

# Acetic acid, hexyl ester

<b>Other names:</b>	1-HEXYL ACETATE Acetic acid n-hexyl ester FEMA No. 2565 Hexyl acetate Hexyl alcohol, acetate Hexyl ester of acetic acid Hexyl ethanoate Hexylester kyseliny octove N-HEXYL ACETATE N-HEXYL ETHANOATE NSC 7323 ethanoic acid, hexyl ester
<b>Inchi:</b>	InChI=1S/C8H16O2/c1-3-4-5-6-7-10-8(2)9/h3-7H2,1-2H3
<b>InchiKey:</b>	AOGQPLXWSUTHQB-UHFFFAOYSA-N
<b>Formula:</b>	C8H16O2
<b>SMILES:</b>	CCCCCOC(C)=O
<b>Mol. weight [g/mol]:</b>	144.21
<b>CAS:</b>	142-92-7

## Physical Properties

Property code	Value	Unit	Source
gf	-217.44	kJ/mol	Joback Method
hf	-453.25	kJ/mol	Joback Method
hfus	19.26	kJ/mol	Joback Method
hvap	52.10	kJ/mol	NIST Webbook
hvap	51.90 ± 0.30	kJ/mol	NIST Webbook
log10ws	-2.46		Aqueous Solubility Prediction Method
logp	2.130		Crippen Method
mcvol	131.020	ml/mol	McGowan Method
nfpaf	%!d(float64=2)		KDB
nfpah	%!d(float64=1)		KDB
pc	2657.03	kPa	Joback Method
rinpol	995.00		NIST Webbook
rinpol	1008.70		NIST Webbook
rinpol	1008.00		NIST Webbook
rinpol	1008.00		NIST Webbook

rinpol	993.00	NIST Webbook
rinpol	1000.00	NIST Webbook
rinpol	1006.00	NIST Webbook
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tb	444.63	K	KDB
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tb	442.20	K	NIST Webbook
tb	442.00	K	NIST Webbook
tb	464.00 ± 2.00	K	NIST Webbook
tb	442.40 ± 1.50	K	NIST Webbook
tb	429.15 ± 3.00	K	NIST Webbook
tb	444.63 ± 0.30	K	NIST Webbook
tb	441.00 ± 4.00	K	NIST Webbook
tc	633.80	K	Joback Method
tf	212.25	K	KDB
tf	192.85	K	Aqueous Solubility Prediction Method
tf	212.10 ± 0.05	K	NIST Webbook
tf	192.30 ± 0.50	K	NIST Webbook
vc	0.507	m <sup>3</sup> /kmol	Joback Method

## Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	346.77	J/mol×K	633.80	Joback Method

cpg	279.70	J/molxK	458.73	Joback Method
cpg	291.94	J/molxK	487.91	Joback Method
cpg	303.75	J/molxK	517.09	Joback Method
cpg	326.10	J/molxK	575.44	Joback Method
cpg	336.64	J/molxK	604.62	Joback Method
cpg	315.14	J/molxK	546.26	Joback Method
dvisc	0.0007820	Paxs	318.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0009620	Paxs	303.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0011180	Paxs	293.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0007330	Paxs	323.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0005790	Paxs	343.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0006890	Paxs	328.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0006490	Paxs	333.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0006120	Paxs	338.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0008360	Paxs	313.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters

dvisc	0.0010360	Paxs	298.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
dvisc	0.0008950	Paxs	308.15	Density and Viscosity Correlation for Several Common Fragrance and Flavor Esters
hfust	19.83	kJ/mol	212.10	NIST Webbook
hfust	19.83	kJ/mol	212.10	NIST Webbook
hvapt	46.20	kJ/mol	418.50	NIST Webbook
hvapt	48.90	kJ/mol	342.50	NIST Webbook
hvapt	50.90	kJ/mol	373.50	NIST Webbook
pvap	55.00	kPa	422.59	Phase Equilibria for Hexyl Acetate Reactive Distillation
pvap	50.00	kPa	419.47	Phase Equilibria for Hexyl Acetate Reactive Distillation
pvap	60.00	kPa	425.57	Phase Equilibria for Hexyl Acetate Reactive Distillation
pvap	65.00	kPa	428.26	Phase Equilibria for Hexyl Acetate Reactive Distillation
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pvap	80.00	kPa	435.68	Phase Equilibria for Hexyl Acetate Reactive Distillation
pvap	85.00	kPa	437.92	Phase Equilibria for Hexyl Acetate Reactive Distillation
pvap	90.00	kPa	439.98	Phase Equilibria for Hexyl Acetate Reactive Distillation
pvap	40.00	kPa	412.14	Phase Equilibria for Hexyl Acetate Reactive Distillation

pvap	35.00	kPa	408.02	Phase Equilibria for Hexyl Acetate Reactive Distillation
pvap	30.00	kPa	403.36	Phase Equilibria for Hexyl Acetate Reactive Distillation
pvap	25.00	kPa	397.97	Phase Equilibria for Hexyl Acetate Reactive Distillation
pvap	0.33	kPa	309.10	Vapour pressures and enthalpies of vaporization of a series of the linear n-alkyl acetates
pvap	0.27	kPa	306.10	Vapour pressures and enthalpies of vaporization of a series of the linear n-alkyl acetates
pvap	0.23	kPa	303.10	Vapour pressures and enthalpies of vaporization of a series of the linear n-alkyl acetates
pvap	0.18	kPa	300.00	Vapour pressures and enthalpies of vaporization of a series of the linear n-alkyl acetates
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pvap	0.10	kPa	291.90	Vapour pressures and enthalpies of vaporization of a series of the linear n-alkyl acetates

pvap	0.08	kPa	289.90	Vapour pressures and enthalpies of vaporization of a series of the linear n-alkyl acetates
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pvap	0.05	kPa	283.80	Vapour pressures and enthalpies of vaporization of a series of the linear n-alkyl acetates
pvap	0.03	kPa	274.50	Vapour pressures and enthalpies of vaporization of a series of the linear n-alkyl acetates
pvap	0.03	kPa	277.70	Vapour pressures and enthalpies of vaporization of a series of the linear n-alkyl acetates
pvap	75.00	kPa	433.38	Phase Equilibria for Hexyl Acetate Reactive Distillation
pvap	0.04	kPa	280.80	Vapour pressures and enthalpies of vaporization of a series of the linear n-alkyl acetates
rfi	1.40960		293.15	Liquid-liquid equilibria study of the (water + phosphoric acid + hexyl or cyclohexyl acetate) systems at T = (298.15, 308.15, and 318.15) K: Measurement and thermodynamic modelling

rho1	855.00	kg/m3	313.15	Densities, Viscosities, and Sound Speed of Binary Mixtures of Hexyl Acetate with Tetrahydrofuran, 1,4-Dioxane, Anisole, and Butyl Vinyl Ether
rho1	859.80	kg/m3	308.15	Densities, Viscosities, and Sound Speed of Binary Mixtures of Hexyl Acetate with Tetrahydrofuran, 1,4-Dioxane, Anisole, and Butyl Vinyl Ether
rho1	863.90	kg/m3	303.15	Densities, Viscosities, and Sound Speed of Binary Mixtures of Hexyl Acetate with Tetrahydrofuran, 1,4-Dioxane, Anisole, and Butyl Vinyl Ether
rho1	868.30	kg/m3	298.15	Densities, Viscosities, and Sound Speed of Binary Mixtures of Hexyl Acetate with Tetrahydrofuran, 1,4-Dioxane, Anisole, and Butyl Vinyl Ether
rho1	868.52	kg/m3	298.15	Experimental and theoretical study of surface tension of binary mixtures of (n-alkyl acetates + heptane, benzene, and toluene)
rho1	868.52	kg/m3	298.15	Surface Tension and Surface Properties of Binary Mixtures of 1,4-Dioxane or N,N-Dimethyl Formamide with n-Alkyl Acetates

# Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.54294e+01
Coeff. B	-4.08917e+03
Coeff. C	-6.47630e+01
Temperature range (K), min.	334.82
Temperature range (K), max.	468.91

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C \cdot \ln(T) + D \cdot T^2$
Coeff. A	8.03443e+01
Coeff. B	-8.74286e+03
Coeff. C	-9.31977e+00
Coeff. D	3.93049e-06
Temperature range (K), min.	192.25
Temperature range (K), max.	618.00

# Sources

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# Legend

<b>cpg:</b>	Ideal gas heat capacity
<b>dvisc:</b>	Dynamic viscosity
<b>gf:</b>	Standard Gibbs free energy of formation
<b>hf:</b>	Enthalpy of formation at standard conditions
<b>hfus:</b>	Enthalpy of fusion at standard conditions
<b>hfust:</b>	Enthalpy of fusion at a given temperature
<b>hvap:</b>	Enthalpy of vaporization at standard conditions
<b>hvapt:</b>	Enthalpy of vaporization at a given temperature
<b>log10ws:</b>	Log10 of Water solubility in mol/l
<b>logp:</b>	Octanol/Water partition coefficient
<b>mcvol:</b>	McGowan's characteristic volume
<b>nfpaf:</b>	NFPA Fire Rating
<b>nfpah:</b>	NFPA Health Rating
<b>pc:</b>	Critical Pressure
<b>pvap:</b>	Vapor pressure
<b>rfi:</b>	Refractive Index
<b>rho:</b>	Liquid Density
<b>rinpol:</b>	Non-polar retention indices
<b>ripol:</b>	Polar retention indices
<b>tb:</b>	Normal Boiling Point Temperature
<b>tc:</b>	Critical Temperature
<b>tf:</b>	Normal melting (fusion) point
<b>vc:</b>	Critical Volume

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