Ethyl hydrogen succinate

Other names: 4-ethoxy-4-oxobutanoic acid

Butanedioic acid, 1-ethyl ester Butanedioic acid, monoethyl ester

Monoethyl butanedioate

Succinic acid monoethyl ester

monoethyl succinate

InChi=1S/C6H10O4/c1-2-10-6(9)4-3-5(7)8/h2-4H2,1H3,(H,7,8)

InchiKey: LOLKAJARZKDJTD-UHFFFAOYSA-N

Formula: C6H10O4

SMILES: CCOC(=O)CCC(=O)O

Mol. weight [g/mol]: 146.14 CAS: 1070-34-4

Physical Properties

Property code	Value	Unit	Source
gf	-500.02	kJ/mol	Joback Method
hf	-676.78	kJ/mol	Joback Method
hfus	19.77	kJ/mol	Joback Method
hvap	61.53	kJ/mol	Joback Method
log10ws	-0.30		Crippen Method
logp	0.414		Crippen Method
mcvol	110.280	ml/mol	McGowan Method
рс	3940.66	kPa	Joback Method
ripol	2395.00		NIST Webbook
ripol	2350.00		NIST Webbook
ripol	2368.00		NIST Webbook
ripol	2367.00		NIST Webbook
tb	559.02	K	Joback Method
tc	738.59	K	Joback Method
tf	340.29	K	Joback Method
VC	0.420	m3/kmol	Joback Method

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source	
cpg	257.90	J/mol×K	559.02	Joback Method	
cpg	266.10	J/mol×K	588.95	Joback Method	
cpg	273.95	J/mol×K	618.88	Joback Method	
cpg	281.47	J/mol×K	648.80	Joback Method	
cpg	288.64	J/mol×K	678.73	Joback Method	
cpg	295.48	J/mol×K	708.66	Joback Method	
cpg	301.97	J/mol×K	738.59	Joback Method	
dvisc	0.0052745	Paxs	340.29	Joback Method	
dvisc	0.0021175	Paxs	376.75	Joback Method	
dvisc	0.0009987	Paxs	413.20	Joback Method	
dvisc	0.0005320	Paxs	449.65	Joback Method	
dvisc	0.0003115	Pa×s	486.11	Joback Method	
dvisc	0.0001965	Paxs	522.56	Joback Method	
dvisc	0.0001317	Paxs	559.02	Joback Method	
pvap	10.13	kPa	454.70	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	2.09	kPa	421.20	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	2.59	kPa	425.10	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	3.09	kPa	428.50	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	3.60	kPa	433.00	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	4.10	kPa	435.60	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	4.60	kPa	436.70	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	5.10	kPa	439.80	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	5.61	kPa	440.30	Phase equilibria in binary mixtures with monoethyl succinate	

pvap	6.11	kPa	443.00	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	6.61	kPa	444.30	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	7.11	kPa	445.90	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	7.61	kPa	447.60	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	8.12	kPa	449.10	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	8.62	kPa	450.50	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	9.12	kPa	452.10	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	9.62	kPa	453.20	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	1.59	kPa	417.70	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	10.63	kPa	455.70	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	11.13	kPa	456.50	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	11.63	kPa	457.20	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	12.14	kPa	458.20	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	12.64	kPa	458.40	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	13.14	kPa	459.80	Phase equilibria in binary mixtures with monoethyl succinate	

pvap 13.64 kPa 460.10 Phase equilibria in binary mixtures with monoethyl succinate pvap 14.14 kPa 460.30 Phase equilibria in binary mixtures with monoethyl succinate pvap 14.65 kPa 461.10 Phase equilibria in binary mixtures with monoethyl succinate pvap 15.15 kPa 462.00 Phase equilibria in binary mixtures with monoethyl succinate pvap 15.65 kPa 463.30 Phase equilibria in binary mixtures with monoethyl succinate pvap 16.15 kPa 463.80 Phase equilibria in binary mixtures with monoethyl succinate pvap 16.15 kPa 463.80 Phase equilibria in binary mixtures with monoethyl succinate pvap 16.15 kPa 463.80 Phase equilibria in binary mixtures with monoethyl succinate	
in binary mixtures with monoethyl succinate pvap 14.65 kPa 461.10 Phase equilibria in binary mixtures with monoethyl succinate pvap 15.15 kPa 462.00 Phase equilibria in binary mixtures with monoethyl succinate pvap 15.65 kPa 463.30 Phase equilibria in binary mixtures with monoethyl succinate pvap 16.15 kPa 463.80 Phase equilibria in binary mixtures with monoethyl succinate pvap 16.15 kPa 463.80 Phase equilibria in binary mixtures with monoethyl succinate	
pvap 15.15 kPa 462.00 Phase equilibria in binary mixtures with monoethyl succinate pvap 15.65 kPa 463.30 Phase equilibria in binary mixtures with monoethyl succinate pvap 15.65 kPa 463.30 Phase equilibria in binary mixtures with monoethyl succinate pvap 16.15 kPa 463.80 Phase equilibria in binary mixtures with monoethyl succinate	
pvap 15.65 kPa 463.30 Phase equilibria in binary mixtures with monoethyl succinate pvap 16.15 kPa 463.80 Phase equilibria in binary mixtures with monoethyl succinate pvap 16.15 kPa 463.80 Phase equilibria in binary mixtures with monoethyl	
pvap 16.15 kPa 463.80 Phase equilibria in binary mixtures with monoethyl succinate pvap with monoethyl succinate in binary mixtures with monoethyl	
in binary mixtures with monoethyl	
pvap 16.66 kPa 464.20 Phase equilibria in binary mixtures with monoethyl succinate	
pvap 17.16 kPa 464.50 Phase equilibria in binary mixtures with monoethyl succinate	
pvap 17.66 kPa 465.20 Phase equilibria in binary mixtures with monoethyl succinate	
pvap 18.16 kPa 465.80 Phase equilibria in binary mixtures with monoethyl succinate	
pvap 18.67 kPa 466.70 Phase equilibria in binary mixtures with monoethyl succinate	
pvap 19.17 kPa 467.30 Phase equilibria in binary mixtures with monoethyl succinate	
pvap 19.67 kPa 467.80 Phase equilibria in binary mixtures with monoethyl succinate	
pvap 20.17 kPa 468.30 Phase equilibria in binary mixtures with monoethyl succinate	

pvap	20.67	kPa	468.80	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	21.18	kPa	469.50	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	21.68	kPa	469.70	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	22.18	kPa	469.80	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	22.68	kPa	470.10	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	23.19	kPa	470.30	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	23.69	kPa	470.40	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	24.19	kPa	470.50	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	24.69	kPa	471.10	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	25.20	kPa	471.40	Phase equilibria in binary mixtures with monoethyl succinate	
pvap	25.70	kPa	471.90	Phase equilibria in binary mixtures with monoethyl succinate	

Sources

Phase equilibria in binary mixtures with https://www.doi.org/10.1016/j.fluid.2011.06.020 monoethyl succinate:
Joback Method: https://en.wikipedia.org/wiki/Joback_method

McGowan Method: http://link.springer.com/article/10.1007/BF02311772

NIST Webbook: http://webbook.nist.gov/cgi/cbook.cgi?ID=C1070344&Units=SI

Crippen Method: http://pubs.acs.org/doi/abs/10.1021/ci990307l

Crippen Method: https://www.chemeo.com/doc/models/crippen_log10ws

Legend

cpg: Ideal gas heat capacity

dvisc: Dynamic viscosity

gf: Standard Gibbs free energy of formationhf: Enthalpy of formation at standard conditionshfus: Enthalpy of fusion at standard conditions

hvap: Enthalpy of vaporization at standard conditions

log10ws: Log10 of Water solubility in mol/llogp: Octanol/Water partition coefficientmcvol: McGowan's characteristic volume

pc: Critical Pressurepvap: Vapor pressure

ripol: Polar retention indices

tb: Normal Boiling Point Temperature

tc: Critical Temperature

tf: Normal melting (fusion) point

vc: Critical Volume

Latest version available from:

https://www.chemeo.com/cid/67-736-1/Ethyl-hydrogen-succinate.pdf

Generated by Cheméo on 2025-12-05 13:33:20.09739744 +0000 UTC m=+4689797.627438104.

Cheméo (https://www.chemeo.com) is the biggest free database of chemical and physical data for the process industry.