e+01
Temperature range (K), min.	258.23
Temperature range (K), max.	378.22

Information	Value
Property code	pvap
Equation	ln(Pvp) = A + B/T + C*ln(T) + D*T^2

Coeff. A	7.56506e+01
Coeff. B	-6.35490e+03
Coeff. C	-9.20098e+00
Coeff. D	7.37481e-06
Temperature range (K), min.	279.69
Temperature range (K), max.	553.54

Datasets

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
303.10	2930.00	0.0008520
305.20	140.00	0.0007960
305.10	960.00	0.0008010
305.20	1960.00	0.0008190
305.20	3940.00	0.0008390
313.80	2920.00	0.0007210
323.70	150.00	0.0006010
324.00	1020.00	0.0006160
323.70	1990.00	0.0006140
323.70	4000.00	0.0006310
348.90	140.00	0.0004320
348.90	990.00	0.0004400
348.90	2080.00	0.0004450
348.90	3030.00	0.0004510
348.90	3930.00	0.0004490
373.70	970.00	0.0003310
373.70	2020.00	0.0003360
373.70	2930.00	0.0003400
373.70	3960.00	0.0003460
398.20	960.00	0.0002580
398.10	2000.00	0.0002620
398.20	2940.00	0.0002660
398.10	4010.00	0.0002700
422.40	960.00	0.0002040
422.50	1970.00	0.0002090
422.50	2960.00	0.0002140
422.50	3960.00	0.0002160

447.50	1010.00	0.0001650
447.60	2040.00	0.0001650
447.70	3010.00	0.0001700
447.70	4000.00	0.0001740
473.40	1930.00	0.0001310
473.30	3000.00	0.0001380
473.40	3930.00	0.0001390
498.20	3020.00	0.0001060
497.90	3050.00	0.0001060
498.10	3980.00	0.0001100
498.30	4020.00	0.0001100
523.00	3050.00	0.0000791
523.00	3970.00	0.0000856

Reference *https://www.doi.org/10.1021/acs.jced.5b00270*

Pressure, kPa	Temperature, K	Viscosity, Pa*s
690.00	313.20	0.0007230
690.00	333.20	0.0005400
690.00	353.20	0.0004240
690.00	373.20	0.0003230
690.00	393.20	0.0002480
5000.00	313.20	0.0007720
5000.00	333.20	0.0005760
5000.00	353.20	0.0004500
5000.00	373.20	0.0003490
5000.00	393.20	0.0002620
10000.00	313.20	0.0008250
10000.00	333.20	0.0006160
10000.00	353.20	0.0004800
10000.00	373.20	0.0003710
10000.00	393.20	0.0002840
20000.00	313.20	0.0009260
20000.00	333.20	0.0006920
20000.00	353.20	0.0005400
20000.00	373.20	0.0004200
20000.00	393.20	0.0003290
30000.00	313.20	0.0010180
30000.00	333.20	0.0007620
30000.00	353.20	0.0005970
30000.00	373.20	0.0004610
30000.00	393.20	0.0003690
40000.00	313.20	0.0011110

40000.00	333.20	0.0008370
40000.00	353.20	0.0006510
40000.00	373.20	0.0005040
40000.00	393.20	0.0004140
50000.00	313.20	0.0012400
50000.00	333.20	0.0009120
50000.00	353.20	0.0007030
50000.00	373.20	0.0005570
50000.00	393.20	0.0004530
60000.00	313.20	0.0013470
60000.00	333.20	0.0009940
60000.00	353.20	0.0007520
60000.00	373.20	0.0006080
60000.00	393.20	0.0004920

Reference *https://www.doi.org/10.1021/je800882f*

Temperature, K	Pressure, kPa	Viscosity, Pa*s
298.15	100.00	0.0008880
298.15	4000.00	0.0009030
298.15	7600.00	0.0009620
298.15	13700.00	0.0010370
298.15	20900.00	0.0011290
298.15	27700.00	0.0012220
298.15	34700.00	0.0013090
318.15	6895.00	0.0006710
318.15	13790.00	0.0007260
318.15	20680.00	0.0007850
318.15	27580.00	0.0008390
318.15	34470.00	0.0009060
318.15	41370.00	0.0009740
318.15	48260.00	0.0010490
318.15	55160.00	0.0011490
318.15	62050.00	0.0012160
323.15	100.00	0.0006060
323.15	7200.00	0.0006670
323.15	14200.00	0.0007210
323.15	21100.00	0.0007760
323.15	27700.00	0.0008350
323.15	40000.00	0.0009520
323.15	48200.00	0.0010350
323.15	50900.00	0.0010610
323.15	52300.00	0.0010720

323.15	54300.00	0.0010910
323.15	55000.00	0.0009150
333.15	100.00	0.0005120
333.15	3800.00	0.0005380
333.15	6895.00	0.0005460
333.15	7300.00	0.0005630
333.15	13790.00	0.0005950
333.15	14100.00	0.0006090
333.15	20600.00	0.0006570
333.15	20680.00	0.0006420
333.15	27580.00	0.0006980
333.15	27800.00	0.0007090
333.15	34470.00	0.0007500
333.15	34700.00	0.0007570
333.15	41370.00	0.0008080
333.15	42000.00	0.0008150
333.15	48260.00	0.0008550
333.15	49000.00	0.0008760
333.15	53500.00	0.0009040
333.15	55160.00	0.0009160
333.15	62050.00	0.0009510
348.15	6895.00	0.0004580
348.15	13790.00	0.0004950
348.15	20680.00	0.0005360
348.15	27580.00	0.0005790
348.15	34470.00	0.0006240
348.15	41370.00	0.0006700
348.15	48260.00	0.0007170
348.15	55160.00	0.0007690
348.15	62050.00	0.0008140
363.15	6895.00	0.0003860
363.15	13790.00	0.0004200
363.15	20680.00	0.0004550
363.15	27580.00	0.0004930
363.15	34470.00	0.0005300
363.15	41370.00	0.0005680
363.15	48260.00	0.0006180
363.15	55160.00	0.0006580
363.15	62050.00	0.0006990
388.15	6895.00	0.0003010
388.15	13790.00	0.0003280
388.15	20680.00	0.0003560
388.15	27580.00	0.0003840
388.15	34470.00	0.0004120

388.15	41370.00	0.0004410
388.15	48260.00	0.0004690
388.15	55160.00	0.0004980
388.15	62050.00	0.0005280
413.15	6895.00	0.0002450
413.15	13790.00	0.0002730
413.15	20680.00	0.0002930
413.15	27580.00	0.0003160
413.15	34470.00	0.0003420
413.15	41370.00	0.0003670
413.15	48260.00	0.0003960
413.15	55160.00	0.0004150
413.15	62050.00	0.0004380

Reference *https://www.doi.org/10.1021/je9000262*

Mass density, kg/m3

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m3 - Liquid
298.15	100.00	773.6

Reference *https://www.doi.org/10.1016/j.fluid.2019.02.006*

Temperature, K	Pressure, kPa	Mass density, kg/m3
293.15	99.46	778.632
293.15	1102.03	779.471
293.15	2002.37	780.22
293.15	4003.86	781.856
293.15	6003.84	783.454
293.15	8003.30	785.025
293.15	10042.20	786.595
293.15	12045.50	788.105
293.15	13918.70	789.495
293.15	15982.40	790.995
293.15	17946.40	792.401
293.15	20017.10	793.855
313.15	102.48	759.667
313.15	1139.02	760.675
313.15	2012.18	761.509
313.15	4102.38	763.47

313.15	5932.83	765.157
313.15	7910.50	766.936
313.15	10017.50	768.784
313.15	12069.20	770.545
313.15	13964.70	772.137
313.15	15901.80	773.737
313.15	17955.80	775.394
313.15	20142.40	777.123
333.15	1112.41	741.367
333.15	2043.58	742.401
333.15	3987.96	744.517
333.15	5966.83	746.613
333.15	8141.84	748.853
333.15	10007.20	750.72
333.15	11993.60	752.664
333.15	14092.70	754.666
333.15	15962.90	756.414
333.15	17994.70	758.261
333.15	19860.60	759.929
353.15	1109.91	721.547
353.15	1973.18	722.669
353.15	4000.02	725.242
353.15	6001.27	727.698
353.15	8046.51	730.125
353.15	10046.10	732.423
353.15	11820.50	734.413
353.15	13860.00	736.633
353.15	15939.70	738.835
353.15	18023.40	740.978
353.15	20002.80	742.965
373.15	1115.51	701.065
373.15	1950.06	702.346
373.15	4154.07	705.638
373.15	6126.03	708.455
373.15	8029.39	711.079
373.15	9951.24	713.63
373.15	12097.10	716.383
373.15	13877.00	718.592
373.15	16148.10	721.319
373.15	18077.70	723.568
373.15	19877.00	725.607
393.15	1162.91	679.792
393.15	1960.31	681.265
393.15	3901.42	684.723

393.15	5983.91	688.253
393.15	7986.39	691.487
393.15	9903.28	694.452
393.15	11974.70	697.527
393.15	13821.00	700.163
393.15	16029.30	703.195
393.15	18027.30	705.845
393.15	20003.70	708.371
413.15	1196.72	657.32
413.15	2172.63	659.527
413.15	4146.43	663.767
413.15	6122.26	667.756
413.15	8132.63	671.583
413.15	10013.20	674.989
413.15	11993.30	678.397
413.15	14003.50	681.703
413.15	16052.90	684.936
413.15	18098.20	688.022
413.15	19934.80	690.694
433.15	1086.72	632.817
433.15	2070.58	635.63
433.15	4050.34	640.931
433.15	6077.00	645.937
433.15	8181.71	650.742
433.15	10076.70	654.811
433.15	12111.10	658.913
433.15	13890.30	662.325
433.15	15958.80	666.096
433.15	18073.30	669.76
433.15	20009.80	672.969
453.15	2100.81	609.942
453.15	4117.30	616.844
453.15	6121.33	623.004
453.15	8117.44	628.596
453.15	9915.40	633.254
453.15	11931.40	638.115
453.15	13934.70	642.628
453.15	15959.00	646.918
453.15	18103.10	651.206
453.15	19890.50	654.601
473.15	2403.47	582.448
473.15	3924.93	589.431
473.15	6045.23	597.933
473.15	8093.25	605.148

473.15	9884.30	610.832
473.15	11911.40	616.733
473.15	13942.60	622.171
473.15	16018.50	627.319
473.15	18132.60	632.216
473.15	20025.00	636.335

Reference *https://www.doi.org/10.1016/j.jct.2010.08.010*

Temperature, K	Pressure, kPa	Mass density, kg/m3
288.15	100.00	782.7
288.15	1000.00	783.7
288.15	5000.00	787.0
288.15	10000.00	790.7
288.15	15000.00	794.1
298.15	100.00	773.2
298.15	1000.00	774.0
298.15	5000.00	777.6
298.15	10000.00	781.8
298.15	15000.00	785.6
298.15	20000.00	789.3
298.15	25000.00	792.9
298.15	30000.00	796.8
298.15	35000.00	799.7
308.15	100.00	763.6
308.15	1000.00	764.5
308.15	5000.00	768.2
308.15	10000.00	772.6
308.15	15000.00	776.8
308.15	20000.00	780.8
308.15	25000.00	784.6
308.15	30000.00	788.3
308.15	35000.00	791.8
308.15	40000.00	795.2
318.15	100.00	754.0
318.15	1000.00	755.0
318.15	5000.00	759.0
318.15	10000.00	763.7
318.15	15000.00	767.9
318.15	20000.00	772.4
318.15	25000.00	776.4
318.15	30000.00	780.3
318.15	35000.00	784.1

318.15	40000.00	787.7
318.15	45000.00	791.1
318.15	50000.00	794.4
328.15	100.00	744.4
328.15	1000.00	745.4
328.15	5000.00	749.7
328.15	10000.00	754.7
328.15	15000.00	759.5
328.15	20000.00	764.0
328.15	25000.00	768.2
328.15	30000.00	772.3
328.15	35000.00	776.1
328.15	40000.00	779.9
328.15	45000.00	783.5
328.15	50000.00	787.0
338.15	100.00	734.5
338.15	1000.00	735.6
338.15	5000.00	740.2
338.15	10000.00	745.7
338.15	15000.00	750.7
338.15	20000.00	755.5
338.15	25000.00	760.0
338.15	30000.00	764.3
338.15	35000.00	768.4
338.15	40000.00	772.3
338.15	45000.00	776.0
338.15	50000.00	779.7
338.15	55000.00	783.2
348.15	100.00	724.6
348.15	1000.00	725.7
348.15	5000.00	730.8
348.15	10000.00	736.5
348.15	15000.00	741.9
348.15	20000.00	747.0
348.15	25000.00	751.7
348.15	30000.00	756.2
348.15	35000.00	760.5
348.15	40000.00	764.6
348.15	45000.00	768.6
348.15	50000.00	772.3
348.15	55000.00	776.0
358.15	100.00	714.3
358.15	1000.00	715.6
358.15	5000.00	720.9

358.15	10000.00	727.2
358.15	15000.00	732.9
358.15	20000.00	738.3
358.15	25000.00	743.3
358.15	30000.00	748.1
358.15	35000.00	752.6
358.15	40000.00	757.0
358.15	45000.00	761.1
358.15	50000.00	765.0
358.15	55000.00	768.9

Reference *https://www.doi.org/10.1016/j.jct.2011.02.008*

Temperature, K	Pressure, kPa	Mass density, kg/m3
283.15	100.00	788.0
283.15	1000.00	788.7
283.15	2000.00	789.5
283.15	5000.00	791.8
293.15	100.00	778.8
293.15	1000.00	779.5
293.15	2000.00	780.4
293.15	5000.00	782.8
293.15	10000.00	786.6
293.15	15000.00	790.4
293.15	20000.00	793.9
313.15	100.00	759.8
313.15	1000.00	760.6
313.15	2000.00	761.5
313.15	5000.00	764.4
313.15	10000.00	768.7
313.15	15000.00	772.9
313.15	20000.00	776.9
333.15	100.00	740.5
333.15	1000.00	741.5
333.15	2000.00	742.6
333.15	5000.00	745.8
333.15	10000.00	750.9
333.15	15000.00	755.6
333.15	20000.00	760.1

Reference *https://www.doi.org/10.1016/j.jct.2012.07.018*

Temperature, K	Pressure, kPa	Mass density, kg/m3

293.15	100.00	778.4
293.15	1000.00	779.1
293.15	2000.00	779.9
293.15	5000.00	782.4
293.15	10000.00	786.3
293.15	15000.00	789.9
293.15	20000.00	793.4
303.15	100.00	769.0
303.15	1000.00	769.8
303.15	2000.00	770.7
303.15	5000.00	773.3
303.15	10000.00	777.5
303.15	15000.00	781.3
303.15	20000.00	785.1
303.15	30000.00	792.1
303.15	40000.00	798.5
313.15	100.00	759.7
313.15	1000.00	760.3
313.15	2000.00	761.2
313.15	5000.00	764.0
313.15	10000.00	768.4
313.15	15000.00	772.6
313.15	20000.00	776.6
313.15	30000.00	784.1
313.15	40000.00	790.9
323.15	100.00	750.1
323.15	1000.00	750.8
323.15	2000.00	751.8
323.15	5000.00	754.8
323.15	10000.00	759.5
323.15	15000.00	763.9
323.15	20000.00	768.2
323.15	30000.00	776.1
323.15	40000.00	783.2
333.15	100.00	740.3
333.15	1000.00	741.1
333.15	2000.00	742.2
333.15	5000.00	745.5
333.15	10000.00	750.5
333.15	15000.00	755.3
333.15	20000.00	759.7
333.15	30000.00	768.1
333.15	40000.00	775.6

Temperature, K	Pressure, kPa	Mass density, kg/m3
318.15	6895.00	761.5
318.15	13789.00	767.7
318.15	20684.00	773.8
318.15	27579.00	779.0
318.15	34474.00	784.1
318.15	41369.00	788.7
318.15	48263.00	793.4
318.15	55158.00	797.4
318.15	62053.00	801.4
333.15	6895.00	747.3
333.15	13789.00	754.1
333.15	20684.00	760.5
333.15	27579.00	766.5
333.15	34474.00	772.0
333.15	41369.00	777.0
333.15	48263.00	781.7
333.15	55158.00	786.3
333.15	62053.00	790.7
348.15	6895.00	733.6
348.15	13789.00	741.2
348.15	20684.00	748.2
348.15	27579.00	754.5
348.15	34474.00	760.5
348.15	41369.00	766.1
348.15	48263.00	771.4
348.15	55158.00	776.2
348.15	62053.00	781.1
363.15	6895.00	719.6
363.15	13789.00	727.9
363.15	20684.00	735.7
363.15	27579.00	742.8
363.15	34474.00	749.1
363.15	41369.00	755.3
363.15	48263.00	760.7
363.15	55158.00	765.8
363.15	62053.00	771.0
388.15	6895.00	694.7
388.15	13789.00	705.0
388.15	20684.00	713.9

388.15	27579.00	721.9
388.15	34474.00	729.2
388.15	41369.00	736.0
388.15	48263.00	742.2
388.15	55158.00	747.8
388.15	62053.00	753.2
413.15	6895.00	669.7
413.15	13789.00	682.1
413.15	20684.00	692.5
413.15	27579.00	701.8
413.15	34474.00	710.1
413.15	41369.00	717.7
413.15	48263.00	724.9
413.15	55158.00	731.2
413.15	62053.00	737.2

Reference *https://www.doi.org/10.1021/je0605036*

Sources

VLE and LLE Data for the System Cyclohexane + Cyclohexene + Water + Cyclohexanol:	https://www.doi.org/10.1021/je049902w
Densities, Viscosities, and Refractive Indices of Mixtures of Hexane with Cyclohexane, Decane, Hexadecane, and Squalane at 298.15K:	https://www.doi.org/10.1007/s10765-005-5572-8
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Hydroxymethylphenylphosphinic Acid, (Hydroxymethyl)phenylphosphinic Acid, p-Methoxyphenylphosphinic Acid, and Phenylphosphinic Acid:	https://www.doi.org/10.1021/je050377q
Liquid–Liquid Equilibria of (Heptane, or Hexane, or Cyclohexane + Toluene + 1-Ethyl-3-methylimidazolium acetate) Ternary Systems at T = 298.15 K:	https://www.doi.org/10.1016/j.jct.2009.11.009
Solubilities of some organic solutes in 1-butyl-3-methylimidazolium methylsulfate, and enthalpies of dissolution of hydroxymethylphenylphosphinic acid, (hydroxymethyl)phenylphosphinic acid, and phenylphosphinic acid:	https://www.doi.org/10.1016/j.jct.2011.11.005
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Bubble Temperature Measurements on Binary Mixtures Formed by Cyclohexane at 54.7 kPa:	https://www.doi.org/10.1021/je201129y
Solubility Measurement and Correlation for Cyclohexane-2,4,6,8,10,12-hexaazaisowurtzitane:	https://www.doi.org/10.1021/je020148t
Determination and Correlation for the Solubilities of Succinic Acid in Solvent + Water Mixtures:	https://www.doi.org/10.1021/acs.jced.8b00353
Solubility and solution thermodynamics of 2,4,6,8,10,12-hexanitrohexaazaisowurtzitane (CL-20) in ten organic solvents at elevated temperatures:	https://www.doi.org/10.1021/acs.jced.7b00956
Solubilities of Alkanes, Aromatic Hydrocarbon + Ethyl Acetate Binary Mixtures at Different Temperatures:	https://www.doi.org/10.1016/j.jct.2016.05.027
Solubility of 2-methyl-3-nitroaniline in ten organic solvents at 283.15 to 323.15 K and thermodynamic properties of mixtures containing:	https://www.doi.org/10.1016/j.jct.2014.01.002
Measurement of Activity Coefficients of Solutes at Infinite Dilution in (Dimethyl Sulfoxide + Hexane, or Octane, or Decane, or Dodecane) at T = 298.15 K:	https://www.doi.org/10.1021/je030122h
2-methoxy-2-methylpropane, alkanol, alkane:	https://www.doi.org/10.1016/j.jct.2014.07.016
Pressure-dependent density of N,N-dimethylacetamide, or N,N-dimethylformamide, or benzyl benzoate, or (benzene, or cyclohexane) at T = (293.15 to 313.15) K:	https://www.doi.org/10.1016/j.tca.2017.12.010
A new analysis method for improving calorimetric and liquid equilibrium (VLE) data of binary mixtures using differential scanning calorimetry (DSC):	
Chromatography at the Temperature Boiling of the Liquid Phase (303.15 K, 313.15 K, and 323.15 K) and p (5 to 15) MPa:	

Excess Gibbs Energies of the Ternary System 2-Methoxyethanol + Tetrahydrofuran + Cyclohexane and Different Binary Solvents from (298.15 to 349.15) K:	https://www.doi.org/10.1021/je100556t
Solubility of Losartan Potassium in Different Binary Solvents from (298.15 to 349.15) K:	https://www.doi.org/10.1021/je700724r
Liquid−Liquid Extraction of Aromatic Compounds from Cycloalkanes Using Ternary Liquid−Liquid Equilibria	https://www.doi.org/10.1021/je300826t
1-Butyl-3-methylimidazolium Methylsulfate Ionic Liquid:	https://www.doi.org/10.1021/je800376f
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Liquid–Liquid Equilibrium Data for the	https://www.doi.org/10.1016/j.jct.2005.02.006
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Viscometric (2) + n-alkanes (3)} at T = 298.15 K: Measurements and Correlation	https://www.doi.org/10.1021/je900050z
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Measurements of Activity Coefficients	https://www.doi.org/10.1021/je101008y
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(Dortmund):	

Legend

af:	Acentric Factor
affp:	Proton affinity
aigt:	Autoignition Temperature
ap:	Aniline Point
basg:	Gas basicity
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity

dm:	Dipole Moment
dvisc:	Dynamic viscosity
fll:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hcg:	Heat of Combustion, Gross form
hcn:	Heat of Combustion, Net Form
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hsubt:	Enthalpy of sublimation at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
nfpah:	NFPA Health Rating
pc:	Critical Pressure
pt:	Triple Point Pressure
pvap:	Vapor pressure
rfi:	Refractive Index
rhoc:	Critical density
rhol:	Liquid Density
rinpol:	Non-polar retention indices
ripol:	Polar retention indices
sdco:	Self diffusion coefficient
sfust:	Entropy of fusion at a given temperature
sg:	Molar entropy at standard conditions
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
svapt:	Entropy of vaporization at a given temperature
tb:	Normal Boiling Point Temperature
tbp:	Boiling point at given pressure
tc:	Critical Temperature
tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature

vc:	Critical Volume
volm:	Molar Volume
zc:	Critical Compressibility
zra:	Rackett Parameter